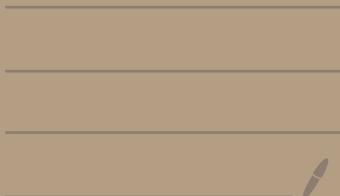


# Lecture 24

- Reynolds Analogy
- Compressible BL behavior w/ Ma



Meeting #2: covers thru compressible [not streaming]

→ probably Manday's material

→ will target material since last meeting cut off

—  
Last time → 1<sup>st</sup> Crocco - Buseman Relation  
(1932) (1931)

$$\Pr = 1 \Rightarrow H = h + \frac{u^2}{2} = \text{const} \quad \text{solved BL eq}$$

→ spoke to balance  $\bar{D}$  and  $q$

Reynolds Analogy

add  $\frac{\partial P}{\partial x} = 0$

x-mom

$$g u \frac{\partial u}{\partial x} + g v \frac{\partial v}{\partial y} = \frac{\partial}{\partial y} \left( \mu \frac{\partial u}{\partial y} \right)$$

D

enthalpy

$$g u \frac{\partial h}{\partial x} + g v \frac{\partial h}{\partial y} = \frac{\partial}{\partial y} \left( \frac{\mu}{\Pr} \frac{\partial h}{\partial y} \right) + \mu \left( \frac{\partial u}{\partial y} \right)^2$$

A

B

C

→ v.similar, more so if  $\Pr = 1$

$\Pr = 1$   
→ only difference is  
a  $u$ -dependent  
"source" in  $h$   
equation

assume  $h = h(u)$  in the sense of it being a useful transform  
 $\rightarrow$  reminiscent of hodograph plane  
 $h \rightarrow u$  compressible potential flow...

(A)  $\frac{\partial h}{\partial x} = \frac{\partial h}{\partial u} \frac{\partial u}{\partial x}$   
 (B)  $\frac{\partial h}{\partial y} = \frac{\partial h}{\partial u} \frac{\partial u}{\partial y}$   
 (C)  $\frac{\partial}{\partial y} \left( \mu \frac{\partial h}{\partial y} \right) = \frac{\partial}{\partial y} \left( \mu \frac{\partial h}{\partial u} \frac{\partial u}{\partial y} \right) = \frac{\partial h}{\partial u} \frac{\partial}{\partial y} \left( \mu \frac{\partial u}{\partial y} \right) + \boxed{\mu \frac{\partial u}{\partial y}} \frac{\partial}{\partial y} \left( \frac{\partial h}{\partial u} \right)$

$\frac{\partial h}{\partial u} \left[ g_u \frac{\partial u}{\partial x} + g_v \frac{\partial u}{\partial y} \right] - \frac{\partial}{\partial y} \left( \mu \frac{\partial u}{\partial y} \right)$   
 $= \mu \frac{\partial u}{\partial y} \frac{\partial^2 h}{\partial u^2} \frac{\partial u}{\partial y} + \mu \left( \frac{\partial u}{\partial y} \right)^2$   
 $= \mu \left[ 1 + \frac{d^2 h}{du^2} \right] \left( \frac{\partial u}{\partial y} \right)^2$

