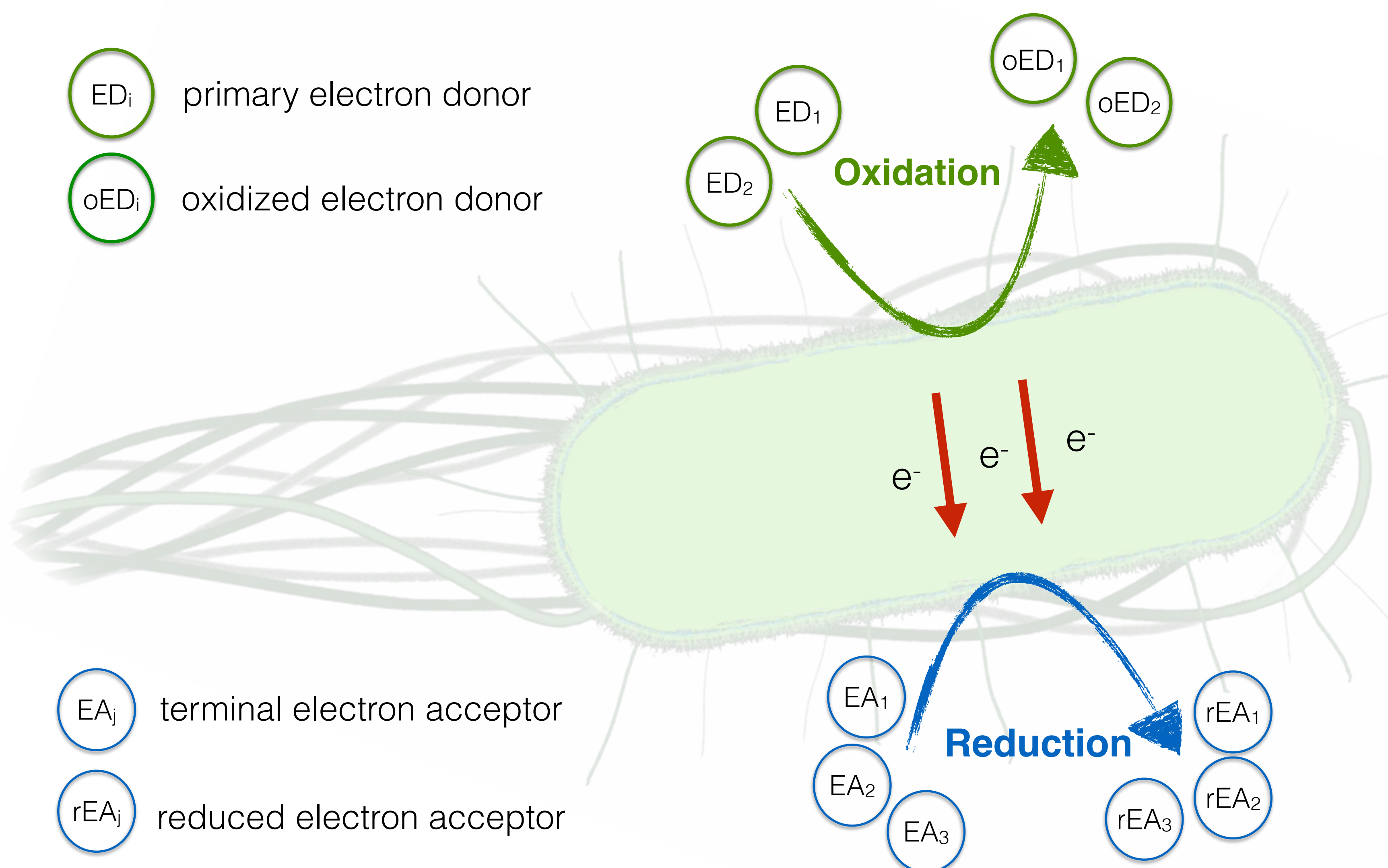


## Competition for electron donors (ED) and electron acceptors (EA)



$$R_i = k_i \cdot X \cdot \left[ \frac{C_{ED}}{K_{ED}^m + C_{ED}} \right]_i \cdot \left[ \frac{C_{EA}}{K_{EA}^m + C_{EA}} \right]_i \cdot F_T^i \cdot F_X^i$$

- $R_i$  - rate of oxidation of a  $i^{th}$  ED by the reduction of  $i^{th}$  EA
- $k_i$  - reaction rate constant per unit biomass
- $X$  - microbial biomass
- $C_{ED}$  - concentration of the electron donor
- $C_{EA}$  - concentration of the electron acceptor
- $K^m$  - half-saturation constant
- $F_T^i$  - thermodynamic term (LaRowe and Van Cappellen, 2011)
- $F_X^i$  - "inhibition" term

