

## HEAT & THERMODYNAMICS

$$\text{Total translational K.E. of gas} = \frac{1}{2} M \langle V^2 \rangle = \frac{3}{2} PV = \frac{3}{2} nRT$$

$$\langle V^2 \rangle = \frac{3P}{\rho} \quad V_{\text{rms}} = \sqrt{\frac{3P}{\rho}} = \sqrt{\frac{3RT}{M_{\text{mol}}}} = \sqrt{\frac{3KT}{m}}$$

**Important Points :**

$$- V_{\text{rms}} \propto \sqrt{T} \quad \bar{V} = \sqrt{\frac{8KT}{\pi m}} = 1.59 \sqrt{\frac{KT}{m}} \quad V_{\text{rms}} = 1.73 \sqrt{\frac{KT}{m}}$$

$$\text{Most probable speed } V_p = \sqrt{\frac{2KT}{m}} = 1.41 \sqrt{\frac{KT}{m}} \quad \therefore V_{\text{rms}} > \bar{V} > V_{\text{mp}}$$

**Degree of freedom :**

Mono atomic  $f = 3$

Diatomic  $f = 5$

polyatomic  $f = 6$

**Maxwell's law of equipartition of energy :**

Total K.E. of the molecule =  $\frac{1}{2} f KT$

For an ideal gas :

$$\text{Internal energy } U = \frac{f}{2} nRT$$

$$\text{Workdone in isothermal process :} \quad W = [2.303 nRT \log_{10} \frac{V_f}{V_i}]$$

$$\text{Internal energy in isothermal process :} \quad \Delta U = 0$$

$$\text{Work done in isochoric process :} \quad dW = 0$$

**Change in int. energy in isochoric process :**

$$\Delta U = n \frac{f}{2} R \Delta T = \text{heat given}$$

**Isobaric process :**

$$\text{Work done } \Delta W = nR(T_f - T_i)$$

$$\text{change in int. energy } \Delta U = nC_v \Delta T$$

$$\text{heat given } \Delta Q = \Delta U + \Delta W$$

$$\text{Specific heat :} \quad C_v = \frac{f}{2} R \quad C_p = \left( \frac{f}{2} + 1 \right) R$$

## Molar heat capacity of ideal gas in terms of R :

(i) for monoatomic gas :  $\frac{C_p}{C_v} = 1.67$

(ii) for diatomic gas :  $\frac{C_p}{C_v} = 1.4$

(iii) for triatomic gas :  $\frac{C_p}{C_v} = 1.33$

**In general :**  $\gamma = \frac{C_p}{C_v} = \left[ 1 + \frac{2}{f} \right]$

Mayer's eq.  $\Rightarrow C_p - C_v = R$  for ideal gas only

## Adiabatic process :

Work done  $\Delta W = \frac{nR(T_i - T_f)}{\gamma - 1}$

## In cyclic process :

$$\Delta Q = \Delta W$$

## In a mixture of non-reacting gases :

$$\text{Mol. wt.} = \frac{n_1 M_1 + n_2 M_2}{n_1 + n_2}$$

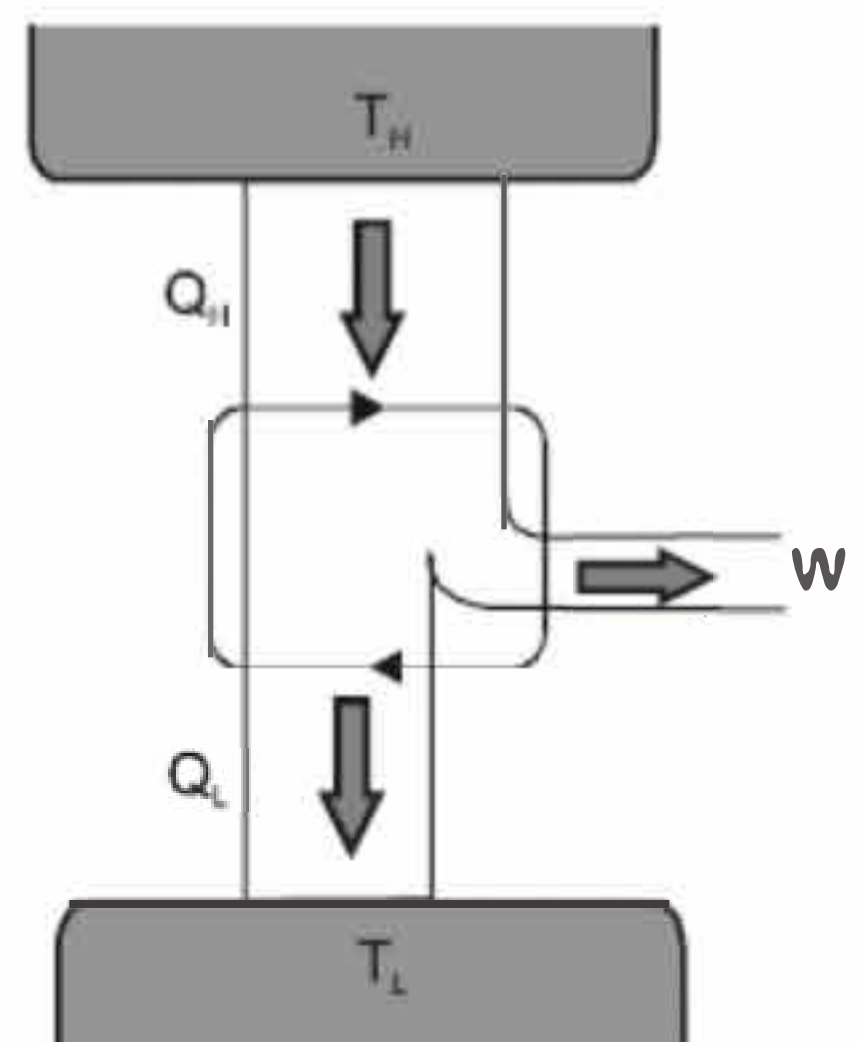
$$C_v = \frac{n_1 C_{v_1} + n_2 C_{v_2}}{n_1 + n_2}$$

