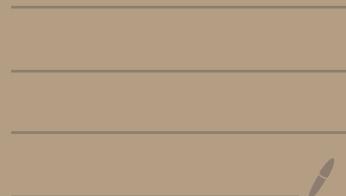


Lecture 22

- One way coupling $\rightarrow T$



- Meeting #2 - sign ups ...

TOTAL ENERGY

$$\int \frac{D e_t}{Dt} = -\nabla \cdot \underline{\dot{q}} + \nabla \cdot \underline{\underline{\sigma}} \cdot \underline{u}$$

advection heat work

KINETIC
 $\underline{u} \cdot (\underline{u})_{(mom)}$

$$\int \rho \frac{De_k}{Dt} = \cancel{\nabla \cdot \underline{\underline{\sigma}} \cdot \underline{u}} - \underline{\underline{\sigma}} : \nabla \underline{u}$$

+

$\underline{u} \cdot \underline{\underline{\sigma}}$

$P \nabla \cdot \underline{u} - \underline{\Phi}$

INTERNAL

$$\int \rho \frac{De_i}{Dt} = -\nabla \cdot \underline{\dot{q}} + \underline{\underline{\sigma}} : \nabla \underline{u}$$

$$\rightarrow -P \nabla \cdot \underline{u} + \underline{\Phi}$$

viscous dissipation ≥ 0

change thermo dynamic variable

$$e_i \rightarrow h \rightarrow s \rightarrow T$$

0
0
s

LAST
TIME

$$T \frac{Ds}{Dt} = \frac{Dh}{Dt} - \frac{1}{c_p} \frac{Dp}{Dt}$$

$$\hookrightarrow g = 1/5$$

source of entropy

S

$$S \frac{Ds}{Dt} = -\frac{1}{T} \nabla \cdot q + \frac{1}{T} \Phi$$

if no thermal conductivity

or $\mu \rightarrow \frac{D_s}{Dt} = 0$ just advects

specific heat

$$h = c_p T$$

take c_p const

$$S c_p \frac{dT}{Dt} = -\nabla \cdot q + \frac{Dp}{Dt} + \Phi$$

assume isobaric
 $p \approx \text{const}$

$$\frac{\Delta p}{p_0} \ll 1$$

small Δp sufficient
preserve flow
w/o thermodynamic
effects
(low Mach)

$$q = -k \nabla T \quad \text{Fourier}$$

$$-\nabla \cdot q = \nabla \cdot k \nabla T$$

Δp 's don't
change T

BL limit?

Assume 1-way coupled
 u affect T
only

NEW

apply BL approximation

non dimensionalize + BL scale (μ, κ const)

$$\begin{aligned}
 x &= \frac{x^*}{L} & \hat{y} &= \frac{y^*}{L} & u &= \frac{u^*}{U} & \hat{v} &= \frac{v^*}{U} & \Theta &= \frac{T^* - T_\infty}{\Delta T} \\
 x^* &= Lx & y^* &= \sqrt{Re} \hat{y} & u^* &= Uu & v^* &= Uv & T^* &= \Delta T \theta + T_\infty \\
 y^* &= \frac{Ly}{\sqrt{Re}} & & & & & & &
 \end{aligned}$$

Sub into  + assume 2D / steady

$$\begin{aligned}
 ① \quad gC_p \frac{\partial T^*}{\partial t} &= gC_p \left(u^* \frac{\partial T^*}{\partial x^*} + v^* \frac{\partial T^*}{\partial y^*} \right) = gC_p \left(U \frac{u \Delta T}{L} \frac{\partial \theta}{\partial x} + \frac{U \sqrt{Re} \Delta T v \partial \theta}{\sqrt{Re} L \partial y} \right) \\
 &= \frac{gC_p U \Delta T}{L} \left(\frac{u \partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} \right)
 \end{aligned}$$

$$② \quad \kappa \nabla^2 T = \kappa \left(\frac{\partial^2 T^*}{\partial x^{*2}} + \frac{\partial^2 T^*}{\partial y^{*2}} \right) = \kappa \frac{\Delta T}{L^2} \left(\frac{\partial^2 \theta}{\partial x^2} + Re \frac{\partial^2 \theta}{\partial y^2} \right)$$

