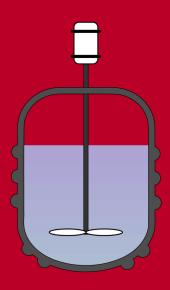
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# Introductory Numerical Methods for Simulating Batch Reactors

Dr. Joshua Pulsipher



# **Learning Outcomes**

1. The relative advantages/disadvantages of using **explicit Euler** methods

2. How to implement explicit Euler to **simulate ODEs** using common computation environments (e.g., Python)

3. How to **simulate batch reactors** using numerical methods

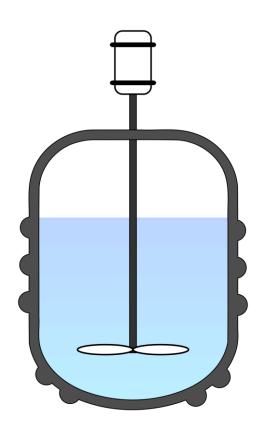
4. A familiarity of **other numerical methods/tools** for simulating batch reactors



- Overview
- Explicit Euler
- Batch Reactors
- Other Numerical Methods



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# **Simulating Dynamic Systems**

Simulating dynamic systems is vital for enabling engineering applications



**Curiosity Rover** 



**Batch Reactor** 

- Simulate using numerical methods to approximate dynamics (e.g., differential equations)
- Enables us to computationally experiment and implement automation



### **Differential Equations**

### **Types**

- Ordinary differential equations (ODEs)
  - Today's focus

$$\frac{dy(t)}{dt} = f(y(t), t)$$
$$y(0) = y_0$$

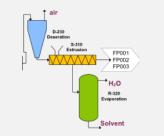
Partial differential equations (PDEs)

$$\frac{\partial y_c(t,x)}{\partial t} = \xi(x) \left( \frac{\partial^2 y_c(t,x)}{\partial x_1^2} + \frac{\partial^2 y_c(t,x)}{\partial x_2^2} \right) + y_g(t,x)$$
$$y_c(0,x), y_c(t, \text{boundary}) = 0$$

### **Applications**

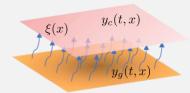
Transient flow balance

$$\frac{df(t)}{dt} = f_{in}(t) - f_{out}(t) + f_{gen}(t)$$



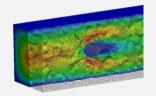
Heat/mass transfer

$$\frac{\partial T(t)}{\partial t} - \alpha \frac{\partial^2 T(t)}{\partial x^2} = 0$$



Fluid flow

$$\rho \frac{DV(t,x)}{Dt} = -\nabla p + \rho g(x) + \mu \nabla^2 V(t,x)$$



Kinetics

$$\frac{dc(t)}{dt} = kc(t)^{\alpha}$$





# **Analytical vs. Numerical Methods**

### **Analytical Methods**

Separate and integrate

$$g(y)\frac{dy}{dx} = h(x)$$
  $\longrightarrow$   $\int g(y)dy = \int h(x)dx + C$ 

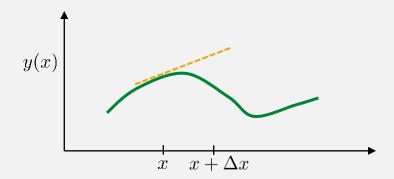
ODEs of special forms

$$\frac{dy}{dx} = \frac{x+y}{x-y} \longrightarrow \frac{1}{2}\log\left(\frac{y^2}{x^2} + 1\right) - \tan^{-1}\left(\frac{y}{x}\right) = C - \log(x)$$

Solving general ODEs is often difficult or not possible

### **Numerical Methods**

- Seek to numerically approximate the solution
- Finite difference methods are common



- More advanced methods are available
  - Not the focus of today



# **My Teaching Philosophy**

ldea: Promote a tutorial-like format that encourages active engagement.

