

TRASF. δQ ΔS

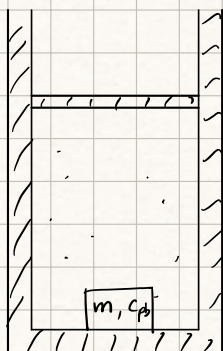
ISOCORA $M C_V dT$ $M C_V \ln \frac{T_f}{T_i} = M C_V \ln \frac{P_f}{P_i}$

ISOBARA $M C_P dT$ $M C_P \ln \frac{T_f}{T_i} = M C_P \ln \frac{V_f}{V_i}$

ISOTERMA $P dV (\delta Q)$ $M R \ln \frac{V_f}{V_i} = -M R \ln \frac{P_f}{P_i}$

ADIABATICA
REVERSIBILE

1)



$n = 1 \text{ mol (monoat.)}$

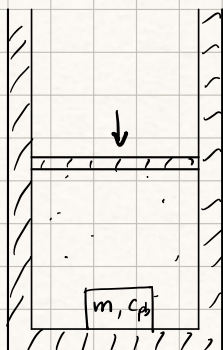
$m = 0,5 \text{ kg}$

$C_{pb} = 130 \text{ J/kg K}$

$T_f = T_i + 10\% = 1,1 T_i$

? $\frac{P_f}{P_i}$ (ISOENTROPICO)

$\Delta S_{\text{sist.}} = 0$



$\Delta S_0 = \Delta S_{\text{sist.}} + \Delta S_{\text{amb}}$

perché NO scambio Q con ambiente (ADIAB.)

$\Rightarrow \Delta S_0 = 0$

$\Delta S_{\text{sist.}} = \Delta S_{\text{gas}} + \Delta S_{\text{pb}} = 0 \Rightarrow \Delta S_{\text{gas}} = -\Delta S_{\text{pb}}$

$\Delta S_{\text{pb}} = \int_i^f \frac{\delta Q}{T} = \int_i^f m c_{pb} \frac{dT}{T} = m c_{pb} \ln \frac{T_f}{T_i}$

considero transf. rev. equiv.:

ISOTERMA: $P_i \rightarrow P_f$

ISOBARA: $T_i \rightarrow T_f$

$\Delta S_{\text{gas}} = -n R \ln \frac{P_f}{P_i} + n c_p \ln \frac{T_f}{T_i}$

$\Rightarrow \Delta S_{\text{pb}} = -\Delta S_{\text{gas}}: m c_{pb} \ln \frac{T_f}{T_i} = n R \ln \frac{P_f}{P_i} - n c_p \ln \frac{T_f}{T_i}$

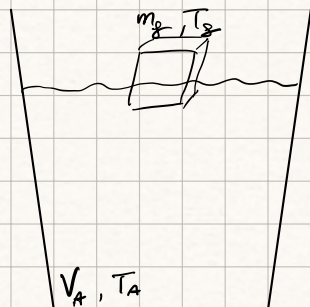
$$\rightarrow nR \ln \frac{P_f}{P_i} = m c_{pb} \ln \frac{T_f}{T_i} + n c_p \ln \frac{T_f}{T_i}$$

$$= \frac{(m c_{pb} + n c_p)}{nR} \ln \frac{T_f}{T_i}$$

$$\Rightarrow \ln \frac{P_f}{P_i} = \ln \left(\frac{T_f}{T_i} \right)^{\frac{m c_{pb} + n c_p}{nR}}$$

$$\Rightarrow \frac{P_f}{P_i} = \left(\frac{T_f}{T_i} \right)^{\frac{c_p}{R} + \frac{m c_{pb}}{nR}} \rightarrow \frac{P_f}{P_i} = 1,1^{\frac{5}{2} + \frac{m c_{pb}}{nR}}$$

2)



$$m_g = 20g$$

$$T_g = -5^\circ C$$

$$V_A = 200ml$$

$$T_A = 25^\circ C$$

? ΔS_u

$$\lambda_g = 3,3 \cdot 10^5 J/kg$$

$$c_g = 2080 J/kg \cdot K$$

$$c_A = 4187 J/kg \cdot K$$

EQUILIBRIO TERMODINAMICO se stessa temperatura

GHIACCIO : $T_g \rightarrow T_0 \rightarrow T_f$
(fusione)

