

# MATH-UA.0251 Intro Math Modeling

**SI**

Dimensional Analysis  
Buckingham  $\pi$  theorem

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Characteristics of a physical system

- qualitative: length, time, stress, velocity, etc.
- quantitative: 2 m, 5 s, 100 Pa, etc.

a number a standard  
(unit)

given in terms of "primary" quantities: L, T, M,  $\Theta$ , C, ...

\* primary quantities can then be used to provide qualitative description of any "secondary" quantity.

EX. Area  $\doteq L^2$ , Velocity  $\doteq LT^{-1}$ , ...

the dimensions  
of an area is  
length  $\times$  length

Dimensional Homogeneity  
ws. dimensions of LHS = dimensions of RHS  
 $\bullet X + Y \rightarrow X$  and  $Y$  must have the same dimensions.  
(e.g.,  $L + M$  is meaningless!)

Ex. Gravitational Force:  $F = G \frac{m_1 m_2}{r^2}$

$m_1$ : mass of object 1  $\doteq M$

$m_2$ : mass of object 2  $\doteq M$

r: distance between the two objects  $\doteq L$

F: Force  $\doteq MLT^{-2}$

$$\text{ws. } MLT^{-2} \doteq [G] \frac{M \times M}{L^2} \rightarrow [G] = L^3 M^{-1} T^{-2}$$

dimensions of G

quantitative?  
 $\approx 6.67 \times 10^{-11} \frac{m^3}{kg \cdot s^2}$

Similarity

- Analytical solution to a problem  $\rightarrow$  an explicit formulae
- Many laws in physics
- Simple models

Ex.  $F = ma \Rightarrow$  How does "a" depend on "F" and "m"? Easy!

What if we don't have such formula?  
Experiments? Numerical solution?

Ex. Flow of a fluid through a long, horizontal, circular pipe → our concern: pressure drop per unit length

Question: what are the factors that will have an effect on the pressure drop?

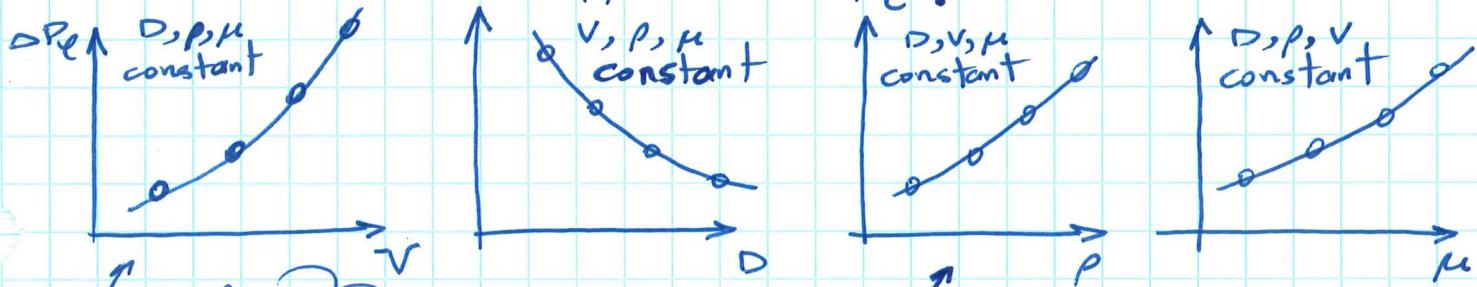
$$\Delta P_e = f(D, \rho, \mu, V)$$

viscosity  
diameter density  
velocity

$\rightarrow \Delta P_e$  is some function of  $D, \rho, \mu, V$ .

Find the nature of this function by experiments:

change one of the parameters and keep all others constant → what happens to  $\Delta P_e$ ?



\* valid for the  
specific type of  
fluid used

\* how possibly  
can one change  
(ρ and keep μ  
constant?)

\* Even if you find all of the fitting curves, how do you combine these data to obtain the desired general functional relationships which would be valid for any similar pipe system? e.g., water vs oil?

\* too many parameters

concept of  
similitude

Fortunately, there is a much simpler approach to this problem → 2 dimensionless groups instead of 5 dimensional parameters

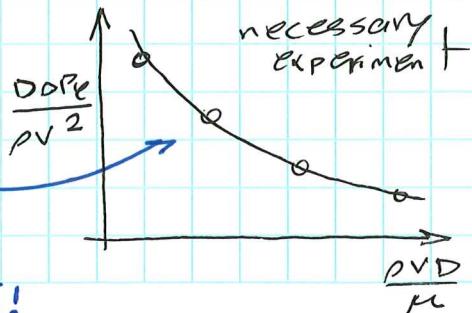
Ex. If two systems

have the same  $\frac{PV}{\mu}$ , they will have the same  $\frac{\Delta P_e}{PV^2}$  as well.

$$\frac{\Delta P_e}{PV^2} = \phi\left(\frac{PV}{\mu}\right)$$

universal  
(valid for any  
similar system)

not dependent on  
the system of units!



→ dimensional analysis → Buckingham π theorem

\* If an equation involving  $k$  variables is dimensionally homogeneous, it can be reduced to a relationship among  $k-r$  independent dimensionless groups, where  $r$  is the minimum number of reference dimensions required.  
π terms

$$u_1 = f(u_2, u_3, \dots, u_k) \Rightarrow \Pi_1 = \phi(\Pi_2, \Pi_3, \dots, \Pi_{k-r})$$

### Determination of $\Pi$ terms

- List all the variables that are involved in the problem.
- Express each of the variables in terms of basic dimensions.
- Determine the required number of  $\Pi$  terms:  $k-r$
- Select "r" repeating variables (independent) that cover all of the required dimensions together. → (not the dependent one)
- Form a  $\Pi$  term by multiplying one of the nonrepeating variables by the product of repeating variables each raised to an exponent.
- Find the exponents so that each  $\Pi$  term is dimensionless.

$$\text{Ex. } \Delta P_e = f(D, \rho, \mu, V)$$

$$\Delta P_e \doteq F L^{-3} \doteq M L^2 T^{-2}; D \doteq L; \rho \doteq M L^{-3}; \mu \doteq M L^{-1} T^{-1}; V \doteq L T^{-1}$$

$$r=3 \Rightarrow \text{number of } \Pi \text{ terms} = 5-3=2$$

repeating variables: take  $D, \rho$ , &  $V$

$$\Rightarrow \Pi_1 = \Delta P_e D^\alpha V^b \rho^c \doteq M L^{-2} T^{-2} L^\alpha L^b T^{-b} M^c L^{-3c} \doteq M^0 L^0 T^0$$

$$\Rightarrow \alpha = 1, b = -2, c = -1 \Rightarrow \Pi_1 = \frac{D \Delta P_e}{\rho V^2}$$

$$\Pi_2 = \mu D^\alpha V^b \rho^c \doteq M L^{-1} T^{-1} L^\alpha L^b T^{-b} M^c L^{-3c}$$

$$\Rightarrow \alpha = -1, b = -1, c = -1$$

$$\Rightarrow \Pi_2 = \frac{\mu}{D V \rho}$$

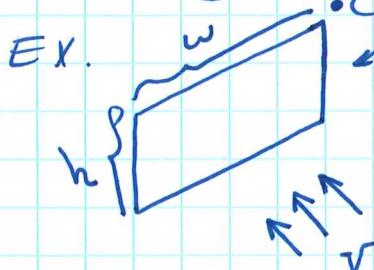
$$\Rightarrow \frac{D \Delta P_e}{\rho V^2} = \phi \left( \frac{\mu}{D V \rho} \right)$$

$$\Pi_1 \Rightarrow \bar{\phi} \left( \frac{\rho V D}{\mu} \right) \quad \Pi_2$$

# 32

- Buckingham  $\pi$  theorem  
(Applications)

- Coordinate systems & Shell Balance
- a thin plate located normal to a moving stream of fluid



$$\rightarrow F_D = f(w, h, \rho, \mu, v) \\ \text{drag force}$$

$$F_D = M L T^{-2}, w = L, h = L, \rho = M L^{-3}, \mu = M L^{-1} T^{-1}, v = L T^{-1}$$

$$\begin{aligned} \# \text{ of variables} &= 6 \\ \# \text{ of basic dimensions} &= 3 \end{aligned} \quad \Rightarrow \# \text{ of } \pi \text{ terms} = 6 - 3 = 3$$

Repeating variables:  $w, v, \rho$

$$\rightarrow \Pi_1 = F_D w^a v^b \rho^c = M^0 L^0 T^0 \Rightarrow a = -2, b = -2, c = -1$$

$$\rightarrow \Pi_1 = \frac{F_D}{w^2 v^2 \rho}$$

$$\Pi_2 = h w^a v^b \rho^c = M^0 L^0 T^0 \Rightarrow a = -1, b = 0, c = 0$$

$$\rightarrow \Pi_2 = \frac{h}{w} \quad (\text{could we guess this?})$$

$$\Pi_3 = \mu w^a v^b \rho^c = M^0 L^0 T^0 \Rightarrow a = -1, b = -1, c = -1$$

$$\rightarrow \Pi_3 = \frac{\mu}{w v \rho} \quad (\text{what about this one?})$$

$$\Rightarrow \frac{F_D}{w^2 v^2 \rho} = \phi\left(\frac{h}{w}, \frac{\mu}{w v \rho}\right) = \bar{\phi}\left(\frac{w}{h}, \frac{w v \rho}{\mu}\right) = \hat{\phi}\left(\frac{w}{h}, \frac{h v \rho}{\mu}\right) = \dots$$

\*one can have new  $\Pi$  terms from the old ones.\*



containing the variable that is to be predicted

$$\text{prototype: } \Pi_1 = \phi(\Pi_2, \Pi_3, \dots, \Pi_n)$$

$$\text{model: } \Pi_{1m} = \phi(\Pi_{2m}, \Pi_{3m}, \dots, \Pi_{nm})$$

the same  
for the two systems

$$\rightarrow \Pi_{2m} = \Pi_2, \Pi_{3m} = \Pi_3, \dots, \Pi_{nm} = \Pi_n \Rightarrow \Pi_1 = \Pi_{im} \text{ cool!}$$

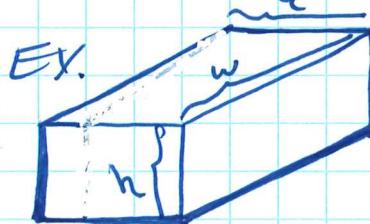
Ex. Reconsider the previous example:

$$\frac{F_D}{w^2 v^2 \rho} = \phi\left(\frac{w}{h}, \frac{\rho v w}{\mu}\right) \quad \text{vs} \quad \frac{F_{Dm}}{w_m^2 v_m^2 \rho_m} = \phi\left(\frac{w_m}{h_m}, \frac{\rho_m v_m w_m}{\mu_m}\right)$$

$$\Rightarrow \frac{w_m}{h_m} = \frac{w}{h} \quad \text{and} \quad \frac{\rho_m v_m w_m}{\mu_m} = \frac{\rho v w}{\mu} \Rightarrow \frac{F_D}{w^2 v^2 \rho} = \frac{F_{Dm}}{w_m^2 v_m^2 \rho_m}$$

$$w_m = \frac{h_m}{h} w \rightarrow v_m = \frac{\mu_m}{\mu} \frac{\rho}{\rho_m} \frac{w}{w_m} V \Rightarrow F_D = \left(\frac{w}{w_m}\right)^2 \left(\frac{\rho}{\rho_m}\right) \left(\frac{V}{v_m}\right)^2 F_{Dm}$$

\* (select an  $h_m$  and a model fluid that are easy to work with) \*



$$\text{vs} \quad \frac{F_D}{w^2 v^2 \rho} = \phi\left(\frac{w}{h}, \frac{w}{l}, \frac{\rho v w}{\mu}\right)$$

$$\text{what if } w=h=l \Rightarrow \frac{F_D}{w^2 v^2 \rho} = \phi\left(\frac{\rho v w}{\mu}\right)$$

$$\text{flow around a sphere: } \frac{F_D}{D^2 v^2 \rho} = \phi\left(\frac{\rho v D}{\mu}\right)$$

$$\text{Convention for } C_D: F_D = \frac{C_D}{2} \rho A V^2 \Rightarrow C_D = \frac{F_D}{\frac{1}{2} \rho A V^2}$$

$$\text{vs} \quad \frac{\frac{1}{2} C_D \rho \frac{\pi D^2}{4} V^2}{D^2 v^2 \rho} = \frac{\pi}{8} C_D = \phi\left(\frac{\rho v D}{\mu}\right) \text{ area} \\ \Rightarrow C_D = \psi\left(\frac{\rho v D}{\mu}\right)$$

Experiments:

\* For low  $Re$  number  $\rightarrow C_D \downarrow$  as  $Re \uparrow$

\* For high  $Re$  number  $\rightarrow C_D = \text{constant} \neq f(Re)$

correct for other geometric shapes as well

$\rightarrow 10^3 - 2 \times 10^5$  for a smooth sphere

(given information)

Stokes flow:  $Re \lesssim 1 \rightarrow$  density does not matter

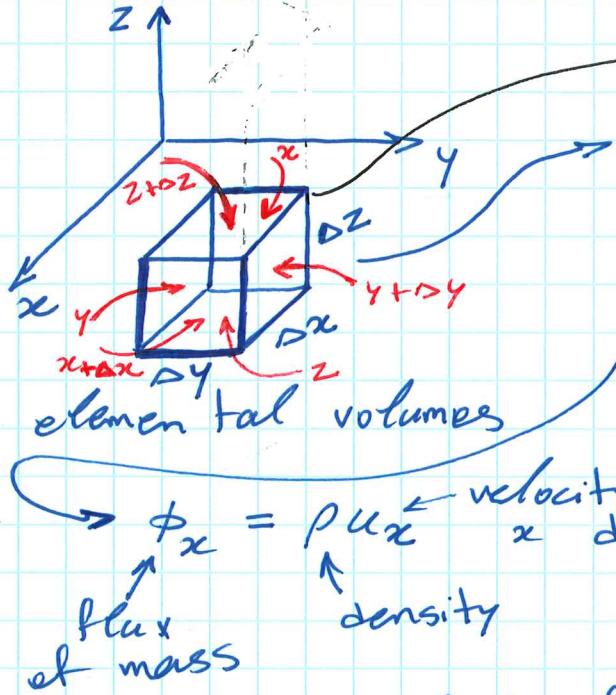
$$\Rightarrow F_D = f(D, \mu, V) \text{ vs } r=3 \Rightarrow \# \text{ of } \pi \text{ terms} = 4 - 3 = 1$$

$$\text{vs} \quad \Pi_1 = \frac{F_D}{\mu V D} = C \Rightarrow F_D = C \mu V D \quad = 3\pi \quad (\text{from theory} \& \text{experiment}) \quad (5)$$

Q: Given  $F_D = 3\pi \mu v D$ , find the function  $\phi$  so that  $C_D = \phi(Re)$  for low Re numbers.

**Coordinate Systems**  $\rightarrow$  a system that uses one-three numbers to uniquely specify the position of points.

- Cartesian Coordinate System



$$V = \Delta x \Delta y \Delta z$$

$$A_x = \Delta y \Delta z, A_y = \Delta x \Delta z, A_z = \Delta x \Delta y$$

$\phi_{x,y,z}$ : flux of a quantity (mass, energy, momentum, ...)  
 $\rightarrow$  quantity per unit area per time

flux  $\times$  Area  $\Rightarrow$  transfer rate of the quantity

**Shell Balance**  $\rightarrow \left\{ \begin{array}{l} \text{rate of change} \\ \text{in} \end{array} \right\} = \left\{ \begin{array}{l} \text{out} \\ \text{out} \end{array} \right\} + \left\{ \begin{array}{l} \text{generation} \end{array} \right\}$

$$\rightarrow \frac{\partial}{\partial t} (\rho \Delta x \Delta y \Delta z) = (\rho u_x \Delta y \Delta z)|_x + (\rho u_y \Delta x \Delta z)|_y + (\rho u_z \Delta x \Delta y)|_z$$

in  $\nearrow$       out  $\searrow$       "  $\nearrow$       "  $\searrow$       "  $\nearrow$       "  $\searrow$   
 $\downarrow$   $\Delta x$        $\downarrow$   $\Delta y$        $\downarrow$   $\Delta z$

generation  $\rightarrow +0$

$\rightarrow$  divide by  $\Delta x \Delta y \Delta z \rightarrow$

$$\frac{\partial \rho}{\partial t} = \frac{(\rho u_x)|_x - (\rho u_x)|_{x+\Delta x}}{\Delta x} + \frac{(\rho u_y)|_y - (\rho u_y)|_{y+\Delta y}}{\Delta y} + \frac{(\rho u_z)|_z - (\rho u_z)|_{z+\Delta z}}{\Delta z}$$

let  $\Delta x, \Delta y, \Delta z \rightarrow 0$  and  $\frac{\partial \rho}{\partial t} + \frac{\partial (\rho u_x)}{\partial x} + \frac{\partial (\rho u_y)}{\partial y} + \frac{\partial (\rho u_z)}{\partial z} = 0$

$\phi_{x,y,z} \equiv$  thermal energy flux

$\phi_{x,y,z} \equiv$  momentum flux

$\phi_{x,y,z} \equiv$  Navier-Stokes eqn

Continuity eqn in Cartesian Coordinates

# 32'

Clarifications re S2:

- For the drag force on a smooth sphere, we showed

$$\frac{F_D}{\rho V^2 \frac{\pi D^2}{4}} = \phi \left( \frac{\rho V D}{\mu} \right)$$



$\uparrow \uparrow \uparrow V, P, \mu$

Equivalently, one can write

$$\frac{F_D}{\frac{1}{2} \rho V^2 \frac{\pi D^2}{4}} = \psi \left( \frac{\rho V D}{\mu} \right) \quad (*)$$

where the difference between functions  $\phi$  and  $\psi$  is the sole constant  $\frac{\pi}{8}$ .

Now, the LHS of eqn (\*) is termed (by convention) as the drag coefficient  $C_D$ :

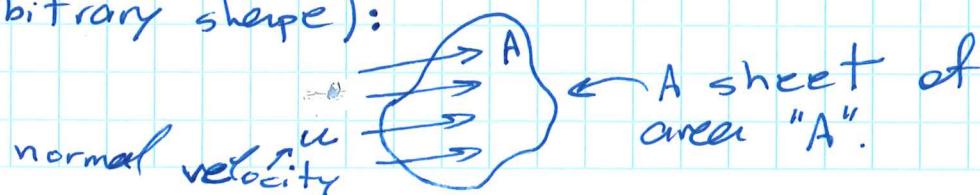
$$C_D = \psi \left( \frac{\rho V D}{\mu} \right), \text{ where } C_D = \frac{F_D}{\frac{1}{2} \rho V^2 \frac{\pi D^2}{4}}$$

We can generalize this relationship to other objects as well:

$$C_D = \psi \left( \frac{\rho V D}{\mu} \right) \rightarrow = \frac{F_D}{\frac{1}{2} \rho V^2 A} \quad \begin{array}{l} \text{projected area} = \frac{\pi D^2}{4} \\ \text{for sphere} \end{array}$$

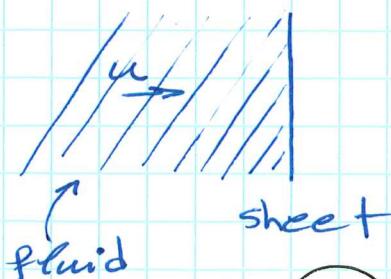
- the flowrate:  $\frac{\text{volume of fluid displaced}}{\text{Time}}$

There are better but more complicated methods to explain this. I reiterate what we discussed in class. Consider a fluid passing through an area  $A$  (with arbitrary shape):

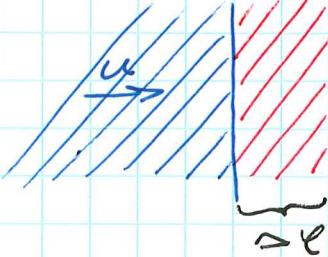


Looking at the sheet from a side:

time =  $t$



time =  $t + \Delta t$



$$\Delta V = A \Delta \ell$$

displaced volume of the fluid (volume of fluid passed through area A)

$$\frac{\text{Volume passed}}{\text{Time}} = \frac{A \Delta \ell}{\Delta t}$$

$$\text{Flowrate} = \frac{\Delta V}{\Delta t}$$

$$\Rightarrow \frac{\Delta V}{\Delta t} = \frac{A \Delta \ell}{\Delta t}$$

take limit  $\Delta t \rightarrow 0$

$$\Rightarrow \underbrace{\lim_{\Delta t \rightarrow 0} \frac{\Delta V}{\Delta t}}_{\text{flowrate}} = A \underbrace{\lim_{\Delta t \rightarrow 0} \frac{\Delta \ell}{\Delta t}}_{\text{velocity}} \Rightarrow Q = Au$$

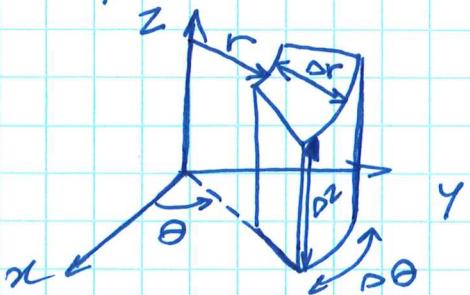
$$\rightarrow \text{mass flowrate} = \rho Q = \rho Au$$

$$\text{mass flux} = \frac{\text{mass flowrate}}{\text{unit area}} = \rho u$$

# S 3

## Coordinate Systems & Shell Balance

### Cylindrical Coordinates



$$\text{for small } \Delta r \text{ and } V = r \Delta \theta \Delta r \Delta z$$

$$A_r = r \Delta \theta \Delta z$$

$$A_\theta = \Delta r \Delta z$$

$$A_z = r \Delta \theta \Delta r$$

$$\begin{aligned} \Rightarrow \frac{\partial}{\partial t} (r \Delta \theta \Delta r \Delta z p) &= (\rho u_r r \Delta \theta \Delta z) \Big|_r \\ &- (\rho u_r r \Delta \theta \Delta z) \Big|_{r+\Delta r} + (\rho u_\theta \Delta r \Delta z) \Big|_\theta \\ &- (\rho u_\theta \Delta r \Delta z) \Big|_{\theta+\Delta \theta} + (\rho u_z r \Delta \theta \Delta r) \Big|_z \\ &- (\rho u_z r \Delta \theta \Delta r) \Big|_{z+\Delta z} \end{aligned}$$

$$\text{divide by } \Delta r \Delta \theta \Delta z \Rightarrow \frac{\partial}{\partial t} (rp) = \frac{(\rho u_r) \Big|_r - (\rho u_r) \Big|_{r+\Delta r}}{\Delta r}$$

$$\text{let } \Delta r, \Delta \theta, \Delta z \rightarrow 0 \quad + \frac{(\rho u_\theta) \Big|_\theta - (\rho u_\theta) \Big|_{\theta+\Delta \theta}}{\Delta \theta} + r \frac{(\rho u_z) \Big|_z - (\rho u_z) \Big|_{z+\Delta z}}{\Delta z}$$

$$\Rightarrow r \frac{\partial p}{\partial t} + \frac{\partial (rpur)}{\partial r} + \frac{\partial (\rho u_\theta)}{\partial \theta} + r \frac{\partial (\rho u_z)}{\partial z} = 0$$

$$\Rightarrow \frac{\partial p}{\partial t} + \frac{1}{r} \frac{\partial (rpur)}{\partial r} + \frac{1}{r} \frac{\partial (\rho u_\theta)}{\partial \theta} + \frac{\partial (\rho u_z)}{\partial z} = 0$$

Continuity eq  
in cylindrical  
coordinates

Could we find this from the eqn of the cartesian coordinates?

$$\text{Cartesian: } \frac{\partial p}{\partial t} + \frac{\partial \rho u_x}{\partial x} + \frac{\partial \rho u_y}{\partial y} + \frac{\partial \rho u_z}{\partial z} = 0$$

Express  $u_x, u_y, u_z$  in terms of the scalar velocities in the cylindrical coordinates.

see S3' for detail.

$$u_x = u_r \cos \theta - u_\theta \sin \theta$$

$$u_y = u_r \sin \theta + u_\theta \cos \theta$$

$$u_z = u_z$$

- express  $x, y, z$  in terms of  $r, \theta, z$  and vice versa.

$$\left. \begin{array}{l} x = r \cos \theta \\ y = r \sin \theta \\ z = z \end{array} \right\} \rightarrow r = \sqrt{x^2 + y^2} \text{ and } \theta = \tan^{-1}\left(\frac{y}{x}\right)$$

$$\text{and } \frac{\partial r}{\partial x} = \frac{2x}{2\sqrt{x^2+y^2}} = \frac{x}{r} = \cos \theta; \quad \frac{\partial r}{\partial y} = \frac{2y}{2\sqrt{x^2+y^2}} = \frac{y}{r} = \sin \theta$$

$$\frac{\partial \theta}{\partial x} = \frac{-y}{x^2} = \frac{-y}{x^2+y^2} = \frac{-r \sin \theta}{r^2} = \frac{-\sin \theta}{r}; \quad \frac{\partial \theta}{\partial y} = \frac{x}{x^2} = \frac{x}{x^2+y^2} = \frac{\cos \theta}{r^2} = \frac{\cos \theta}{r}$$

$$\Rightarrow \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x} (\rho u_x) + \frac{\partial}{\partial y} (\rho u_y) + \frac{\partial}{\partial z} (\rho u_z) = 0$$

$$\begin{aligned} &\Rightarrow \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial r} (\rho u_x) \frac{\partial r}{\partial x} + \frac{\partial}{\partial \theta} (\rho u_x) \frac{\partial \theta}{\partial x} + \frac{\partial}{\partial z} (\rho u_x) \frac{\partial z}{\partial x} \\ &\quad + \frac{\partial}{\partial r} (\rho u_y) \frac{\partial r}{\partial y} + \frac{\partial}{\partial \theta} (\rho u_y) \frac{\partial \theta}{\partial y} + \frac{\partial}{\partial z} (\rho u_y) \frac{\partial z}{\partial y} \\ &\quad + \frac{\partial}{\partial r} (\rho u_z) \frac{\partial r}{\partial z} + \frac{\partial}{\partial \theta} (\rho u_z) \frac{\partial \theta}{\partial z} + \frac{\partial}{\partial z} (\rho u_z) \frac{\partial z}{\partial z} \end{aligned}$$

$$\begin{aligned} &= \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial r} (\rho u_r \cos \theta - \rho u_\theta \sin \theta) (\cos \theta) + \frac{\partial}{\partial \theta} (\rho u_r \cos \theta - \rho u_\theta \sin \theta) \left(-\frac{\sin \theta}{r}\right) \\ &\quad + \frac{\partial}{\partial r} (\rho u_r \sin \theta + \rho u_\theta \cos \theta) (\sin \theta) + \frac{\partial}{\partial \theta} (\rho u_r \sin \theta + \rho u_\theta \cos \theta) \left(\frac{\cos \theta}{r}\right) \\ &\quad + \frac{\partial}{\partial z} (\rho u_z) \end{aligned}$$

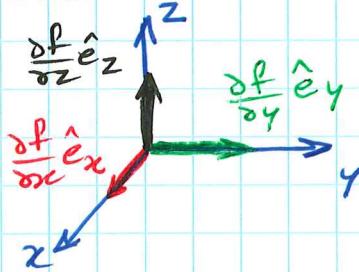
$$\begin{aligned} &= \cancel{\frac{\partial \rho}{\partial t} + \cos \theta \left[ \cos \theta \frac{\partial \rho u_r}{\partial r} - \sin \theta \frac{\partial \rho u_\theta}{\partial r} \right]} - \frac{\sin \theta}{r} \left[ \cos \theta \frac{\partial \rho u_r}{\partial \theta} - \sin \theta \frac{\partial \rho u_r}{\partial \theta} \right] - \cancel{\sin \theta \left[ \sin \theta \frac{\partial \rho u_r}{\partial r} + \cos \theta \frac{\partial \rho u_\theta}{\partial r} \right]} + \cancel{\cos \theta \left[ \sin \theta \frac{\partial \rho u_r}{\partial \theta} + \cos \theta \frac{\partial \rho u_\theta}{\partial \theta} \right]} \\ &\quad + \cancel{\frac{\partial}{\partial z} (\rho u_z)} = 0 \end{aligned}$$

$$\begin{aligned} &\Rightarrow \frac{\partial \rho}{\partial t} + \frac{\partial \rho u_r}{\partial r} \left( \cos^2 \theta + \sin^2 \theta \right) + \frac{\partial \rho u_\theta}{\partial \theta} \left( \frac{\sin^2 \theta}{r} + \frac{\cos^2 \theta}{r} \right) + \cancel{\frac{\partial \rho u_r}{\partial \theta} (0)} + \cancel{\frac{\partial \rho u_\theta}{\partial r} (0)} \\ &\quad + \rho u_r \left( \frac{\sin^2 \theta}{r} + \frac{\cos^2 \theta}{r} \right) + \rho u_\theta (0) + \cancel{\frac{\partial \rho u_z}{\partial z} (0)} = 0 \end{aligned}$$

$$\Rightarrow \frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (\rho u_r) + \frac{1}{r} \frac{\partial \rho u_\theta}{\partial \theta} + \frac{\partial \rho u_z}{\partial z} = 0 \quad \checkmark$$

