

CARBONIC ANHYDRASE: KINETICS OF REMOVAL OF Zn(II) By 2,6-PYRIDINECARBOXYLATE

Paul Nickerson*

Department of Chemistry, University of Florida, Gainesville, FL, US

E-mail: pvnick@ufl.edu

Abstract

In the past decade, supervised activity recognition methods have been studied by many researchers, however these methods still face many challenges in real world settings. Supervised activity recognition methods assume that we are provided with labeled training examples from a set of predefined activities. Annotating and hand labeling data is a very time consuming and laborious task. Also, the assumption of consistent pre-defined activities might not hold in reality. More importantly, these algorithms do not take into account the streaming nature of data, or the possibility that the patterns might change over time. In this chapter, we will provide an overview of the state of the art *unsupervised* methods for activity recognition. In particular, we will describe a scalable activity discovery and recognition method for complex large real world datasets, based on sequential data mining and stream data mining methods.

*To whom correspondence should be addressed

Introduction

Carbonic anhydrase (CA) catalyzes the interconversion of carbon dioxide and carbonic acid/bicarbonate as follows:



In the active form, CA is bound to a Zn^{2+} cofactor (denoted as $\text{CA}\cdot\text{Zn}$), which it relies upon for its catalytic activity. The zinc ion can be stripped from the enzyme using a Lewis base ligand, which donates electrons to the ion to form a covalent bond. The ligand being studied in this experiment is 2,6-pyridinecarboxylate, commonly called dipicolinate (or dipic). Figure ?? shows the structure of dipic. In this experiment, the rate of zinc removal by dipic will be measured.

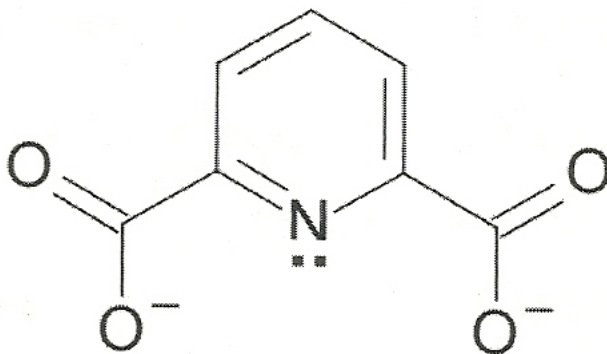


Figure 1: Structure of 2,6-pyridinecarboxylate (dipic) ?

Mechanism

When $[\text{dipic}] \gg [\text{CA}]$, that is, when $\frac{[\text{dipic}]}{[\text{CA}]} \geq 25$, then the removal of zinc is pseudo-first-order with respect to $\text{CA}\cdot\text{Zn}$ because the concentration of dipic, denoted as L , does not change appreciably. Thus the formation of the inactive enzyme, apoCA, can be modeled

using the following rate equation:

$$\frac{d[\text{apoCA}]}{dt} = k_{obs}[\text{CA}\cdot\text{Zn}] \quad (2)$$

The pseudo-first-order rate constant, k_{obs} , increases as $[\text{L}]$ increases, but levels off at sufficiently high concentrations of L. Biochemists will recognize behavior similar to Michaelis-Menten enzyme kinetics in which the enzyme, CA·Zn, and the substrate, L, reversibly form a CA·Zn·L complex with association constant K_{EML} (EML stands for Enzyme-Metal-Ligand):



This can be modeled as follows:

$$K_{EML} = \frac{[\text{CA}\cdot\text{Zn}\cdot\text{L}]}{[\text{CA}\cdot\text{Zn}][\text{L}]} \quad (4)$$

CA·Zn·L can either revert back to the original species or irreversibly convert to the inactive form of the enzyme, apoCA, and the covalently bound zinc-dipic molecule, ZnL:



This yields the following differential rate law:

$$\frac{d[\text{apoCA}]}{dt} = k_d[\text{CA}\cdot\text{Zn}\cdot\text{L}] \quad (6)$$

