

# Solutions lecture 5

## 5.1 Heat loss of a person by radiation

### Analysis

We need to determine the rate of heat loss from a person by radiation.

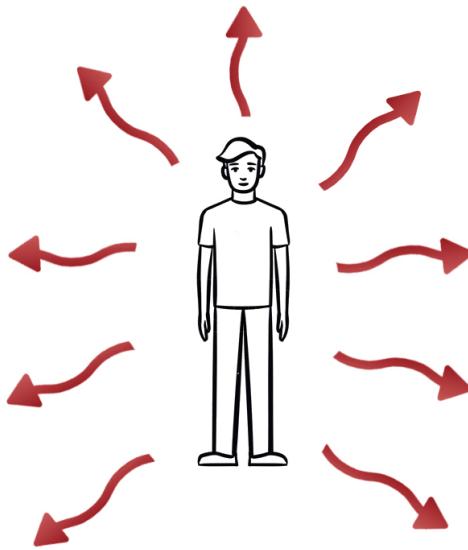


Figure 5.1: Radiation person

Given values are the surface area of the person,  $A = 1.7 \text{ m}^2$ , the emissivity constant  $\varepsilon = 0.7$ , the temperature of the person,  $T_s = 32^\circ\text{C}$ , and the temperature of the environment (the wall temperature) of  $T_\infty = 27^\circ\text{C}$

### Approach

#### Assumptions

#### Route to solution

This question can be solved by substituting all values in the Stefan-Boltzmann law:

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot A \cdot (T^4 - T_\infty^4)$$

Where  $\sigma = 5.670 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$ . Note that the temperatures are in **Kelvin**, not Celsius!

### Elaboration

Substituting all values gives:

$$\dot{Q}_{rad} = 0.7 \cdot 5.67 \cdot 10^{-8} \cdot 1.7(305.15^4 - 300.15^4) = 37.4W$$

## Evaluation

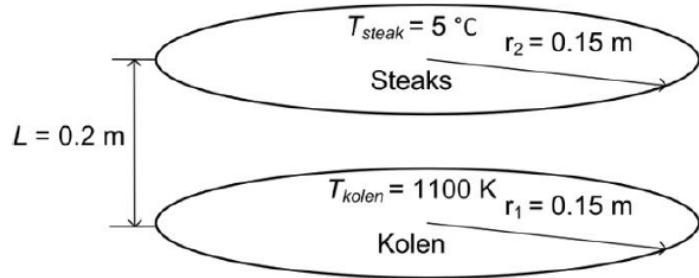
Check your answer:

- Does the answer have the correct dimensions?
- Is the answer in the right order of magnitude?
- Did you answer all the questions that were asked?

## 5.2 The BBQ

### Analysis

We need to determine the initial rate of radiation heat transfer from the coal bricks to the steaks, and the initial rate of radiation heat transfer to the stakes if the side opening of the grill is covered by aluminium foil, which can be approximated as a re-radiating surface. The diameter of the grill is 0.30m. The coal bricks have a temperature of 827 °C, the steaks have an initial temperature of 5 °C. The distance between the bricks and the steaks is 0.20 m. See the sketch below.



### Approach

#### Assumptions

Both surfaces can be treated as blackbodies, we assume the grill to be completely covered with steaks.

#### Route to solution

This question can be solved by substituting all values in the Stefan-Boltzmann law:

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot A \cdot (T_{coal}^4 - T_{steak}^4)$$

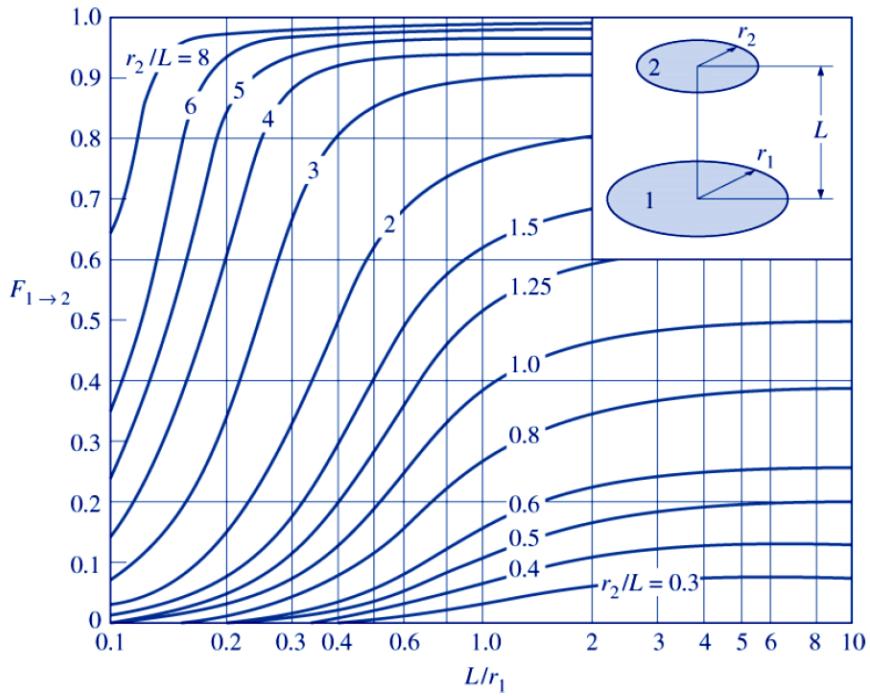
Where  $\sigma = 5.670 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$ . Note that the temperatures are in **Kelvin**, not Celsius! However, not all radiation will reach the steaks, since there is a fair distance between the surfaces. Consequently, the ‘visibility factor’  $F_{1 \rightarrow 2}$  needs to be calculated. This factor gives the ratio between the radiation coming from surface 1 reaching surface 2. Since both bodies can be treated as black bodies, they both have an emissivity of  $\varepsilon = 1$ .