Gradient of a scalar  $\nabla f$

Cartesian coordinates  $\Rightarrow \nabla f = \frac{\partial f}{\partial x} \hat{e}_x + \frac{\partial f}{\partial y} \hat{e}_y + \frac{\partial f}{\partial z} \hat{e}_z$



↑  
a vector  
 $\hat{e}_x, \hat{e}_y, \hat{e}_z$ : unit vectors  
in  $x, y, z$  directions

Cylindrical system?  $\hat{e}_x = \hat{e}_r \cos \theta - \hat{e}_\theta \sin \theta$

$$\hat{e}_y = \hat{e}_r \sin \theta + \hat{e}_\theta \cos \theta$$

$$\hat{e}_z = \hat{e}_z$$

$$\begin{aligned} \Rightarrow \nabla f &= \frac{\partial f}{\partial r} \frac{\partial r}{\partial x} (\hat{e}_r \cos \theta - \hat{e}_\theta \sin \theta) + \frac{\partial f}{\partial \theta} \frac{\partial \theta}{\partial x} (\hat{e}_r \cos \theta - \hat{e}_\theta \sin \theta) \\ &\quad + \frac{\partial f}{\partial r} \frac{\partial r}{\partial y} (\hat{e}_r \sin \theta + \hat{e}_\theta \cos \theta) + \frac{\partial f}{\partial \theta} \frac{\partial \theta}{\partial y} (\hat{e}_r \sin \theta + \hat{e}_\theta \cos \theta) \\ &\quad + \frac{\partial f}{\partial z} \hat{e}_z \end{aligned}$$

$$= \cancel{\frac{\partial f}{\partial r} (\cos \theta)} (\hat{e}_r \cos \theta - \hat{e}_\theta \sin \theta) + \cancel{\frac{\partial f}{\partial \theta} \left(-\frac{\sin \theta}{r}\right)} (\hat{e}_r \cos \theta - \hat{e}_\theta \sin \theta)$$

$$+ \cancel{\frac{\partial f}{\partial r} (\sin \theta)} (\hat{e}_r \sin \theta + \hat{e}_\theta \cos \theta) + \cancel{\frac{\partial f}{\partial \theta} \left(\frac{\cos \theta}{r}\right)} (\hat{e}_r \sin \theta + \hat{e}_\theta \cos \theta) + \frac{\partial f}{\partial z} \hat{e}_z$$

$$= \frac{\partial f}{\partial r} \left[ \cos^2 \theta \hat{e}_r - \sin \theta \cos \theta \hat{e}_\theta + \sin^2 \theta \hat{e}_r + \sin \theta \cos \theta \hat{e}_\theta \right]$$

$$+ \frac{\partial f}{\partial \theta} \left[ \frac{-\sin \theta \cos \theta}{r} \hat{e}_r + \frac{\sin^2 \theta}{r} \hat{e}_\theta + \frac{\sin \theta \cos \theta}{r} \hat{e}_r + \frac{\cos^2 \theta}{r} \hat{e}_\theta \right] + \frac{\partial f}{\partial z} \hat{e}_z$$

$$\Rightarrow \boxed{\nabla f = \frac{\partial f}{\partial r} \hat{e}_r + \frac{1}{r} \frac{\partial f}{\partial \theta} \hat{e}_\theta + \frac{\partial f}{\partial z} \hat{e}_z}$$

# SS'

How  $u_x, u_y, u_z$  depend on  $u_r, u_\theta, u_z$

$u_x$ : scalar component of velocity in the  $x$  direction  
 dot product

$$\text{ns } u_x = \underline{u} \cdot \hat{e}_x \quad \begin{matrix} \leftarrow \text{unit vector} \\ \text{in the } x\text{ direction} \end{matrix}$$

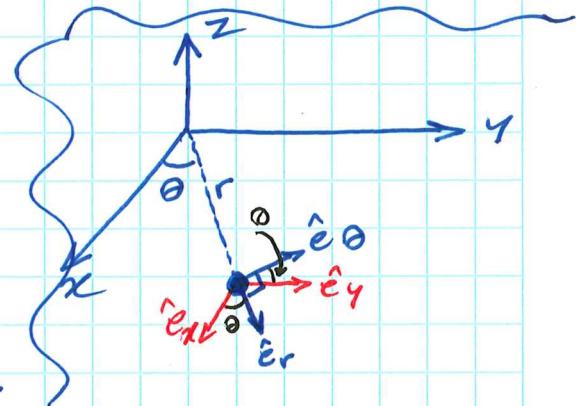
$\leftarrow$  vector of velocity

We can express  $\underline{u}$  in terms of scalar velocity components in the cylindrical coordinates:

$$\underline{u} = u_r \hat{e}_r + u_\theta \hat{e}_\theta + u_z \hat{e}_z$$

Insert into the  $u_x$  eqn above:

$$\begin{aligned} u_x &= (u_r \hat{e}_r + u_\theta \hat{e}_\theta + u_z \hat{e}_z) \cdot \hat{e}_x \\ &= u_r \hat{e}_r \cdot \hat{e}_x + u_\theta \hat{e}_\theta \cdot \hat{e}_x + u_z \hat{e}_z \cdot \hat{e}_x \end{aligned}$$



dot product of two unit vectors is simply the cosine of the angle between them.

$$\begin{aligned} \Rightarrow u_x &= u_r (\cos \theta) + u_\theta (\cos (\frac{\pi}{2} + \theta)) + u_z (\cos \frac{\pi}{2}) \\ \Rightarrow u_x &= u_r \cos \theta - u_\theta \sin \theta \end{aligned}$$

Similarly:  $u_y = (u_r \hat{e}_r + u_\theta \hat{e}_\theta + u_z \hat{e}_z) \cdot \hat{e}_y$

$$\begin{aligned} &= u_r \hat{e}_r \cdot \hat{e}_y + u_\theta \hat{e}_\theta \cdot \hat{e}_y + u_z \hat{e}_z \cdot \hat{e}_y \\ &= u_r \cos(\frac{\pi}{2} - \theta) + u_\theta \cos \theta + 0 \end{aligned}$$

ns  $u_y = u_r \sin \theta + u_\theta \cos \theta$

# 34

Heat eqn  $\equiv$  species continuity eqn

Recall the continuity eqn in the Cartesian coordinates:

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u_x}{\partial x} + \frac{\partial \rho u_y}{\partial y} + \frac{\partial \rho u_z}{\partial z} = 0$$

More generally:

$$\frac{\partial \Psi}{\partial t} + \frac{\partial \phi_x}{\partial x} + \frac{\partial \phi_y}{\partial y} + \frac{\partial \phi_z}{\partial z} = S$$

generation source  
(quantity per unit volume per unit time)

$\Psi$ : quantity of interest per unit volume  
e.g., Mass/<sub>Volume</sub> = Density ( $\rho$ )

$\phi_{x,y,z}$ : flux of the quantity in  $x, y, z$  directions

Ex. For total mass (quantity):

$S=0$ ,  $\Psi=\rho$ ,  $\phi_x=\rho u_x$ ,  $\phi_y=\rho u_y$ ,  $\phi_z=\rho u_z \rightarrow$  Continuity eqn

Cylindrical Coordinates? Easy!

$$\frac{\partial \Psi}{\partial t} + \frac{1}{r} \frac{\partial \phi_r}{\partial r} + \frac{1}{r} \frac{\partial \phi_\theta}{\partial \theta} + \frac{\partial \phi_z}{\partial z} = S$$

In vector form

$$\frac{\partial \Psi}{\partial t} + \underline{\nabla} \cdot \underline{\phi} = S$$

Heat eqn in Cartesian coordinates:

$$\Psi = \frac{\text{Energy}}{\text{Volume}} = \frac{m C_p T}{V} = \rho C_p T$$

vector form

$$\phi_x = -K \frac{\partial T}{\partial x} + \rho u_x C_p T$$

$$(\underline{\phi} = -K \nabla T + \rho \underline{u} C_p T)$$

$\uparrow$   
 $y, z$   
Fourier's Law  
(conduction)

$\uparrow$   
flux of energy  
carried by fluid

$$\rightarrow \frac{\partial P_{CPT}}{\partial t} + \frac{\partial}{\partial x} \left( -K \frac{\partial T}{\partial x} + \rho u_x C_{PT} \right) + \frac{\partial}{\partial y} \left( -K \frac{\partial T}{\partial y} + \rho u_y C_{PT} \right) \\ + \frac{\partial}{\partial z} \left( -K \frac{\partial T}{\partial z} + \rho u_z C_{PT} \right) = S$$

$$\text{now } \frac{\partial P_{CPT}}{\partial t} + \frac{\partial \rho C_P u_x T}{\partial x} + \frac{\partial \rho C_P u_y T}{\partial y} + \frac{\partial \rho C_P u_z T}{\partial z} \\ = \frac{\partial}{\partial x} \left( K \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( K \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial T}{\partial z} \right) + S$$

For constant  $K, \rho, C_P$ :

$$C_P \left( \frac{\partial T}{\partial t} + u_x \frac{\partial T}{\partial x} + u_y \frac{\partial T}{\partial y} + u_z \frac{\partial T}{\partial z} \right) = K \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + S$$

Heat earn

# 55

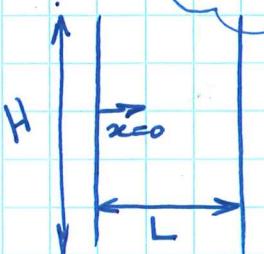
1D, steady-state transport problems

$$\text{Heat eqn: } \rho c_p \left( \frac{\partial T}{\partial t} + \underline{u} \cdot \nabla T \right) = k \nabla^2 T + s$$

Temp distribution in a plane wall

$$\underline{u} = 0, \text{ steady-state} \rightarrow \frac{\partial T}{\partial t} = 0, \text{ no source} \Rightarrow s = 0$$

$$\Rightarrow k \nabla^2 T = 0 \rightarrow k \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) = 0$$



very large in other directions

It can be assumed that  $\frac{\partial^2 T}{\partial x^2}$  is  $\gg \frac{\partial^2 T}{\partial y^2}$  and  $\frac{\partial^2 T}{\partial z^2}$ .

Why? Let  $\tilde{x} = \frac{x}{L}$ ,  $\tilde{y} = \frac{y}{H}$ ,  $\tilde{z} = \frac{z}{W}$

size in  $x, y, z$  directions

$$\rightarrow k \left( \frac{\partial^2 T}{L^2 \partial \tilde{x}^2} + \frac{\partial^2 T}{H^2 \partial \tilde{y}^2} + \frac{\partial^2 T}{W^2 \partial \tilde{z}^2} \right) = 0$$

$$\tilde{x} = O(1), \tilde{y} = O(1), \tilde{z} = O(1) \Rightarrow \frac{\partial^2 T}{\partial \tilde{x}^2} = O(T)$$

$$\frac{\partial^2 T}{\partial \tilde{y}^2} = O(T), \frac{\partial^2 T}{\partial \tilde{z}^2} = O(T) \Rightarrow \frac{1}{L^2} \gg \frac{1}{H^2} \text{ & } \frac{1}{L^2} \gg \frac{1}{W^2}$$

=> only the first term matters

$$\Rightarrow k \frac{\partial^2 T}{\partial x^2} = 0 \Rightarrow \frac{\partial T}{\partial x} = C, \Rightarrow T = C_1 x + C_2$$

Boundary Conditions

Dirichlet  $\rightarrow$

$$\text{at } x=0 \Rightarrow T = T_0$$

$$\text{at } x=L \Rightarrow T = T_L$$

value of the variable is given

$$\rightarrow \text{I: } T_0 = C_2; \text{ II: } T_L = C_1 L + T_0 \rightarrow C_1 = \frac{T_L - T_0}{L}$$

$$\Rightarrow T = \frac{T_L - T_0}{L} x + T_0$$

Neumann

at  $x=0 \Rightarrow T = T_0$  (I)  
 at  $x=L \Rightarrow \frac{dT}{dx} \Big|_{x=L} = 0$  (II) gradient is given

$$\textcircled{I}: C_2 = T_0; \quad \textcircled{II}: \frac{dT}{dx} = C_1 = 0$$

$T = T_0$

Robin

$$\text{at } x=0 \Rightarrow T = T_0 \quad \textcircled{I}$$

$$\text{at } x=L \Rightarrow -K \frac{dT}{dx} \Big|_{x=L} = h(T_L - T_\infty) \quad \textcircled{II}$$

$h(T_w - T_\infty)$  is known as  
 the Newton's cooling law  $\rightarrow$  heat flux from  
 a surface to a  
 medium is proportional  
 to the temp. difference  
 convection  
 heat-transfer  
 coefficient

$$\textcircled{I}: C_2 = T_0; \quad \textcircled{II}: -K C_1 = h(C_1 L + T_0 - T_\infty)$$

$$\Rightarrow C_1(hL + K) = h(T_\infty - T_0) \Rightarrow C_1 = \frac{h(T_\infty - T_0)}{hL + K}$$

$$\Rightarrow T = \frac{h(T_\infty - T_0)}{hL + K} x + T_0$$

Homogeneous Neumann at  $x=0 \& L$

$$\begin{aligned} \text{at } x=0 &\Rightarrow \frac{dT}{dx} = 0 \\ \text{at } x=L &\Rightarrow \frac{dT}{dx} = 0 \end{aligned} \quad \left. \right\} \Rightarrow C_1 = 0; C_2 = ?!!!$$

Note: heat flux through a solid can be expressed as  $-K \nabla T \rightarrow$  1D system  $\Rightarrow q = -K \frac{dT}{dx}$

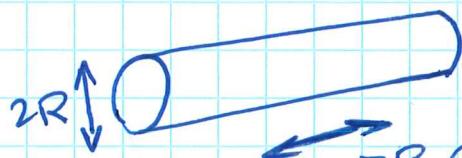
$\frac{dT}{dx} = 0 \equiv -K \frac{dT}{dx} = 0 \Rightarrow$  insulation  $\rightarrow$  total energy is conserved

$$C_2 = \frac{1}{L} \int_0^L T_{\text{initial}} dx \quad (\text{depends on initial conditions})$$

average temp.  
 at  $t=0$

A cylinder with heat source

$$T = T_w \text{ at } r = R$$



only the  $r$ -direction term matters  
symmetric/uniform in  $\theta$  direction

$$\rightarrow \frac{K}{r} \frac{d}{dr} \left( r \frac{dT}{dr} \right) + S = 0 \rightarrow d\left(r \frac{dT}{dr}\right) = -\frac{S}{K} r dr$$

$$\Rightarrow r \frac{dT}{dr} = -\frac{S}{2K} r^2 + C_1 \rightarrow T = -\frac{S}{4K} r^2 + C_1 \ln r + C_2$$

$T$  should be finite at  $t=0$

$$\rightarrow C_1 = 0$$

$$r=R \Rightarrow T_w = -\frac{SR^2}{4K} + C_2 \Rightarrow C_2 = T_w + \frac{SR^2}{4K}$$

$$\Rightarrow T = -\frac{S}{4K} (r^2 - R^2) + T_w$$

Consistency check  $\rightarrow$  Heat generated = Heat out

$$\frac{S}{4\pi R^2 K} = -K \frac{dT}{dr} \Big|_{2\pi RL}$$

$$= -K \left(-\frac{2SR}{4K}\right) \Big|_{2\pi RL} \quad \checkmark$$

\* Heat and Mass transfer equations are mathematically "identical".

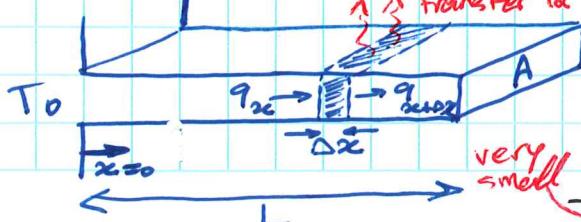
## Conduction - Convection Systems (Fin)



$$T_\infty$$

$$A, T_0 \quad Q = hA(T_0 - T_\infty)$$

An idea  $\rightarrow$  increase  $A$



$h$  is hard to change.

$T_0 - T_\infty$  is usually constant.

not water? room temp  
temp. difference in y,z directions  
Assumption: temp. changes only in the  $x$  direction.

$$( \rightarrow -K \nabla T \sim h (T - T_\infty) )$$

$$\Delta T \sim \frac{hL}{K} (T - T_\infty) \quad \text{length scale in y,z directions}$$

(17)

$$\text{energy balance} \rightarrow q_x = (-k \frac{dT}{dx} A)_x ; q_{x+\Delta x} = (-k \frac{dT}{dx} A)_{x+\Delta x}$$

$$Q = h P \Delta x (T - T_\infty)$$

$$\Rightarrow (-k \frac{dT}{dx} A)_x - (-k \frac{dT}{dx} A)_{x+\Delta x} = h P \Delta x (T - T_\infty)$$

constant  
 $k$  and  $A$

$$\frac{d^2 T}{dx^2} - \frac{hP}{kA} (T - T_\infty) = 0 \quad m^2 = \frac{hP}{kA}$$

$$\text{Let } \Theta = T - T_\infty \rightarrow \frac{d^2 \Theta}{dx^2} - m^2 \Theta = 0$$

$$\text{Guess } \Theta = e^{mx} \Rightarrow \alpha = \pm m \Rightarrow \Theta = C_1 e^{mx} + C_2 e^{-mx}$$

$$\text{BCs: at } x=0 \rightarrow T=T_0 \rightarrow \Theta = T_0 - T_\infty = \Theta_0 \Rightarrow C_1 + C_2 = \Theta_0$$

$$\text{Assume } L \rightarrow \infty \Rightarrow \Theta = 0 \text{ as } x \rightarrow \infty \Rightarrow C_1 = 0$$

↑  
the surface temp. reaches to  
the ambient temp for large  $L$

$$\rightarrow \Theta = \Theta_0 e^{-mx} \rightsquigarrow \frac{T - T_\infty}{T_0 - T_\infty} = e^{-mx} \quad = \int_0^L h P \Theta dx$$

$$\text{Total heat into the ambient } Q = -kA \left. \frac{dT}{dx} \right|_{x=0}$$

$$= -kA \left. \frac{d\Theta}{dx} \right|_{x=0} = \sqrt{kA h P} \Theta_0$$

# 36 An evaporating water droplet

Concentration: amount of material

(e.g., concentration of water vapor per unit volume)

Concentration of water vapor per unit volume of air  $\xrightarrow{\text{diffusivity coefficient}}$

$$\text{Flux of mass} \equiv J_A = -D \frac{\partial C_A}{\partial r} + u C_A$$

mass/mole

of a species (A)  
in a medium

(e.g., water vapor  
in air)

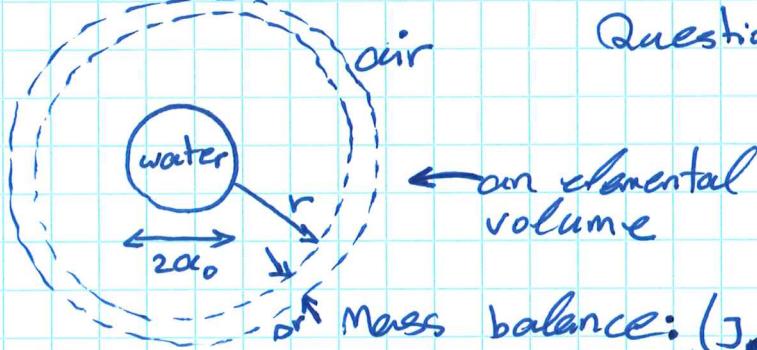
Fick's law

$\uparrow$

diffusion

convection

$\uparrow$



Question: How long does it take for the radius to drop to some  $\alpha < \alpha_0$  due to evaporation?

$$\text{or Mass balance: } (J_{Ar} 4\pi r^2)_r - (J_{Ar} 4\pi r^2)_{r+\Delta r} = 0$$

\* Clearly  $\alpha$  (radius of the droplet) is changing due to evaporation.

But we assume that happens very slowly so that the concentration profile around the droplet is almost steady-state at all times.

\* pseudo steady state

diffusion time scale << evaporation time scale

$$\frac{d}{dr} (J_{Ar} 4\pi r^2) = 0 \Rightarrow -D \frac{dC_A}{dr} (4\pi r^2) = k,$$

$$= -D \frac{dC_A}{dr}$$

$$\Rightarrow C_A = \frac{k_1}{4\pi D r} + k_2$$

BCs: at  $r=\alpha \Rightarrow C_A = C_A^*$   $\leftarrow$  saturation concentration (function of temp)

as  $r \rightarrow \infty \Rightarrow C_A \rightarrow C_A^\infty$

$\leftarrow$  concentration of water vapor in the ambient

$$\Rightarrow \frac{C_A - C_A^\infty}{C_A^* - C_A^\infty} = \frac{\alpha}{r}$$

Now we write a balance for the droplet:

$$\frac{d}{dt} \left( \frac{4}{3} \pi \alpha^3 \rho / \text{MW} \right) = - \left( J A_r 4 \pi r^2 \right)_{r=\alpha} = \left[ \frac{D \alpha (C_A^* - C_A^\infty)}{\rho \pi} \right]_{r=\alpha}^{2\alpha}$$

time derivative  
of the total  
moles of water  
in the droplet

$$\Rightarrow 4 \pi \alpha^2 \frac{\rho}{\text{MW}} \frac{d\alpha}{dt} = - D \alpha (C_A^* - C_A^\infty) / \rho \pi$$

$$\rightarrow \frac{d\alpha}{dt} = - \frac{D \text{MW} (C_A^* - C_A^\infty)}{\rho \alpha^2}$$

Integrate now  $\alpha^2 = \alpha_0^2 \left( 1 - \frac{2 D \text{MW} (C_A^* - C_A^\infty)}{\rho \alpha_0^2} t \right)$

$$T_e = \frac{\rho \alpha_0^2}{2 D \text{MW} (C_A^* - C_A^\infty)}$$

time scale of evaporation

$$T_D = \frac{\alpha_0^2}{D}$$

time scale of diffusion

has dimensions  $\frac{1}{\text{time}}$

$$\frac{\rho \alpha_0^2}{2 D \text{MW} (C_A^* - C_A^\infty)} \gg \frac{\alpha_0^2}{D}$$

$$\rightarrow \frac{\rho}{2 \text{MW} (C_A^* - C_A^\infty)} \gg 1 \quad \checkmark$$

How much does it take for the droplet radius to decrease to  $\alpha = \alpha_c$

$$\Rightarrow t_c = \left( 1 - \left( \frac{\alpha_c}{\alpha_0} \right)^2 \right) \frac{\rho \alpha_0}{2 D \text{MW} (C_A^* - C_A^\infty)}$$

Let  $\rho = 1000 \frac{\text{kg}}{\text{m}^3}$ ,  $D = 2.5 \times 10^{-5} \frac{\text{m}^2}{\text{s}}$ ,  $\text{MW} = 18 \times 10^{-3} \frac{\text{kg}}{\text{mol}}$

$$C_A^* = 1.2 \frac{\text{mol}}{\text{m}^3}, C_A^\infty = \frac{1}{150} C_A^* \Rightarrow \alpha_0 = 5 \mu\text{m}$$

$$\frac{P_A^*}{RT} \leftarrow 3 \times 10^3 \text{ Pa} \quad \alpha_c = 2.5 \mu\text{m} \quad \Rightarrow t_c = 34 \text{ ms}$$

150 Relative Humidity

respiratory droplet size for breathing and talking

How long does it take for the respiratory drop to fall on the ground?

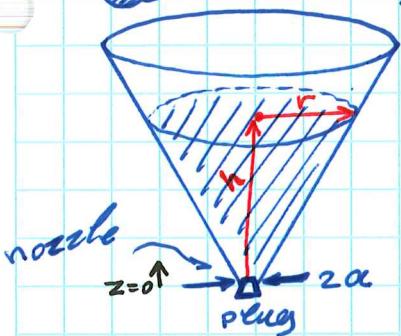
Stokes?  $V = \frac{4 \alpha_0^2 (\rho - \rho_{\text{air}}) g}{18 \mu_{\text{air}}} \approx 2.7 \frac{\text{mm}}{\text{s}} \Rightarrow Re = \frac{\rho_{\text{air}} V (2 \alpha_0)}{\mu_{\text{air}}} \approx 0.0014 \ll 1 \quad \checkmark$

Falling time  $\approx \sqrt{\frac{H}{V}} \approx 740 \text{ s}$   
 $\approx 2 \text{ m}$

It is actually more than this because  $\alpha < \alpha_0$  and  $\rho < \rho_{\text{water}}$

# 37

- \* A draining cone-shape reservoir
- \* Bernoulli's eqn
- \* Finite difference method & Euler method



We remove the plug at  $t=0$ ; how long does it take for the height of the liquid ( $h$ ) to drop to  $h' < h$ ?

Bernoulli's eqn (steady, inviscid, velocity head incompressible flow)

$$\text{pressure} \rightarrow P + \frac{1}{2} \rho u^2 + \rho g z = \text{constant}$$

point 1: on the surface of liquid at  $z=h$ ,  $P=P_{\text{atm}}$ ,  $u=u_1$   
 " 2: at the outlet (nozzle) at  $z=0$ ,  $P=P_{\text{atm}}$ ,  $u=u_2$

$$P_{\text{atm}} + \frac{1}{2} \rho u_1^2 + \rho g h = P_{\text{atm}} + \frac{1}{2} \rho u_2^2 + 0 \Rightarrow gh = \frac{1}{2} u_2^2 \left(1 - \left(\frac{u_1}{u_2}\right)^2\right)$$

$$\begin{aligned} r &\rightarrow \tan \theta = \frac{r-\alpha}{h} \rightarrow r = \alpha + h \tan \theta \\ \text{Conservation of mass: } A_1 u_1 &= A_2 u_2 \\ \Rightarrow \pi (\alpha + h \tan \theta)^2 u_1 &= \pi \alpha^2 u_2 \end{aligned}$$

$$\Rightarrow \frac{u_1}{u_2} = \frac{\alpha^2}{(\alpha + h \tan \theta)^2} = \left(\frac{1}{1 + \frac{h \tan \theta}{\alpha}}\right)^2 \ll 1 \text{ for } \alpha \ll h$$

$$\therefore \Rightarrow gh \approx \frac{1}{2} u_2^2 \Rightarrow u_2 = \sqrt{2gh}$$

Volume of fluid (a truncated cone)

$$V = \frac{1}{3} \pi \frac{h}{r-\alpha} (r^3 - \alpha^3) = \frac{\pi}{3 \tan \theta} (r^3 - \alpha^3)$$

Balance for the volume of fluid:

$$\begin{aligned} \frac{dV}{dt} &= -A_2 u_2 \Rightarrow \frac{d}{dt} \left( \frac{\pi}{3 \tan \theta} (r^3 - \alpha^3) \right) = -\pi \alpha^2 \sqrt{2gh} = -\pi \alpha^2 \sqrt{2g \frac{r-\alpha}{\tan \theta}} \\ \Rightarrow \frac{\pi}{3 \tan \theta} \pi r^2 \frac{dr}{dt} &= -\pi \alpha^2 \sqrt{2g \frac{r-\alpha}{\tan \theta}} \rightarrow r^2 \frac{dr}{dt} = -\alpha^2 \sqrt{2g \tan \theta} \sqrt{r-\alpha} \end{aligned}$$

We need to solve this ODE to find  $r$  vs  $t$  constant:  $\gamma$

Approach 1:  $r^2 \frac{dr}{dt} = -\gamma \sqrt{r-\alpha} \rightarrow$  integrate to find  $r$  as a function of  $t$   
 ↳ focus of next session

Approach 2: Numerical solution to \*

$$\frac{dr}{dt} = -\frac{\gamma \sqrt{r-\alpha}}{r^2}$$

Recall

$$\frac{dr}{dt} = \lim_{\Delta t \rightarrow 0} \frac{r(t+\Delta t) - r(t)}{\Delta t}$$

what if  $\Delta t$  is something small but not  $\rightarrow 0$ ?

$$\Rightarrow \frac{dr}{dt} \approx \frac{r(t+\Delta t) - r(t)}{\Delta t} = -\frac{\gamma \sqrt{r-\alpha}}{r^2}$$

$$\Rightarrow \frac{r(t+\Delta t) - r(t)}{\Delta t} = -\frac{\gamma \sqrt{r(t)-\alpha}}{r(t)}$$

→ if we know  $r(t)$ , we can find  $r(t+\Delta t)$

\* More generally:  $\frac{r_{i+1} - r_i}{\Delta t} = -\gamma \frac{\sqrt{r_i - \alpha}}{r_i^2}$

to  $t_1, t_2, \dots, t_i, \dots$   
 o  $\Delta t, 2\Delta t, \dots, i\Delta t, \dots$

$$r_{i+1} = r_i - \Delta t \gamma \frac{\sqrt{r_i - \alpha}}{r_i^2}$$

↳ what about this one?