ACQUA : $T_A \rightarrow T_f$
(raffreddamento : $< T_A$)

$$\Delta Q = 0 \Rightarrow \underbrace{m_g c_g (T_0 - T_f)}_{\text{riscaldamento ghiaccio}} + \underbrace{m_g \lambda_g}_{\text{calore latente di fusione}} + \underbrace{m_g c_A (T_f - T_0)}_{\text{riscaldamento ghiaccio diventato acqua}} + \underbrace{m_A c_A (T_f - T_A)}_{\text{raffreddamento acqua}} = 0$$

① ② ③ → trasformato in acqua ④

$$T_f = 288,15 K$$

$$\Delta S_u = \Delta S_{sist} + \Delta S_{sub} = \Delta S_1 + \Delta S_2 + \Delta S_3 + \Delta S_4$$

$$\Delta S_1 = \int_i^f \frac{\delta Q}{T} = \int_{T_g}^{T_0} m_g c_g \frac{dT}{T} = m_g c_g \ln \frac{T_0}{T_g}$$

↳ sistema isolato

$$\Delta S_2 = \int_i^f \frac{\delta Q}{T} = \frac{1}{T} \int_i^f \delta Q = \frac{m_g \lambda_g}{T_0}$$

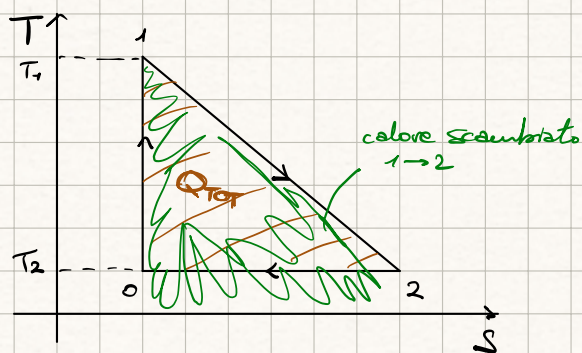
↳ fusione avviene a temp. cost

$$\Delta S_3 = m_g c_A \ln \frac{T_f}{T_0}$$

$$\Delta S_4 = m_A c_A \ln \frac{T_f}{T_A}$$

$$\Rightarrow \Delta S_u = 1,97 J/K$$

3) PIANO S-T



$$T_1 = 500 \text{ K}$$

$$T_2 = 300 \text{ K}$$

? η

? P (durante intervallo τ)
↳ potenza

$$Q_{TOT} = \frac{(S_2 - S_1)(T_1 - T_2)}{2} ; \quad \Delta U_{ciclo} = 0 \quad \Rightarrow \quad Q_{TOT} = W$$

$$\eta = \frac{W}{|Q_{ASS}|}$$

• $0 \rightarrow 1$: ISENTROPICO $\Rightarrow \Delta S = 0 \Rightarrow Q = 0$

• $1 \rightarrow 2$: $Q_{12} = \frac{(T_1 + T_2)(S_2 - S_1)}{2} > 0$ calore assorbito dalla macchina

• $2 \rightarrow 0$: ISOTERMA $\rightarrow Q_{20} = (S_1 - S_2)T_2 < 0$ calore ceduto
! attento al verso della trasformazione.

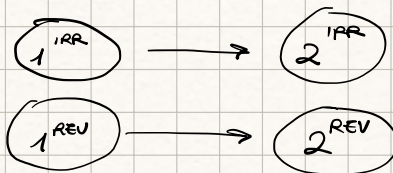
$$\Rightarrow \eta = \frac{W}{Q_{12}} = \frac{(S_2 - S_1)(T_1 - T_2)}{(T_1 + T_2)(S_2 - S_1)} = \frac{T_1 - T_2}{T_1 + T_2} = 0,25$$

