

Ans 1:

$$\Delta H_{rxn} = \sum v_i \Delta H_f^P - \sum v_i \Delta H_f^R$$

$$C-H = 414 \text{ kJ/mol}$$

$$C-C = 347 \text{ kJ/mol}$$

$$C-Cl = 377 \text{ kJ/mol}$$

$$Cl-Cl = 243 \text{ kJ/mol}$$

$$H-Cl = 431 \text{ kJ/mol}$$

$$\begin{aligned}\Delta H &= 5(C-H) + (C-Cl) + (Cl-Cl) - 4(C-H) - 2(C-Cl) - (H-Cl) \\ &= 5 \times 414 + 377 + 243 - 4 \times 414 - 2 \times 377 - 431 \\ &= -757 \text{ kJ/mol}\end{aligned}$$

Ans 2:

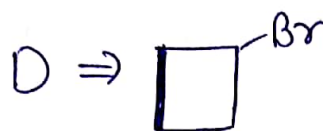
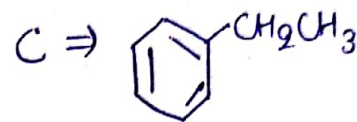
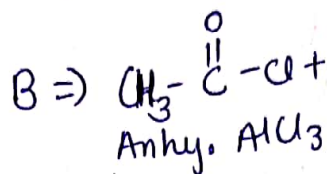
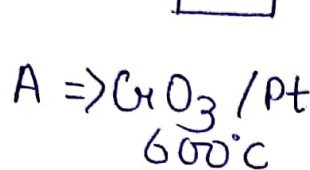
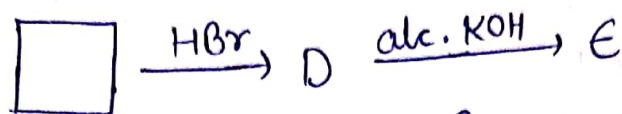
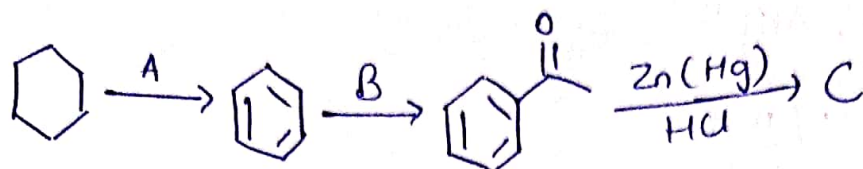
### Bulk Polymerization

- Due to absence of solvent the mixture becomes highly viscous which ~~cause~~ difficulty in stirring.
- Due to high viscosity, chain termination is difficult.
- We obtain polymer of high molecular wt. distribution.
- The reaction is too vigorous that sometimes lead to explosion area.
- Polymer of high quality is obtained.
- No separation is required.
- We are not using any solvent so process is economical.

### Solution Polymerization

- Due to presence of solvent, the mixture is not so much viscous therefore can be stirred easily.
- Chain termination is easier.
- No molecular distribution. Almost same type of polymer are made.
- Presence of solvent enables dissipation of heat so chances of explosion are reduced.
- Polymer are not pure.
- Separation of solvent and polymer is needed.
- Not so economical.

Ans 3:



Ans 4:

$$K_2 = 10000 \text{ s}^{-1}$$

$$K_1 = 4500 \text{ s}^{-1}$$

$$E_a = 58000 \text{ J/mol}$$

$$T_1 = 1^\circ\text{C} = 274 \text{ K}$$

$$R = 8.314$$

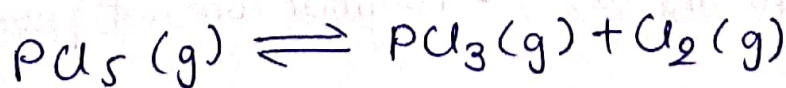
$$\log \left[ \frac{K_2}{K_1} \right] = \frac{E_a}{2.303R} \left[ \frac{1}{T_1} - \frac{1}{T_2} \right]$$

$$\log \left[ \frac{10000}{4500} \right] = \frac{58000}{2.303 \times 8.314} \left[ \frac{1}{274} - \frac{1}{T_2} \right]$$

$$0.347 = 3019.22 \left[ \frac{1}{274} - \frac{1}{T_2} \right]$$

$$T_2 = 286.53 \text{ K}$$

Ans 5:



