

General Information

Prof. Antonella Ferrara

<https://scholar.google.com/citations?user=r5JuMskAAAAJ&hl=en>

Course Teaching Material:

KIRO UNIPV <https://elearning.unipv.it/>

- [504462 - PROCESS CONTROL 2025-26 - PROF.SSA FERRARA ANTONELLA](#)

Lecture Time-table:

<http://www-3.unipv.it/ingserv/orario2526/1sem/insegnamenti/ProCont.html>

Exams:

<https://studentionline.unipv.it/esse3/Home.do>

<https://kirotesting.unipv.it/>



UNIVERSITÀ
DI PAVIA

Introduction

- Program of the course:

Advanced SISO control schemes:

Pre-filters and parallel compensators, two degrees of freedom control schemes, compensation of measurable disturbances, systems with delays and Smith Predictor, Padé approximation, decoupling in the frequency domain, control of open loop unstable systems.

Advanced MIMO control schemes:

Decoupling based control schemes, decentralized control, relative gain array.

PID controllers:

Features and properties. Rules for the empirical calibration. Wind-up and anti wind-up schemes.

Digital control:

Discrete-time systems. The concept of equilibrium for discrete-time systems. Stability of linear time-invariant discrete-time systems. Jury test. Digital control schemes. Zeta transform and its properties. Transfer functions in the z domain. Sampling and aliasing. Choice of the sampling time. Zero-order-Hold. Discretization of continuous-time controllers. Bilinear transformation, Euler and Tustin methods.

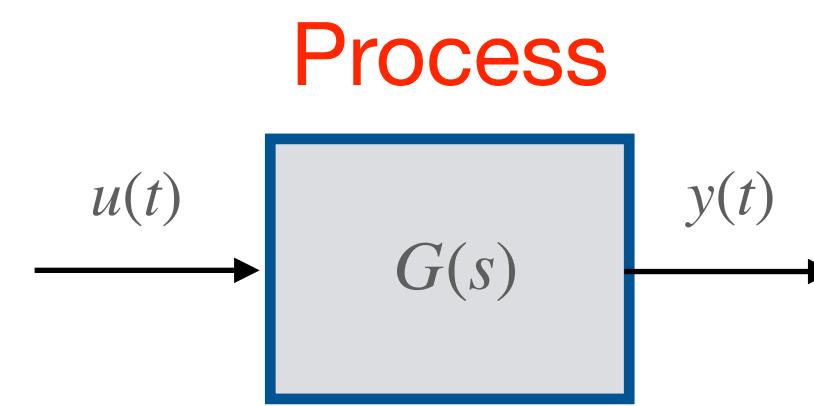


Introduction

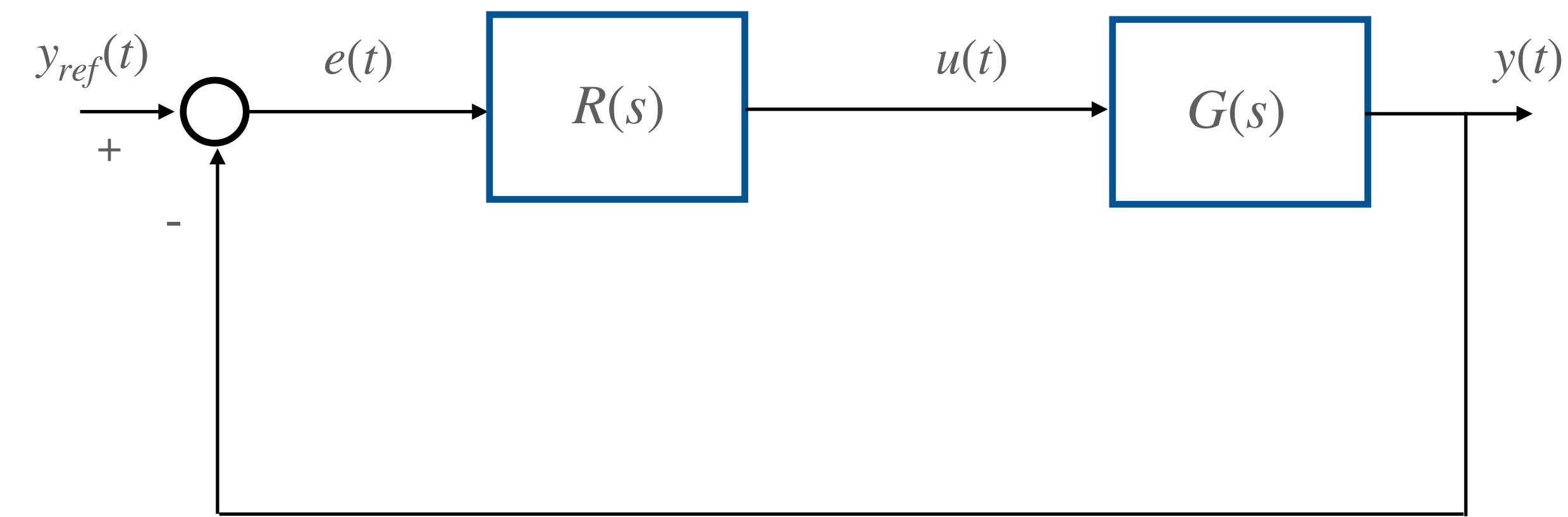
- Some of the figures in these slides, kindly provided by McGraw-Hill, are those of the Textbook:



Design of PID Controllers



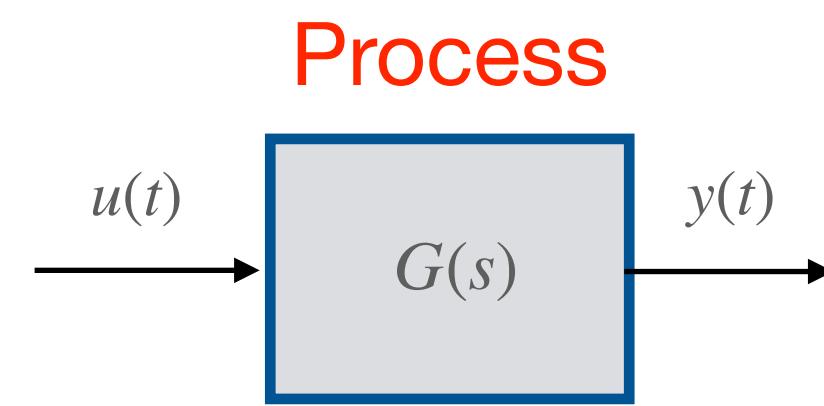
$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



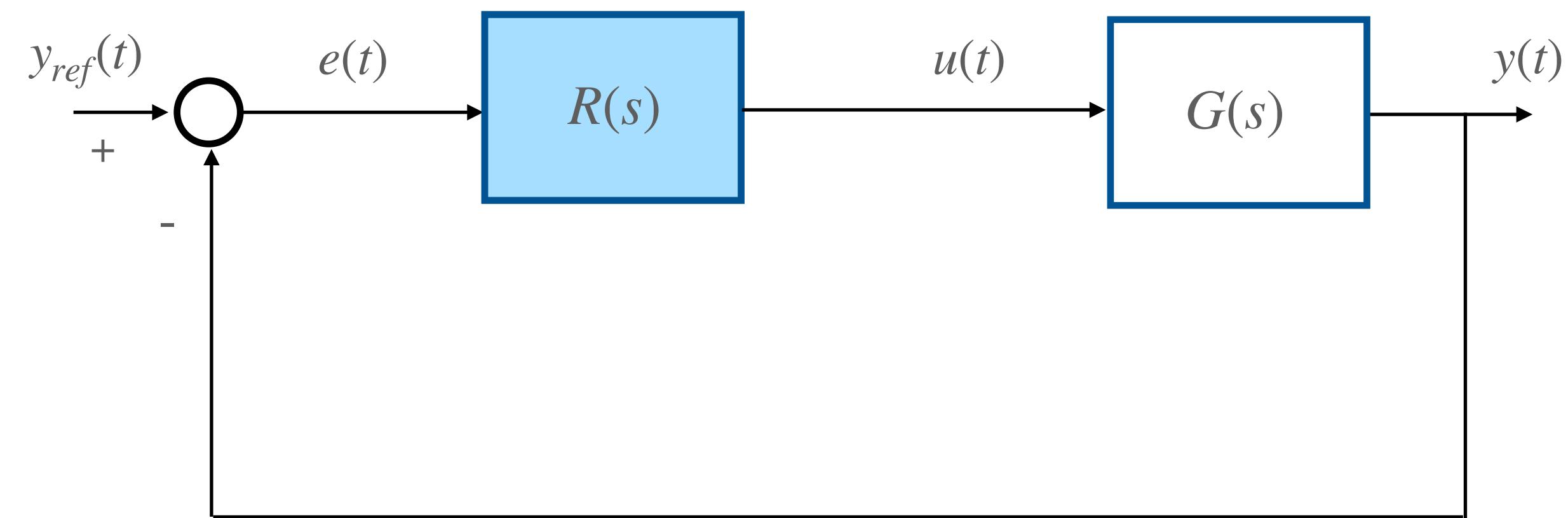
Unitary Feedback Control Scheme



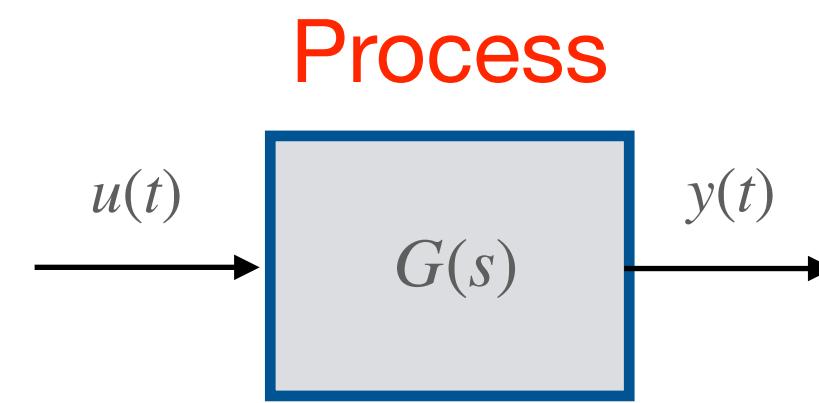
Design of PID Controllers



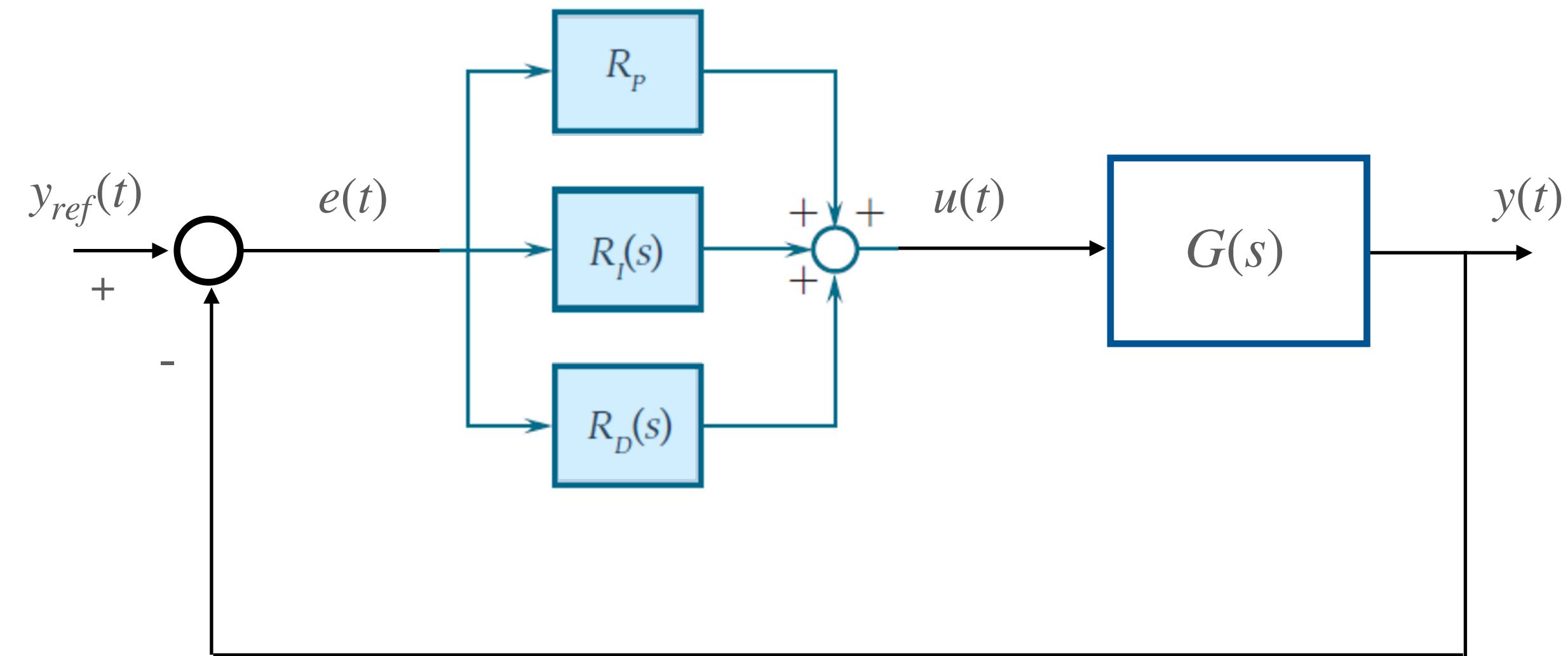
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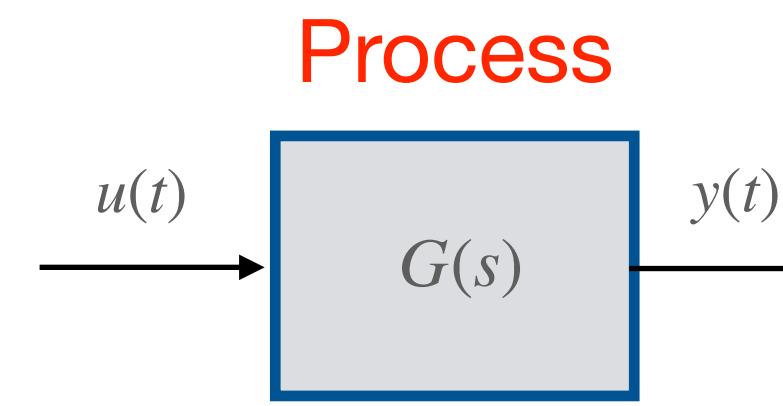
Design of PID Controllers



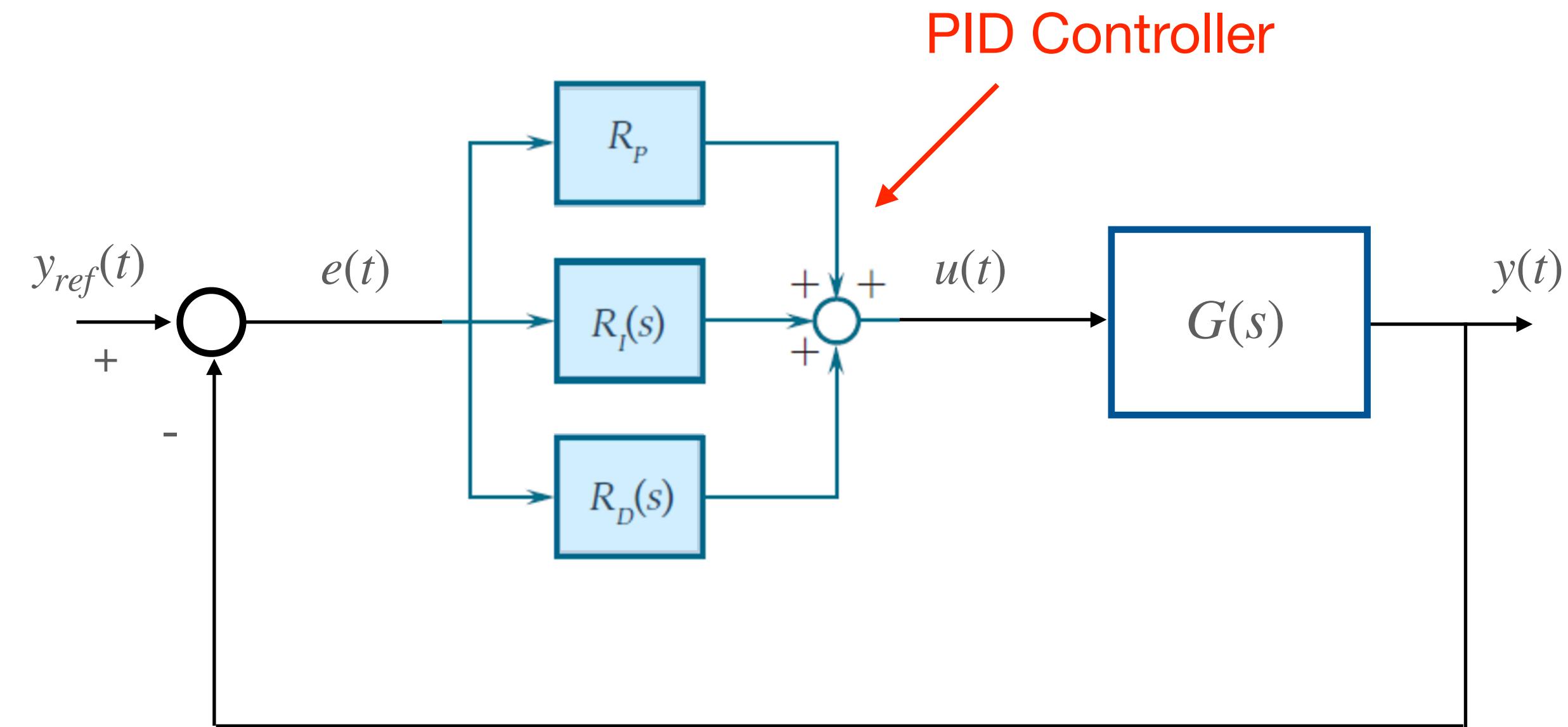
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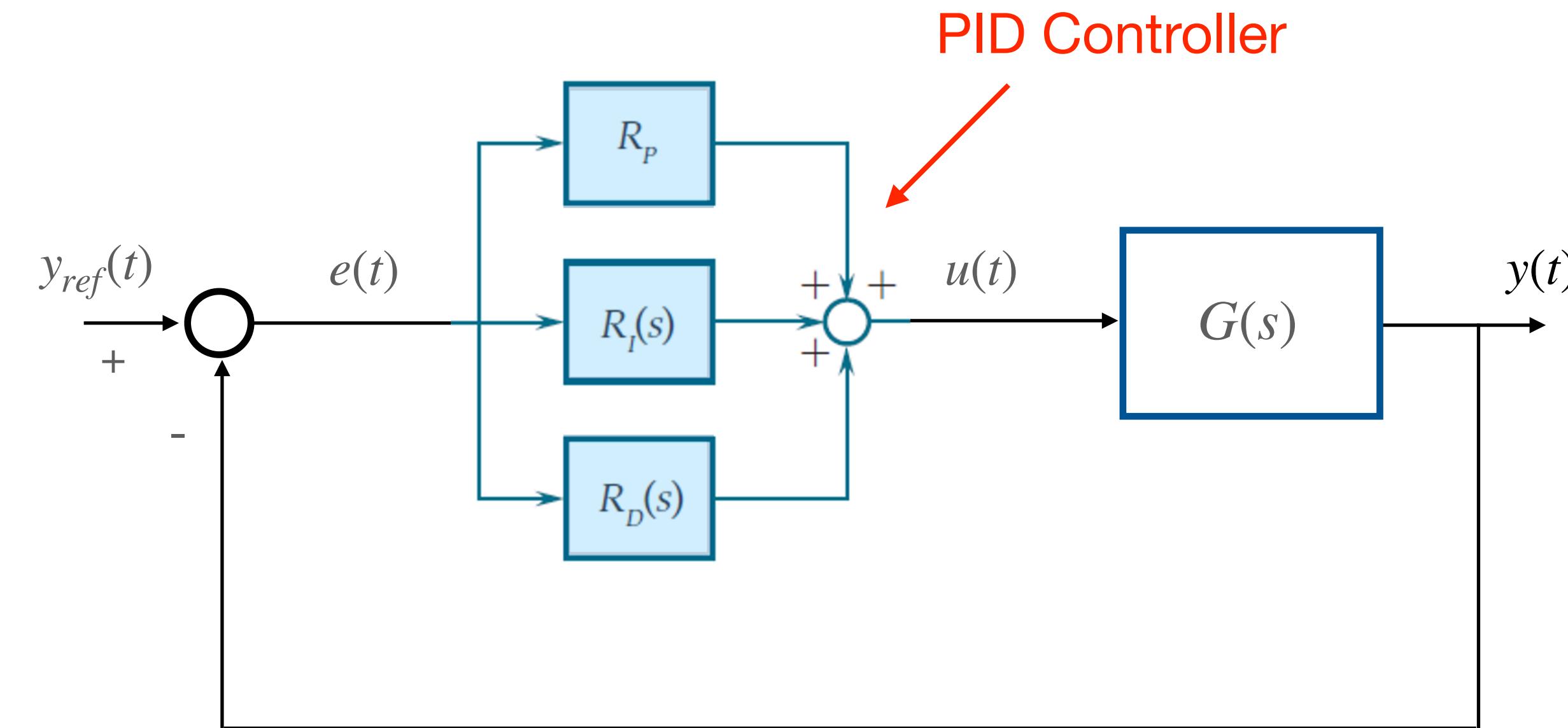
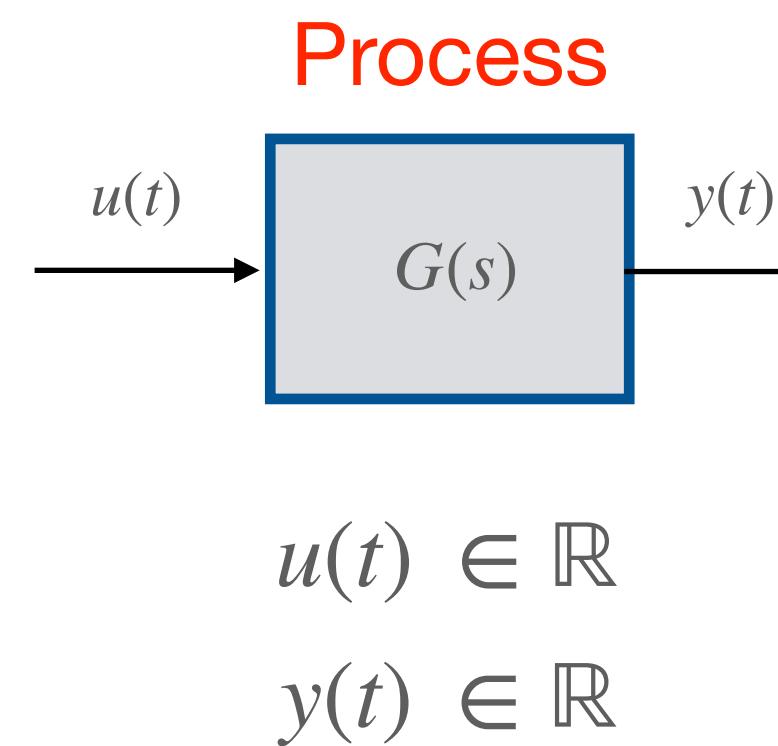
Design of PID Controllers



