

# Entrained flow reactor (EFR)

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## 1 Introduction

This report provides an overview of the Entrained Flow Reactor (EFR) at NREL and associated computational modeling tasks. The reactor operates at fast pyrolysis conditions to thermochemically convert biomass into gaseous products. The EFR is part of the Thermochemical Process Development Unit (TCPDU) at NREL which was originally designed for biomass gasification where the EFR was used as a thermal cracker. An overview of the TCPDU system is shown in Figure 1.

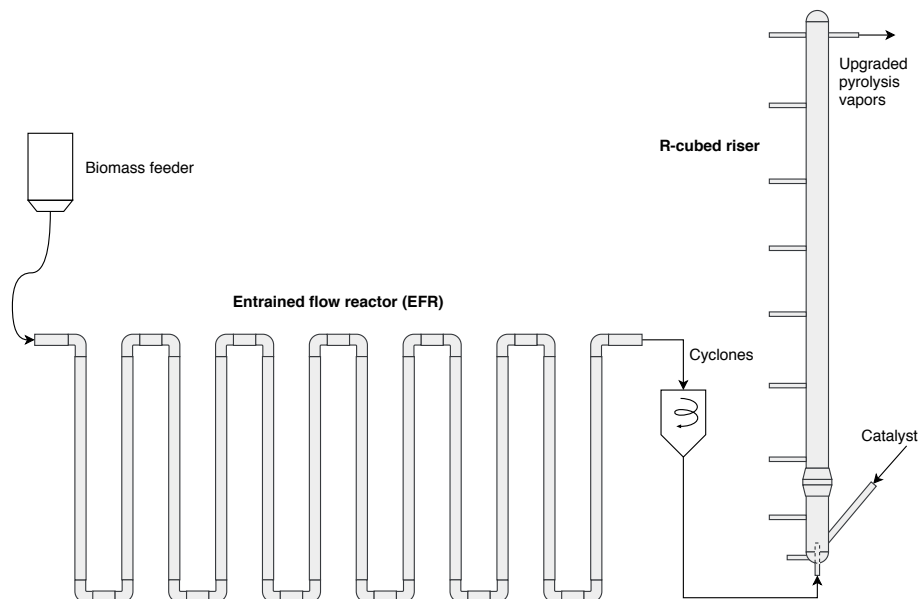


Figure 1: Overview of the main components of the NREL TCPDU system. Fast pyrolysis of biomass occurs in the entrained flow reactor. Catalytic vapor phase upgrading occurs in the R-cubed riser reactor.

## 2 Experimental setup

This section provides geometric dimensions and typical operating conditions for the entrained flow reactor. Characteristics for the Blend3 and forest residue feedstocks are also discussed.

### 2.1 Entrained flow reactor

Fast pyrolysis in the TCPDU system occurs in the entrained flow reactor (EFR) which is comprised of a series of horizontal and vertical pipes connected with 90 degree elbows (see Figure 2). The EFR is essentially a pneumatic conveyor where biomass particles flow through a long pipe with several bends. Dimensions and material information about the EFR are provided in Figure 3 below. Operating conditions such as temperatures, pressures, and flow rates for the EFR are shown in Figure 4. Nitrogen gas at 500°C is generally used as the conveying medium for the solids.

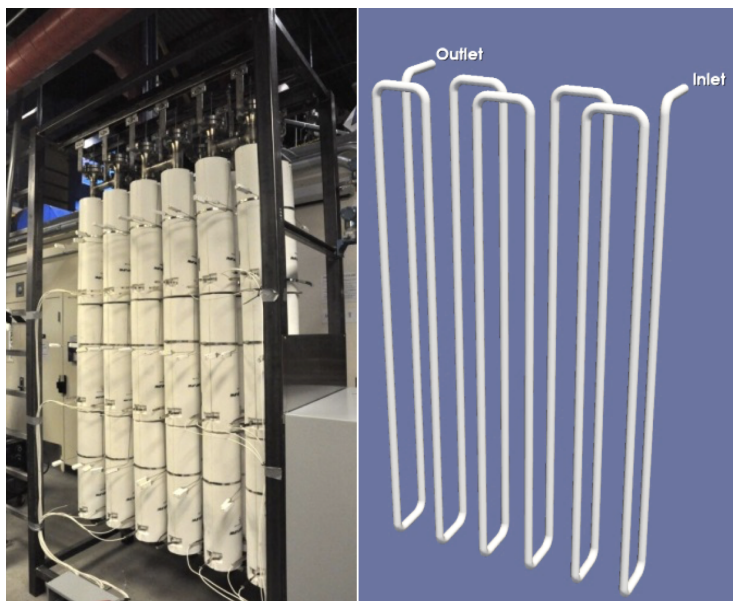


Figure 2: Left - picture of the EFR assembly with heat jackets, insulation, and thermocouples. Right - CAD representation of the EFR pipe assembly used for MFiX simulations.