Note the difference in assumptions between this reaction and the Michaelis-Menten model; M-M kinetics assumes the enzyme is reformed and that only the substrate is modified, while (??) shows that both the substrate and the enzyme are permanently modified. Recall that $[\text{L}] \gg [\text{CA}\cdot\text{Zn}]$, so $[\text{L}]$ can be assumed to stay constant at $[\text{L}]_0$, which is substituted into a

rearranged form of equation (??),

$$[\text{CA}\cdot\text{Zn}\cdot\text{L}] = K_{EML}[\text{CA}\cdot\text{Zn}][\text{L}]_0 \quad (7)$$

Carbonic anhydrase can exist in one of three forms: the metalloenzyme $\text{CA}\cdot\text{Zn}$, the enzyme-metal-ligand complex $\text{CA}\cdot\text{Zn}\cdot\text{L}$, or the inactivated enzyme apoCA. Initially, all CA is tied up in the metalloenzyme, and none exists as $\text{CA}\cdot\text{Zn}\cdot\text{L}$ or apoCA. As the activated form of the enzyme gets bound to L and then inactivated,

$$[\text{CA}\cdot\text{Zn}] = [\text{CA}\cdot\text{Zn}]_0 - [\text{apoCA}] - [\text{CA}\cdot\text{Zn}\cdot\text{L}], \quad (8)$$

which can be combined with equation (??) to yield

$$[\text{CA}\cdot\text{Zn}] = [\text{CA}\cdot\text{Zn}]_0 - [\text{apoCA}] - K_{EML}[\text{CA}\cdot\text{Zn}][\text{L}]_0 \quad (9)$$

and can be rearranged as follows:

$$[\text{CA}\cdot\text{Zn}] = \frac{[\text{CA}\cdot\text{Zn}]_0 - [\text{apoCA}]}{1 + K_{EML}[\text{L}]_0} \quad (10)$$

Equations (??) and (??) can be combined to give

$$\frac{d[\text{apoCA}]}{dt} = k_d K_{EML}[\text{CA}\cdot\text{Zn}][\text{L}]_0 \quad (11)$$

Therefore, the rate of apoCA formation is first-order with respect to $\text{CA}\cdot\text{Zn}$. Combining equations (??) and (??) yields

$$\frac{d[\text{apoCA}]}{dt} = k_d K_{EML}[\text{L}]_0 \frac{[\text{CA}\cdot\text{Zn}]_0 - [\text{apoCA}]}{1 + K_{EML}[\text{L}]_0} \quad (12)$$

Rearranging and integrating,

$$\begin{aligned} \int_{[apoCA]_0}^{[apoCA]_t} \frac{d[apoCA]}{[CA \cdot Zn]_0 - [apoCA]_t} &= \int_0^t \frac{k_d K_{EML} [L]_0}{1 + K_{EML} [L]_0} dt \\ &= \frac{k_d K_{EML} [L]_0}{1 + K_{EML} [L]_0} t \end{aligned} \quad (13)$$

The left side must be integrated using u-sub:

$$u = [CA \cdot Zn]_0 - [apoCA]_t$$

$$du = -d[apoCA]$$

To change the integral boundaries,

$$u(t = 0) = [CA \cdot Zn]_0, \text{ since no inactivated enzyme has been formed}$$

$$u(t = t) = [CA \cdot Zn]_0 - [apoCA]_t$$

Therefore,

$$\begin{aligned} \int_{[apoCA]_0}^{[apoCA]_t} \frac{d[apoCA]}{[CA \cdot Zn]_0 - [apoCA]_t} &= - \int_{[CA \cdot Zn]_0}^{[CA \cdot Zn]_0 - [apoCA]_t} \frac{du}{u} \\ &= -\ln(u) \Big|_{[CA \cdot Zn]_0}^{[CA \cdot Zn]_0 - [apoCA]_t} \\ &= -\ln \left(\frac{[CA \cdot Zn]_0 - [apoCA]}{[CA \cdot Zn]_0} \right) \end{aligned} \quad (14)$$

Combining the evaluated integrals from equations (??) and (??) yields

$$\ln \left(\frac{[CA \cdot Zn]_0 - [apoCA]}{[CA \cdot Zn]_0} \right) = -\frac{k_d K_{EML} [L]_0}{1 + K_{EML} [L]_0} t \quad (15)$$

Assuming steady-state conditions for $CA \cdot Zn \cdot L$, that is, $[CA \cdot Zn \cdot L]$ is always negligible, then