## Common practice

The most widely used expression to simulate the succession of electron acceptor utilization during the microbial degradation of organic matter is that of Humphrey (1972):

$$F_X^i = \prod_{j=1}^N \frac{K_I^{i-1}}{K_I^{i-1} + C_{EA}^{i-1}}$$

- $C_{EA}^{i-1}$  - concentrations of all oxidants stronger than the  $i^{th}$  EA
- $K_I^{i-1}$  - inhibition constant

### Drawbacks

- Inhibition model requires the **a priori assignment of the order** of EA utilization.
- Inhibition constants are specific to a particular set of environmental or experimental conditions and, hence, **lack general applicability**.
- The inhibition model cannot respond to variations in **dynamic conditions** that may reshuffle the order of EA or ED utilization (e.g., causing sulfate to be used before ferric iron oxyhydroxides – see Jakobsen R. & Postma D, 1999).

## Alternative approach

In energy-limited environments (e.g., the subsurface), microbial communities compete for energy substrates. We propose to represent this competition by taking into account the **power** ( $P_i$ ) of catabolic reactions:

$$P_i = -\Delta G_i^e \cdot R_i^e$$

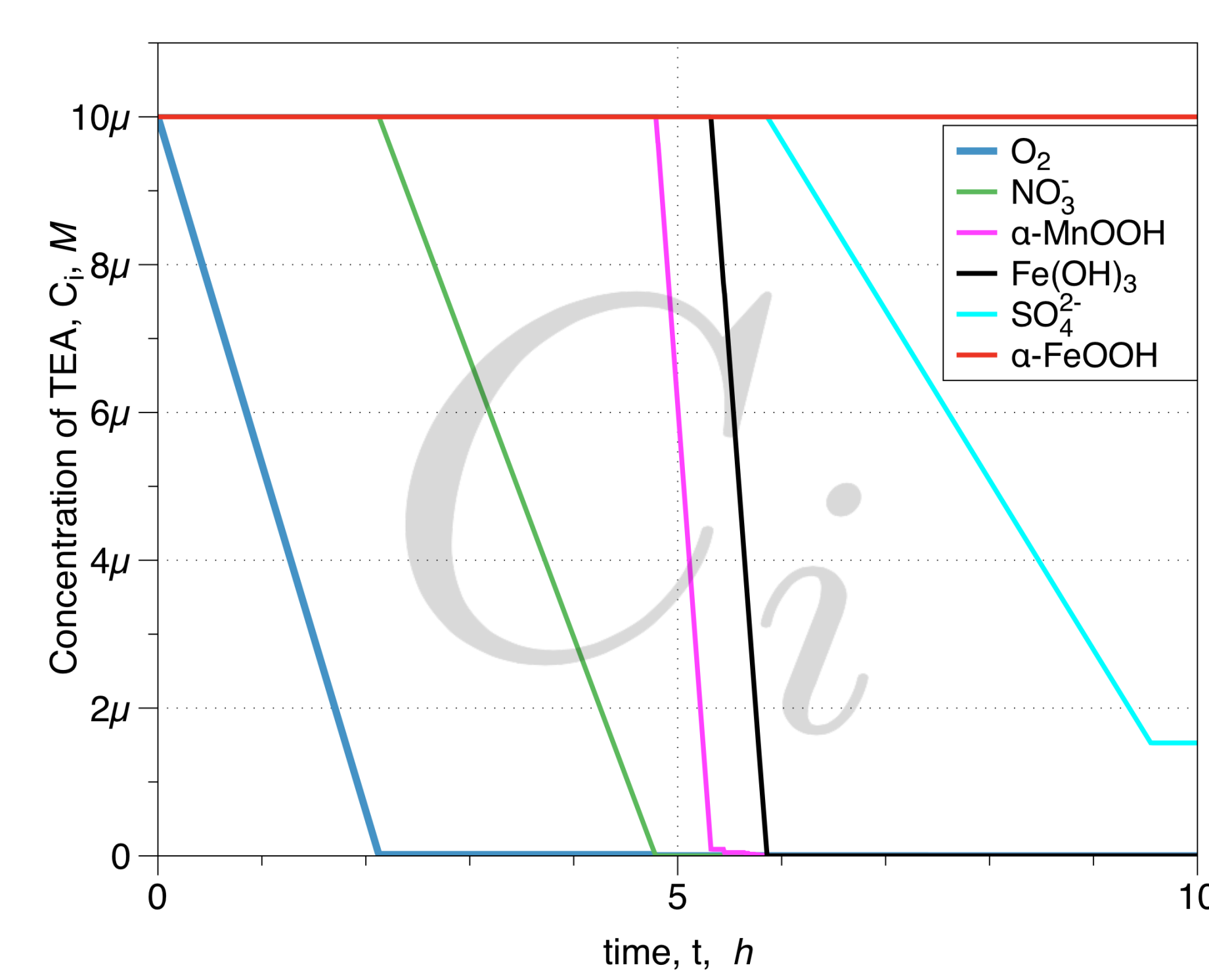
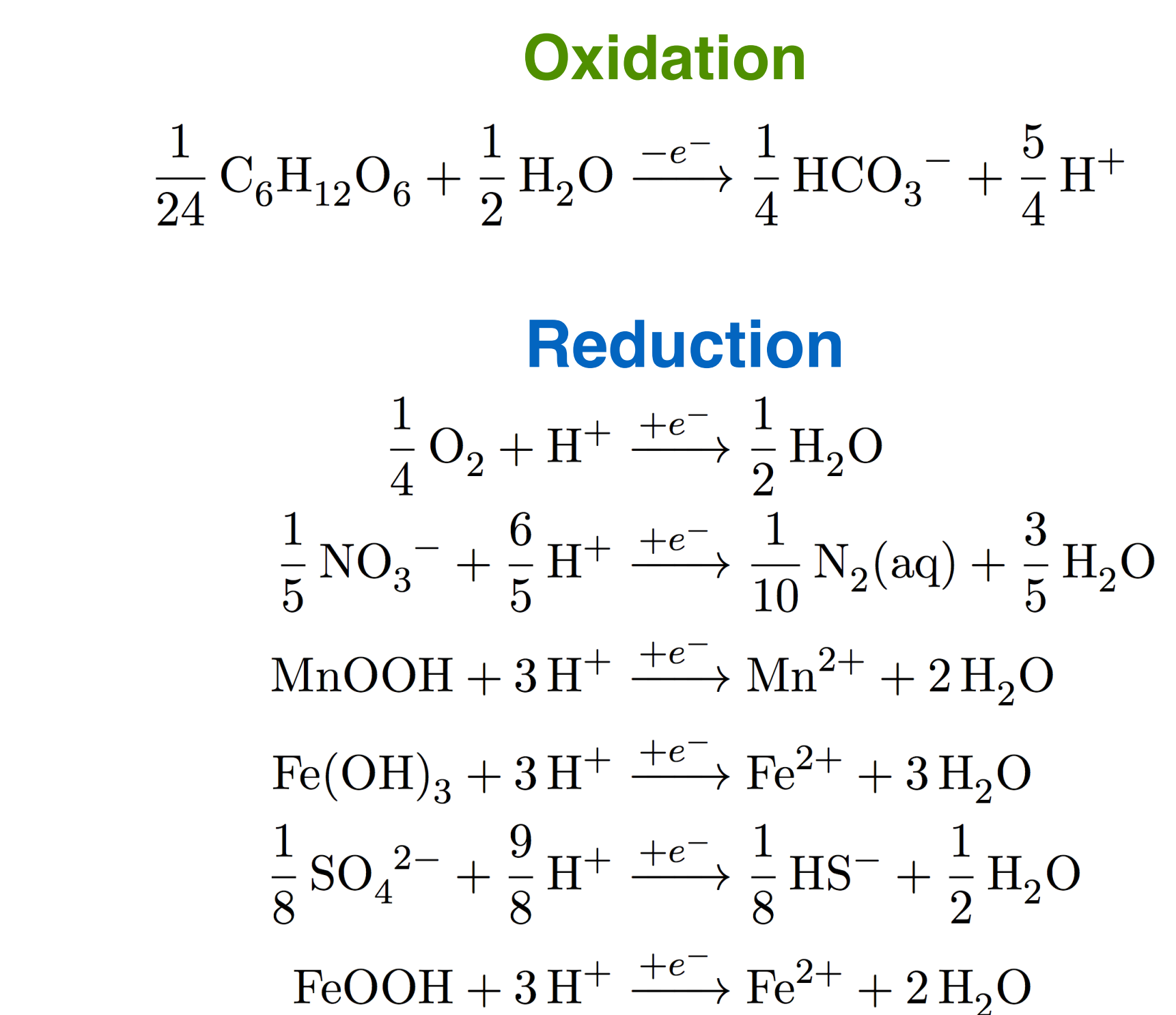
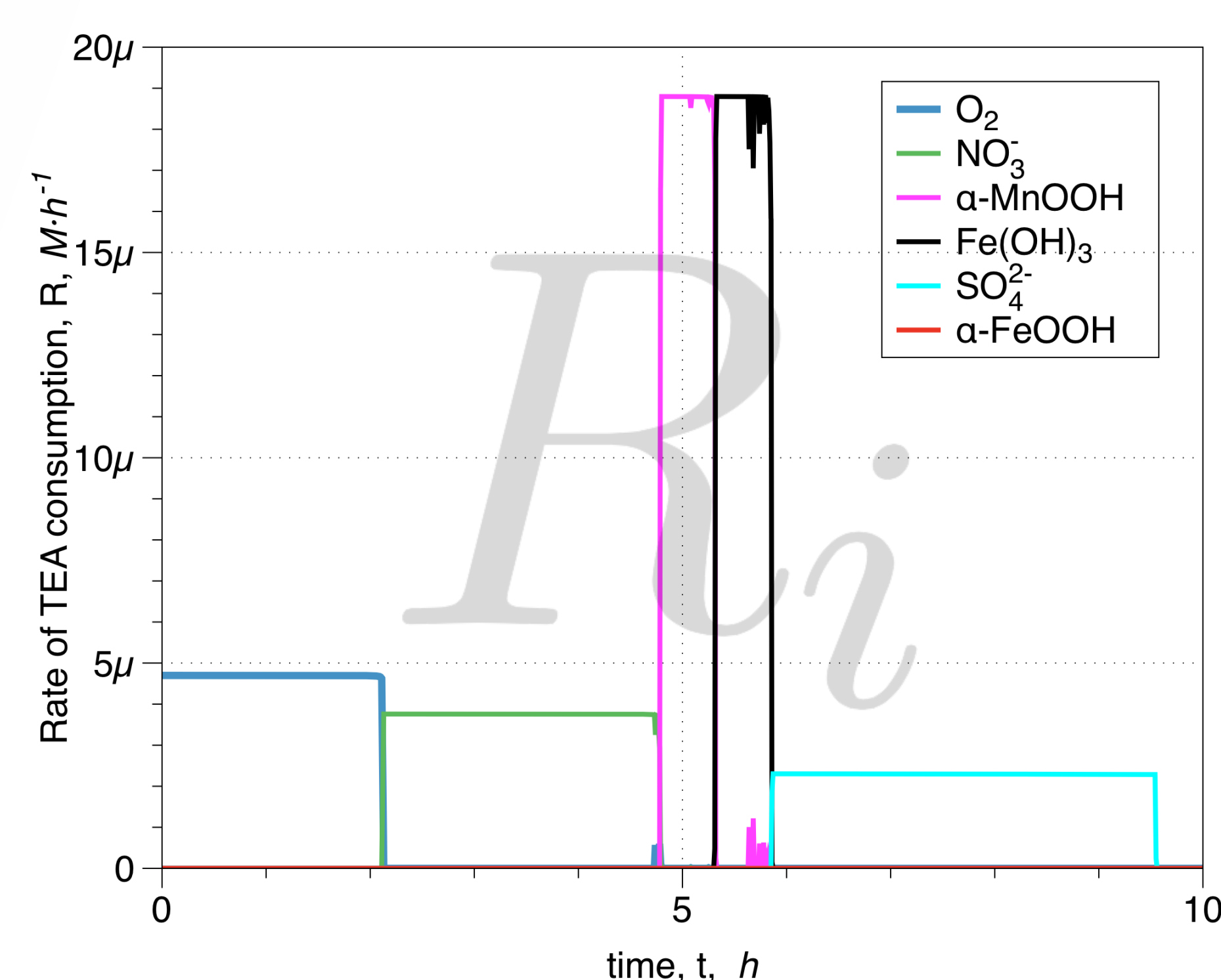
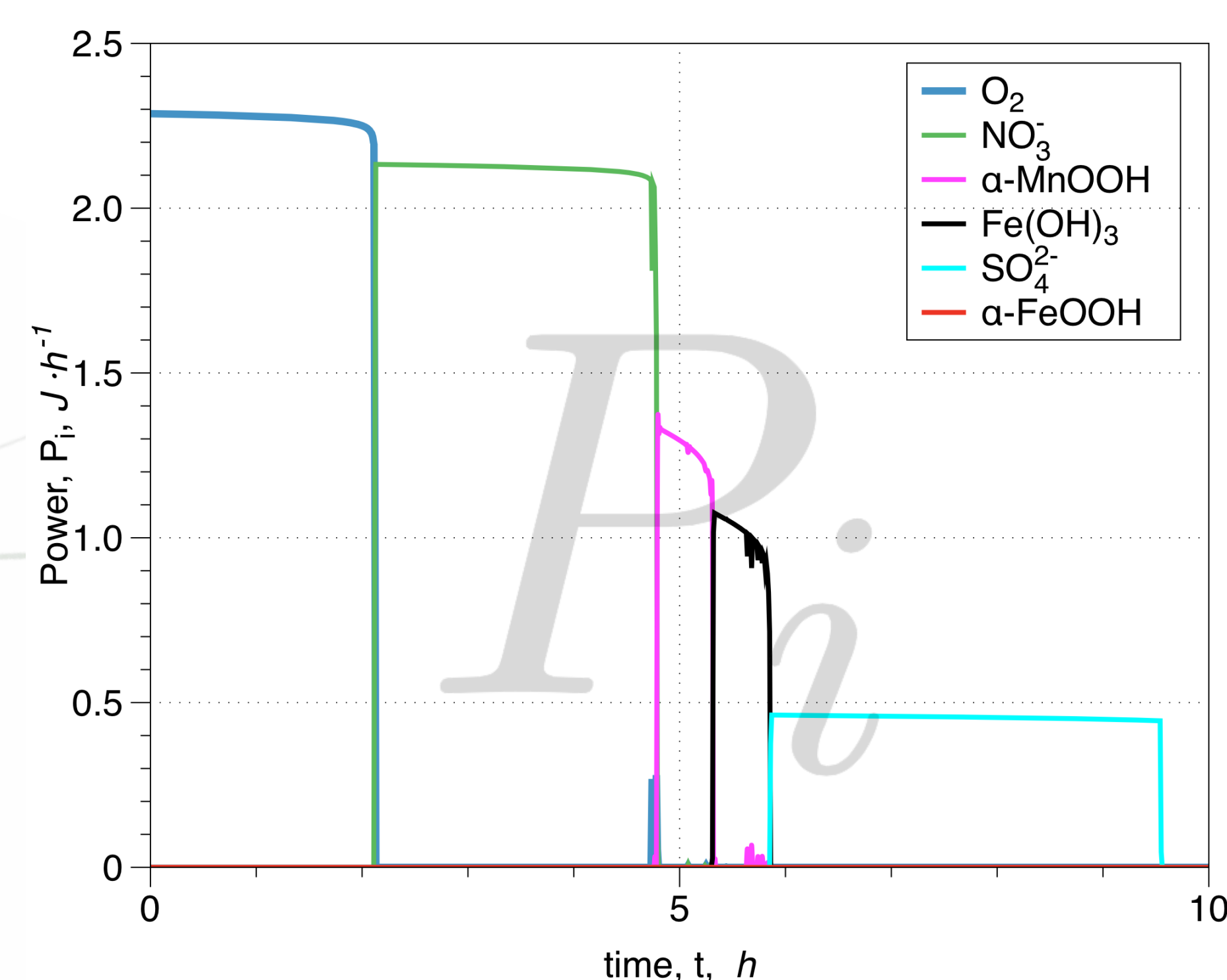
The sequence of redox reactions is now determined by the power that can be harvested by the microbial populations.