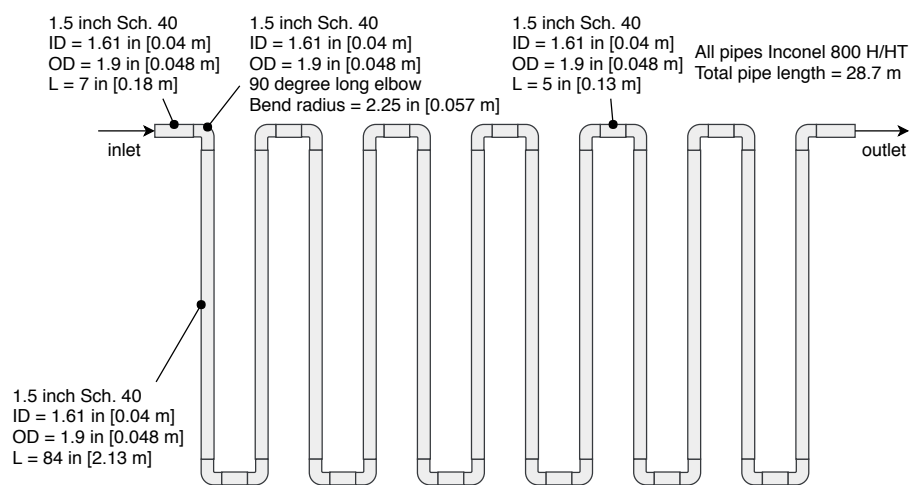


Figure 3: Geometry of the entrained flow reactor at NREL.

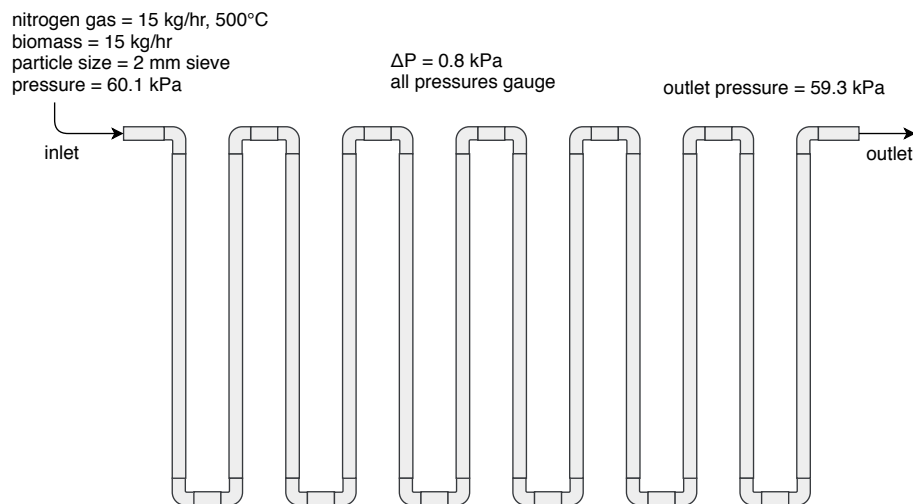


Figure 4: Typical operating conditions for the entrained flow reactor.

## 2.2 Blend3 feedstock

General information about the Blend3 feedstock used in the entrained flow reactor is provided in Table 1. There is currently no information regarding identification of the feedstock or who performed the feedstock measurements and data preparation. Proximate and ultimate analysis data for the feedstock are presented in Tables 2 and 3. Only one set of analysis data is available therefore the uncertainty in the values is unknown.

Table 1: General information for the Blend3 feedstock.

Item	Description
Name	Blend3
ID	?
Contact	?

Table 2: Blend3 proximate analysis mass percent, as-received basis. Source [3].

Proximate	% ar	% ar	% ar
FC	16.92	?	?
VM	76.40	?	?
ash	0.64	?	?
moisture	6.04	?	?

Table 3: Blend3 ultimate analysis mass percent, as-received basis. Source [3].

Element	% ar	% ar	% ar
C	49.52	?	?
H	5.28	?	?
O	38.35	?	?
N	0.15	?	?
S	0.02	?	?
ash	0.64	?	?
moisture	6.04	?	?

The chemical analysis of the Blend3 feedstock is presented in Table 4. Again, only one set of data is available so the uncertainty in the measurements is unknown. The chemical analysis measurements are used to determine the biomass composition which is needed for the kinetics model.

Table 4: Blend3 chemical analysis mass percent, dry basis. Source [6].

