Thermodynamics

Definitions

Isolated system: No exchanges

Closed system: Only energy exchange

Open system: Energy & mass exchange

Intensive state variables:

Independent of mass

Extensive state variables:

Proportional to mass

Reservoirs: Infinite/very large system that remains unchanged when in contact with finite system.

Mechanical equilibrium:

No unbalanced forces

Thermal equilibrium:

No temperature differences

Thermodynamic equilibrium:

Intensive state variables of system are <u>constant</u>. Alternatively our system is in <u>mechanical</u> and <u>thermal</u> equilibrium.

Reversible processes:

Every intermediate is an equilibrium state. $\,$

Quasi-static processes:

Process sufficiently slow such that only infinitesimal temperature or pressure gradients exist.

Frictionless quasi-static processes are reversible.

Cyclic processes:

$$\Delta U = 0$$
 and $W = Q$

For conservative forces:

$$\oint \mathrm{d}X = 0$$

where X is a state variable.

Adiabatic processes: $\Delta Q = 0$

Isothermal processes: $\Delta T = 0$

Isobaric processes: $\Delta P = 0$

Density

We define the density of a material as:

$$\rho = \frac{m}{V}.$$

If mass m is constant:

$$\Delta V = m \left(\frac{1}{\rho_f} - \frac{1}{\rho_i} \right)$$

assuming homogeneous material.

Zeroth law

If A is in thermal equilibrium with B and C seperately then B and C are also in thermal equilibrium.

Ideal gas state equation

Given n moles of gas at temperature T:

$$PV = nRT$$
$$= Nk_BT$$

where $R = N_A k_B = 8.314 \text{JK}^{-1} \text{mol}^{-1}$ and N the number of molecules.

Calculus identities

1.
$$df(x,y) = \left(\frac{\partial f}{\partial x}\right)_y dx + \left(\frac{\partial f}{\partial y}\right)_x dx$$

if $f = f(x,y)$.

2. Differential df is **inexact** if:

$$\int_C df$$
 is dependent of path.

$$3. \ \left(\frac{\partial Z}{\partial Y}\right)_X = \left[\left(\frac{\partial Y}{\partial Z}\right)_X\right]^{-1}$$

$$4. \left(\frac{\partial X}{\partial Y}\right)_{Z} \left(\frac{\partial Y}{\partial Z}\right)_{Y} \left(\frac{\partial Z}{\partial X}\right)_{Y} = -1$$

First law

Total energy E is conserved and:

$$\Delta U = Q - W$$
$$dU = dQ - dW$$

 $\dot{U} = \dot{Q} - \dot{W}$

where U is internal energy and $E \geq U$.

transfer into system.

- Heat exchange Q:
 The energy transfer of two systems at different temperatures in thermal contact. Q > 0 represents energy
- Work exchange W:
 The work done on the surroundings by system is represented by W > 0.

Work is generally path dependent.

The work done \underline{by} a fluid in **reversible** processes is:

$$dW = PdV$$

and has units Joules (J).

Isothermal expansion

Let $P_1 > P_2$ where P_1 and P_2 denote system and external pressure respectively. Only mechanical work is exchanged via a piston. By applying a force such that there exists pressure difference dP, our expansion becomes reversible and hence:

$$W_{1\to 2} = nRT \int_{V_1}^{V_2} \frac{\mathrm{d}V}{V}.$$

Note that for isothermal processes under ideal gas assumption, $\Delta U = 0$.

Heat capacity

Heat capacity (JK^{-1}) is defined as:

$$C(P,T) = \lim_{\Delta T \to 0} \frac{\Delta Q}{\Delta T}$$

and is the heat needed to produce unit change in sample temperature.

Specific heat capacity $(Jkg^{-1}K^{-1})$:

$$Q = mc\Delta T.$$

We define the **isochoric** heat capacity as:

$$C_V(T) := \left(\frac{\mathrm{d}Q}{\mathrm{d}T}\right)_V = \left(\frac{\partial U}{\partial T}\right)_V$$

and the **isobaric** heat capacity as:

$$\begin{split} C_P &:= \left(\frac{\mathrm{d}Q}{\mathrm{d}T}\right)_P \\ &= C_V + \left[P + \left(\frac{\partial U}{\partial V}\right)_T\right] \left(\frac{\partial V}{\partial T}\right)_P. \end{split}$$

For ideal gases we have that:

$$C_P - C_V = nR.$$

Adiabatic expansion

The <u>reversible adiabatic</u> expansion of an **ideal** gas is given by:

$$dU = -PdV \text{ and } dU = C_V dT$$

$$\implies \frac{dT}{T} + \frac{C_P - C_V}{C_V} \frac{dV}{V} = 0$$

since U = U(T). Integrating this yields:

$$TV^{\gamma-1} = \text{constant}$$

$$PV^{\gamma} = \text{constant}$$

$$T^{\frac{1}{\gamma-1}}V = \text{constant}$$

where γ is the adiabatic exponent:

$$\gamma = \frac{C_P}{C_V} = \frac{f+2}{f}$$

$$U = \frac{f}{2}nRT$$

and f is degrees of freedom. The practical computation of work done for adiabats is given by:

$$W_{1\to 2} = -\int_{T_1}^{T_2} C_V dT.$$

General form for first law

Given system with m conjugate pairs (x_i, X_i) that represent various modes of work exchange:

$$\mathrm{d}U = \mathrm{d}Q + \sum_{i=1}^{m} x_i \mathrm{d}X_i$$

for each $\{x_i\}$ drives $\{X_i\}$.

