

## 2.2 General Theory for Filtration 过滤基本理论

Now we turn to the mathematical description of filtration.

(对过滤过程机械描述)

## Darcy's law (达西定律)

- Darcy's law relates the flow rate through a porous bed of solids to the pressure drop causing that flow  
(定律把流速与压降联系起来。)

$$v = \frac{k \Delta p}{\mu l} \quad (\text{式 1})$$

- $v$  directly proportional to  $\Delta p$   
(流速正比压降)
- inversely proportional to  $l/k$   
(反比于  $l/k$ )

- where  $v$  is the velocity of the liquid
- $k$ : a proportionality constant (usually called the Darcy's law permeability of the bed)

( $k$ 比例常数,过滤床渗透性的达西方程参数)

- $\Delta p$  : the pressure drop across the bed of thickness  $l$

通过厚度为 $l$ 的床产生的压降

- $\mu$ : viscosity of the liquid

流体粘度

## Darcy's law holds only when $Re < 5$

（当 $R_e < 5$ 时达西定律才成立）

$$Re = \frac{dv\rho}{\mu(1-\varepsilon)} \quad (\text{式2})$$

- $d$  – particle size（粒径）
- $\varepsilon$  – the void fraction in the cake（滤饼空隙率）
- $\rho$  – the liquid density（流体的密度）
- $R_e$  – Reynolds number（雷诺准数）

- **For batch filtration** (分批过滤) ,
- **the velocity is**

$$v = \frac{1}{A} \frac{dV}{dt} \quad (\text{式3})$$

**where**

- **A – filtration area** (过滤面积)
- **V – the total volume of filtrate** (滤液总体积)
- **t – the filtration time** (过滤时间)

**so**

$$l/k = R_M + R_C \quad (\text{式 4})$$

- rewrite the resistance ( $1/k$ ) to include explicitly the contributions of cake and filter medium.
- $R_M$  is the resistance of the filter medium  
过滤介质的阻力
- $R_C$  is the resistance of accumulated cake biomass  
滤饼的阻力
- Combining Eqs.(1), (3), and (4),

We find basic differential equation for batch filtration at constant pressure drop .

(分批过滤压降是常数)

$$\frac{1}{A} \frac{dV}{dt} = \frac{\Delta p}{\mu(R_M + R_C)} \quad (\text{式 } 5)$$

**$R_M$  is a constant, independent of the cake**

( $R_M$ 是常数，与滤饼无关)

**The cake's resistance  $R_C$  varies with the amount filtered volume of filtration.**

( $R_C$ 与滤液总体积有关)

**The exact nature of this variation depends on whether the cake is incompressible or not.**

( $R_C$ 的变化取决于滤饼是不可压缩还是可压缩)

## 1. Incompressible Cakes (不可压缩滤饼)

**If the cake is incompressible (rigid), the cake thickness is directly proportional to the filtrate volume and inversely proportional to the filter area.**

如果滤饼是不可压缩的，则滤饼的厚度正比于过滤液的体积，反比于过滤面积。

**As a result the cake's resistance  $R_C$  is described by the equation:**

$$R_C = \alpha \rho_0 (V/A) \quad (\text{式 6})$$



- where  $\alpha$  represents the specific cake resistance  
(滤饼的阻力特性)
- $\rho_0$  - the mass of cake solids per volume of filtrate  
(单位体积滤液含固体滤饼量)
- Substitution of Eq.(6) into Eq.(5). Differential equation for incompressible cake is:

$$\frac{1}{A} \frac{dV}{dt} = \frac{\Delta p}{\mu \left[ \alpha \rho_0 (V / A) + R_M \right]} \quad (\text{式7})$$

- The equation is subject to the initial condition  
初始条件为

$$t=0 \quad V=0$$

This condition says that at the start of the experiment,  
no solution has been filtered.

开始时没有滤液被过滤

Equation(2.2-7) is easily integrated and rearranged  
to give

代入（式7）积分后整理得

$$\left( \frac{At}{V} \right) = K \left( \frac{V}{A} \right) + B \quad (\text{式8})$$

where (其中)

$$K = \frac{\mu \alpha \rho_0}{2\Delta p}$$

and

$$B = \frac{\mu R_M}{\Delta p}$$

- **Thus a plot of  $(At/V)$  versus  $(V/A)$  should be linear.**  
( $At/V$ 对  $V/A$ 作图)
- **The slope  $K$  is a function of the pressure drop  $\Delta p$  and of the properties of the cake, represented by  $\alpha$  and  $\rho_0$ .**  
斜率 $K$ 是压降 $\Delta p$ 及滤饼特性 $\alpha$ 、 $\rho_0$ 的函数。
- **The Intercept  $B$  should be independent of the properties of the cake, but it is proportional to the medium's resistance  $R_M$ , usually  $R_M$  is insignificant.**  
截距 $B$ 与滤饼特性无关，但它正比于介质阻力 $R_M$ 。通常 $R_M$ 可忽略不计

- **Eq.(8) becomes simpler still:**

$$t = \left( \frac{\mu \alpha \rho_0}{2 \Delta p} \right) \left( \frac{V}{A} \right)^2 \quad (\text{式 9})$$

