1)
$$\Gamma_{i=3cm}$$
 $T_{i=400K}$ $h_{f}=27\frac{\omega}{m^{2}K}$ $\Gamma_{o=5cm}$ $T_{o=326K}$ $K=?$ $T_{F=300K}$

Lyall variables are Known,
use this for q
This since q is constant, use the

$$K = \frac{(L^2 - L^2)}{(L^2 - L^2) \cdot |u(\frac{u_1}{L_0})|}$$

$$K = \frac{27 \frac{\omega}{m^{2} \cdot K} \cdot 0.05 m \cdot (326-300) K \cdot \ln(\frac{0.05}{0.03})}{(400-326) K}$$

$$9'' = \mathcal{E} \cdot \nabla \cdot (T_{5}^{4} - T_{5}u_{r}^{4})$$

$$9'' = \mathcal{E} \cdot \nabla \cdot (T_{5}^{2} + T_{5}u_{r}^{2})(T_{5}^{2} - T_{5}u_{r}^{2})$$

$$9'' = \mathcal{E} \cdot \nabla \cdot (T_{5}^{2} + T_{5}u_{r}^{2})(T_{5} + T_{5}u_{r})(T_{5} - T_{5}u_{r})$$

$$h_{r}$$

$$9'' = h_{r} \cdot \Delta T$$

$$1_{7} \text{ where } h_{r} = \mathcal{E} \cdot \nabla \cdot (T_{5}^{2} + T_{5}u_{r}^{2})(T_{5} + T_{5}u_{r})$$

$$h_{r} = 0.8 \left(5.67 \times 10^{-8} \frac{\omega}{m^{3} \cdot K^{4}}\right) \left(323.15 K^{2} + 473.15 K^{2}\right) \left(323.15 K + 473.15 K\right)$$

$$h_{r} = 11.858 \frac{\omega}{m^{3} \cdot K}$$

3)
$$K = 0.139 \frac{\omega}{m \cdot K}$$
 $P = 4.1 \times 10^{-5} \frac{m^2}{5}$ $L = 0.1 m$ $P = 4 \cdot \frac{Ac}{P} = 4 \cdot \frac{0.01 \cdot 0.0 M}{(2.0.01) + (2.0.01)} = 0.01 L$ $P = 854 \frac{K_{\frac{1}{2}}}{m^2}$ $G = 45.25 \frac{K_{\frac{1}{2}}}{m^2 \cdot 5}$ $\omega = 0.04 m$ $\omega = 0.01 m$ $\omega = 0.01 m$

a) mass flow rate b) volumetric flow rate c) Velocity
$$m = 6.4$$
 $m = 45.25 \frac{K_8}{m^2 \cdot s} (0.01 \times 0.04) m^2$ $Q = 0.0181 \frac{K_9}{s} / 854 \frac{K_9}{m^3}$ $V = 2.110$

Re= 20.68, Laminar

e) Convective HT, $\mu = 4.36$ F) ΔT wall -7 fluid $h_c = \mu \frac{R}{D_h}$ $\Delta T = \frac{9^{11}}{h_c}$ $\Delta T = \frac{9^{11}}{h_c}$ $\Delta T = \frac{100^{11}}{M^2} \sqrt{37.8715} \frac{\omega}{m^2 \cdot K}$

mass flow rate b) volumetric flow rate c) Velocity
$$\dot{m} = 6.4$$
 $\dot{q} = \dot{m}/e$ $\dot{q} = \dot{m}/e$ $\dot{q} = 0.0181 \frac{K_{4}}{5} / (0.01\times0.04) m^{2}$ $\dot{q} = 0.0181 \frac{K_{4}}{5} / (0.01\times0.04) m^{2}$

h_= 37.8775 W AT= 2.64K

9)
$$\Delta T$$
 inlet \Rightarrow outlet h) Pressure Drop, Re. $f = 73$

$$\Delta T = 9^{11} \cdot A/_{m \cdot Cp}$$

$$\Delta T = 100 \frac{M}{m^2} \cdot (0.01 \times 0.04) m^2 /_{0.0161} \frac{K_9}{5} (2120 \frac{T}{K_9 \cdot K})$$

$$\Delta T = \frac{1}{2} (854 \frac{K_9}{m^2}) (0.053 \frac{2}{2}) \cdot \frac{73}{10.68} \cdot \frac{(0.1)m}{0.0167}$$