$$P = \frac{W}{\tau} = \frac{(S_2 - S_1)(T_1 - T_2)}{2\tau}$$

$$4) \quad V_1^{IRR} = V_1^{REV} = V_1$$

$$T_1^{IRR} = T_1^{REV} = T_1$$

$$V_2^{IRR} = V_2^{REV} = V_2$$



$$? \frac{T_2^{IRR}}{T_2^{REV}}$$

$$\text{REVERSIBILE: } TV^{\gamma-1} = \text{cost} \rightarrow T_1 V_1^{\gamma-1} = T_2^{REV} V_2^{\gamma-1} \Rightarrow T_2^{REV} = \left(\frac{V_1}{V_2}\right)^{\gamma-1} T_1$$

IRREVERSIBILE: tr. eq. rev. \rightarrow ISOTERMA $V_1 \rightarrow V_2$
ISOCORA: $T_1 \rightarrow T_2^{IRR}$

$\frac{Q_{REV}}{Q_{IRR}}$ (Mayer)

$$\Delta S = nR \ln \frac{V_2}{V_1} + nC_v \ln \frac{T_2^{IRR}}{T_1} \rightarrow \ln \frac{T_2^{IRR}}{T_1} = \frac{\Delta S}{nC_v} + \ln \left(\frac{V_2}{V_1} \right)^{\frac{R}{C_v}}$$

$$\rightarrow \frac{T_2^{IRR}}{T_1} = \left(\frac{V_2}{V_1} \right)^{\frac{R}{C_v}} e^{\frac{\Delta S}{nC_v}} \Rightarrow T_2^{IRR} = T_1 \left(\frac{V_2}{V_1} \right)^{\frac{R}{C_v}} e^{\frac{\Delta S}{nC_v}} \quad \Delta S > 0$$

$$\Rightarrow \frac{T_2^{IRR}}{T_2^{REV}} = e^{\frac{\Delta S}{nC_v}} \Rightarrow T_2^{IRR} > T_2^{REV}$$

5) $T_2 = 800^\circ\text{C}$
 $T_1 = 300^\circ\text{C}$
 $P = 10\text{ W}$
 $\chi = 60\%$
 $\eta = \chi \eta_c$
 $\Delta t = 1\text{ h}$

a) ? Q_{ASS} ? Q_{CED}

b) ? ΔS_0

$$\eta_c = 1 - \frac{T_1}{T_2} ; \quad \eta = \chi \left(1 - \frac{T_1}{T_2} \right) = \frac{P}{|Q_{ASS}|} \Rightarrow |Q_{ASS}| = \frac{P}{\chi \left(1 - \frac{T_1}{T_2} \right)}$$

$$\mathcal{L} = P \Delta t \Rightarrow |Q_{ASS}| = \frac{P \Delta t}{\chi \left(1 - \frac{T_1}{T_2} \right)} = 1,3 \cdot 10^8 \text{ J}$$

$$\Delta U_{ciclo} = 0 ; \quad Q = \mathcal{L} + \Delta U \Rightarrow \mathcal{L} = +Q_{TOT} \Rightarrow$$

$$\mathcal{L} = |Q_{ASS}| - |Q_{CED}| \Rightarrow |Q_{CED}| = |Q_{ASS}| - Q_{TOT} = |Q_{ASS}| - P \Delta t = 5,4 \cdot 10^7 \text{ J}$$

oppure $\eta = 1 - \frac{|Q_{CED}|}{|Q_{ASS}|} \Rightarrow |Q_{CED}| = \dots$

! Trasf. ciclica rev. $\Delta S_{sist} = 0$

$$\Delta S_0 = \Delta S_{amb} = \Delta S_1 + \Delta S_2 = \frac{Q_{S1}}{T_1} + \frac{Q_{S2}}{T_2}$$

$$Q_{S,1} = -Q_{CED} = |Q_{CED}|$$

$$Q_{S,2} = -Q_{ASS} = -|Q_{ASS}|$$

$$\Rightarrow \Delta S_0 = \frac{|Q_{CED}|}{T_1} - \frac{|Q_{ASS}|}{T_2} = 4,3 \cdot 10^4 \text{ J/K}$$

