

# Modeling of Combined Lead Fast Reactor and Concentrating Solar Power Supercritical Carbon Dioxide Cycles to Demonstrate Feasibility, Efficiency Gains, and Cost Reductions

Brian White <sup>1</sup>, Michael Wagner <sup>1</sup>, Ty Neises <sup>3</sup>, Cory Stansbury <sup>4</sup>, and Ben Lindley <sup>2\*</sup>

<sup>1</sup> Department of Mechanical Engineering, University of Wisconsin - Madison, 1415 University Drive, Madison, WI 53706, United States; dept@me.engr.wisc.edu

<sup>2</sup> Department of Engineering Physics, University of Wisconsin - Madison, 1500 Engineering Drive, Madison, WI 53706, United States; EMAIL

<sup>3</sup> National Renewable Energy Laboratory, Thermal Systems Group, 15013 Denver West Parkway, Golden, CO 80401, United States; EMAIL

<sup>4</sup> Westinghouse Electric Company, Lead Fast Reactor Systems Development, ADDRESS United States; EMAIL

\* Correspondence: lindely2@wisc.edu (B.L.); Tel.: +1-608-265-2001 (B.L.)

**Abstract:** Separate cycles for solar concentrating power and lead fast reactors, which innately have issues with weather, grid demand, and time of day, have potential to benefit when coupled together in a supercritical CO<sub>2</sub> Brayton cycle. Combining these cycles could allow for the lead fast reactor cycle to thermally charge the salt storage in the solar concentrating power cycle during low demand periods and be utilized when grid demand increases. The implementation of the independent cycles into one cycle is modeled to find the preferred location of the lead fast reactor heat exchanger, concentrating solar power heat exchanger, salt charging heat exchanger, turbines, and recuperators within the supercritical CO<sub>2</sub> Brayton cycle. Three cycle configurations have been studied: a two-cycle configuration which uses CSP and LFR heat for dedicated turbocompressors, combined cycle with two high temperature recuperators for both the CSP and LFR, and a combined cycle with CSP and LFR heat sources in parallel. [CONCLUSION]

**Keywords:** Supercritical carbon dioxide Brayton Cycle; Concentrating Solar Power (CSP); Lead Fast Reactor (LFR), Cogeneration, Combined Cycle, Thermal Energy Storage (TES)

**Citation:** White, B.; Lindley, B.; Wagner, M. Modeling of Combined Lead Fast Reactor and Concentrating Solar Power Supercritical Carbon Dioxide Cycles to Demonstrate Feasibility, Efficiency Gains, and Cost Reductions. *Sustainability* **2021**, *1*, 0. <https://doi.org/>

Received:  
Accepted:  
Published:

**Publisher's Note:** MDPI stays neutral with regard to jurisdictional claims in published maps and institutional affiliations.

**Copyright:** © 2021 by the authors. Submitted to *Sustainability* for possible open access publication under the terms and conditions of the Creative Commons Attribution (CC BY) license (<https://creativecommons.org/licenses/by/4.0/>).

## 1. Introduction

## 2. Materials and Methods

### 2.1. Cycle Component Modeling

#### 2.1.1. Heat Exchangers

#### 2.1.2. Turbines

#### 2.1.3. Compressors

#### 2.1.4. Concentrating Solar Power Cycle

### 2.2. Cycle Models

## 3. Results

There are various cycles that have been modeled to test their advantages and disadvantages. These various models cycles two different categories: non-charging and charging. The non-charging category will decide the configuration of the cycle with a focus on generating electricity. This includes the number of turbines, recuperators, and where heat is put into the system by the CSP and LFR. The charging category tests different locations of where heat is drawn from the LFR to be stored in the CSP's TES for later use.

### 3.1. Non-Charging Cycle Configurations

The cycles presented are generalized in order to draw a more direct comparison between cycles. These general parameters include isentropic efficiencies, heat exchanger approach temperatures, pressures, heat input, and pump constants. These values are summarized in Table 1.

**Table 1.** Constant cycle parameters with definition, variable and set value.

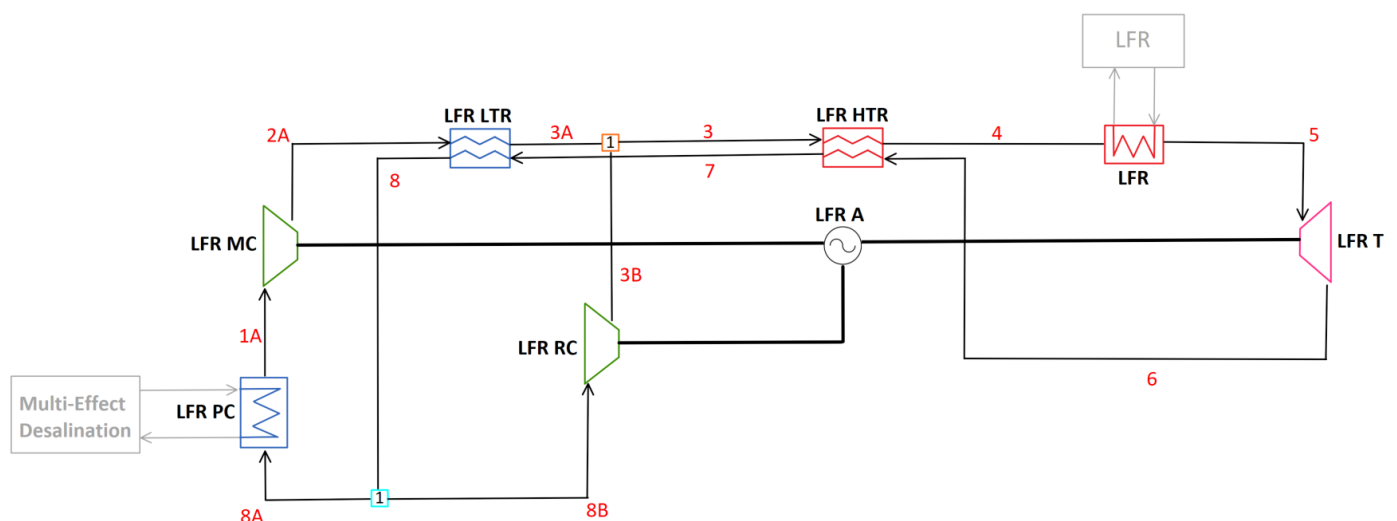
Parameter	Variable	Design Point Value
<i>Efficiencies</i>		
Main Compressor	$\eta_{MC}$	0.91 (-)
Re-Compressor	$\eta_{RC}$	0.89 (-)
Turbine	$\eta_T$	0.90 (-)
Pump	$\eta_P$	0.90 (-)
<i>Approach Temperatures</i>		
Low Temperature Recuperator	$\delta_{LTR}$	10 (K)
High Temperature Recuperator	$\delta_{HTR}$	10 (K)
Concentrating Solar Power Heat Exchanger	$\delta_{CSPHX}$	10 (K)
<i>Pressures</i>		
Pressure Ratio	$PR$	3.27 (-)
High Side Pressure	$P_{2A}$	2.88e7 (Pa)
<i>Heat Into System</i>		
Lead-Fast Reactor Heat Transfer	$\dot{Q}_{LFRHX}$	9.5e8 (W)
Concentrating Solar Power Heat Transfer	$\dot{Q}_{CSP}$	7.5e8 (W)
<i>Temperature</i>		
Main Compressor Inlet	$T_{1A}$	313.2 (K)
Lead-Fast Reactor Low Temperature	$T_4, T_{1C}, T_{5A}, T_{4C}$	673.2 (K)
<i>Pumps</i>		
Pressure Rise Across Pump	$\Delta_P$	3.726e6 (Pa)
Pump Low Side Pressure	$P_{S5-B}$	3.0e6 (Pa)