$$\gamma = \frac{C_{p(\text{mix})}}{C_{v(\text{mix})}} = \frac{n_1 C_{p_1} + n_2 C_{p_2} + \dots}{n_1 C_{v_1} + n_2 C_{v_2} + \dots}$$

## Heat Engines

Efficiency,  $\eta = \frac{\text{work done by the engine}}{\text{heat supplied to it}}$

$$= \frac{W}{Q_H} = \frac{Q_H - Q_L}{Q_H} = 1 - \frac{Q_L}{Q_H}$$



## Second law of Thermodynamics

### • Kelvin- Planck Statement

It is impossible to construct an engine, operating in a cycle, which will produce no effect other than extracting heat from a reservoir and performing an equivalent amount of work.

### • Rudlope Classius Statement

It is impossible to make heat flow from a body at a lower temperature to a body at a higher temperature without doing external work on the working substance

## Entropy

• change in entropy of the system is  $\Delta S = \frac{\Delta Q}{T} \Rightarrow S_f - S_i = \int_i^f \frac{\Delta Q}{T}$

• In an adiabatic reversible process, entropy of the system remains constant.

## Efficiency of Carnot Engine

(1) Operation I (Isothermal Expansion)

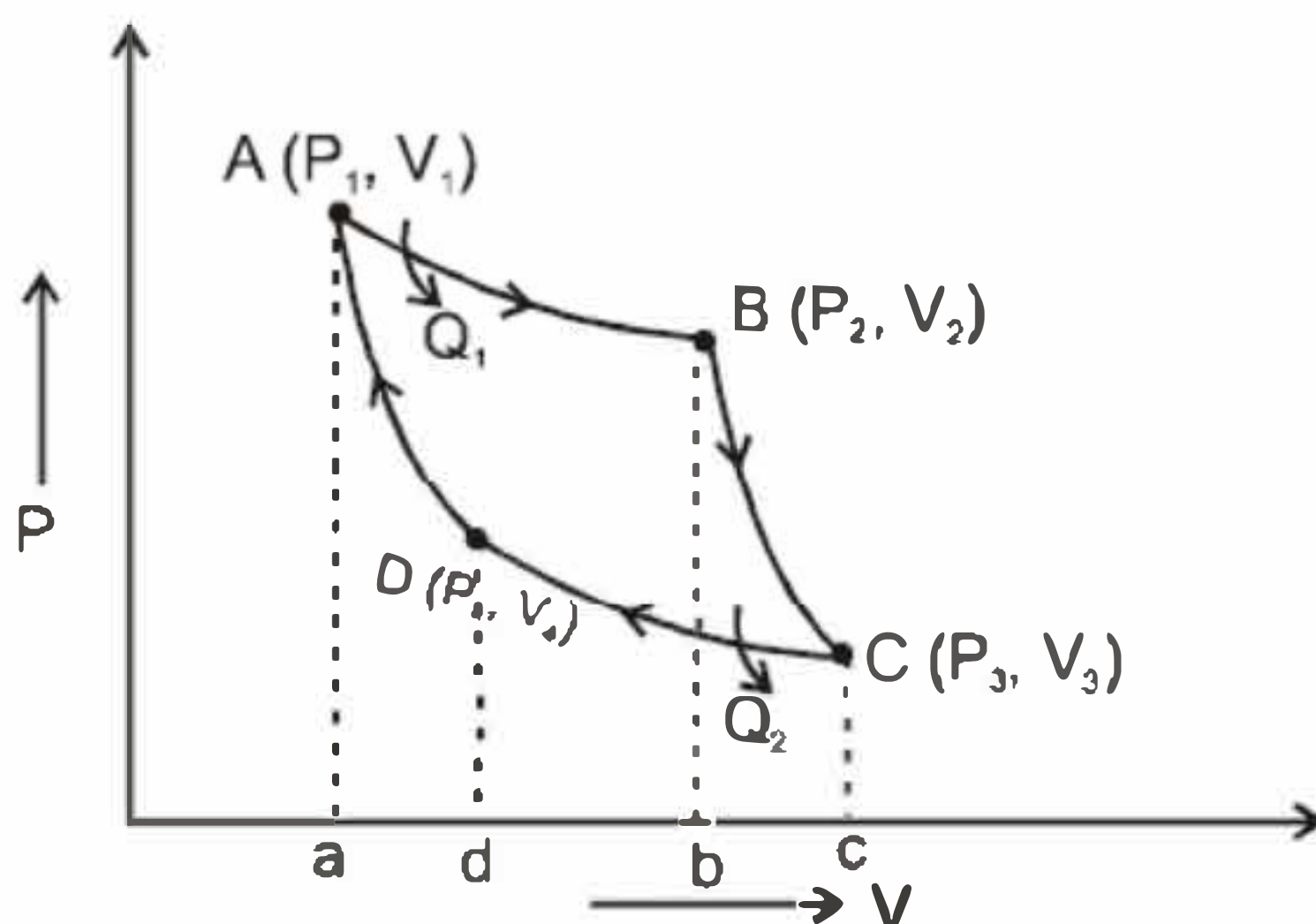
(2) Operation II (Adiabatic Expansion)