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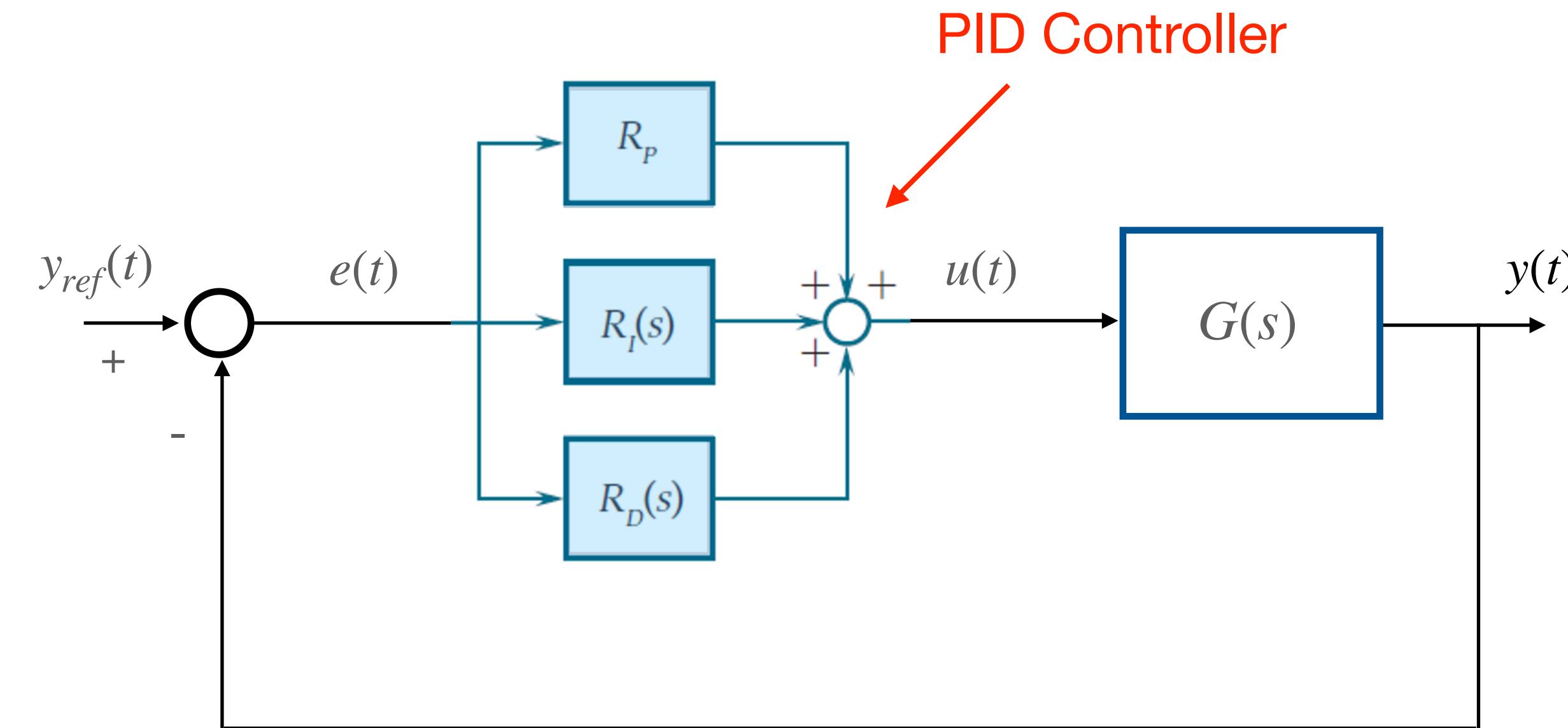
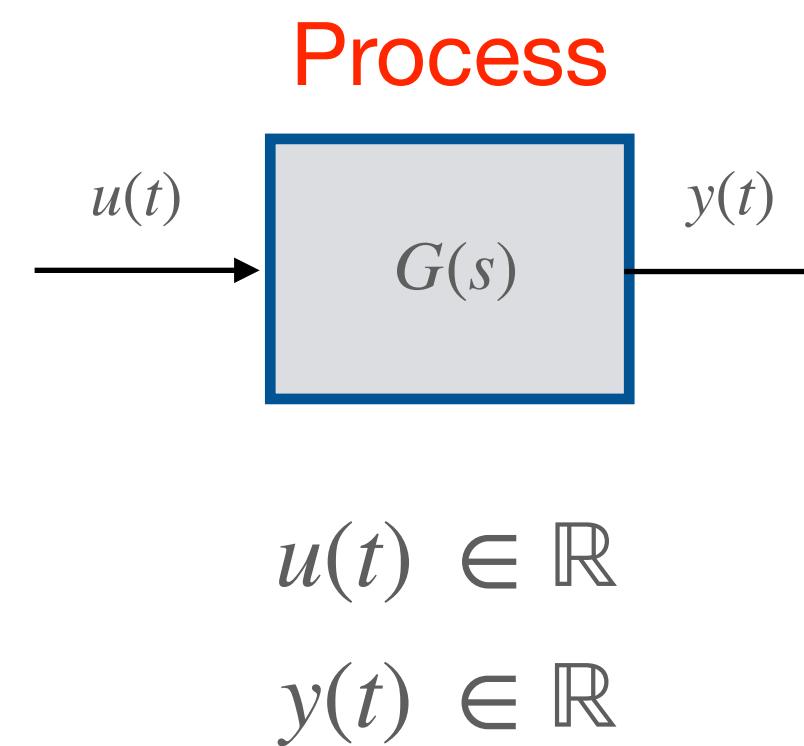
Design of PID Controllers



Ideal PID Controller: $u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \frac{de(t)}{dt}$



Design of PID Controllers

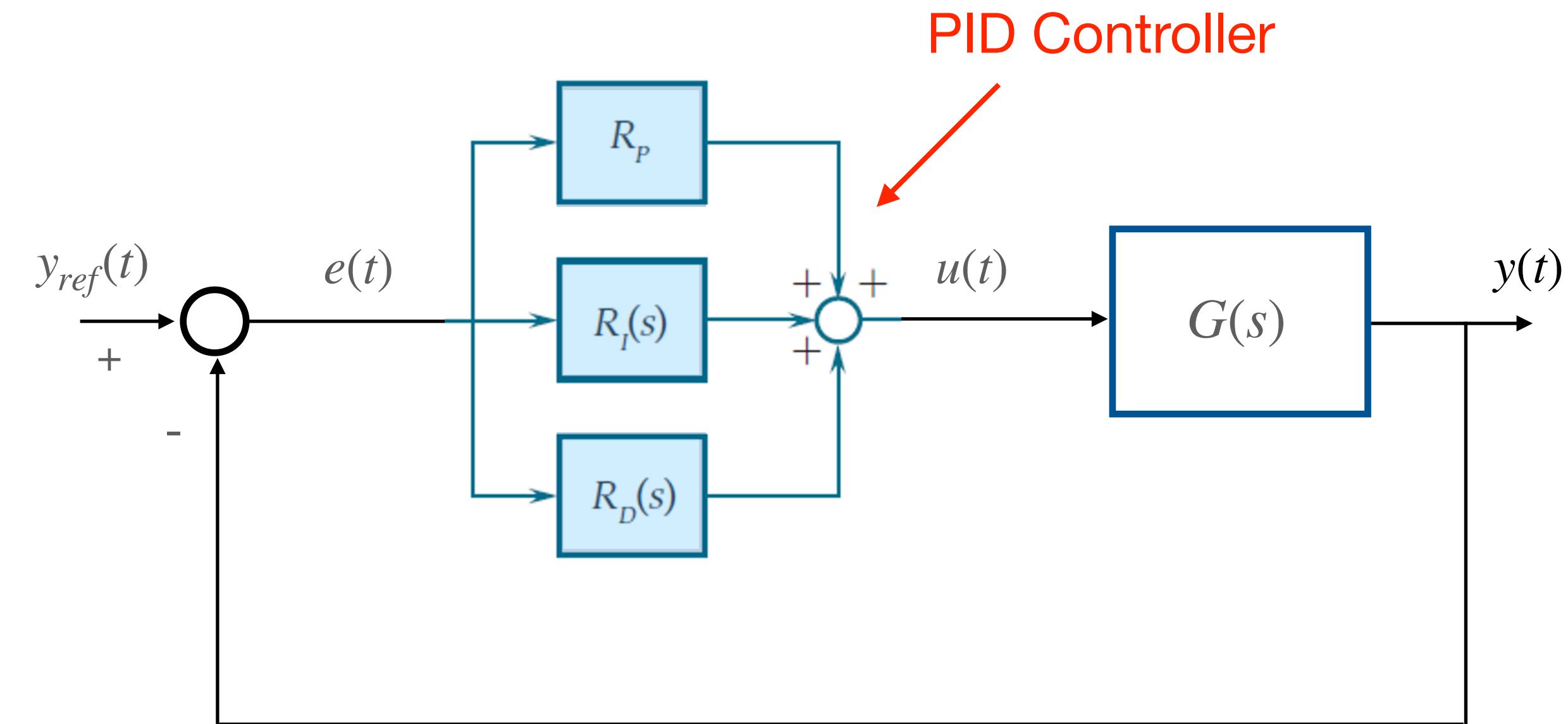
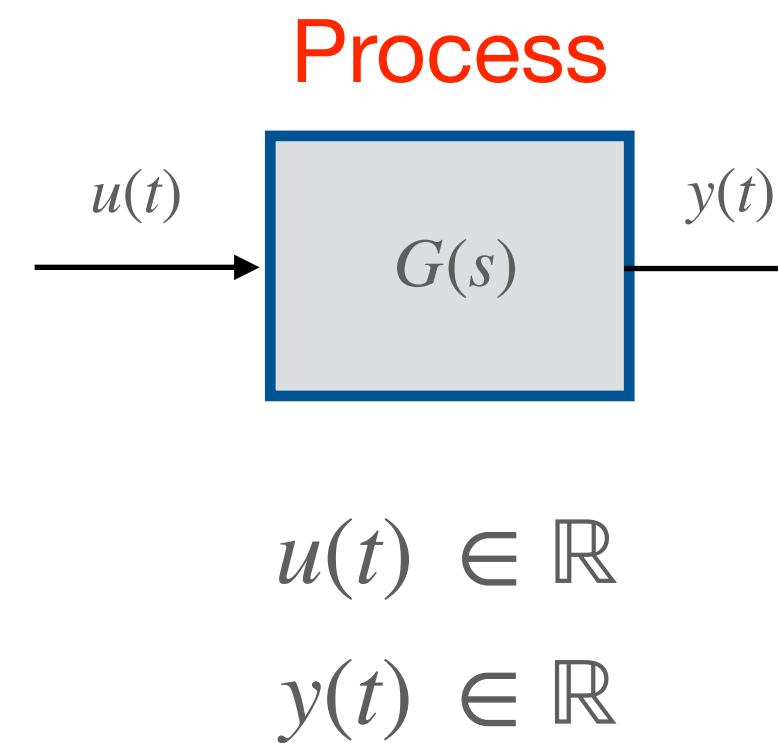


Ideal PID Controller: $u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \frac{de(t)}{dt}$

$$\mathcal{L}\{u(t)\} = U(s) = \mathcal{L}\left\{ K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \frac{de(t)}{dt} \right\} = \left(K_P + \frac{K_I}{s} + K_D s \right) E(s)$$



Design of PID Controllers



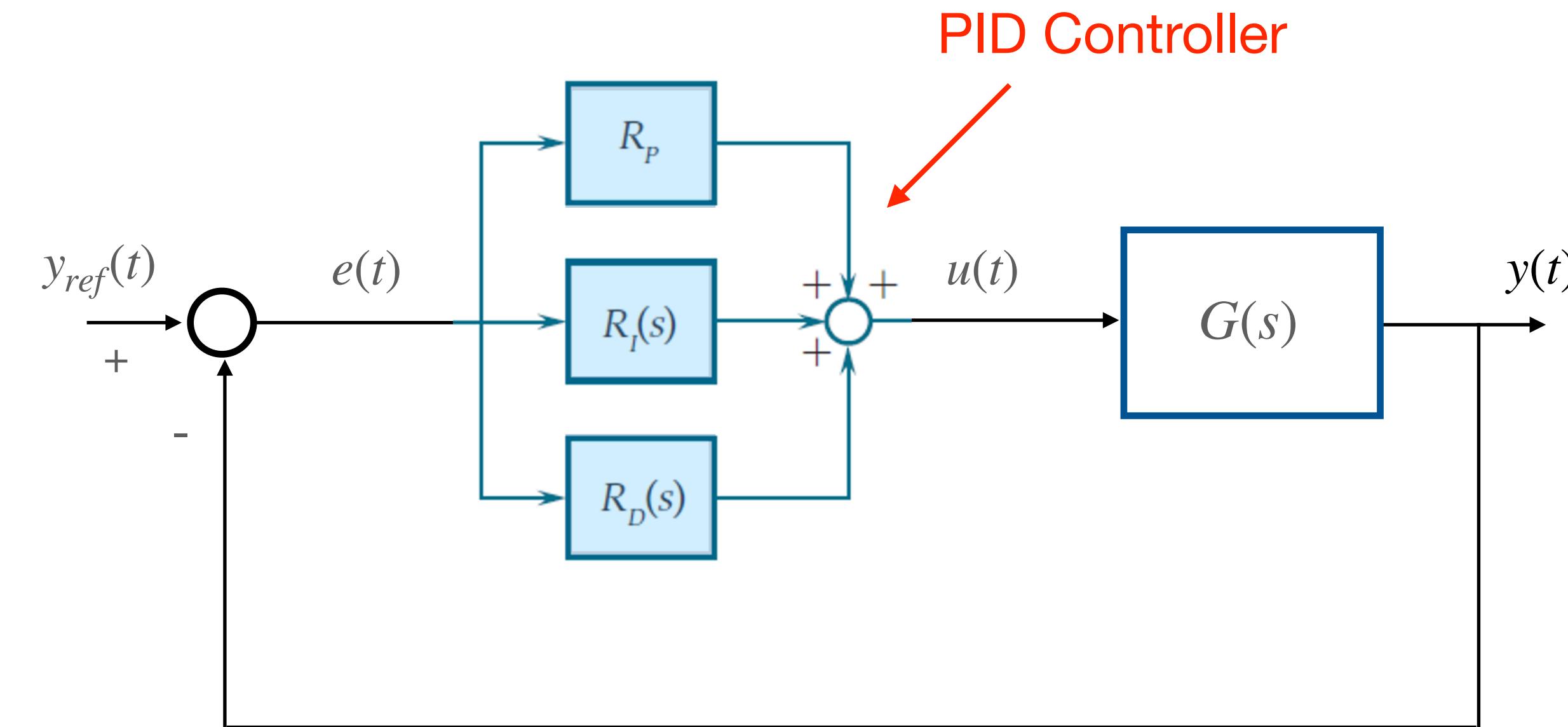
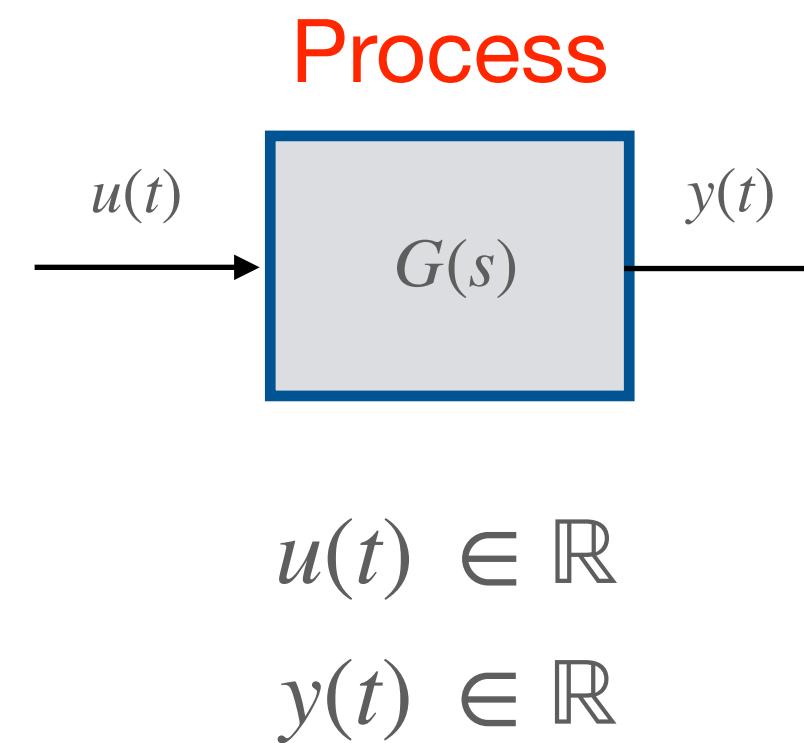
$$R_{PID_{id}}(s) = \frac{U(s)}{E(s)} = K_P + \frac{K_I}{s} + K_D s = \frac{K_D s^2 + K_P s + K_I}{s}$$