Chemical component	% dry	% dry	% dry
glucan	38.95	?	?
acetyl	1.59	?	?
arabinan	1.40	?	?
galactan	3.16	?	?
mannan	10.52	?	?
xylan	7.89	?	?
lignin	29.48	?	?
free fructose	0.07	?	?
free glucose	0.04	?	?
sucrose	0.04	?	?
water extractives	2.75	?	?
ethanol extractives	3.49	?	?
non-structural inorganics	0.22	?	?
structural inorganics	0.41	?	?

Table 5: Blend3 ash analysis as weight percent of ash. Source [3].

Metal oxide	wt. %	wt. %	wt. %
SiO <sub>2</sub>	28.1	?	?
Al <sub>2</sub> O <sub>3</sub>	7.06	?	?
TiO <sub>2</sub>	0.34	?	?
CaO	21.8	?	?
Na <sub>2</sub> O	0.71	?	?
K <sub>2</sub> O	13.8	?	?
P <sub>2</sub> O <sub>5</sub>	5.47	?	?
SO <sub>3</sub>	1.23	?	?
Cl	0.09	?	?
CO <sub>2</sub>	5.14	?	?

Table 6: Blend3 particle properties from pelletized crushed feedstock. The crushed feedstock is used in the entrained flow reactor.

Property	Value	Description	Source
$\rho$	1,050 kg/m <sup>3</sup>	particle density, daf basis	[5]
$\eta$	0.27	particle porosity	
$k$	0.23 W/mK	thermal conductivity	

Table 7: Entrained flow reactor yields for Blend3 feedstock.

Yield	wt. %
total liquid	64.9
char	13.9 $\pm$ 0.1
gas	17.2 $\pm$ 0.2
mass balance	96.9 $\pm$ 1.5
carbon balance	93.0 $\pm$ 1.0

## 2.3 Forest residue feedstock

The forest residue feedstock is comprised of branches/twigs, cambium, needles, bark, and whitewood. This feedstock is used in the NREL fluidized bed reactor (FBR) for the purposes of the FCIC project. The FBR is operated at fast pyrolysis conditions for the thermochemical conversion of biomass. The reactor is sometimes referred to as the 2FBR.

Table 8: General information for the forest residue feedstock.

Item	Description
Name	forest residue
ID	?
Contact	?

Table 9: Bark ultimate analysis mass percent, dry ash-free basis. Source [1].

Element	% daf	% daf	% daf
C	48.27	?	?
H	5.72	?	?
N	0.52	?	?

Table 10: Branches/twigs ultimate analysis mass percent, dry ash-free basis. Source [1].

Element	% daf	% daf	% daf
C	49.69	?	?
H	6.36	?	?
N	0.25	?	?

Table 11: Cambium ultimate analysis mass percent, dry ash-free basis. Source [1].

Element	% daf	% daf	% daf
C	48.52	?	?
H	6.39	?	?
N	0.11	?	?

Table 12: Needles ultimate analysis mass percent, dry ash-free basis. Source [1].

Element	% daf	% daf	% daf
C	48.59	?	?
H	5.92	?	?
N	1.22	?	?

Table 13: Whitewood ultimate analysis mass percent, dry ash-free basis. Source [1].

Element	% daf	% daf	% daf
C	48.27	?	?
H	6.15	?	?
N	0.10	?	?

Table 14: Whitewood biomass composition mass percent, dry basis. Source [2].

Component	% dry
Cellulose	38.04
Hemicellulose	24.2

### 3 Model development

Here.

#### 3.1 Biomass pyrolysis kinetics

Chemical species in the Debiagi et al. kinetic scheme for biomass pyrolysis [4].

Table 15: Chemical species in the Debiagi kinetics scheme for biomass pyrolysis.

Item	Name	Formula	Phase	Description
1	CELL	$C_6H_{10}O_5$	solid	cellulose
2	CELLA	$C_6H_{10}O_5$	solid	active cellulose
3	GMSW	$C_5H_8O_4$	solid	hemicellulose softwood
4	XYHW	$C_5H_8O_4$	solid	hemicellulose hardwood
5	XYGR	$C_5H_8O_4$	solid	hemicellulose grass
6	HCE1	$C_5H_8O_4$	solid	intermediate hemicellulose
7	HCE2	$C_5H_8O_4$	solid	intermediate hemicellulose
8	ITANN	$C_8H_4O_4$	solid	intermediate phenolics
9	LIG	$C_{11}H_{12}O_4$	solid	intermediate lignin
10	LIGC	$C_{15}H_{14}O_4$	solid	carbon rich lignin
11	LIGCC	$C_{15}H_{14}O_4$	solid	intermediate lignin
12	LIGH	$C_{22}H_{28}O_9$	solid	hydrogen rich lignin
13	LIGO	$C_{20}H_{22}O_{10}$	solid	oxygen rich lignin
14	LIGOH	$C_{19}H_{22}O_8$	solid	intermediate lignin
15	TANN	$C_{15}H_{12}O_7$	solid	tannins
16	TGL	$C_{57}H_{100}O_7$	solid	triglycerides
17	CHAR	C	solid	char as pure carbon
18	G{COH2} loose	$CH_2O$	metaplastic	loose formaldehyde
19	G{CO2}	$CO_2$	metaplastic	trapped carbon dioxide
20	G{CO}	CO	metaplastic	trapped carbon monoxide
21	G{CH3OH}	$CH_4O$	metaplastic	trapped methanol



