CARBONIC ANHYDRASE: KINETICS OF REMOVAL OF Zn(II) By 2,6-PYRIDINECARBOXYLATE

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Abstract

In the past decade, supervised activity recognition methods have been studied by many researchers, however these methods still face many challenges in real world settings. Supervised activity recognition methods assume that we are provided with labeled training examples from a set of predefined activities. Annotating and hand labeling data is a very time consuming and laborious task. Also, the assumption of consistent pre-defined activities might not hold in reality. More importantly, these algorithms do not take into account the streaming nature of data, or the possibility that the patterns might change over time. In this chapter, we will provide an overview of the state of the art *unsupervised* methods for activity recognition. In particular, we will describe a scalable activity discovery and recognition method for complex large real world datasets, based on sequential data mining and stream data mining methods.

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Introduction

Carbonic anhydrase (CA) catalyzes the interconversion of carbon dioxide and carbonic acid/bicarbonate as follows:

$$CO_2 + H_2O \stackrel{CA}{\rightleftharpoons} H_2CO_3$$
 (1)

In the active form, CA is bound to a Zn²⁺ cofactor (denoted as CA·Zn), which it relies upon for its catalytic activity. The zinc ion can be stripped from the enzyme using a Lewis base ligand, which donates electrons to the ion to form a covalent bond. The ligand being studied in this experiment is 2,6-pyridinecarboxylate, commonly called dipicolinate (or dipic). Figure 1 shows the structure of dipic. In this experiment, the rate of zinc removal by dipic will be measured.

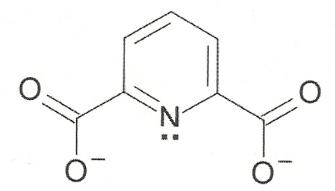


Figure 1: Structure of 2,6-pyridinecarboxylate (dipic) ¹

Mechanism

When [dipic] >> [CA], that is, when $\frac{[dipic]}{[CA]} \ge 25$, then the removal of zinc is pseudo-first-order with respect to CA·Zn because the concentration of dipic, denoted as L, does not change appreciably. Thus the formation of the inactive enzyme, apoCA, can be modeled

using the following rate equation:

$$\frac{d[\text{apoCA}]}{dt} = k_{obs}[\text{CA·Zn}]$$
 (2)

The pseudo-first-order rate constant, k_{obs} , increases as [L] increases, but levels off at sufficiently high concentrations of L. Biochemists will recognize behavior similar to Michaelis-Menten enzyme kinetics in which the enzyme, CA·Zn, and the substrate, L, reversibly form a CA·Zn·L complex with association constant K_{EML} (EML stands for Enzyme-Metal-Ligand):

$$CA \cdot Zn + L \stackrel{K_{EML}}{\longleftarrow} CA \cdot Zn \cdot L$$
 (3)

This can be modeled as follows:

$$K_{EML} = \frac{[\text{CA}\cdot\text{Zn}\cdot\text{L}]}{[\text{CA}\cdot\text{Zn}][\text{L}]}$$
(4)

CA·Zn·L can either revert back to the original species or irreversibly convert to the inactive form of the enzyme, apoCA, and the covalently bound zinc-dipic molecule, ZnL:

$$CA \cdot Zn \cdot L \xrightarrow{k_d} apoCA + ZnL$$
 (5)

This yields the following differential rate law:

$$\frac{d[\text{apoCA}]}{dt} = k_d[\text{CA}\cdot\text{Zn}\cdot\text{L}] \tag{6}$$

Note the difference in assumptions between this reaction and the Michaelis-Menten model; M-M kinetics assumes the enzyme is reformed and that only the substrate is modified, while (5) shows that both the substrate and the enzyme are permanently modified. Recall that $[L] >> [CA \cdot Zn]$, so [L] can be assumed to stay constant at $[L]_0$, which is substituted into a

rearranged form of equation (4),

$$[CA \cdot Zn \cdot L] = K_{EML}[CA \cdot Zn][L]_{0}$$
(7)

