

Lecture 04

- Exact NS
 - Stagnation Flow
 - ω transport



... continued

$$u(y=0, t) = U \quad (\text{const})$$

$$u(y=0, t) = U_0 t^r \quad r > 0 \quad \text{--- ODE} \quad f'' + f' y' - r f = 0$$

→ numerically

more observations from Stokes 1st

- S_{99} : $\frac{u(y=S_{99})}{U} = .99 \rightarrow S_{99} \approx 3.6 \sqrt{vt}$

$$V_{\text{entr}} = 0.15 \text{ cm}^2/\text{s} \quad S_{99} = 10 \text{ cm} \text{ in } 1 \text{ min}$$

- ω - vorticity \Rightarrow even more confined near wall

$$\omega_z = \frac{\partial u}{\partial x} - \frac{\partial v}{\partial y} = A t^\alpha f' B t^\beta$$

$$\omega_z = \frac{-U}{\sqrt{\pi vt}} e^{-y^2/4vt}$$

note singular at $t=0 \Rightarrow$ vortex sheet on the wall

note

$$\int \omega_z dy = -U \quad \text{constant vorticity}$$

$$\int \left(\frac{\partial u}{\partial x} - \frac{\partial u}{\partial y} \right) dy = U \quad \text{any } u(y) \text{ profile}$$

- wall stress (\sim drag component)

$$\tau_{xy} = \mu \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)$$

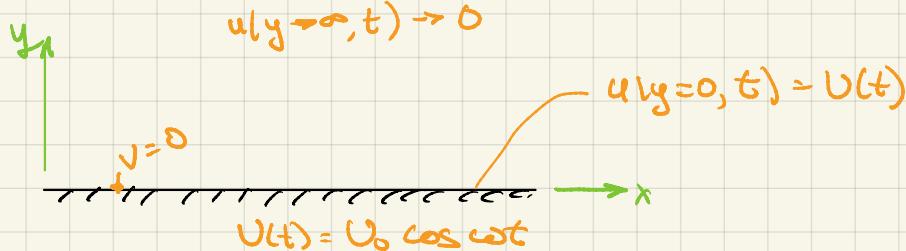
$$\tau_{xy} \Big|_{\text{wall}} = \tau_w = \mu \frac{\partial u}{\partial y} \Big|_{\text{wall}} = \frac{U \mu}{\sqrt{\pi \nu t}}$$

decreases over time

Stokes 2nd Problem

Stokes Oscillating Plate

- interested in time keeping \rightarrow drag on a pendulum



- some assumptions: μ, ρ const, $\nabla \cdot \underline{u} = 0$
- same V B.C.

• same x -uniformity $\partial_x \rightarrow 0$

↳ same PDE

$$\frac{\partial u}{\partial t} = v \frac{\partial^2 u}{\partial y^2}$$

$$u(y=0, t) = U_0 \cos \omega t$$

$$u(\infty, t) = 0$$

→ long $t \Rightarrow$ assume any initial transient

decays → sort of informed by Stokes 1st

take $\hat{u}(y, t) = \operatorname{Re} \{ \hat{u}(y) e^{i \omega t} \}$

$$i \omega \hat{u} = v \frac{d^2 \hat{u}}{dy^2} \rightarrow \frac{d^2 \hat{u}}{dy^2} - \frac{i \omega}{v} \hat{u} = 0$$

$$\hat{u}(y) = A_+ e^{+\sqrt{\frac{i \omega}{v}} y} + A_- e^{-\sqrt{\frac{i \omega}{v}} y}$$

$$\hat{u}(0) = U_0$$

$$\hat{u}(y) = A_+ e^{+\sqrt{\frac{i \omega}{v}} y} e^{i \sqrt{\frac{i \omega}{v}} y} + A_- e^{-\sqrt{\frac{i \omega}{v}} y} e^{-i \sqrt{\frac{i \omega}{v}} y}$$