moles at $t=0$	0.1	0	0
at $t=t$	$0.1-x$	$x$	$x$

$$K_c = \frac{[\text{PCl}_3][\text{Cl}_2]}{[\text{PCl}_5]}$$



$$K_c = \frac{[x/5][x/5]}{[0.1-x/5]}$$

$$\left\{ c = \frac{\text{moles}}{\text{volume}} \right\}$$

$$1.8 \times 5 = \frac{x^2}{0.1-x}$$

$$9 = \frac{x^2}{0.1-x}$$

$$x^2 + 9x - 0.9 = 0$$

$$x = \frac{-9 \pm \sqrt{81+3.6}}{2}$$

$$x = \frac{-9 \pm 9.19}{2}$$

$$x = \frac{-9 + 9.19}{2}, \quad x = \frac{-9 - 9.19}{2} \text{ (Not valid)}$$

$$\boxed{x = 0.095}$$

$$[PCl_5] = \frac{0.1 - 0.095}{5} = \frac{0.005}{5} = 0.001 \text{ mol/L or M}$$

$$[PCl_3][Cl_2] = \frac{0.095}{5} = 0.019 \text{ mol/L or M}$$

$$\text{Ans 6: } M_n = \frac{\sum N_i M_i}{\sum N_i} = \frac{100 \times 1000 + 200 \times 2000 + 300 \times 3000}{100 + 200 + 300}$$

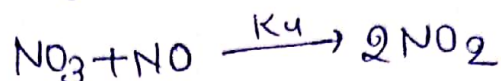
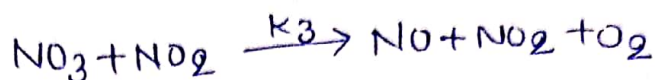
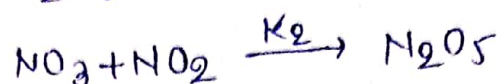
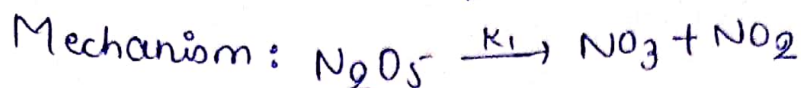
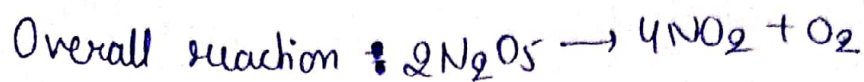
$$\boxed{M_n = 3.33 \times 10^3}$$

$$M_w = \frac{\sum N_i M_i^2}{\sum N_i M_i} = \frac{100 \times (1000)^2 + 200 \times (2000)^2 + 300 \times (3000)^2}{100 \times 1000 + 200 \times 2000 + 300 \times 3000}$$

$$\boxed{M_w = 4.2 \times 10^3}$$

$$PDI = \frac{M_w}{M_n} = 1.26$$

Ans:



$$\begin{aligned} \frac{d[\text{NO}_2]}{dt} &= k_1[\text{N}_2\text{O}_5] - k_2[\text{NO}_3][\text{NO}_2] - k_3[\text{NO}_3][\text{NO}_2] + k_4[\text{NO}_3][\text{NO}_2] \\ &= k_1[\text{N}_2\text{O}_5] + k_4[\text{NO}_3][\text{NO}_2] - (k_3 + k_2)[\text{NO}_3][\text{NO}_2] \quad \text{--- (1)} \end{aligned}$$

$$\frac{d[\text{NO}_3]}{dt} = 0 = k_1[\text{N}_2\text{O}_5] - k_2[\text{NO}_3][\text{NO}_2] - k_3[\text{NO}_3][\text{NO}_2]$$

$$[\text{NO}_3] = \frac{k_1[\text{N}_2\text{O}_5]}{(k_2 + k_3)[\text{NO}_2]} \quad \text{--- (2)}$$

from (1) & (2)

$$\begin{aligned} \frac{d[\text{NO}_2]}{dt} &= k_1[\text{N}_2\text{O}_5] + \frac{k_4 \cdot k_1[\text{N}_2\text{O}_5][\text{NO}_2]}{(k_2 + k_3)[\text{NO}_2]} - \frac{(k_2 + k_3) k_1[\text{N}_2\text{O}_5][\text{NO}_2]}{(k_2 + k_3)[\text{NO}_2]} \\ &= \frac{k_4 \cdot k_1[\text{N}_2\text{O}_5][\text{NO}_2]}{(k_2 + k_3)[\text{NO}_2]} \quad \text{--- (3)} \end{aligned}$$

$$\frac{d[\text{NO}]}{dt} = 0 = k_3[\text{NO}_3][\text{NO}_2] - k_4[\text{NO}_3][\text{NO}]$$

$$[\text{NO}] = \frac{k_3}{k_4} [\text{NO}_2] \quad \text{--- (4)}$$

from (3) & (4)

$$\frac{d[\text{NO}_2]}{dt} = \frac{k_4 \cdot k_1[\text{N}_2\text{O}_5]}{(k_2 + k_3)[\text{NO}_2]} \cdot \frac{k_3}{k_4} [\text{NO}_2]$$

$$\boxed{\frac{d[\text{NO}_2]}{dt} = \left( \frac{k_3 k_1}{k_2 + k_3} \right) [\text{N}_2\text{O}_5]}$$



