

TODAY: HEAT EQ'S - TOWARDS SPACIAL SYSTEMS

WE'LL BE FOLLOWING CONVENTIONS IN BOOK, CHAPTERS 9-11.

Basics of Heat Transfer:

SIMPLE COOLING EXAMPLE:



PICTURE: HEAT IS KINETIC ENERGY OF TINY MOLECULES. HEAT CONTENT IS ROUGHLY TOTAL KINETIC ENERGY OF PART. MAKING UP THE MASS.

ASSUMPTIONS:

- HEAT IS A QUANTITY
- TEMPERATURE U IS PROP. TO AVERAGE KINETIC ENERGY.
- FOR A SYSTEM WITH FIXED MASS, IF HEAT LEAVES TEMP GOES DOWN, AND VISA VERSA.

SO WE HAVE FOLLOWING EQUATION:

$$Q = CM \frac{dU}{dt}$$

WHERE

Q - RATE OF CHANGE OF HEAT, J/S

C - SPECIFIC HEAT J/kg°C.

m - MASS IN KG

U - TEMPERATURE.

THIS IS NOT STANDARD!
USUALLY \dot{Q}

NOTE: C DEPENDS ON MATERIAL AND OTHER PARAMETERS, MEASURED EXPERIMENTALLY.

NEWTONS LAW OF COOLING

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THE RATE OF CHANGE OF HEAT LOSS TO SURROUNDINGS IS PROPORTIONAL TO THE TEMP. DIFFERENCE.

$$\left\{ \begin{array}{l} \text{RATE HEAT IS} \\ \text{EXCHANGED WITH} \\ \text{SURROUNDINGS} \end{array} \right\} = \pm h S \Delta U$$

WHERE

h - NEWTONS COOLING COEFF.

S - SURFACE AREA OF INTERFACE

$\Delta U = U - U_s$, U_s TEMP OF SURROUNDINGS

NOTE: SIGN \pm DEPENDS ON IF WE

USE $\Delta U = U - U_s$

OR $\Delta U = U_s - U$

WANT: IF $U_s > U$ THEN

WANT TO BE LOSING HEAT

FROM SYSTEM. SO NEED TO

MAKE SURE SIGN IS FIXED
TO MAKE THAT TRUE.

EX:

$$\left\{ \begin{array}{l} \text{RATE OF} \\ \text{CHANGE OF} \\ \text{HEAT IN} \\ \text{COFFEE} \end{array} \right\} = \left\{ \begin{array}{l} \text{RATE HEAT} \\ \text{LOST TO} \\ \text{SURROUNDINGS} \end{array} \right\}$$

$$C_m \frac{dU}{dt} = \pm h S (U - U_s)$$

NEED TO PICK SIGN: IF $U_s < U$,
EXPECT COOLING SO $U' < 0$.

$$C_m \frac{dU}{dt} = -h S (U - U_s) = h S (U_s - U)$$

OR

$$U' = -\frac{h S}{C_m} (U - U_s)$$

WHAT IF U_s AND U_s IS CONSTANT?

$$U = U_s + (U_0 - U_s) e^{-\frac{h S}{C_m} t}$$

IF ROOM TEMP U_s CHANGES:

$$C_m U' = -h S (U - U_s)$$

$$C_m U_s = h S (U - U_s)$$

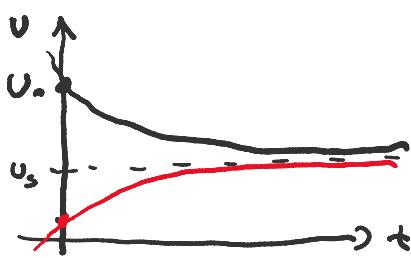
WHAT IS SIGN?

IF $U_s > U$ THEN

$$U' < 0$$

NOTE: CAN SOLVE WITH
SUBSTITUTION + LINEAR
ODE THEORY.

$$U = U_s + (U_0 - U_s) e^{-\frac{hs}{cm} t}$$

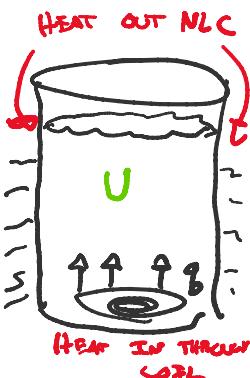


SUBSTITUTION + LINEAR ODE THEORY.
Ex: WHAT IS SOLUTION?

$$\vec{U}' = A \vec{U}$$

NOTE: DECREASE FASTER WHEN ΔU IS LARGE.

