

# Course ME1100 (Module 3)

(Thermodynamics)

# Course Grading and Exam Timing:

- Assignments: 40%
- Quizzes: 60%
  - 4 Quizzes and best 3 will be considered
- Quiz 3: 23<sup>rd</sup> june
- Quiz 4:

# Ideal Gas

## Part 1

# Ideal Gases & Ideal Gas Mixtures

- **Properties of ideal gas-**

1. collisions between all molecules are perfectly elastic.
2. attractive (Van der Waals) forces between molecules are negligible.
3. An ideal gas follows the Boyle's and Charles' laws.

# Boyle's and Charles' laws

- **Boyle's Law-**

$V \propto 1/p$  at constant Temp.

- **Charles' law-**

$V \propto T$  at constant P.

# Ideal gas equation

- $PV=nRT$  where  $R= 8.314J/(Kmol)$

$R=(\text{Universal gas constant})$

- $PV=mR_1T$  where  $R_1= R/M,$

$R_1= (\text{Specific gas constant})$

$M= \text{molecular weight of the gas (kg/kmol)}$

# Joule's Experiment

- Joule's experiments proved that internal energy of an ideal gas depends on temperature alone.

=> If change in  $T=0$

Then change in  $U$ (internal energy) will be zero.

# Internal energy of a gas( $U$ )

- $U_1 = (1/2)kT$  where  $k$  is Boltzmann Constant  
and  $k = 1.38 \times 10^{-26} \text{ kJ/K}$   
 $k = R/N_A$  where  $N_A$ —Avogadro Number
- Total degrees of freedom =  $D$   
 $U_1(\text{per molecule}) = (1/2)kTD$
- Molar internal energy( $U$ ) =  $(D/2)RT$



- Molar enthalpy =  $H = ((D+2)/2) RT$

We can write-

$$dH = ((D+2)/2) R dT, \text{ where } C_p = ((D+2)/2) R$$

And

$$dU = (D/2) R dT, \text{ where } C_v = (D/2) R$$

And

$$\gamma = C_p / C_v = (D+2) / D$$

# Ideal Gas Mixture

- Consider a mixture of  $N$  constituents
- Number of moles of each species in mixture are  $n_1, n_2, \dots, n_N$
- Mass of each species are  $m_1, m_2, \dots, m_N$

So, Total number of moles  $n = n_1 + n_2 + \dots + n_N$

And Total mass  $m = m_1 + m_2 + \dots + m_N$

- Mole fraction =  $x_i = \mathbf{n_i/n}$
- Mass fraction =  $y_i = \mathbf{m_i/m}$