22	G{CH4}	CH <sub>4</sub>	metaplastic	trapped methane
23	G{C2H4}	C <sub>2</sub> H <sub>4</sub>	metaplastic	trapped ethylene
24	G{C6H5OH}	C <sub>6</sub> H <sub>6</sub> O	metaplastic	trapped phenol
25	G{COH2} stiff	CH <sub>2</sub> O	metaplastic	stiff formaldehyde
26	G{H2}	H <sub>2</sub>	metaplastic	trapped hydrogen
27	G{C2H6}	C <sub>2</sub> H <sub>6</sub>	metaplastic	trapped ethane
28	C2H4	C <sub>2</sub> H <sub>4</sub>	gas	ethylene
29	C2H6	C <sub>2</sub> H <sub>6</sub>	gas	ethane
30	CH2O	CH <sub>2</sub> O	gas	formaldehyde
31	CH4	CH <sub>4</sub>	gas	methane
32	CO	CO	gas	carbon monoxide
33	CO2	CO <sub>2</sub>	gas	carbon dioxide
34	H2	H <sub>2</sub>	gas	hydrogen
35	C2H3CHO	C <sub>3</sub> H <sub>4</sub> O	liquid	acrolein
36	C2H5CHO	C <sub>3</sub> H <sub>6</sub> O	liquid	propionaldehyde
37	C2H5OH	C <sub>2</sub> H <sub>6</sub> O	liquid	ethanol
38	C5H8O4	C <sub>5</sub> H <sub>8</sub> O <sub>4</sub>	liquid	xylofuranose
39	C6H10O5	C <sub>6</sub> H <sub>10</sub> O <sub>5</sub>	liquid	levoglucosan
40	C6H5OCH3	C <sub>7</sub> H <sub>8</sub> O	liquid	anisole
41	C6H5OH	C <sub>6</sub> H <sub>6</sub> O	liquid	phenol
42	C6H6O3	C <sub>6</sub> H <sub>6</sub> O <sub>3</sub>	liquid	5-(hydroxymethyl)-furfural
43	C24H28O4	C <sub>24</sub> H <sub>28</sub> O <sub>4</sub>	liquid	heavy molecular weight lignin
44	CH2OHCH2CHO	C <sub>3</sub> H <sub>6</sub> O <sub>2</sub>	liquid	propionic acid
45	CH2OHCHO	C <sub>2</sub> H <sub>4</sub> O <sub>2</sub>	liquid	acetic acid
46	CH3CHO	C <sub>2</sub> H <sub>4</sub> O	liquid	acetaldehyde
47	CH3CO2H	C <sub>2</sub> H <sub>4</sub> O <sub>2</sub>	liquid	acetic acid
48	CH3OH	CH <sub>4</sub> O	liquid	methanol
49	CHOCHO	C <sub>2</sub> H <sub>2</sub> O <sub>2</sub>	liquid	glyoxal
50	CRESOL	C <sub>7</sub> H <sub>8</sub> O	liquid	cresol
51	FURFURAL	C <sub>5</sub> H <sub>4</sub> O <sub>2</sub>	liquid	furan-2-carboxaldehyde(furfural)
52	H2O	H <sub>2</sub> O	liquid	water from reactions
53	HCOOH	CH <sub>2</sub> O <sub>2</sub>	liquid	formic acid
54	MLINO	C <sub>19</sub> H <sub>34</sub> O <sub>2</sub>	liquid	methyl linoleate
55	U2ME12	C <sub>13</sub> H <sub>22</sub> O <sub>2</sub>	liquid	linalyl propionate
56	VANILLIN	C <sub>8</sub> H <sub>8</sub> O <sub>3</sub>	liquid	vanillin
57	ACQUA	H <sub>2</sub> O	liquid	water within biomass

### 3.2 Biomass characterization

Here.

Table 16: Blend3 biomass composition mass percent, dry basis. Values are calculated from Table 4.

Biomass composition	% dry
cellulose	38.95
hemicellulose	24.56
lignin	29.48
tann	2.90
tgl	3.49
ash	0.63

## 4 Results and discussion

Here.

## 5 Conclusions

Here.

## 6 Source code

The Python code used to develop the models and generate results discussed in this paper is available on GitHub at <https://github.com/ccpcode/nrel-efr>.

## References

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