

Notes on Fluids and Plasmas in Astrophysics

1 Lecture 1 - 17/09/2019

A fluid

- flows (yes... indeed)
- is typically a liquid or a gas
- is composed of electrically neutral atoms or molecules.

The fluid model of a system is a macroscopic description of a system as a manifold in which macroscopic forces act.

The fluid description of a system is a valid one if the mean free path of it's constituents is much smaller than the characteristic length of the system.

$$\lambda_c \ll L$$

2 Lecture 2 - 19/09/2019

Most fluids present some resistance to stress and are therefore viscous. If this does not happen that fluid is called an **ideal fluid**.

2.1 Derivatives

We start by establishing some notation.

2.2 Eulerian Derivative

The Eulerian derivative describe the change of a variable with respect to time for a fixed point in space. It can be identified as a partial time derivative.

2.3 Lagrangian Derivative

The Lagrangian derivative describes the change of a variable with respect to both physical and temporal displacement. It can be identified with a total derivative.

$$dQ = \frac{\partial Q}{\partial t} dt + \frac{\partial Q}{\partial x} dx + \frac{\partial Q}{\partial y} dy + \frac{\partial Q}{\partial z} dz = \frac{\partial Q}{\partial t} dt + (d\vec{r} \cdot \nabla) Q$$

In particular, if one is describing a change in velocity, one may write

$$\frac{d\vec{v}}{dt} = \frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v}$$

2.4 Conservation Laws

Let V be an element of fluid limited by a surface S . The flux through an oriented element of surface $d\vec{S}$ is given by

$$\frac{\partial}{\partial t} \int_V \rho dV = - \oint_S \rho \vec{v} \cdot \vec{n} dS$$

By the divergence theorem we have

$$\int_V \left[\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) \right] dV = 0$$

and follows the continuity equation

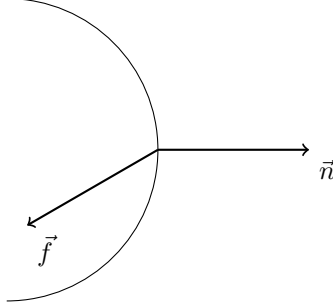
$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) = 0 \quad (1)$$

2.5 Equation of Motion

Let δV be an element of fluid of mass $\rho \delta V$. From Newton's second law

$$\rho \delta V \frac{\partial \vec{v}}{\partial t} = \delta \vec{F}_{\text{volume}} + \delta \vec{F}_{\text{surface}}$$

Let \vec{f} be a volumetric force density per unit mass (also called acceleration density). We have the relation $\delta \vec{F}_{\text{volume}} = \rho \delta V \vec{f}$. It is then natural to define a **total pressure** tensor P_{ij} ¹ that can be interpreted as the component i of the pressure exerted in a surface of normal vector component j .



Then we have

$$\vec{f}_{\text{surface}} = \int_S d\vec{f}_{\text{surface}} = \oint_S P_{ij} dS_j$$

Applying the diverge theorem in the right side

$$\oint_S P_{ij} dS_j = \int_V \frac{\partial P_{ij}}{\partial x_j} dV_i$$

As the tensor is defined positively in the outwards direction, we add a negative sign for convenience. We then get the relation

$$\rho \frac{d\vec{v}}{dt} = \rho \vec{f} - \nabla \cdot p \quad (2)$$

¹We study fluids exclusively in euclidean geometry, that means $g_{\mu\nu} = \delta_{\mu\nu}$. To keep the notes as comprehensible as possible, we make no distinction between covariant and contravariant entities, and all indices will be written as subscripts.

3 Lecture 3 - 24/09/2019

3.1 Fluid in Static Equilibrium

For a fluid in static equilibrium ($v = 0$), the force that acts on an element of area is perpendicular to its normal vector. That is

$$P_{ij} = p\delta_{ij} \quad (3)$$

We may now give an alternative definition of a fluid, as a substance for which movement is induced whenever a superficial force with an tangential component (also called a *shear force*) is exerted.

In this case, from equation 2 follows

$$dF_{\text{sup}} = -p dS$$

However, one may not forget that the relation 3 is no longer true for a fluid in motion. One should expect a shear force to carry momentum from the faster layers of fluid to the slower ones. These shear forces are described expressed through a **viscosity coefficient**. In other words, equation 3 is only true for non-viscous (ideal) fluids.

3.2 Ideal Fluids

For an ideal fluid the equation of motion reduces to

$$\rho \frac{d\vec{v}}{dt} = -\nabla p + \rho \vec{f}$$

which may be rewritten as

$$\rho \frac{\partial \vec{v}}{\partial t} + \rho(\vec{v} \cdot \nabla) \vec{v} = -\nabla p + \rho \vec{f} \quad (4)$$

3.3 Equation of Energy

Remembering the **First Law of Thermodynamics**

$$dQ = dU + p dV \quad (5)$$

we aim to apply it to a fluid in motion.