$$A_+ = 0 \text{ for } \hat{u}(y \rightarrow \infty) = 0$$

$$\hookrightarrow A_- = U_0$$

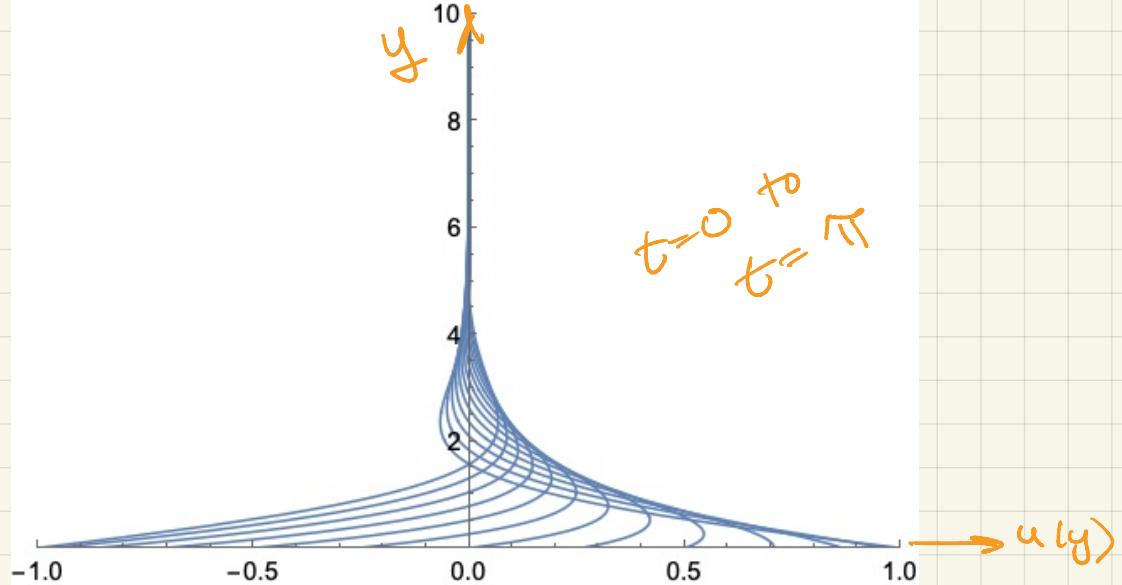
$$u(y, t) = \operatorname{Re} \{ U_0 e^{-\sqrt{\frac{i \omega}{v}} y} e^{-i \sqrt{\frac{i \omega}{v}} y + i \omega t} \}$$

$$= U_0 e^{-\sqrt{\frac{\omega}{v}} y} \cos(\omega t - \sqrt{\frac{\omega}{v}} y)$$

$$\sqrt{i} = \frac{1+i}{\sqrt{2}}$$

$$i = e^{i\pi/2}$$

$$\sqrt{i} = e^{i\pi/4}$$



$$S_{qq} = 4.5 \sqrt{\frac{2\omega}{\omega}}$$

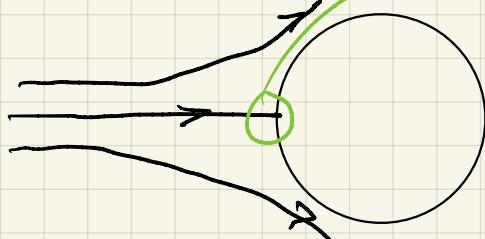
thinner for larger ω
 $\propto \sqrt{\omega}$