(3) Operation III (Isothermal Compression)

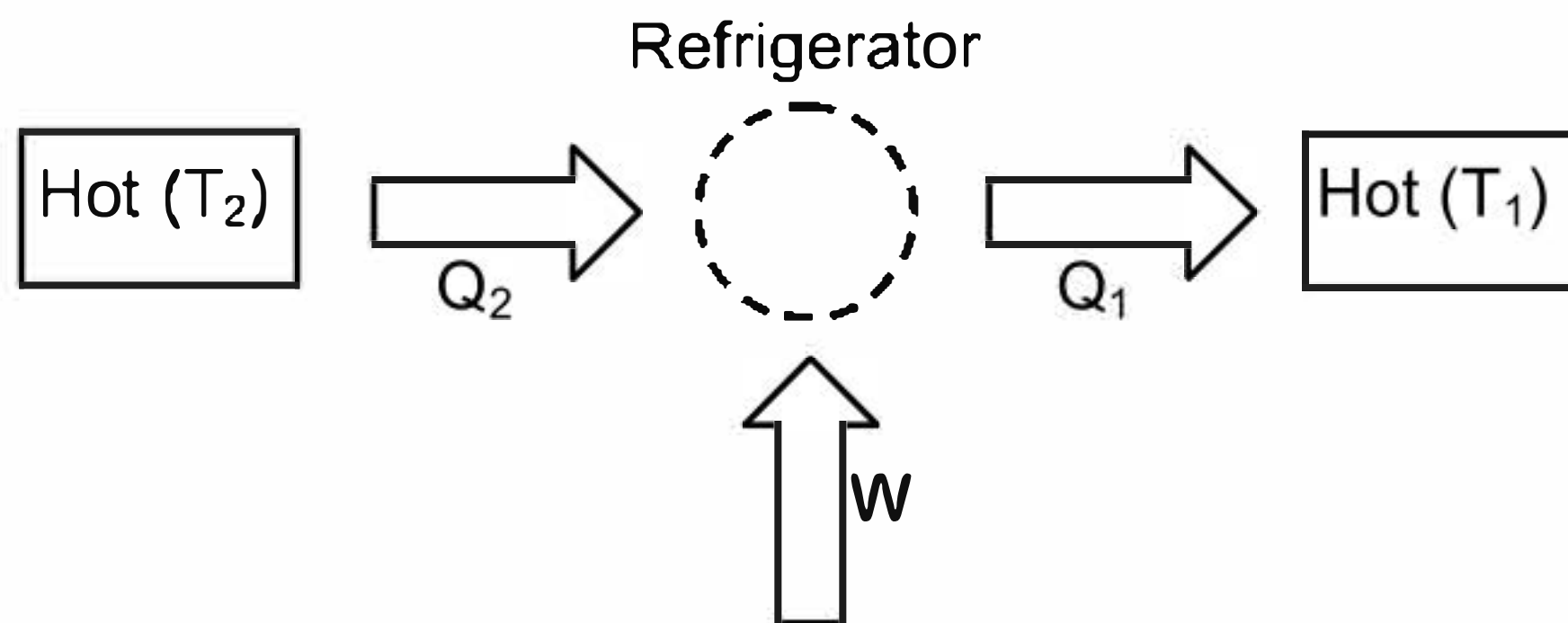
(4) Operation IV (Adiabatic Compression)