Ex: WATER HEATER:



\Rightarrow EQUATIONS:

$$cm U' = -hs(U - U_s) + q$$

RATE OF CHANGE OF HEAT: $\frac{d}{dt}$ q IS CONST. HEAT IN IN J/S.

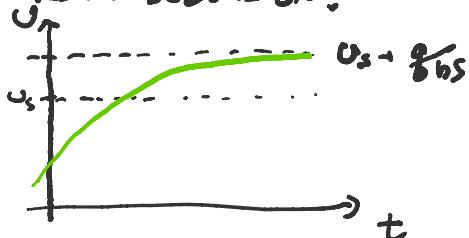
How Does THE ADDITION OF q EFFECT SOLUTIONS?

WRITE

$$U' = -\frac{hs}{cm} \left(U - U_s - \frac{q}{hs} \right)$$

SO IF U_s IS CONSTANT, THIS JUST ACTS AS A SHIFT IN EQUILIB.

RIUM SOLUTION:



$$U = U_s + \frac{q}{hs} + \left(U_0 - U_s - \frac{q}{hs} \right) e^{-\frac{hs}{cm} t}$$

$$U = U_s + \frac{Q}{hs} + \left(U_o - U_s - \frac{Q}{hs} \right) e^{-\frac{hs}{cm} t}$$

FOURIERS LAW AND HEAT FLUX

NEWTONS LAW IS ABOUT HEAT TRANSFER AT THE BOUNDARY OF TWO MATERIALS. HEAT FLOW WITHIN A (STATIC) MATERIAL CAN BE MODELED USING FOURIERS LAW.

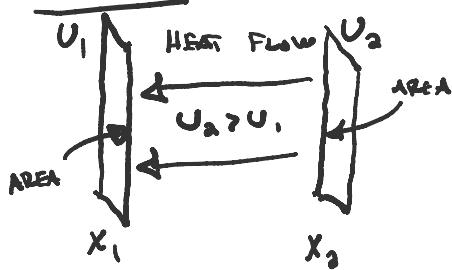
HEAT FLUX: THE RATE OF HEAT

HEAT FLOW (IN POSITIVE X DIR)

PER UNIT TIME PER UNIT AREA

$$J(x) \xrightarrow{\text{USUALLY NOT } J \text{ FOR HEAT FLUX}} \frac{W}{m^2} = \frac{J}{Sm^2}$$

PICTURE:



FOURIERS LAW: HEAT FLUX INCREASES

AS ΔU INCREASES, AND DECREASES AS Δx INCREASES.

$J(x)$ PROPORTIONAL TO $\frac{\Delta U}{\Delta x}$ SO
FOR $\Delta x \ll 1$

$$J(x) = -K \frac{dU}{dx}, \frac{J}{Sm^2}$$

THIS IS SLICELY NONSTANDARD.

WHY $-KU'$? FOR $\Delta U = U(x_2) - U(x_1)$
SO IF $U(x_2) > U(x_1)$, i.e. $\Delta U > 0$
THEN HOTTER AT x_2 THEN AT x_1 , SO HEAT FLOWS FROM x_2 TO x_1 .

IF WE CHANGE X ORIENTATION

$$x \mapsto -x$$

THEN NEED TO CHANGE

$$\Delta U \mapsto x_1 - x_2$$

TO BE "RIGHT TO LEFT"

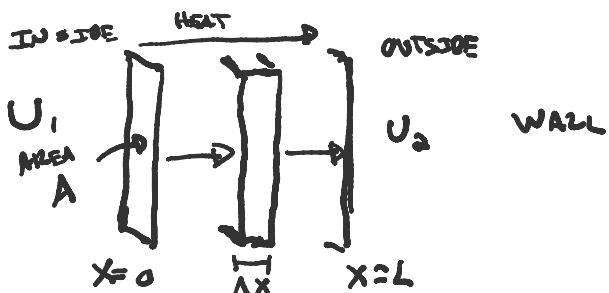


$x_1 > v$ then flow \rightarrow
 $x_2 \text{ TO } x_1$.