↑ dominant

$$= \frac{\kappa \Delta T \rho c}{L^2} \frac{\partial^2 \theta}{\partial y^2}$$

$$(3) \quad \Phi = \frac{1}{2} \mu (\nabla u^* + \nabla u^{*\top}) : (\nabla u^* + \nabla u^{*}) + \lambda (\nabla u^*)^2$$

$$\begin{pmatrix} 0 & 0 \\ 0 & 0 \end{pmatrix} \begin{pmatrix} 0 & 0 \\ 0 & 0 \end{pmatrix}$$

$$+ \frac{1}{2} \mu \left(2 \frac{\partial u^*}{\partial x^*} \right) \left(2 \frac{\partial u^*}{\partial x^*} \right) + \frac{1}{2} \mu \left[\frac{\partial u^*}{\partial y^*} + \frac{\partial v^*}{\partial x^*} \right] \left[\frac{\partial u^*}{\partial y^*} + \frac{\partial v^*}{\partial x^*} \right]$$

$$+ \frac{1}{2} \mu \left(\frac{\partial v^*}{\partial x^*} + \frac{\partial u^*}{\partial y^*} \right) \left(\frac{\partial v^*}{\partial x^*} + \frac{\partial u^*}{\partial y^*} \right) + \frac{1}{2} \mu \left(2 \frac{\partial v^*}{\partial y^*} \right) \left(2 \frac{\partial v^*}{\partial y^*} \right)$$

$$+ \lambda \left(\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} \right)^2$$

$$= \mu \frac{U^2}{L^2} \left\{ 2 \left[\left(\frac{\partial u}{\partial x} \right)^2 + \frac{Re}{Ra} \left(\frac{\partial v}{\partial y} \right)^2 \right] + \left(\frac{Ra}{Re} \frac{\partial u}{\partial y} + \frac{1}{Ra} \frac{\partial v}{\partial x} \right)^2 \right\}$$

O(1) O(1) O(Re) O(Ra)

$$+ \lambda \frac{U^2}{L^2} \left(\frac{\partial u}{\partial x} + \frac{Ra}{Ra} \frac{\partial v}{\partial y} \right)^2$$

O(1) O(1)

$$= \mu \frac{U^2}{L^2} Re \left(\frac{\partial u}{\partial y} \right)^2$$

$$\textcircled{1} \quad \frac{gC_p U \Delta T}{L} \left(u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} \right) = \frac{\kappa \Delta T R e}{L^2} \frac{\partial^2 \theta}{\partial y^2} + \mu \frac{U^2 R e}{L^2} \left(\frac{\partial u}{\partial y} \right)^2$$

$$u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} = \underbrace{\frac{\kappa \Delta T R e L}{g C_p U \Delta T L^2} \frac{\partial^2 \theta}{\partial y^2}}_{\frac{\kappa R e L}{g C_p U L^2 \mu}} + \underbrace{\frac{\mu U^2 R e L}{g C_p U \Delta T L^2} \left(\frac{\partial u}{\partial y} \right)^2}_{\frac{\mu U^2 \delta V L}{g C_p U \Delta T L^2}}$$

$$\frac{\kappa}{C_p \mu} = \frac{1}{Pr} \#$$

$$\frac{U^2}{C_p \Delta T} = E_c$$

a fluid property \rightarrow

$$Prandtl \# = \frac{\text{viscous thermal conductivity}}{\text{thermal conductivity}}$$

Eckert #

$$E_c \# = \frac{KE}{dissipation}$$

"source" - internal heating

$$u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} = \frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} + E_c \left(\frac{\partial u}{\partial y} \right)^2$$

[dimensionless version] $g C_p \left(u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} \right) = \kappa \frac{\partial^2 \theta}{\partial y^2} + \mu \left(\frac{\partial u}{\partial y} \right)^2$

+ potential to change flow temp relative

to ΔT by viscous heating
 $\sim Ma^2$

Linear - break into two parts

$$\Theta(x, y, P_r, E_c) = \Theta_1(x, y, P_r) + E_c \Theta_2(x, y, P_r)$$

$$u \frac{\partial \Theta_1}{\partial x} + v \frac{\partial \Theta_1}{\partial y} = \frac{1}{P_r} \frac{\partial^2 \Theta_1}{\partial y^2}$$

$$u \frac{\partial \Theta_2}{\partial x} + v \frac{\partial \Theta_2}{\partial y} = \frac{1}{P_r} \frac{\partial^2 \Theta_2}{\partial y^2} + \left(\frac{\partial u}{\partial y} \right)^2$$