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Design of PID Controllers



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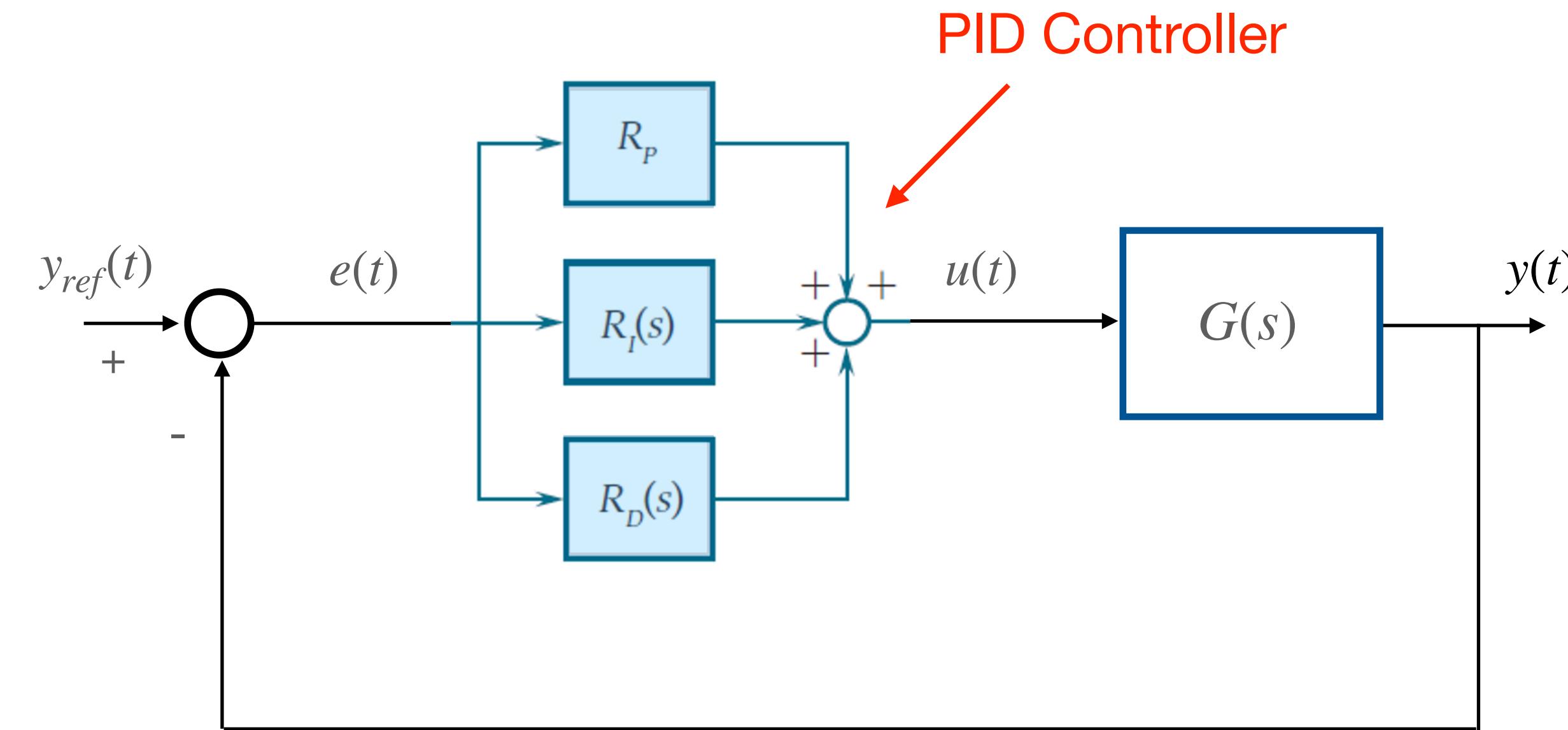
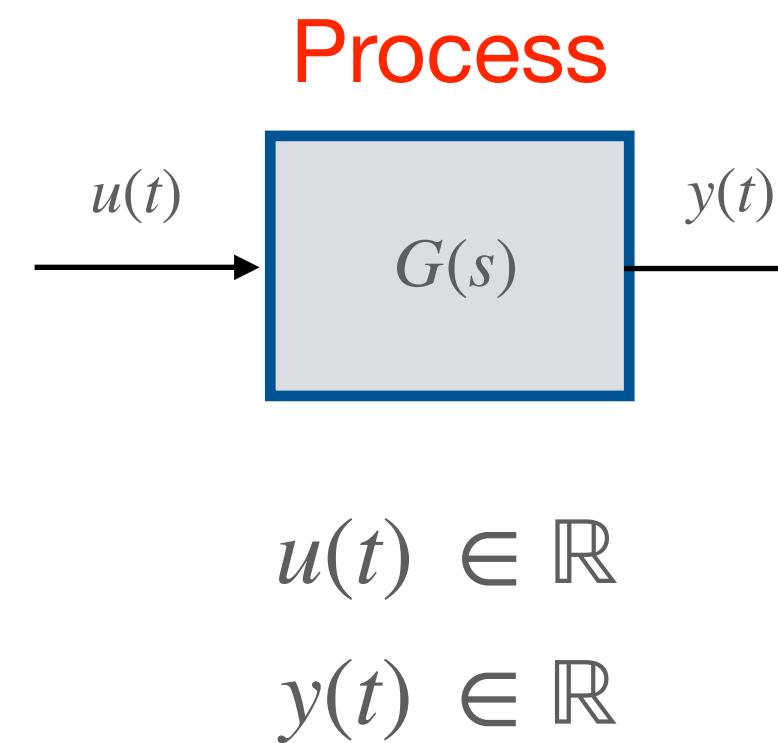
It is not causal

Ideal PID Controller: $u(t) = K_P e(t) + K_I \int_0^t e(\tau) d\tau + K_D \frac{de(t)}{dt}$

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Design of PID Controllers



Alternative representation:

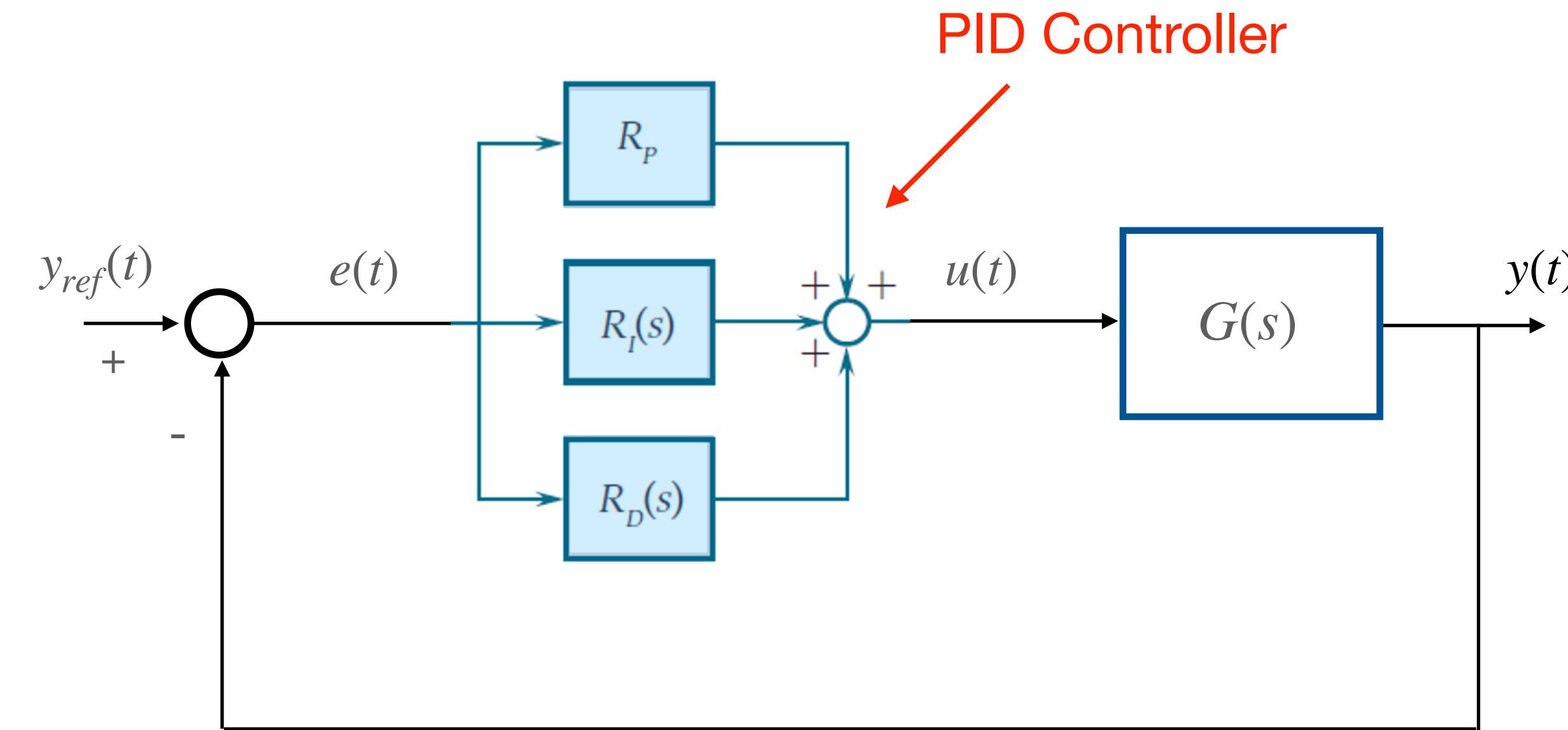
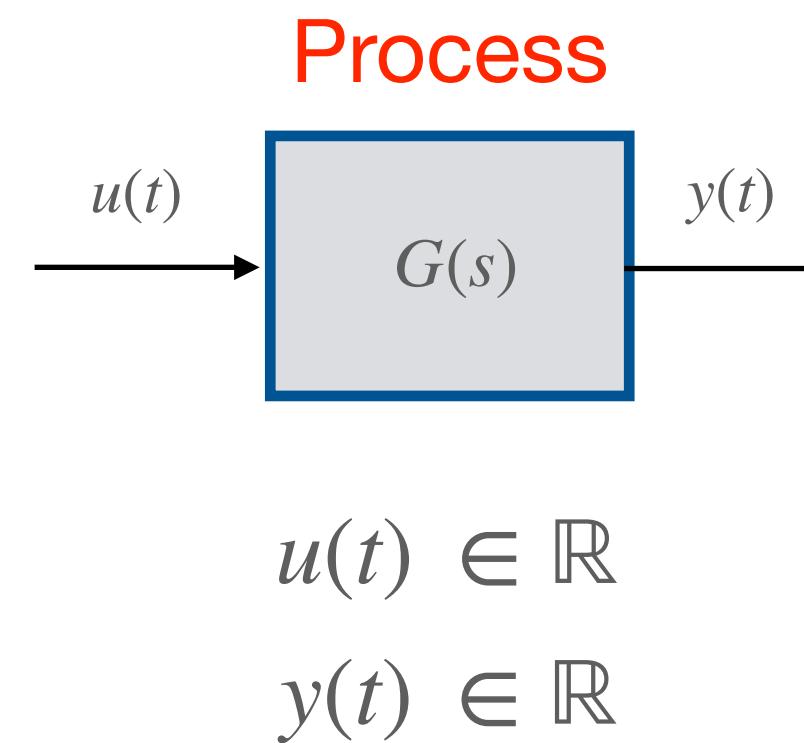
$$R_{PID_{id}}(s) = \frac{U(s)}{E(s)} = K_P + \frac{K_I}{s} + K_D s = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$

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Design of PID Controllers



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To make it causal

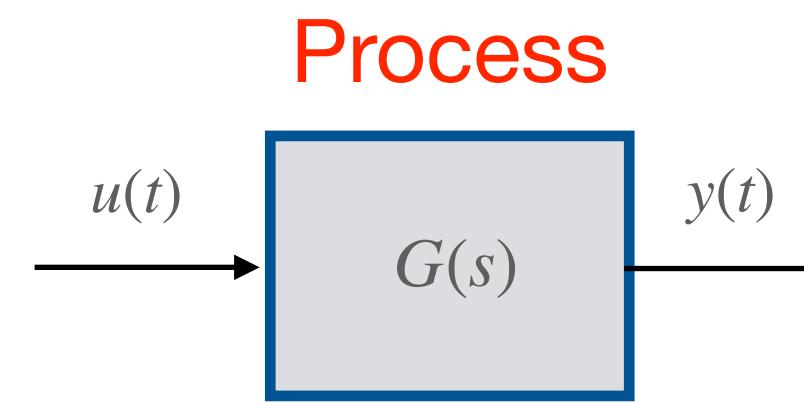
$$R_{PID}(s) = K_P \left(1 + \frac{1}{T_I s} + \frac{T_D s}{1 + \frac{T_D}{N} s} \right)$$

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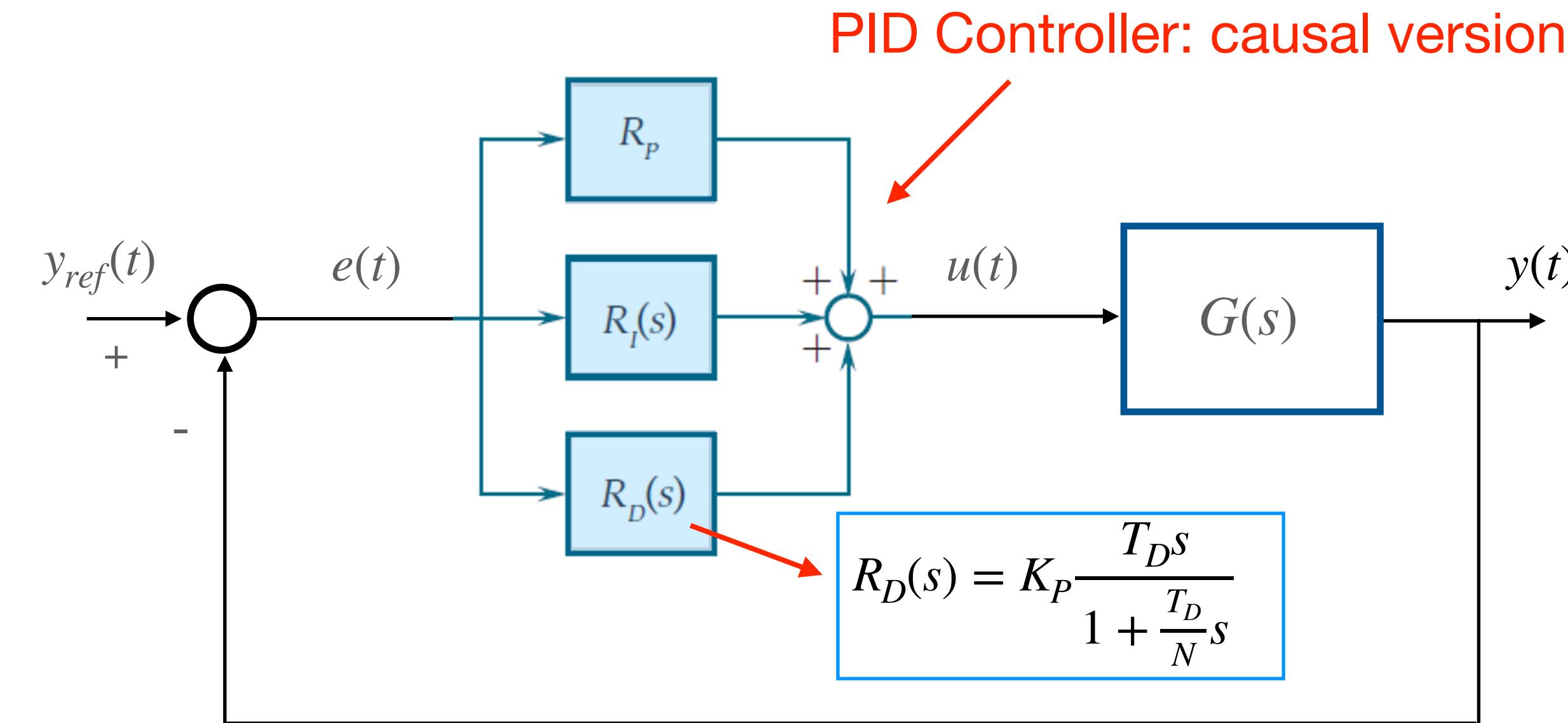
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Design of PID Controllers



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



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To make it
causal

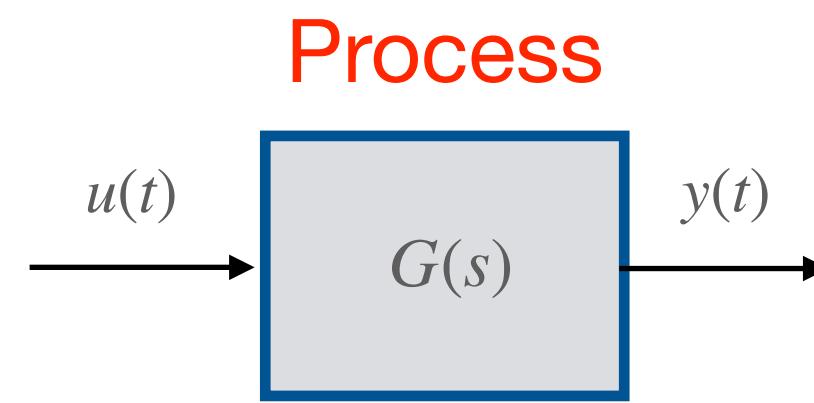
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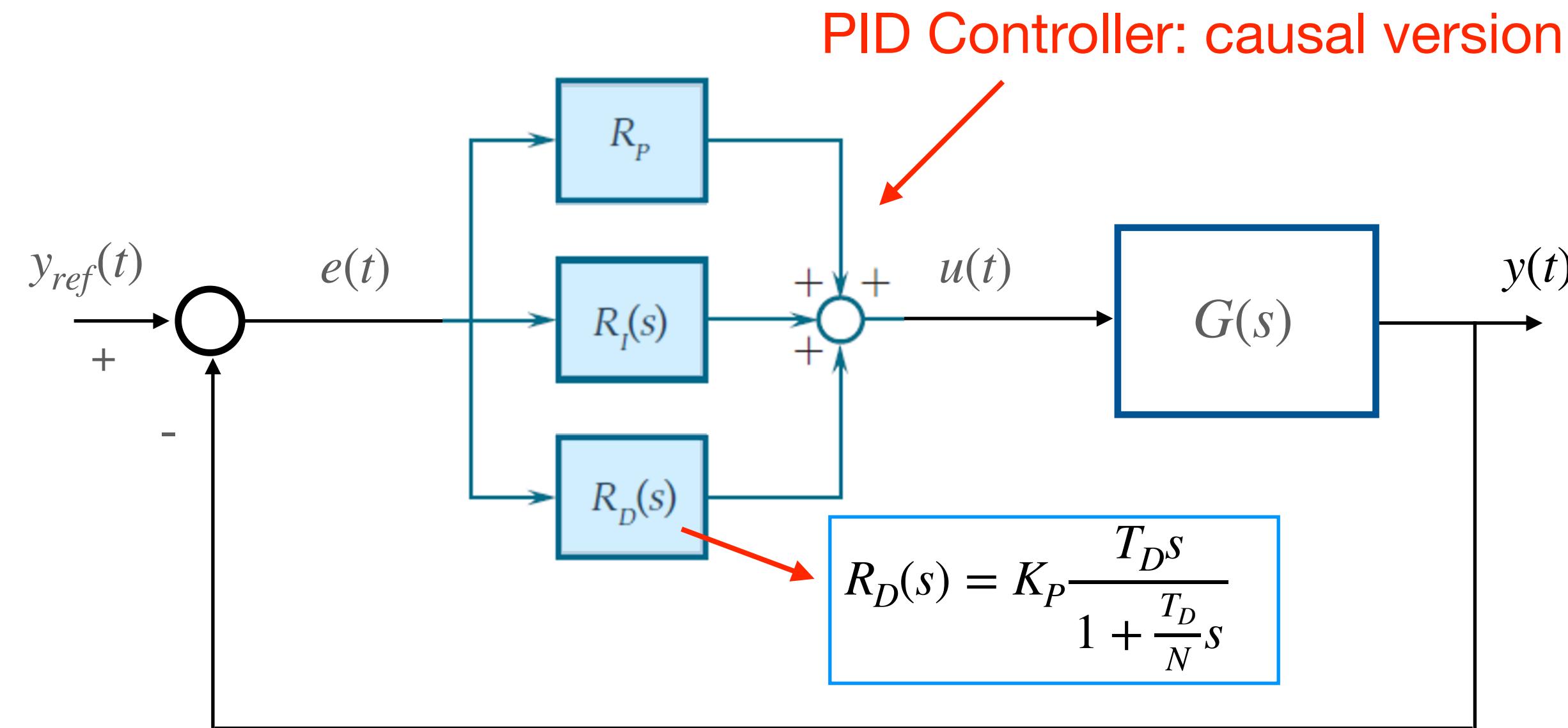
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Design of PID Controllers