## Conversion of Mole fraction to Mass fraction

Mass fraction  $\mathbf{y_i = (x_i M_i) / M}$

where  $\mathbf{x_i}$  = mole fraction

$\mathbf{M_i}$  = molecular weight of  $i^{\text{th}}$  species

$\mathbf{M}$  = molecular weight of all species

# partial volume and partial pressure

- ***Dalton's law***

$$pV = nRT$$

*If partial pressures are  $p_1, p_2, p_3, \dots$*

$$\text{Then } x_i = n_i/n = p_i/p$$

- ***Amagat's law***

$$pV = nRT$$

*if partial volumes are  $v_1, v_2, v_3, \dots$*

$$\text{Then } x_i = n_i/n = V_i/V$$

# ***Properties of the mixture evaluated by mass basis or mole basis approach***

- ***Mass basis approach***

- Internal energy  $U = mu = m_1u_1 + m_2u_2 + \dots$

- Where  $u = y_1u_1 + y_2u_2 + y_3u_3 + \dots$

- Enthalpy  $H = mh = m_1h_1 + m_2h_2 + \dots$

- Where  $h = y_1h_1 + y_2h_2 + y_3h_3 + \dots$

- Volume  $v = V/m = y_1v_1 + y_2v_2 + y_3v_3 + \dots$

- ***Mole basis approach***

- Replace  $y_i$  by  $x_i$  and apply same approach as mass basis approach

# Gas constant of a mixture

- $R_{mix} = R / M_{mix}$
- $R_{mix} = y_A R_A + y_B R_B + \dots$



# **Second Law of Thermodynamics**

## Part 2



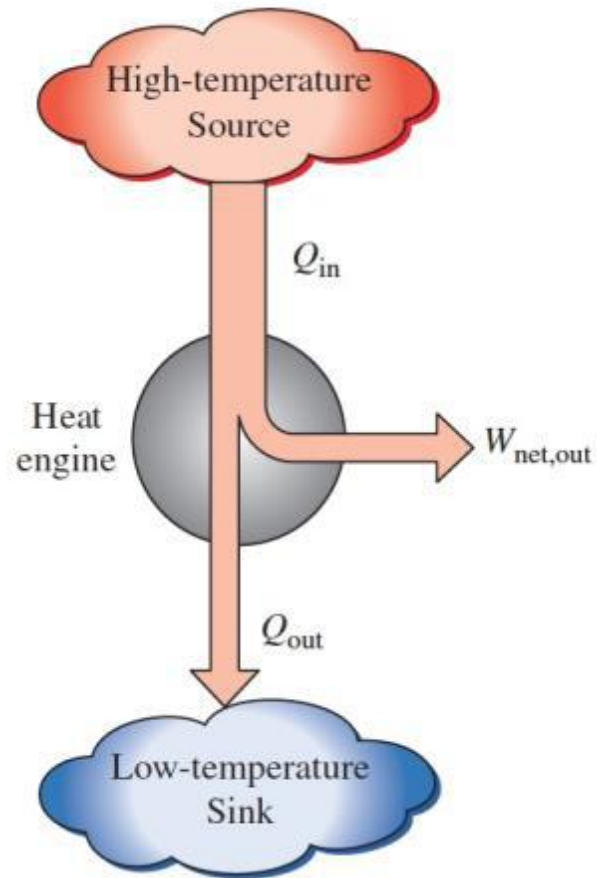
# Introduction to 2<sup>nd</sup> Law

- First Law talks about conservation of energy in terms of its magnitude and not about the direction of energy flow, but 2<sup>nd</sup> law gives nice information regarding energy flow and its magnitude.
- And also it gives the knowledge of efficiency of a system/engine.

# Heat Engines

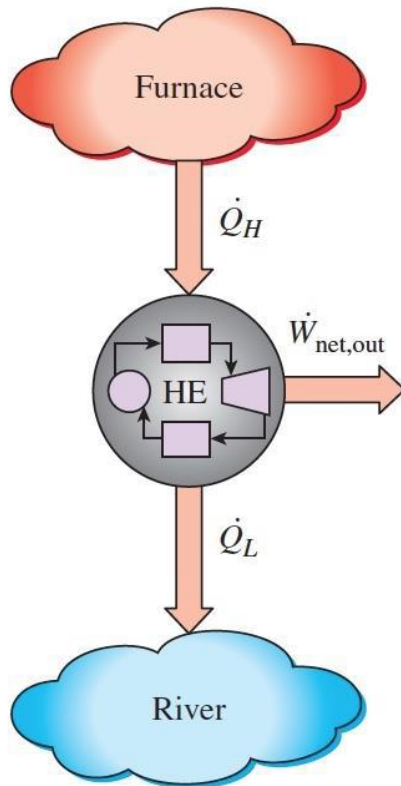
- Heat engine is a continuously operating device and operating in a thermodynamic cycle with heat and work interactions.
- The heat engine receives heat from the source, converts a part of it into work, and rejects the remaining to the sink.

