

# PID Control

## A Comprehensive Guide to PID Control Systems

CS637: EMBEDDED AND CYBER-PHYSICAL SYSTEMS

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## 1 Conclusion

- **PID Controller:** The most widely used control algorithm in industry.
  - Governs the majority of feedback loops in basic form or with minor variations.
- **Implementations:**
  - Standalone devices
  - Direct Digital Control (DDC) systems
  - Hierarchical distributed process control systems
- **Chapter Overview:**
  - **Fundamentals:** Introduction to PID control, fundamental algorithm, and representations.
  - **Controller Behavior:** Intuitive discussion of closed-loop system behavior.
  - **Integral Windup:** Addressing integral windup caused by actuator saturation and prevention methods.

# The Principle of Feedback in Control Systems

- **Feedback in Control Systems:**

- Fundamental concept enabling systems to maintain desired performance despite external disturbances and internal variations.
- Illustrated by a simple feedback control loop (see Figure 1).

## Negative Feedback

- Controller's response opposes the disturbance.
- Essential for stabilizing the system and accurate setpoint tracking.

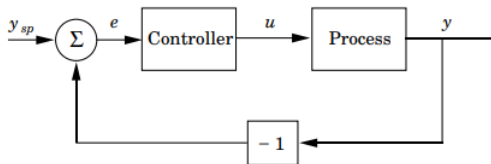


Figure: Block Diagram of a Process with a Feedback Controller

# Proportional Action

- **Definition:**

- Control action proportional to the current error  $e(t)$ .
- Simplified PID control law:

$$u(t) = K_p e(t) + u_b$$

where  $K_p$  is the proportional gain and  $u_b$  is the bias.

- **Characteristics:**

- Reduces oscillations compared to on-off control.
- Introduces steady-state error.
- Response improves with higher  $K_p$ , but excessive  $K_p$  can cause instability.

- **Bias ( $u_b$ ):**

- Often set to midpoint of control signal range:

$$u_b = \frac{u_{\max} + u_{\min}}{2}$$

- Can be adjusted to eliminate steady-state error at a specific setpoint.

- **Purpose:**

- Eliminate steady-state error between process output  $y$  and setpoint  $y_{sp}$ .

- **Control Law:**

$$u(t) = K_p e(t) + \frac{K_p}{T_i} \int_0^t e(\tau) d\tau$$

where  $T_i$  is the integral time constant.

- **Characteristics:**

- Accumulates error over time to adjust control signal.
- Ensures  $e(t)$  approaches zero in steady state.
- Can introduce slower response and potential oscillations.

- **Steady-State Behavior:**

- In steady state,  $e(t) = 0$  ensures  $u(t) = u_b$ .
- Integral action adjusts  $u_b$  to eliminate persistent errors.

# Derivative Action

- **Purpose:**

- Enhance stability and improve transient response of the control system.
- Predict future errors based on the rate of change of the current error.

- **Control Law:**

$$u(t) = K_p e(t) + K_d \frac{de(t)}{dt}$$

where  $K_d$  is the derivative gain.

- **Characteristics:**

- Dampens oscillations and reduces overshoot.
- Sensitive to high-frequency noise; requires careful tuning.
- Acts as a predictive mechanism to anticipate future errors.

- **Behavior:**

- Uses the derivative (rate of change) of the error to adjust  $u(t)$ .
- Can be interpreted using a Taylor series expansion:

$$e(t + T_d) \approx e(t) + T_d \frac{de(t)}{dt}$$

- Control signal becomes proportional to an estimate of the error  $T_d$  seconds into the future.

# PID Controller Variations

- **Standard (Non-Interacting / Parallel) PID Controller:**

$$G(s) = K \left( 1 + \frac{1}{sT_i} + sT_d \right)$$

- **Interacting (Series) PID Controller:**

$$G_P(s) = K_P \left( 1 + \frac{1}{sT_{Pi}} \right) (1 + sT_{Pd})$$

3.png

4.png



# Conversion Between Forms & Comparison

- **Conversion from Interacting to Non-Interacting Form:**

- 

$$K = K_P \left( \frac{T_{Pi} + T_{Pd}}{T_{Pi}} \right)$$

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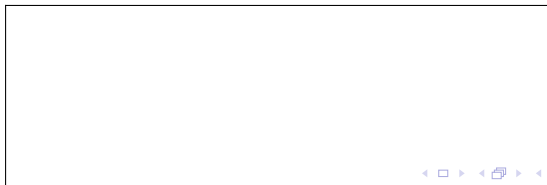
$$T_i = T_{Pi} + T_{Pd}$$