### **Active Learning**

- Mastery comes through deliberate practice
- Magnify class time to gain guided hands-on experiences



#### **In-Class Exercises**

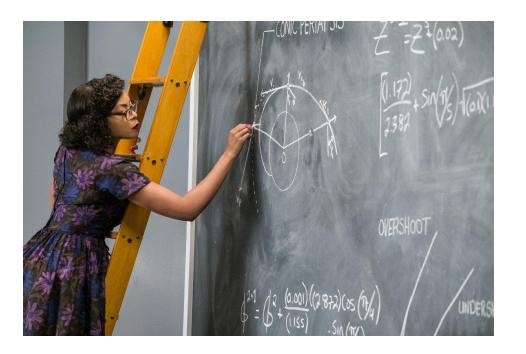
- We will be using Jupyter notebooks with a Julia and/or a Python kernel today
- No downloads/installation are/is needed
- https://github.com/pulsipher/eulercourse







- Overview
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### The Basics

### Methodology

Consider a 1<sup>st</sup> order ODE

$$\frac{dy(t)}{dt} = f(y(t), t)$$
$$y(0) = y_0$$

• Define time steps  $\Delta t$ 

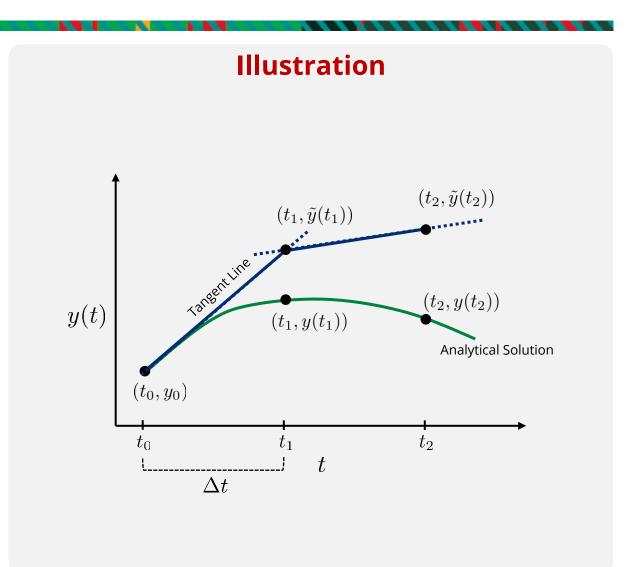
$$t \in [t_0, t_f] \qquad t_k = t_0 + k\Delta t$$

Approximate derivative as finite difference

$$\left. \frac{dy(t)}{dt} \right|_{t_k} \approx \frac{\tilde{y}(t_{k+1}) - \tilde{y}(t_k)}{\Delta t}$$

Define update rule

$$\tilde{y}(t_{k+1}) = \tilde{y}(t_k) + f(y(t_k), t_k) \Delta t$$



# **Properties: Error**

#### **Local Truncation Error (LTE)**

Recall update rule

$$\tilde{y}(t_{k+1}) = \tilde{y}(t_k) + f(y(t_k), t_k) \Delta t$$

Taylor series expansion of analytic solution

$$y(t_k + \Delta t) = y(t_k) + \Delta t \frac{dy(t)}{dt} \Big|_{t_k} + O(\Delta t^2)$$