Ans 8

1(i) Composition of components

$$H_2 (30\%) = 0.3 m^3$$

$$CH_4 (5\%) = 0.05 m^3$$

$$CO (20\%) = 0.2 m^3$$

$$O_2 (5\%) = 0.05 m^3$$

Volume of  $O_2$  needed

$$0.3 \times 0.5 = 0.15 m^3$$

$$0.05 \times 0.2 = 0.01 m^3$$

$$0.2 \times 0.5 = 0.1 m^3$$

$$\text{Total} = 0.35 m^3$$

$$\text{less } O_2 \text{ in fuel gas} = -0.05 m^3$$

$$\text{Net } O_2 \text{ needed} = 0.3 m^3$$

$$= 300 L$$

Volume of air required for  $1 m^3$  of gas using 50% excess air

$$= 300 \times \frac{100}{21} \times \frac{150}{100}$$

$$= 2142.8 L$$

Hence, weight of air actually supplied per  $m^3$  of the gas

$$= 2142.8 L \times \left( \frac{1 \text{ mol}}{22.4 L} \right) \times \left( \frac{28.97 \text{ gm}}{\text{mol}} \right)$$

$$= 2771 \text{ gm}$$

Ans 8

1(ii)  $x = w_1 = 1.6 g$

$$w_2 = 1.42 g$$

$$w_3 = 0.98 g$$

$$w_4 = 0.41 g$$

$$\% \text{ moisture} = \frac{w_1 - w_2}{x} \times 100 = \frac{1.6 - 1.42}{1.6} \times 100$$

$$= 11.25 \%$$

$$\% \text{ Vm} = \frac{w_2 - w_3}{x} \times 100 = \frac{1.42 - 0.98}{1.40} \times 100$$

$$= 27.5 \%$$

$$\% \text{ ash} = \frac{w_4}{x} \times 100 = \frac{0.41}{1.6} \times 100 = 25.625 \%$$

$$\begin{aligned}\text{Fixed Carbon} &= 100 - \% (\text{Moisture} + \text{V.M} + \text{ash}) \\ &= 100 - \% (11.25 + 27.5 + 25.625) \\ &= 35.625 \%\end{aligned}$$

Q8 ~~2(i)~~ 2(i) weight of fuel ( $x$ ) = (weight of the crucible + fuel) - (weight of crucible)

$$= 3.58 - 2.34$$

$$x = 1.24 \text{ g}$$

$$A = 6500 \text{ g}$$

$$W = 2200 \text{ g}$$

$$T_2 - T_1 = 4.24^\circ\text{C}$$

$$C.C = 0.048^\circ\text{C}$$

$$A.C = 60 \text{ cal}$$

$$\begin{aligned}G.C.V &= \frac{\{ (A+W) \times S.W \times (T_f - T_i + C.C) \} - \{ F.C + \text{Cotton Correction} + A.C \}}{x} \\ &= \frac{\{ (6500 + 2200) \times 1 \times (4.24 + 0.048) \} - 60}{1.24}\end{aligned}$$

$$G.C.V = 9807.097 \text{ cal/g}$$

$$\% H = 4\%$$

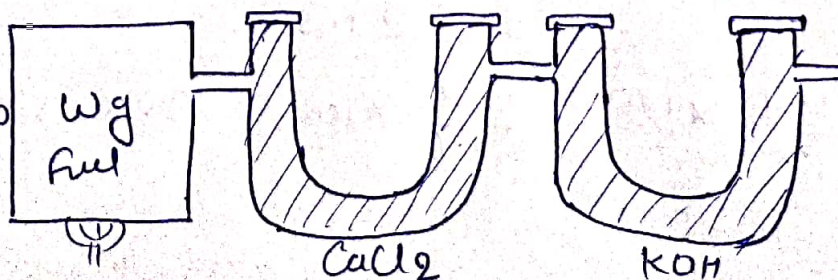
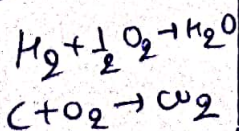
$$G.C.V = N.C.V + 0.09H \times 587$$

$$N.C.V = G.C.V - (0.09H \times 587)$$

$$N.C.V = 9807.097 - (0.09 \times 4 \times 587)$$

$$N.C.V = 9595.777 \text{ cal/g}$$

Ans 8 2(ii)

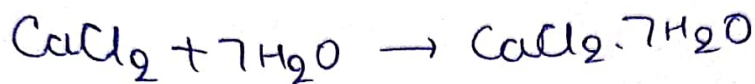




Before passing the gas

$$\begin{cases} \text{wt of U-tube with CaCl}_2 = w_1 g \\ \text{wt of U-tube with KOH} = w_2 g \end{cases}$$

After passing the gas (CO<sub>2</sub> + H<sub>2</sub>O)

$$\begin{cases} \text{wt of CaCl}_2 \text{ U-tube} = w_3 g \\ \text{wt of KOH tube} = w_4 g \end{cases}$$


% H = increase in wt(g)

$$\frac{\text{CaCl}_2 \text{ tube}}{w} \times \frac{2}{18} \times 100$$

% C = increase in wt(g)

$$\frac{\text{KOH tube}}{w} \times \frac{12}{44} \times 100$$