- 

$$T_d = \frac{T_{Pi} T_{Pd}}{T_{Pi} + T_{Pd}}$$

- **Condition for Conversion:**

- $T_i \geq 4T_d$
- Ensures stability during conversion



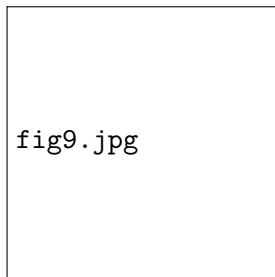
# Integrator Windup in PID Control

- **Key Concepts:**

- Integrator windup occurs when the control output exceeds actuator limits, leading to continuous accumulation of error in the integral term.
- Effects of windup include prolonged overshoot, oscillations, delayed settling, and reduced control accuracy.

- **Illustration:**

- The figure below shows the impact of integrator windup on system behavior, highlighting the oscillations and overshoot caused by accumulated integral action.



- **Methods to Prevent Windup:**

- **Integrator Clamping:** Temporarily holds the integrator value when saturation is detected.
- **Back-Calculation:** Adjusts the integrator based on the difference between desired and actual actuator output.
- **Incremental Algorithms:** Applies incremental control changes, reducing the risk of windup.
- **Tracking Mode in Digital Controllers:** Dynamically adjusts the integrator based on actuator behavior.

- **Benefits of Anti-Windup Mechanisms:**

- Improved stability and control performance
- Reduced oscillations and overshoot
- Faster settling times

# Incremental Algorithms and Back-Calculation

- **Early Development:** Integral action was initially integrated directly with actuators, using motor-driven valves to prevent windup by stopping integration at limits.
- **Digital Transition:** Digital control systems retained analog-like setups, leading to velocity algorithms for incremental control signal changes to avoid windup.
- **Back-Calculation:**
  - When actuator output saturates, back-calculation adjusts the integral term with time constant  $T_t$  and feedback gain  $\frac{1}{T_t}$ .
  - This adjustment resets the integrator at a rate controlled by  $T_t$ .
  - Recommended  $T_t$  range:  $T_d < T_t < T_i$ ; typically,  $T_t = \sqrt{T_i T_d}$ .
- **Steady-State Behavior:**
  - At steady state,  $e_s = 0$ , enabling normal operation without affecting the integrator.
  - During saturation,  $e_s \neq 0$  resets the integrator, keeping output within limits.

# Tracking Mode and Applications

- **Tracking Mode:**

- Controllers operate in two modes:
  - **Normal Mode:** Standard PID response to setpoint and output.
  - **Tracking Mode:** Aligns output with a tracking signal, dynamically adjusting as needed.
- Tracking is inhibited when tracking signal  $w$  equals output  $v$ , ensuring stability without manual mode switching.

- **Benefits of Tracking:**

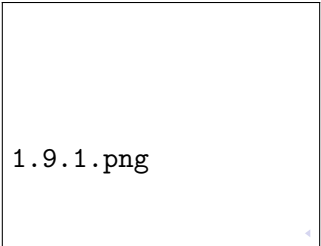
- Enhanced stability with automatic adjustments.
- Simplified integration for complex control strategies.
- Improved performance by adapting to external signals.

- **Applications:**

- **Cascade Control:** Enables inner loop controllers to follow outer loop signals.
- **Override Control:** Adjusts output based on predefined safety or performance signals.
- **Setpoint Scheduling:** Allows smooth setpoint changes to reduce sudden control adjustments.

# PID Tuning Methods

- **Tuning Overview:** Ziegler-Nichols methods set PID parameters for effective control, focusing on load disturbances, noise, and process dynamics.
- **Step Response Method:**
  - Characterizes open-loop step response to find  $a$  and  $L$ .
  - Steps:
    - Perform a step test on the open-loop system.
    - Identify max slope; draw tangent to find  $a$  and  $L$ .
    - Use  $a$  and  $L$  to calculate controller parameters (Table 1.1).
    - Estimate closed-loop period  $T_p$ .
- **Advantages:** Simple, widely used; provides baseline PID parameters.



1.9.1.png

# Frequency Response Method

- **Frequency Response Method:**

- Uses system oscillations in proportional-only mode.
- Steps:
  - Set PID controller to proportional mode ( $T_i = \infty$ ,  $T_d = 0$ ).
  - Increase  $K$  until sustained oscillations occur.
  - Record  $K_u$  (ultimate gain) and  $T_u$  (ultimate period).
  - Use  $K_u$  and  $T_u$  to set PID parameters (Table 1.2).