The values displayed in Table 1 are representative of LFR and CSP design while being consistent with design parameters given by our industry partner, Westinghouse Electric Corporation.

#### 3.1.1. Two-Cycle Configuration: C-LFR-ON and C-CSP-ON

The first cycle that will be tested has independent sCO<sub>2</sub> loops bridged by the CSP. This cycle has two Brayton Cycles: a LFR cycle and a CSP cycle. These two cycles individually operate when the focus of plant operation is primarily electricity generation.

The LFR cycle for this two-cycle configuration is labeled as C-LFR-ON and the cycle diagram is illustrated in Figure 1.



**Figure 1.** Diagram for C-LFR-ON with focus on electricity generation

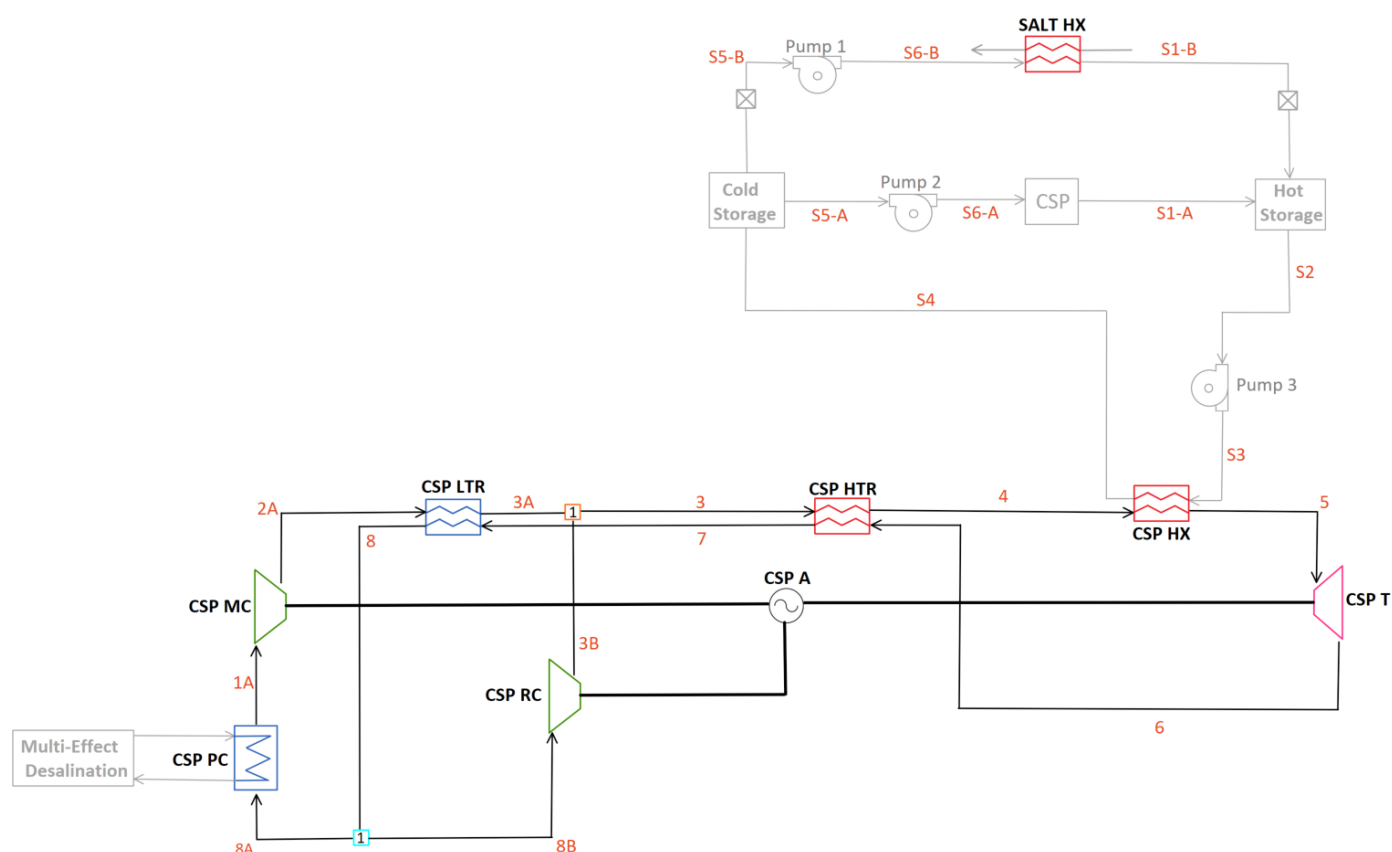
Modeling the C-LFR-ON cycle in EES yielded the results in Table 2. Two separate sensitivity studies were completed on the LFR inlet temperature. The unconstrained (*U*) values were from parametric studies on mass flow to the main compressor while maximizing cycle efficiency. The constrained (*C*) values were calculated by setting the LFR inlet temperature to the design value of 673.2 K.