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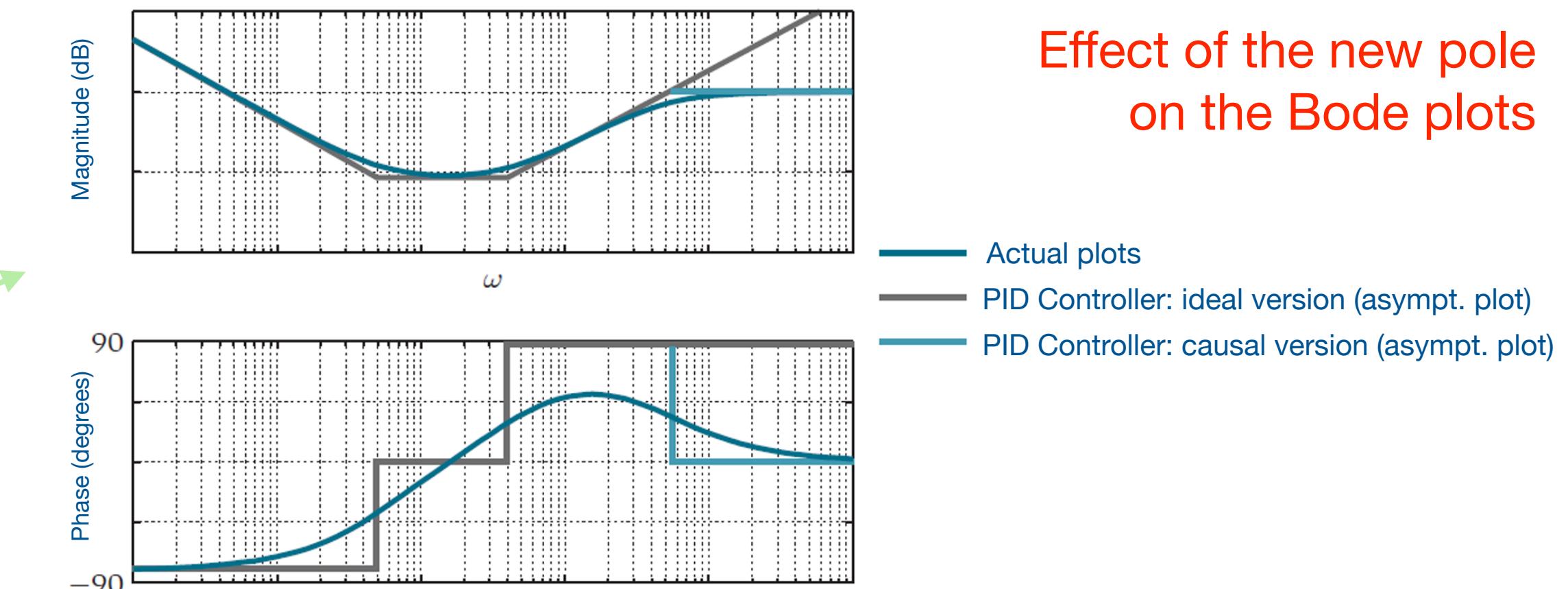


Alternative representation:

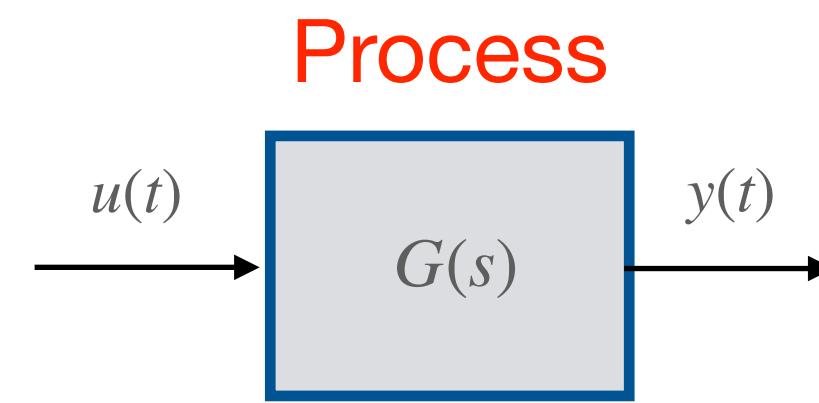
$$R_{PID_{id}}(s) = \frac{U(s)}{E(s)} = K_P + \frac{K_I}{s} + K_D s = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$

It is causal

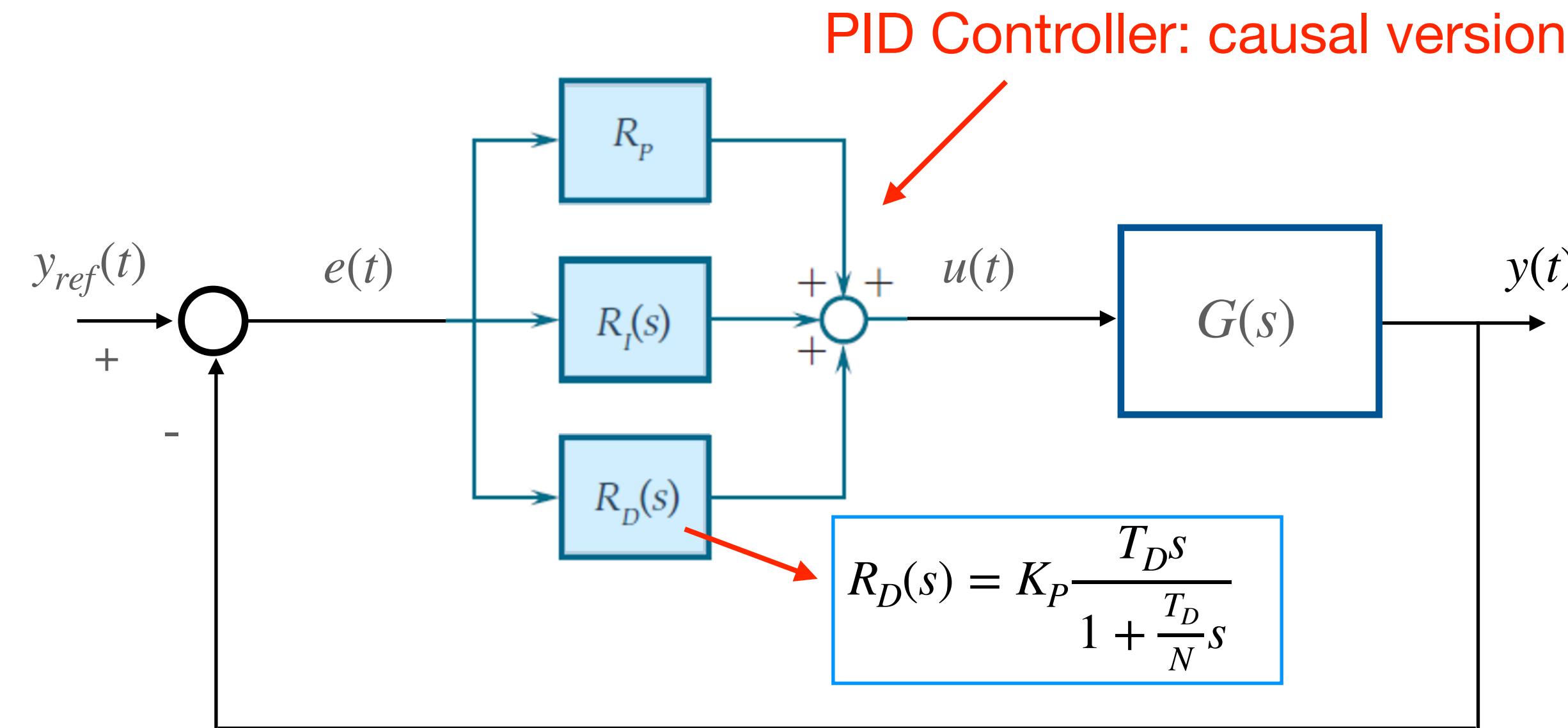
$$R_{PID}(s) = K_P \left(1 + \frac{1}{T_I s} + \frac{T_D s}{1 + \frac{T_D}{N} s} \right)$$



Design of PID Controllers



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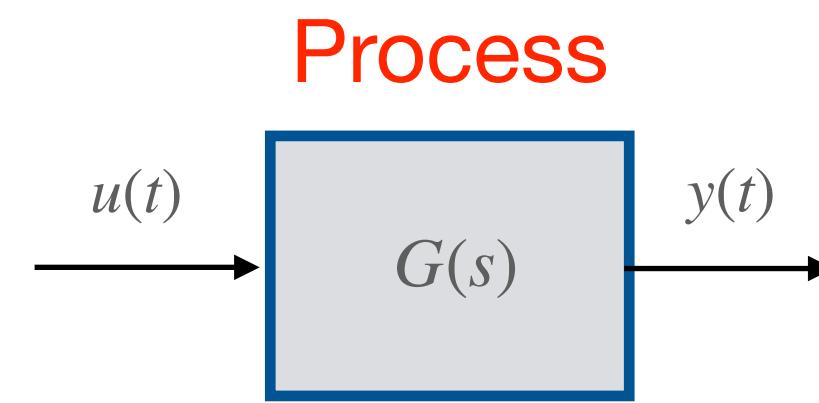
$$R_{PID}(s) = K_P \left(1 + \frac{1}{T_I s} + \frac{T_D s}{1 + \frac{T_D}{N} s} \right)$$

Effect of the new pole on the PID zeros:

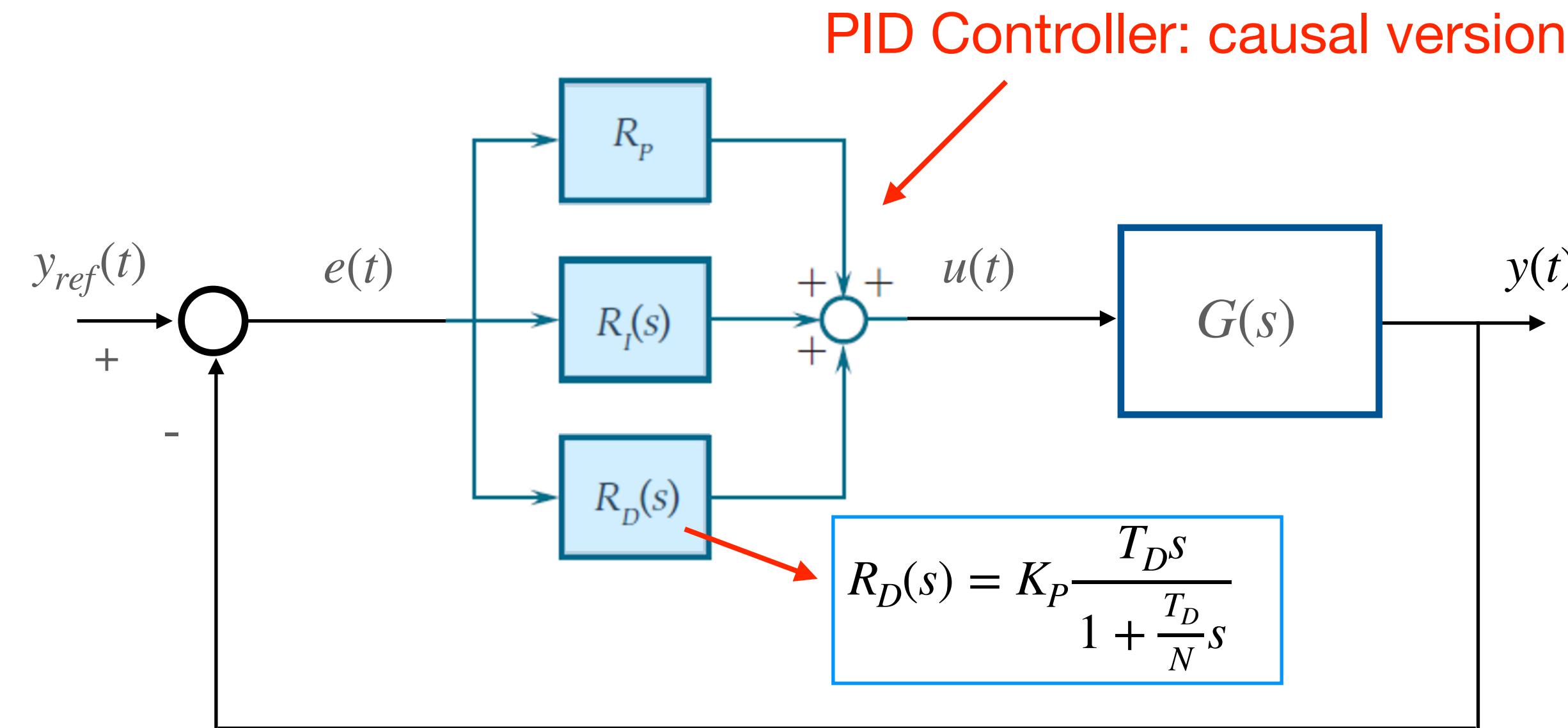
$$R_{PID}(s) = K_P \left(1 + \frac{1}{T_I s} + \frac{T_D N s}{T_D s + N} \right) = \frac{K_P \left[T_D s^2 + \left(1 + \frac{T_D}{T_I} \right) s + \frac{1}{T_I} N \right]}{s(T_D s + N)}$$



Design of PID Controllers



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



Alternative representation:

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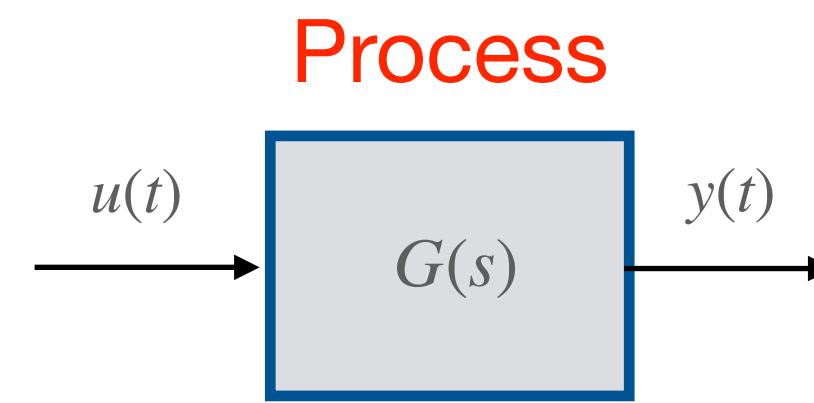
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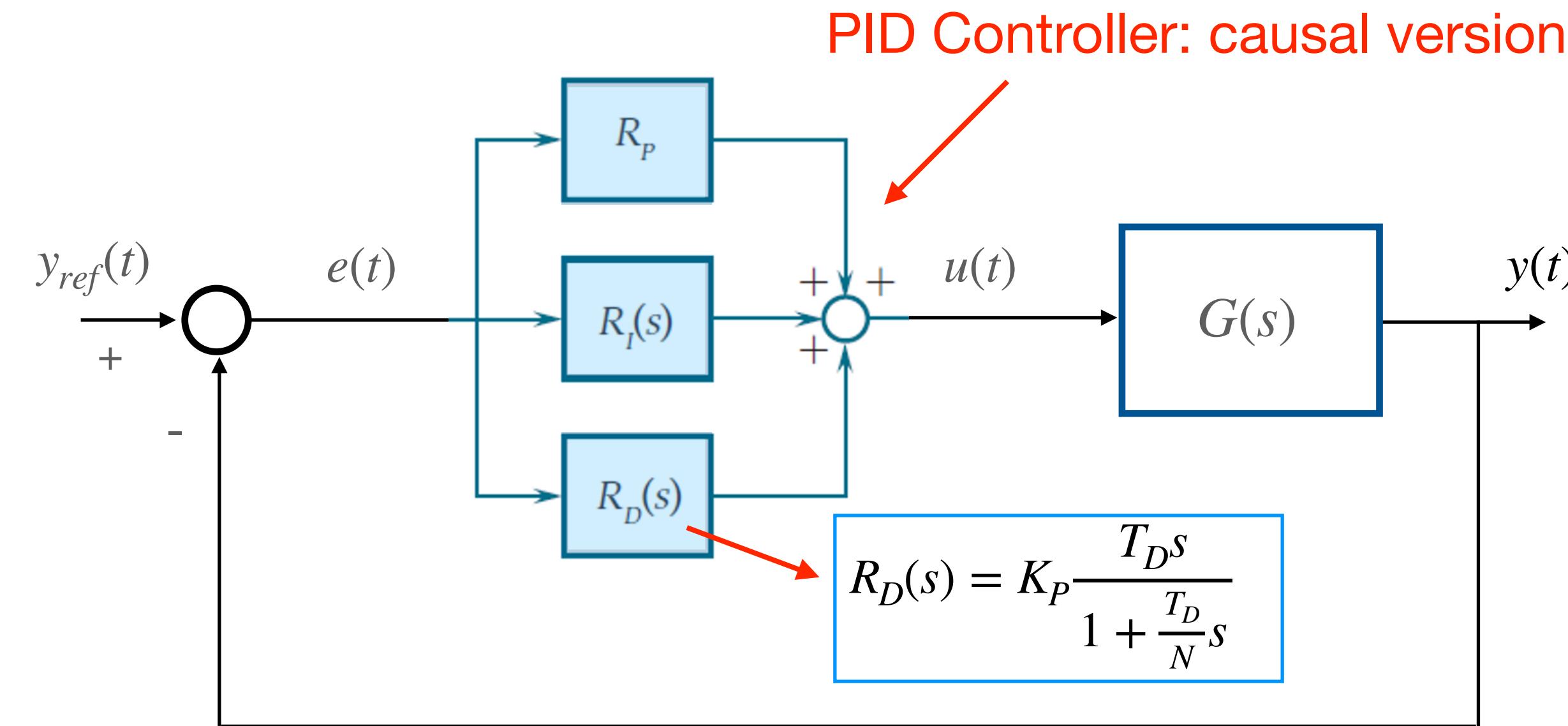
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Design of PID Controllers



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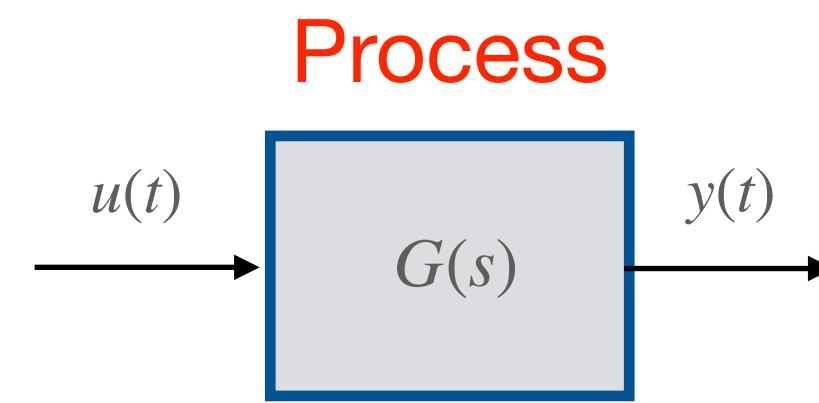
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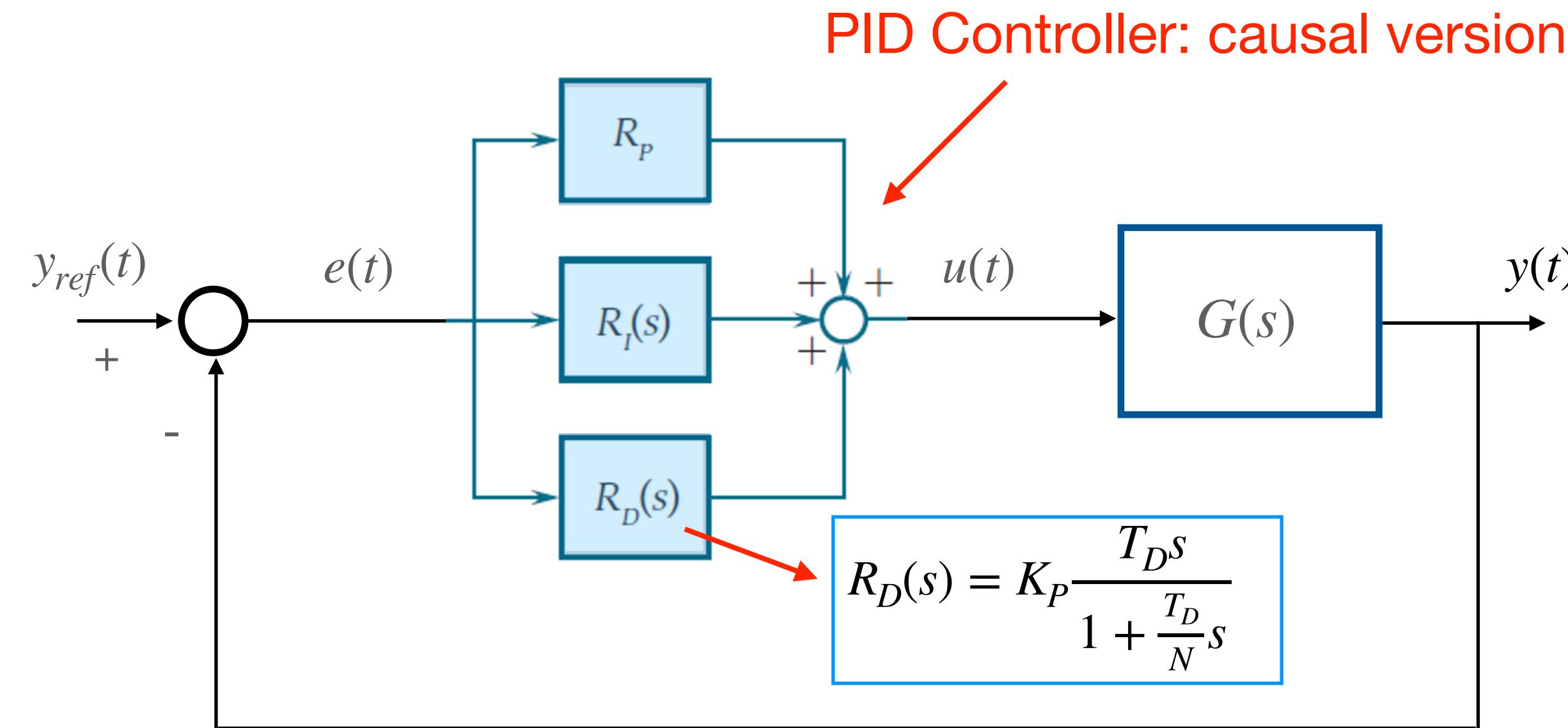
+∞ the zeros are practically the same as before