Carbonic anhydrase can exist in one of three forms: the metalloenzyme CA·Zn, the enzyme-metal-ligand complex CA·Zn·L, or the inactivated enzyme apoCA. Initially, all CA is tied up in the metalloenzyme, and none exists as CA·Zn·L or apoCA. As the activated form of the enzyme gets bound to L and then inactivated,

$$[CA \cdot Zn] = [CA \cdot Zn]_0 - [apoCA] - CA \cdot Zn \cdot L, \tag{8}$$

which can be combined with equation (7) to yield

$$[CA \cdot Zn] = [CA \cdot Zn]_0 - [apoCA] - K_{EML}[CA \cdot Zn][L]_0$$
(9)

and can be rearranged as follows:

$$[CA \cdot Zn] = \frac{[CA \cdot Zn]_0 - [apoCA]}{1 + K_{EML}[L]_0}$$
(10)

Equations (6) and (7) can be combined to give

$$\frac{d[\text{apoCA}]}{dt} = k_d K_{EML} [\text{CA-Zn}][L]_0$$
(11)

Therefore, the rate of apoCA formation is first-order with respect to CA·Zn. Combining equations (11) and (10) yields

$$\frac{d[\operatorname{apoCA}]}{dt} = k_d K_{EML}[L]_0 \frac{[\operatorname{CA} \cdot \operatorname{Zn}]_0 - [\operatorname{apoCA}]}{1 + K_{EML}[L]_0}$$
(12)

Rearranging and integrating,

$$\int_{[apoCA]_t}^{[apoCA]_t} \frac{d[apoCA]}{[CA \cdot Zn]_0 - [apoCA]_t} = \int_0^t \frac{k_d K_{EML}[L]_0}{1 + K_{EML}[L]_0} dt$$

$$= \frac{k_d K_{EML}[L]_0}{1 + K_{EML}[L]_0} t$$
(13)

The left side must be integrated using u-sub:

$$u = [CA \cdot Zn]_0 - [apoCA]_t$$

$$du = -d[apoCA]$$

To change the integral boundaries,

 $u(t=0) = [CA \cdot Zn]_0$, since no inactivated enzyme has been formed

$$u(t = t) = [CA \cdot Zn]_0 - [apoCA]_t$$

Therefore,

$$\int_{[apoCA]_{t}}^{[apoCA]_{t}} \frac{d[apoCA]}{[CA \cdot Zn]_{0} - [apoCA]_{t}} = -\int_{[CA \cdot Zn]_{0}}^{[CA \cdot Zn]_{0} - [apoCA]_{t}} \frac{du}{u}$$

$$= -ln(u) \Big|_{[CA \cdot Zn]_{0}}^{[CA \cdot Zn]_{0} - [apoCA]_{t}}$$

$$= -ln \left(\frac{[CA \cdot Zn]_{0} - [apoCA]}{[CA \cdot Zn]_{0}} \right)$$
(14)

Combining the evaluated integrals from equations (14) and (13) yields

$$ln\left(\frac{\left[\text{CA}\cdot\text{Zn}\right]_{0} - \left[\text{apoCA}\right]}{\left[\text{CA}\cdot\text{Zn}\right]_{0}}\right) = -\frac{k_{d}K_{EML}[L]_{0}}{1 + K_{EML}[L]_{0}}t\tag{15}$$

Assuming steady-state conditions for CA·Zn·L, that is, [CA·Zn·L] is always negligible, then $\frac{\text{[CA·Zn]}_0-\text{[apoCA]}}{\text{[CA·Zn]}_0}$ is simply the fraction of CA·Zn remaining after reaction time t and can be

referred to as $F_{\text{CA-Zn}}$:

$$ln\left(F_{\text{CA-Zn}}\right) = -\frac{k_d K_{EML}[L]_0}{1 + K_{EML}[L]_0} t \tag{16}$$