$r \approx r(t)$  or  $r(t+\Delta t)$

Euler's method

$$r_{i+1} = r_i + \Delta t \gamma \frac{\sqrt{r_i - \alpha}}{r_i^2}$$

$$r_i = r(t_i)$$

$$t_{i+1} = t_i + \Delta t$$

$r_0$  is given by the initial conditions:

$$\text{at } t=0, h=h_0 \Rightarrow r_0 = \alpha + h_0 \tan \theta$$

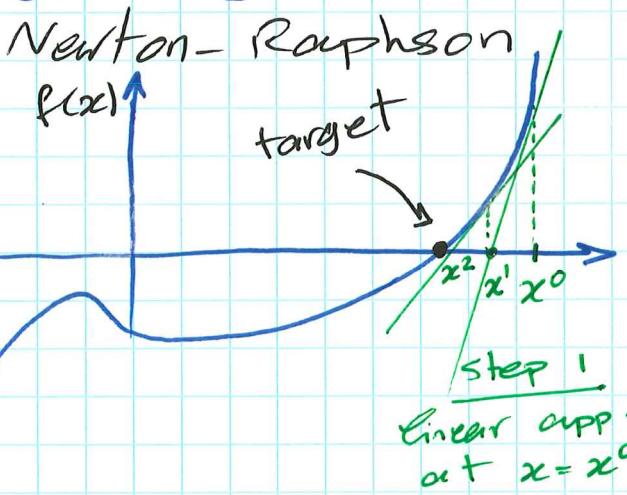
\* See the code drawing Reservoir.py

# 38

Newton-Raphson

Projectile motion with drag  
A radiating body

$$f(x) = 0$$



$$\text{step 1: } f'(x^0) = \frac{L(x^0) - L(x^1)}{x^0 - x^1}$$

$$\Rightarrow x^1 = x^0 - \frac{f(x^0)}{f'(x^0)}$$

$$\Rightarrow x^{k+1} = x^k - \frac{f(x^k)}{f'(x^k)}$$

in each iteration

$x^0$  (initial guess)  $\rightarrow x^1, x^2, \dots$

Recall from last session:

$$|f(x^k)| < \epsilon \quad (\text{tolerance})$$

small value

$$r^2 \frac{dr}{dt} = -8\sqrt{r-a} \rightarrow \int \frac{r^2}{\sqrt{r-a}} dr = -8t + C$$

from the LC  
 $r=r_0$  at  $t=0$

$$\Rightarrow \frac{2}{15} \sqrt{r-a} (8a^2 + 4ar + 3r^2) + 8t - C = 0$$

$\rightarrow$  at each time  $t=t_i$ :  $(t_0, t_1, t_2, \dots)$

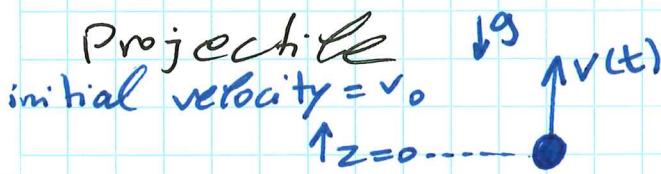
$$f(r) = \frac{2}{15} \sqrt{r-a} (8a^2 + 4ar + 3r^2) + 8t_i - C = 0$$

$$f'(r) = \frac{2}{15} \left[ \frac{2}{\sqrt{r-a}} (8a^2 + 4ar + 3r^2) + \sqrt{r-a} (4a + 6r) \right]$$

$$r^{k+1} = r^k - \frac{f(r^k)}{f'(r^k)}, \quad r^0 = r_{i-1} \quad \begin{matrix} \text{value from the} \\ \text{previous time} \end{matrix}$$

when  $|f(r^k)| < \epsilon \Rightarrow r_i = r^k$

see code  
drainingReservoirNewton.py



$$m \ddot{z} = -mg - \epsilon \dot{z}^3$$

$$\Rightarrow m \ddot{v} = -mg - \epsilon v^3$$

$$2f \epsilon = 0 \Rightarrow m \ddot{v} = -mg \rightarrow \ddot{v} = -g \rightarrow v = -gt + v_0$$

$$\Rightarrow z = -\frac{1}{2}gt^2 + v_0 t$$

Note: max height happens when  $v=0 \Rightarrow t = \frac{v_0}{g}$

When  $\epsilon \neq 0 \rightarrow$  numerical (or perturbation)

$$m \frac{dv}{dt} = -mg - \epsilon v^3$$

Focus of another session

$$\text{Euler's method: } \frac{v_{i+1} - v_i}{\Delta t} = -g - \frac{\epsilon}{m} v_i^3$$

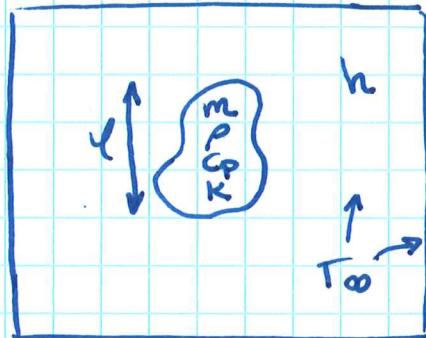
$$\Rightarrow v_{i+1} = v_i - \Delta t \left( g + \frac{\epsilon}{m} v_i^3 \right)$$

$$\frac{dz}{dt} = v \Rightarrow \frac{z_{i+1} - z_i}{\Delta t} = v_i \Rightarrow z_{i+1} = z_i + \Delta t v_i$$

see code projectile.py

## A radiating body

Consider a body of material (e.g., a sphere, cylinder, cubes etc.) in a large room.



## Energy balance

$$\frac{d}{dt}(mc_p T) = -hA(T - T_\infty) - \sigma \epsilon (T^4 - T_\infty^4)A$$

$\sigma \approx 5.7 \times 10^{-8} \frac{W}{m^2 \cdot K^4}$   
 emissivity  
 $\tau_{cond} \approx \frac{K}{\alpha} \leftarrow$  thermal diffusivity  
 radiation  
 $= 1$  for Stefan-Boltzmann  
 black body equation

$$\Rightarrow \frac{dT}{dt} = -\frac{hA}{mc_p} (T - T_\infty) - \frac{\sigma \epsilon A}{mc_p} (T^4 - T_\infty^4)$$

$$\text{Euler? } T_{i+1} = T_i - \Delta t \left[ \frac{hA}{mc_p} (T - T_\infty) + \frac{\sigma \epsilon A}{mc_p} (T^4 - T_\infty^4) \right]$$

see code radiatingBody.py

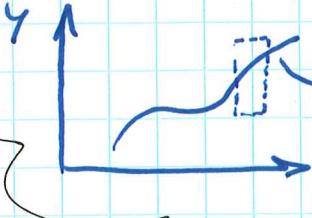
$$\tau_{conv} \sim \frac{mc_p}{hA}$$

# 39

## Flows on the line

12n

A digression on calculus (re HW #2)



$$\frac{ds}{dy} \approx \frac{dy}{dx} \Rightarrow ds = \sqrt{dx^2 + dy^2}$$

$$= |dx| \sqrt{1 + \left(\frac{dy}{dx}\right)^2} \rightarrow \dots$$

$$\dot{x} = f(x)$$

~~$\dot{x} = P(x, t)$  ?~~

not for now

$x(t) \rightarrow$  a real valued function of  $t$   
 $f(x) \rightarrow$  a " " " "  
 smooth  
 usually nonlinear

Interpreting a differential eqn as a vector field

$$\dot{x} = \sin x \Rightarrow dt = \frac{dx}{\sin x} \Rightarrow t = \int \frac{\sin^2 \frac{x}{2} + \cos^2 \frac{x}{2}}{2 \sin \frac{x}{2} \cos \frac{x}{2}} dx \rightarrow \dots$$

$$t = \ln |\tan \frac{x}{2}| + C$$

$$\text{Let } x = x_0 \text{ at } t = 0 \Rightarrow C = -\ln |\tan \frac{x_0}{2}|$$

$$\Rightarrow t = \ln \left| \frac{\tan \frac{x}{2}}{\tan \frac{x_0}{2}} \right|$$

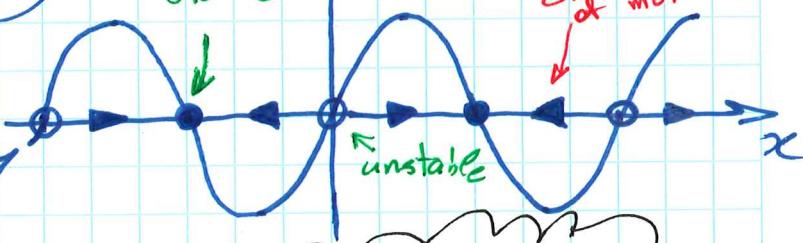
exact but very difficult to interpret

Alternative:

$t \rightarrow$  time

$x \rightarrow$  position of an imaginary particle moving along the real line

$\dot{x} \rightarrow$  velocity of that particle



a vector field on the line

→ dictates the velocity vector at each  $x$

$\dot{x} > 0 \rightarrow$  flow to the right

$\dot{x} < 0 \rightarrow$  " " " left

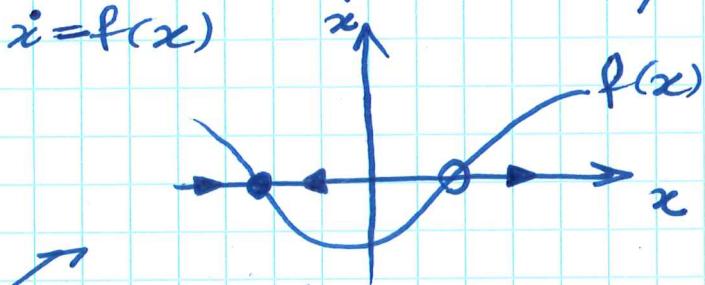
$\dot{x} = 0 \rightarrow$  no flow (fixed points)

Stable FP: attractors, sinks      Unstable FP: repellers, sources

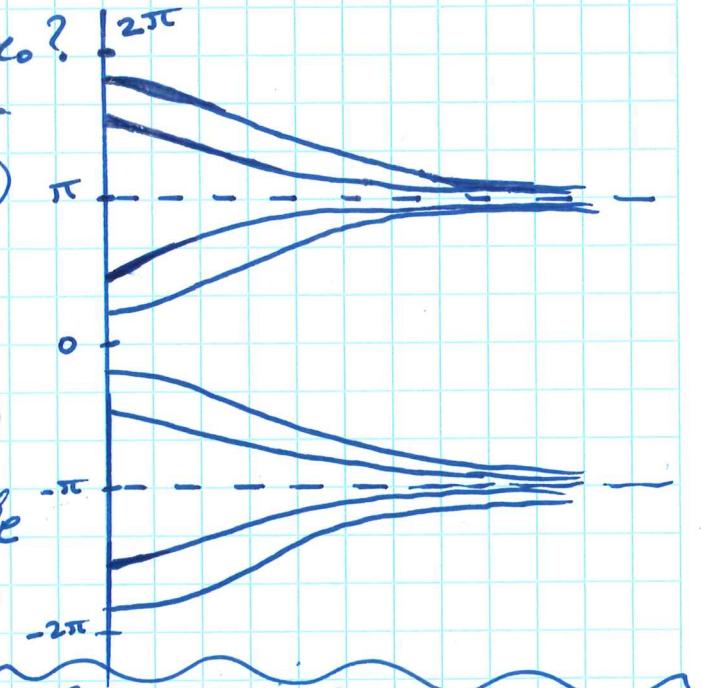
Q: Suppose  $x_0 = \frac{\pi}{4} \rightarrow$  describe the qualitative features of the solution  $x(t)$  for all  $t > 0$ . What happens as  $t \rightarrow \infty$ ?

Q: What about an arbitrary  $x_0$ ?

Fixed Points & Stability



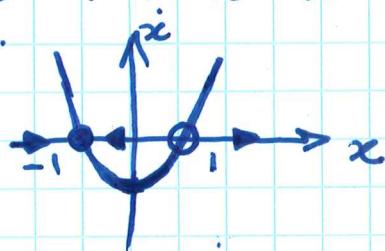
phase point: our imaginary particle  
trajectory:  $x(t)$  (based on  $x_0$ )  
phase portrait



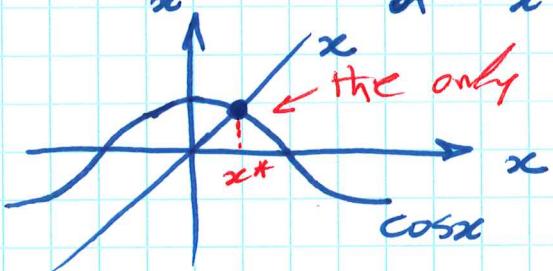
EX. Find all fixed points for  $\dot{x} = x^2 - 1$ , and classify their stability.

$$f(x^*) = 0 \Rightarrow x^* = \pm 1$$

↑  
fixed  
point



EX. Determine the stability of the fixed points of  $\dot{x} = x - \cos x$



$$\begin{aligned} x > x^* &\Rightarrow \dot{x} > 0 \\ x < x^* &\Rightarrow \dot{x} < 0 \end{aligned} \quad \left. \begin{array}{l} \Rightarrow \text{unstable} \end{array} \right\}$$

but what is the value of  $x^*$ ?

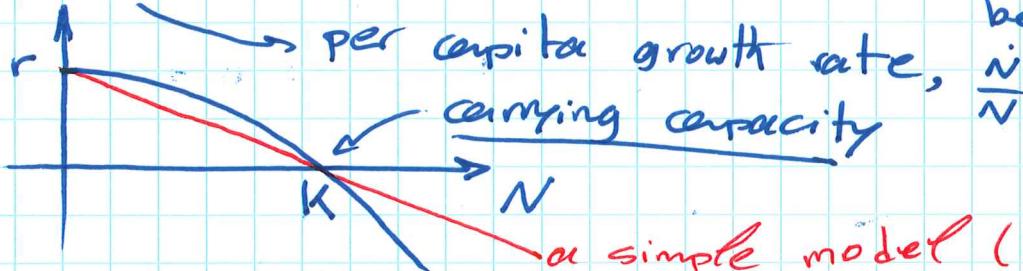
# 310

## Population Growth Linear Stability Analysis Potentials

population of organisms at time  $t$

$$\dot{N} = rN \rightarrow r > 0 \text{ is the growth rate}$$

and  $\frac{dN}{dt} = rN \Rightarrow N = N_0 e^{r t}$  unreasonable!  
growth rate + the growth rate cannot be constant



a simple model (linear)

$$\Rightarrow \frac{\dot{N}}{N} = r(1 - \frac{N}{K}) \Rightarrow \dot{N} = rN(1 - \frac{N}{K})$$

Analytical solution:  $\frac{dN}{dt} = rN(1 - \frac{N}{K}) \Rightarrow \frac{dN}{N(1 - \frac{N}{K})} = r dt$

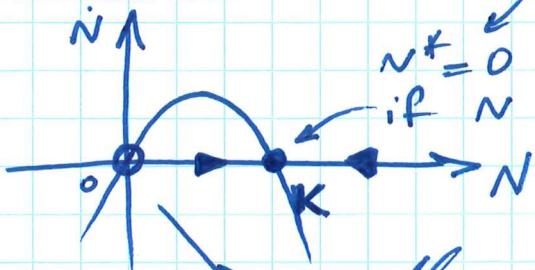
partial fractions:

$$\frac{1}{N(1 - \frac{N}{K})} = \frac{A}{N} + \frac{B}{1 - \frac{N}{K}} = \frac{A - \frac{A}{K}N + BN}{N(1 - \frac{N}{K})} \Rightarrow A = 1, B = \frac{A}{K} = \frac{1}{K}$$

$$\Rightarrow \int \frac{dN}{N(1 - \frac{N}{K})} = \int \frac{1}{N} dN + \int \frac{1}{1 - \frac{N}{K}} dN = \ln \left| \frac{N}{1 - \frac{N}{K}} \right| = rt + C$$

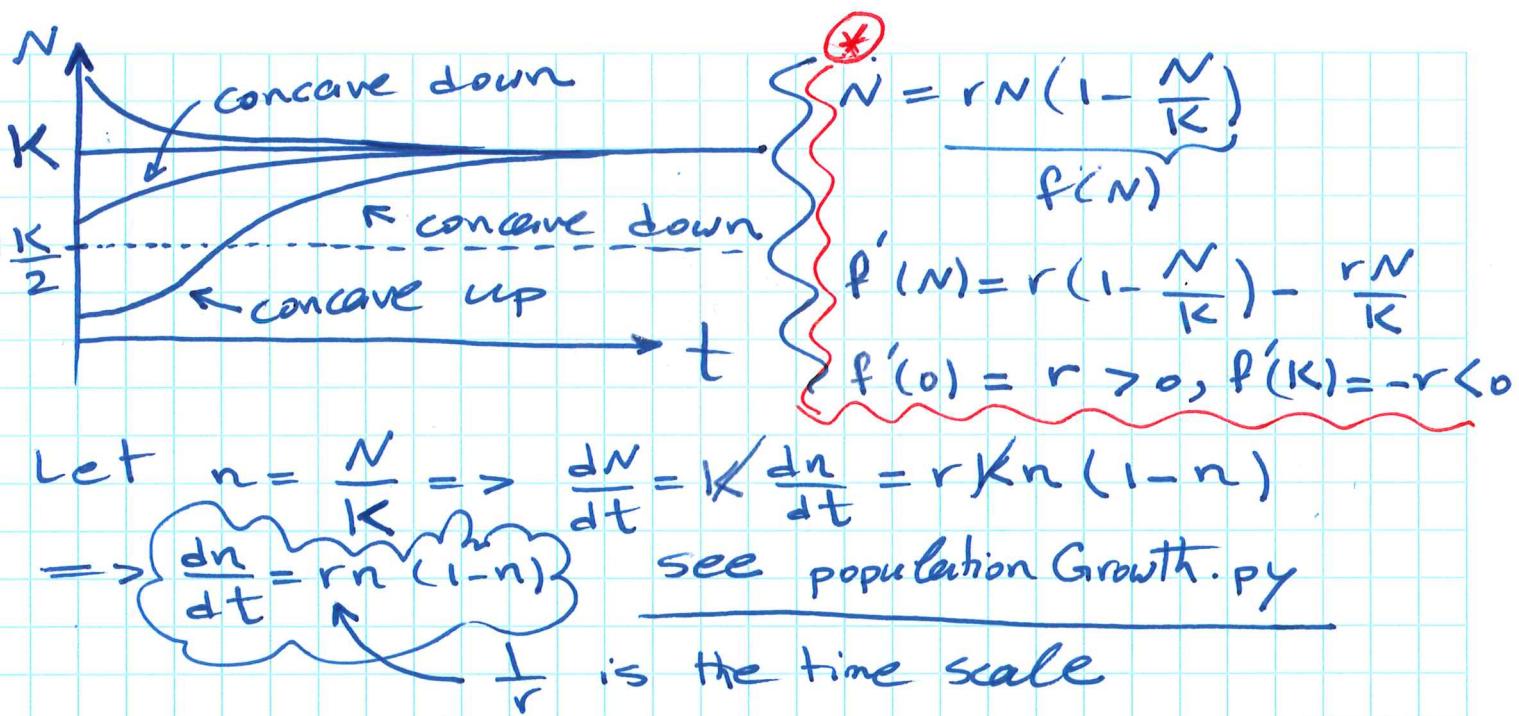
Alternative  $\rightarrow$  Let  $x = \frac{1}{N} \Rightarrow ...$

Graphical:



$N^* = 0$  and  $N^* = K$  are the fixed points  
if  $N$  is disturbed from  $K \Rightarrow N \rightarrow K$  as  $t \rightarrow \infty$   
monotonically

a small population grows exponentially fast  
 $N_0 = 0?$   $\Rightarrow$  there's nobody around to reproduce!



### Linear stability Analysis

Let  $x^*$  be a fixed point of the system  $\dot{x} = f(x)$ .  
 Let  $\eta = x - x^*$  be a small perturbation away from  $x^*$ .

$\dot{\eta} = \dot{x} - \overset{\circ}{\eta} = \dot{x} = f(x) = f(x^* + \eta)$

$x^*$  is constant

From Taylor series expansion:  $f(x^* + \eta) = f(x^*) + f'(x^*)\eta + O(\eta^2)$

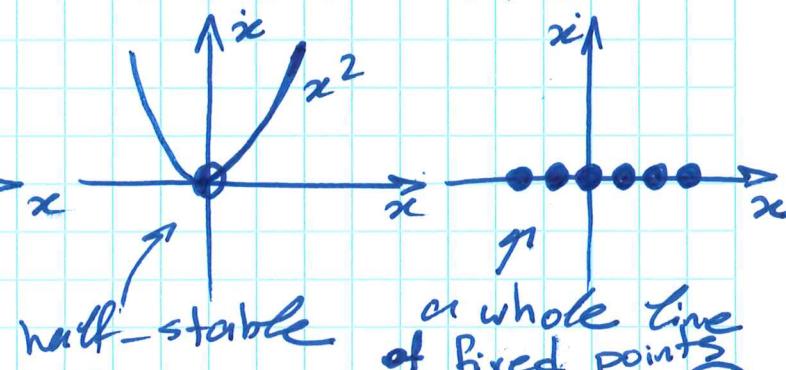
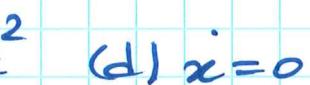
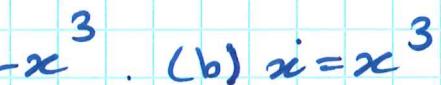
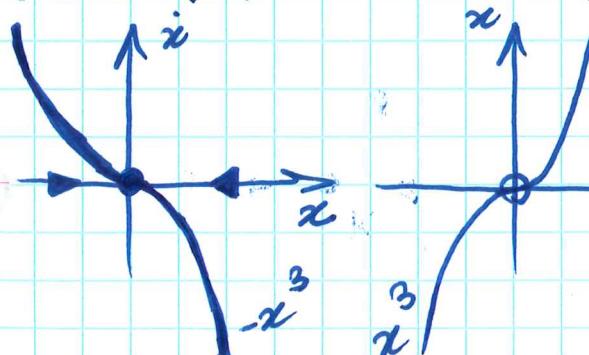
$\Rightarrow \dot{\eta} \approx f'(x^*)\eta \rightarrow \eta(t) = \eta_0 \exp(f'(x^*)t)$

\*  $f'(x^*) < 0 \rightarrow$  decays ;  $f'(x^*) > 0 \rightarrow$  grows  
 (stable) (unstable)

If  $f'(x^*) = 0$ , then  $O(\eta^2)$  is not negligible and a nonlinear analysis is needed. (or via a case-by-case analysis)

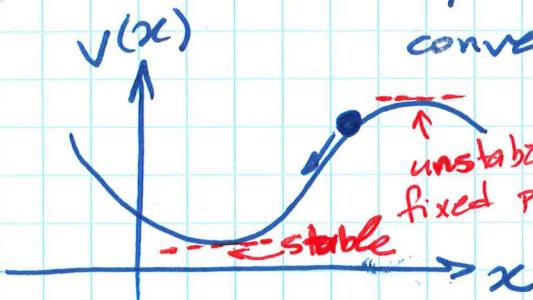
Q: What does the magnitude of  $f'(x^*)$  tell us?

Ex. (a)  $\dot{x} = -x^3$  (b)  $\dot{x} = x^3$  (c)  $\dot{x} = x^2$  (d)  $\dot{x} = 0$



## Potentials

$$\dot{x} = f(x) = -\frac{dV}{dx}$$



convention: particle always move downhill

\* no inertia  $\rightarrow$  impossibility of oscillation  
(topic of a future session)

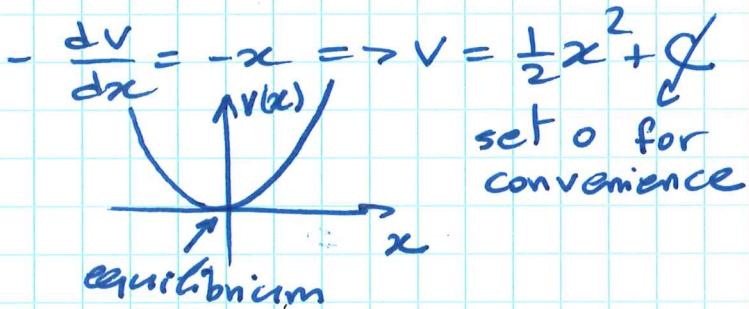
(the only force on the particle is from the potential energy)

see  $x$  as a function of  $t$

$$\rightarrow \frac{dv(x(t))}{dt} = \frac{dV}{dx} \frac{dx}{dt} = -\left(\frac{dV}{dx}\right)^2 \leq 0$$

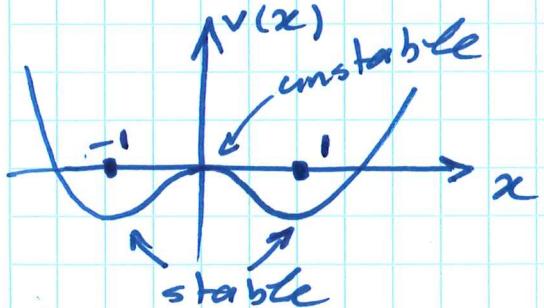
$\Rightarrow v(t)$  decreases along trajectories!

Ex. Graph the potential for the system  $\dot{x} = -x$



(potential is only defined up to an additive constant)

$$\text{Ex. } \dot{x} = x - x^3 \Rightarrow -\frac{dV}{dx} = x - x^3 \Rightarrow V(x) = -\frac{1}{2}x^2 + \frac{1}{4}x^4 + C$$



- double-well potential
- the system is bistable

**311**

# Language Death Laser Threshold

# Language Death

Let X and Y be two languages competing for speakers in a given society.

Assume everybody is monolingual and the population well-mixed

$$\dot{x} = -x P_{XY} + (1-x) P_{YX}$$

$\circ \langle x \rangle_1$ : fraction of the population speaking X

$$1-x : \quad " \quad Y$$

$P_{YX}$ : rate at which individuals switch from Y to X

→ attractiveness of the language X

$$P_{Y|X} = S x^{\alpha} \leftarrow \begin{array}{l} \text{an adjustable} \\ \text{parameter} > 1 \end{array}$$

o<sub>1</sub>SS<sub>1</sub>: perceived status, reflects the social or economic opportunities afforded to the speakers of X

By symmetry:  $P_{XY} = (1-s)(1-x)^{\alpha}$

$$\Rightarrow x' = -x(1-s)(1-x)^\alpha + (1-x)sx^\alpha = f(x)$$

Fixed Points:  $f(x) = 0$

$$\Rightarrow x(1-x) \left[ -(1-s)(1-x)^{\alpha-1} + s x^{\alpha-1} \right] = 0$$

$$\Rightarrow x^* = 0; x^* = \frac{1}{1-\alpha}$$

$$f(x) = (1-x) \left[ -(1-s)(1-x)^{\alpha-1} + sx^{\alpha-1} \right]$$

$$-x \left[ -(1-s)(1-x)^{\alpha-1} + sx^{\alpha-1} \right]$$

$$+ x(1-x) \left[ (\alpha-1)(1-s)(1-x)^{\alpha-2} + (\alpha-1)sx^{\alpha-2} \right]$$

$$x^* = 0 \Rightarrow f'(x^*) = s - 1 < 0 \quad \text{stable}$$

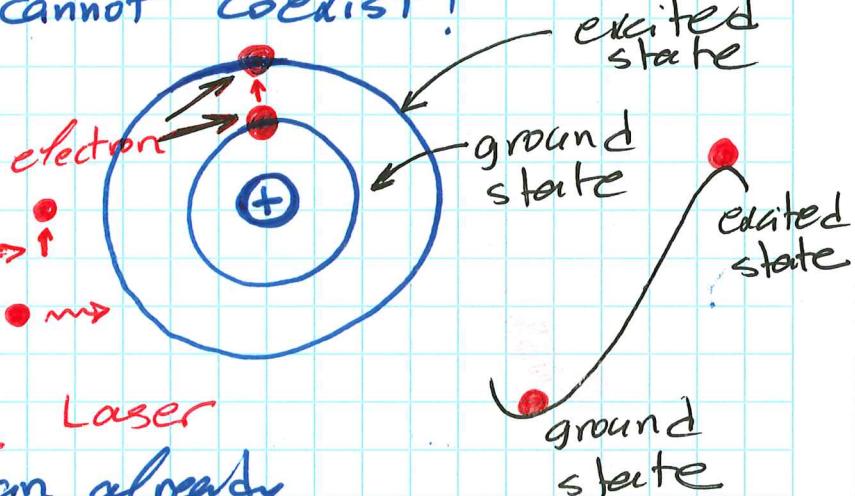
$$x^* = 1 \Rightarrow f'(x^*) = -s < 0 \quad \text{stable}$$

$$x^* = \alpha \Rightarrow f'(x^*) > 0 \quad (\text{check}) \quad \text{unstable}$$

$\Rightarrow$  two languages cannot coexist!