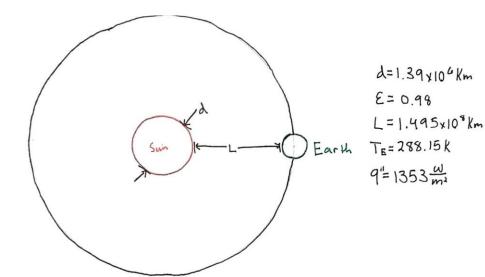
$$\Delta T = 0.02606K$$

h) Pressure Drop, Re. f=73
$$\Delta P = \frac{1}{2} P \cdot V^{2} \cdot f \cdot \frac{L}{D_{h}}$$

$$\Delta P = \frac{1}{2} (854 \frac{K_{0}}{M^{2}}) (0.053 \frac{2}{2}) (\frac{73}{10.68}) \cdot (\frac{0.1 M}{0.016 \text{ ps}})$$

$$\Delta P = 26.46 \frac{K_{0}}{M \cdot 5^{2}}$$

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$$9 = 3.8 \times 10^{26}$$

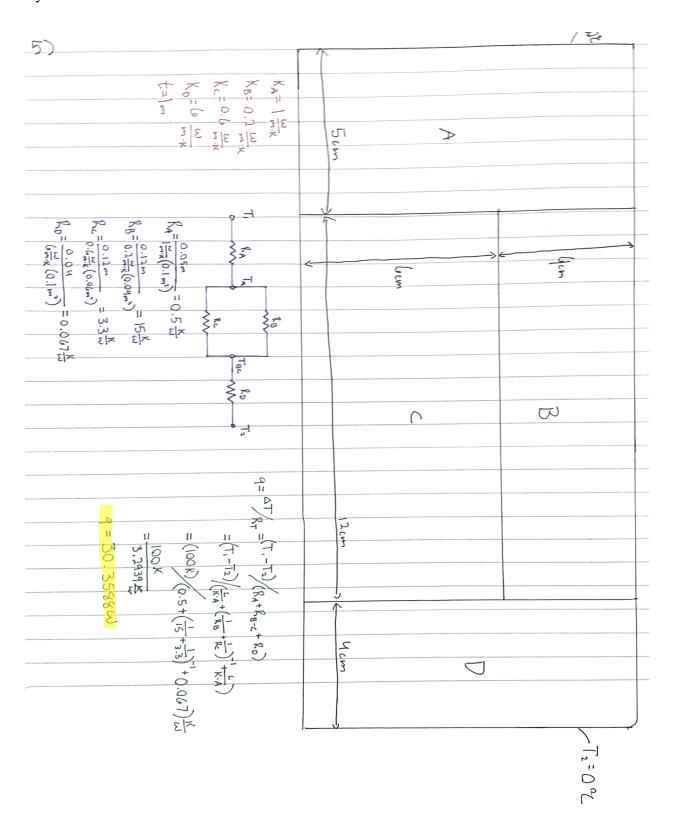
$$3.8 \times 10^{26}$$

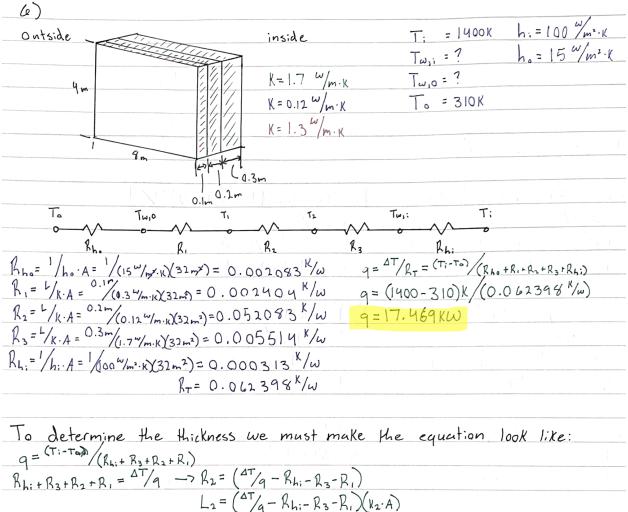
$$4.\pi \cdot (6.95 \times 10^{6})^{2} = 0.98(5.67 \times 10^{-8})$$

$$7 \times 10^{26}$$

$$4.\pi \cdot (6.95 \times 10^{6})^{2} = 0.98(5.67 \times 10^{-8})$$

$$\sqrt{\frac{6.26 \times 10^{7} \frac{60}{10^{2}}}{0.98(5.67 \times 10^{-8} \frac{100}{10^{2} \times 10^{2}})} + 288.15 K^{4}} = T_{5}$$





Everything else is known, plug in values: $L_{2} = \frac{(1400 - 320 \text{K})}{17444W} - 0.000313 \frac{\text{K}}{W} - 0.005514 \frac{\text{K}}{W} - 0.002404 \frac{\text{K}}{W} \times (0.12 \frac{\text{W}}{\text{m.K}} \times (32 \text{m}^{2})}$ $L_{1} = \frac{(0.0536 \frac{\text{K}}{W})(0.12 \frac{\text{W}}{\text{m.K}})(32 \text{m}^{2})}{(32 \text{m}^{2})}$

L2=0.205802m