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot A \cdot F_{1 \rightarrow 2} (T_{coal}^4 - T_{steak}^4)$$

Determining the visibility factor  $F_{1 \rightarrow 2}$  can be done using the diagram given in lecture 5, also given below.

Substituting all values, in Stefan Boltzmann’s law will give the initial rate of radiation heat transfer.

For the second part, we assume that the aluminum foil is an ideal reflector, such that all radiation coming from the coals reaches the steaks. In other words,  $F_{1 \rightarrow 2} = 1$ . Substituting all values will give the initial rate of radiation heat transfer for this case.



## Elaboration

We first need to determine the visibility factor from the figure. The following ratios are needed:

$L/r_{coal}$  (along the x-axis)  $\implies$  in this situation;  $L/r_{coal} = 0.2/0.15 = 1.33$  (x-axis)

$r_{steak}/L$  (along the lines)  $\implies$  in this situation;  $r_{steak}/L = 0.15 / 0.2 = 0.75$  (line)

The line 0.75 is not depicted in the diagram, so the answer needs to be extrapolated between the 0.6 and 0.8 line at the 1.33 point on the x-axis. This gives a visibility factor of about 0.28. All parameters are now determined and can be substituted into the formula:

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot A \cdot F_{1 \rightarrow 2} (T_{coal}^4 - T_{steak}^4) = 1 \cdot 5.67 \cdot 10^{-8} \cdot \pi \cdot 0.15^2 \cdot 0.28 \cdot (1100^4 - 278^4) = 1637 \text{W}$$

And for the case when the sides are covered with aluminium foil:

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot A \cdot F_{1 \rightarrow 2} (T_{coal}^4 - T_{steak}^4) = 1 \cdot 5.67 \cdot 10^{-8} \cdot \pi \cdot 0.15^2 \cdot 1 \cdot (1100^4 - 278^4) = 5845 \text{W}$$

## Evaluation

Check your answer:

- Does the answer have the correct dimensions?
- Is the answer in the right order of magnitude?
- Did you answer all the questions that were asked?

## 5.3 Radiation of heat from a coffee machine

### Analysis

We look at the coffee machine from exercise 4.2. We need to determine the emissivity of the heater plate surface, and find the total thermal resistance between the heater surface and the surrounding, as well as the total heat transfer coefficient, including convection and radiation.

### Approach

#### Assumptions

#### Route to solution

The total power is 90 W. From that,  $90 - 42.9 = 47.1$  W is radiation. Equating this to Stefan Boltzmann's law, will give  $\varepsilon$ .

For the second question,  $h_{convection}$  was determined in 4.2. the radiation part can be determined with

$$h_{rad} = \varepsilon \cdot \sigma (T_s^2 + T_\infty^2) \cdot (T_s + T_\infty)$$

The total heat transfer coefficient is defined by

$$h_{tot} = h_{convection} + h_{rad}$$

The thermal resistance from the convection part is :

$$R_{conv} = \frac{1}{h_{convection} A}$$

And the thermal resistance for the radiation part:

$$R_{rad} = \frac{1}{h_{rad} \cdot A} = \frac{1}{\varepsilon \cdot \sigma \cdot (T_s^2 + T_\infty^2) \cdot (T_s + T_\infty) \cdot A}$$

The total thermal resistance is then

$$\frac{1}{R_{tot}} = \frac{1}{R_{conv}} + \frac{1}{R_{rad}}$$

### Elaboration

For the first question, we can substitute all known values in Stefan Boltzmann's law.

$$\dot{Q}_{rad} = \varepsilon \cdot \sigma \cdot F_{1 \rightarrow \text{surface}} \cdot A \cdot (T_s^4 - T_\infty^4) = 47.1 \text{W}$$

With a visibility factor of 1, we get

$$\dot{Q}_{rad} = \varepsilon \cdot 5.670 \cdot 10^{-8} \cdot 1 \cdot \pi \left( \frac{0.16}{2} \right)^2 \cdot ((220 + 273)^4 - (20 + 273)^4) = 47.1 \text{W}$$

This gives  $\varepsilon = 0.799$ .

Now for the second question, substituting the known values into the equation for the radiation heat transfer coefficient:

$$h_{rad} = \varepsilon \cdot \sigma (T_s^2 + T_\infty^2) \cdot (T_s + T_\infty) = 11.7 \text{W m}^{-2} \text{K}^{-1}$$

With  $h_{convection} = 10.7 \text{W m}^{-2} \text{K}^{-1}$ , the total heat transfer coefficient becomes

$$h_{tot} = h_{convection} + h_{rad} = 10.7 + 11.7 = 22.4 \text{W m}^{-2} \text{K}^{-1}$$

The convection resistance is

$$R_{conv} = \frac{1}{h_{convection} A} = \frac{1}{10.7 \cdot \pi \cdot \left( \frac{0.16}{2} \right)^2} = 4.65 \text{K W}^{-1}$$

The radiation resistance:

$$R_{rad} = \frac{1}{h_{rad} \cdot A} = \frac{1}{\varepsilon \cdot \sigma \cdot (T_s^2 + T_\infty^2) \cdot (T_s + T_\infty) \cdot A} = 4.10 \text{ K W}^{-1}$$

The total thermal resistance is then

$$\frac{1}{R_{tot}} = \frac{1}{4.65} + \frac{1}{4.10} = 2.22 \text{ K W}^{-1}$$