Q: where is the ω peak (in phase)
 → easy to compute

Both Stokes 1 and 2 \Rightarrow for $\nu \rightarrow 0 / Re \rightarrow \infty$

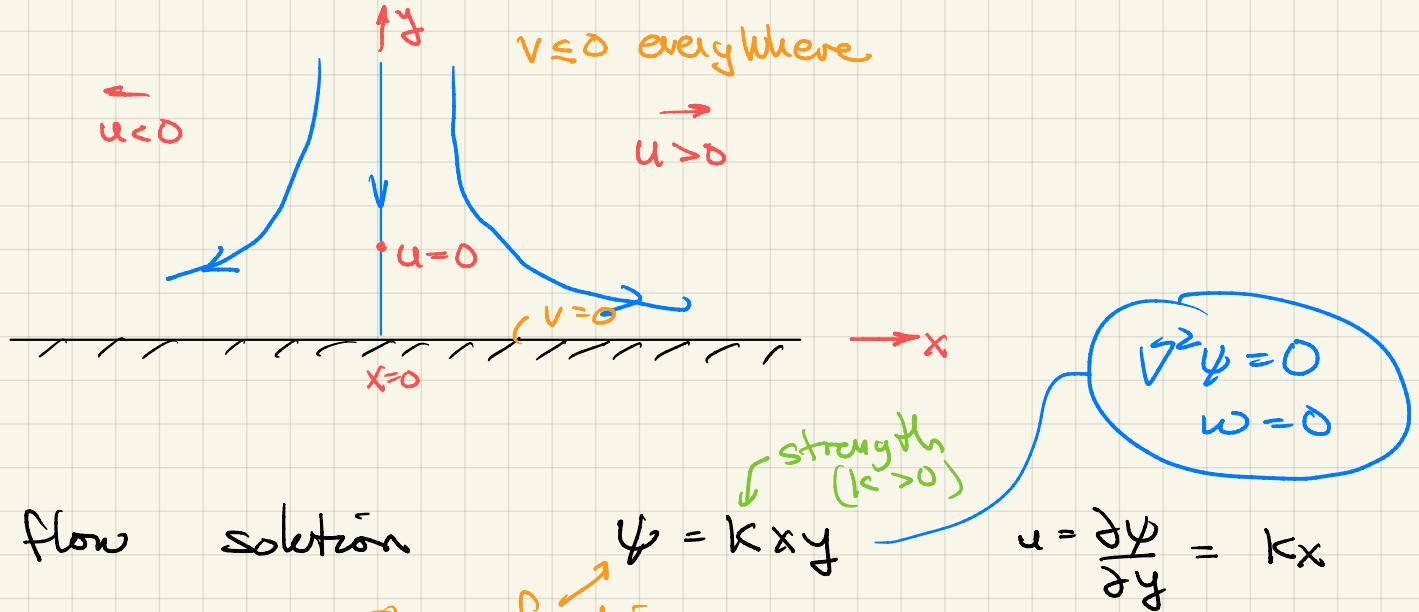


Stagnation Pt Flow



analyze this region — recall $P_{\mu=0}$ solution was good here

locally flat



potential flow solution

full N-S , can

show

$$\nabla^2 \psi = -\omega \quad (2D)$$

it "works"

potential flow $\nabla^2 \psi = 0$

↳ ψ irrotational

"Add" no slip — make some assumptions

↳ inform strategy/setup — not simplify

main assumption

- Assume ω stays near the wall

- rationale I
 - \rightarrow small
 - diffusive process

\Rightarrow don't expect ω to "get far"

a mild concern = steady flow sort of implies
 $t \rightarrow \infty \rightarrow$ diffusion can
 go a long way

- rationale II - vorticity transport mechanics

$$\nabla \times \left(\frac{Du}{Dt} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 u \right) \quad \underline{\omega} = \nabla \times \underline{u}$$

\therefore do this

The vorticity transport equation $\frac{D\omega}{Dt} = \underline{\omega} \cdot \nabla \underline{u} + \nu \nabla^2 \underline{\omega}$

no P !

$$\frac{D\omega}{Dt} = \underline{\omega} \cdot \nabla \underline{u} + \nabla \cdot \underline{\omega}$$

$$\frac{\partial \omega_z}{\partial t} + u \frac{\partial \omega_z}{\partial x} + v \frac{\partial \omega_z}{\partial y} + \dots$$

