

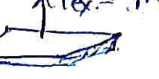




1. Cohesive vs Adhesive force  
 ↓  
 b/w  
 sig of same  
 substance  
 (17g-17g)  
 b/w differe  
 substance mole.  
 (17g-17g)

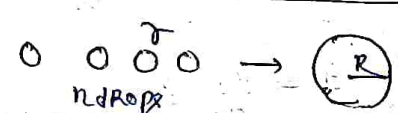
2. Surface tension  
 → ties have min. Area  
 →  $S = \frac{F}{L}$   
  
 $F = mg + 2 \cdot S \cdot 2\pi r$

3.  
  
 $F_{ex} = mg + S \cdot 2\pi r$   
  
 $F_{ex} = mg + S(2\pi r + 2\pi r)$


4. Surface energy  
 $S = \frac{E}{A} \Rightarrow E = SA$   
 → Surface Area  
 → Surface Tension

Energy of drop  
  
 $E = S 4\pi R^2$

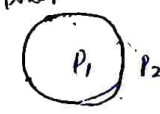
Energy of Bubble  
  
 $E = 2S 4\pi R^2$


5. Standard question on surface energy  
  
 $\therefore Vol^m \text{ is same}$   
 $R = r n^{1/3}$

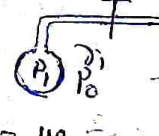
$E_i = n S 4\pi r^2$   
 $E_f = S 4\pi R^2$   
 $E_i - E_f = \text{incr. Temp \& Bigger drop by } \Delta T$   
 $E_i - E_f = m S \Delta T$

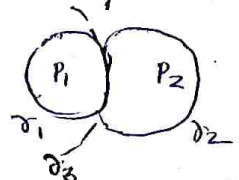
6. Bubble → drop at diff. diff  
  
 $\therefore Vol^m \text{ of liq. same}$   
 $E_i = 2S 4\pi r^2$   
 $E_f = S 4\pi R^2 \Rightarrow (4\pi r^2)t = \frac{4}{3}\pi R^3$   
 $R = (3r^2 t)^{1/3}$   
 $E_i - E_f = m S \Delta T$

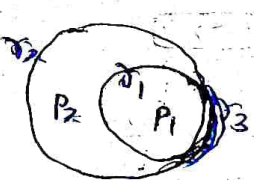
6. Excess pressure in liq. drop and bubble:


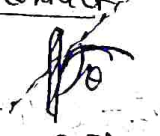
Drop  
  
 $P_1 = P_2$   
 $P_{ex} P_1 - P_2 = \frac{2S}{r}$



Bubble in (liq.)  
  
 $P_1 - P_2 = \frac{2S}{r}$

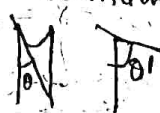
  
 $P_1 = \frac{4S}{r_1} + P_0$   
 $P_2 = \frac{4S}{r_2} + P_1$

7. Two soap bubbles in contact  
  
 $P_1 - P_0 = \frac{4S}{r_1}$   
 $P_2 - P_0 = \frac{4S}{r_2}$   
 $P_1 - P_2 = 4S \left( \frac{1}{r_1} - \frac{1}{r_2} \right)$   
 $\Rightarrow r_3 = \frac{r_1 r_2}{r_2 - r_1}$


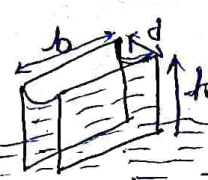
Internally  
  
 $P_1 - P_2 = \frac{4S}{r_1}$   
 $P_2 - P_0 = \frac{4S}{r_2}$   
 $P_1 - P_0 = 4S \left[ \frac{1}{r_1} + \frac{1}{r_2} \right]$   
 $P_1 - P_0 = \frac{4S}{r_3}$   
 $r_3 = \frac{r_1 r_2}{r_1 + r_2}$   
 $r_3$  will be smaller


8. Angle of contact  
  
 C.F. < A.F.  
  
 C.F. > A.F.  
 ex Hg

  
 $\theta < 90^\circ$   
 L. liq. wets the surface  
  
 $\theta > 90^\circ$

10. Insufficient tube height ( $H < h$ )  
  
 liq. overflows X  
 Contact angle ( $\theta' > \theta$ )