Design of PID Controllers



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



Alternative representation:

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It is causal

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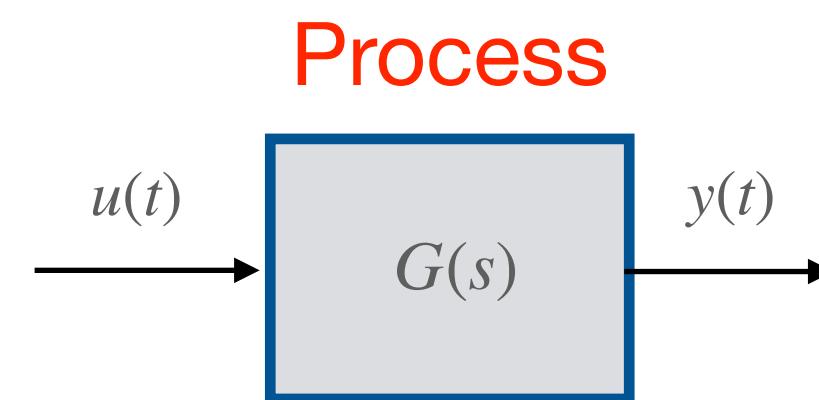
when $T_I = 4T_D$ the zeros coincide in $s = -\frac{1}{2T_D}$

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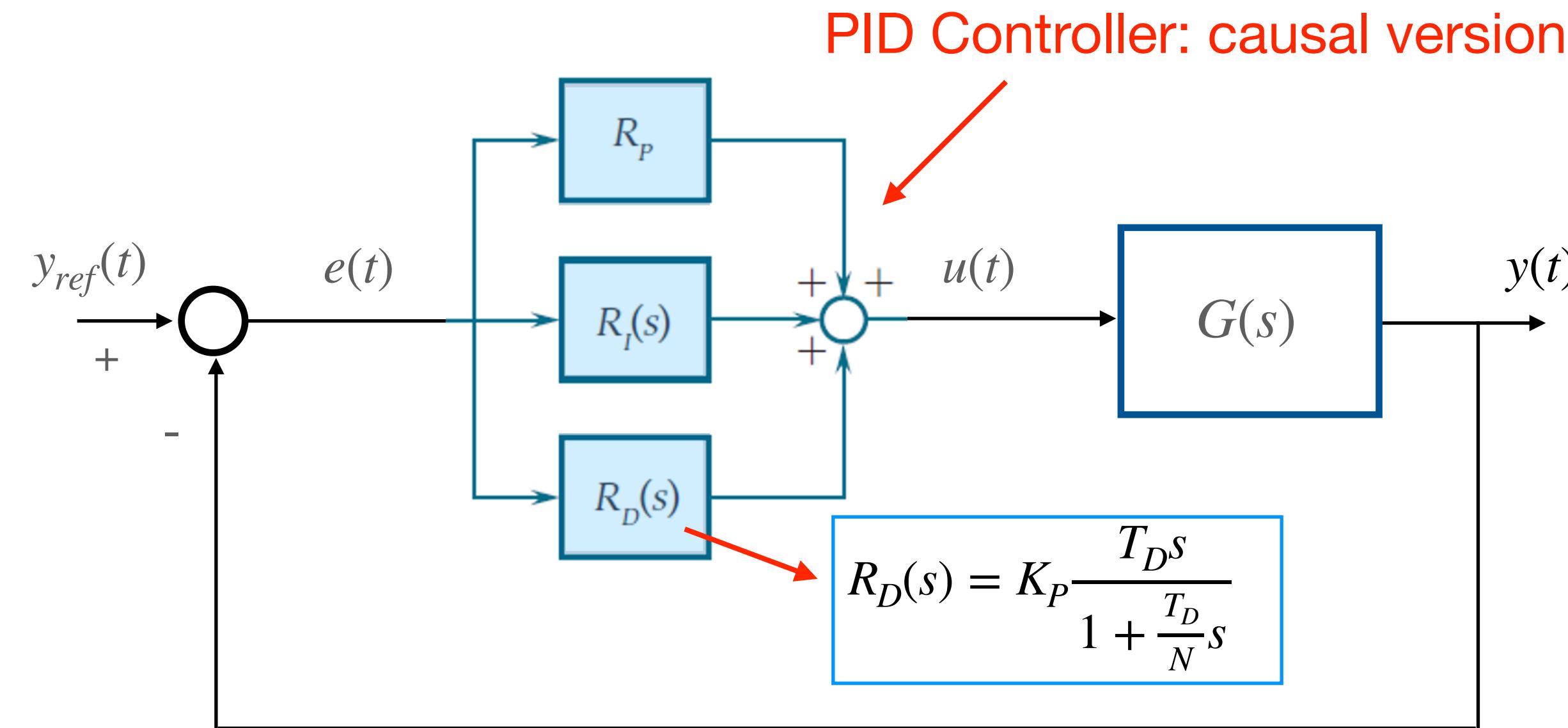
+∞ the zeros are practically the same as before



Design of PID Controllers



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



$$R_D(s) = K_P \frac{T_D s}{1 + \frac{T_D}{N} s}$$

Alternative representation:

$$R_{PID_{id}}(s) = \frac{U(s)}{E(s)} = K_P + \frac{K_I}{s} + K_D s = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$

It is causal

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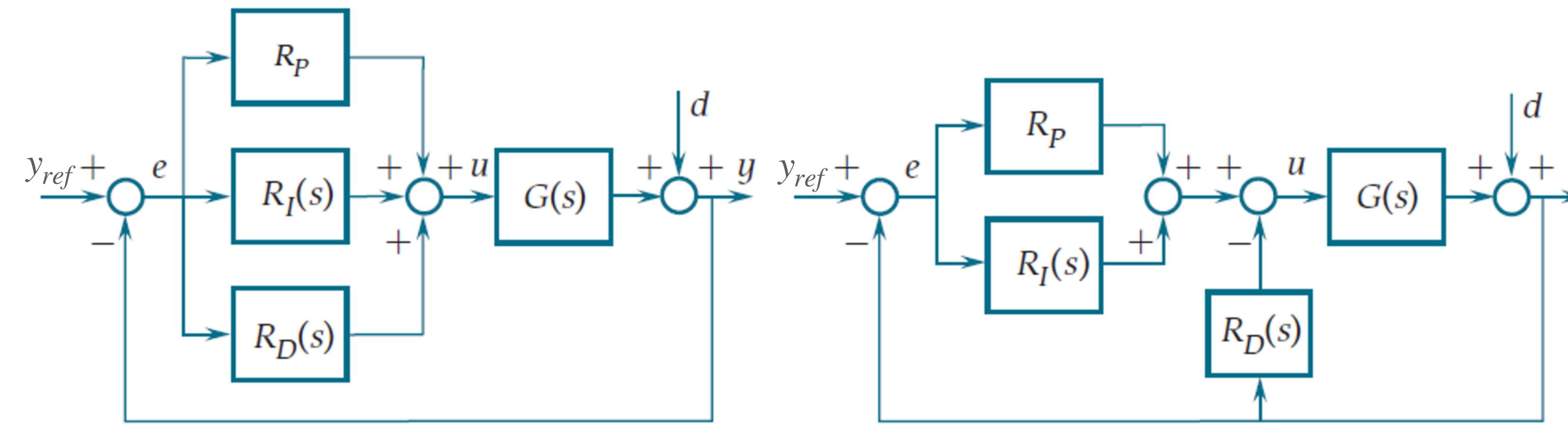
choice made to simplify
PID parameter tuning
when $T_I = 4T_D$ the zeros coincide in $s = -\frac{1}{2T_D}$

$$R_{PID}(s) = K_P \left(1 + \frac{1}{T_I s} + \frac{T_D N s}{T_D s + N} \right) = \frac{K_P \left[T_D s^2 + \left(1 + \frac{T_D}{T_I} \right) s + \frac{1}{T_I} N \right]}{s(T_D s + N)}$$

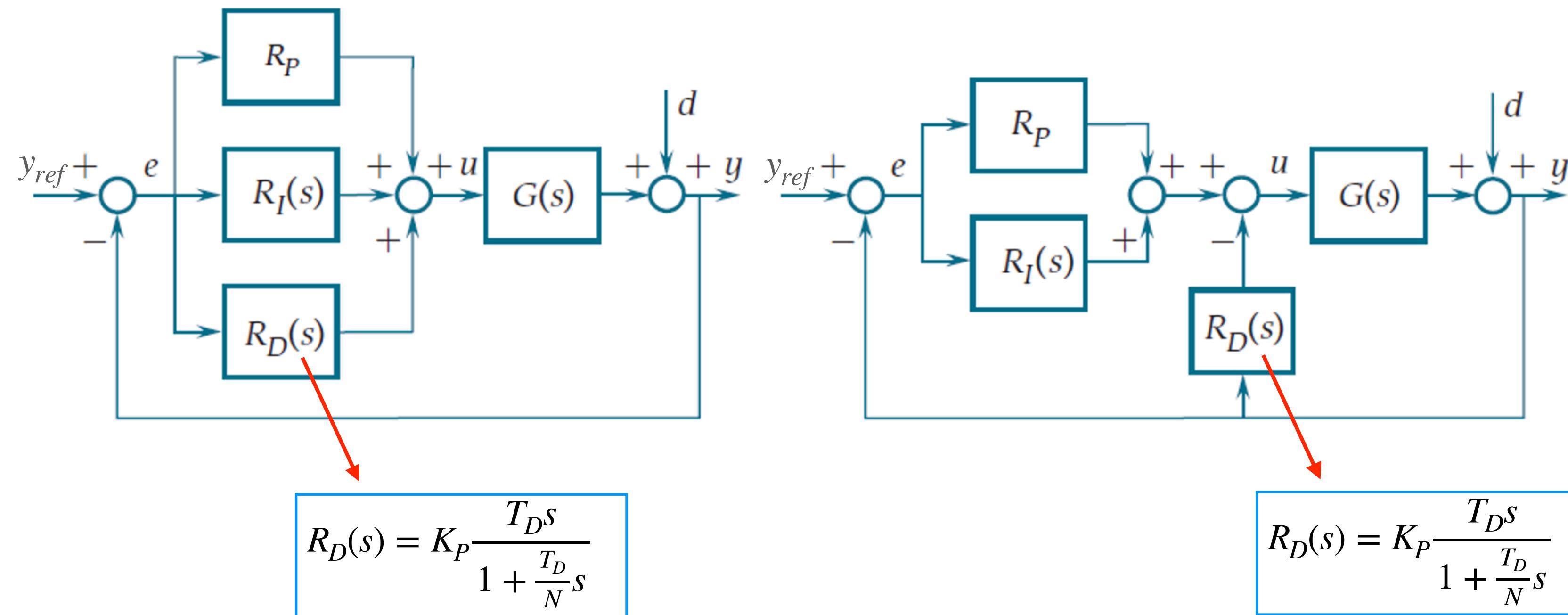
+∞ the zeros are practically the same as before



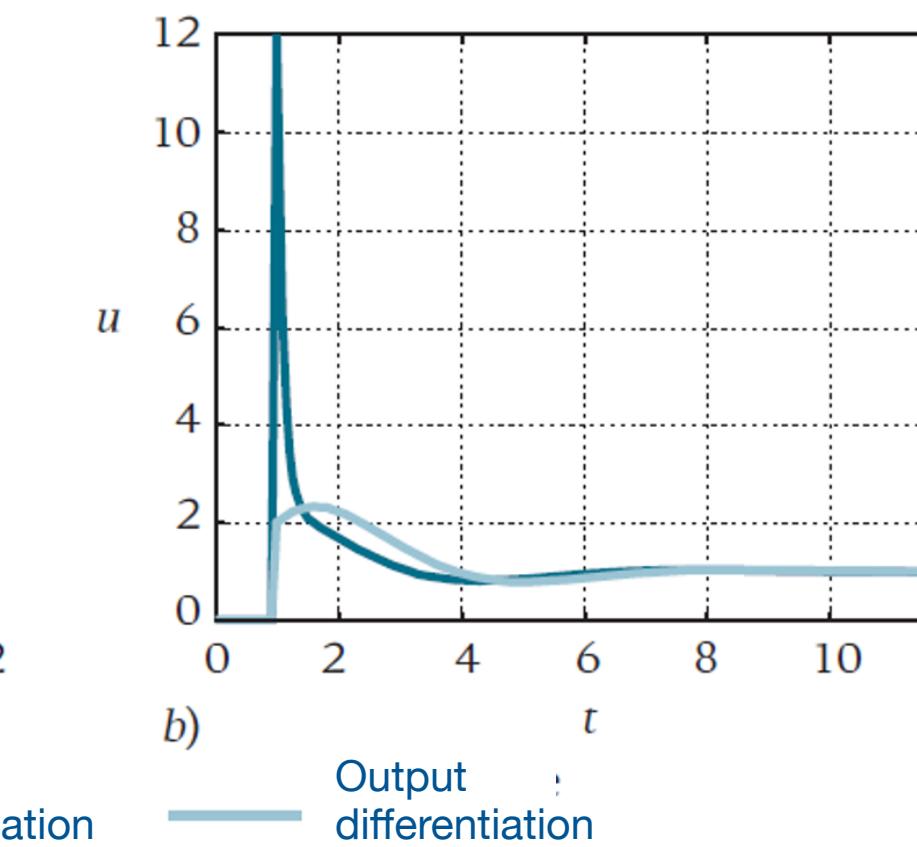
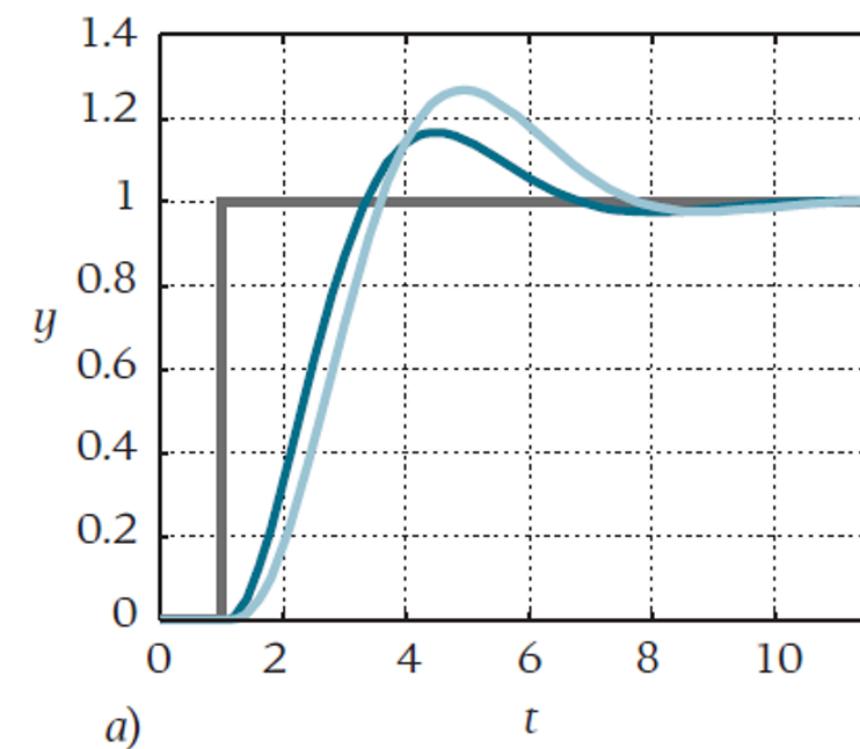
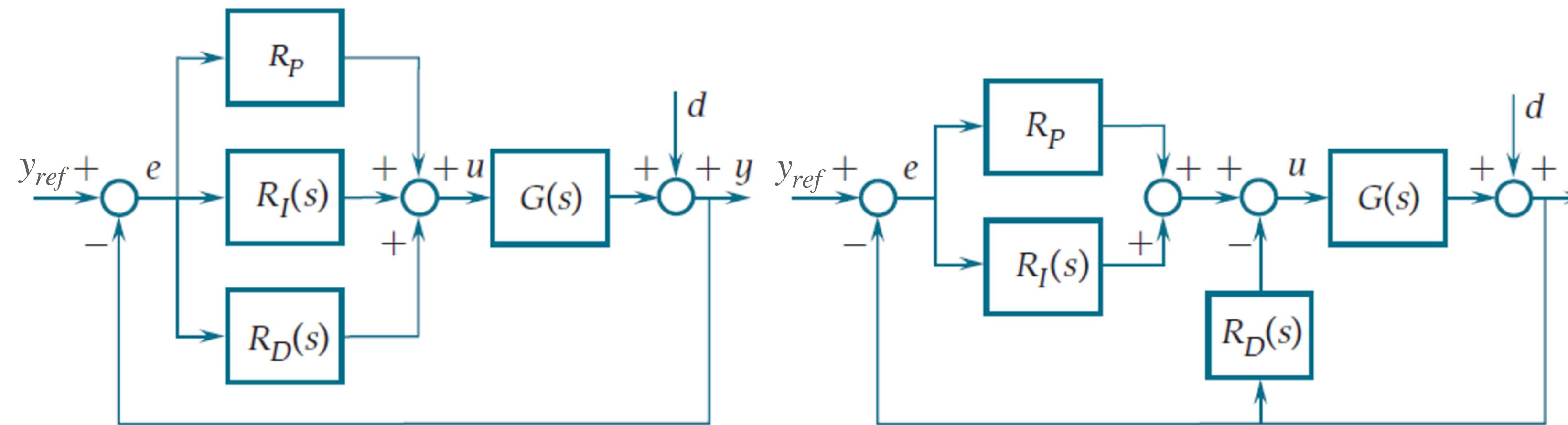
Practical Implementation of PID Controllers