Stimulated Absorption  $\xrightarrow{\text{photon}} \text{electron}$   
Spontaneous Emission  $\text{electron} \xrightarrow{\downarrow} \text{photon}$



stimulated emission  $\xrightarrow{\text{photon}} \text{Laser}$   
or photon disturbs an already excited electron.

$$\dot{n} = G n N - K n$$

↑  
gain coefficient



$n$ : number of photons  
 $N$ : number of excited atoms

$$\text{loss of photon} \rightarrow T = \frac{1}{\text{lifetime } K}$$

Note:  $N$  decreases by the emission of photons

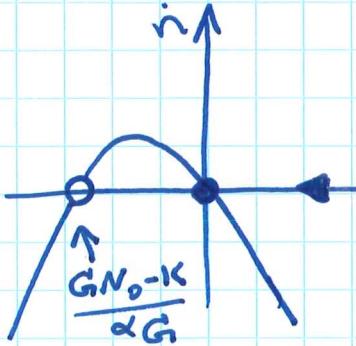
$$\text{Let } N(t) = N_0 - \alpha n$$

$$\Rightarrow \dot{n} = G n (N_0 - \alpha n) - K n$$

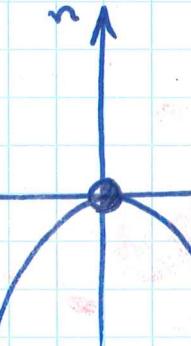
$$\Rightarrow \dot{n} = (G N_0 - K) n - \alpha G n^2$$

↑  
number of excited atoms in the absence of laser action (fixed)

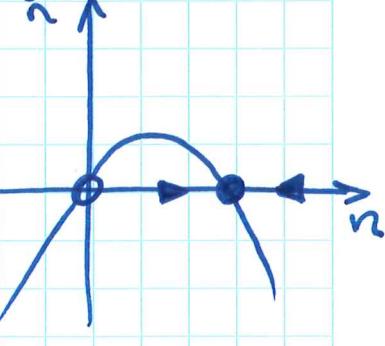
$$GN_0 < K$$



$$GN_0 = K$$

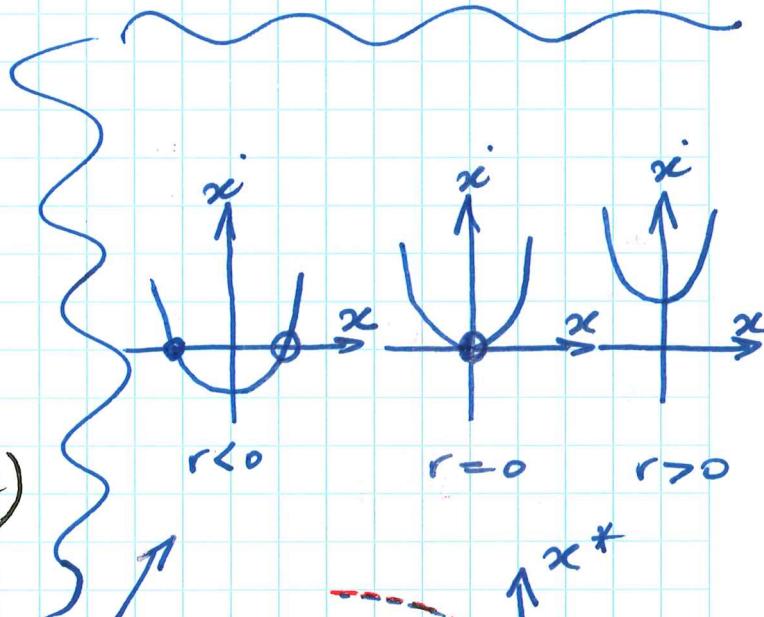
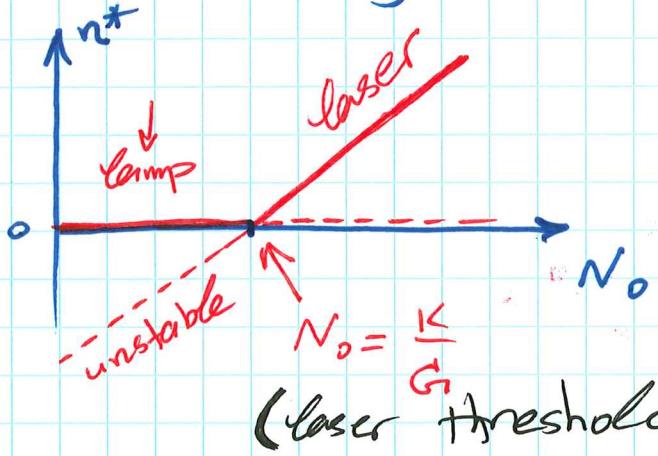


$$GN_0 > K$$



### Transcritical Bifurcation

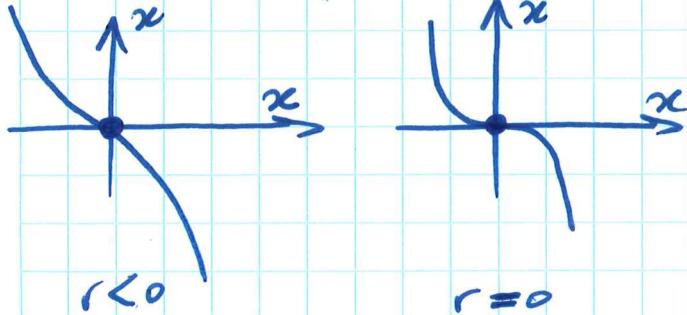
Bifurcation Diagram:



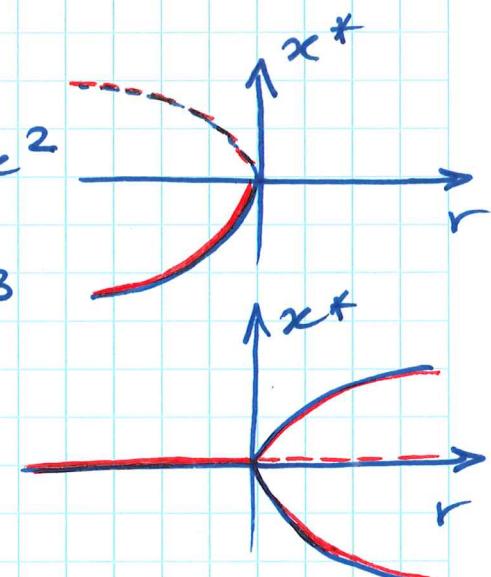
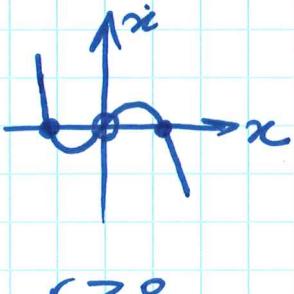
Other Bifurcations

Saddle-node bifurcation:  $\dot{x} = r + x^2$

Pitchfork bifurcation:  $\dot{x} = rx - x^3$



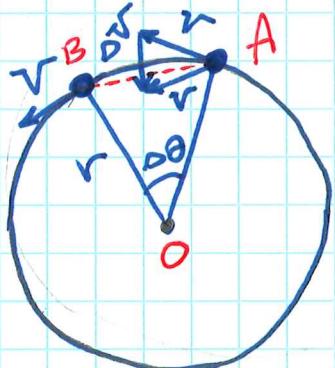
$$\dot{x} = rx - x^3$$



# 312

Over damped Board on a Rotating Hoop

Centrifugal force:



The triangles  $OAB$  and the little triangle are congruent:

$$\frac{\overline{AB}}{r} = \frac{\Delta V}{V}$$

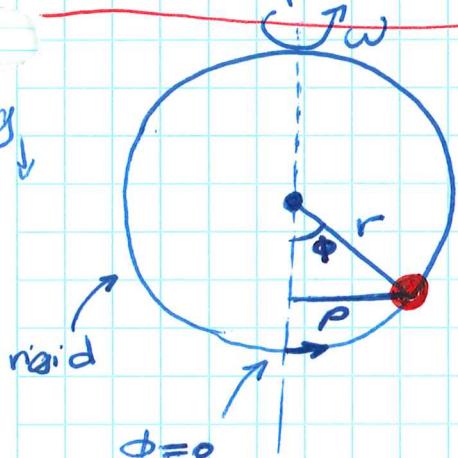
$$\overline{AB} = 2r \sin \frac{\Delta \theta}{2}$$

$\Rightarrow$  for  $\Delta \theta \rightarrow 0 \rightarrow \overline{AB} = r \Delta \theta = v \Delta t$

$$\Rightarrow \frac{v \Delta t}{r} = \frac{\Delta V}{V} \Rightarrow \frac{\Delta V}{\Delta t} = \frac{v^2}{r} \Rightarrow a = \frac{v^2}{r} = r \omega^2$$

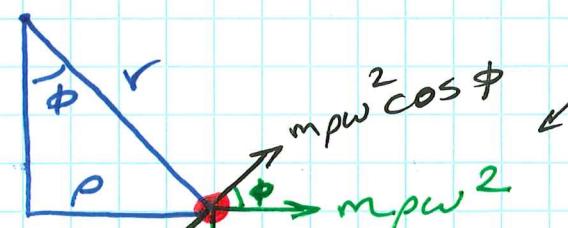
centrifugal acceleration

Over damped board on a rotating hoop



This hoop rotates around the  $z$  (vertical axis)  
 $\phi \in (-\pi, \pi]$

Force balance in the tangential direction:



Note that the rotation occurs around the  $z$  axis.

$$ma = mp\omega^2 \cos \phi - mg \sin \phi$$

$$mr\ddot{\phi} = mp\omega^2 \cos \phi - mg \sin \phi - b\dot{\phi}$$

$$= mr\ddot{\phi} = mr\omega^2 \sin \phi \cos \phi - mg \sin \phi - b\dot{\phi}$$

This force balance is oversimplified!

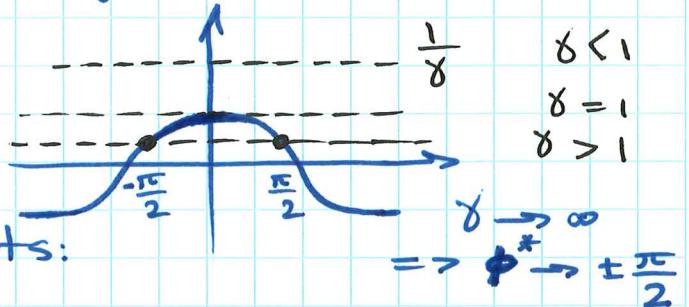
Let  $mr\ddot{\phi} \approx 0$  for now! We will get back to this point later.

$$\Rightarrow b\dot{\phi} = mg \sin \phi \left[ \underbrace{\frac{rw^2}{g} \cos \phi - 1}_{\gamma} \right] = f(\phi)$$

$$f(\phi^*) = 0 \Rightarrow \phi^* = 0 \text{ and } \pi$$

$$\phi^* = \pm \cos^{-1} \frac{1}{\gamma} \quad \text{for } \gamma \geq 1$$

$$[\dots] \Rightarrow \cos \phi = \frac{1}{\gamma}$$

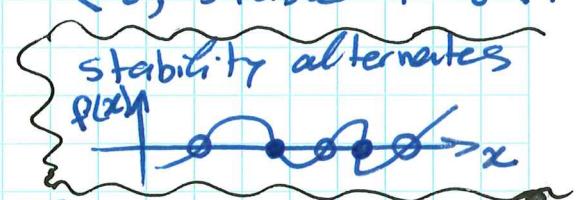
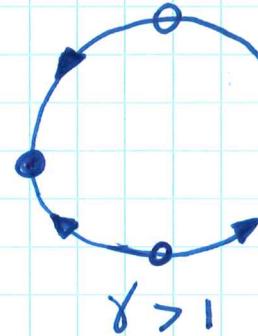
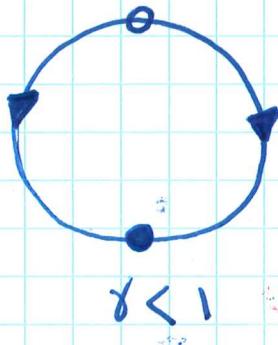


Stability of the fixed points:

$$\frac{df}{d\phi} = mg \cos \phi [\gamma \cos \phi - 1] + mg \sin \phi [-\gamma \sin \phi]$$

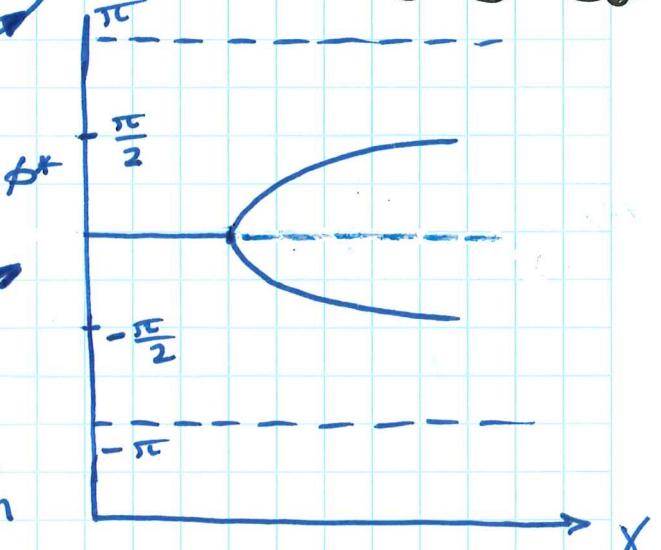
$$\phi^* = \pi \Rightarrow \frac{df(\pi)}{d\phi} = -mg \cdot (-\gamma - 1) = mg(\gamma + 1) > 0$$

$$\phi^* = 0 \Rightarrow \frac{df(0)}{d\phi} = mg(\gamma - 1) \rightarrow \begin{cases} > 0, \text{unstable if } \gamma > 1 \\ < 0, \text{stable if } \gamma < 1 \end{cases}$$



Bifurcation Diagram:

pitchfork bifurcation



Question: when is it valid to neglect the inertial term  $m r \ddot{\phi}$ ?  $m=0$ ? Nope!

It helps to write the equation in dimensionless form  $\rightarrow$  scales, meaning of small, orders

Define a dimensionless time  $\tau = \frac{t}{T}$  / time scale (obvious sometimes)

$$mr \frac{d^2\phi}{dt^2} = mr\omega^2 \sin\phi \cos\phi - mg \sin\phi - b \frac{d\phi}{dt}$$

$$t = T\tau \Rightarrow \frac{mr}{T^2} \frac{d^2\phi}{d\tau^2} = mr\omega^2 \sin\phi \cos\phi - mg \sin\phi - \frac{b}{T} \frac{d\phi}{d\tau}$$

divide by  $mg$ :

$$\frac{r}{gT^2} \frac{d^2\phi}{d\tau^2} = \frac{rw^2}{g} \sin\phi \cos\phi - \sin\phi - \frac{b}{mgT} \frac{d\phi}{d\tau}$$

We want the left hand side to be small compared to the right hand side terms.

We need  $\underbrace{\frac{b}{mgT} \sim O(1)}$  and  $\frac{r}{gT^2} \ll 1$

Let  $T = \frac{b}{mg}$  ( $\tau$  is also useful to get rid of the parameters)

$$\Rightarrow \frac{r}{gT^2} = \frac{rm^2g}{b^2} \underset{\sim}{\ll} 1$$

$\epsilon$  (a dimensionless group)

$$\Rightarrow \epsilon \frac{d^2\phi}{d\tau^2} = \gamma \sin\phi \cos\phi - \sin\phi - \frac{d\phi}{d\tau}$$

for  $\epsilon \ll 1 \rightarrow$  we can neglect the inertia terms.

# 313

Insect Outbreak  
(Ludwig et al. 1978)

→ outbreak of an insect called the spruce budworm

they can defoliate  
and kill most of the  
fir trees in the forest  
in about four years!

a serious pest ↑  
in eastern Canada

Time scales:

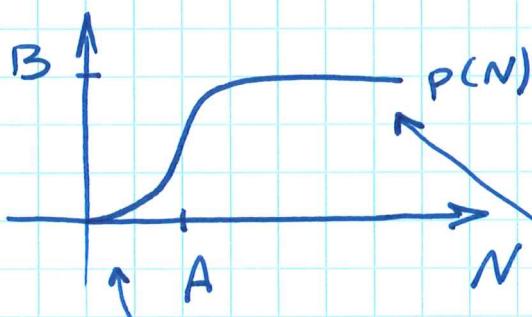
Forest variables can be assumed constant

- budworm population (fast)  
(population can increase five fold in a year) →  $T \approx$  months
- trees population (slow)  
(trees can completely replace their foliage in  $\approx 7-10$  years; their lifespan in the absence of budworm  $\approx 100-150$  years)

Proposed Model

$$\dot{N} = RN \left(1 - \frac{N}{K}\right) - P(N)$$

Logistic term carrying capacity depends on the amount of foliage left on the trees



Qualitative shape of  $P(N)$

no predation when budworms are scarce

(the birds look for food elsewhere)

saturation: the birds are eating as fast as they can!

$$P(N) = \frac{BN^2}{A^2 + N^2} \quad A, B > 0$$

$$\Rightarrow \dot{N} = RN \left(1 - \frac{N}{K}\right) - \frac{BN^2}{A^2 + N^2}$$

**Outbreak**  $\rightarrow$  as parameters drift, the budworm population,  $N$ , suddenly jumps from a low to a high level.

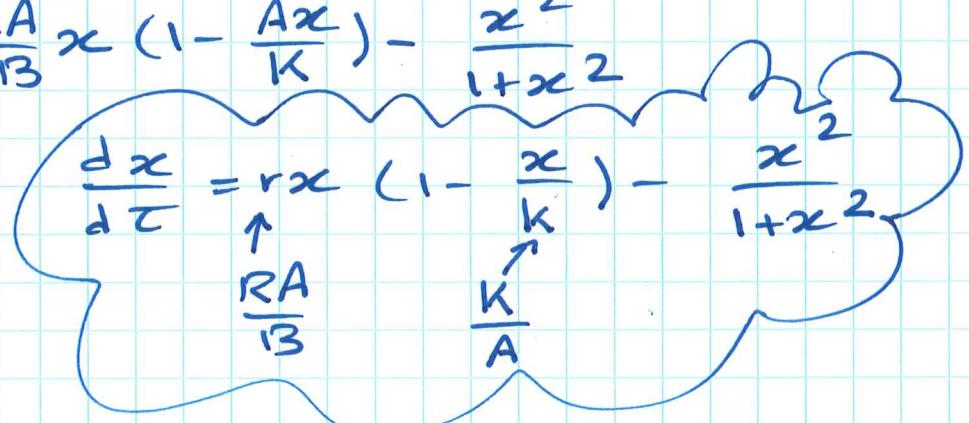
## Dimensionless Form

$$\text{Let } x = \frac{N}{A} \rightarrow N = xA ; \quad \tau = \frac{t}{T} \rightarrow t = \tau T$$

$$\text{Ans} \quad \frac{A}{T} \frac{dx}{dt} = RAx \left(1 - \frac{Ax}{K}\right) - \frac{BA^2x^2}{A^2 + A^2x^2} \quad \text{to be determined}$$

$$\rightarrow \frac{A}{B T} \frac{dx}{dt} = \frac{RA}{B} x \left(1 - \frac{Ax}{K}\right) - \frac{x^2}{1+x^2}$$

$$G_T = \frac{A}{B} \Rightarrow \frac{dx}{dt} = rx \left(1 - \frac{x}{k}\right) - \frac{x^2}{1+x^2}$$

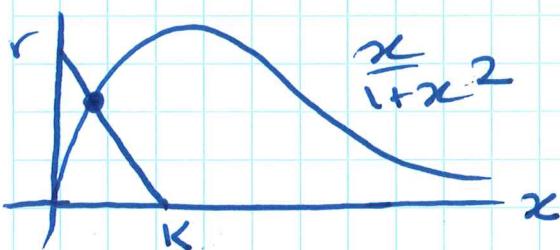


## Fixed Points

$x^t=0 \rightarrow$  it is always unstable

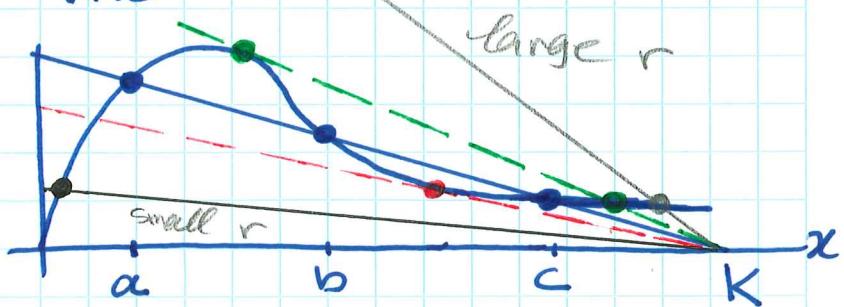
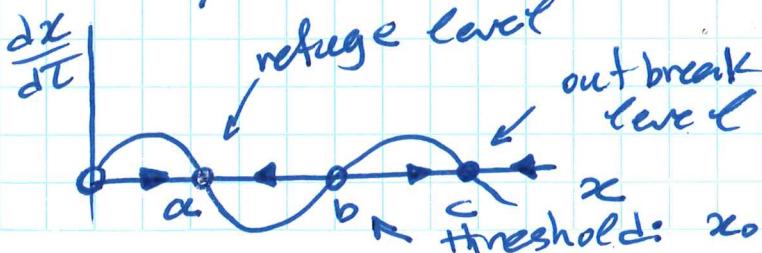
$$\frac{dx}{dt} = 0 \Rightarrow r(1 - \frac{x}{K}) = \frac{x}{1+x^2}$$

↑ *input parameter*



sufficiently small  $K$   
(stable?).

## stability alternates



## Bifurcations:

- b & c coalesce deg r ↓
  - a & b " " " r ↑)

large  $r$  ( $\alpha$  disappears)  
leads to outbreak too

outbreak!

Bifurcation Curves  $\rightarrow$  curves in  $(K, r)$  space where the system undergoes bifurcations.

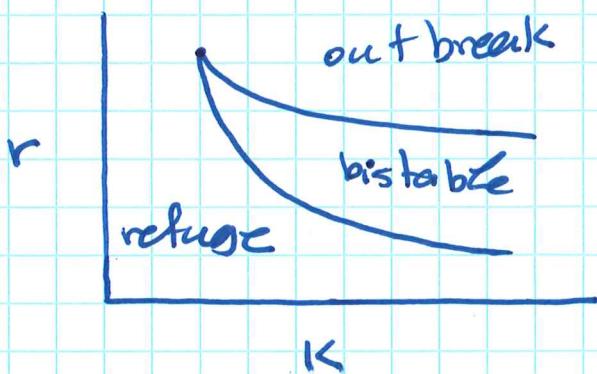
$\rightarrow$  we can't find an explicit formula

Bifurcation occurs when the two curves are tangent to each other (intersect tangentially)

$$\rightarrow r\left(1 - \frac{x}{K}\right) = \frac{x}{1+x^2} \text{ and } \frac{d}{dx}\left[r\left(1 - \frac{x}{K}\right)\right] = \frac{d}{dx}\left[\frac{x}{1+x^2}\right]$$

$$\Rightarrow r = \frac{2x^3}{(1+x^2)^2} \text{ and } K = \frac{2x^3}{x^2-1} \leftarrow x > 1$$

For each  $x > 1$ , we plot  $(K(x), r(x))$  in the  $(K, r)$  plane:



see insect outbreak

Can you find the  $r, K$ , and  $x$  of the cusp point?

# 314

- 2D Flows
- Simple harmonic oscillator

$$A = \begin{bmatrix} a & b \\ c & d \end{bmatrix}$$

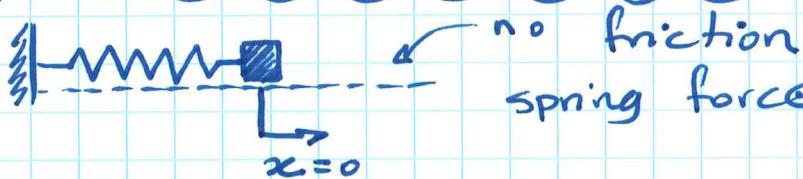
$$\dot{\mathbf{X}} = \begin{bmatrix} x \\ y \end{bmatrix}$$

$$\begin{aligned} \dot{x} &= f(x, y) = ax + by \\ \dot{y} &= g(x, y) = cx + dy \end{aligned} \Rightarrow \dot{\mathbf{X}} = A\mathbf{X}$$

linear: if  $\mathbf{X}_1$  and  $\mathbf{X}_2$  are solutions, then any linear combination  $c_1 \mathbf{X}_1 + c_2 \mathbf{X}_2$  is a solution as well.

Solutions can be visualized as trajectories moving on the  $(x, y)$  plane (phase plane in this context)

## Simple harmonic oscillator



no friction

$$\text{spring force: } -kx = m\ddot{x} + kx = 0$$

Analytical solution? easy! more on that later...

\* We want to develop methods for deducing the behavior of systems like this without actually solving them.

$x$  and  $v = \dot{x}$  determine the state of the system:

$$\text{let } \omega^2 = \frac{k}{m}$$

$$m\ddot{x} = -kx \rightarrow \ddot{x} = -\frac{k}{m}x$$

$$\begin{cases} \dot{v} = -\omega^2 x \\ x = v \end{cases}$$

The system assigns a vector

$(\dot{x}, \dot{v}) = (v, -\omega^2 x)$  at each point  $(x, v)$  → represents a vector field on the phase plane.

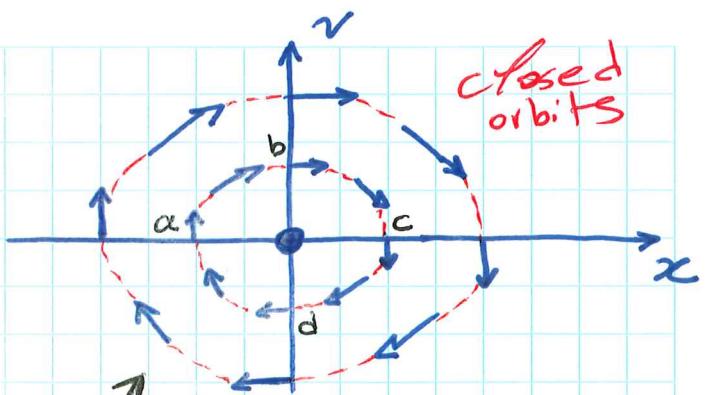
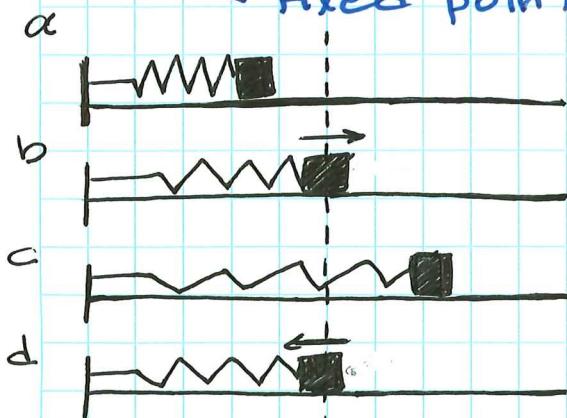
$(\dot{x}, \dot{v})$ : local velocity of the imaginary particle in the phase plane

$$\nu = 0 \rightarrow (\dot{x}, \dot{v}) = (0, -\omega^2 x)$$

$$x = 0 \rightarrow (\dot{x}, \dot{v}) = (\nu, 0)$$

the flow of the imaginary particle swirls about the origin.

fixed point



phase portrait of the system:  
overall picture of the trajectories

\* closed orbits correspond to the periodic motions of the mass.

shape of the closed orbits?