- advection - velocity advecting vorticity

- it moves like a scalar field in flow

dye concentration ξ

$$\frac{D\xi}{Dt} = 0 \quad \text{if no diffusion}$$

- note - actually nonlinear

redistribution/
concentration
by $\nabla \underline{u}$

→ between
components
of $\underline{\omega}$

→ intensity /
diminish
a component

"vortex stretching"

MAIN THING:

totally inactive
if $\underline{\omega} = 0$

Fickian-like
diffusion

like heat

$$\frac{\partial T}{\partial t} = \nabla^2 T$$

→ concentration
of ω →
spreads but
in a conserved
way

in creation/
destruction

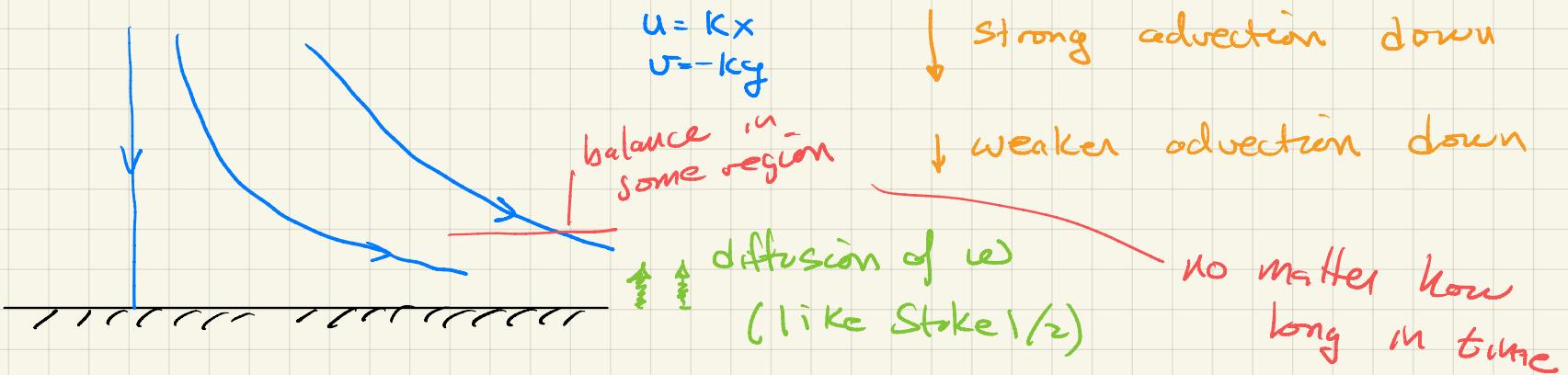
never active in 2D

$$\underline{u} = (u, v, 0)$$

$$\underline{\omega} = (0, 0, \omega_z)$$

$$\underline{\omega} \cdot \nabla \underline{u} = 0$$

$$\nabla = (\partial_x, \partial_y, 0)$$



- rationale III - if "works" - we do find self-consistent N-S advection

Solution

- take $\psi(x, y) = x f(y)$ in layer close to wall

- "blend" to $\psi(x, y) = kxy$ above ($f(y) \rightarrow ky$)

$$u = xf' \quad v = -f$$

$$\omega = \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) = -xf''$$

ω transport in
2D

$$\cancel{\frac{\partial \omega}{\partial t}} + u \frac{\partial \omega}{\partial x} + v \frac{\partial \omega}{\partial y} = \nu \left(\frac{\partial^2 \omega}{\partial x^2} + \frac{\partial^2 \omega}{\partial y^2} \right)$$

steady

$$-x f' f'' + f x f''' = \nu (0 - x f''')$$

$\therefore x$

$$-f' f'' + f f''' = -\nu f'''$$

$$u(x, y=0) = 0 \rightarrow f'(0) = 0$$

$$v(x, y=0) = 0 \rightarrow f(0) = 0$$

$$f(y \rightarrow \infty) = Ky \quad \text{matching}$$

$$f''(y \rightarrow 0) = 0$$