- **Example:**

- If  $K_u = 2$  and  $T_u = 5$ :
- $K = 0.6 \times 2 = 1.2$ ,  $T_i = 0.5 \times 5 = 2.5$  sec,  $T_d = 0.125 \times 5 = 0.625$  sec

- **Advantages:** Good for dynamic processes; adjusts parameters based on oscillations.

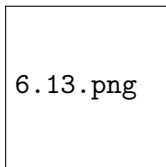


Figure: Frequency Response Method for PID Tuning

# Digital Implementation of PID Controllers

- **Discretization:** Continuous PID terms are approximated at discrete sampling instants  $\{t_k\}$ .
- **Proportional Action:**

$$P(t_k) = K(b \cdot y_{sp}(t_k) - y(t_k))$$

- **Integral Action (Forward Difference):**

$$I(t_{k+1}) = I(t_k) + \frac{Kh}{T_i} e(t_k)$$

- **Derivative Action (Backward Difference):**

$$D(t_k) = \frac{T_d}{T_d + Nh} D(t_{k-1}) - \frac{KT_d N}{T_d + Nh} (y(t_k) - y(t_{k-1}))$$

- **Discrete PID Control Signal:**

$$u(t_k) = P(t_k) + I(t_k) + D(t_k)$$



# Velocity Algorithms in PID Control

- **Overview:** Velocity algorithms output the rate of change, ideal for systems with external integrators (e.g., motor-driven).

- **Incremental Form:**

$$\Delta u(t_k) = \Delta P(t_k) + \Delta I(t_k) + \Delta D(t_k)$$

- Each term (P, I, D) calculated as an increment, allowing efficient computations.

- **Advantages:** Reduced computational load, easy anti-windup, compatible with legacy systems.
- **Non-Integral Controllers:** Uses offset term  $u_b$  to hold steady state:

$$\Delta u(t) = Ke(t) + u_b - u(t - h)$$

# Feedforward Control with Feedback Integration

- **Concept:** Feedforward ( $u_{FF}$ ) preempts disturbances, added to feedback ( $u_{FB}$ ) for combined control:

$$u = u_{FB} + u_{FF}$$

- **Role of Feedforward and Feedback:** - Feedforward handles predictable disturbances; feedback corrects unexpected errors.
- **Anti-Windup Strategy:** Applies to total  $u$  to avoid windup when feedforward signals are added.
- **Incremental Approach:**

$$\Delta u = \Delta u_{FB} + \Delta u_{FF}$$

$$u(t) = u(t - h) + \Delta u(t)$$

- Smooth control updates; minimizes windup by synchronizing feedback and feedforward changes.

# Applications of PID Control

- **General Use:** Widely used in industry for its simplicity and effectiveness in setpoint tracking, disturbance rejection, and noise handling.
- **When PI Control is Sufficient:**
  - Suitable for systems with first-order dynamics or those with less stringent precision needs.
  - Effective in eliminating steady-state error and providing adequate transient response.
  - Indicators: First-order step response, or Nyquist plot within first and fourth quadrants.
- **When PID Control is Ideal:**
  - Best for systems with second-order dynamics or multiple time constants.
  - Common applications:
    - **Varying time constants:** Derivative action enhances stability.
    - **Temperature control:** Derivative action dampens oscillations, speeds up settling.
    - **High-precision control:** Derivative action improves damping, allowing for higher gains.

# Limitations of PID Control

- **Higher-Order Processes:** PID struggles with systems beyond second-order, which may lead to suboptimal performance or instability.
- **Systems with Long Dead Time:** Delays between control action and effect can cause PID to respond too late, leading to oscillations.
- **High-Frequency Noise Sensitivity:** Derivative term amplifies noise, requiring careful tuning and possibly extra filtering.
- **Alternatives:** For these cases, consider advanced controls like Model Predictive Control (MPC) or adaptive strategies to improve stability and performance.

# Conclusion

- **PID Controllers:** Widely applicable, offering robust and simple control for many systems.
- **Proportional Control:** Reduces oscillations; may leave steady-state error.
- **Integral Control:** Removes steady-state error; can slow response.
- **Derivative Control:** Improves stability and transient response; sensitive to noise.
- **Tuning Methods:** Essential for optimal performance; includes Step and Frequency Response methods.
- **Digital Implementation:** Requires discretization for continuous-time control.
- **Applications and Limitations:** Versatile but may need alternative approaches for complex dynamics.

## Future Directions:

- Integrating advanced control techniques and complex systems.
- Enhancing digital methods for precision and stability.

# Thank You!

Questions?