9. Capillary Action

(i) thin tube  
  
 $h$   
 $r$ : tube radius  
 $R$ : meniscus  


force to separate in large plane  
  
 $F = \frac{S}{L} = \frac{2SA \cos \theta}{d}$   
 $F = \frac{2SAC \cos \theta}{d}$   
 $A$ : liq. cross section Area  
 $\cos \theta = 1$  if H<sub>2</sub>O

$$h = \frac{2S \cos \theta}{\rho g r} = \frac{2S}{\rho g r} \Rightarrow \frac{2S \cos \theta}{\rho g r}$$

tho  $\cos \theta = 1$

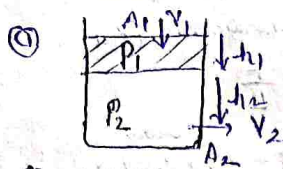


# 1. Streamline & turbulent flow

Velocity of fluid at a point always same

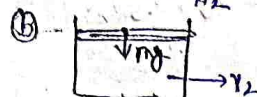
Not

## 8. Speed of efflux:



$$P_1gh_1 + P_2gh_2 = \frac{1}{2}\rho V_2^2$$

at the same point



$$(P_0 + \rho gh + \frac{\rho V^2}{2}) - P_0 = \frac{1}{2}\rho V_2^2$$

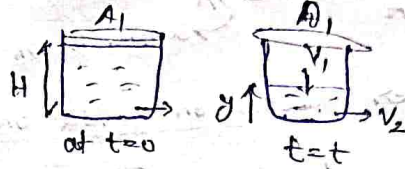
## 9. Vessel emptying time

$$A_1V_1 = A_2V_2$$

$$A_1(-\frac{dy}{dt}) = A_2\sqrt{2gh}$$

$$y \left| \frac{dy}{\sqrt{y}} \right|_H = \frac{A_2}{A_1} \sqrt{2g} \int_0^t dt$$

$$2(\sqrt{H} - \sqrt{h}) = -\frac{A_2}{A_1} \sqrt{2g} \cdot t$$



$$t = \frac{A_1}{A_2} \sqrt{\frac{2}{g}} (\sqrt{H} - \sqrt{h})$$

to empty.  $y=0, t=t_0$

$$t_0 = \frac{A_1}{A_2} \sqrt{\frac{2H}{g}}$$

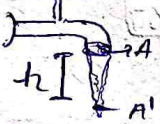
## 3. Ideal fluid

incompressible  
non-viscous  
stream flow  
no rotational effect

## 4. Eqn of continuity:-

$$\frac{dV}{dt} = A \cdot \frac{dx}{dt} = AV = \text{const.}$$

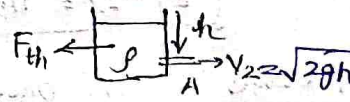
Volume flow rate



## 10. Thrust on vessel

$$F_{th} = \rho AV^2$$

$$F_{th} = \rho A 2gh$$



## Berthoulli's eqn

$$P + \frac{1}{2}\rho V^2 + \rho gh = \text{const.}$$

Pressure ends / Volume  $\frac{KE}{Vol.}$   $\frac{PE}{Vol.}$   
 $[m \rightarrow p]$

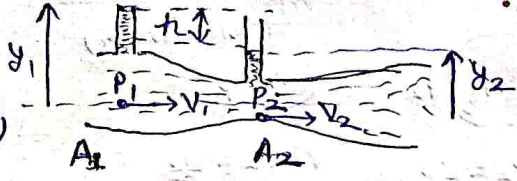
## 11. Venturimeter

$$P_1 - P_2 = \frac{1}{2}\rho(V_2^2 - V_1^2)$$

$$\therefore A_1V_1 = A_2V_2$$

$$\Rightarrow \rho gh = \frac{1}{2}\rho V_1^2 \left[ \left( \frac{A_1}{A_2} \right)^2 - 1 \right]$$

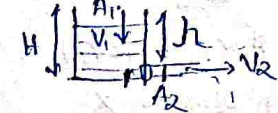
$$V_1 = \sqrt{\frac{2gh}{\left( \frac{A_1}{A_2} \right)^2 - 1}}$$



## 6. P-V Relation for horizontal flow

$$\frac{\text{Loss in pressure energy}}{\text{Volume}} = \frac{\text{Gain in KE.}}{\text{Vol.}}$$

## 7. Speed of Efflux: Toricelli's Law



$$(P_0 + \rho gh) - P_0 = \frac{1}{2}\rho V_2^2 - \frac{1}{2}\rho V_1^2$$

$$\rho gh = \frac{1}{2}\rho V_2^2$$

$$V_2 = \sqrt{2gh}$$

$$P_1 - P_2 = \frac{1}{2}\rho V_2^2 - \frac{1}{2}\rho V_1^2$$

$$\Rightarrow \rho_m gh = \frac{1}{2}\rho \left( \frac{A_1V_1}{A_2} \right)^2 - \frac{1}{2}\rho V_1^2$$

$$V_1 = \sqrt{\frac{2\rho_m gh}{\rho \left( \left( \frac{A_1}{A_2} \right)^2 - 1 \right)}}$$

$$(2) \text{ Range } R = V_2 \sqrt{\frac{2(H-h)}{g}} = 2\sqrt{h(H-h)}$$

$$R_{\text{max.}} \frac{dR}{dh} = 0 \Rightarrow h = \frac{H}{2}$$

$$R_{\text{max.}} = H$$

# Soap bubble is energy 2 times