Let's solve it analytically:  $\ddot{x} + \omega^2 x = 0$

guess  $x = e^{at}$   $\Rightarrow a^2 e^{at} + \omega^2 e^{at} = 0 \rightarrow a = \pm i\omega$

$$\Rightarrow x = A e^{i\omega t} + B e^{-i\omega t} = A' \cos \omega t + B' \sin \omega t = C \cos(\omega t - \phi)$$

$$\Rightarrow x = C \cos(\omega t - \phi) \Rightarrow v = \dot{x} = -C\omega \sin(\omega t - \phi)$$

$$\begin{cases} \omega x = C\omega \cos(\omega t - \phi) \\ v = -C\omega \sin(\omega t - \phi) \end{cases} \Rightarrow \begin{cases} \omega^2 x^2 + v^2 = C^2 \omega^2 [\cos^2(\omega t - \phi) + \sin^2(\omega t - \phi)] \\ \omega^2 x^2 + v^2 = K^2 \end{cases}$$

ellipses

Example:  $\dot{x} = \alpha x$   
 $\dot{y} = -y$   $\rightarrow$  Graph the phase portrait as  $\alpha$  varies from  $-\infty$  to  $\infty$ , showing the qualitatively different cases.

$\rightarrow x = x_0 e^{\alpha t}$

$$y = y_0 e^{-t}$$

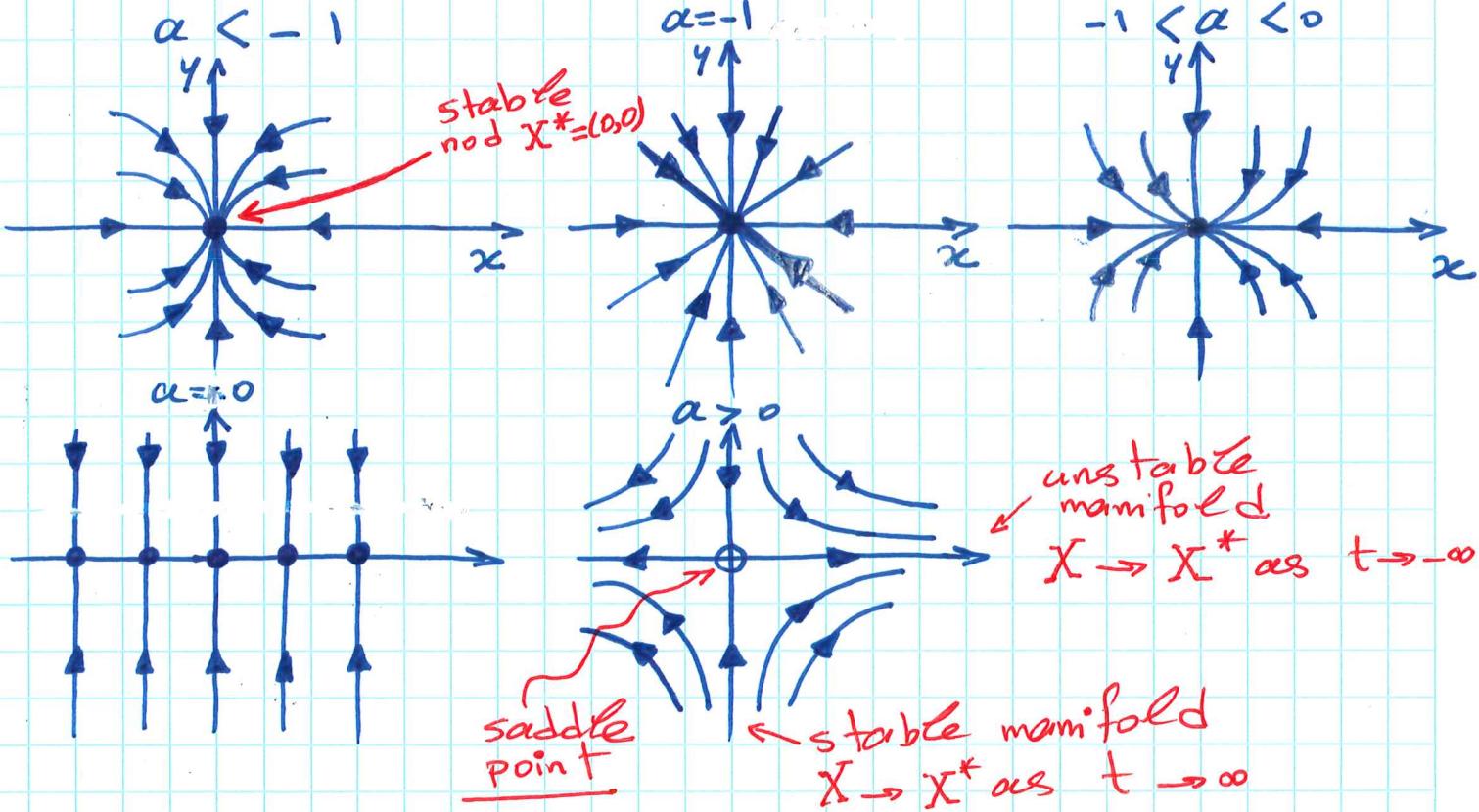
$$\rightarrow \frac{dy}{dx} = -\frac{y_0}{\alpha x_0} e^{(-\alpha-1)t}$$

$\star \alpha < 0 \rightarrow$  as  $t \rightarrow \infty$   
 $\Rightarrow x, y \rightarrow 0$

$\star \alpha = 0 \rightarrow x$  does not change

stable node

$\star \alpha > 0 \rightarrow x$  increases exponentially



# 315

Classification of 2D Linear systems  
Love affairs

\*  $\dot{X} = AX$  with  $A = \begin{bmatrix} a & b \\ c & d \end{bmatrix}$ ,  $X = \begin{bmatrix} x \\ y \end{bmatrix}$

straight-line trajectories are determined by the eigenvectors of the matrix A.

eigen solutions  $X(t) = e^{\lambda t} V$

eigenvalue eigenvector  
(constant)

Insert into the eqn \*:

$$\cancel{\lambda e^{\lambda t} V} = A e^{\lambda t} V \Rightarrow \boxed{AV = \lambda V} \rightarrow (A - \lambda I)V = 0$$

$$\Rightarrow \det(A - \lambda I) = 0$$

$$\Rightarrow \det \begin{bmatrix} a-\lambda & b \\ c & d-\lambda \end{bmatrix} = 0 \rightarrow \lambda^2 - (a+d)\lambda + ad - bc = 0 \rightarrow \text{roots are } \lambda_1 \text{ and } \lambda_2$$

$$\begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}$$

Our focus  $\rightarrow$  typical situation  $\lambda_1 \neq \lambda_2$

Find  $V_1$  and  $V_2$  from  $\lambda_1$  and  $\lambda_2$ :

\*  $\begin{bmatrix} a-\lambda_1 & b \\ c & d-\lambda_1 \end{bmatrix} \begin{bmatrix} \alpha_1 \\ \beta_1 \end{bmatrix} = 0 \rightarrow \alpha_1 = ? \quad \beta_1 = ? \Rightarrow V_1 = \begin{bmatrix} \alpha_1 \\ \beta_1 \end{bmatrix}$

$$\begin{bmatrix} a-\lambda_2 & b \\ c & d-\lambda_2 \end{bmatrix} \begin{bmatrix} \alpha_2 \\ \beta_2 \end{bmatrix} = 0 \rightarrow \alpha_2 = ? \quad \beta_2 = ? \Rightarrow V_2 = \begin{bmatrix} \alpha_2 \\ \beta_2 \end{bmatrix}$$

$$\Rightarrow X(t) = c_1 e^{\lambda_1 t} V_1 + c_2 e^{\lambda_2 t} V_2$$

To sketch the phase portrait

1) Find  $\lambda_1$  and  $\lambda_2$

2) Find the corresponding eigenvectors  $V_1$  and  $V_2$

3) Draw straight lines  $V_1$  and  $V_2$  on the phase plane

4) Direction of flow is determined by the sign of  $\lambda$

5) Draw (qualitatively) the other trajectories

\*

4-2

# Love Affairs

(Strogatz 1988)

$R(t)$ : Romeo's love/hate for Juliet at time  $t$   
 $J(t)$ : Juliet's " Romeo " " "

→ For two identically cautious lovers:

$$\begin{aligned} \dot{R} &= \alpha R + b J \\ \dot{J} &= b R + \alpha J \end{aligned}$$

$\alpha < 0$ : measure of cautiousness  
 $b > 0$ : " responsiveness

Sketch the phase portrait and interpret the results.

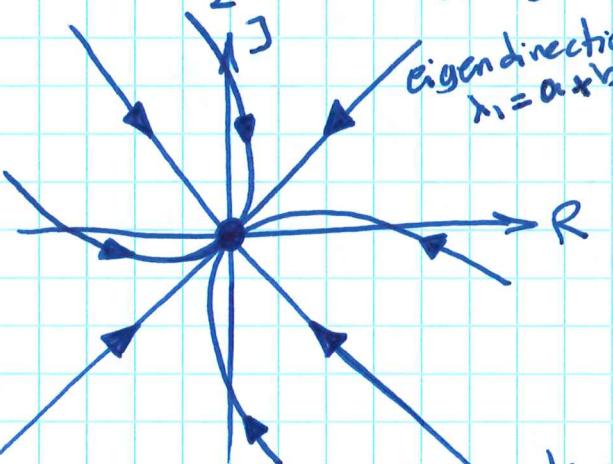
$$A = \begin{bmatrix} \alpha & b \\ b & \alpha \end{bmatrix} \rightarrow \det\left(\begin{bmatrix} \alpha - \lambda & b \\ b & \alpha - \lambda \end{bmatrix}\right) = 0 \Rightarrow (\alpha - \lambda)^2 - b^2 = 0$$
 $\Rightarrow \lambda_1 = \alpha + b, \lambda_2 = \alpha - b$

$$\begin{bmatrix} \alpha - \lambda & b \\ b & \alpha - \lambda \end{bmatrix} \begin{bmatrix} x \\ y \end{bmatrix} = 0 \Rightarrow \begin{cases} (\alpha - \lambda)x + by = 0 \\ bx + (\alpha - \lambda)y = 0 \end{cases}$$

$$\lambda = \lambda_1 = \alpha + b \Rightarrow \begin{cases} -bx + by = 0 \\ bx - by = 0 \end{cases} \rightarrow x = 1, y = 1 \Rightarrow v_1 = \begin{bmatrix} 1 \\ 1 \end{bmatrix}$$

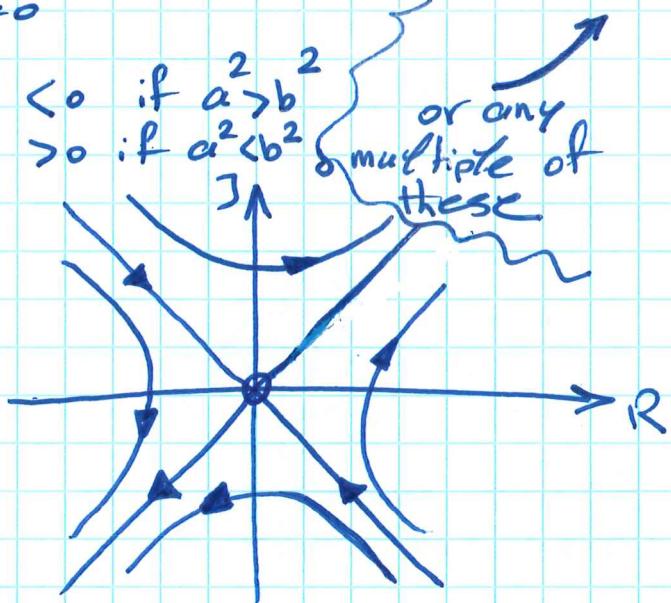
$$\lambda = \lambda_2 = \alpha - b \Rightarrow \begin{cases} bx + by = 0 \\ bx + by = 0 \end{cases} \rightarrow x = 1, y = -1 \Rightarrow v_2 = \begin{bmatrix} 1 \\ -1 \end{bmatrix}$$

Note:  $\lambda_2 = \alpha - b < 0$ ;  $\lambda_1 = \alpha + b < 0$  if  $\alpha^2 > b^2$



$$\alpha^2 > b^2$$

$$|\alpha - b| > |\alpha + b|$$



$$\alpha^2 < b^2$$

$\alpha^2 > b^2$ : the relationship fuzzes out to mutual indifference

$\alpha^2 < b^2$ : love fest or war!

→ Juliet is a fickle lover  
Romeo tends to echo Juliet

↳ he warms up when she loves her and grows cold when she hates him.

the more Romeo loves her, the more Juliet wants to run away!

$$\text{mrs } \begin{cases} \dot{R} = \alpha \\ \dot{j} = -bR \end{cases} \Rightarrow A = \begin{bmatrix} 0 & \alpha \\ -b & 0 \end{bmatrix} \rightarrow \lambda = \pm i\sqrt{\alpha b}$$

$$\lambda_1 = i\sqrt{\alpha b} \Rightarrow v_1 = \begin{bmatrix} -i\sqrt{\frac{\alpha}{b}} \\ 1 \end{bmatrix}$$

$$\lambda_2 = -i\sqrt{\alpha b} \Rightarrow v_2 = \begin{bmatrix} i\sqrt{\frac{\alpha}{b}} \\ 1 \end{bmatrix}$$

$$\text{mrs } X = c_1 e^{i\sqrt{\alpha b}t} \begin{bmatrix} -i\sqrt{\frac{\alpha}{b}} \\ 1 \end{bmatrix} + c_2 e^{-i\sqrt{\alpha b}t} \begin{bmatrix} i\sqrt{\frac{\alpha}{b}} \\ 1 \end{bmatrix}$$

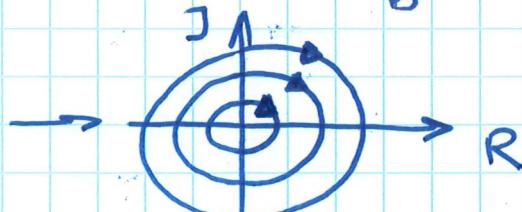
$$\Rightarrow R = -i\sqrt{\frac{\alpha}{b}} c_1 e^{i\sqrt{\alpha b}t} + i\sqrt{\frac{\alpha}{b}} c_2 e^{-i\sqrt{\alpha b}t}$$

$$i\sqrt{\frac{\alpha}{b}}] = i\sqrt{\frac{\alpha}{b}} c_1 e^{i\sqrt{\alpha b}t} + i\sqrt{\frac{\alpha}{b}} c_2 e^{-i\sqrt{\alpha b}t}$$

$$\Rightarrow R^2 = -\frac{\alpha}{b} c_1^2 e^{2i\sqrt{\alpha b}t} - \frac{\alpha}{b} c_2^2 e^{-2i\sqrt{\alpha b}t} + 2 \frac{\alpha}{b} c_1 c_2$$

$$-\frac{\alpha}{b} c_1^2] = -\frac{\alpha}{b} c_1^2 e^{2i\sqrt{\alpha b}t} - \frac{\alpha}{b} c_2^2 e^{-2i\sqrt{\alpha b}t} - 2 \frac{\alpha}{b} c_1 c_2$$

$$\Rightarrow R^2 + \frac{\alpha}{b} c_1^2 = 4 \frac{\alpha}{b} c_1 c_2$$



a never-lasting cycle of love and hate!

Question: what if  $\lambda_{1,2} = \alpha \pm iw$ ?

# S16

- Perturbation solution
- Projectile
- Weakly damped linear oscillator

Projectile:  $mv = -mg - \delta v^3$

$$\text{Let } \tilde{v} = \frac{v}{v_0}, \tilde{t} = \frac{t}{\tau}$$

$$\Rightarrow \frac{m v_0}{\tau} \frac{d\tilde{v}}{d\tilde{t}} = -mg - \delta v_0^3 \tilde{v}^3 \Rightarrow \frac{v_0}{g\tau} \frac{d\tilde{v}}{d\tilde{t}} = -1 - \frac{\delta v_0^3}{mg} \tilde{v}^3$$

$$\text{Let } \tau = \frac{v_0}{g} \Rightarrow \frac{d\tilde{v}}{d\tilde{t}} = -1 - \epsilon \tilde{v}^3 \quad \text{with } \tilde{t} = \frac{t g}{v_0}, \tilde{v} = \frac{v}{v_0}$$

For very small  $\epsilon$  values ( $\epsilon \ll 1$ ), we seek solutions in the form of a power series in  $\epsilon$ :

$$v(t) = \underbrace{\epsilon^0 v^{(0)}(t) + \epsilon^1 v^{(1)}(t) + \epsilon^2 v^{(2)}(t) + \dots}_{\text{first-order perturbation}} + \dots \quad (\text{dropped } \epsilon \text{ sign for simplicity})$$

Substitute into the eqn and conditions and equate the coefficients of each power of  $\epsilon$  to zero separately.  
(Equate the terms with common power of  $\epsilon$ )

$$\frac{d}{dt} (\epsilon^0 v^{(0)} + \epsilon^1 v^{(1)}) = -1 - \epsilon (\epsilon^0 v^{(0)} + \epsilon^1 v^{(1)})^3$$

$$\text{Now } \frac{d v^{(0)}}{d t} + \epsilon \frac{d v^{(1)}}{d t} = -1 - \epsilon [v^{(0)}^3 + 3v^{(0)}^2 \epsilon v^{(1)} + 3v^{(0)} \epsilon^2 v^{(1)}^2 + \epsilon^3 v^{(1)}^3] \\ = -1 - \epsilon v^{(0)}^3 - 3\epsilon^2 v^{(0)} v^{(1)} - 3\epsilon^3 v^{(0)} v^{(1)}^2 - \epsilon^4 v^{(1)}^3$$

$$\Rightarrow \frac{d v^{(0)}}{d t} + \epsilon \frac{d v^{(1)}}{d t} = -1 - \epsilon v^{(0)}^3 + O(\epsilon^2)$$

$$\Rightarrow \left[ \frac{d v^{(0)}}{d t} + 1 \right] + \epsilon \left[ \frac{d v^{(1)}}{d t} + v^{(0)}^3 \right] + O(\epsilon^2) = 0$$

$$\text{Initial conditions: } \epsilon^0 v^{(0)} + \epsilon^1 v^{(1)} = 1 \Rightarrow [v^{(0)} - 1] + \epsilon v^{(1)} = 0$$

zeroth-order  $\frac{dv^{(0)}}{dt} = -1 ; v^{(0)}(0) = 1$

$$\rightarrow v^{(0)} = -t + 1$$

first-order  $\frac{dv^{(1)}}{dt} = -v^{(0)^3} = -(1-t)^3 ; v^{(1)}(0) = 0$

$$C = -\frac{1}{4}$$

$$\rightarrow v^{(1)} = \frac{1}{4}(t-1)^4 + C \rightarrow v^{(1)} = \frac{1}{4}[(t-1)^4 - 1]$$

$$\Rightarrow v(t) = 1-t + \frac{\epsilon}{4}[(t-1)^4 - 1] + O(\epsilon^2)$$

see "perturbation\_projective.py"

Higher orders? Why not? It is like a domino!

weakly damped linear oscillator

$$\ddot{x} + 2\epsilon\dot{x} + x = 0 ; x(0) = 0 ; \dot{x}(0) = 1$$

Analytical solution:  $r^2 + 2\epsilon r + 1 = 0 \Rightarrow r = -\epsilon \pm i\sqrt{1-\epsilon^2}$

$$\Rightarrow x = e^{-\epsilon t} [A \cos \sqrt{1-\epsilon^2} t + B \sin \sqrt{1-\epsilon^2} t]$$

$$x(0) = 0 \Rightarrow A = 0 ; \dot{x}(0) = 1 \Rightarrow -\epsilon e^{-\epsilon t} B \sin \sqrt{1-\epsilon^2} t + \sqrt{1-\epsilon^2} e^{-\epsilon t} B \cos \sqrt{1-\epsilon^2} t = 1 \text{ at } 0$$

$$\Rightarrow \sqrt{1-\epsilon^2} B = 1 \Rightarrow B = \frac{1}{\sqrt{1-\epsilon^2}}$$

$$\Rightarrow x = \frac{e^{-\epsilon t}}{\sqrt{1-\epsilon^2}} \sin \sqrt{1-\epsilon^2} t$$

Let  $x = x^{(0)} + \epsilon x^{(1)} + O(\epsilon^2)$

$$\rightarrow \ddot{x}^{(0)} + \epsilon \ddot{x}^{(1)} + 2\epsilon(\dot{x}^{(0)} + \epsilon \dot{x}^{(1)}) + x^{(0)} + \epsilon x^{(1)} = 0$$

$$\rightarrow [\ddot{x}^{(0)} + x^{(0)}] + \epsilon [\ddot{x}^{(1)} + 2\dot{x}^{(0)} + x^{(1)}] + O(\epsilon^2) = 0$$

initial conditions:  $x^{(0)}(0) + \epsilon x^{(1)}(0) = 0$   
 $\dot{x}^{(0)}(0) + \epsilon \dot{x}^{(1)}(0) = 1$

zeroth-order  $\ddot{x}^{(0)} + x^{(0)} = 0 ; \quad x^{(0)}(0) = 0 ; \quad \dot{x}^{(0)}(0) = 1$

$r^2 + 1 = 0 \Rightarrow r = \pm i \Rightarrow x^{(0)} = A \cos t + B \sin t \Rightarrow x^{(0)} = \sin t$

first-order  $\ddot{x}^{(1)} + 2\dot{x}^{(0)} + x^{(1)} = 0 ; \quad x^{(1)}(0) = 0 ; \quad \dot{x}^{(1)}(0) = 0$

$$\Rightarrow \ddot{x}^{(1)} + x^{(1)} = -2 \cos t \rightarrow x^{(1)} = -t \sin t$$

$$\Rightarrow x = \sin t - \epsilon t \sin t + O(\epsilon^2)$$

grows with time  
without bound!

see "perturbation-damped.py"

# 317

## Two-timing

ODE:  $\ddot{x} + 2\epsilon \dot{x} + x = 0$

$$\text{analytical: } x = \frac{e^{-\epsilon t}}{\sqrt{1-\epsilon^2}} \sin(\sqrt{1-\epsilon^2}t)$$

\* the true solution exhibits two time scales:

- fast  $O(1)$  for the oscillation
- slow  $O(\frac{1}{\epsilon})$  over which the amplitude decays

$\uparrow$   
kicks in  
at large  
times

Our perturbation solution  
misrepresents the slow  
time scale behavior

$$x = \sin t - \epsilon t \sin t$$

## Two-timing

$$\begin{array}{ll} \tau = t & \text{fast time} \\ T = \epsilon t & \text{slow time} \end{array}$$

Note: functions of  $T$  (slow time) can be regarded as constant on the fast time scale, e.g., your height is constant on the time scale of a day

$$x(t) = x^{(0)}(\tau, T) + \epsilon x^{(1)}(\tau, T) + O(\epsilon^2)$$

chain rule  $\frac{dx}{dt} = \frac{\partial x}{\partial \tau} \frac{\partial \tau}{\partial t} + \frac{\partial x}{\partial T} \frac{\partial T}{\partial t} = \frac{\partial x}{\partial \tau} + \epsilon \frac{\partial x}{\partial T}$

$$\Rightarrow \frac{dx}{dt} = \frac{\partial x^{(0)}}{\partial \tau} + \epsilon \frac{\partial x^{(1)}}{\partial \tau} + \epsilon \frac{\partial x^{(0)}}{\partial T} + \epsilon^2 \frac{\partial x^{(1)}}{\partial T}$$

$$\Rightarrow \frac{dx}{dt} = \frac{\partial x^{(0)}}{\partial \tau} + \epsilon \left( \frac{\partial x^{(1)}}{\partial \tau} + \frac{\partial x^{(0)}}{\partial T} \right) + O(\epsilon^2)$$

$$\frac{d^2 x}{dt^2} = \frac{\partial^2 x^{(0)}}{\partial \tau^2} + \epsilon \left( \frac{\partial^2 x^{(1)}}{\partial \tau^2} + \frac{\partial^2 x^{(0)}}{\partial \tau \partial T} \right)$$

$$+ \epsilon \left[ \frac{\partial^2 x^{(0)}}{\partial \tau \partial T} + \epsilon \left( \frac{\partial^2 x^{(1)}}{\partial \tau \partial T} + \frac{\partial^2 x^{(0)}}{\partial T^2} \right) \right] + O(\epsilon^2)$$

$$\Rightarrow \frac{d^2 x}{dt^2} = \frac{\partial^2 x^{(0)}}{\partial \tau^2} + \epsilon \left( \frac{\partial^2 x^{(1)}}{\partial \tau^2} + 2 \frac{\partial^2 x^{(0)}}{\partial \tau \partial T} \right) + O(\epsilon^2)$$

\*\*

(48)

\* & \*\* → ODE:

$$\frac{\partial^2 x^{(0)}}{\partial T^2} + \varepsilon \left( \frac{\partial^2 x^{(1)}}{\partial T^2} + 2 \frac{\partial^2 x^{(0)}}{\partial T \partial T} \right) + 2\varepsilon \left( \frac{\partial x^{(0)}}{\partial T} + \varepsilon \left( \frac{\partial x^{(1)}}{\partial T} + \frac{\partial x^{(0)}}{\partial T} \right) \right) + x^{(0)} + \varepsilon x^{(1)} = 0$$

functions of  $T$  I

$$O(\varepsilon^0): \frac{\partial^2 x^{(0)}}{\partial T^2} + x^{(0)} = 0 \Rightarrow x^{(0)} = A \sin T + B \cos T$$

$$O(\varepsilon^1): \frac{\partial^2 x^{(1)}}{\partial T^2} + 2 \left( \frac{\partial^2 x^{(0)}}{\partial T \partial T} + \frac{\partial x^{(0)}}{\partial T} \right) + x^{(1)} = 0$$

$$\Rightarrow \frac{\partial^2 x^{(1)}}{\partial T^2} + x^{(1)} = -2 \frac{\partial}{\partial T} \left[ \frac{\partial x^{(0)}}{\partial T} + x^{(0)} \right]$$

$$= -2 \frac{\partial}{\partial T} [A' \sin T + B' \cos T + A \sin T + B \cos T]$$

$$\Rightarrow \frac{\partial^2 x^{(1)}}{\partial T^2} + x^{(1)} = -2(A' + A) \cos T + 2(B' + B) \sin T$$

As it is, the equation leads to the same problem we had because the RHS is a "resonant forcing" → solutions of the form  $T \sin T$  and  $T \cos T$

Unless  $\begin{cases} A' + A = 0 \\ B' + B = 0 \end{cases}$  }  $\Rightarrow A = A(0) e^{-T}$   
 $B = B(0) e^{-T}$   $x^{(1)} = \alpha \sin T + b \cos T$  II

Initial conditions:  $x(0) = 0, \dot{x}(0) = 1$

$$x(t) = x^{(0)}(t, T) + \varepsilon x^{(1)}(t, T)$$

$$\Rightarrow x(0) = 0 = x^{(0)}(0, 0) + \varepsilon x^{(1)}(0, 0) \Rightarrow x^{(0)}(0, 0) = 0 \quad ①$$

$$\dot{x}(t) = \frac{\partial x^{(0)}(t, T)}{\partial T} + \varepsilon \left( \frac{\partial x^{(1)}(t, T)}{\partial T} + \frac{\partial x^{(0)}(t, T)}{\partial T} \right) \quad x^{(1)}(0, 0) = 0 \quad ②$$

$$\Rightarrow \dot{x}(0) = 1 = \frac{\partial x^{(0)}(0, 0)}{\partial T} + \varepsilon \left( \frac{\partial x^{(1)}(0, 0)}{\partial T} + \frac{\partial x^{(0)}(0, 0)}{\partial T} \right)$$

$$\Rightarrow \underbrace{\frac{\partial x^{(0)}(0, 0)}{\partial T}}_{\text{③}} = 1, \quad \underbrace{\frac{\partial x^{(1)}(0, 0)}{\partial T} + \frac{\partial x^{(0)}(0, 0)}{\partial T}}_{\text{④}} = 0$$

I ①:  $0 = A(0) \sin 0 + B(0) \cos 0 \Rightarrow B(0) = 0 \Rightarrow B = 0$   
 ③:  $1 = A(0) \cos 0 \Rightarrow A(0) = 1 \Rightarrow A = e^{-T}$