Difference w/ explicit Euler

$$y(t_k + \Delta t) - \tilde{y}(t_{k+1}) = O(\Delta t^2)$$

Hence, the error incurred after one step is

$$O(\Delta t^2)$$

#### **Global Truncation Error (GTE)**

The number of steps

$$\frac{t - t_0}{\Delta t} \propto \frac{1}{\Delta t}$$

Multiplying this with the LTE, we get GTE that is

$$O(\Delta t)$$

Hence, explicit Euler is a first order method

Higher order methods are available



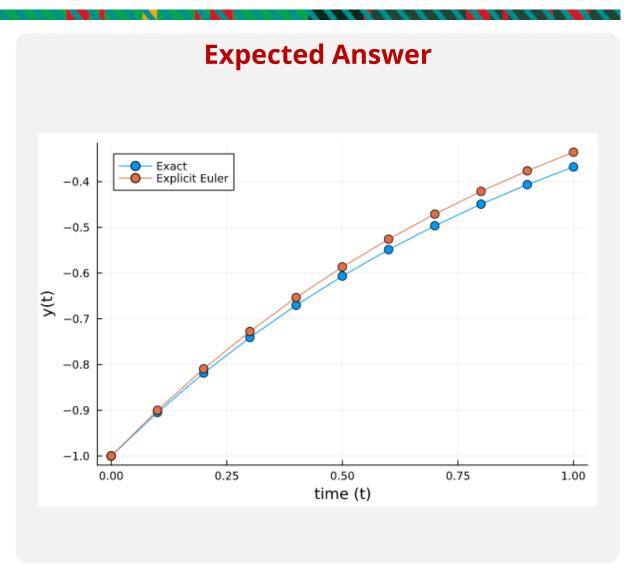
### **Tutorial 1**

### **Problem Setup**

Solve the ODE

$$\frac{dy(t)}{dt} = e^{-t}$$
$$y(0) = -1$$

- Specifications
  - $t \in [0, 1]$
  - $\Delta t = 0.1$
- Plot the result against the analytical answer
- Experiment with varied  $\Delta t$





## Simulating a System of ODEs

### System of 1st order ODEs

General representation

$$\frac{dy_1(t)}{dt} = f_1(y_1, y_2, \dots, y_n)$$

$$\frac{dy_2(t)}{dt} = f_2(y_1, y_2, \dots, y_n)$$

$$\vdots$$

$$\frac{dy_n(t)}{dt} = f_n(y_1, y_2, \dots, y_n)$$

$$y_1(0) = y_{1,0}, y_2(0) = y_{2,0}, \dots, y_n(0) = y_{n,0}$$

Vectorize

$$\frac{d\mathbf{y}(t)}{dt} = \mathbf{f}(\mathbf{y}(t), t)$$
$$\mathbf{y}(0) = \mathbf{y_0}$$

We can represent a higher order ODE as a 1<sup>st</sup> order system

### **Vectorized Explicit Euler**

Update rule uses vectorized representation

$$\tilde{\mathbf{y}}(t_{k+1}) = \tilde{\mathbf{y}}(t_k) + \mathbf{f}(\mathbf{y}(t_k), t_k) \Delta t$$

■ **Tutorial 2:** Simulate coupled ODEs w/  $\Delta t = 0.01$  and  $t \in [0, 1]$ 

$$\frac{dy_1(t)}{dt} = -5y_1(t) + 5y_2(t)$$
$$\frac{dy_2(t)}{dt} = 14y_1(t) - 2y_2(t)$$
$$y_1(0) = y_2(0) = 1$$



### **Properties: Stability**

### **Example 1**

• Simulate ODE w/  $\Delta t = 0.1$  in  $t \in [0, 1]$ 

$$\frac{dy(t)}{dt} = -20y(t)$$
$$y(0) = 1$$

Compare w/ analytic answer

### **Linear Stability**

Consider the linear ODE

$$\frac{dy(t)}{dt} = \lambda y(t)$$

For a stable solution we must have

$$|1 + \lambda \Delta t| < 1$$

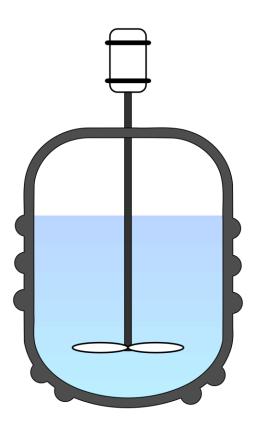
#### Stiff ODEs

- Systems that exhibit numerical instability
- Precise mathematical definition is nontrivial
- Common with reaction systems
  - Coexistence of small and large rate constants
- So, what can we do? → Use **implicit methods**

$$\tilde{y}(t_{k+1}) = \tilde{y}(t_k) + \frac{f(y(t_{k+1}), t_{k+1})}{\Delta t}$$



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## **Batch Reactor Modeling**

### **Simple ODE Model**

Arrhenius equation for species i and reaction j

$$k_{ij}(t) = A_{ij} \exp\left(\frac{-E_{a,ij}}{RT(t)}\right)$$

Reaction rates

$$r_j(\mathbf{c},t) = \sum_{i \in I} k_{ij}(t) c_i^{\beta_{ij}}(t)$$

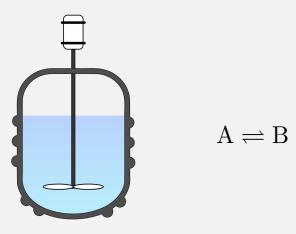
Species generation rates

$$r_i(\mathbf{c}, t) = \sum_{j \in J} \gamma_{ij} r_j(\mathbf{c}, t)$$

Species balances

$$\frac{dc_i(t)}{dt} = r_i(\mathbf{c}, t), \quad i \in I$$
$$c_i(0) = c_{i,0}, \qquad i \in I$$