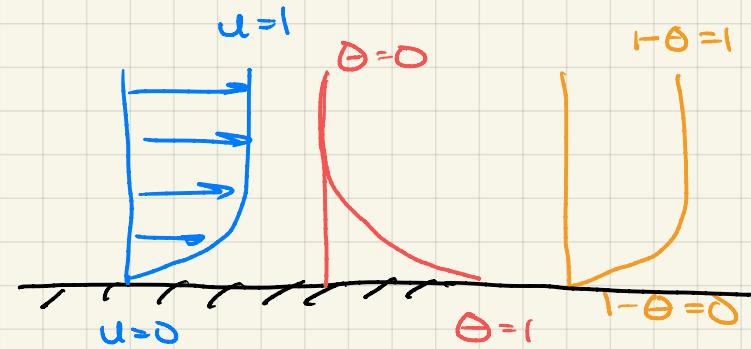
focus on this first (E_c small)

$(\Theta_1 \rightarrow \Theta)$

$$u \frac{\partial \Theta}{\partial x} + v \frac{\partial \Theta}{\partial y} = \frac{1}{P_r} \frac{\partial^2 \Theta}{\partial y^2}$$

x -mom

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\partial^2 u}{\partial y^2}$$



u and $1-\theta$ have some BC's

$P_r = 1 \rightarrow$ identical

gases

$P_r \approx 1$

air 0.7

$$\rightarrow S_{th} \approx S_{mom} \quad \text{same thickness}$$

$$Pr \rightarrow 0$$

[liquid metal

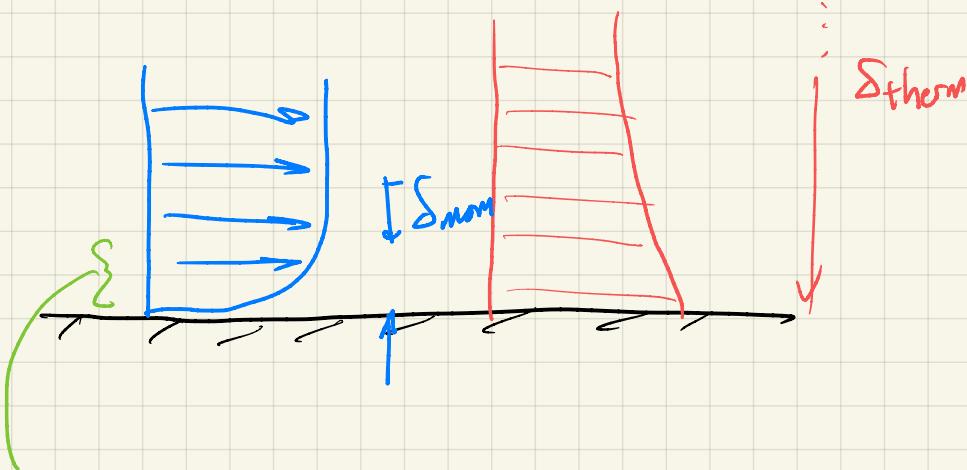
$$\frac{\mu}{C_p K} = \frac{\nu}{\chi} = Pr$$