$$\begin{cases} \max \left\{ -\sum_{i=1}^N \Delta G_i^e \cdot R_i^e \cdot F_X^i \right\} \\ \sum_{i=1}^N F_X^i = 1 \\ F_X^i \geq 0 \end{cases} \quad \text{Optimize power generation!}$$

- $P_i$  - power produced by  $i^{th}$  redox reaction
- $\Delta G_i^e$  - Gibbs energy of the reaction per electron equivalent
- $R_i^e$  - rate of the reaction per electron equivalent
- $F_X^i$  - the **unknown**. The part of bacteria which utilize  $i^{th}$  reaction

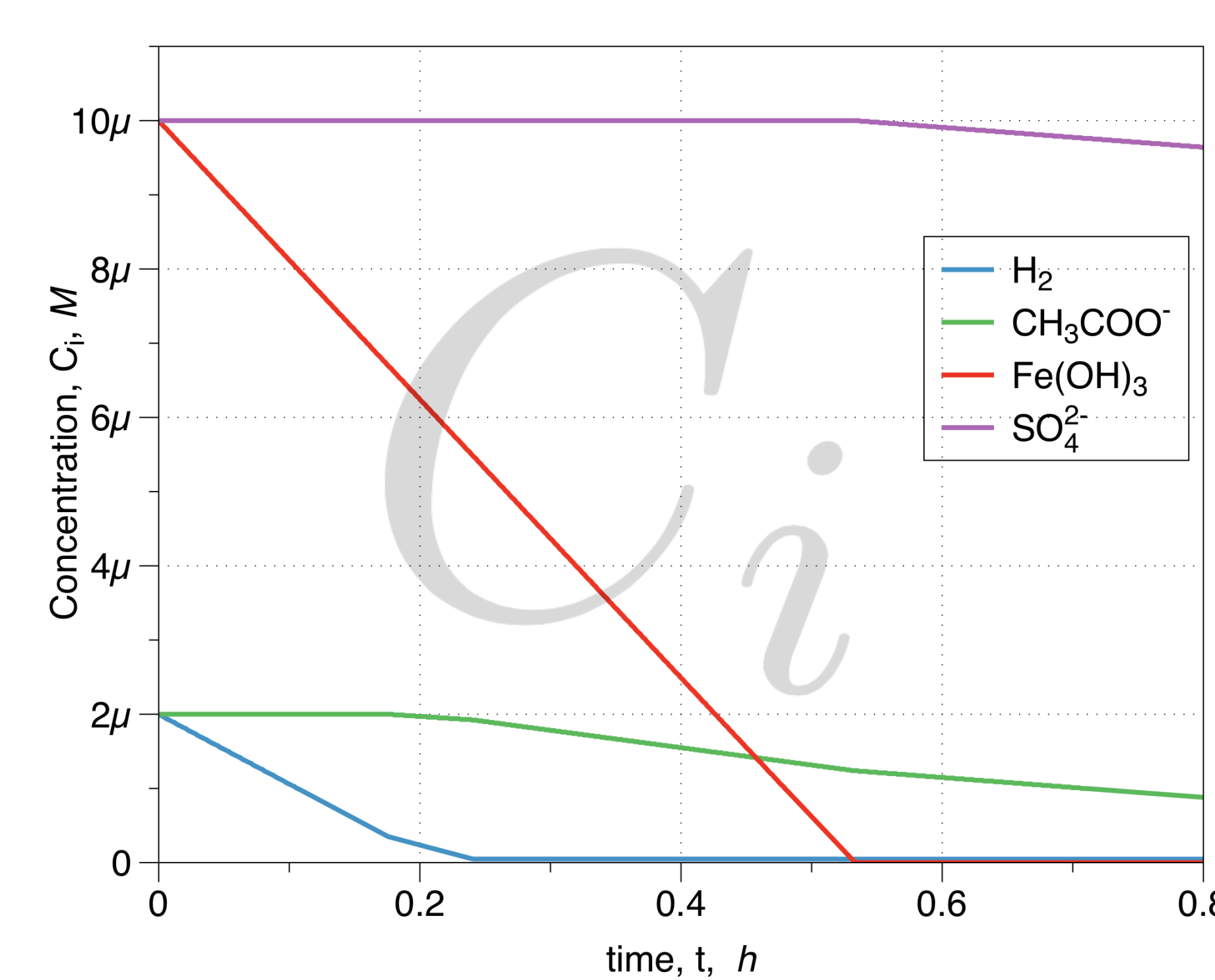
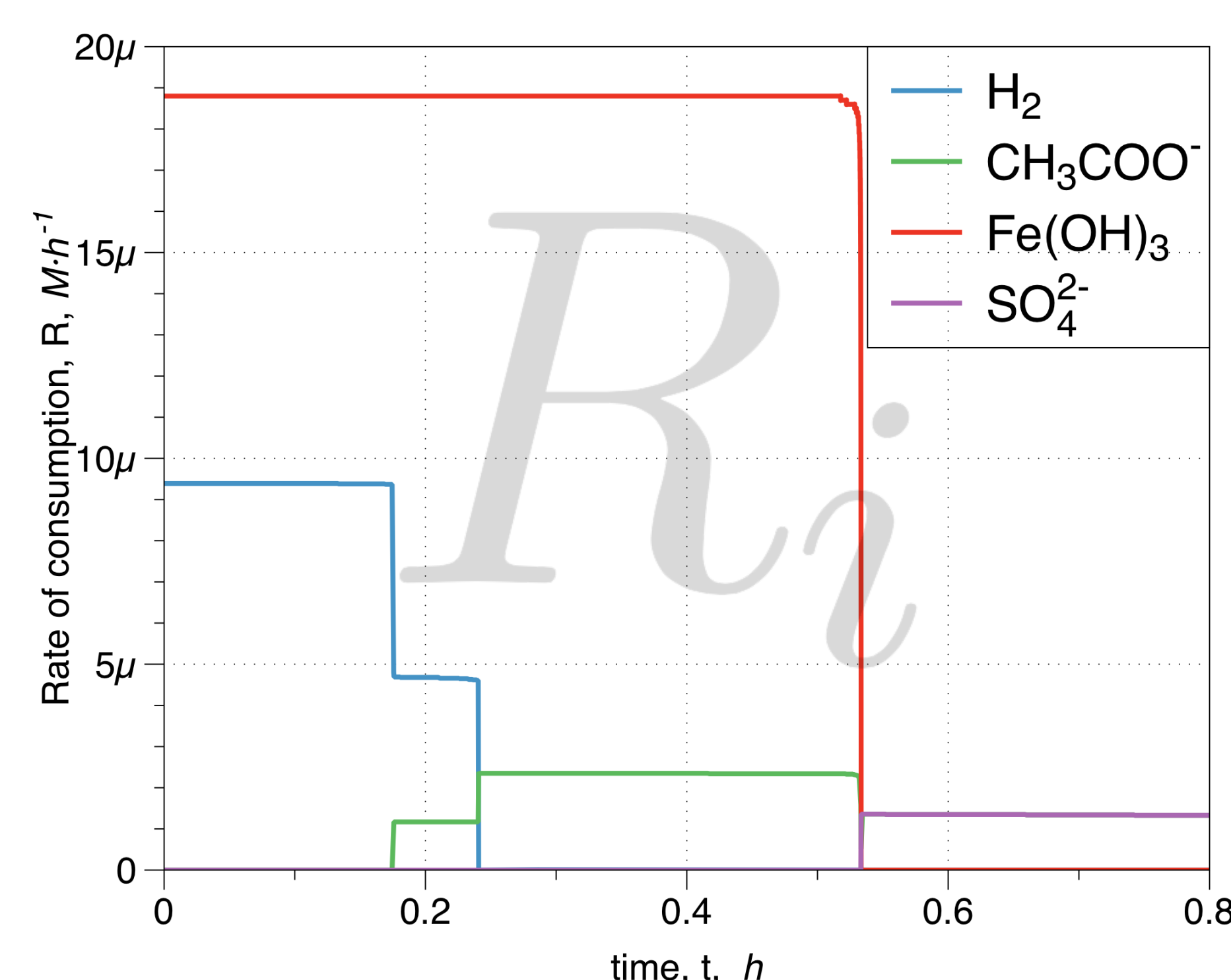