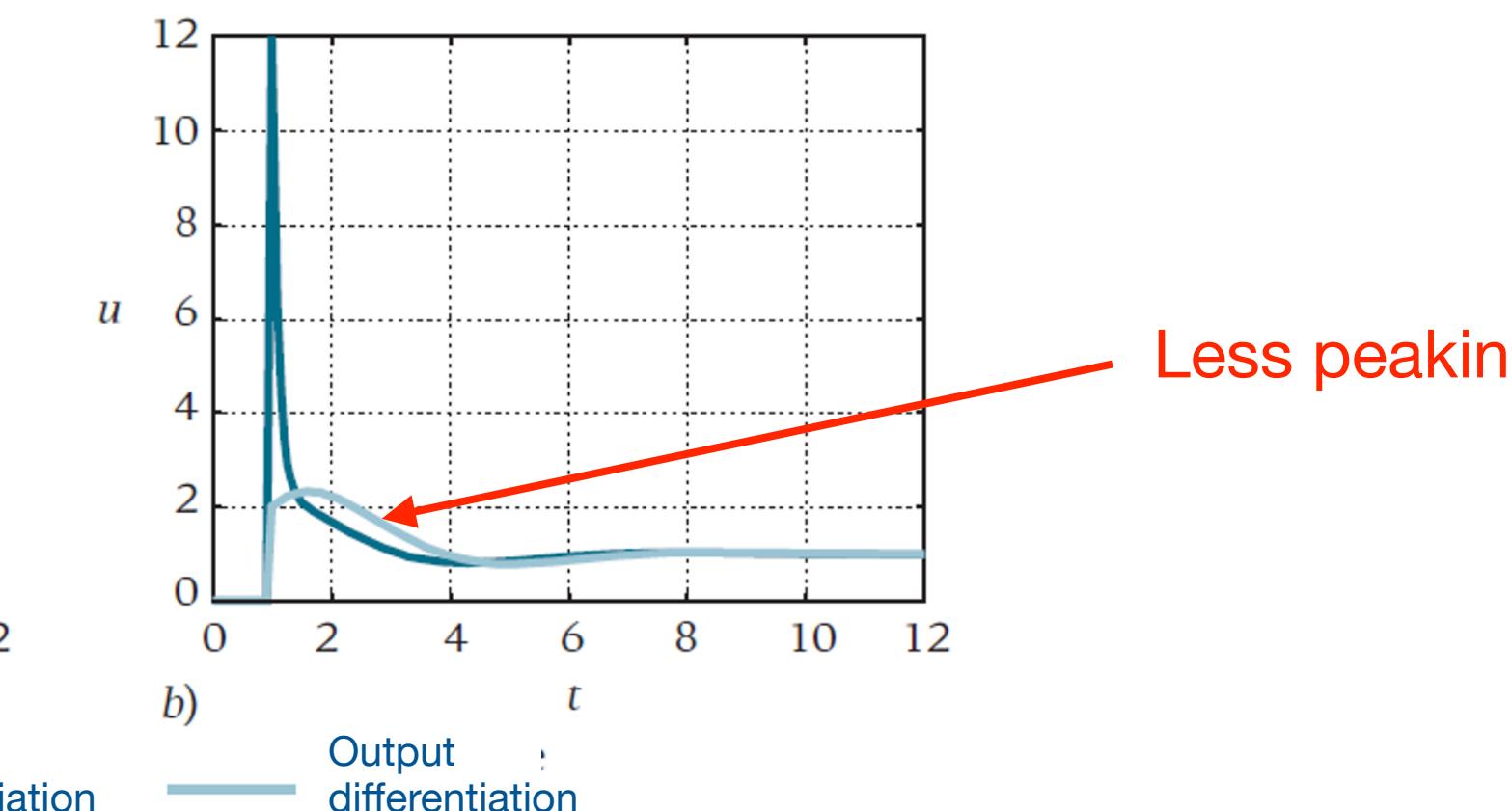
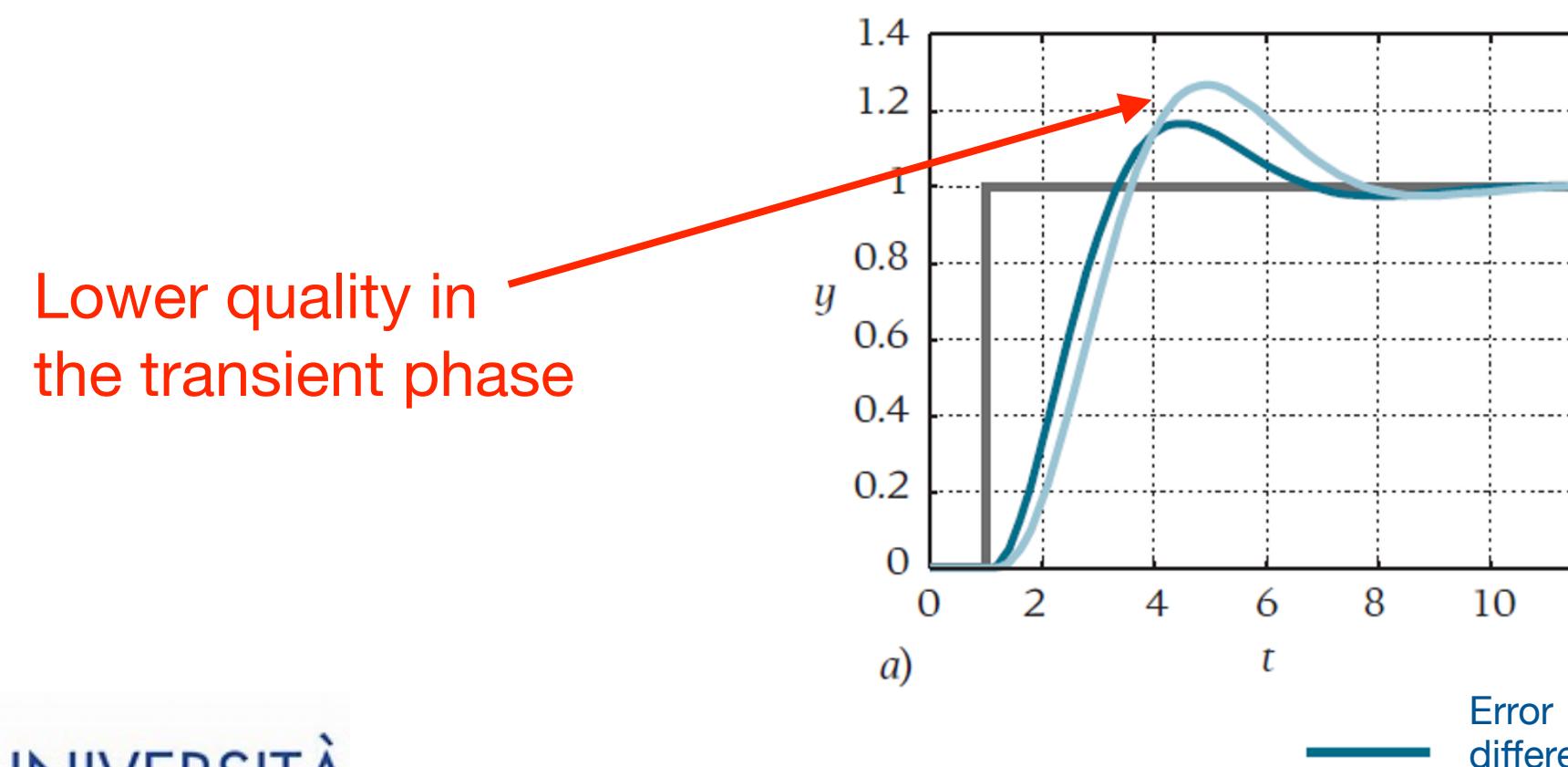
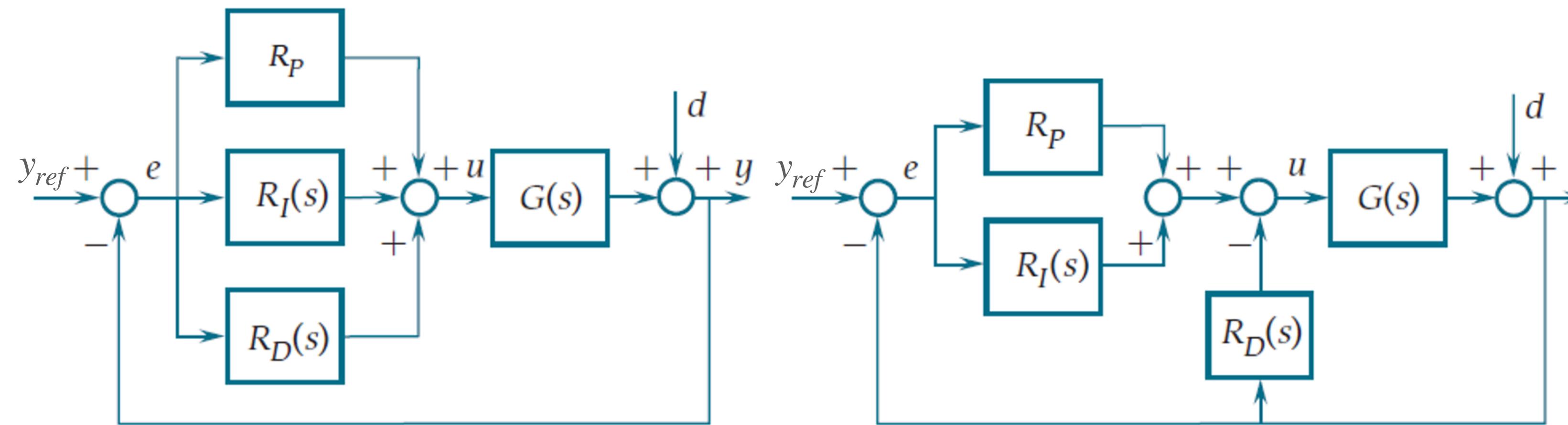
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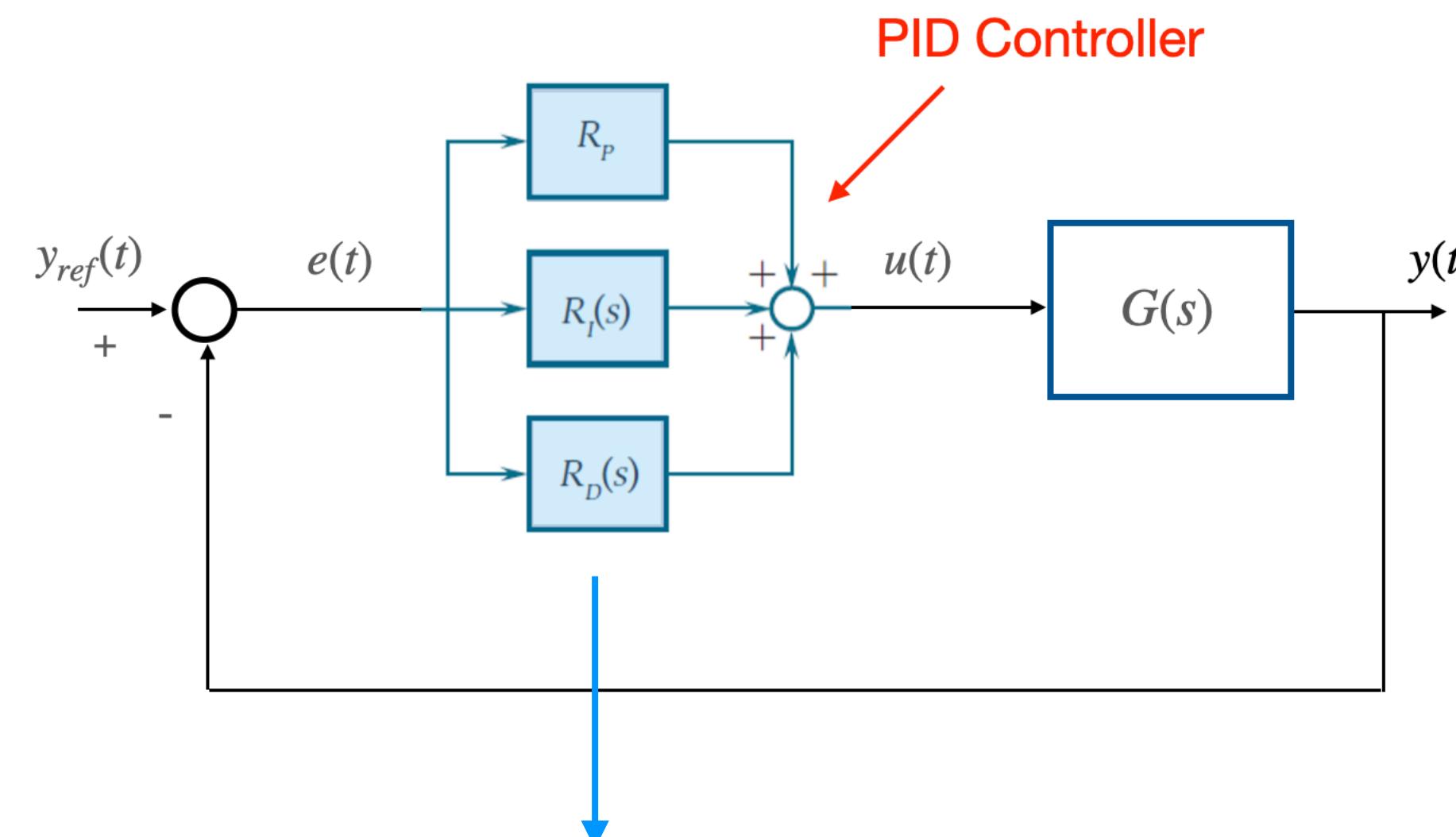
Practical Implementation of PID Controllers



Practical Implementation of PID Controllers



Practical Implementation of PID Controllers: Tuning Rules



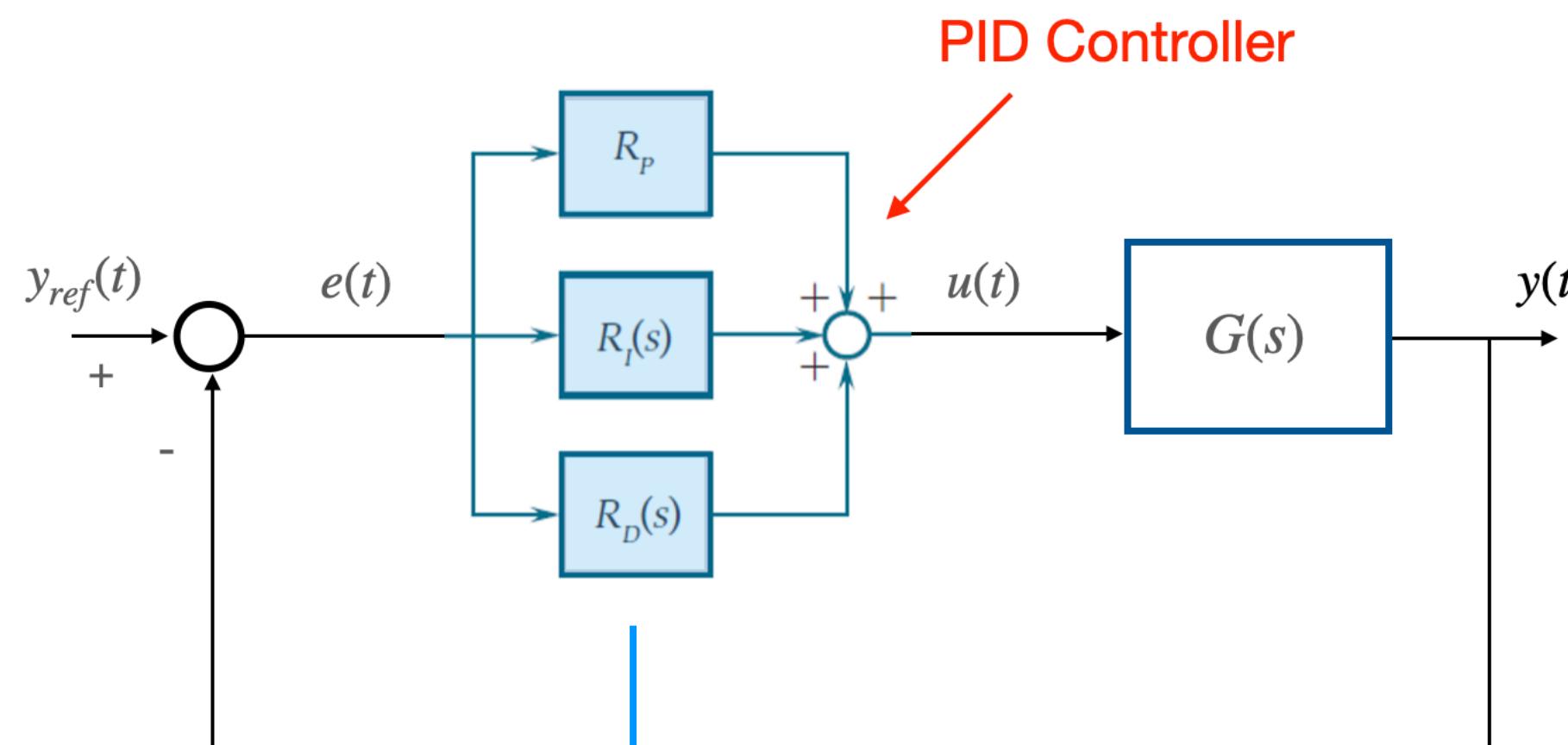
Closed-loop Ziegler-Nichols Method

Testing phase:

$$R_P(s) = K_P, \quad R_I(s) = 0, \quad R_D(s) = 0$$



Practical Implementation of PID Controllers: Tuning Rules

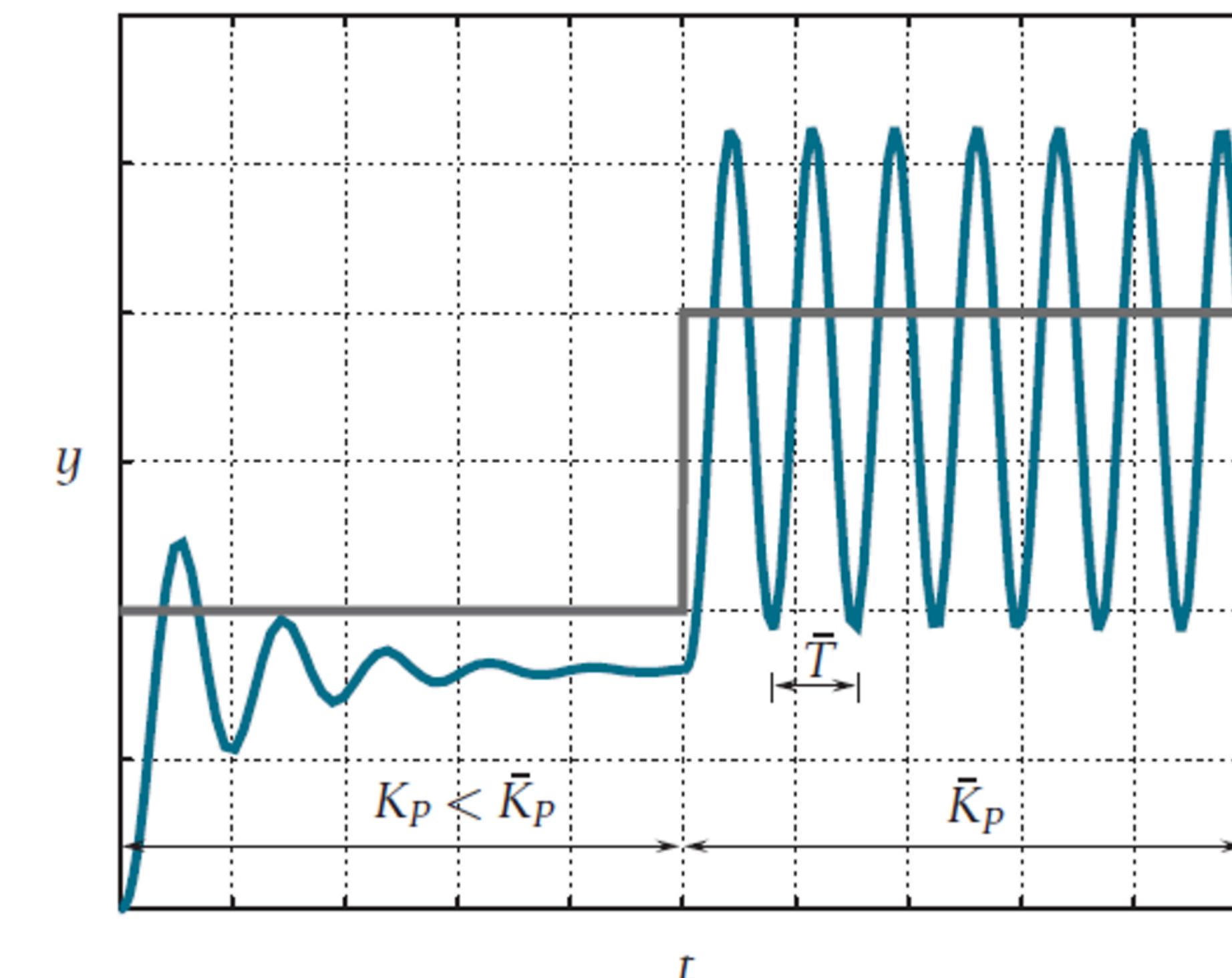


PID Controller

Testing phase:

$$R_P(s) = K_P, \quad R_I(s) = 0, \quad R_D(s) = 0$$

Closed-loop Ziegler-Nichols Method

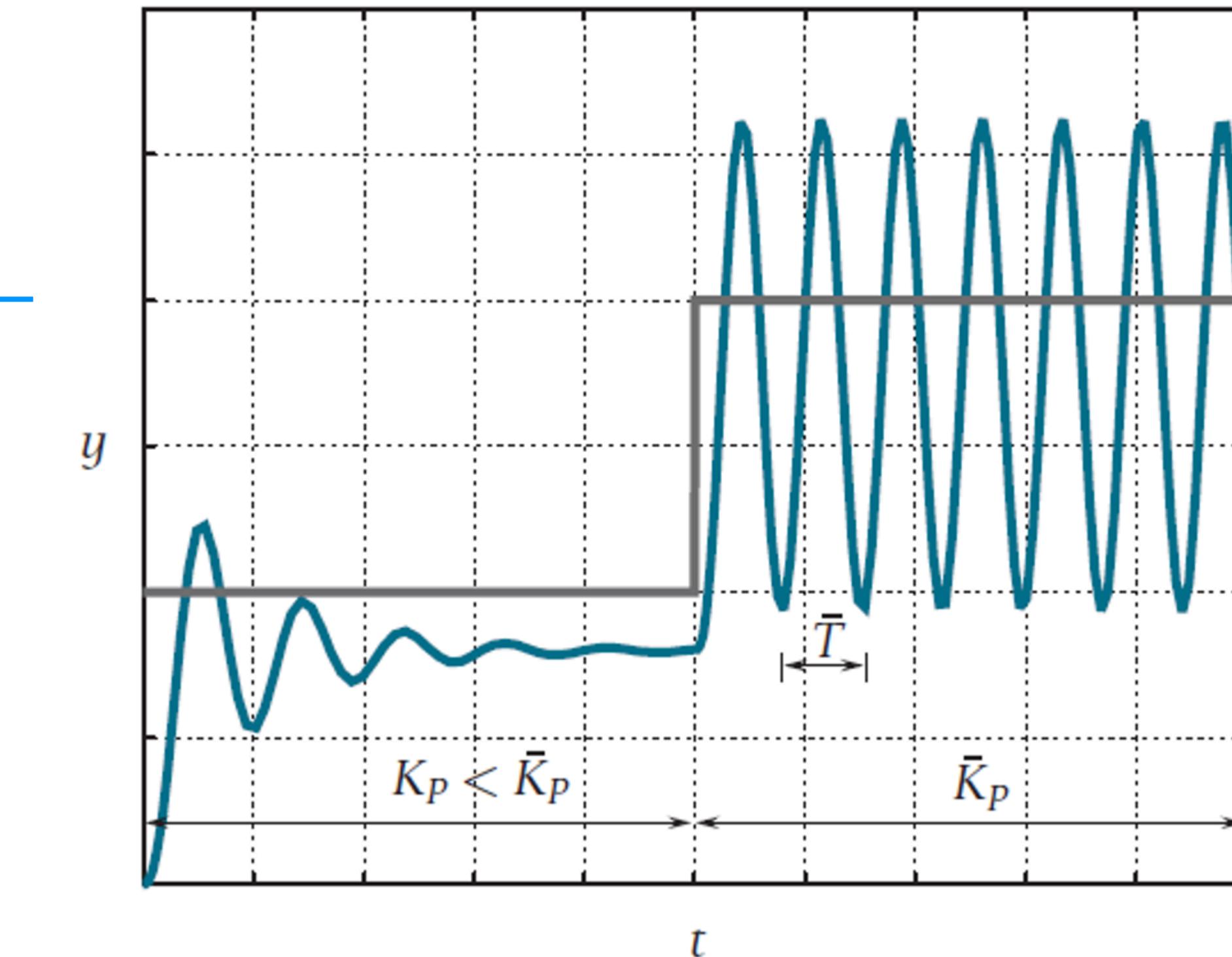


Practical Implementation of PID Controllers: Tuning Rules

Closed-loop Ziegler-Nichols Method

	K_P	T_I	T_D
P	$0.5\bar{K}_P$		
PI	$0.45\bar{K}_P$	$0.8\bar{T}$	
PID	$0.6\bar{K}_P$	$0.5\bar{T}$	$0.125\bar{T}$

$$R_{PID_{id}}(s) = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$



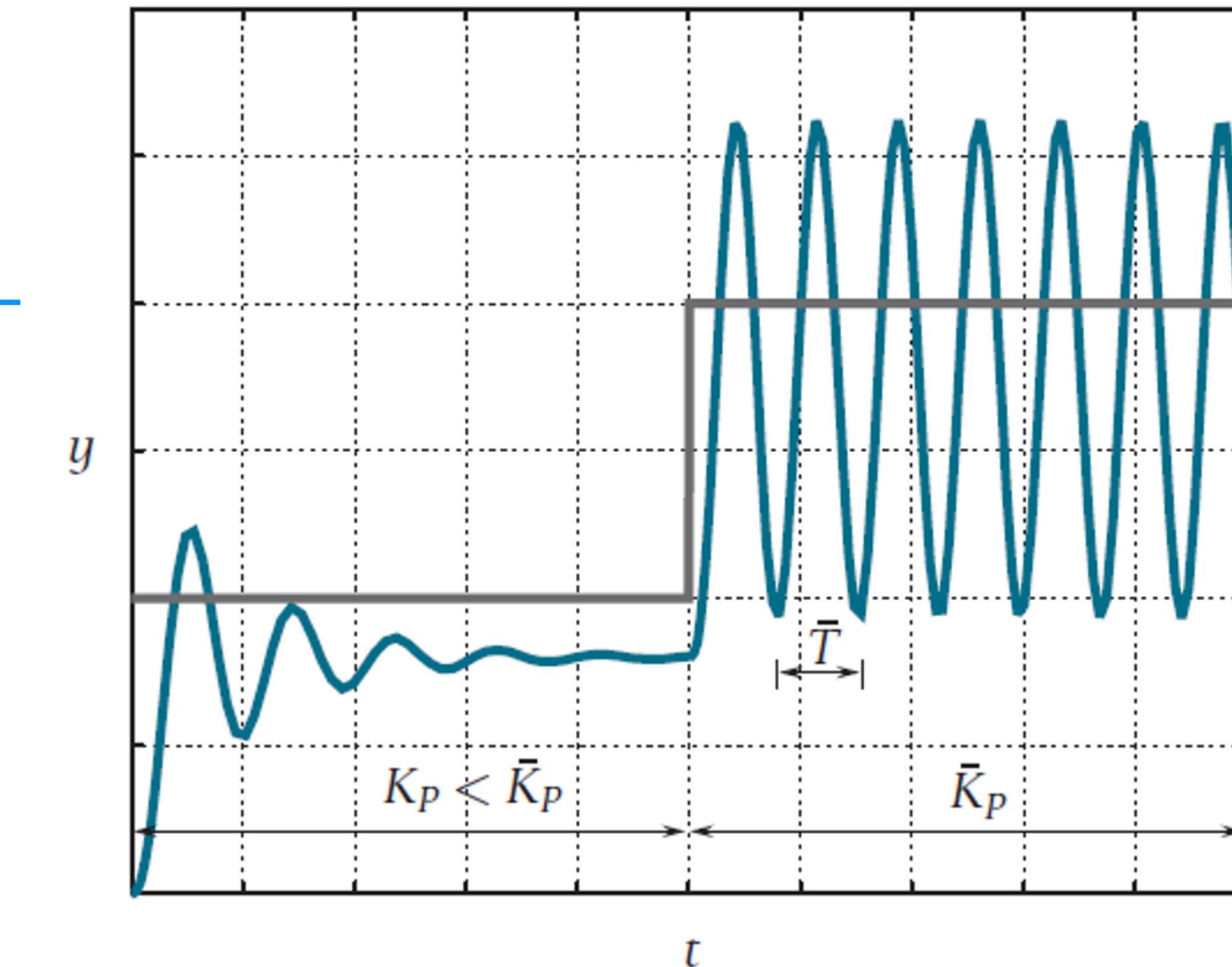
Practical Implementation of PID Controllers: Tuning Rules

	K_P	T_I	T_D
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Note that $T_I = 4T_D \rightarrow$ the PID zeros coincide in $s = -\frac{1}{2T_D}$

Closed-loop Ziegler-Nichols Method



Practical Implementation of PID Controllers: Tuning Rules

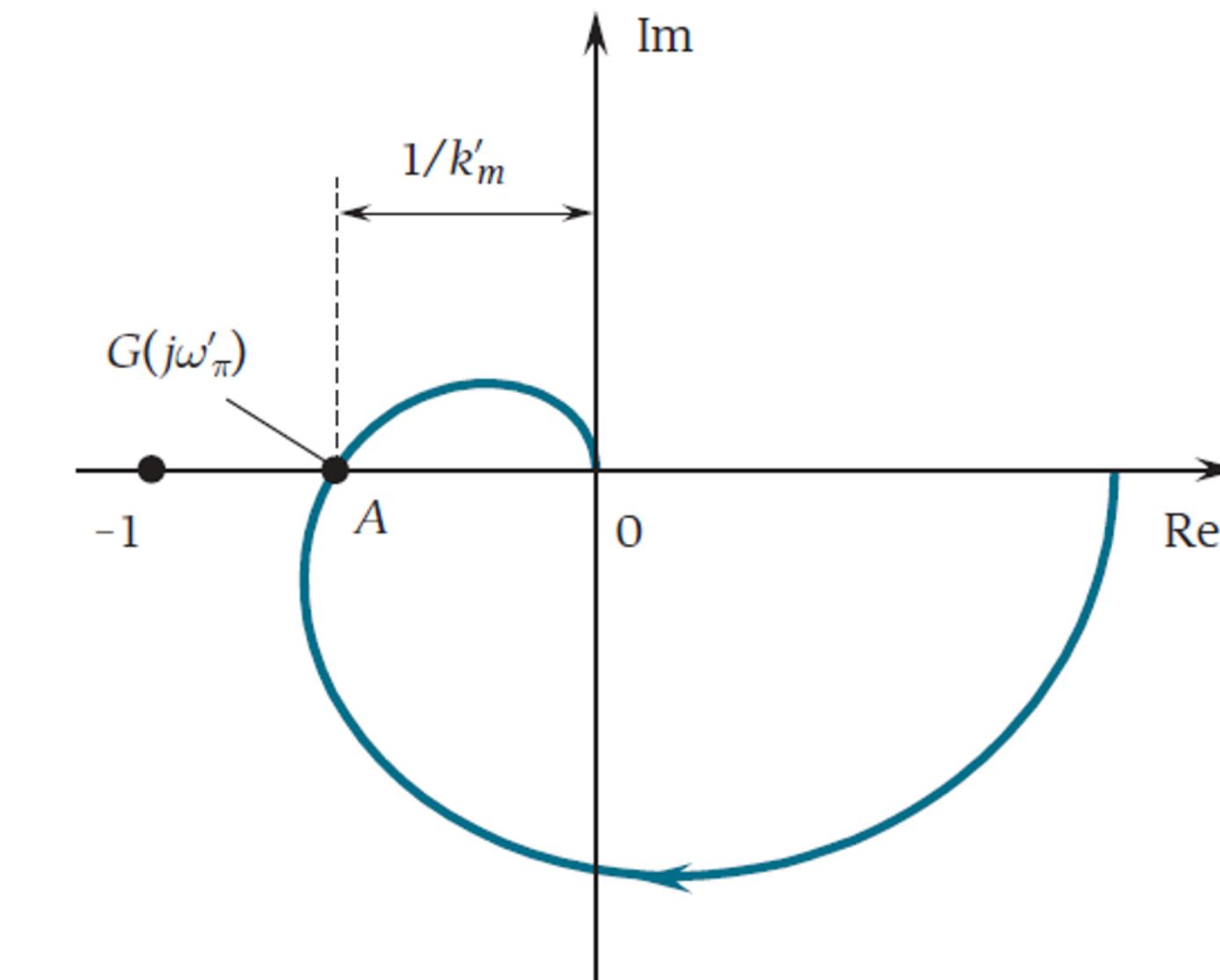
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Closed-loop Ziegler-Nichols Method: Interpretation



$\bar{K}_p = k'_m \rightarrow$ Gain Margin of $G(s)$

$\bar{T} = \frac{\pi}{\omega'_\pi} \rightarrow$ where ω'_π is the pulse corresponding to point A



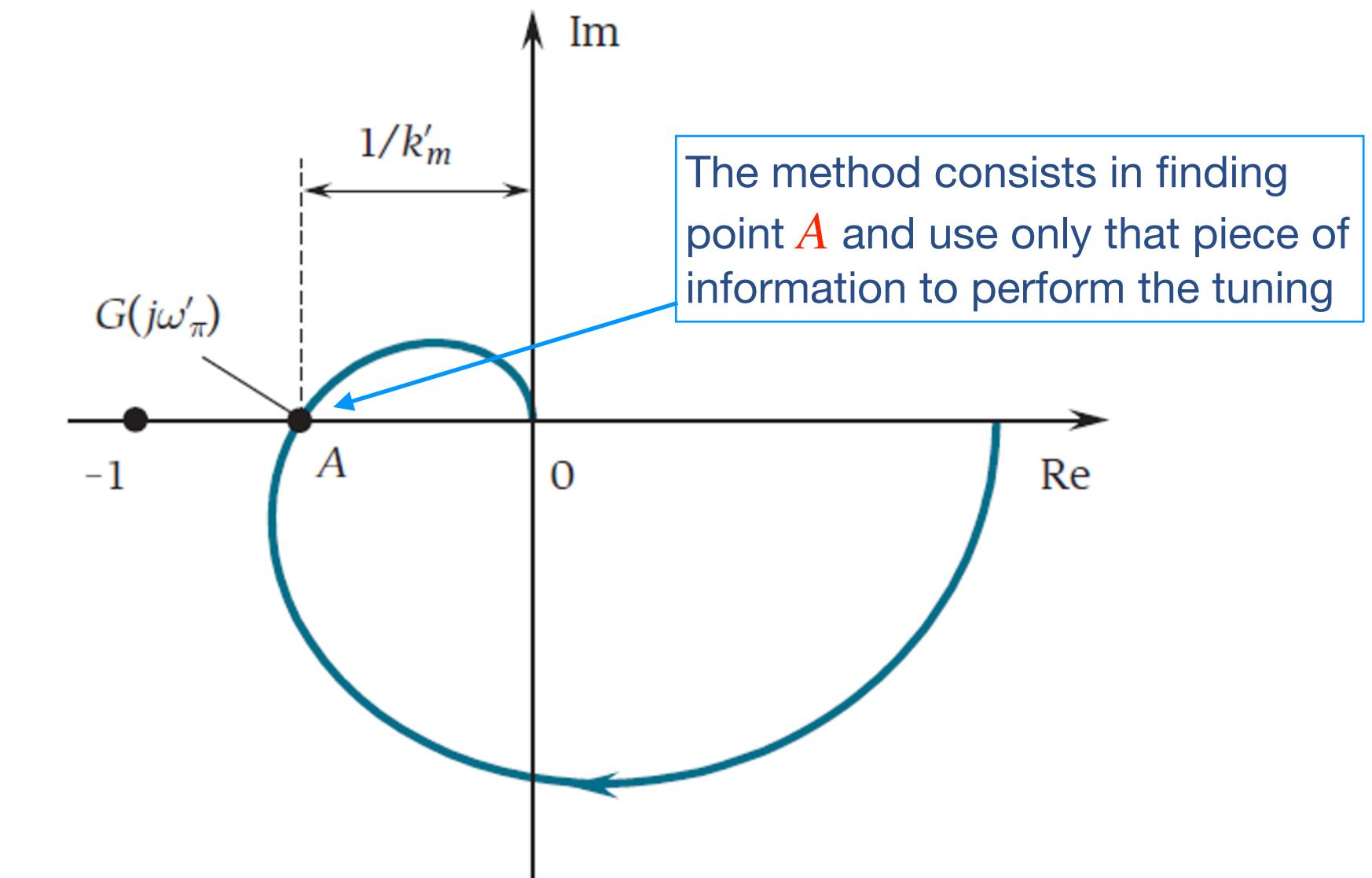
Practical Implementation of PID Controllers: Tuning Rules

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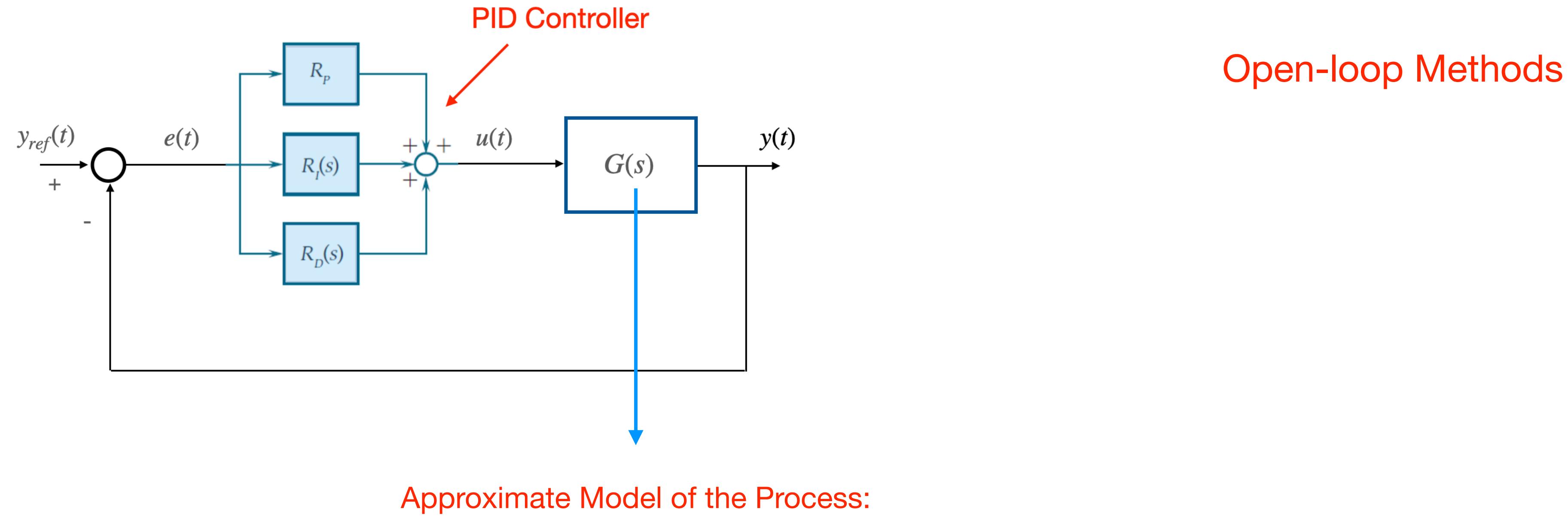