**Table 2.** Calculated system parameters for non-charging C-LFR-ON cycle configuration with constrained (*C*) and unconstrained (*U*) Lead-Fast Reactor low-end temperature.

Definition	Variable	<i>U</i>	<i>C</i>
LFR Inlet Temperature (K)	$T_4$	Data	Data
Cycle Efficiency (%)	$\eta_{cycle}$	Data	Data
Alternator Power (W)	$\dot{W}_A$	Data	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data	Data
MC Power (W)	$\dot{W}_{MC}$	Data	Data
RC Power (W)	$\dot{W}_{RC}$	Data	Data
Turbine Power (W)	$\dot{W}_T$	Data	Data
MC Mass Flow Fraction (-)	$y_1$	Data	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data	Data
LTR Effectiveness (-)	$\varepsilon_{LTR}$	Data	Data
HTR UA Value (W/K)	$UA_{HTR}$	Data	Data
HTR Capacitance Ratio (-)	$CR_{HTR}$	Data	Data
HTR Heat Transfer Rate (W)	$\dot{Q}_{HTR}$	Data	Data
HTR Effectiveness (-)	$\varepsilon_{HTR}$	Data	Data

## Discussion of Results

The CSP cycle for this two-cycle configuration is labeled C-CSP-ON and the cycle diagram is shown in Figure 2. The CSP is shown in this diagram with the necessary pumps, TES tanks, and salt heat exchanger.



**Figure 2.** Diagram for C-CSP-ON with focus on electricity generation

C-CSP-ON is not directly impacted by constrained or unconstrained LFR low temperatures because it is an independent cycle while focused on electricity generation. Instead a sensitivity study was done on the temperature of the cold TES. Two temperatures were tested, 663.2 K and 713.2 K, to observe the impacts on cycle efficiency. The EES model outputs for C-CSP-ON are listed in Table 3.

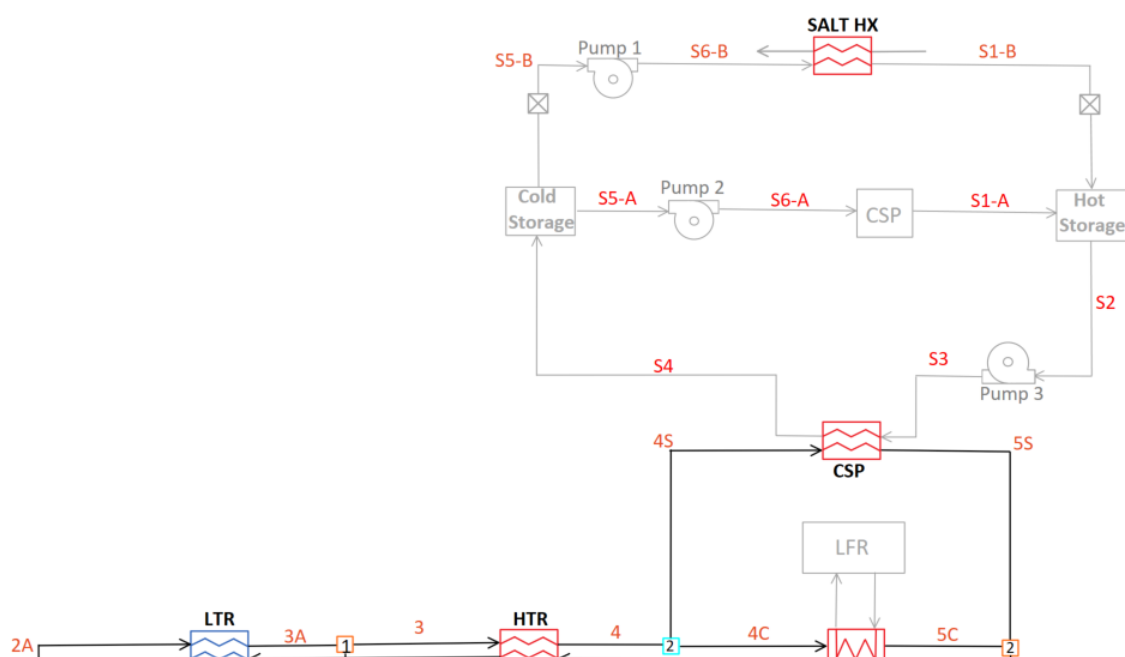
**Table 3.** Calculated system parameters for non-charging C-CSP-ON cycle configuration with varied TES cold temperature.

Definition	Variable		
Cold TES Temperature (K)	$T_{CS}$	Data	Data
Cycle Efficiency (%)	$\eta_{cycle}$	Data	Data
Alternator Power (W)	$\dot{W}_A$	Data	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data	Data
MC Power (W)	$\dot{W}_{MC}$	Data	Data
RC Power (W)	$\dot{W}_{RC}$	Data	Data
Turbine Power (W)	$\dot{W}_T$	Data	Data
MC Mass Flow Fraction (-)	$y_1$	Data	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data	Data
LTR Effectiveness (-)	$\varepsilon_{LTR}$	Data	Data
HTR UA Value (W/K)	$UA_{HTR}$	Data	Data
HTR Capacitance Ratio (-)	$CR_{HTR}$	Data	Data
HTR Heat Transfer Rate (W)	$\dot{Q}_{HTR}$	Data	Data
HTR Effectiveness (-)	$\varepsilon_{HTR}$	Data	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data	Data
CSPHX Effectiveness (-)	$\varepsilon_{CSPHX}$	Data	Data

## Discussion of Results

### 3.1.2. C-1HTR1T-ON

One of the drawbacks of having a two-cycle design as seen in the C-LFR-ON and C-CSP-ON is the number of system components is essentially doubled. Combining the two cycles into one would reduce this redundancy. Heat addition from the CSP and LFR in parallel orientation was therefore studied in the C-1HTR1T-ON model. This model is important to study the impact on cycle efficiency when mixing different temperature flows prior to the turbine. The diagram for this cycle is illustrated in Figure 3.