# Heat Engine Layout

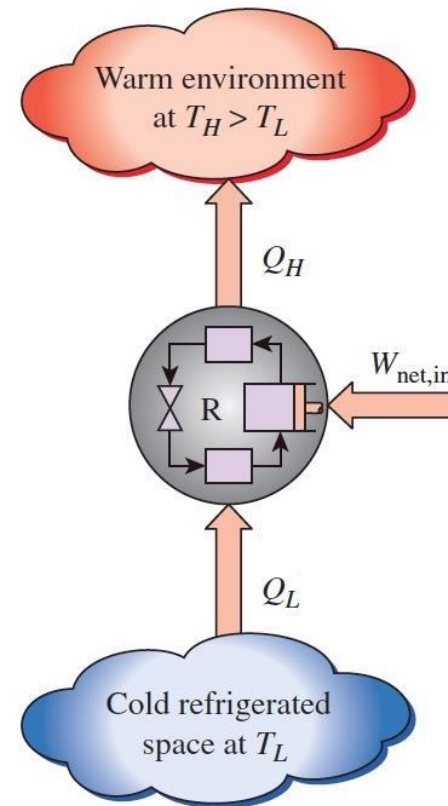


# Direct Engines & Reverse Engines

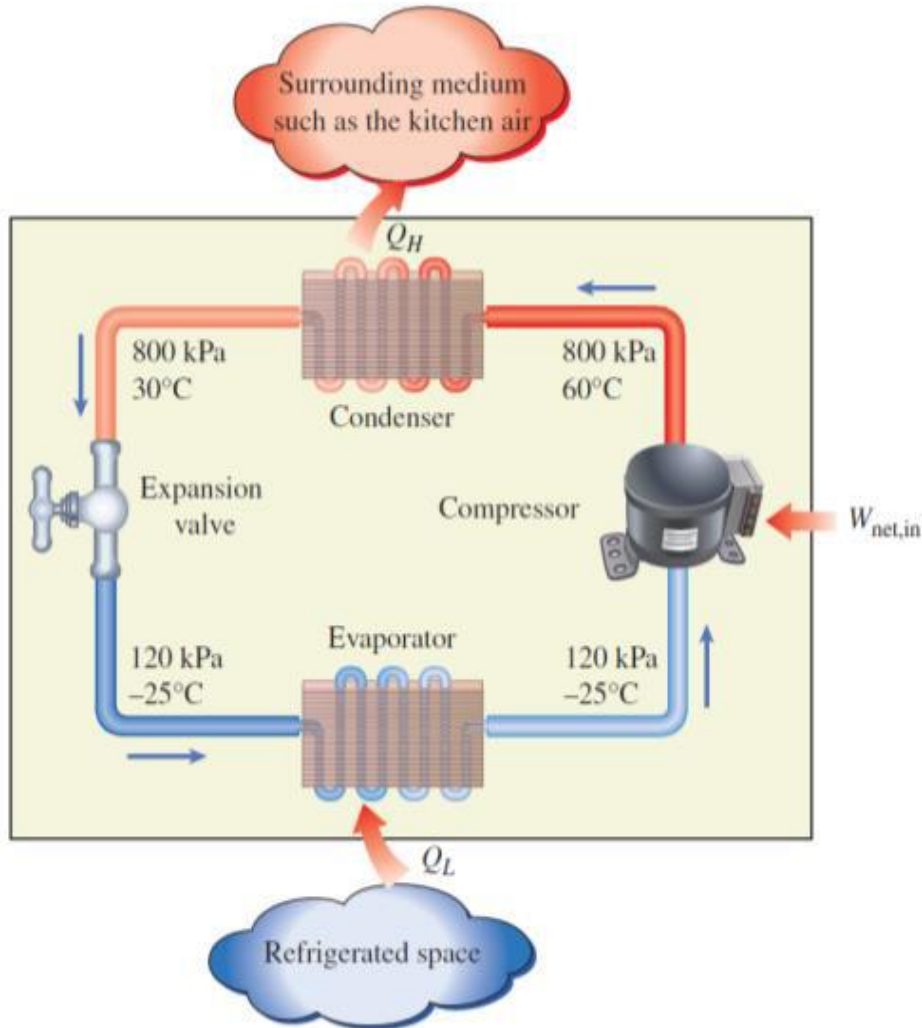
## Direct Engines



## Reverse Engines



# Refrigerator



- In refrigerator the flow of heat is from a low-temperature device to a high-temperature device.

# Quantification of the performance of heat engines

$$\text{Thermal efficiency} = \frac{\text{Net work output}}{\text{Total heat input}}$$

$$\eta_{\text{th}} = \frac{W_{\text{net,out}}}{Q_{\text{in}}}$$

$$W_{\text{net,out}} = Q_H - Q_L$$

$$\eta_{\text{th}} = \frac{W_{\text{net,out}}}{Q_H} \quad \text{or} \quad \eta_{\text{th}} = 1 - \frac{Q_L}{Q_H}$$

# **COP<sub>Ref</sub> and COP<sub>Heat Pump</sub>**

1. If transferred heat is maximum
    - from the lower temp for Reg.
    - from the high temp for heat pump.
  2. And minimize the work output
- ⇒ Then the ratio can exceed 1 and it called  
“Coefficient of Performance”(COP)

# **COP<sub>Ref</sub> and COP<sub>Heat Pump</sub>**

- $COP_{Ref} = (\text{Desired Output} / \text{Required Input}) = Q_L / W_{in}$   
 $COP_{Ref} = Q_L / (Q_H - Q_L)$
- $COP_{HP} = (\text{Desired Output} / \text{Required Input}) = Q_H / W_{in}$   
 $COP_{HP} = Q_H / (Q_H - Q_L)$



# Kelvin-Planck Statement

- It refers to direct engines.
  - It is impossible to construct a device that will operate in a thermodynamic cycle and produce a net amount of work by exchange of heat with a single source.
  - its mean, there two sources are required, and the second one being the sink where some heat is to be rejected.
- => The thermal efficiency of 100% is unachievable.