Now: $J(x)$ IS DENS. (CHARGE)
 OF HEAT FLOW AS WE MOVE IN
 X DIR. SO IF $\Delta v > 0$,
 CHANGE IN HEAT IS AGAINST
 DIR. OF INCREASING X . HENCE
 SIGN.

Def: THERMAL EQUILIBRIUM
 OCCURS WHEN NO TEMPS ARE
CHANGING.

Ex: HEAT CONDUCTION THROUGH A WALL



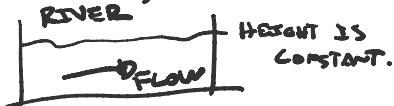
WANT TO USE FOURIER'S LAW TO
 UNDERSTAND HOW HEAT CONDUCTS
 THROUGH VOLUME.

IN SECTION OF WIDTH Δx

{ RATE OF CHANGE }
 { OF HEAT IN SECTION }

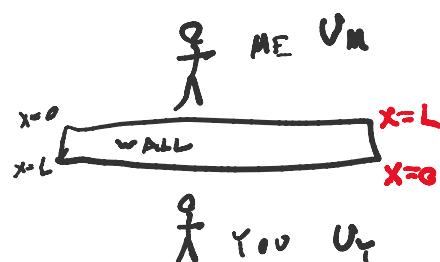
$$= \left\{ \begin{array}{l} \text{HEAT CONDUCTED} \\ \text{AT } x \end{array} \right\} - \left\{ \begin{array}{l} \text{HEAT COND.} \\ \text{AT } x+\Delta x \end{array} \right\}$$

AT THERMAL EQ, HEAT CONTENT IN
 SECTION IS CONSTANT. HEAT NOT
 BE FLOWING THROUGH BUT NO NET
 CHANGE, LIKE WATER IN RIVER



HERE:

$$\circ = J(x)A - J(x+\Delta x)A$$



I CHOSE x TO
 INCREASE FROM ME TO
 YOU, BUT YOU
 COULD CHOOSE x TO
 INCREASE FROM YOU
 TO ME

$$Q = J(x)A - J(x+\Delta x)A$$

SO CAN WRITE DIFF EQ:

$$Q = \lim_{\Delta x \rightarrow 0} \frac{J(x)A - J(x+\Delta x)A}{\Delta x}$$

$$= -A \frac{dJ}{dx}$$

$$= A \left(\frac{d}{dx} \left(-K \frac{du}{dx} \right) \right)$$

$$= A \cdot K \frac{d^2 u}{dx^2}$$

SECOND ORDER DIFF EQ.

WHAT IS SOLUTION TO

$$\frac{d^2 u}{dx^2} = 0, \text{ WITH } u(0) = u_1, \\ u(L) = u_2$$

INTEGRATE TWICE:

$$u = ax + b \quad \leftarrow \text{GENERAL SOLUTION TO DIFF EQ.}$$

WITH INITIAL CONDITIONS

$$u(0) = b = u_1,$$

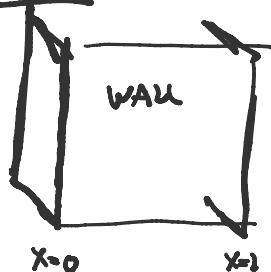
$$u(L) = aL + u_1 = u_2$$

so

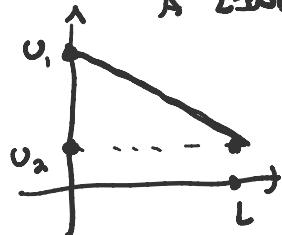
$$a = \frac{u_2 - u_1}{L}$$

$$u = \frac{u_2 - u_1}{L} x + u_1$$

PICTURE:

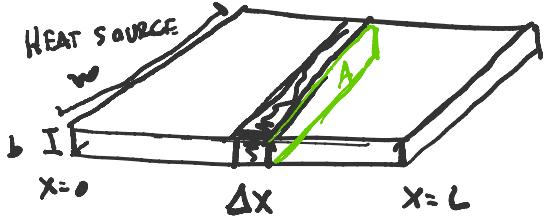


so TEMP IS
A LINE.