In this cycle the LFR and CSP are linked due to the parallel orientation. Therefore, three sensitivity studies were done on the C-1HTR1T-ON EES model. The initial two studies had the low LFR temperature constrained to the value of 673.2 K with varied cold CSP TES and maximized cycle efficiency. The two tested values for cold CSP TES with constrained LFR low temperature were 683.2 K and 713.2 K. The desired cold CSP TES temperature of 663.2 K was not possible with the constraint on the LFR low temperature. To obtain the desired cold CSP TES temperature, the constraint was removed dropping the temperature of the LFR inlet to 653.2 K. These values are displayed in Table 4.

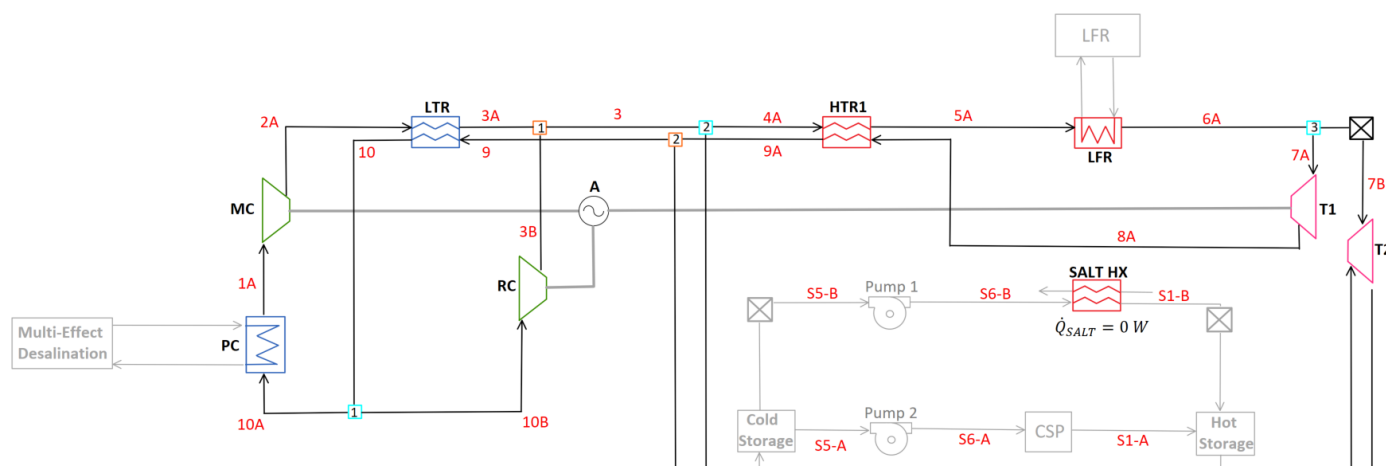
**Table 4.** Calculated system parameters for non-charging C-1HTR1T-ON cycle configuration with constrained (C) and unconstrained (U) Lead-Fast Reactor low-end temperature. Temperature of TES cold temperature is also varied.

Definition	Variable	C-1HTR1T-ON		
		U	C	C
Cold TES Temperature (K)	$T_{CS}$	Data	Data	Data
LFR Inlet Temperature (K)	$T_{4C}$	Data	Data	Data
Cycle Efficiency (%)	$\eta_{cycle}$	Data	Data	Data
Alternator Power (W)	$\dot{W}_A$	Data	Data	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data	Data	Data
MC Power (W)	$\dot{W}_{MC}$	Data	Data	Data
RC Power (W)	$\dot{W}_{RC}$	Data	Data	Data
Turbine Power (W)	$\dot{W}_T$	Data	Data	Data
MC Mass Flow Fraction (-)	$y_1$	Data	Data	Data
LFR Mass Flow Fraction (-)	$y_2$	Data	Data	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data	Data	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data	Data	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data	Data	Data
LTR Effectiveness (-)	$\epsilon_{LTR}$	Data	Data	Data
HTR UA Value (W/K)	$UA_{HTR}$	Data	Data	Data
HTR Capacitance Ratio (-)	$CR_{HTR}$	Data	Data	Data
HTR Heat Transfer Rate (W)	$\dot{Q}_{HTR}$	Data	Data	Data
HTR Effectiveness (-)	$\epsilon_{HTR}$	Data	Data	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data	Data	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data	Data	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data	Data	Data
CSPHX Effectiveness (-)	$\epsilon_{CSPHX}$	Data	Data	Data

## Discussion of Results

### 3.1.3. C-2HTR3T-ON

Mixing two different temperature flows before the turbine in a Brayton cycle has a negative effect on cycle efficiency. To quantify the reduction in cycle efficiency, another cycle with no mixing prior to the turbine was desired. This cycle is labeled at C-2HTR3T-ON. This cycle, seen in Figure 4, has two high temperature recuperators and three turbines.



Three sensitivity studies were done on the C-2HTR3T-ON model. Two with the LFR low temperature constrained and one without this constraint. The two constrained studies had varied cold CSP TES temperature with the lowest temperature of 663.2 K and highest temperature of 713.2 K. The unconstrained low LFR inlet study was done at a cold CSP TES temperature of 663.2 K. The calculated values from these studies are displayed in Table 5.

**Table 5.** Calculated system parameters for non-charging C-2HTR3T-ON cycle configuration with constrained (C) and unconstrained (U) Lead-Fast Reactor low-end temperature.

Definition	Variable	C-2HTR3T-ON		
		$U$	$C$	$C$
Cold TES Temperature (K)	$T_{CS}$	Data	Data	Data
LFR Inlet Temperature (K)	$T_{5A}$	Data	Data	Data
Cycle Efficiency (%)	$\eta_{cycle}$	Data	Data	Data
Alternator Power (W)	$\dot{W}_A$	Data	Data	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data	Data	Data
MC Power (W)	$\dot{W}_{MC}$	Data	Data	Data
RC Power (W)	$\dot{W}_{RC}$	Data	Data	Data
T1 Power (W)	$\dot{W}_{T1}$	Data	Data	Data
T2 Power (W)	$\dot{W}_{T2}$	Data	Data	Data
MC Mass Flow Fraction (-)	$y_1$	Data	Data	Data
LFR Mass Flow Fraction (-)	$y_2$	Data	Data	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data	Data	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data	Data	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data	Data	Data
LTR Effectiveness (-)	$\varepsilon_{LTR}$	Data	Data	Data
HTR1 UA Value (W/K)	$UA_{HTR1}$	Data	Data	Data
HTR1 Capacitance Ratio (-)	$CR_{HTR1}$	Data	Data	Data
HTR1 Heat Transfer Rate (W)	$\dot{Q}_{HTR1}$	Data	Data	Data
HTR1 Effectiveness (-)	$\varepsilon_{HTR1}$	Data	Data	Data
HTR2 UA Value (W/K)	$UA_{HTR2}$	Data	Data	Data
HTR2 Capacitance Ratio (-)	$CR_{HTR2}$	Data	Data	Data
HTR2 Heat Transfer Rate (W)	$\dot{Q}_{HTR2}$	Data	Data	Data
HTR2 Effectiveness (-)	$\varepsilon_{HTR2}$	Data	Data	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data	Data	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data	Data	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data	Data	Data
CSPHX Effectiveness (-)	$\varepsilon_{CSPHX}$	Data	Data	Data