# Clausius Statement

- It refers to reverse heat engines.
- The main statement is “The reverse engine doesn't operate without external work .”

# Difference Between Reversible and Irreversible Processes

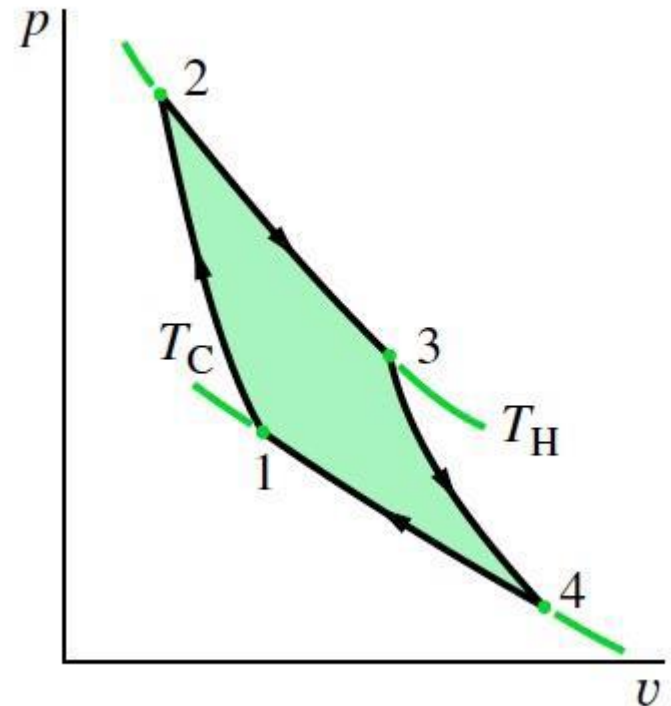
- Main difference—
    - Reversible process delivers the maximum amount of work and consumes the least amount of work.
    - And Irreversible process delivers lesser work and consumes more work.
- ⇒ Therefore, a reversible engine is the best for a given pair of reservoirs (source and sink) rather than irreversible.
- ⇒ All reversible engines have the same and maximum efficiency.

# Carnot Cycle

- All processes are reversible.
- Consists only isothermal and adiabatic process.
- Its efficiency is maximum.

# Carnot Cycle: Representation

- 1-2: Adiabatic compression
- 2-3: Isothermal heat addition from a reservoir at temperature  $T_H$
- 3-4: Adiabatic expansion
- 4-1: Isothermal heat rejection to a reservoir at temperature  $T_C$



# Some Calculations

Process	Equation	Q	W	$\Delta U$
1 – 2 (adiabatic)	$P_1 V_1^\gamma = P_2 V_2^\gamma$	0	$\frac{P_1 V_1 - P_2 V_2}{\gamma - 1}$	$-\left(\frac{P_1 V_1 - P_2 V_2}{\gamma - 1}\right)$
2 – 3 (isothermal)	$P_2 V_2 = P_3 V_3$	$P_2 V_2 \ln \frac{V_3}{V_2}$	$P_2 V_2 \ln \frac{V_3}{V_2}$	0
3 – 4 (adiabatic)	$P_3 V_3^\gamma = P_4 V_4^\gamma$	0	$\frac{P_3 V_3 - P_4 V_4}{\gamma - 1}$	$-\left(\frac{P_3 V_3 - P_4 V_4}{\gamma - 1}\right)$
4 – 1 (isothermal)	$P_4 V_4 = P_1 V_1$	$P_4 V_4 \ln \frac{V_1}{V_4}$	$P_4 V_4 \ln \frac{V_1}{V_4}$	0

# Carnot cycle efficiency

$$\text{Carnot Efficiency} = 1 - \frac{T_1 \ln \frac{P_1}{P_4}}{T_2 \ln \frac{P_2}{P_3}} = 1 - \frac{T_1}{T_2} = 1 - \frac{T_C}{T_H}$$

Thank You