③ ②:  $0 = \alpha \sin \omega + b \cos \omega \Rightarrow b = 0$

④:  $\alpha \cos \omega - e^{-\varepsilon t} \sin \omega \Rightarrow \alpha = 0$

$$\frac{\partial x^{(1)}(\omega, 0)}{\partial \omega}$$

$$\frac{\partial x^{(0)}(\omega, 0)}{\partial \omega}$$

$$\Rightarrow x = e^{-\varepsilon t} \sin t$$

$$vs \frac{e^{-\varepsilon t}}{\sqrt{1-\varepsilon^2}} \sin(\sqrt{1-\varepsilon^2}t)$$

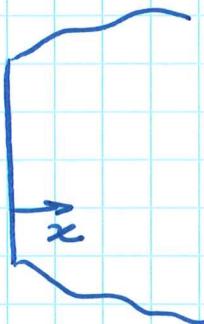
see "perturbation\_damped.py"

with twoTiming = True

# 318

- semi-infinite regions
- Combination of variables
- Stefan problem

Heating of a semi-infinite slab



$$x \in [0, \infty)$$

$$T(x, 0) = T_0$$

$$T(0, t) = T_w$$

$$T(x, t) \quad \text{for } x \rightarrow \infty = T_0$$

$$\text{Find } T(x, t)$$

Assume that the domain goes to infinity in all directions except the one at  $x=0$   $\rightarrow$  like a thick, tall, wide, wall!  $\rightarrow$  one-dimensional heat eqn:

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2} \rightarrow T = T(x, t, \alpha)$$

$$\text{Let } \Theta = \frac{T - T_0}{T_w - T_0} \rightarrow \frac{\partial \Theta}{\partial t} = \alpha \frac{\partial^2 \Theta}{\partial x^2} \rightarrow \Theta = \Theta(\eta)$$

dimensions  
combination  
of the  
quantities

$$[x] \doteq \text{length} \quad [t] \doteq \text{time} \quad [\alpha] = \frac{\text{length}}{\text{time}}^2$$

$$\Rightarrow \eta = \frac{cx}{\sqrt{\alpha t}} \quad \begin{array}{l} \text{some number} \\ \text{(will be chosen in such way} \\ \text{to simplify the equations)} \end{array}$$

$$\text{Chain rule: } \frac{\partial \Theta}{\partial t} = \frac{\partial \Theta}{\partial \eta} \frac{\partial \eta}{\partial t} = \frac{\partial \Theta}{\partial \eta} \left( -\frac{1}{2} \frac{cx}{\sqrt{\alpha t}} t^{-3/2} \right)$$

$$\frac{\partial \Theta}{\partial x} = \frac{\partial \Theta}{\partial \eta} \frac{\partial \eta}{\partial x} = \frac{\partial \Theta}{\partial \eta} \frac{c}{\sqrt{\alpha t}}$$

$$\frac{\partial^2 \Theta}{\partial x^2} = \frac{\partial}{\partial \eta} \left( \frac{\partial \Theta}{\partial \eta} \frac{c}{\sqrt{\alpha t}} \right) \frac{\partial \eta}{\partial x} = \frac{\partial^2 \Theta}{\partial \eta^2} \frac{c^2}{\alpha t}$$

$$\Rightarrow -\frac{1}{2} \frac{cx}{\sqrt{\alpha t}} t^{-3/2} \frac{d\Theta}{d\eta} = \frac{c^2}{\alpha t} \frac{d^2 \Theta}{d\eta^2}$$

$$\frac{d^2\theta}{dn^2} + \frac{1}{2c} \frac{x}{\sqrt{at}} \frac{d\theta}{dn} = 0$$

$$\hookrightarrow \text{take } c^2 = \frac{1}{4} \Rightarrow c = \frac{1}{\sqrt{4}}$$

$$\Rightarrow \frac{d^2\theta}{dn^2} + 2n \frac{d\theta}{dn} = 0, \quad n = \frac{x}{\sqrt{4at}}, \quad \text{at } n = \infty \Rightarrow \theta = 0 \\ \text{at } n = 0 \Rightarrow \theta = 1$$

$$\text{To solve, let } \psi = \frac{d\theta}{dn} \Rightarrow \frac{d\psi}{dn} + 2n\psi = 0$$

$$\Rightarrow \frac{d\psi}{\psi} = -2n dn \Rightarrow \psi = C_1 e^{-n^2}$$

$$\Rightarrow \frac{d\theta}{dn} = C_1 e^{-n^2} \Rightarrow d\theta = C_1 e^{-n^2} dn$$

$$\frac{T-T_0}{T_w-T_0}$$

$$\Rightarrow \theta = C_1 \int_0^n e^{-\bar{n}^2} d\bar{n} + C_2 = C_3 \operatorname{erf}(n) + C_2$$

$$n=0 \Rightarrow \theta=1 \Rightarrow \boxed{C_2=1}$$

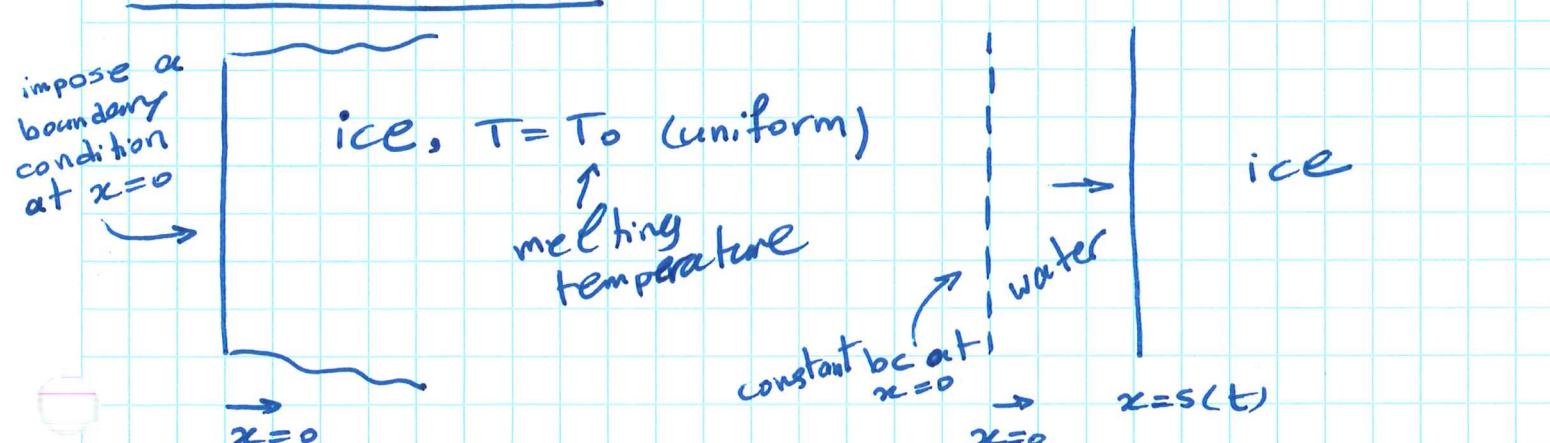
$$n=\infty \Rightarrow \theta=0 \Rightarrow 0 = C_3 + 1 \Rightarrow \boxed{C_3 = -1}$$

$\operatorname{erf}(\infty) = 1$  (Can you prove this?)

$$\Rightarrow \theta = 1 - \operatorname{erf}(n) = 1 - \operatorname{erf}\left(\frac{x}{\sqrt{4at}}\right)$$

see "semi-infinite" for a demonstration

### Stefan Problem



Question: find the temp distribution in water and  $s$  as a function of time

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2} \quad (1) \quad x \in [0, s(t)]$$

$T = T_w$  at  $x=0$  &  $T = T_0$  at  $x=s(t)$

the melting process:

the heat conducted to the interface balances with the heat required to melt the ice (latent heat)

↗ no temperature change

this is why winds make you

feel cooler: evaporation from the skin removes heat

$$\Rightarrow -K \frac{dT(s(t))}{dx} A = q \rho_i A \frac{ds}{dt}$$

$\uparrow$  energy       $\uparrow$  density  
 unit mass      of ice

$$\Rightarrow -K \frac{dT(s(t))}{dt} = q \rho_i \frac{ds}{dt} \quad (2)$$

We solve (1) using combination of variables:

$$\Theta = A \operatorname{erf}\left(\frac{x}{\sqrt{4\alpha t}}\right) + B$$

$$\frac{T-T_0}{T_w-T_0}$$

$$①: 1 = A \operatorname{erf}(0) + B \Rightarrow B = 1$$

$$\begin{aligned} \Theta &= 1 && \text{at } x=0 \\ \Theta &= 0 && \text{at } x=s(t) \end{aligned} \quad (1) \quad (2)$$

$$②: 0 = A \operatorname{erf}\left(\frac{s(t)}{\sqrt{4\alpha t}}\right) + 1 \Rightarrow A = -\frac{1}{\operatorname{erf}(\lambda)}$$

Note: since  $A$  is a constant,  $\lambda$  must also be a constant  $\Rightarrow s(t) \propto \sqrt{t}$  (we will see if it makes sense)

$$(*) -K \frac{d}{dt} \left( 1 - \frac{1}{\operatorname{erf}(\lambda)} \operatorname{erf}\left(\frac{x}{\sqrt{4\alpha t}}\right) \right) = q \rho_i \frac{d}{dt} (\lambda \sqrt{4\alpha t})$$

$$\Rightarrow -K \left( -\frac{1}{\operatorname{erf}(\lambda)} \frac{x}{\sqrt{4\alpha t}} e^{-\frac{x^2}{4\alpha t}} \right) \Big|_{x=s(t)} = q \rho_i \lambda \sqrt{4\alpha t} \frac{1}{2} t^{-1/2}$$

$$\frac{K(T_w-T_0)}{\operatorname{erf}(\lambda) \sqrt{4\alpha t}} e^{-\lambda^2} = \frac{q \rho_i \lambda \sqrt{\alpha}}{\sqrt{t}} \Rightarrow \operatorname{erf}(\lambda) e^{-\lambda^2} = \frac{K(T_w-T_0)}{q \rho_i \sqrt{\alpha}}$$

$$\text{Summary} \rightarrow \left\{ \begin{array}{l} \theta(x,t) = 1 - \frac{1}{\operatorname{erf}(\lambda)} \operatorname{erf}\left(\frac{x}{\sqrt{4at}}\right) \\ s(t) = 2\lambda\sqrt{at} \end{array} \right.$$

Neumann solution

$$s(t) = 2\lambda\sqrt{at}$$

$$\lambda \operatorname{erf}(\lambda) e^{\lambda^2} = \frac{k(T_w - T_0)}{\rho_i q \sqrt{\pi}} = \frac{C_p(T_w - T_0)}{a \sqrt{\pi}} = \beta$$

$\frac{k}{C_p}$  and  $\rho_i \approx \rho$

$$\rightarrow \text{For water, } \beta \approx 0.007(T_w - T_0)$$

$$q \approx 336000 \frac{J}{kg} \quad C_p \approx 4184 \frac{J}{kg \cdot K}$$

we implicitly assumed that there is no volume change

# 319

- Stefan problem (continued)
- film condensation

## Stefan problem

We have  $\lambda \operatorname{erf}(\lambda) e^{\frac{\lambda^2}{2}} = \beta \rightarrow S(t) = 2\lambda \sqrt{\pi t}$

→ Strictly increasing

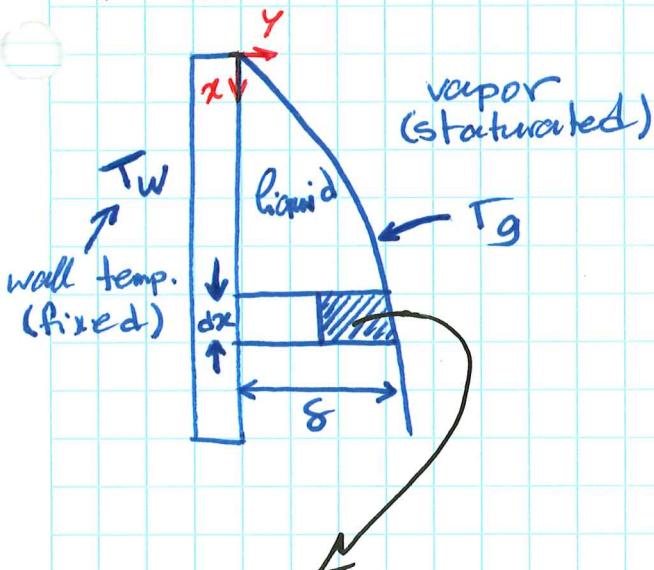
Find  $\lambda$  using Newton's method  $\rightarrow \text{sv } \theta \checkmark$

$$\theta(x,t) = 1 - \frac{1}{\operatorname{erf}(\lambda)} \operatorname{erf}\left(\frac{x}{2\sqrt{\pi t}}\right)$$

Note that  $\theta(S(t), t) = 0$

see "Stefan.py"

## Film condensation



(first proposed by Nusselt) 1916

Tg: equilibrium temp (e.g., 100°C for water at 1 atm)

$$T_w < T_g$$

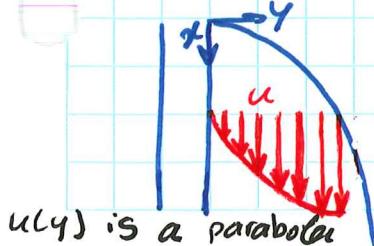
wall removes heat from vapor → vapor turns to liquid

Weight of the element:  $W = dx(\delta-y)\rho g$   
Buoyancy force:  $B = dx(\delta-y)\rho_v g$

There is a gradient of velocity in the x direction → it increases from the wall to the interface

→ the element will experience a shear force pulling it up:

$$S = \mu \frac{du}{dy} dx$$



At the interface, we assume negligible shear stress by the vapor phase.

$$\rightarrow \frac{d\sigma}{dx}(\delta-y)\rho g = \frac{d\sigma}{dx}(\delta-y)\rho_v g + \mu \frac{du}{dy} \frac{d\sigma}{dx}$$

$$\Rightarrow u = \frac{g}{\mu} (\rho - \rho_v) \left( \delta y - \frac{1}{2} y^2 \right) + C_0$$

velocity in the  $x$  direction

because  $u(0) = 0$   
(no-slip boundary condition)

mass flow of condensate at each  $x$ :

$$m = \int_0^\delta \rho u(y) dy = \frac{\rho(\rho - \rho_v)g}{\mu} \left[ \delta \frac{\delta^2}{2} - \frac{1}{2} \frac{\delta^3}{3} \right]$$

$$= m = \frac{\rho(\rho - \rho_v)g \delta^3}{3\mu}$$

the amount of condensate added between  $x$  and  $x+dx$  is the differential of  $m$ :

$$dm = \frac{\rho(\rho - \rho_v)g \delta^2}{\mu} d\delta$$

Energy needs to be removed from vapor to condense it. This energy will conduct to the wall:

$$(dm) \times h = (q_{-y} dx) = k \frac{dT}{dy} \Big|_{y=\delta} dx$$

$\approx 2260 \frac{\text{kJ}}{\text{kg}}$  latent heat of condensation      heat flux in the " $-y$ " direction

Assume a linear temperature distribution between wall and interface  $\rightarrow \frac{dT}{dy} = \frac{T_g - T_w}{\delta}$

$$\Rightarrow \frac{h\rho(\rho - \rho_v)g \delta^2}{\mu} dx = k \frac{T_g - T_w}{\delta} dx$$

$$\Rightarrow \delta^3 d\delta = \frac{\mu k (T_g - T_w)}{h \rho (\rho - \rho_v) g} dx$$

$$\Rightarrow \frac{1}{4} \delta^4 = \frac{\mu k (T_g - T_w)}{h \rho (\rho - \rho_v) g} x + C$$

$$\text{at } x=0 \Rightarrow \delta=0 \Rightarrow C=0$$

$$\Rightarrow \delta = \left[ \frac{4 \mu k (T_g - T_w)}{h \rho (\rho - \rho_v) g} x \right]^{1/4}$$

# 320

## Angular Momentum & Fixed Axis Rotation

$\vec{x}$  is a vector  
 $x$  is  $|\vec{x}|$

Translational Motion:

→ force, linear momentum, center of mass

Rotational Motion:

→ torques, angular momentum, moment of inertia

Angular Momentum of a Particle

not an extended body

→ angular momentum  $\vec{L}$  of a particle that has momentum  $\vec{p} = m\vec{v}$  and is at position  $\vec{r}$  with respect to a given origin:

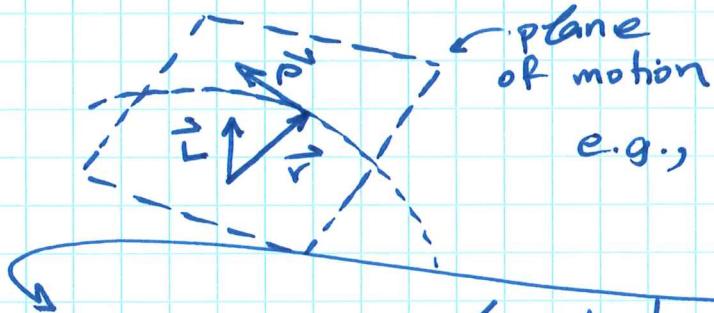
$$\vec{L} = \vec{r} \times \vec{p}$$

$$L = r p \sin \alpha$$

$$[L] = \frac{ML^2}{T}$$

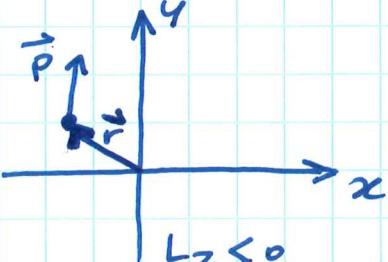
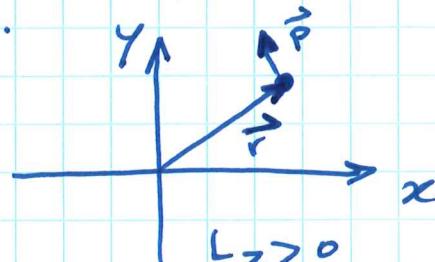
Remarks:

- $\vec{p}$  is independent of the coordinate system but  $\vec{L}$  is not!
- $\vec{L}$  is perpendicular to the plane of motion

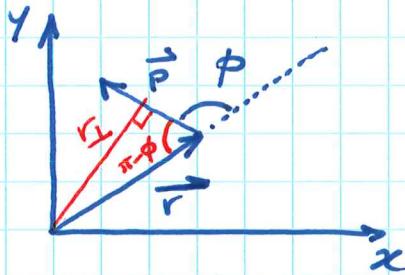


e.g., if  $\vec{r}$  and  $\vec{p}$  lie in the xy plane,  $\vec{L}$  lies along the z direction.

Right hand rule determines if it is in the positive or negative z directions: point your fingers (right hand) along  $\vec{r}$  and orient your hand so that you can bend your fingers toward  $\vec{p}$ ; your thumb then points in the direction of  $\vec{L}$ .



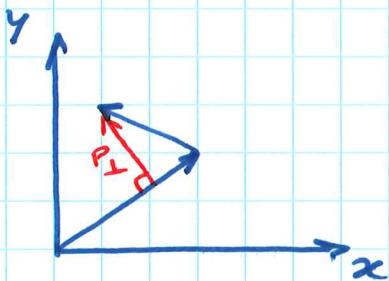
# Geometrical Understanding



- Decompose  $\vec{r}$  into  $\vec{r}_{\perp}$  that is perpendicular to the trajectory and  $\vec{r}_{\parallel}$  that is parallel.

$$r_{\perp} = r \sin(\pi - \phi) = r \sin \phi$$

$$\Rightarrow L_z = r p \sin \phi = \frac{r_{\perp} p}{\cancel{\pi - \phi}}$$



- Decompose  $\vec{p}$  into  $\vec{p}_{\perp}$  that is perpendicular to  $\vec{r}$  and  $\vec{p}_{\parallel}$  that is parallel.

$$p_{\perp} = p \sin(\pi - \phi) = p \sin \phi$$

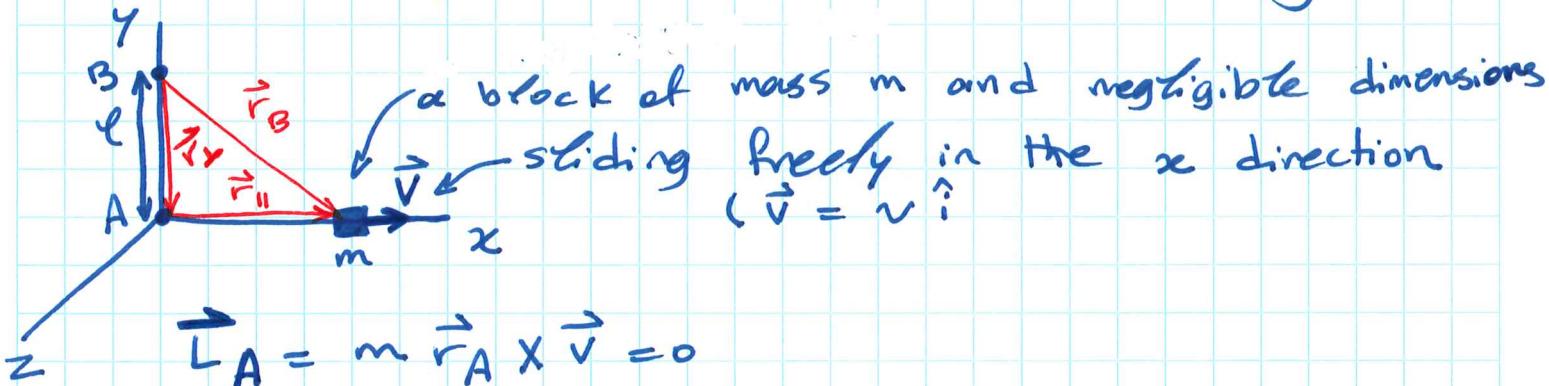
$$\Rightarrow L_z = r p \sin \phi = \frac{r p_{\perp}}{\cancel{\pi - \phi}}$$

algebraically:

$$\vec{r} = (x, y, 0), \quad \vec{p} = (m v_x, m v_y, 0)$$

$$\Rightarrow \vec{L} = \vec{r} \times \vec{p} = m \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ x & y & 0 \\ v_x & v_y & 0 \end{vmatrix} = m (x v_y - y v_x) \hat{k}$$

Example: Angular Momentum of a sliding Block



$$\vec{L}_A = m \vec{r}_A \times \vec{v} = 0$$

$$\vec{L}_B = m \vec{r}_B \times \vec{v} = m (\vec{r}_{\parallel} + \vec{r}_{\perp}) \times \vec{v} = m \ell v \hat{k}$$

Or,

$$\vec{L}_B = m \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ x & y & 0 \\ \ell & 0 & 0 \end{vmatrix} = m \ell v \hat{k}$$

# Fixed Axis Rotation

direction of rotation around z for example  
 (z is the axis of rotation)  
 the axis of rotation is always along the same line: e.g.,

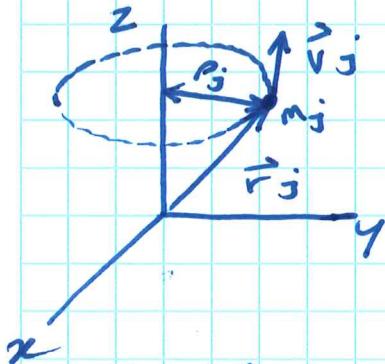
a car wheel attached to an axle undergoes fixed axis rotation as long as the car drives straight.

- When a rigid body rotates around an axis, every particle in the body remains at a fixed distance from the axis.

→ a coordinate system with its origin on the axis,  $|\vec{r}| = \text{constant}$  for every particle

⇒  $\vec{r}$  changes while  $|\vec{r}|$  remains constant: velocity is perpendicular to  $\vec{r}$ .

Consider a body rotating around the z axis:



$p_j$ : perpendicular distance to the axis of rotation from particle  $m_j$

$$|\vec{v}_j| = p_j \omega_j$$

rate of rotation (angular speed)

Angular momentum of the jth particle:

$$\vec{L}_j = \vec{r}_j \times m_j \vec{v}_j$$

not exactly in the z direction!

Our focus: The component of angular momentum along the axis of rotation (z here)

$$\Rightarrow L_{j,z} = p_j m_j v_j^2 = m_j p_j^2 \omega_j$$

sum over all particles of the body

$$\text{for the whole body: } L_z = \sum_j L_{j,z} = \sum_j m_j p_j^2 \omega_j \quad w \text{ is constant (rigid body)}$$

# 321

## Moment of Inertia Parallel Axis Theorem

$$L_z = \sum_j L_{j,z} = \sum_j m_j p_j^2 \omega \equiv I \omega$$

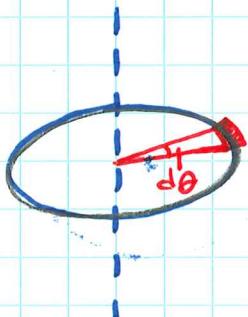
analogies:  $\vec{p} = m \vec{v}$   
 $I = \sum m_j p_j^2$

$I$ : geometrical quantity called "moment of inertia"

For continuously distributed matter:  $I = \int p^2 dm$

### Moments of inertia of some simple objects <sup>M</sup>

(a) Uniform thin ring of mass  $M$  and radius  $R$ , around the axis of symmetry of the ring

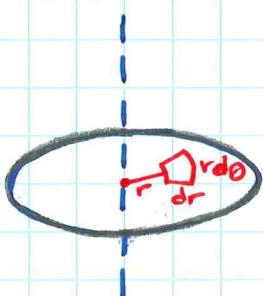


Let  $\lambda = \frac{M}{2\pi R}$  mass per unit length of the ring

$$\Rightarrow dm = R d\theta \lambda$$

$$\Rightarrow I = \int^{2\pi} R^2 \cdot (R d\theta \lambda) = 2\pi R^3 \lambda = MR^2$$

(b) Uniform thin disk of mass  $M$  and radius  $R$ , around the axis of symmetry of the disk

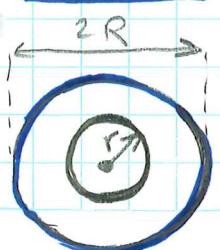


$\lambda = \frac{M}{\pi R^2}$  mass per unit area of the disk

$$dm = r d\theta dr \lambda$$

$$\Rightarrow I = \int_0^{2\pi} \int_0^R r^2 \cdot (r d\theta dr \lambda) = 2\pi \lambda \frac{R^4}{4}$$

Alternatively: divide the disk into rings with top view



$$\Rightarrow I = \int dI = \int_0^R 2\pi r^3 \lambda dr = 2\pi \lambda \frac{R^4}{4} = \frac{1}{2} MR^2$$

moment of inertia  
for a ring of mass  $2\pi r dr \lambda$   
and radius  $r$

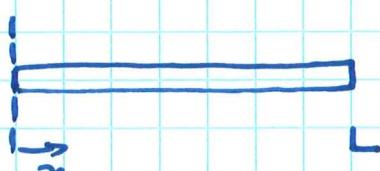
(c) Uniform thin stick of mass  $M$  and length  $L$ , around a perpendicular axis through its midpoint



$$\lambda = \frac{M}{L}$$

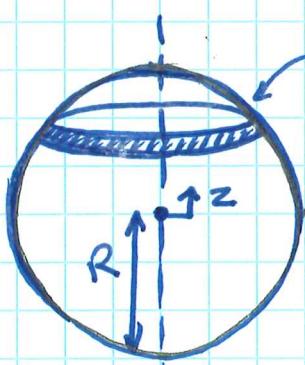
$$I = \int_{-L/2}^{L/2} x^2 \lambda dx = \frac{1}{12} \lambda L^3 = \frac{1}{12} M L^2$$

(d) Uniform thin stick around a perpendicular axis at its end.



$$I = \int_0^L x^2 \lambda dx = \frac{1}{3} \lambda L^3 = \frac{1}{3} M L^2$$

(e) Uniform sphere of mass  $M$  and radius  $R$ , around an axis through its center



disks of radius  $r(z)$  and thickness  $dz$

$$I = 2 \int dI = 2 \int_0^R \frac{1}{2} \pi r^4 \lambda dz = \pi \lambda \int_0^R r^4 dz$$

↑ moment of inertia  
for a disk of mass  $\pi r^2 dz$   
and radius  $r$

$$r = \sqrt{R^2 - z^2} \Rightarrow I = \pi \lambda \int_0^R (R^2 - z^2)^2 dz = \frac{2}{5} M R^2$$

$$\lambda = \frac{M}{\frac{4}{3} \pi R^3}$$

### Parallel Axis Theorem

tells us  $I$ , the moment of inertia around any axis, provided that we know  $I_0$ , the moment of inertia around an axis through the center of mass parallel to the first.

$$I = I_0 + M \ell^2$$

$$\vec{X} = \frac{1}{M} \sum_{j=1}^N m_j \vec{r}_j$$

$\ell$ : distance between the two axes of mass  $m_j$  and  $\vec{r}_j$

(center of mass for  $N$  masses)

$M$ : total mass

In continuous form  $\rightarrow \vec{x} = \frac{1}{m} \int \vec{r} dm$

Example: moment of inertia of a M disk around axis at the rim

the center of mass for a disk is out its center:

Can you prove it?

$$\Rightarrow I = I_0 + MR^2$$

$$I_0 = \frac{1}{2} MR^2$$

radius of the disk

$$= \frac{1}{2} MR^2 + MR^2 = \frac{3}{2} MR^2$$

# 322

## Torque Torque & Angular Momentum Yo-Yo motion

Torque

$$\vec{\tau} = \vec{r} \times \vec{F}$$

torque due to force  $\vec{F}$   
that acts on a particle  
at position  $\vec{r}$

$$|\vec{\tau}| = |\vec{r}_\perp| |\vec{F}| = |\vec{r}| |\vec{F}_\perp|$$

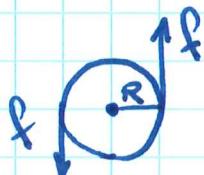
Also,

$$\vec{\tau} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ x & y & z \\ F_x & F_y & F_z \end{vmatrix}$$

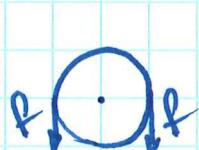
$\Rightarrow$  torque depends on the  
origin we choose but  
force does not.