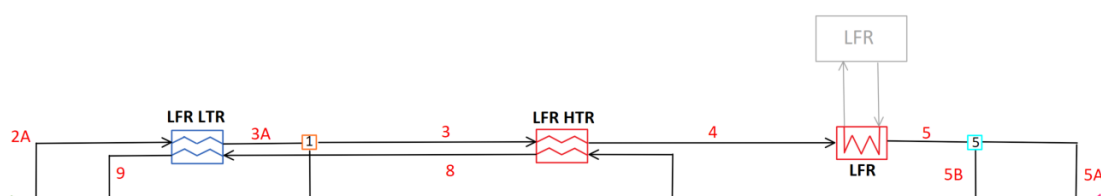
## Discussion of Results

### 3.2. Thermal Energy Storage Charging Techniques

When the grid demand is not high, the non-charging cycle configurations focus on an energy storage operating mode. Alternator power is set to zero and power from the turbine is solely powering the two compressors. The excess energy from the LFR is thermally stored in the TES for later use instead of generating electricity. Comparison of where thermal energy is drawn from the cycle is done by using the same recompression cycle and configuring the salt heat exchanger in different locations around the turbine.

### 3.2.1. C-LFR-PRE

Flow leaves the turbine with excess thermal energy that was not transformed into mechanical energy. This thermal energy can be used to charge the hot CSP TES. The diagram outlining this process is C-LFR-PRE in Figure 5.



Problems arise with this salt charging configuration. The primary issue is that the temperature out of the turbine is not high enough to charge the hot CSP TES to the required value of 833.2 K. To raise the temperature, some of the high temperature flow before the turbine is redirected through a valve and combined after the turbine. This combination of different temperature flows has a large impact on heat storage efficiency. The calculations from this TES charging technique are shown in Table 6.

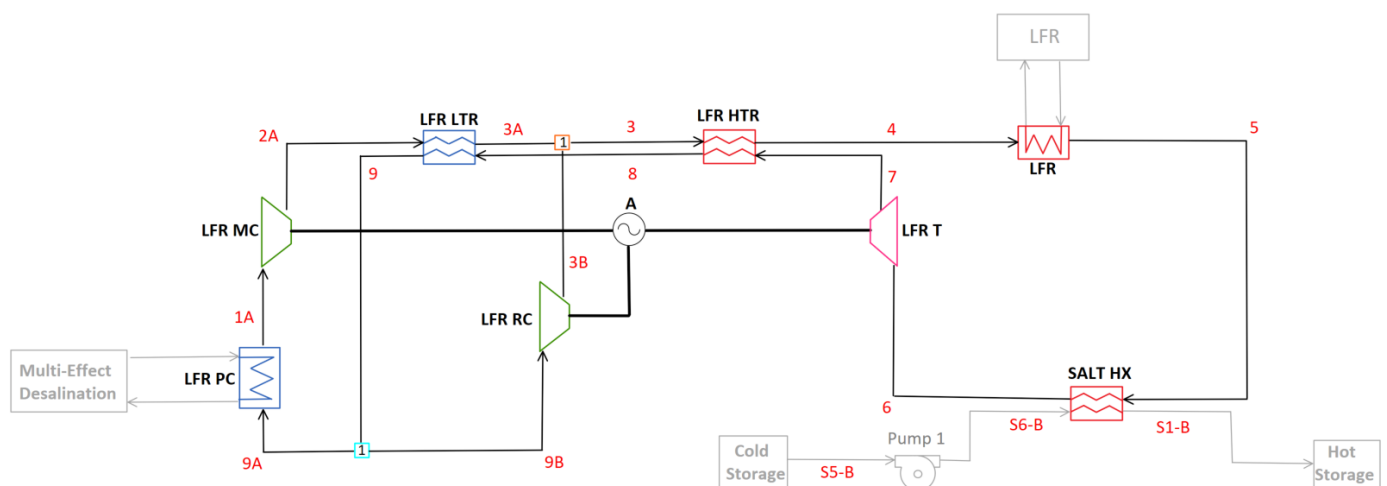
**Table 6.** Calculated system parameters for salt charging C-LFR-PRE cycle configuration with TES cold storage set to 663.2 K.

Definition	Variable	C-LFR-PRE C
Cold TES Temperature (K)	$T_{CS}$	Data
LFR Inlet Temperature (K)	$T_4$	Data
Heat Storage Efficiency (%)	$\eta_{heatstorage}$	Data
Alternator Power (W)	$\dot{W}_A$	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data
MC Power (W)	$\dot{W}_{MC}$	Data
RC Power (W)	$\dot{W}_{RC}$	Data
Turbine Power (W)	$\dot{W}_T$	Data
MC Mass Flow Fraction (-)	$y_1$	Data
Valve Mass Flow Fraction (-)	$y_5$	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data
LTR Effectiveness (-)	$\epsilon_{LTR}$	Data
HTR UA Value (W/K)	$UA_{HTR}$	Data
HTR Capacitance Ratio (-)	$CR_{HTR}$	Data
HTR Heat Transfer Rate (W)	$\dot{Q}_{HTR}$	Data
HTR Effectiveness (-)	$\epsilon_{HTR}$	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data
CSPHX Effectiveness (-)	$\epsilon_{CSPHX}$	Data

## Discussion of Results

### 3.2.2. C-LFR-POST

Moving the heat extraction prior to the turbine was qualitatively analyzed in C-LFR-POST. This diagram is seen in Figure 6.