complete derivatives  $h(u)$   
 $u(x, y)$   $v(x, y)$   
 $x(u, v)$   $y(u, v)$

$$\left[ 1 + \frac{d^2 h}{du^2} \right] \left( \frac{du}{dy} \right)^2 = 0$$

↑  
≠ 0



$$\frac{d^2 h}{du^2} = -1$$

$$\frac{dh}{du} = -u + C_1$$

$$h = -\frac{1}{2}u^2 + C_1 u + C_2$$

BC

take  $h(y=0) = h_w$

$$C_2 = h_w$$

no slip  $u = 0$

$\underline{h(y \rightarrow \infty) = h_\infty}$

$u = U$

$$h_\infty = -\frac{1}{2}U^2 + C_1 U + h_w$$

$$C_1 = (\underline{h_\infty + \frac{1}{2}U^2} - h_w) / U$$

$H = h_\infty + \frac{1}{2}U^2$

$H \text{ const}$  1st C-B need  
 $H_\infty = h_w$  BC

$$A \quad h + \frac{u^2}{2} = (h_\infty - h_w) u / \rho + h_w$$

C did not go into details  
 $\Phi \approx q$   
balance

$H$  is linear in  $u$  in BL

take  $C_p = \text{const}$

$$h = C_p T$$

$$A \quad C_p T + \frac{u^2}{2} = C_p T_w + \left( C_p T_\infty + \frac{u^2}{2} - C_p T_w \right) u / \rho$$

$h_\infty = C_p T_\infty$   
 $T_\infty = C_p T_w$   
 $= C_p T_w$   
adibatic wall

solve for  $T$

( $\div C_p$ )

$$T = T_w + \left( T_\infty + \frac{u^2}{2 C_p} - T_w \right) \frac{u}{\rho} - \frac{u^2}{2 C_p}$$

$$q_w = K_w \frac{\partial T}{\partial y} \Big|_w$$

$$= \frac{(T_\infty - T_w)}{\rho} K_w \frac{\partial u}{\partial y} \Big|_w - K_w \frac{u w \frac{\partial u}{\partial y}}{C_p} \Big|_w$$

$u_w = 0$

$q_w, T_w$   
are 2 main interests

↑ related to  $T_w$

$$T_w = \mu_w \frac{\partial u}{\partial y} \Big|_w$$

$$\frac{\partial u}{\partial y} \Big|_w = \frac{T_w}{\mu_w}$$

$$1 \times \frac{\partial u}{\partial y} \Big|_w = \frac{\mu_w T_w}{\mu_w}$$

$$= \frac{C_p T_w}{Pr}$$

$$Pr = \frac{C_p}{\mu K}$$

$$q_w = \frac{T_{aw} - T_w}{U}$$
 related (circled) (circled) ↓

$$\frac{q_w}{C_p (T_{aw} - T_w)} = \frac{T_w}{U}$$

$\therefore$   
 $S_U$

$$\frac{q_w}{S_U C_p (T_{aw} - T_w)} = \frac{T_w}{S_U U^2}$$



heat transfer  
coefficient



$C_f/z$   
friction coefficient

Reynolds Analogy

thermal flux = drag

⇒ viscous heating balanced by conduction cooling

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was a huge "industry" looking for transforms that lead to self similarity . . .

→ cool they exist

→ not illuminating

→ just a hint

Illingworth  
Transform

$$g_u = \frac{\partial \psi}{\partial y}$$

$$g_v = -\frac{\partial \psi}{\partial x}$$

$$\Rightarrow \nabla \cdot g_u = 0 \\ (\text{steady mass})$$

split form

$$\psi(\xi, \eta) = \int g_u dy = G(\xi) f(\eta)$$

$$u(\xi, \eta) = U(\xi) f'(\eta)$$

→ viscous effects →  $\xi$

→ density change →  $\eta$

$$\xi = \int_0^x \rho_\infty(x) U(x) \mu_\infty(x) dx = \xi(x)$$

$$\eta = \frac{C}{\sqrt{2\xi}} \int_0^y \xi dy = \eta(x, y)$$

∴

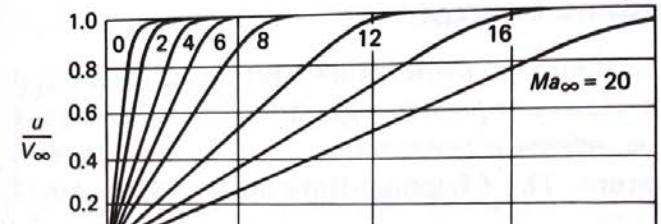
$$(C f'')' + (f f'') + \frac{2\xi}{C} \frac{dU}{d\xi} \left( \frac{\rho_\infty}{\xi} - f'^2 \right) = 0$$