$\frac{[CA \cdot Zn]_0 - [apoCA]}{[CA \cdot Zn]_0}$ is simply the fraction of $CA \cdot Zn$ remaining after reaction time t and can be

referred to as $F_{\text{CA}\cdot\text{Zn}}$:

$$\ln(F_{\text{CA}\cdot\text{Zn}}) = -\frac{k_d K_{\text{EML}}[\text{L}]_0}{1 + K_{\text{EML}}[\text{L}]_0} t \quad (16)$$

Since $-\frac{k_d K_{\text{EML}}[\text{L}]_0}{1 + K_{\text{EML}}[\text{L}]_0}$ is a constant for a given concentration of dipic, equation (??) exhibits linear behavior. Therefore, a linear least squares regression procedure can be performed for measurements of $\ln(F_{\text{CA}\cdot\text{Zn}})$ over time, and the slope, denoted $-k_{\text{obs}}$, will be

$$-k_{\text{obs}} = -\frac{k_d K_{\text{EML}}[\text{L}]_0}{1 + K_{\text{EML}}[\text{L}]_0} \quad (17)$$

Taking the reciprocal of equation (??) yields

$$\begin{aligned} \frac{1}{k_{\text{obs}}} &= \frac{1 + K_{\text{EML}}[\text{L}]_0}{k_d K_{\text{EML}}[\text{L}]_0} \\ &= \frac{1}{k_d K_{\text{EML}}[\text{L}]_0} + \frac{K_{\text{EML}}[\text{L}]_0}{k_d K_{\text{EML}}[\text{L}]_0} \\ &= \frac{1}{k_d K_{\text{EML}}} \times \frac{1}{[\text{L}]_0} + \frac{1}{k_d} \end{aligned} \quad (18)$$

Again, a linear pattern is observed; measuring k_{obs} at several different dipic concentrations enables one to perform a least squares regression procedure on $\frac{1}{k_{\text{obs}}}$ versus $\frac{1}{[\text{L}]_0}$ to determine the slope, $m = \frac{1}{k_d K_{\text{EML}}}$, and intercept, $b = \frac{1}{k_d}$. k_d and K_{EML} are thus calculated as follows:

$$k_d = \frac{1}{b} \quad (19)$$

$$K_{\text{EML}} = \frac{b}{m} \quad (20)$$

Rate Measurements

While equations (??) and (??) seem to imply that the determination of k_{obs} requires knowing $[\text{CA}\cdot\text{Zn}]$ or $[\text{apoCA}]$ at any point in time, in reality a plot of $f(t)$ vs t , where $f(t)$ is proportional to $F_{\text{CA}\cdot\text{Zn}}$, will still exhibit the same slope $-k_{\text{obs}}$. The Michaelis-Menten kinetics model states that, for sufficiently large substrate concentrations, the enzyme is fully saturated and

the reaction velocity asymptotically approaches a number, $V_{max} = k_{cat}[\text{CA} \cdot \text{Zn}]$, where k_{cat} (the "turnover number") is amount of substrate that can be converted to product by a single saturated enzyme molecule in a given unit of time.[?]

Data and Results

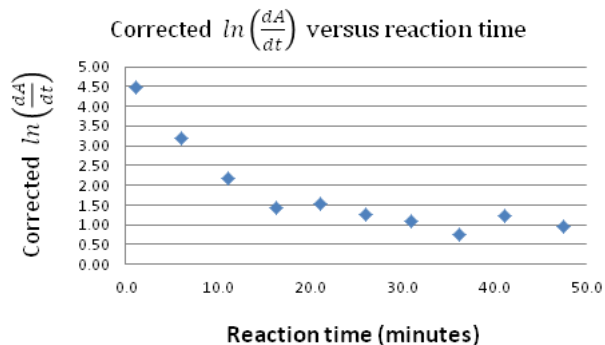


Figure 2: laksjdf askdfj asdkljfhaslkdjfhaklsdjfh asldkfjhasdlkfjhalksdjfhalksdjfh
asldkfjhasdlkfjashdlfkajsdhflkajshdf asdfa sdiufhaisdu fas dfasd fasef asefasef asefas
efasefkahsdlkfjhaslkdjfh sdfasldkfjhasdlfkjasdh falksdjfhalskdjfhaskdlkfjah sdfkjasldkfjah
sdlkfjh asldkfj asldkfjhalksdjfhalksjdh flkajsdhf alsdkjfash dflaskdjfah .