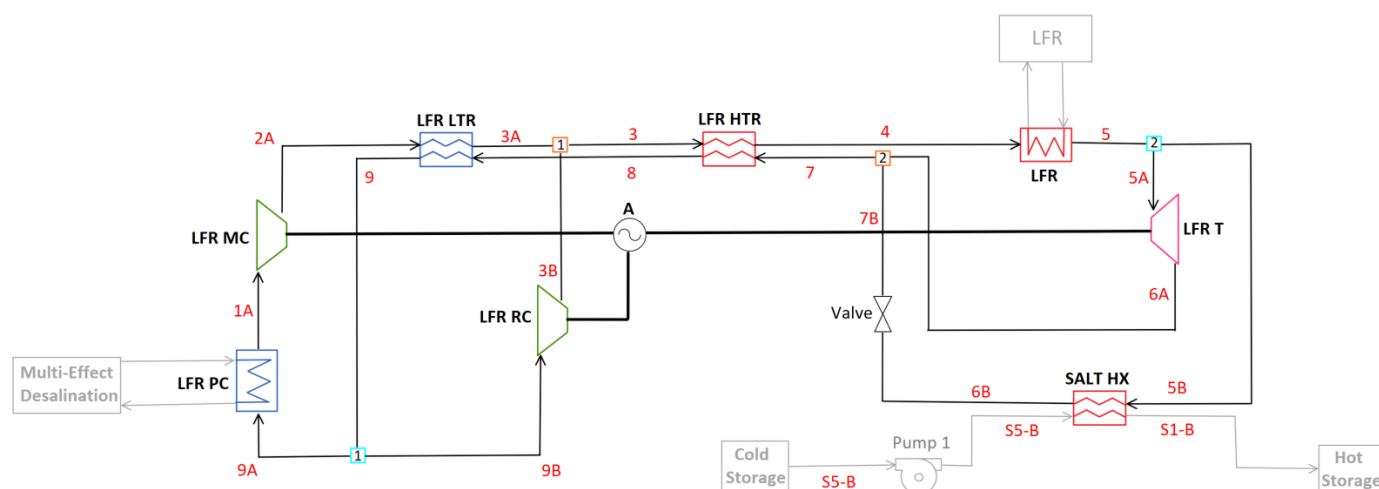
**Figure 6.** Diagram for C-LFR-POST thermal energy storage charging orientation



109 This TES charging cycle was extracting heat before the turbine and therefore would  
110 have a large negative effect on the amount of work that the turbine could produce. The  
111 turbine needs to offset the requirements of both compressors and this would require  
112 the inlet temperature to be high. The amount of energy that could be extracted before  
113 the turbine would be small and therefore the heat storage efficiency would be small.  
114 There was no quantitative study done on this diagram because it theoretically would be  
115 non-viable.

## 116 3.2.3. C-LFR-PAR

The requirement of the turbine and hot CSP TES temperature could be accomplished by splitting the flow before the turbine. The flow through the salt heat exchanger would therefore be separate from the turbine. After the salt heat exchanger a valve would need to reduce the pressure, this TES charging cycle is C-LFR-PAR shown in Figure 7.



**Figure 7.** Diagram for C-LFR-PAR thermal energy storage charging orientation

This cycle had two sensitivity studies done with varying cold CSP TES. The low temperature study was done at 663.2 K and the high temperature study was done at 713.2 K. The results from this study are displayed in Table 7.



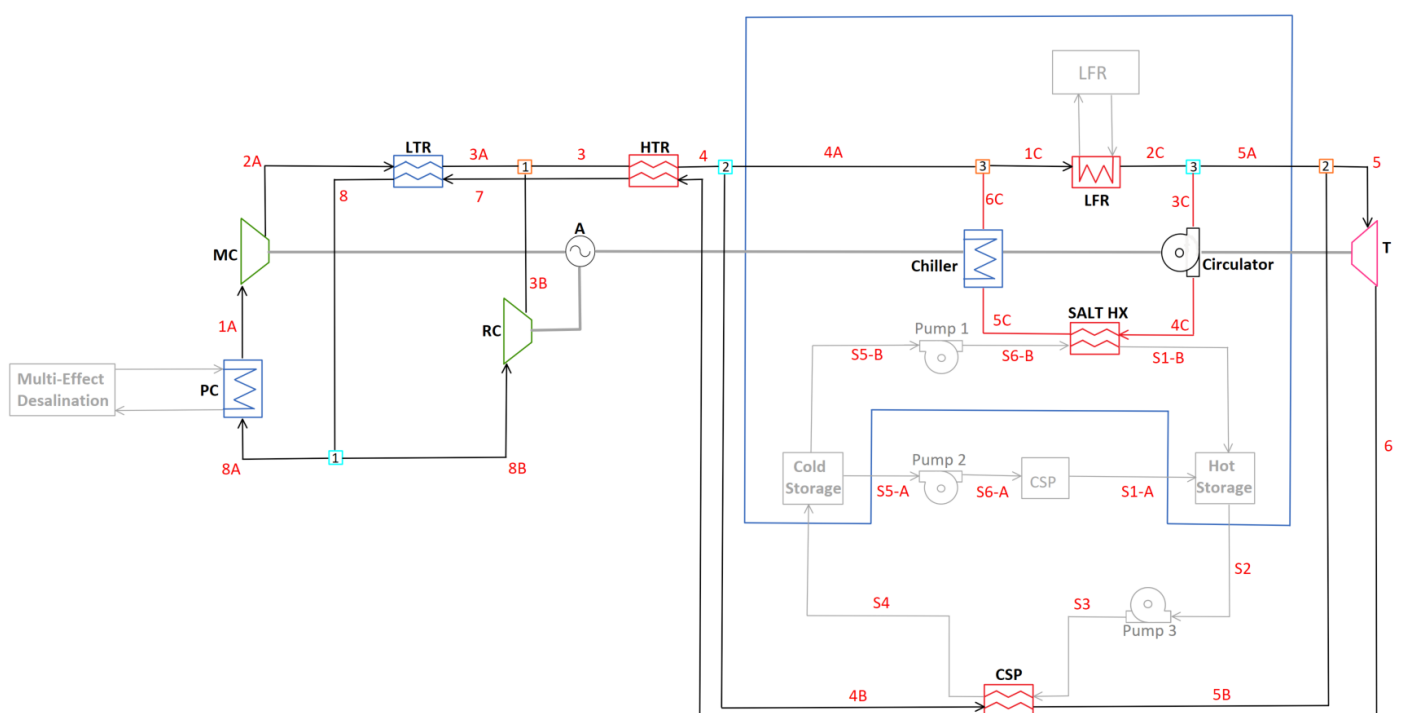
**Table 7.** Calculated system parameters for salt charging C-LFR-PAR cycle configuration with TES cold storage varied and LFR low temperature set to 673.2 K.