$$C = \frac{\rho_\infty}{\rho_\infty \mu_\infty} = (1/\eta)$$

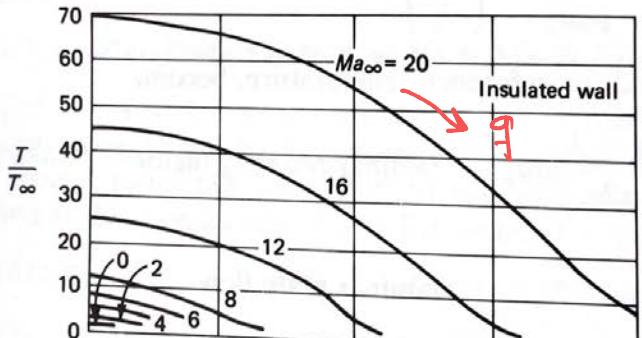
∴

$$U, \xi, \mu \text{ cons} \quad f'' + f f''' = 0$$

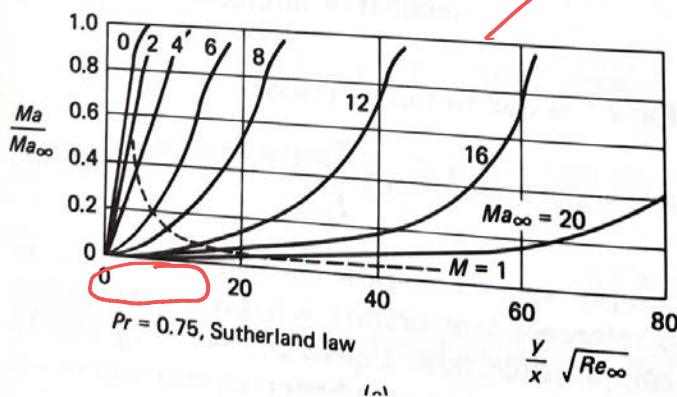
$$\therefore \text{can do} \quad U = K x^m$$



(a)



(b)

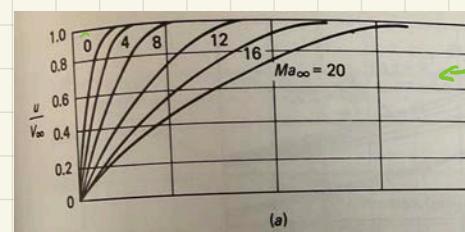


(c)

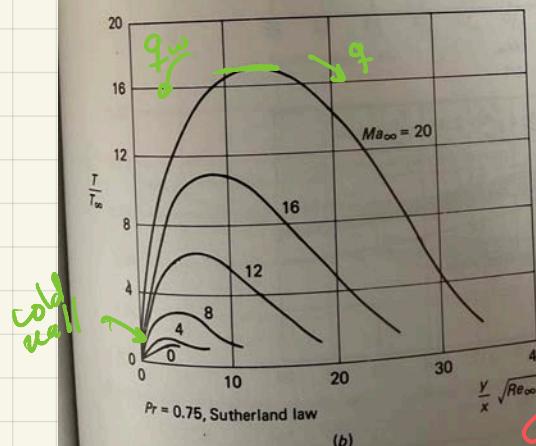
*Blasius*  
much thicker  
at higher Ma

i'm mostly subsonic  
because  $\alpha = \sqrt{\gamma RT}$   
 $q_w = 0$

**FIGURE 7-2**  
Calculations of the laminar ~~com~~  
impermeable boundary layer on an  
insulated flat plate by van Driest  
(1952a): (a) velocity profiles; (b)  
(c) temperature profiles;



(a)