Thermodynamics

Enthalpy

The state function enthalpy simplies the description of heat transfer.

Enthalpy has units J and is defined as:

$$H = U + PV$$

$$dH = dU + VdP + PdV$$
$$= dQ + VdP.$$

Under isobaric reversible conditions:

$$\mathrm{d}H=\mathrm{d}Q_P.$$

$$\therefore C_P = \left(\frac{\partial H}{\partial T}\right)_P$$

Latent heats

Latent heat is heat needed for sample to undergo a phase transition:

$$\Delta U_m = Q_m - P\Delta V_m$$

$$L_m = Q_m = \Delta H_m.$$

Chemical reactions

Since $Q = \Delta U + P_0 \Delta V = \Delta H$:

- Q < 0: exothermic (heat is released)
- Q > 0: endothermic (heat is absorbed)

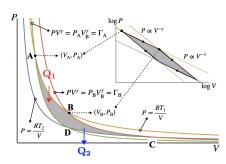
at constant pressure P_0 .

Carnot's theorem

Peak efficiency of a cyclic heat engine:

$$\eta := \frac{\dot{W}}{\dot{Q_H}} = 1 - \frac{Q_C}{Q_H} = 1 - \frac{T_C}{T_H}$$

and is either in terms of rate or value, with units J or Js⁻¹. This ideal cycle is known as the Carnot cycle:



where AB,CD are isothermal processes and BC, DA are adiabatic processes.

Entropy

The state function entropy is a measure of disorder defined as:

$$S = \frac{Q}{T}$$

where Q is heat received from a reservoir at temperature T and units JK^{-1} .

Then for a reversible cyclic heat engine:

$$dS = dQ/T$$

$$dU = TdS - PdV.$$

For all processes the following holds:

$$dH = TdS + VdP.$$

Entropy of mixing

$$\Delta S = n_A R \ln \frac{V_A + V_B}{V_A} + n_B R \ln \frac{V_A + V_B}{V_B}$$
$$\Delta s_{mix} = -R(x_A \ln x_A + x_B \ln x_B)$$
$$x_A = \frac{n_A}{n_A + n_B} \text{ and } x_B = \frac{n_B}{n_A + n_B}$$

Second law

$$\Delta S_{total} = \Delta_{system} + \Delta_{reservoir} \ge 0$$
$$dS \ge \frac{dQ}{T}$$

Helmholtz free energy

$$F = U - TS$$
$$dF = -SdT - PdV$$

Gibbs free energy

$$G = H - TS$$
$$dG = -SdT + VdP$$

Chemical reactions are spontaneous if:

$$\Delta G = \Delta H - T\Delta S < 0.$$

Maxwell relations

$$\begin{split} \left(\frac{\partial T}{\partial V}\right)_S &= -\left(\frac{\partial P}{\partial S}\right)_V \\ \left(\frac{\partial T}{\partial P}\right)_S &= \left(\frac{\partial V}{\partial S}\right)_P \\ \left(\frac{\partial S}{\partial V}\right)_T &= \left(\frac{\partial P}{\partial T}\right)_V \\ -\left(\frac{\partial S}{\partial P}\right)_T &= \left(\frac{\partial V}{\partial T}\right)_P \end{split}$$

The isobaric expansivity is defined as:

$$\beta = \frac{1}{V} \left(\frac{\partial V}{\partial T} \right)_P$$

and the isothermal compressibility:

$$\kappa_T = -\frac{1}{V} \left(\frac{\partial V}{\partial P} \right)_T.$$

Throttling

Throttling is the <u>adiabatic</u> reduction in gas pressure and is an isenthalpic process. We define the slope of a P-T plot:

$$\mu_{JK} = \left(\frac{\partial T}{\partial P}\right)_{H}$$
$$= \frac{V(T, P)}{C_{P}}(\beta T - 1)$$

as the Joule-Kelvin coefficient.

Clausius-Clapeyron equation

The slope of any phase boundary is:

$$\frac{\mathrm{d}P}{\mathrm{d}T} = \frac{\Delta S}{\Delta V} = \frac{\Delta H}{T\Delta V}$$

since constant pressure at boundaries.

Van der Waals state equation

$$\left(P + \frac{an^2}{V^2}\right)\left(V - nb\right) = nRT$$

Chemical potentials

The Euler equation for a 1-component **open** system with N particles is:

$$U = TS - PV + \mu N$$

with modified first law statement:

$$dU = TdS - PdV + \mu dN.$$

This gives the Gibbs-Duhem relation:

$$SdT - VdP + Nd\mu = 0$$

where μ is the chemical potential:

$$\mu = \frac{G}{N}$$

since G is extensive. At constant T with ideal gas assumptions:

$$\mu(P,T) = RT \ln \frac{P}{P_0} + \mu_0(P,T).$$

Chemical potential μ has units J.

Third law

$$S = 0$$
 at $T = 0$ K.

Questions

1. What is temperature?