Definition	Variable	C-2HTR3T-ON	C
Cold TES Temperature (K)	$T_{CS}$	Data	Data
LFR Inlet Temperature (K)	$T_4$	Data	Data
Heat Storage Efficiency (%)	$\eta_{heatstorage}$	Data	Data
Alternator Power (W)	$\dot{W}_A$	Data	Data
PC Heat Transfer	$\dot{Q}_{PC}$	Data	Data
MC Power (W)	$\dot{W}_{MC}$	Data	Data
RC Power (W)	$\dot{W}_{RC}$	Data	Data
Turbine Power (W)	$\dot{W}_T$	Data	Data
MC Mass Flow Fraction (-)	$y_1$	Data	Data
SALT HX Mass Flow Fraction (-)	$y_2$	Data	Data
LTR UA Value (W/K)	$UA_{LTR}$	Data	Data
LTR Capacitance Ratio (-)	$CR_{LTR}$	Data	Data
LTR Heat Transfer Rate (W)	$\dot{Q}_{LTR}$	Data	Data
LTR Effectiveness (-)	$\varepsilon_{LTR}$	Data	Data
HTR UA Value (W/K)	$UA_{HTR}$	Data	Data
HTR Capacitance Ratio (-)	$CR_{HTR}$	Data	Data
HTR Heat Transfer Rate (W)	$\dot{Q}_{HTR}$	Data	Data
HTR Effectiveness (-)	$\varepsilon_{HTR}$	Data	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data	Data
CSPHX Effectiveness (-)	$\varepsilon_{CSPHX}$	Data	Data
CSPHX Approach Temperature (K)	$\delta_{CSPHX}$	Data	Data

Changing the temperature of the cold CSP TES had little effect on the heat storage  
 efficiency. The CSP salt mass flow rate and approach temperature of the SALT HX  
 would adjust according to the temperature difference in the TES and keep the efficiency  
 constant.

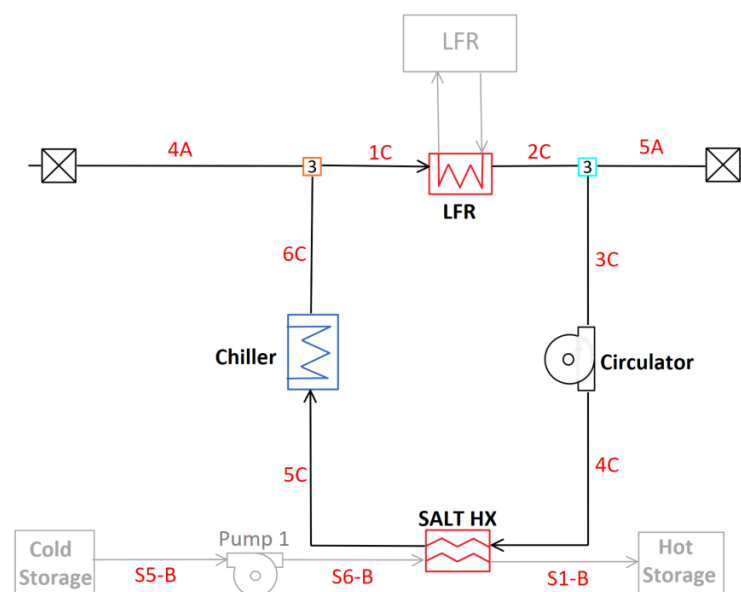
## 128 3.2.4. C-LFR-CIRC

129 The full diagram for C-LFR-CIRC is shown in Figure 8.



**Figure 8.** Full diagram for C-LFR-CIRC thermal energy storage charging orientation

The charging subsection of this diagram is composed of a circulation cycle that has heat inputed through the LFR heat exchanger. This subsection is seen in Figure 9.



**Figure 9.** Diagram for C-LFR-CIRC subcycle thermal energy storage charging orientation

The flow then continues through a circulator which has negligible pressure rise. A heat exchanger then extracts heat from the flow, transferring into the hot TES for later use. Excess heat that is not extracted is then dumped into a reservoir through the chiller to bring the temperature of the flow down to LFR cool side operating temperature of 673.2 K. Three different temperatures; 663.2 K, 683.2 K, and 713.2 K, are compared in Table 8 to show cold thermal energy storage's affect on heat storage efficiency.

**Table 8.** Calculated system parameters for charging C-LFR-CIRC subcycle configuration with constrained Lead-Fast Reactor low-end temperature.

Definition	Variable	C-LFR-CIRC		
Cold TES Temperature (K)	$T_{CS}$	Data	Data	Data
LFR Inlet Temperature (K)	$T_{1C}$	Data	Data	Data
Heat Storage Efficiency (%)	$\eta_{heatstorage}$	Data	Data	Data
Chiller Heat Transfer (W)	$\dot{Q}_{chill}$	Data	Data	Data
CSPHX UA Value (W/K)	$UA_{CSPHX}$	Data	Data	Data
CSPHX Capacitance Ratio (-)	$CR_{CSPHX}$	Data	Data	Data
CSPHX Heat Transfer Rate (W)	$\dot{Q}_{CSPHX}$	Data	Data	Data
CSPHX Effectiveness (-)	$\varepsilon_{CSPHX}$	Data	Data	Data

#### 4. Discussion

Authors should discuss the results and how they can be interpreted from the perspective of previous studies and of the working hypotheses. The findings and their implications should be discussed in the broadest context possible. Future research directions may also be highlighted.

#### 5. Conclusions

This section is not mandatory, but can be added to the manuscript if the discussion is unusually long or complex.