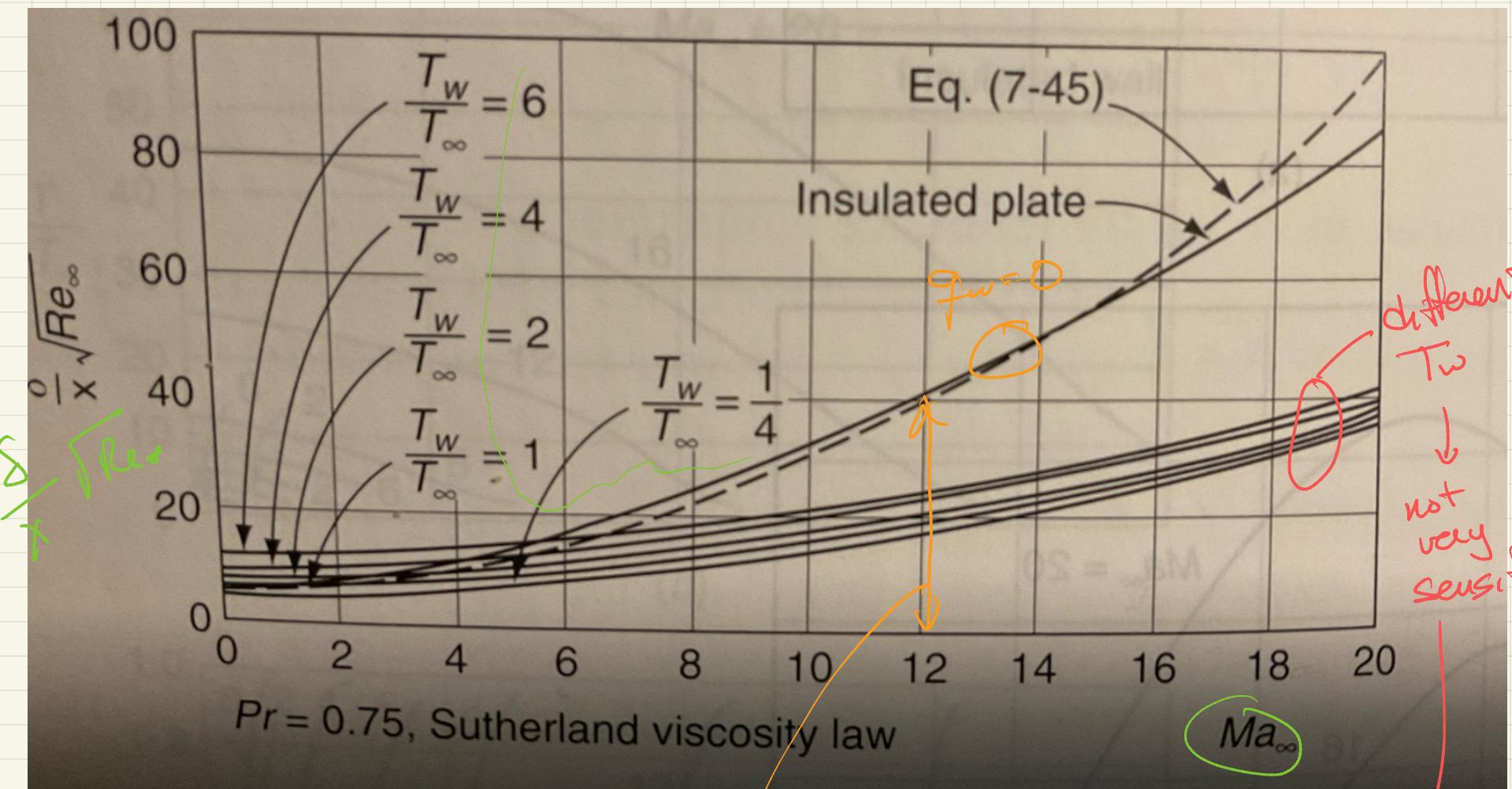


(b)

**FIGURE 7-3**  
Calculations by van Driest (1952a)  
of the compressible laminar  
boundary layer on a cold flat plate  
( $T_w = T_\infty/4$ ): (a) velocity profiles;  
(b) temperature profiles.

cold wall  
profiles are well fit

not quite  
so thick  
in Ma,  
but still  
thicker  
L thermal  
Expansion



about  $2x$   
as thick  
→ latter  
of only 1-way to  
free stream

because  
peak  $T$  in  
BC much  
higher