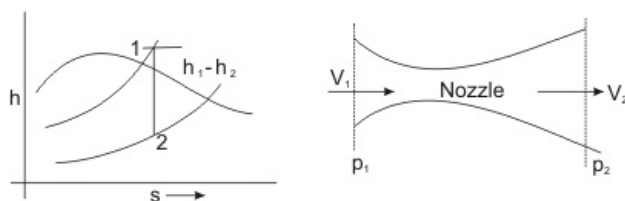


Isentropic Flow of a vapor or gas through a nozzle



First law of thermodynamics:

$$h_1 + \frac{V_1^2}{2} = h_2 + \frac{V_2^2}{2}$$

$$V_2 \approx \sqrt{2(h_1 - h_2)} \quad (\text{if } V_1 \ll V_2)$$

Where $(h_1 - h_2)$ is enthalpy drop across the nozzle

Again we know, $Tds = dh - vdp$

For the isentropic flow, $dh = vdp$

$$\text{or, } \int_1^2 dh = \int_1^2 v dp$$

$$\text{or, } (h_1 - h_2) = - \int_1^2 v dp \quad (20.1)$$

Assuming that the pressure and volume of steam during expansion obey the law $p\nu^n = \text{constant}$, where n is the isentropic index

$$- \int_1^2 v dp = - \int_1^2 (p_1 v_1^n)^{\frac{1}{n}} p^{-\frac{1}{n}} dp = - \int_1^2 (p_2 v_2^n)^{\frac{1}{n}} p^{-\frac{1}{n}} dp$$

$$= - \left\{ p_2^{\frac{1}{n}} v_2 \left[\frac{p^{1-\frac{1}{n}}}{1-\frac{1}{n}} \right]_1^2 \right\}$$

$$= - \frac{n}{n-1} \left\{ p_2^{\frac{1}{n}} v_2^2 \left[\frac{n-1}{p_2^{\frac{n-1}{n}}} - \frac{n-1}{p_1^{\frac{n-1}{n}}} \right] \right\}$$

$$= - \frac{n}{n-1} (p_2 v_2 - p_1^{\frac{1}{2}} v_1^{\frac{n-1}{n}} p_1^{\frac{1}{n}})$$

$$= \frac{n}{n-1} (p_1 v_1 - p_2 v_2) \quad (20.2)$$

Now, mass flow rate

$$\dot{m} = \rho_2 A_2 V_2$$

$$\frac{\dot{m}}{A_2} = \rho_2 V_2 = \frac{V_2}{v_2}$$

Therefore, the mass flow rate at the exit of the nozzle

$$\frac{\dot{m}}{A_2} = \frac{1}{v_2} \sqrt{\frac{2n}{n-1} p_1 v_1 \left(1 - \left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} \right)}$$

$$= \sqrt{\frac{2n}{n-1} \frac{p_1}{v_1} \left[\left(\frac{p_2}{p_1} \right)^{\frac{2}{n}} - \left(\frac{p_2}{p_1} \right)^{\frac{n+1}{n}} \right]} \quad (20.3)$$

The exit pressure, p_2 determines the \dot{m} for a given inlet condition. The mass flow rate is maximum

when,

$$\frac{d}{dy} \left[y^{\frac{2}{n}} - y^{\frac{n+1}{n}} \right] = 0 \quad ; \quad y = \frac{p_2}{p_1}$$

$$y = \left[\frac{2}{n+1} \right]^{\frac{n}{n-1}}$$

For maximum \dot{m} ,

$$\frac{p_{or}}{p_1} = \frac{p^*}{p_1} = \frac{p_2}{p_1} = \left[\frac{2}{n+1} \right]^{\frac{n}{n-1}} \quad (20.4)$$

$n = \gamma = 1.4$, for diatomic gases
 $= 1.3$, for super saturated steam
 $= 1.135$, for dry saturated steam
 $= 1.035 + 0.1x$, for wet steam with dryness fraction x

For, $n = 1.4$, $p^* = 0.528 p_1$ (50% drop in inlet pressure)

$n = 1.3$, $p^* = 0.546 p_1$

If we compare this with the results of sonic properties, as described in the earlier section, we shall observe that the critical pressure occurs at the throat for $Ma = 1$. The critical pressure ratio is defined as the ratio of pressure at the throat to the inlet pressure, for checked flow when $Ma = 1$