#### **The Basics**



Derivation from mole balance

$$\frac{N_i(t)}{dt} = F_i(t) - F_i(t) + \int_{-\infty}^{V} r_i(t) dV(t)$$

Assume perfect mixing and constant volume

$$\frac{N_i(t)}{dt} = r_i(t)V \qquad \qquad \frac{c_i(t)}{dt} = r_i(t)$$



### **Exercise: Batch Reactor**

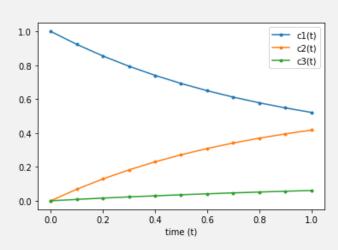
#### **Exercise 1**

• Simulate the following reaction system using explicit Euler for  $t \in [0, 1]$ 

$$A \rightleftharpoons B$$

$$A \rightleftharpoons C$$

• Experiment with different choices of  $\Delta t$ 



#### **Problem Information**

$$R = 1.987$$

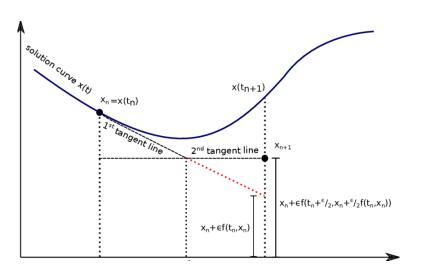
$$A = \begin{bmatrix} 3.6362e6 & 190.6879 \\ -2.5212e16 & 0 \\ 0 & -8.7409e24 \end{bmatrix}$$

$$E_a = \begin{bmatrix} 10000 & 5000 \\ 25000 & 0 \\ 0 & 40000 \end{bmatrix} \qquad \beta = 1 \qquad \gamma = \begin{bmatrix} -1 & -1 \\ 1 & 0 \\ 0 & 1 \end{bmatrix}$$

$$T(t) = \begin{cases} 333, & t < 0.5 \\ 325, & t \ge 0.5 \end{cases} \qquad \mathbf{c}_0 = \begin{bmatrix} 1 \\ 0 \\ 0 \end{bmatrix}$$



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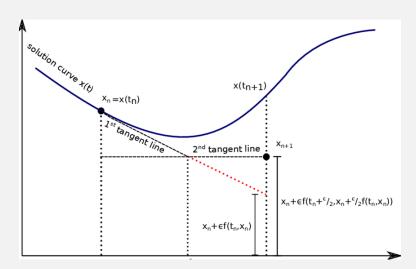




### **More Advanced Methods**

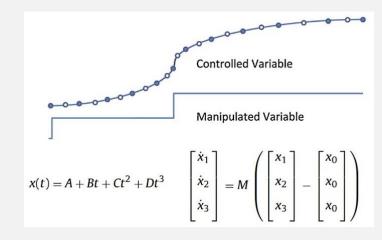
### **Runge-Kutta**

- Family of explicit and implicit iterative methods
- Various orders based on GTE  $O(h^p)$ 
  - 1st order methods are the Euler methods
  - 4<sup>th</sup> order methods are popular



### **Orthogonal Collocation over Finite Elements**

- The discretization uses finite elements
- We approximate the solution in each element as a polynomial function
- End up solving a system of linear equations





### **Common Simulation Tools**

### **ODE Integrators**

- Common in scripting languages
- Provide numerical solutions to ODE systems









### **Symbolic Solvers**

- Can provide analytic solutions when possible
- Typically, not used for large problems





### **Optimization Tools**

 Can incorporate differential equations when solving optimization problems







### **Problem Specific**

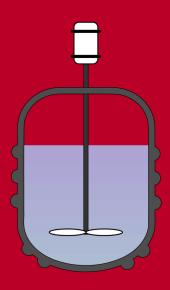
Simulate dynamics for particular systems







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