We start by noticing that a sufficiently small element of fluid is trivially in thermodynamic equilibrium. Let δm be the mass of an element of fluid. Let also $dq = \frac{dQ}{\delta m}$ and $d\epsilon = \frac{du}{\delta m}$. Then

$$\frac{dq}{dt} = \frac{d\epsilon}{dt} + p \frac{d}{dt} \left(\frac{1}{\rho} \right)$$

From equation 1

$$p \frac{d}{dt} \left(\frac{1}{\rho} \right) = -\frac{p}{\rho^2} \frac{d\rho}{dt} = \frac{p}{\rho} \nabla \cdot \vec{v}$$

Substituting

$$\rho \frac{d\epsilon}{dt} + p \nabla \cdot \vec{v} = \rho \frac{dq}{dt}$$

If one defines

$$-\mathcal{L} = \rho \frac{dq}{dt} \quad (6)$$

the relation simplifies to

$$\rho \frac{d\epsilon}{dt} + p \nabla \cdot \vec{v} = -\mathcal{L} \quad (7)$$

If the variations of heat are a case of simply **heat flux**

$$\mathcal{F} = -k \nabla T$$

with k being the thermal conductivity coefficient. \mathcal{F} is related to \mathcal{L} through

$$\mathcal{L} = \nabla \cdot \mathcal{F} = -\nabla \cdot (k \nabla T)$$

Substituting in equation 7

$$\rho \left(\frac{\partial \epsilon}{\partial t} + (\vec{v} \cdot \nabla) \epsilon \right) + p \nabla \cdot \vec{v} - \nabla \cdot (k \nabla T) = 0$$

Other phenomena may contribute to \mathcal{L} with, for example

- gain of heat by viscous dissipation of movement
- radiation
- convection

3.4 Euler's Equation in Conservative Form

In component form equation 1 and 2 become

$$\begin{aligned} v_i \frac{\partial \rho}{\partial t} &= -v_i \frac{\partial}{\partial x_j} (\rho v_j) \\ \rho \frac{\partial v_i}{\partial t} + \left(v_j \frac{\partial}{\partial x_j} \right) v_i &= -\frac{\partial p}{\partial x_i} + \rho f_i \end{aligned}$$

Summing the equations and simplifying

$$\frac{\partial}{\partial t} (\rho v_i) + \frac{\partial}{\partial x_j} (\rho v_i v_j) = -\frac{\partial p}{\partial x_i} + \rho f_i$$

If $f_i = 0$ we get

$$\frac{\partial}{\partial t} (\rho v_i) + \frac{\partial T_{ij}}{\partial x_i} = 0 \quad (8)$$

where $T_{ij} = p \delta_{ij} + \rho v_i v_j$ is the **momentum flux** tensor. In fact, the total momentum of an element with volume V is

$$p = \int_V \rho v_i dV$$

and it's time derivative

$$\frac{\partial}{\partial t} \int_V \rho v_i dV = - \int_V \frac{\partial T_{ij}}{\partial x_i} dV = - \oint_S T_{ij} dS_i$$

3.5 Energy Equation in Conservative Form

The energy density is

$$\rho\epsilon + \frac{1}{2}\rho v^2$$

So one may write

$$\frac{\partial}{\partial t} \left(\rho\epsilon + \frac{1}{2}\rho v^2 \right) = -\frac{\partial}{\partial x_j} (\epsilon\rho v_j) + \frac{\partial}{\partial x_j} (pv_j) + \frac{\partial}{\partial x_j} \left(k \frac{\partial T}{\partial x_j} \right) - \frac{1}{2} (\delta_{ij} v_j v_i) \frac{\partial}{\partial x_j} (\rho v_j) - \rho v_i \left(v_j \frac{\partial}{\partial x_j} \right) v_i v_i$$

and simplifying

$$\frac{\partial}{\partial t} \left(\rho\epsilon + \frac{1}{2}\rho v^2 \right) - \nabla \cdot \left[\rho \vec{v} \left(\frac{1}{2}v^2 + w \right) - k \nabla T \right] \quad (9)$$

where $w = \epsilon + \frac{p}{\rho}$ is the **enthalpy density**.

4 Lecture 4 - 26/09/2019

4.1 Bernoulli's Principle

For stationary stream ($\frac{\partial \vec{v}}{\partial t} = 0$), we may define current lines that are tangent to \vec{v} at every point. If the stream is stationary, the current lines trace the path of a given element of fluid. Let $\vec{f} = \vec{f}_{\text{grav}} = -\nabla\Phi$ where Φ is the gravitational potential.

Considering the identity

$$\nabla(\vec{A} \cdot \vec{B}) = \vec{A} \times (\nabla \times \vec{B}) + \vec{B} \times (\nabla \times \vec{A}) + (\vec{A} \cdot \nabla) \vec{B} + (\vec{B} \cdot \nabla) \vec{A}$$

Taking Euler's equation for a stationary fluid (eq. 4)

$$(\vec{v} \cdot \nabla) \vec{v} = -\frac{1}{\rho} \nabla p + \vec{f}$$

Using the previous identity

$$\nabla \left(\frac{v^2}{2} \right) - \vec{v} \times (\nabla \times \vec{v}) = -\frac{1}{\rho} \nabla p - \nabla \Phi$$

Integrating along the path of the current

$$\int_l \left[\nabla \left(\frac{v^2}{2} \right) - \vec{v} \times (\nabla \times \vec{v}) + \frac{1}{\rho} \nabla p + \nabla \Phi \right] d\vec{l} = 0$$

which gives

$$\frac{1}{2}v^2 + \int \frac{dp}{\rho} + \Phi = \text{const} \quad (10)$$

In the case of an **incompressible fluid** $\int \frac{dp}{\rho} = \frac{p}{\rho}$ we get

$$\frac{1}{2}v^2 + \frac{p}{\rho} + gh = \text{const} \quad (11)$$