* thermal diffusivity

$$S_{mom} \sim \sqrt{Pr}$$

$$S_{therm} \sim \sqrt{\alpha} \sim \sqrt{\nu Pr}$$

$$S_{therm} \gg S_{mom}$$



Velocity change only covers a small fraction of T change

slab height

$$\Theta = \operatorname{erf} \gamma$$

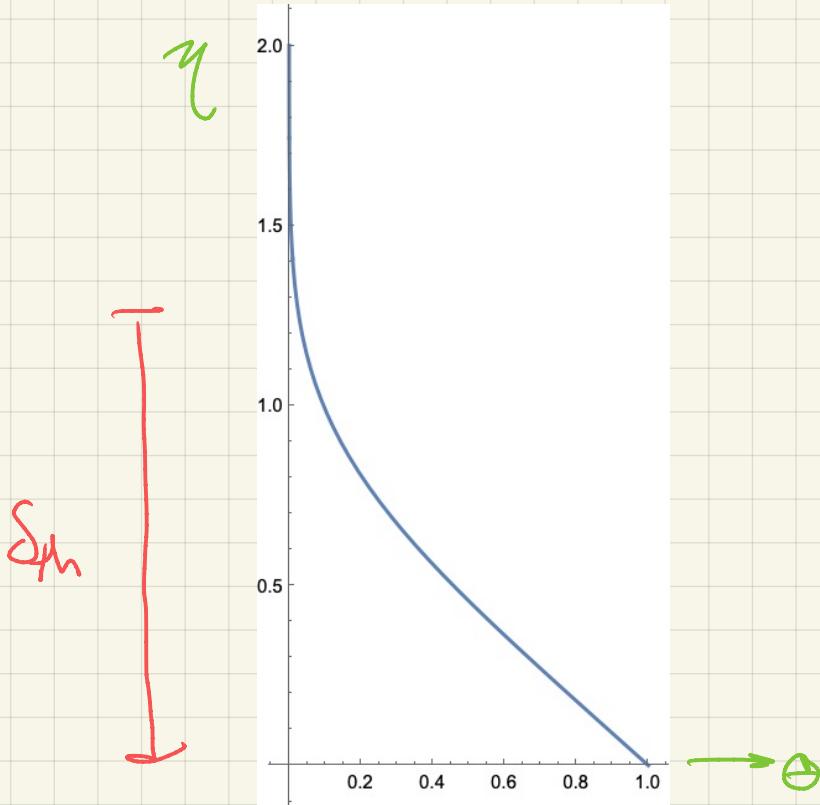
$$\gamma = y \frac{U(x)}{\sqrt{2} \int_0^x U(k) dk}$$

$\text{Pr} \rightarrow \infty$ → all T change right on wall where $u \approx 0$

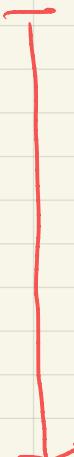
$$\dots \gamma = \gamma \sqrt{\frac{\bar{c}_{\text{w}}}{\mu}} \left(q_0 + \int_{x_0}^x \sqrt{\frac{\bar{c}_{\text{w}}(x)}{\mu}} dx \right)$$

⋮

$$\frac{d^2\Theta}{d\gamma^2} + 3\gamma^2 \frac{d\Theta}{d\gamma} = 0 \dots \Theta = \frac{\Gamma(\frac{1}{3}, \gamma^3)}{\Gamma(\gamma_3)}$$

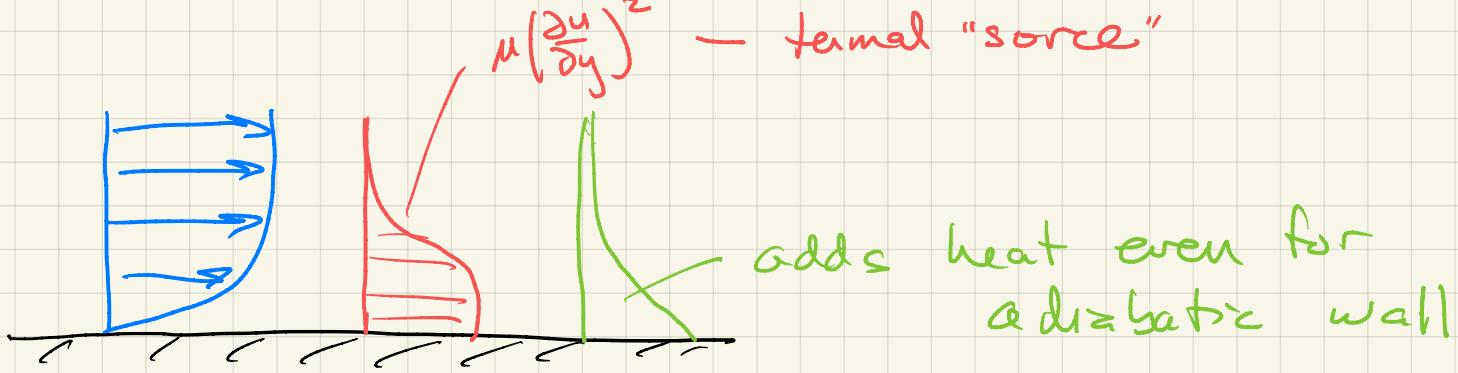


S_{th}



γ

Θ_2 ?



→ v. important for very speed flows....