## 147 6. how to use

### 148 6.1. Subsection

149 Citing a journal paper [1] . Now citing a book reference [2] or other reference types  
150 [3]. [4]

#### 151 6.1.1. Subsubsection

152 Bulleted lists look like this:

- 153 • First bullet;
- 154 • Second bullet;
- 155 • Third bullet.

156 Numbered lists can be added as follows:

- 157 1. First item;
- 158 2. Second item;
- 159 3. Third item.

160 The text continues here.

### 161 6.2. Figures, Tables and Schemes

162 All figures and tables should be cited in the main text as Figure 10, Table 9, etc.



**Figure 10.** This is a figure. Schemes follow the same formatting. If there are multiple panels, they should be listed as: (a) Description of what is contained in the first panel. (b) Description of what is contained in the second panel. Figures should be placed in the main text near to the first time they are cited. A caption on a single line should be centered.

**Table 9.** This is a table caption. Tables should be placed in the main text near to the first time they are cited.

Title 1	Title 2	Title 3
Entry 1	Data	Data
Entry 2	Data	Data

163 Text.

164 Text.

### 165 6.3. Formatting of Mathematical Components

This is the example 1 of equation:

$$a = 1, \quad (1)$$

166 the text following an equation need not be a new paragraph. Please punctuate equations  
167 as regular text.

168 This is the example 2 of equation:

$$\begin{aligned} a &= b + c + d + e + f + g + h + i + j + k + l \\ &+ m + n + o + p + q + r + s + t + u + v + w + x + y + z \end{aligned} \quad (2)$$

169 Please punctuate equations as regular text. Theorem-type environments (including  
170 propositions, lemmas, corollaries etc.) can be formatted as follows:

171 **Theorem 1.** *Example text of a theorem.*

172 The text continues here. Proofs must be formatted as follows:

173 **Proof of Theorem 1.** Text of the proof. Note that the phrase “of Theorem 1” is optional  
174 if it is clear which theorem is being referred to.  $\square$

175 The text continues here.

**Author Contributions:** For research articles with several authors, a short paragraph specifying their individual contributions must be provided. The following statements should be used “Conceptualization, X.X. and Y.Y.; methodology, X.X.; software, X.X.; validation, X.X., Y.Y. and Z.Z.; formal analysis, X.X.; investigation, X.X.; resources, X.X.; data curation, X.X.; writing—original draft preparation, X.X.; writing—review and editing, X.X.; visualization, X.X.; supervision, X.X.; project administration, X.X.; funding acquisition, Y.Y. All authors have read and agreed to the published version of the manuscript.”, please turn to the [CRediT taxonomy](#) for the term explanation. Authorship must be limited to those who have contributed substantially to the work reported.

**Funding:** Please add: “This research received no external funding” or “This research was funded by NAME OF FUNDER grant number XXX.” and “The APC was funded by XXX”. Check carefully that the details given are accurate and use the standard spelling of funding agency names at <https://search.crossref.org/funding>, any errors may affect your future funding.

**Data Availability Statement:** In this section, please provide details regarding where data supporting reported results can be found, including links to publicly archived datasets analyzed or generated during the study. Please refer to suggested Data Availability Statements in section “MDPI Research Data Policies” at <https://www.mdpi.com/ethics>. You might choose to exclude this statement if the study did not report any data.

**Acknowledgments:** In this section you can acknowledge any support given which is not covered by the author contribution or funding sections. This may include administrative and technical support, or donations in kind (e.g., materials used for experiments).

**Conflicts of Interest:** Declare conflicts of interest or state “The authors declare no conflict of interest.” Authors must identify and declare any personal circumstances or interest that may be perceived as inappropriately influencing the representation or interpretation of reported research results. Any role of the funders in the design of the study; in the collection, analyses or interpretation of data; in the writing of the manuscript, or in the decision to publish the results must be declared in this section. If there is no role, please state “The funders had no role in the design of the study; in the collection, analyses, or interpretation of data; in the writing of the manuscript, or in the decision to publish the results”.

## Nomenclature

The following abbreviations and variables are used in this manuscript:

## Abbreviations:

A	Alternator
CSP	Concentrating solar power
EES	Engineering Equation Solver
HTR	High temperature recuperator
HX	Heat exchanger
LFR	Lead-fast reactor
LTR	Low temperature recuperator
MC	Main compressor
NREL	National Renewable Energy Laboratory
P	Pump
PC	Pre-cooler
RC	Re-compressor
sCO <sub>2</sub>	supercritical carbon dioxide
T	Turbine
TES	Thermal energy storage

## Variables [Units]:

CR	Capacitance Ratio [-]
$\dot{C}$	Capacitance Rate [W/K]
$\Delta$	Temperature difference [K]
$\delta$	Approach temperature of heat exchanger [K]
$\varepsilon$	Effectiveness of heat exchanger [-]
$\eta$	Isentropic efficiency [-]
$h$	Enthalpy [J/kg]
$\dot{m}$	Mass flow rate [kg/s]
NTU	Number of transfer units [-]
$P$	Pressure [Pa]
$\dot{Q}$	Heat transfer rate [W]
$T$	Temperature [K]
UA	Conductivity of heat exchanger [W/K]
$v$	Volumetric flow rate [ $m^3/kg$ ]
$\dot{W}$	Power [W]
$y$	Splitter Fraction [-]

```
#My ees file
def myfunc():
    return x
x = y

f = 8*y^2
```

$$a^2 + b^2 = c^2 \quad (3)$$

## References

1. Wagner, M.J. Optimization of stored energy dispatch for concentrating solar power systems. PhD thesis, Colorado School of Mines, 2017.
2. Blair, N.; Dobos, A.; Freeman, J.; Gilman, P.; Janzou, P.; Wagner, M.; Neises, T.; Mehos, M. SAM five year solar technologies roadmap. *Applied energy* **2005**, *231*, 1109–1121.
3. Hirsch, T.; Eck, M.; Blanco, M.J.; Wagner, M.; Feldhoff, J.F. Standardization of CSP Performance Model Projection: Latest Results From the guiSmo Project. *Energy Sustainability*, 2011, Vol. 54686, pp. 737–742.
4. Nellis, G.; Klein, S. *Heat Transfer*; Cambridge University Press, 2008. doi:10.1017/CBO9780511841606.