CL 206 - Dead-end filtration (DEF) and Rotary vacuum filter — practice problems

Q 1) The table below gives experimental data obtained during a bench scale experiment on filtration of suspensions of rehydrated active dry yeast. The membrane area was **0.0017 m^2**, the applied pressure was **60 kPa**, the wet cell concentration was **32 g/l** and the viscosity of the filtrate can be taken to be **0.001 Ns/m^2**. Determine the specific cake resistance.

$$t(s)$$
 30 60 120 180 240 270 300 360 $V_f(ml)$ 15.0 21.0 29.6 36.1 41.9 44.2 46.9 51.4

- Q 2) An aqueous suspension forms filter cakes with a specific resistance of **4x10^11 m/kg**. What filter area would be required to produce **40 l** of clear filtrate from a **20 g/l** suspension in **10 minutes**, if the operating pressure is **50 kPa**? Take the viscosity of the filtrate to be **0.001 Ns/m^2** and assume that the membrane resistance is negligible.
- Q 3) Filter cakes of E. Coli are found to have a specific cake resistance that is described by Equation $\alpha = a$ (\delta P)^n with $a = 8x10^10$ and n = 0.79, with \delta P in Pa and α in m/kg. A 20 g/l suspension is to be filtered at 30 kPa in a filter with an area of 0.5 m². How long will it take to produce 10 l of filtrate? How long would it take if the pressure were doubled? Take $\mu = 0.001$ Ns/m² and ignore the memrbane resistance.
- Q 4) A rotary vacuum filter with an area of 10 m² produces a certain filtrate flowrate at a drum speed of 1.2 rpm. An alternative filter is made available that has an area of 15 m².

At what speed should this be operated to give the same flowrate?