Since $-\frac{k_d K_{EML}[L]_0}{1+K_{EML}[L]_0}$ is a constant for a given concentration of dipic, equation (16) exhibits linear behavior. Therefore, a linear least squares regression procedure can be performed for measurements of $ln(F_{CA\cdot Zn})$ over time, and the slope, denoted $-k_{obs}$, will be

$$-k_{obs} = -\frac{k_d K_{EML}[L]_0}{1 + K_{EML}[L]_0}$$
 (17)

Taking the reciprocal of equation (17) yields

$$\frac{1}{k_{obs}} = \frac{1 + K_{EML}[L]_0}{k_d K_{EML}[L]_0}
= \frac{1}{k_d K_{EML}[L]_0} + \frac{K_{EML}[L]_0}{k_d K_{EML}[L]_0}
= \frac{1}{k_d K_{EML}} \times \frac{1}{[L]_0} + \frac{1}{k_d}$$
(18)

Again, a linear pattern is observed; measuring k_{obs} at several different dipic concentrations enables one to perform a least squares regression procedure on $\frac{1}{k_{obs}}$ versus $\frac{1}{[L]_0}$ to determine the slope, $m = \frac{1}{k_d K_{EML}}$, and intercept, $b = \frac{1}{k_d}$. k_d and K_{EML} are thus calculated as follows:

$$k_d = \frac{1}{b} \tag{19}$$

$$K_{EML} = \frac{b}{m} \tag{20}$$

Rate Measurements

While equations (16) and (17) seem to imply that the determination of k_{obs} requires knowing [CA·Zn] or [apoCA] at any point in time, in reality a plot of f(t) vs t, where f(t) is proportional to $F_{\text{CA·Zn}}$, will still exhibit the same slope $-k_{obs}$. The Michaelis-Menten kinetics model states that, for sufficiently large substrate concentrations, the enzyme is fully satu-

rated and the reaction velocity asymptotically approaches a number, $V_{max} = k_{cat}[\text{CA-Zn}]$, where k_{cat} (the "turnover number") is amount of substrate that can be converted to product by a single saturated enzyme molecule in a given unit of time.² Thus for sufficiently large concentrations of substrate, the enzyme catalytic activity fulfills the requirement of proportionality to $F_{\text{CA-Zn}}$. Ideally, the determination of the enzymatic activity from V_{max} , that is, an enzyme assay, can be done using a substrate which is cheap, readily available, and easily measurable. As Figure 2 shows, carbonic anhydrase happens to hydrolyze para-nitrophenyl acetate (pNPA):

$$O_2N$$
 O_2N O_2N O_2N O_3 O_4 O_4 O_5 O_5 O_6 O_7 O_8 O_8

Figure 2: Carbonic anhydrase-catalyzed hydrolysis of para-nitrophenyl acetate to para-nitrophenol and acetic acid

Data and Results



Figure 3: laksjdf askdfj asdkljfhaslkdjfhaklsdjfh asldkfjhasdlkjfhalksdjfhalksdjfh asldkfjhasdlkfjashdlfkajsdhflkajshdf asdfa sdiufhaisdu fas dfasd fasef asefase efasefkahsdkjfhaskldjfha sdfasldkfjhasdlfkjasdh falksdjfhalskdjfhasdlkfjah sdlkfjh aslkdjfhalksdjfhalksdjfhalksjdh flkajsdhf alsdkjfash dflaskdjfah.

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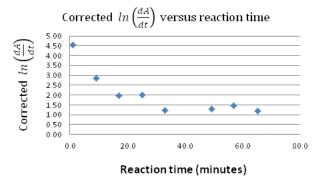


Figure 4: blahblah.

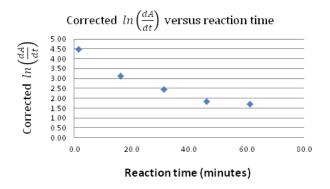


Figure 5: blahblah.



Figure 6: blahblah.



Figure 7: blahblah.

References

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