**These equations, valid for incompressible cakes, will be tested in the examples given later in the section.**

该式仅适合不可压缩的滤饼

## 2. Compressible cake (可压缩滤饼)

- **Almost all cakes formed of biological materials are compressible, and so cannot be described with the simple analysis just outlined.**
- **As these cakes compress, filtration rates drop.**

大多数生物滤饼都可压缩，不能仅用作图法描述，滤饼可压缩，则过滤速度降低。

**To estimate the effects of compressibility, we assume that the cake resistance  $\alpha$  is a function of the pressure drop.**

为了估计可压缩性的影响，我们假定滤饼阻力 $\alpha$ 是压降的函数来估计可压缩性滤饼的影响

$$\alpha = \alpha'(\Delta p)^s \quad (\text{式 10})$$

where

- $\alpha'$  -- a constant related largely to the size and shape of the particles forming the cake.

$\alpha'$ 是一个与滤饼组成、粒子大小和形状相关的常数

- $s$  -- the cake compressibility

$s$ 是压缩系数

$s=0$  a rigid & highly incompressible cake

$s=0$  理想的不可压缩

$s=1$  a highly compressible cake

$s=1$  高度可压缩

$s=0.1 \sim 0.8$  in practice

实践中,  $s$ 的变化范围从0.1到0.8

**Values of  $s$  and  $\alpha'$  are most easily determined by plotting the logarithm of  $\alpha$  versus the logarithm of  $\Delta p$ , as shown in Fig.(1)**

计算 $s$ 和 $\alpha'$ 可用 $\log \alpha$ 对 $\log \Delta p$ 作图。



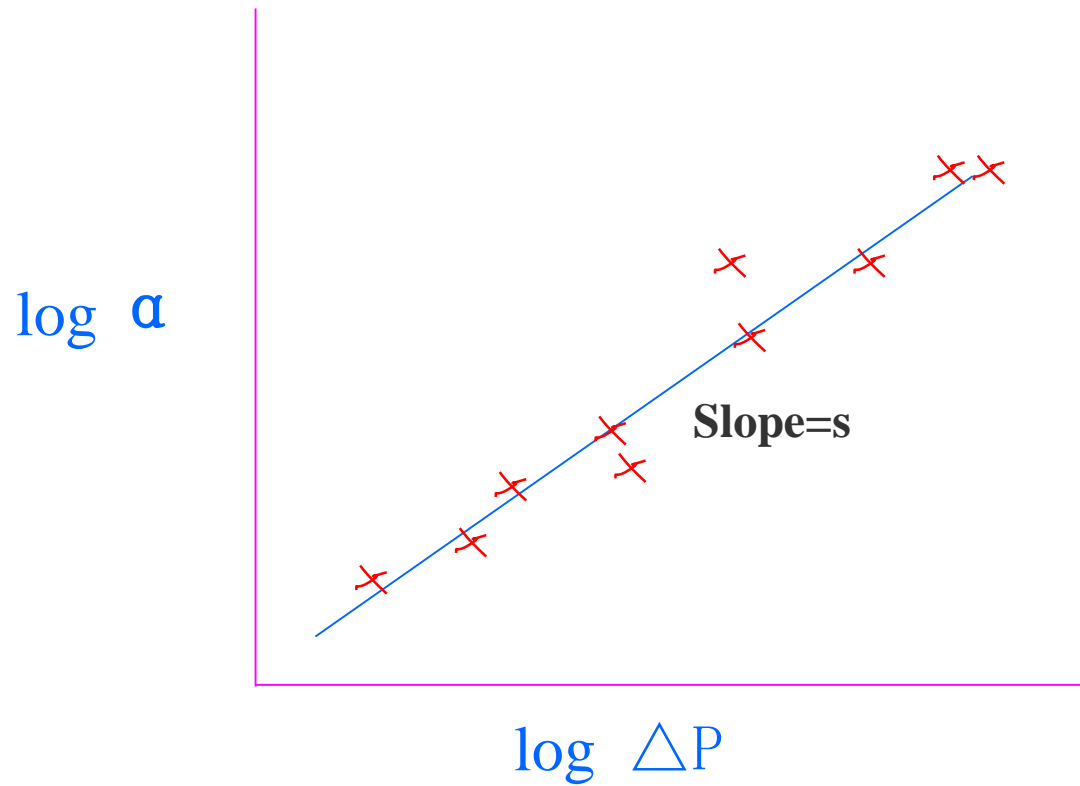


Fig1 Cake resistance versus pressure drop

图1  $\log \alpha$  对  $\log \Delta p$  作图

**When values of  $s$  are high , one should consider pretreating the feed with filter aids, as described in Section 2.1 .**

**当 $s$ 的数值很高时，须加入助滤剂对原液进行预处理**

**The fact that a cake is compressible dose not change the basic result for a constant pressure filtration, given by Eq (10).**

**可压缩滤饼并不改变式（10）给出的对基本结果**

**The value of  $K$  measured with this equation may be a more complex function of  $p$  than first expected. It should not change the value of  $B$ .**

**$K$ 转变为关于 $\Delta P$ 的复杂函数，与压力成正比的 $B$ 值不变**