Ex: HEAT FIN FOR HEAT DISPOSITION

PICTURE:



HEAT CONDUCTS USING FOURIER'S LAW, AND IS TRANSFERED TO AIR USING NEWTON'S LAW. ASSUME U IS CONSTANT ALONG WIDTH WITH ONLY CHANGE IN X DIR.

w - WIDTH OF FIN

b - HEIGHT OF FIN

x - PARAMETERIZES LENGTH DIR

U_s - SURROUNDING TEMP, CONST.

AT EQUILIBRIUM:

$$\left\{ \begin{array}{l} \text{RATE OF CHANGE} \\ \text{IN } \Delta x \\ \text{OF HEAT} \end{array} \right\} = \left\{ \begin{array}{l} \text{CONDUCTED} \\ \text{AT } x \end{array} \right\} - \left\{ \begin{array}{l} \text{CONDUCTION} \\ \text{AT } x+\Delta x \end{array} \right\} - \left\{ \begin{array}{l} \text{HEAT TRANSFERRED} \\ \text{TO SURROUNDING} \end{array} \right\}$$

EQUATION:

$$0 = \underbrace{J(x)A - J(x+\Delta x)A}_{\substack{\text{AT EQUIL.} \\ \text{CONDUCTING}}} - Sh(U(x^*) - U_s)$$

• x^* IS A REP. POINT IN $[x, x+\Delta x]$.

• S IS SURFACE AREA. ASSUME FOR SIMPLICITY THAT $b \ll w$
SO NEGIGIBLE HEAT LOSS FROM SIDES. SO HEAT LOSS ONLY FROM TOP AND BOTTOM!

$$S = \underbrace{2w \cdot \Delta x}_{\substack{\text{TOP AND} \\ \text{BOTTOM}}} + \underbrace{2b \Delta x}_{\text{SIDES}}$$

• $A = bw$

SO

$$- \frac{A}{S} = \frac{1}{2} \left(\frac{1}{w} (T_w - T_{x+\Delta x}) \right)$$

SO

$$0 = bw \left(J(x) - J(x + \Delta x) \right) \\ - 2(w+b)\Delta x h (U(x^*) - U_s)$$

SO

$$0 = \lim_{\Delta x \rightarrow 0} \frac{1}{\Delta x} \left[bw \left(J(x) - J(x + \Delta x) \right) \right. \\ \left. - \Delta x 2(w+b) h (U(x^*) - U_s) \right]$$

$$0 = -bw \frac{dJ}{dx} - 2(w+b) h (U(x) - U_s)$$

SO

$$0 = -bw \left(-k \frac{d^2 U}{dx^2} \right) - 2(w+b) h (U - U_s)$$

REWRITE AS

$$\frac{d^2 U}{dx^2} = \beta (U - U_s)$$

WHERE $\beta = \frac{2(w+b)b}{bw}$.

THIS IS SECOND ORDER, LINEAR,
CONSTANT COEFF. EQUATION.

HOW DO WE SOLVE?

HOMOGENIOUS CASE:

$$ax'' + bx' + cx = 0 \quad (*)$$

WE CAN SOLVE BY TURNING INTO
A PAIR OF FIRST ORDER EQUATIONS.

IDEA: WRITE

$$x' = y$$

THEN (x) BECOMES

$$ay' + by + cx = 0$$

$$y' = Ax^2 + Cx + D$$

$$ay' + by + cx = 0$$

OR

$$\begin{aligned} y' &= -\frac{c}{a}x - \frac{b}{a}y \\ x' &= y \end{aligned}$$

$\Rightarrow \begin{cases} y' = Ax + B \\ x' = y \end{cases}$

FIRST ORDER,
LINEAR HOMO.
SYSTEM

SO SOLUTIONS ARE OF THE FORM

$$x = C_1 e^{r_1 t} + C_2 e^{r_2 t}$$

TO FIND r_i , JUST FEED $e^{rt} = x$
INTO (*):

$$ar^2 e^{rt} + bre^{rt} + ce^{rt} = 0$$

$$\Rightarrow ar^2 + br + c = 0$$

SO r_1 AND r_2 ARE GIVEN
BY FACTORING.