## Thermal Efficiency of a Carnot engine

$$\frac{V_2}{V_1} = \frac{V_3}{V_4} \Rightarrow \frac{Q_2}{Q_1} = \frac{T_2}{T_1} \Rightarrow \eta = 1 - \frac{T_2}{T_1}$$



## Refrigerator (Heat Pump)



- Coefficient of performance,  $\beta = \frac{Q_2}{W} = \frac{1}{\frac{T_1}{T_2} - 1} = \frac{1}{\frac{T_1}{T_2} - 1}$

## Calorimetry and thermal expansion

### Types of thermometers :

(a) Liquid Thermometer : 
$$T = \left[ \frac{\ell - \ell_0}{\ell_{100} - \ell_0} \right] \times 100$$

(b) Gas Thermometer :

Constant volume : 
$$T = \left[ \frac{P - P_0}{P_{100} - P_0} \right] \times 100 \quad ; \quad P = P_0 + \rho g h$$

Constant Pressure : 
$$T = \left[ \frac{V}{V - V'} \right] T_0$$

(c) Electrical Resistance Thermometer :

$$T = \left[ \frac{R_t - R_0}{R_{100} - R_0} \right] \times 100$$

### Thermal Expansion :

(a) Linear :

$$\alpha = \frac{\Delta L}{L_0 \Delta T} \quad \text{or} \quad L = L_0 (1 + \alpha \Delta T)$$

**(b) Area/superficial :**

$$\beta = \frac{\Delta A}{A_0 \Delta T} \quad \text{or} \quad A = A_0 (1 + \beta \Delta T)$$

**(c) volume/ cubical :**

$$\gamma = \frac{\Delta V}{V_0 \Delta T} \quad \text{or} \quad V = V_0 (1 + \gamma \Delta T)$$

$$\boxed{\alpha = \frac{\beta}{2} = \frac{\gamma}{3}}$$

**Thermal stress of a material :**

$$\frac{F}{A} = Y \frac{\Delta \ell}{\ell}$$

**Energy stored per unit volume :**

$$E = \frac{1}{2} K (\Delta L)^2 \quad \text{or} \quad E = \frac{1}{2} \frac{AY}{L} (\Delta L)^2$$

**Variation of time period of pendulum clocks :**

$$\Delta T = \frac{1}{2} \alpha \Delta \theta T$$

$T' < T$  - clock-fast : time-gain

$T' > T$  - clock slow : time-loss

**CALORIMETRY :**

$$\text{Specific heat } S = \frac{Q}{m \cdot \Delta T}$$

$$\text{Molar specific heat } C = \frac{\Delta Q}{n \cdot \Delta T}$$

$$\text{Water equivalent} = m_w S_w$$

**HEAT TRANSFER**

$$\text{Thermal Conduction :} \quad \frac{dQ}{dt} = -KA \frac{dT}{dx}$$

$$\text{Thermal Resistance :} \quad R = \frac{\ell}{KA}$$

### Series and parallel combination of rod :

(i) **Series :**  $\frac{\ell_{eq}}{K_{eq}} = \frac{\ell_1}{K_1} + \frac{\ell_2}{K_2} + \dots$  (when  $A_1 = A_2 = A_3 = \dots$ )

(ii) **Parallel :**  $K_{eq} A_{eq} = K_1 A_1 + K_2 A_2 + \dots$  (when  $\ell_1 = \ell_2 = \ell_3 = \dots$ )

for absorption, reflection and transmission

$$r + t + a = 1$$

**Emissive power :**  $E = \frac{\Delta U}{\Delta A \Delta t}$

**Spectral emissive power :**  $E_\lambda = \frac{dE}{d\lambda}$

**Emissivity :**  $e = \frac{\text{E of a body at T temp.}}{\text{E of a black body at T temp.}}$

**Kirchoff's law :**  $\frac{E(\text{body})}{a(\text{body})} = E(\text{black body})$

**Wein's Displacement law :**  $\lambda_m \cdot T = b$   
 $b = 0.282 \text{ cm-k}$

**Stefan Boltzmann law :**

$$u = \sigma T^4 \quad s = 5.67 \times 10^{-8} \text{ W/m}^2 \text{ K}^4$$
$$\Delta u = u - u_0 = e \sigma A (T^4 - T_0^4)$$

**Newton's law of cooling :**  $\frac{d\theta}{dt} = k (\theta - \theta_0) ; \quad \theta = \theta_0 + (\theta_i - \theta_0) e^{-kt}$