$\vec{\tau}$  and  $\vec{F}$  are always mutually  
perpendicular.

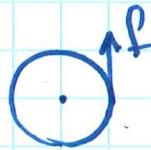
- Force and torque are inherently different quantities.



$$F = 0$$



$$F = 2f$$



$$F = f$$

three different cases  
of  $\tau$ ,  $F$  combinations  
( $\tau$  is evaluated around  
the center of the  
disk)

### Torque due to gravity

For a uniform gravitational field:  $\vec{\tau} = \vec{R} \times \vec{W}$

$$\text{Proof: } \vec{\tau}_j = \vec{r}_j \times m_j \vec{g} = m_j \vec{r}_j \cdot \vec{g}$$

$$\Rightarrow \vec{\tau} = \sum_j \vec{\tau}_j = \underbrace{\left( \sum_j m_j \vec{r}_j \right)}_{M \vec{R}} \times \vec{g}$$

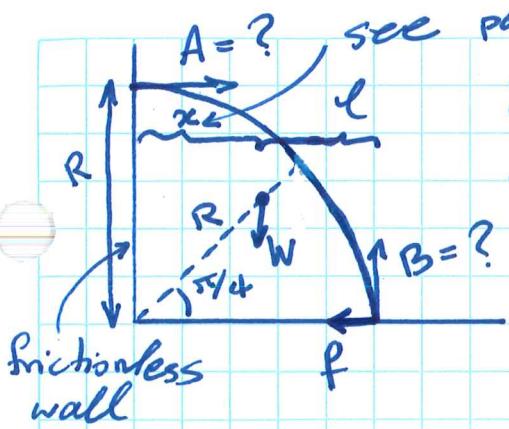
vector to the center  
of mass

$$\vec{\tau} = \vec{R} \times M \vec{g} \quad \checkmark$$

### Torque and Force in Equilibrium

equilibrium  $\rightarrow$  total force = 0  
total torque = 0

around any origin (better to choose a point  
where several forces act, since then torques  
due to these forces all vanish.)



see page 67 for details  
a uniform rod of length  $\frac{\pi R}{2}$  bent in the shape of a quadrant of radius  $R$

force balance in the  $x$  and  $y$  directions:

$$x: A = f$$

$$y: B = W$$

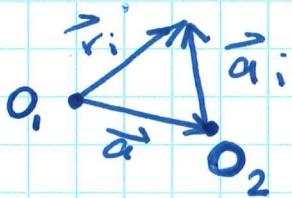
torque about the point where the quadrant rests:

$$\tau = \ell W - RA = 0 \Rightarrow A = \frac{\ell W}{R}$$

$$\Rightarrow A = \frac{W}{R} \left(1 - \frac{2}{\pi}\right) R \approx 0.36 W$$

$$\ell = R - x = \left(1 - \frac{2}{\pi}\right) R$$

\* If the total torque is zero about a point, it will be zero around any other point given that  $\sum F = 0$  (total force is zero)



$$\sum_i \vec{r}_i \times \vec{F}_i = 0 \quad (\text{about } O_1)$$

$$\begin{aligned} \text{force index} \Rightarrow \sum_i \vec{r}_i \times \vec{F}_i &= \sum_i (\vec{\alpha} + \vec{q}_i) \times \vec{F}_i \\ &= \sum_i \vec{\alpha} \times \vec{F}_i + \sum_i \vec{q}_i \times \vec{F}_i \\ &= \vec{\alpha} \times (\sum_i \vec{F}_i) + \sum_i \vec{q}_i \times \vec{F}_i \end{aligned}$$

$$\Rightarrow \sum_i \vec{r}_i \times \vec{F}_i = \sum_i \vec{q}_i \times \vec{F}_i = 0$$

## Torque & Angular Momentum

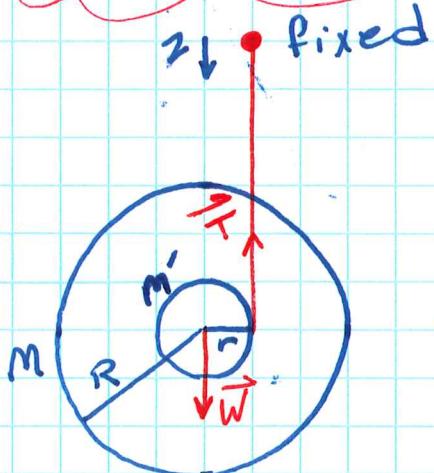
$$\begin{aligned} \vec{L} &= \vec{r} \times \vec{p} \Rightarrow \frac{d\vec{L}}{dt} = \frac{d\vec{r}}{dt} \times \vec{p} + \vec{r} \times \frac{d\vec{p}}{dt} = \underbrace{\vec{v} \times \vec{p}}_0 + \vec{r} \times \frac{d\vec{p}}{dt} \\ \Rightarrow \frac{d\vec{L}}{dt} &= \vec{r} \times \vec{F} = \vec{\tau} \end{aligned}$$

$$\vec{F} = \frac{d\vec{p}}{dt}$$

$$\begin{aligned} \frac{d\vec{L}}{dt} &= \vec{\tau} \\ \frac{d\vec{p}}{dt} &= \vec{F} \end{aligned}$$

(by Newton's second law)

Yo-Yo motion



total moment of inertia:

$$I = I_{\text{outer}} + I_{\text{inner}} = \frac{1}{2}MR^2 + \frac{1}{2}mr^2 \quad (m=M+m')$$

two large cylinders

one small cylinder

- Linear momentum:

$$\begin{aligned} \frac{d\vec{P}}{dt} &= \vec{W} + \vec{T} \Rightarrow m \frac{d\vec{v}}{dt} = \vec{W} + \vec{T} \\ &\Rightarrow m \frac{d\vec{v}}{dt} = W - T \end{aligned} \quad (\text{i})$$

velocity of center of mass

- Angular momentum: (about the center of mass)

$$\frac{d\vec{L}}{dt} = I \frac{d\vec{\omega}}{dt} = \vec{r} \times \vec{T} \Rightarrow I \frac{d\omega}{dt} = rT \quad (\text{iii})$$

Note that  $v = \frac{dz}{dt} = r\omega \Rightarrow \dot{\omega} = \frac{\dot{v}}{r}$

$$\textcircled{*} \rightarrow (\text{ii}) \Rightarrow \frac{I}{r} \dot{v} = rT \stackrel{(\text{ii})}{=} r(W - m\dot{v})$$

$$\Rightarrow \frac{I}{r} \dot{v} = rm\ddot{v} - rm\dot{v} \Rightarrow \dot{v} \left( \frac{I}{r} + rm \right) = rm\ddot{v}$$

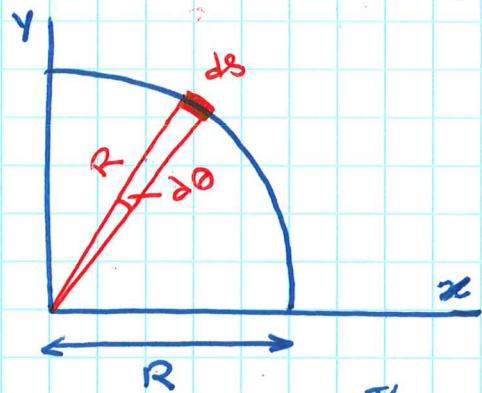
$$\Rightarrow \dot{v} = \frac{g}{1 + \frac{I}{r^2 m}}$$

acceleration is lower than gravitational

If we had only one cylinder with radius  $r$  and mass  $m \rightarrow I = \frac{1}{2}mr^2$

$$\Rightarrow \dot{v} = \frac{g}{1 + \frac{1}{2}} = \frac{2}{3}g$$

Center of mass of a bent rod (example from session 22)



$$\vec{x} = \frac{1}{m} \int \vec{r} dm \quad \lambda = \frac{m}{\pi R} \frac{\pi R}{2}$$

$$dm = \lambda ds = \lambda R d\theta$$

$$\vec{r} = R \hat{r} = R (\cos \theta \hat{i} + \sin \theta \hat{j})$$

$$\Rightarrow \vec{x} = \frac{1}{m} \int_0^{\pi/2} R (\cos \theta \hat{i} + \sin \theta \hat{j}) \lambda R d\theta = \frac{\lambda R^2}{m} \int_0^{\pi/2} (\cos \theta \hat{i} + \sin \theta \hat{j}) d\theta$$

$$\Rightarrow \vec{x} = \frac{\lambda R^2}{m} (\hat{i} + \hat{j}) = \frac{2R}{\pi} (\hat{i} + \hat{j})$$

$$\Rightarrow \ell = R - x = R - \frac{2}{\pi} R \approx 0.36 R$$

# 323

- Conservation of angular momentum
- Law of equal areas (Kepler's 2nd law)
- effective area of a far-off planet

$$\frac{d\vec{L}}{dt} = \vec{\tau} \rightsquigarrow \vec{\tau} = 0 \Rightarrow \vec{L} \text{ is constant and the angular momentum is conserved.}$$

## Law of equal areas (Kepler's second law)

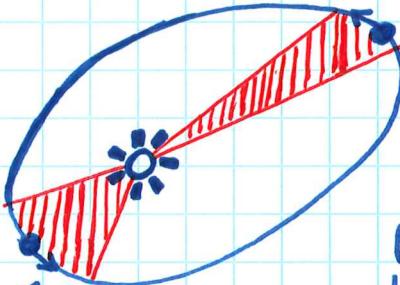
Explanation:

earth is moving under a central force (gravity, but can be extended to any central force):

$$\vec{F}(r) = f(r) \hat{r} \quad \begin{matrix} \text{unit vector} \\ \text{in the radial direction} \end{matrix}$$

$$\rightsquigarrow \vec{\tau} = \vec{r} \times \vec{F} = \vec{r} \times f(r) \hat{r} = 0$$

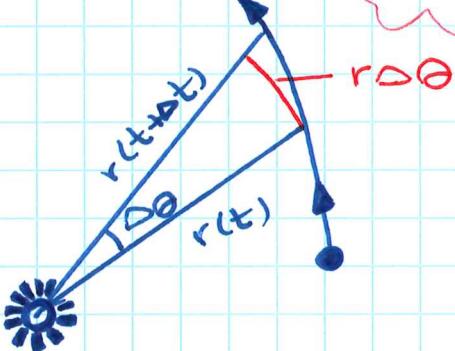
(around sun)



The area swept by the earth for a given time is constant.

→ the angular momentum is conserved

- $\vec{L}$  is therefore constant in both magnitude and direction → motion is confined to a plane!



For small  $\Delta\theta$ , the area swept by earth can be approximated as

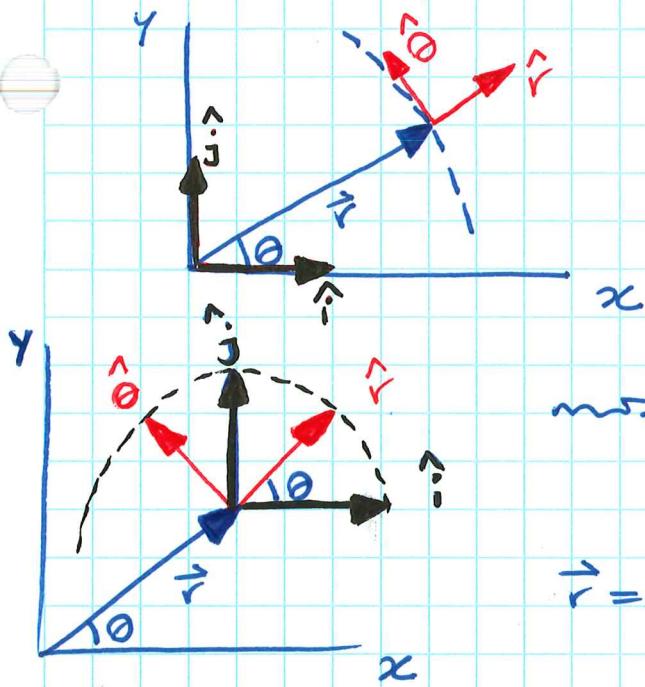
$$\begin{aligned}\Delta A &\approx \frac{1}{2} (r(t+\Delta t)) \cdot (r \Delta\theta) \\ &= \frac{1}{2} (r + \Delta r) \cdot (r \Delta\theta) \\ &= \frac{1}{2} r^2 \Delta\theta + \frac{1}{2} r \Delta r \Delta\theta\end{aligned}$$

The rate at which area is swept is

$$\frac{dA}{dt} = \lim_{\Delta t \rightarrow 0} \frac{\Delta A}{\Delta t} = \lim_{\Delta t \rightarrow 0} \left[ \frac{1}{2} r^2 \frac{\Delta\theta}{\Delta t} + \frac{1}{2} r \frac{\Delta r \Delta\theta}{\Delta t} \right]$$

$$\rightsquigarrow \frac{dA}{dt} = \frac{1}{2} r^2 \dot{\theta} \quad (*)$$

# A digression to polar coordinates



Fundamental difference: the directions of  $\hat{r}$  and  $\hat{\theta}$  vary with position, whereas  $\hat{i}$  and  $\hat{j}$  have fixed directions

$$\Rightarrow \hat{r} = \hat{i} \cos \theta + \hat{j} \sin \theta \\ \hat{\theta} = -\hat{i} \sin \theta + \hat{j} \cos \theta$$

$$\vec{r} = r \cos \theta \hat{i} + r \sin \theta \hat{j} \\ = r (\cos \theta \hat{i} + \sin \theta \hat{j}) = r \hat{r}$$

Velocity in polar coordinates  $\vec{v}$ :

$$\frac{d\vec{r}}{dt} = \frac{dr}{dt} \hat{r} + r \frac{d\hat{r}}{dt} \quad \Rightarrow \quad \frac{d\hat{r}}{dt} = \frac{d}{dt} (\cos \theta \hat{i} + \sin \theta \hat{j})$$

$$\Rightarrow \frac{d\vec{r}}{dt} = \dot{r} \hat{r} + r \dot{\theta} \hat{\theta} \\ \Rightarrow \vec{v} = \dot{r} \hat{r} + r \dot{\theta} \hat{\theta}$$

$$\vec{L} = \vec{r} \times m \vec{v} = r \hat{r} \times m (\dot{r} \hat{r} + r \dot{\theta} \hat{\theta})$$

$$= m r \cancel{\dot{r} \hat{r} \times \hat{r}} + m r^2 \dot{\theta} \hat{r} \times \hat{\theta} \quad \Rightarrow \quad \vec{L} = m r^2 \dot{\theta} \hat{k}$$

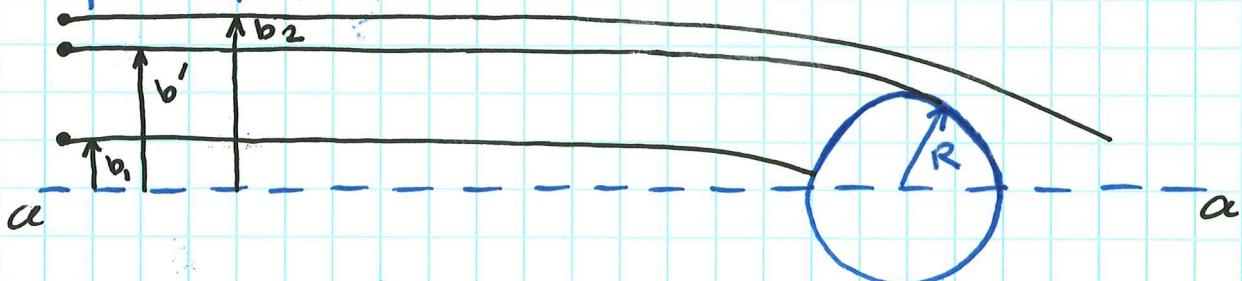
$$\Rightarrow L_z = m r^2 \dot{\theta}$$

$$\textcircled{*} \rightarrow \frac{dA}{dt} = \frac{1}{2} r^2 \dot{\theta} = \frac{L_z}{2m} \quad \text{constant for any central force}$$

$$\Rightarrow \frac{dA}{dt} = \text{constant} \quad \checkmark$$

## Effective area of a far planet

How accurately must you aim the trajectory of an unpowered space craft to hit a far-off planet?

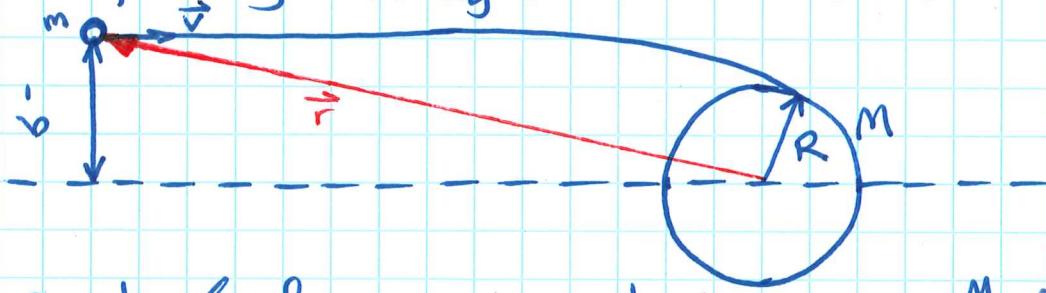


$$\text{geometrical area: } A_g = \pi R^2$$

$$\text{effective area: } A_e = \pi b'^2$$

$\left. \begin{array}{l} \\ \end{array} \right\} A_e > A_g \text{ due to gravity}$

Distance between the launch point and the planet is  $\gg R \rightarrow$  different trajectories are parallel to "aa" passing through the center of the planet.



$$\text{Central force (gravity)} = -G \frac{mM}{r^2} \hat{r}$$

$\vec{\tau} = \vec{r} \times (-G \frac{mM}{r^2} \hat{r}) = 0 \rightarrow$  conservation of angular momentum around the center of the planet

$$\text{Conservation of energy: } E = \frac{1}{2}mv^2 - G \frac{mM}{r}$$

$$\text{Initially: } E_i = \frac{1}{2}mv_0^2 - 0 \quad r \rightarrow \infty$$

$$L_i = -b'mv_0$$

$$\vec{F} = -\nabla U$$

↑  
potential energy

At the point of closest approach,  $\vec{v}$  and  $\vec{r}$  are perpendicular upon collision:

$$L_c = -mRv(R); E_c = \frac{1}{2}mv^2(R) - G \frac{mM}{R}$$

$$L_i = L_c \Rightarrow v(R) = v_0 \frac{b'}{R}$$

$$E_i = E_C \Rightarrow \frac{1}{2}mv_0^2 = \frac{1}{2}mv(R)^2 - G\frac{mM}{R}$$

$$= \frac{1}{2}mv_0^2 \frac{b'^2}{R^2} - G\frac{mM}{R}$$

$-U(R)$

$$\Rightarrow \frac{1}{2}mv_0^2 \left( \frac{b'^2}{R^2} - 1 \right) = G\frac{mM}{R} \Rightarrow b'^2 = R^2 \left( 1 + \frac{G\frac{mM}{R}}{\frac{1}{2}mv_0^2} \right)$$

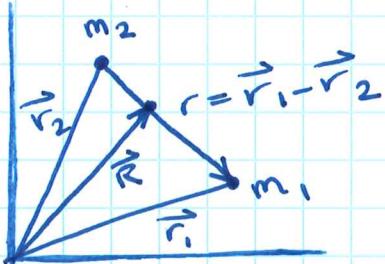
$\Rightarrow A_e = \pi b'^2 = A_g \left( 1 - \frac{U(R)}{E_i} \right)$

$$\frac{\frac{1}{2}mv_0^2}{E_i}$$

# 324

- Central force motion
- Universal features of central force motion
- Energy eqn and energy diagrams

Central force motion as a one-body problem



An isolated system of two particles interacting under a central force  $\vec{f}(r) \hat{r}$

equations of motion:  $m_1 \ddot{\vec{r}}_1 = \vec{f}(r) \hat{r} \quad (1)$   
 $m_2 \ddot{\vec{r}}_2 = -\vec{f}(r) \hat{r} \quad (2)$

$\vec{f}(r) < 0 \rightarrow$  attractive  
 $\vec{f}(r) > 0 \rightarrow$  repulsive

Write (1) & (2) in terms of  $\vec{r} = \vec{r}_1 - \vec{r}_2$  and

$$\vec{R} = \frac{m_1 \vec{r}_1 + m_2 \vec{r}_2}{m_1 + m_2} \quad (\text{center of mass})$$

$\vec{r}$ : divide (1) by  $m_1$  and (2) by  $m_2$  to get

$$\ddot{\vec{r}}_1 = \frac{\vec{f}(r)}{m_1} \hat{r}, \quad \ddot{\vec{r}}_2 = \frac{\vec{f}(r)}{m_2} \hat{r} \Rightarrow \underbrace{\frac{m_1 m_2}{m_1 + m_2} \ddot{\vec{r}}}_{\mu} = \vec{f}(r) \hat{r}$$

$$\Rightarrow \mu \ddot{\vec{r}} = \vec{f}(r) \hat{r} \quad (*)$$

$\mu$  (reduced mass)

$\vec{R}$ : add (1) & (2) and divide by  $m_1 + m_2$ :

$$\Rightarrow \ddot{\vec{R}} = \ddot{\vec{R}}_0 + \vec{v} t$$

center of mass is

origin at the center of mass?  $\vec{R}_0 =$   
stationary?  $\vec{v} = 0$

(\*) eqn of motion for a single particle.  
(not generalizable to systems with more than two particles)

$$\vec{r} \& \vec{R} \text{ are known} \rightarrow \vec{r}_1 = \vec{R} + \left(\frac{m_2}{m_1 + m_2}\right) \vec{r} \& \vec{r}_2 = \vec{R} - \left(\frac{m_1}{m_1 + m_2}\right) \vec{r}$$

## Conservation of angular momentum (see session 23)

→ the angular momentum is conserved  
 $\Rightarrow L = \text{constant}$  and the motion is confined to a plane  
 $\Rightarrow$  law of equal areas

## Conservation of energy

the kinetic energy of  $\mu$  is (written in polar coordinates)

$$K = \frac{1}{2}\mu v^2 = \frac{1}{2}\mu(r\dot{r}\hat{r} + r^2\dot{\theta}\hat{\theta})^2 = \frac{1}{2}\mu(r^2 + r^2\dot{\theta}^2)$$

there is also a potential energy associated with the central force  $f(r)$ :

$$f(r) = -\frac{dU(r)}{dr} \rightarrow U(r) = -\int f(r) dr$$

$$\Rightarrow E = K + U = \frac{1}{2}\mu v^2 + U(r) \quad (U \rightarrow 0 \text{ as } r \rightarrow \infty)$$

$$= \frac{1}{2}\mu r^2 + \frac{1}{2}\mu r^2 \dot{\theta}^2 + U(r)$$

$$= \frac{1}{2}\mu r^2 + \frac{1}{2} \frac{L^2}{\mu r^2} + U(r)$$

centrifugal potential

$U_{\text{eff}}(r)$

$$L = \mu r^2 \dot{\theta}$$

true potential

$$\Rightarrow E = K + U_{\text{eff}} = \frac{1}{2}\mu r^2 + U_{\text{eff}}(r)$$

energy  $E$  is  
for a particle  
moving in one  
dimension.

all reference to  $\theta$  is gone!

## Energy eigen and energy diagrams

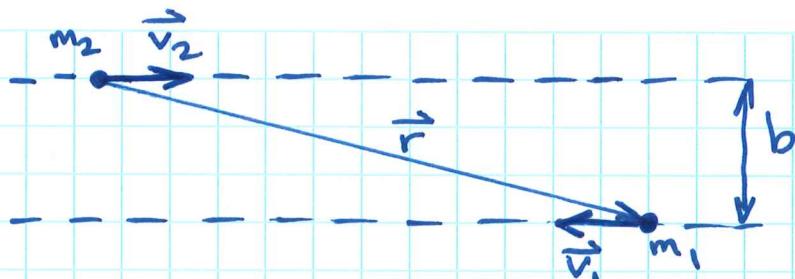
$$E = \frac{1}{2}\mu v^2 + U(r) = \frac{1}{2}\mu r^2 + U_{\text{eff}}(r)$$

depends on  
or single  
coordinate  
only:  $r$

handy for evaluating  $E$ ; all we need to know is the relative speed and position at some instant.

can be used  
in energy diagrams  
versus  $r$

Example  
non-interacting particles  
 $(U(r)=0)$



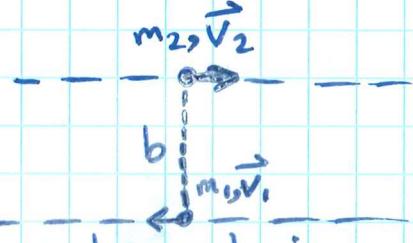
Goal is to plot  $U_{\text{eff}}$  versus  $r$  and interpret the system behavior.

$$U_{\text{eff}} = \frac{1}{2} \frac{L^2}{\mu r^2} + U(r) \quad E = \frac{1}{2} m v^2 + U(r) = \frac{1}{2} \mu r^2 + U_{\text{eff}}(r)$$

$$\Rightarrow \frac{1}{2} m v^2 = \frac{1}{2} \mu r^2 + \frac{1}{2} \frac{L^2}{\mu r^2}$$

$$\vec{v} = \frac{d\vec{r}}{dt} = \vec{v}_1 - \vec{v}_2 = \vec{v}_0 \quad (\text{constant})$$

$$\Rightarrow \frac{1}{2} m v_0^2 = \frac{1}{2} \mu r^2 + \frac{1}{2} \frac{L^2}{\mu r^2}$$

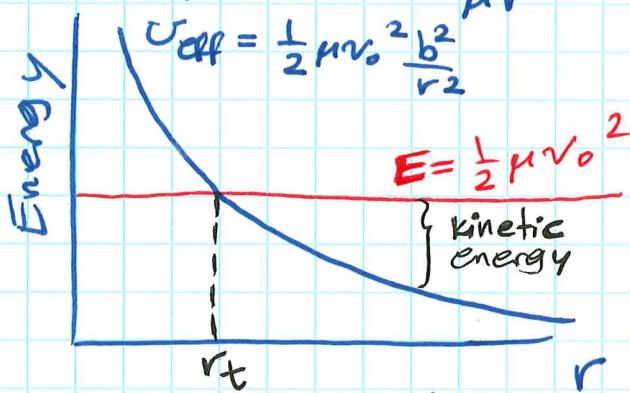


When  $m_1$  and  $m_2$  pass each other,  $r=b$  and  $v=0$

$$\Rightarrow \frac{1}{2} m v_0^2 = 0 + \frac{1}{2} \frac{L^2}{\mu b^2} \Rightarrow L = \mu b v_0$$

Alternatively  $\vec{L} = \vec{r} \times \mu \vec{v} = \mu b v_0$  (try it!)

$$\Rightarrow U_{\text{eff}}(r) = \frac{1}{2} \frac{L^2}{\mu r^2} = \frac{1}{2} \mu v_0^2 \frac{b^2}{r^2}$$



$\Rightarrow$  motion is restricted to regions where  $E - U_{\text{eff}} > 0$ .

the kinetic energy associated with the radial motion is

$$\frac{1}{2} \mu r^2 = U_{\text{eff}} + E$$

can never be negative

$E - U_{\text{eff}} > 0$ .