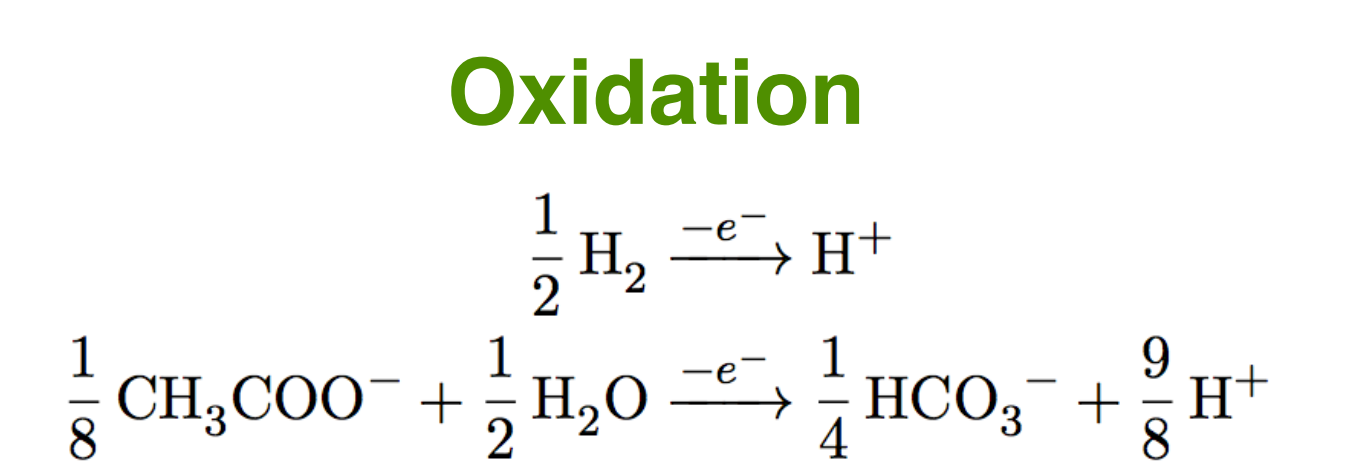
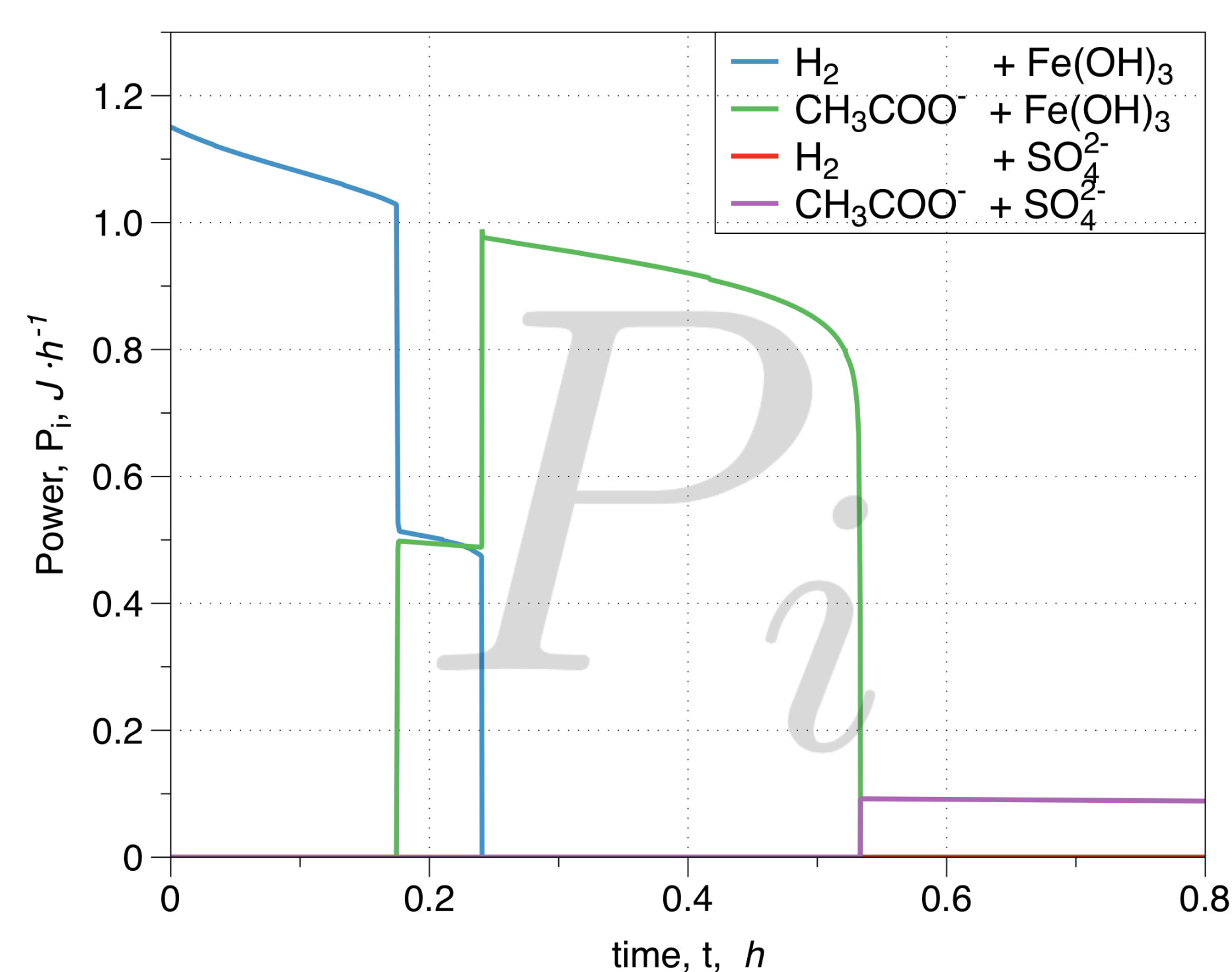
## Example: 1 ED and 6 EA

$$P[O_2] > P[NO_3^-] > P[\alpha\text{-MnOOH}] > P[Fe(OH)_3] > P[SO_4^{2-}] > P[\alpha\text{-FeOOH}]$$



## Example: 2 ED and 2 EA

$$P[H_2 + Fe(OH)_3] > P[CH_3COO^- + Fe(OH)_3] > P[CH_3COO^- + SO_4^{2-}] > P[H_2 + SO_4^{2-}]$$



## Geochemical implications

Using an approach based on the **optimization of the power** generated by catabolic processes allows one to account for **dynamic** environmental conditions (e.g., variability of temperature, pH, ionic strength, activities of redox active species). The method can be applied to simulate the redox stratification observed in **early diagenesis** and other **energy-limited environments**, such as oligotrophic aquifers, where energy substrates are in low abundance.

## References

- Humphrey A. E. (1972). Adv. Chem, p. 630-650
- Jakobsen R. & Postma D. (1999). Geochim. Cosmochim. Acta, p. 137-151
- LaRowe D. E. & Van Cappellen P. (2011). Geochim. Cosmochim. Acta, p. 2030-2042