In the past decade, supervised activity recognition methods have been studied by many researchers, however these methods still face many challenges in real world settings. Supervised activity recognition methods assume that we are provided with labeled training examples from a set of predefined activities. Annotating and hand labeling data is a very time consuming and laborious task. Also, the assumption of consistent pre-defined activities might not hold in reality. More importantly, these algorithms do not take into account the streaming nature of data, or the possibility that the patterns might change over time. In this chapter, we will provide an overview of the state of the art *unsupervised* methods for activity recognition. In particular, we will describe a scalable activity discovery and recognition method for complex large real world datasets, based on sequential data mining and stream data mining methods.

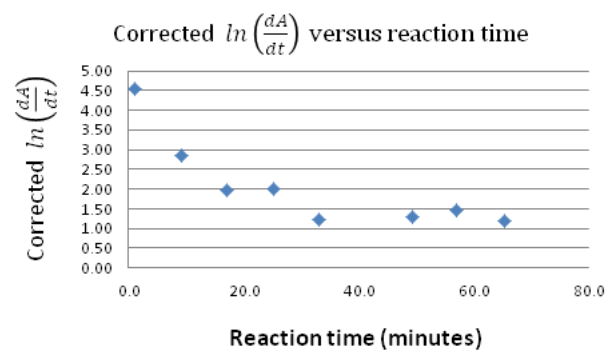


Figure 3: blahblah.

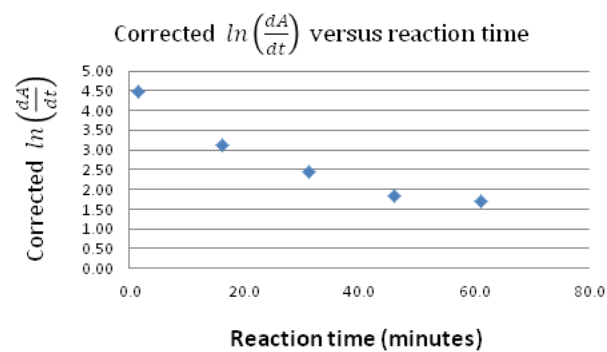


Figure 4: blahblah.

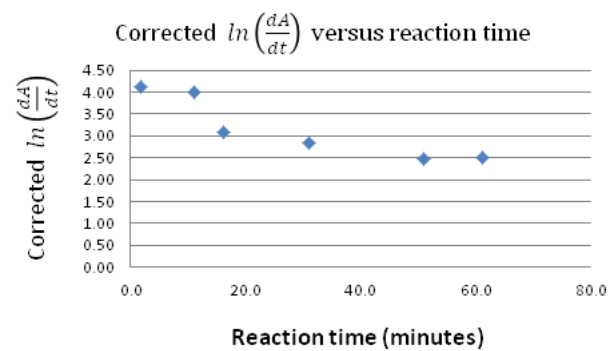


Figure 5: blahblah.

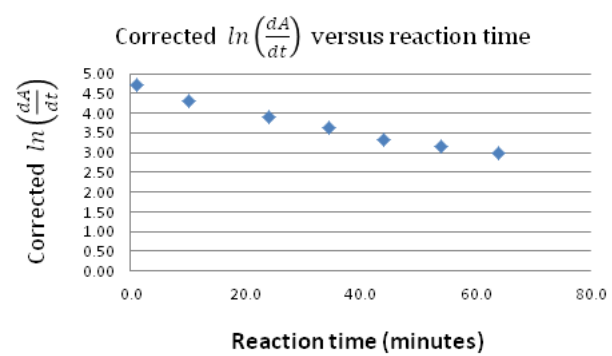


Figure 6: blahblah.

References

- (1) Killian, B. J. *Experiments for Physical Chemistry Laboratory*, Summer 2014, Target Copy: Gainesville, **2014**. 45 - 50.
- (2) Nelson, D. L.; Cox, M. M. *Lehninger Principles of Biochemistry*, 5th ed.; W. H. Freeman, 2008. 195 - 200.