Initially  $r$  is very large and  $U_{\text{eff}} \approx 0$ . As the particles approach, the kinetic energy decreases, vanishing at the "turning point" where the radial velocity is zero:

$$E = U_{\text{eff}}(r_t)$$

$$\Rightarrow \frac{1}{2}\mu v^2 = \frac{1}{2}\mu v_0^2 \frac{b^2}{r_t^2} = -\underbrace{\epsilon}_{r_t = b}$$

$\uparrow$   
distance of  
the closest approach  
of the particles

# 325

- Energy diagram of planetary motion
- Perturbed circular orbit

Gravitational force (always attractive):  $f(r) = -G \frac{m_1 m_2}{r^2}$

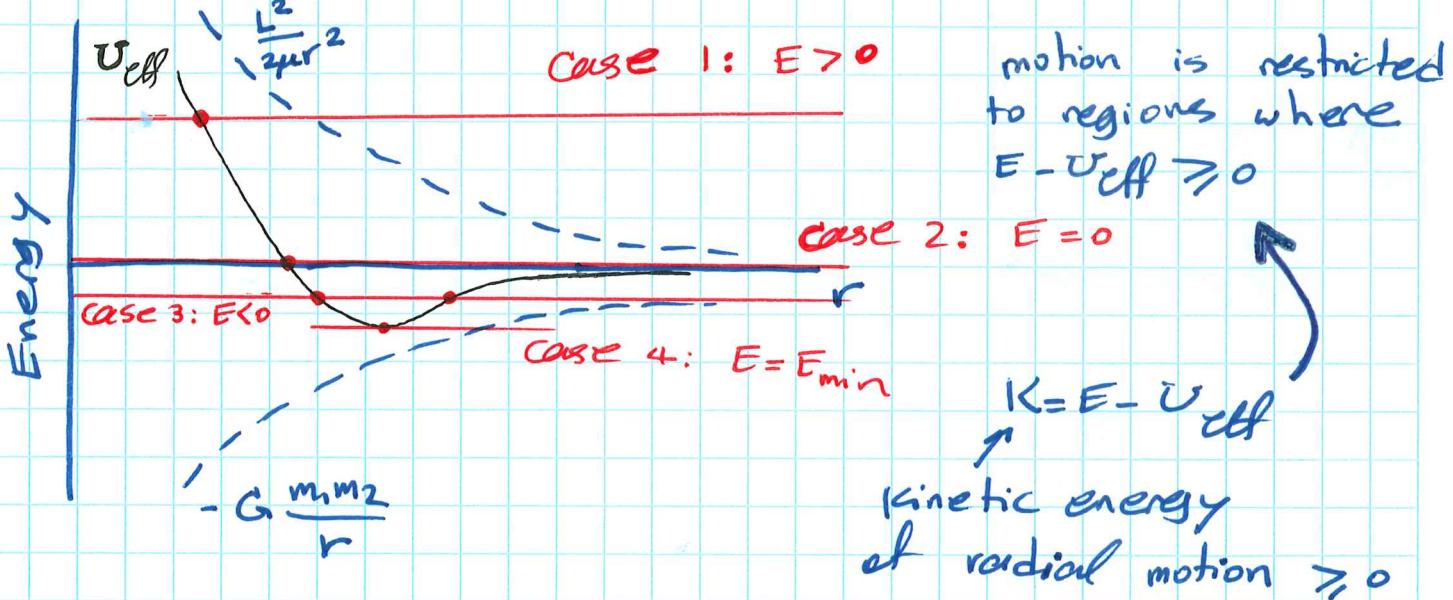
Associating potential  $\rightarrow f(r) = -\frac{dU(r)}{dr}$

$$\Rightarrow U(r) - U(\infty) = - \int_{\infty}^r f(r') dr' = - G \frac{m_1 m_2}{r}$$

$$\text{now } U_{\text{eff}} = \frac{L^2}{2\mu r^2} - G \frac{m_1 m_2}{r}$$

$L=0$ ? collision along a straight line (no barrier)

- $L \neq 0 \rightarrow$ 
  - repulsive centrifugal potential dominates at small  $r$
  - attractive gravitational " " " " " larger  $r$



Case 1:  $r$  is unbounded for large values but cannot be less than a certain minimum  $\rightarrow$  the particles (hyperbola) are kept apart by a "centrifugal barrier."

Case 2: quantitatively similar to case 1 but at the border!

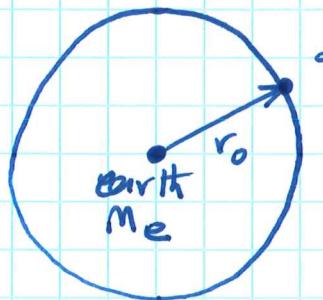
Case 3: the motion is bounded for both small and large  $r$  values. the two particles form a bound system.

Case 4:  $r$  is restricted to one value. particles stay a constant distance from one another.

$E = E_{\min}$   
(circle)

(76)

# Perturbed Circular Orbit



satellite of mass  $m$   
orbit is a circle at radius  $r_0$

At  $t=0$ , one of its engines is fired briefly toward the center of the earth, changing the energy of the satellite but not its angular momentum  $\rightarrow$  find the new orbit.

$M_E \gg m \Rightarrow$  the earth is relatively fixed (the center of mass is near the center of earth!)

If  $E_f$  is not much larger than  $E_i$ , the energy diagram shows that  $r$  never differs from  $r_0$  much.

Approximate  $U_{\text{eff}}(r)$  in the neighborhood of  $r_0$  by a parabola:

$$(\text{drop "eff"}) \quad U(r) \approx U(r_0) + (r-r_0) \frac{dU}{dr} \Big|_{r_0} + \frac{1}{2} (r-r_0)^2 \frac{d^2U}{dr^2} \Big|_{r_0}$$

$$\Rightarrow U(r) \approx U(r_0) + \frac{1}{2} (r-r_0)^2 \frac{d^2U}{dr^2} \Big|_{r_0}$$

$$\frac{d^2U}{dr^2} = \frac{3L^2}{\mu r_0^4} - \frac{2Gm_m m_2}{r_0^3} = K$$

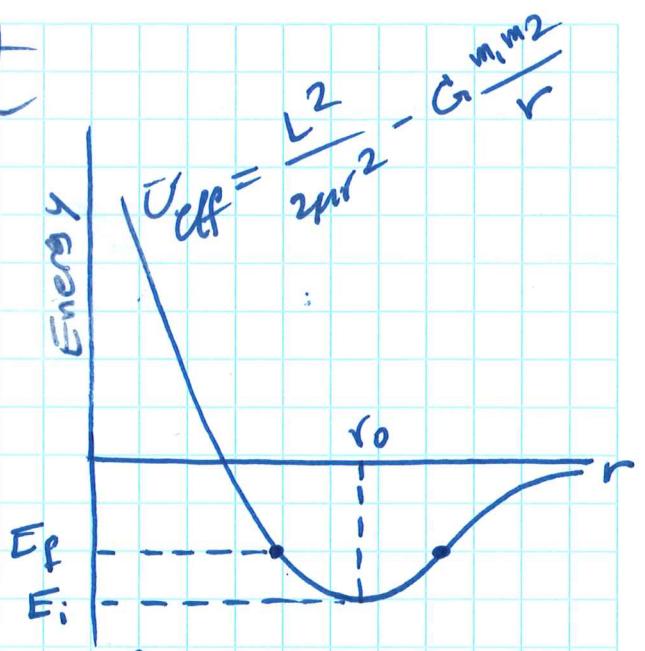
$$K = \frac{Gm_m m_2}{r_0^3}$$

$$\Rightarrow U(r) \approx U(r_0) + \frac{K}{2} (r-r_0)$$

Potential energy of a harmonic oscillator



$$\Rightarrow F(r) = -K(r-r_0)$$



$\Rightarrow$  the system reacts as  $\beta = \frac{L}{\mu r_0^2}$

$$\mu \frac{d^2r}{dt^2} = -K(r - r_0) \xrightarrow{u = r - r_0} \frac{du}{dt} + K u = 0$$

$$B = \sqrt{\frac{K}{\mu}} \quad \text{or} \quad B = \sqrt{\frac{L}{\mu r_0^2}}$$

$$\Rightarrow u = A \sin \beta t + B \cos \beta t \Rightarrow r = r_0 + A \sin \beta t + B \cos \beta t$$

$$\text{at } t=0, r=r_0 \Rightarrow B=0 \Rightarrow r = r_0 + A \sin \beta t$$

$A \ll r_0$  for  $E_f \approx E_i$

To find the new orbit we need  $r$  as a function of  $\theta$ . For a circular orbit:

$$L \approx \mu r_0^2 \dot{\theta} \Rightarrow \dot{\theta} = \frac{L}{\mu r_0^2} \Rightarrow \theta = \frac{L}{\mu r_0^2} t = \beta t$$

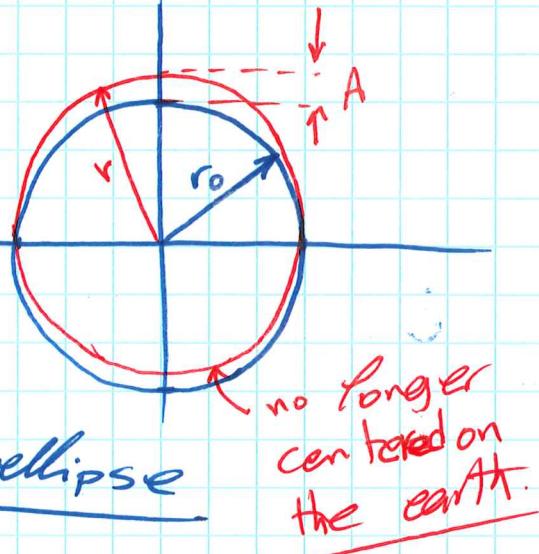
Note: Frequency of rotation is equal to the frequency of radial oscillation.

$$\Rightarrow r = r_0 + A \sin \theta \quad (*)$$

The exact orbit is given by

$$r = \frac{r_0}{1 - \frac{A}{r_0} \sin \theta} \quad \text{an ellipse}$$

$\approx (*)$  for small  $\frac{A}{r_0}$



# 326

- Planetary motion
- Elliptic orbits
- Kepler's first & third laws

Goal: finding the orbit for a planet of mass  $m$  moving about a star of mass  $M$  under interaction.

$$\rightarrow U(r) = -G \frac{mM}{r} = -\frac{C}{r}$$

Recall:  $E = \frac{1}{2}\mu r^2 + U_{\text{eff}}(r)$

$$\Rightarrow \dot{r} = \sqrt{\frac{2}{\mu}(E - U_{\text{eff}})}$$

the results would also apply to a satellite of mass  $m$  orbiting a planet of mass  $M$ , or even a binary star system, Coulomb scattering, ...

$$\Rightarrow \dot{\theta} = \frac{L}{\mu r^2} \quad \Rightarrow \quad \frac{d\theta}{dr} = \frac{d\theta}{dt} \frac{dt}{dr} = \frac{L}{r^2 \sqrt{2\mu(E - U_{\text{eff}})}}$$

$$\Rightarrow \theta - \theta_0 = L \int_{r_0}^r \frac{dr}{r^2 \sqrt{2\mu(E - U_{\text{eff}})}}$$

$$U_{\text{eff}} = \frac{L^2}{2\mu r^2} - \frac{C}{r} \Rightarrow \theta - \theta_0 = L \int_{r_0}^r \frac{dr}{r^2 \sqrt{2\mu(E - \frac{L^2}{2\mu r^2} + \frac{C}{r})}}$$

$$\Rightarrow \theta - \theta_0 = L \int_{r_0}^r \frac{dr}{r \sqrt{2\mu E r^2 - L^2 + 2\mu C r}} \quad *$$

Evaluating the integral  $*$  → see Kleppner Ch 10

$$\text{Let, } \begin{aligned} r_0 &= \frac{L^2}{\mu C} \\ \theta_0 &= -\frac{\pi}{2} \\ E &= \sqrt{1 + \frac{2EL^2}{\mu C^2}} \end{aligned} \Rightarrow r = \frac{\frac{L^2}{(\mu C)}}{1 - \sqrt{1 + \left(\frac{2EL^2}{\mu C^2}\right)} \sin(\theta - \theta_0)}$$

$r$  at  $\theta = \theta_0$  (also, radius of the circular orbit corresponding to  $L, \mu, C$ )

$$\Rightarrow r = \frac{r_0}{1 - e \cos \theta}$$

eccentricity

In Cartesian coordinates:  $r = \sqrt{x^2 + y^2}$ ,  $x = r \cos \theta$

$$\Rightarrow r_0 = r - \epsilon x = \sqrt{x^2 + y^2} - \epsilon x$$

$$\Rightarrow r_0^2 = x^2 + y^2 + \epsilon^2 x^2 - 2\epsilon x$$

$$= (1 - \epsilon^2)x^2 + y^2 + 2\epsilon x^2 - 2\epsilon x$$

$$= 2\epsilon x(\epsilon x - r) \\ - r_0$$

$$= (1 - \epsilon^2)x^2 + y^2 - 2\epsilon r_0 x = r_0^2$$

The shape of the orbit depends on  $\epsilon = \sqrt{1 + \frac{2EL^2}{\mu c^2}}$ .

$$\epsilon > 1 \quad (E > 0) \rightarrow y^2 - Ax^2 - Bx = \text{constant} \quad (\text{hyperbola})$$

$$\epsilon = 1 \quad (E = 0) \rightarrow x = \frac{y^2}{2r_0} - \frac{r_0}{2} \quad (\text{parabola})$$

$$0 < \epsilon < 1 \quad (-\mu c^2 / 2L^2 < E < 0) \rightarrow \text{system is bounded}$$

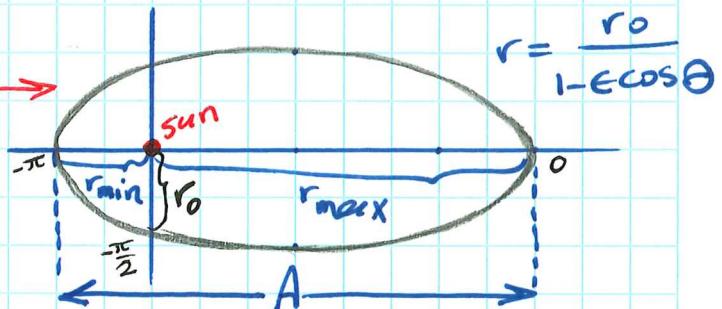
$$y^2 + Ax^2 - Bx = \text{constant} \quad (\text{ellipse})$$

$$\epsilon = 0 \quad (E = -\mu c^2 / 2L^2) \rightarrow x^2 + y^2 = r_0^2 \quad (\text{circle})$$

minimum energy

Elliptic orbits

Kepler's  
first law

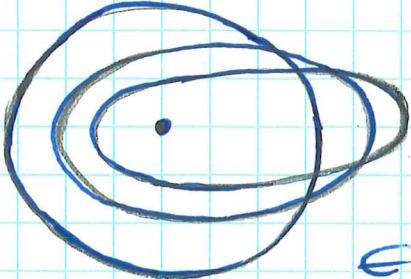


It can be shown that a focus of the ellipse is at the origin (the center of mass)  $\rightarrow$  Solar system? The sun!

The length of the major axis:

$$A = r_{\min} + r_{\max} = \frac{2r_0}{1 - \epsilon^2} = \frac{2 \frac{L^2}{\mu c^2}}{-\frac{2EL^2}{\mu c^2}} = -\frac{C}{E} \quad \text{independent of } L$$

$$r_{\min} = \frac{r_0}{1 + \epsilon}, \quad r_{\max} = \frac{r_0}{1 - \epsilon}$$



All orbits in the sketch correspond to the same value of  $E$  but different  $L$ .

$\epsilon$  is a measure of eccentricity

$\Rightarrow \epsilon = 0 \Rightarrow$  circle

$\epsilon \rightarrow 1 \Rightarrow$  elongated ellipse

$$E = \frac{1}{2} \mu v^2 + U = \frac{1}{2} \mu v^2 - \frac{C}{r}$$

$\uparrow - \frac{C}{A}$

$$\Rightarrow v^2 = \frac{2C}{\mu} \left( \frac{1}{r} - \frac{1}{A} \right)$$

orbital speed  
at any radial position (cool!)

The period of an elliptic orbit

$$\frac{dr}{dt} = \sqrt{\frac{2}{\mu} (E - U_{\text{eff}})} \Rightarrow \frac{dt}{dr} = \frac{\mu r}{\sqrt{2\mu Er^2 - L^2 + 2\mu Cr}}$$

$$\Rightarrow t_b - t_a = \int_{r_a}^{r_b} \frac{dr}{\sqrt{\frac{2\mu Er^2 + 2\mu Cr - L^2}{2E}}} \Big|_{r_a=0}^{r_b}$$

$$- \left( \frac{\mu C}{2E} \right) \frac{1}{\sqrt{-2\mu E}} \sin^{-1} \left( \frac{-2\mu Er - \mu C}{\sqrt{\mu^2 C^2 + 2\mu E L^2}} \right) \Big|_{r_a}^{r_b}$$

$T = t_b - t_a$  (period)

$$\Rightarrow T = \frac{\pi \mu C}{-E} \frac{1}{\sqrt{-2\mu E}} \Rightarrow T^2 = \frac{\pi^2 \mu C^2}{-2E^3}$$

$$\Rightarrow T^2 = \frac{\pi^2 \mu}{2C} A^3$$

using  $A = -\frac{C}{E}$

Kepler's second law

$T^2 = KA^3$  ( $K$  the same for all planets)

(81)

Table 10.1 of Kleppner

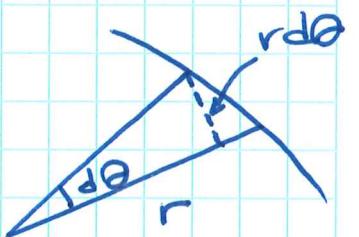
	$E$	$A, \text{ km}$	$T, \text{ s}$	$A^3/T^2$
Mercury	0.206	$1.16 \times 10^8$	$7.62 \times 10^6$	$2.69 \times 10^{10}$
Earth	0.017	$2.99 \times 10^8$	$3.16 \times 10^7$	$2.68 \times 10^{10}$
Mars	0.093	$4.56 \times 10^8$	$5.93 \times 10^7$	$2.7 \times 10^{10}$
Jupiter	0.048	$1.557 \times 10^9$	$3.74 \times 10^8$	$2.69 \times 10^{10}$
Neptune	0.007	$9.05 \times 10^9$	$5.25 \times 10^9$	$2.69 \times 10^{10}$

wow!

A simpler way to calculate the period:

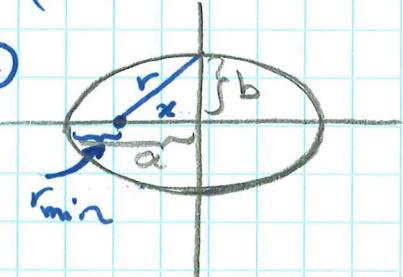
$$L = \mu r^2 \frac{d\theta}{dt} \Rightarrow \frac{L}{2\mu} dt = \frac{1}{2} r^2 d\theta$$

area element  
in polar  
coordinates (see session 23)



$$\Rightarrow \frac{L}{2\mu} dt = dA$$

$$\Rightarrow \frac{L}{2\mu} T = \text{area of ellipse} = \pi a b \quad (*)$$



$$a = \frac{A}{2} = \frac{r_0}{1-e^2} = -\underbrace{\frac{c}{2E}}_{(i)}$$

$$x = a - r_{\min} = \frac{r_0}{1-e^2} - \frac{r_0}{1+e} = \frac{r_0 e}{1-e^2}$$

$$r = \frac{r_0}{1-e\cos\theta} = \frac{r_0}{1-e\frac{x}{r}} \Rightarrow r = r_0 + e x = \frac{r_0}{1-e^2}$$

$$\Rightarrow b = \sqrt{r^2 - x^2} = \frac{r_0}{\sqrt{1-e^2}} = \frac{L}{\sqrt{-2\mu E}} \quad (iii)$$

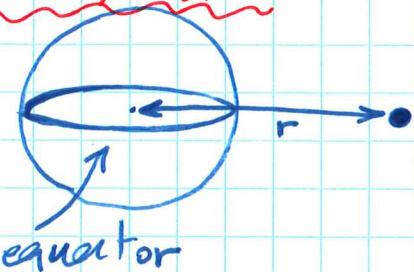
$$(*) : T = \frac{2\mu}{L} \pi a b = \underbrace{\frac{2\mu}{K} \pi}_{\text{K}} \underbrace{\frac{-c}{2E}}_{(ii)} \frac{K}{\sqrt{-2\mu E}} = \frac{-\mu \pi c}{E \sqrt{-2\mu E}}$$

$$\Rightarrow T^2 = \frac{\mu \pi^2}{2c} A^3 \quad \checkmark$$

# 327

- Geostationary orbit
- Satellite orbit transfer

Geostationary orbit



a satellite with orbit in  
the equatorial plane  
(geostationary)

$$A = 2\pi r, \mu \approx m, v = r\Omega_e$$

$$\Rightarrow v^2 = \frac{C}{m} \left( \frac{1}{r} - \frac{1}{2r} \right)$$

$$\Rightarrow r^3 = \frac{C}{m\Omega_e^2} = \frac{g R_e^2}{\Omega_e^2}$$

$$\Omega_e = \frac{2\pi}{24 \times 60 \times 60} = \frac{2\pi}{86400} \frac{\text{rad}}{\text{s}}$$

$$g = 9.8 \text{ m/s}^2, R_e = 6400 \text{ km}$$

$$\Rightarrow r \approx 42250 \text{ km}$$

altitude

$$\Rightarrow h = 42250 - 6400 = \underline{\underline{35850 \text{ km}}}$$

Orbital speed:  $v = r\Omega_e = 3070 \text{ m/s} \approx 6870 \text{ mi/hr}$

Satellite orbit transfer

the most energy efficient approach to put a satellite into circular orbit:

Step 1) launch it into an elliptical transfer orbit whose apogee is at the desired final radius

Step 2) when the satellite is at apogee, it is accelerated tangentially into the circular orbit

for communication purposes,  
the orbital speed is set  
to match the angular velocity  
of the rotating earth,  $\Omega_e$ .  
(satellite is stationary  
above a point on earth)

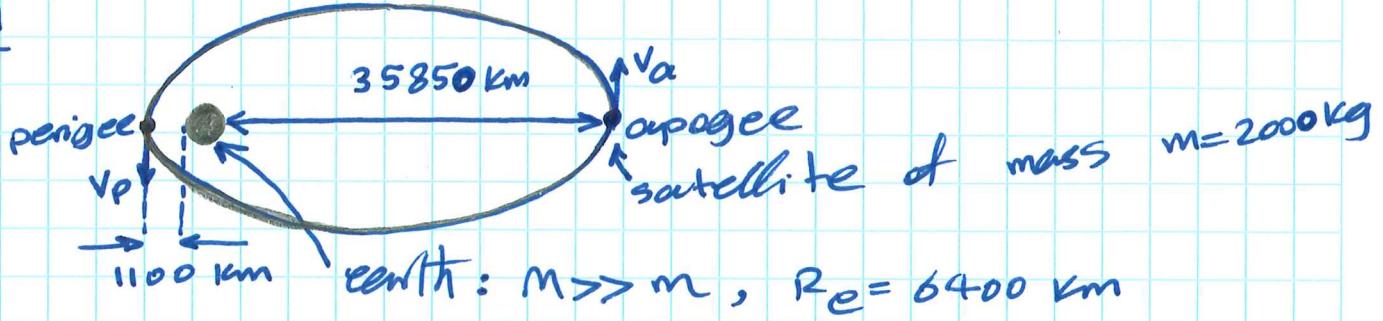
On earth:  $F_{\text{Gravitational}} = -G \frac{mM}{r^2}$

$$= -G \frac{mM}{R_e^2}$$

$$= -mg \Rightarrow g = \frac{GM}{R_e^2}$$

$$\Rightarrow C = GmM = mgR_e^2$$

### Step 1



Suppose that the launching angle, angular momentum, etc. were chosen so that the satellite heights (altitude) at perigee and apogee are 1100 km and 35850 km, respectively.

~~radius of desired geostationary orbit altitude~~

$$E_{\text{Launch}}? \rightsquigarrow E_{\text{ground}} = K_0 + U(R_E)$$

kinetic energy because  
of the earth rotation

$$= \frac{1}{2} m (R_E \Omega_E)^2 - \frac{C}{R_E} = -mgR_E$$

$$\Rightarrow E_{\text{ground}} = -1.25 \times 10^{10} \text{ J}$$

$$A = 1100 + 35850 + 2R_E = 5 \times 10^7 \text{ m}$$

$$\Rightarrow E_{\text{orb}} = - \frac{C}{A} = - \frac{mgR_E^2}{A} = -1.61 \times 10^{10} \text{ J}$$

$\Rightarrow$  the energy needed to launch the satellite:

$$E_{\text{Launch}} = E_{\text{orb}} - E_{\text{ground}} = 1.09 \times 10^{10} \text{ J}$$

$$\epsilon? \rightsquigarrow r = \frac{r_0}{1 - \epsilon \cos \theta} \Rightarrow r_{\min} = \frac{r_0}{1 + \epsilon}, r_{\max} = \frac{r_0}{1 - \epsilon}$$

$$\Rightarrow r_0 = (1 + \epsilon)r_{\min} = (1 - \epsilon)r_{\max} \rightsquigarrow \epsilon = \frac{r_{\max} - r_{\min}}{r_{\max} + r_{\min}}$$

$\rightarrow \epsilon = 0.7$

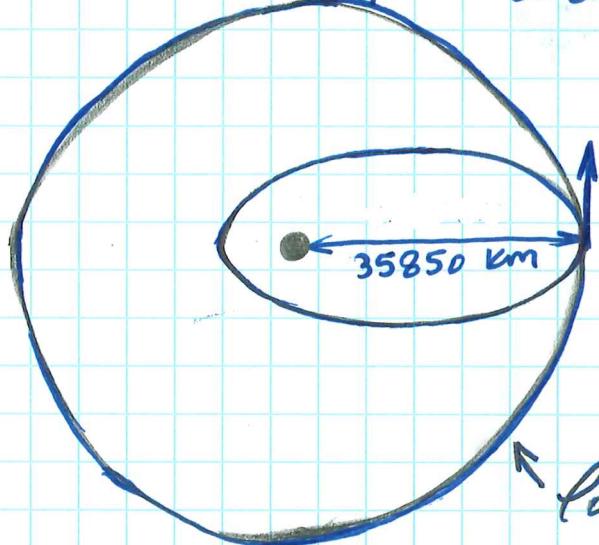
$$L=? \rightsquigarrow \epsilon = \sqrt{1 + \frac{2EL^2}{mc^2}} \rightsquigarrow L = 1.43 \times 10^{14} \frac{\text{kg} \cdot \text{m}^2}{\text{s}}$$

$v_p$  and  $v_\alpha$ ?

At the perigee and apogee:  $r_p = 1100 + 6400 = 7.5 \times 10^6 \text{ m}$   
 $r_\alpha = 35850 + 6400 = 4.225 \times 10^7 \text{ m}$

$$L = mr_p v_p = mr_\alpha v_\alpha \Rightarrow v_p = 9530 \text{ m/s} = 21300 \text{ mi/hr}$$

$$v_\alpha = 1690 \text{ m/s} = 3800 \text{ mi/hr}$$



The engine gives a burst to increase the speed from  $v_\alpha = 1690 \text{ m/s}$  to  $v = 3070 \text{ m/s}$  (the geostationary speed at altitude 35850 km)

looks like a potato!

desired  
geostationary  
orbit

$$\Delta E = -C \left( \frac{1}{A_f} - \frac{1}{A_i} \right) = -mgR_e^2 \left( \frac{1}{A_f} - \frac{1}{A_i} \right)$$

$$A_i = 5.0 \times 10^7 \text{ m}, A_f = 2 \times (35850 + 6400) \text{ km} = 8.45 \times 10^7 \text{ m}$$

$\Delta E = 6.6 \times 10^9 \text{ J}$

$$E_i \rightarrow E_f$$

$$-16.1 \times 10^9 \text{ J} \quad -9.5 \times 10^9 \text{ J}$$

Similar considerations apply when a spacecraft on a space mission returns to earth:

Step 1) The spacecraft is slowed enough to be captured in a circular orbit.

Step 2) Then it is transferred to an elliptic orbit that intersects the Earth.