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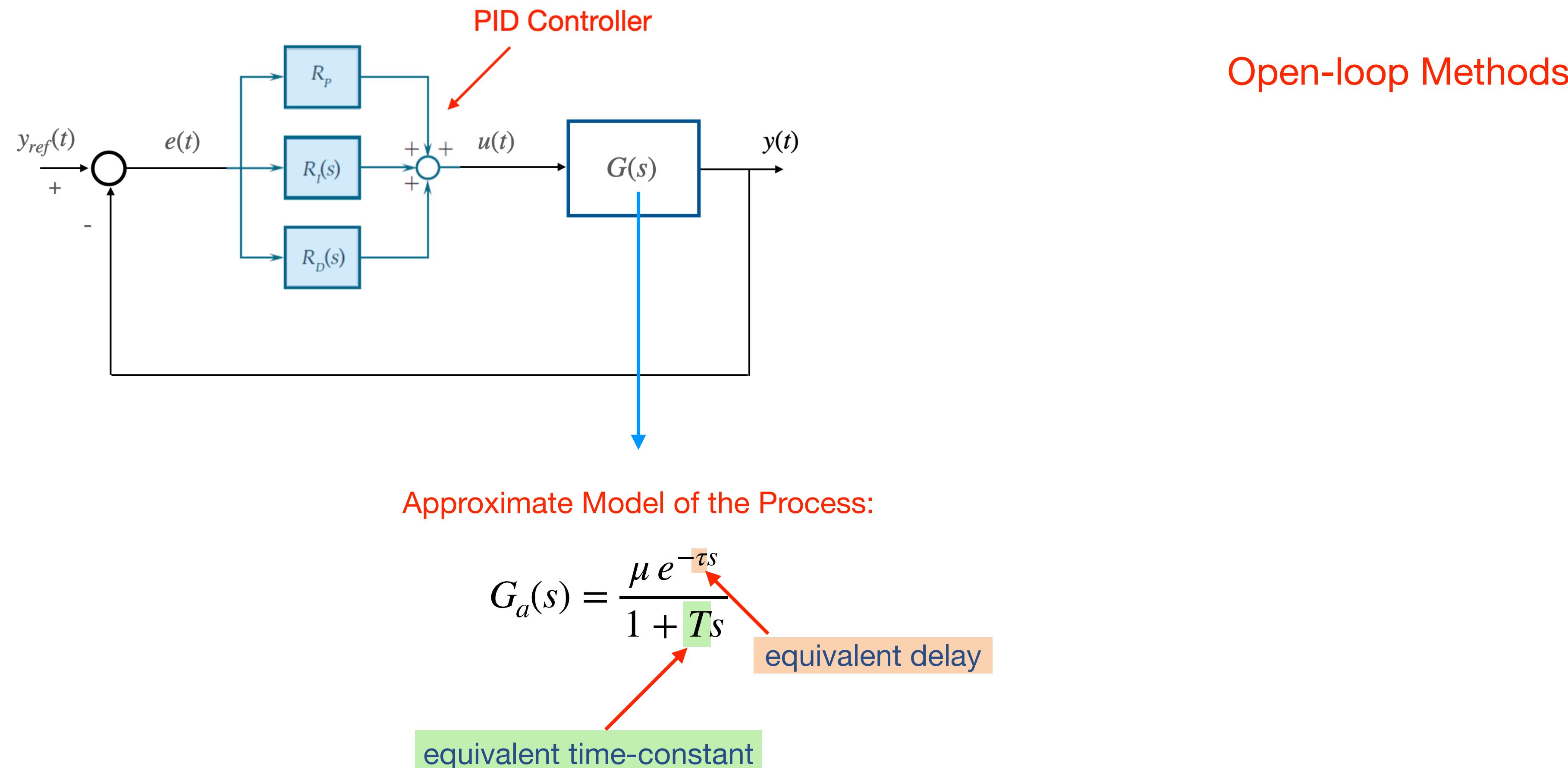
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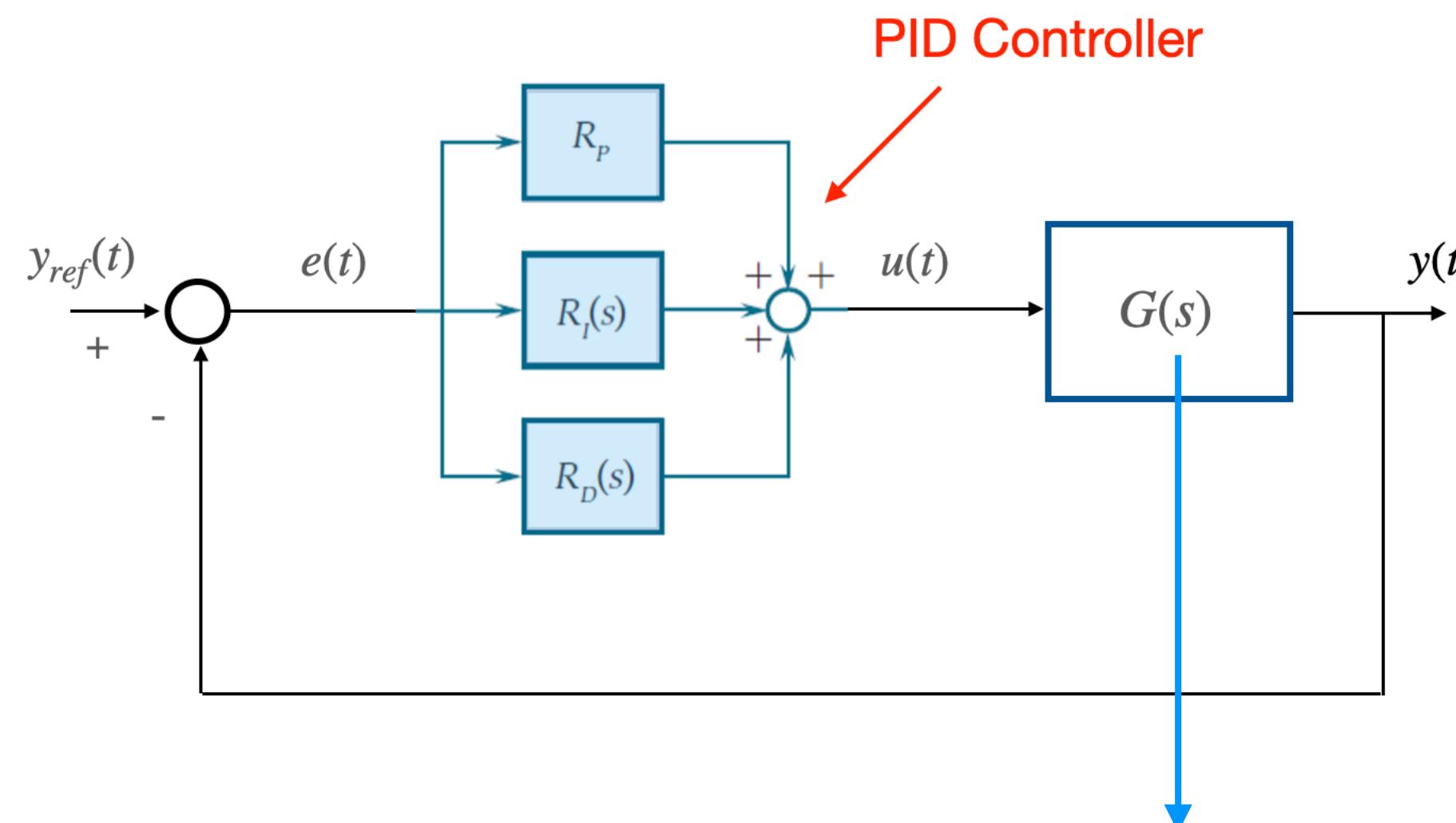
$$G_a(s) = \frac{\mu e^{-\tau s}}{1 + Ts}$$



Practical Implementation of PID Controllers: Tuning Rules



Practical Implementation of PID Controllers: Tuning Rules



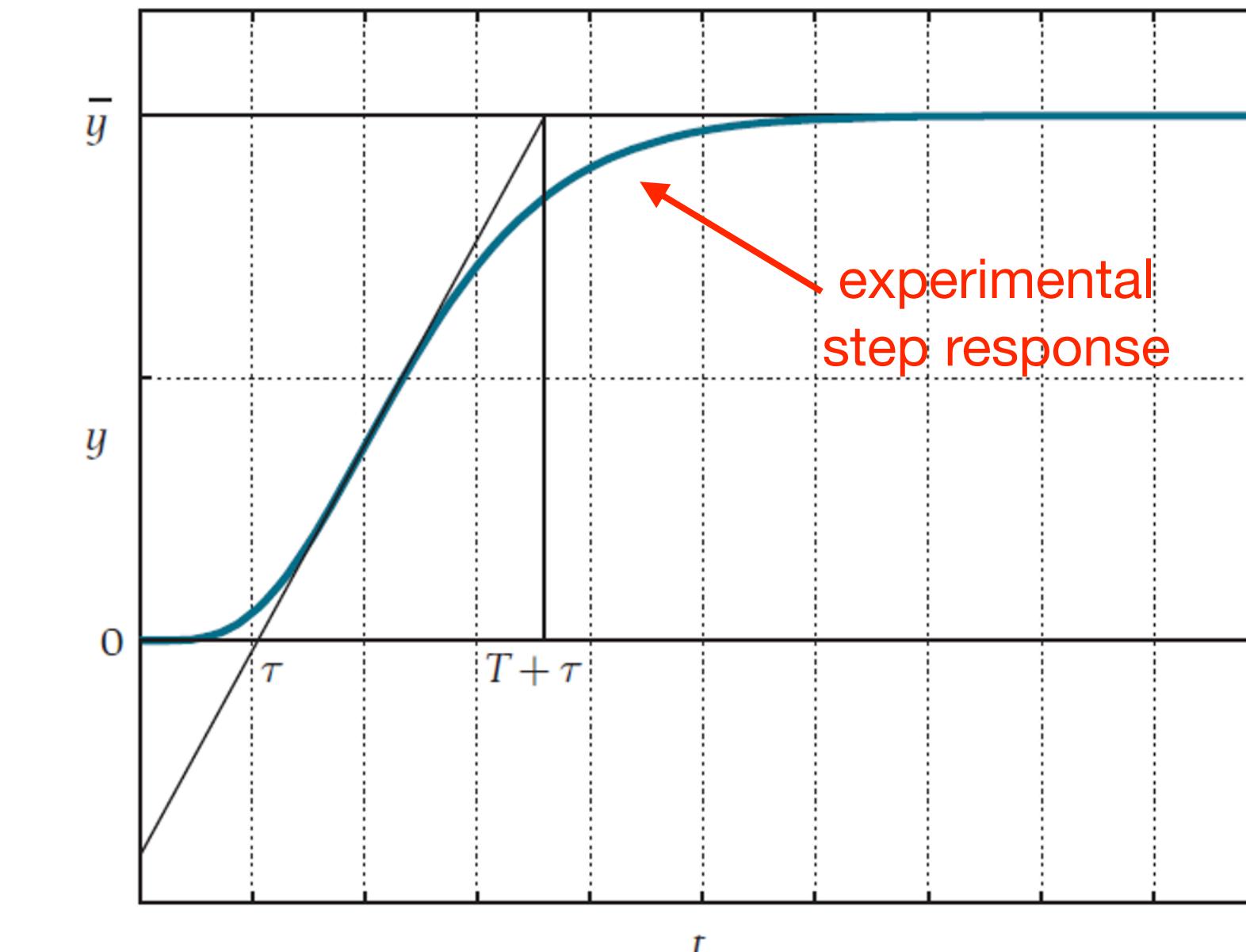
Approximate Model of the Process:

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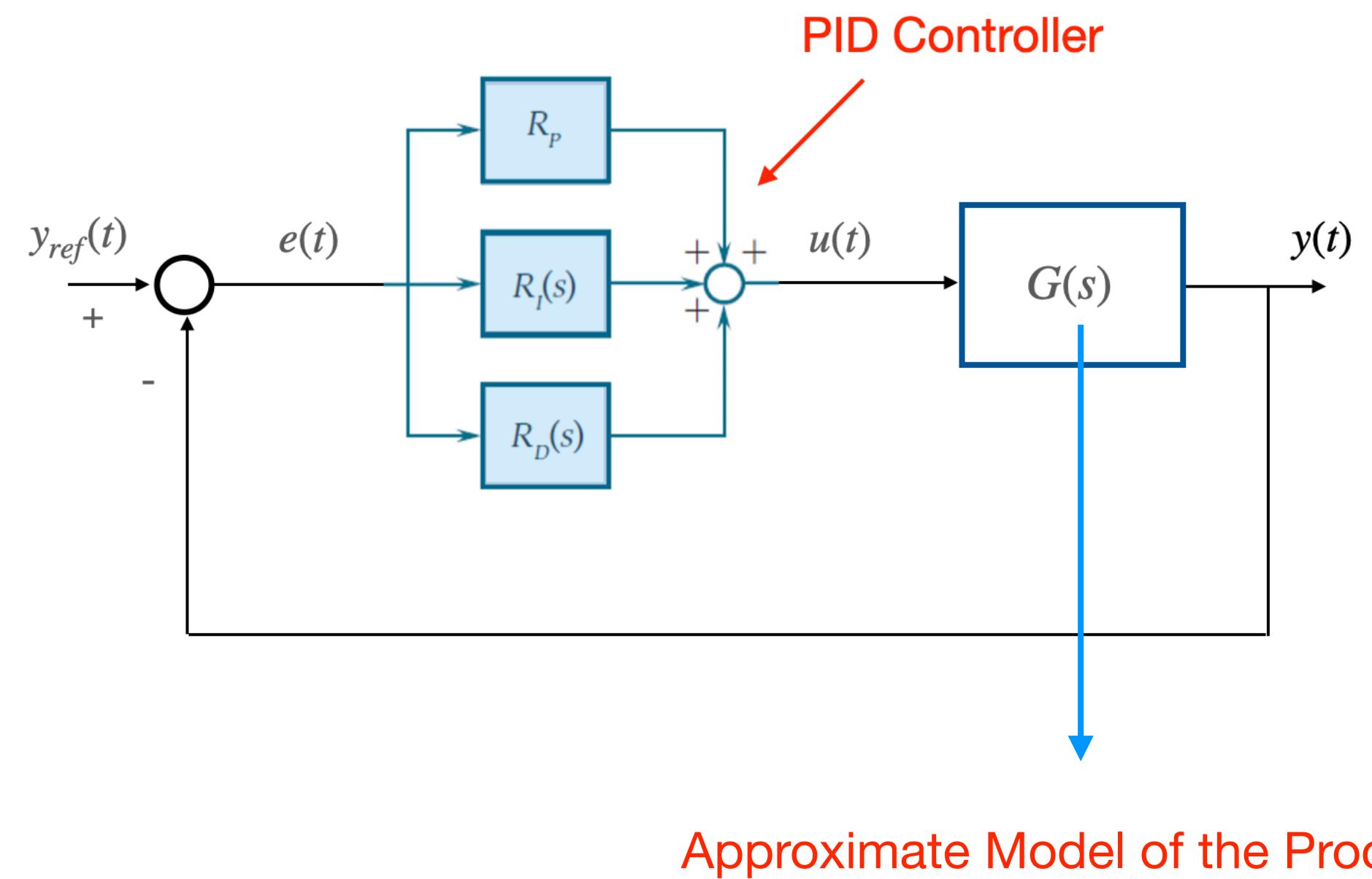
equivalent time-constant

Open-loop Methods

Parameters τ , T determination via the Tangent Method



Practical Implementation of PID Controllers: Tuning Rules



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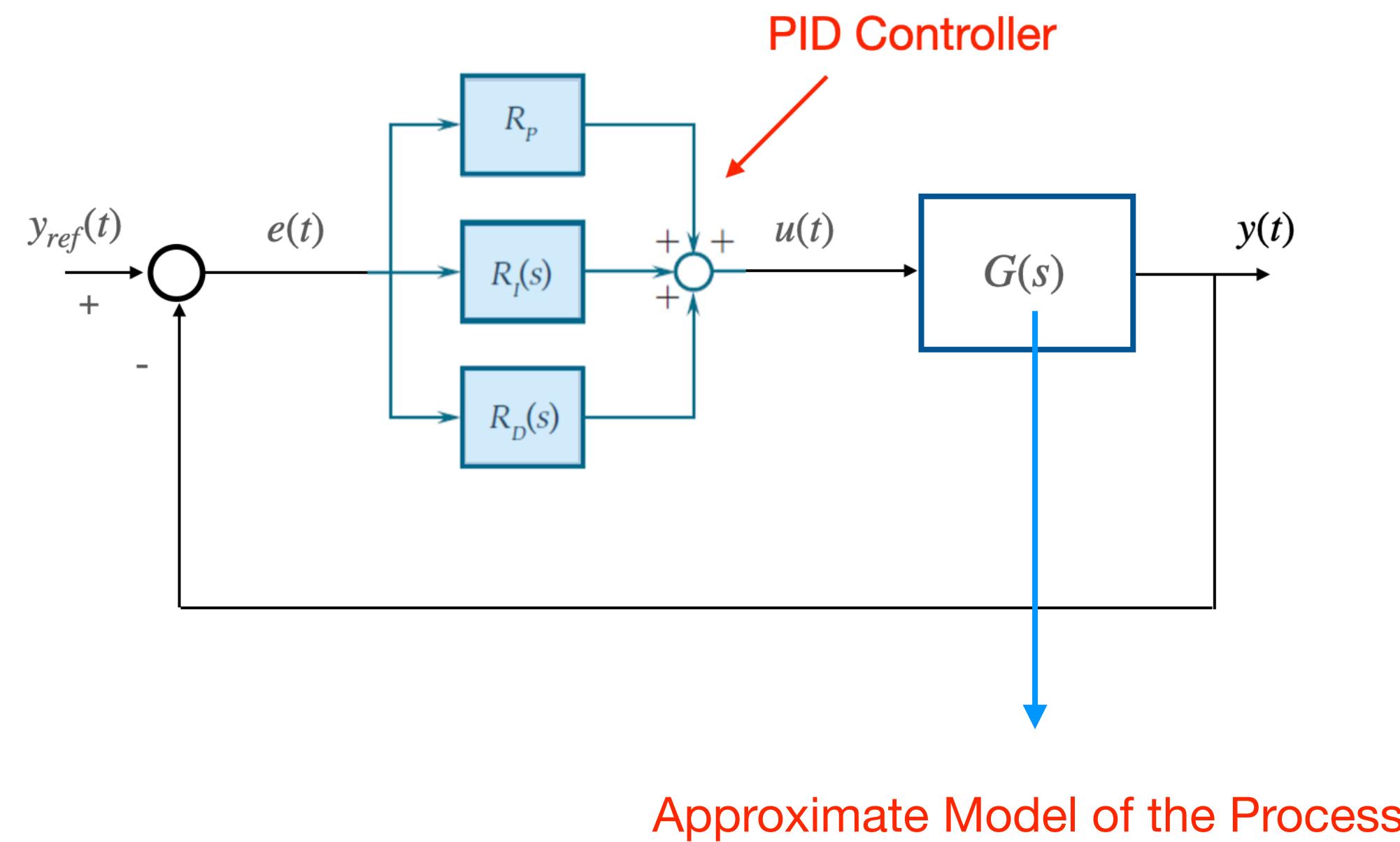
Open-loop Ziegler-Nichols Method

	K_P	T_I	T_D
P	$\frac{T}{\mu\tau}$		
PI	$\frac{0.9T}{\mu\tau}$	3τ	
PID	$\frac{1.2T}{\mu\tau}$	2τ	0.5τ

$$R_{PID_{id}}(s) = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$



Practical Implementation of PID Controllers: Tuning Rules



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Open-loop Ziegler-Nichols Method

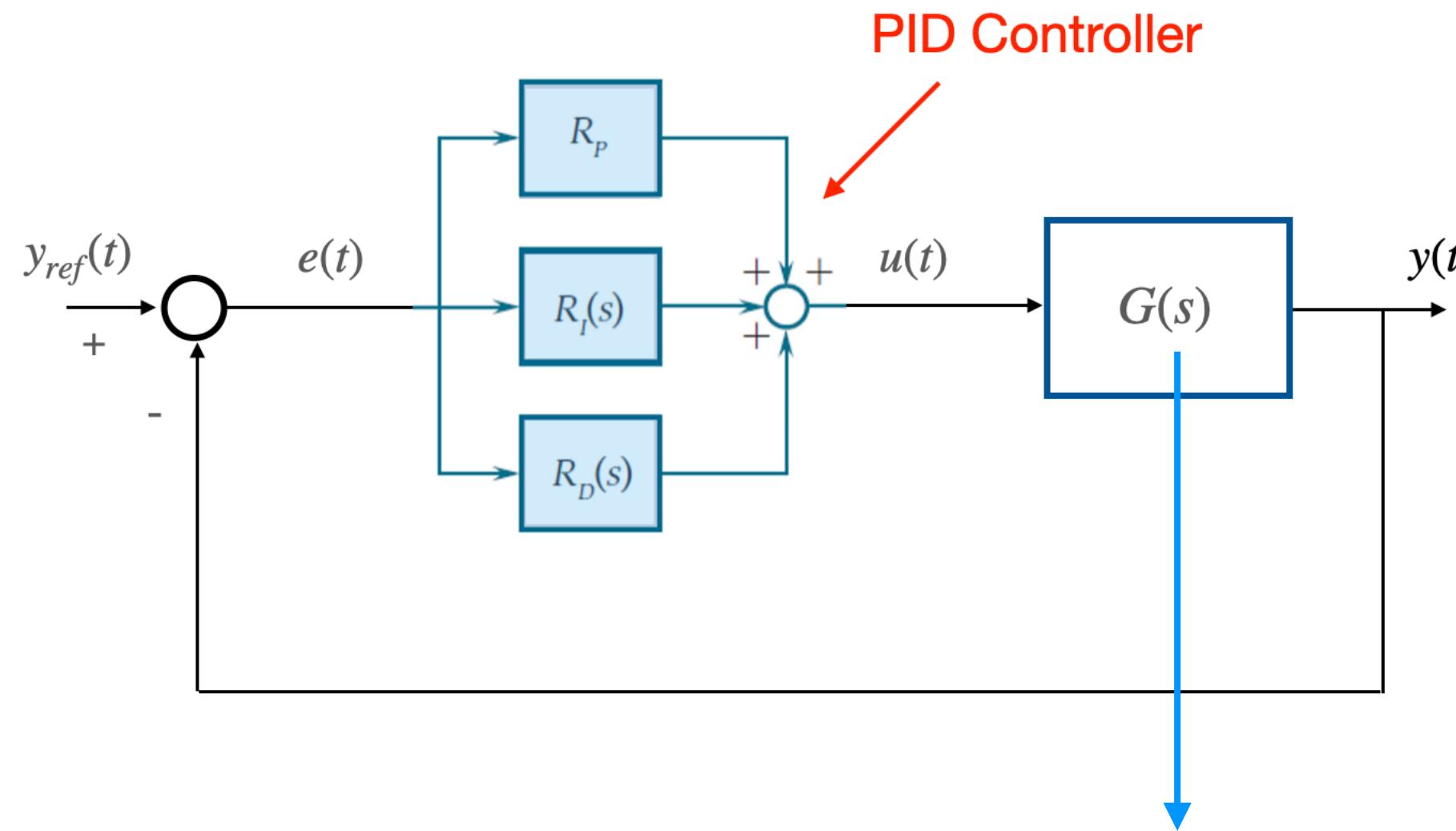
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Practical Implementation of PID Controllers: Tuning Rules



Open-loop Cohen-Coon Method

	K_P	T_I	T_D
P	$\frac{3T + \tau}{3\mu\tau}$		
PI	$\frac{10.8T + \tau}{12\mu\tau}$	$\tau \frac{30T + 3\tau}{9T + 20\tau}$	
PID	$\frac{16T + 3\tau}{12\mu\tau}$	$\tau \frac{32T + 6\tau}{12\tau}$	$\frac{4T\tau}{11T + 2\tau}$

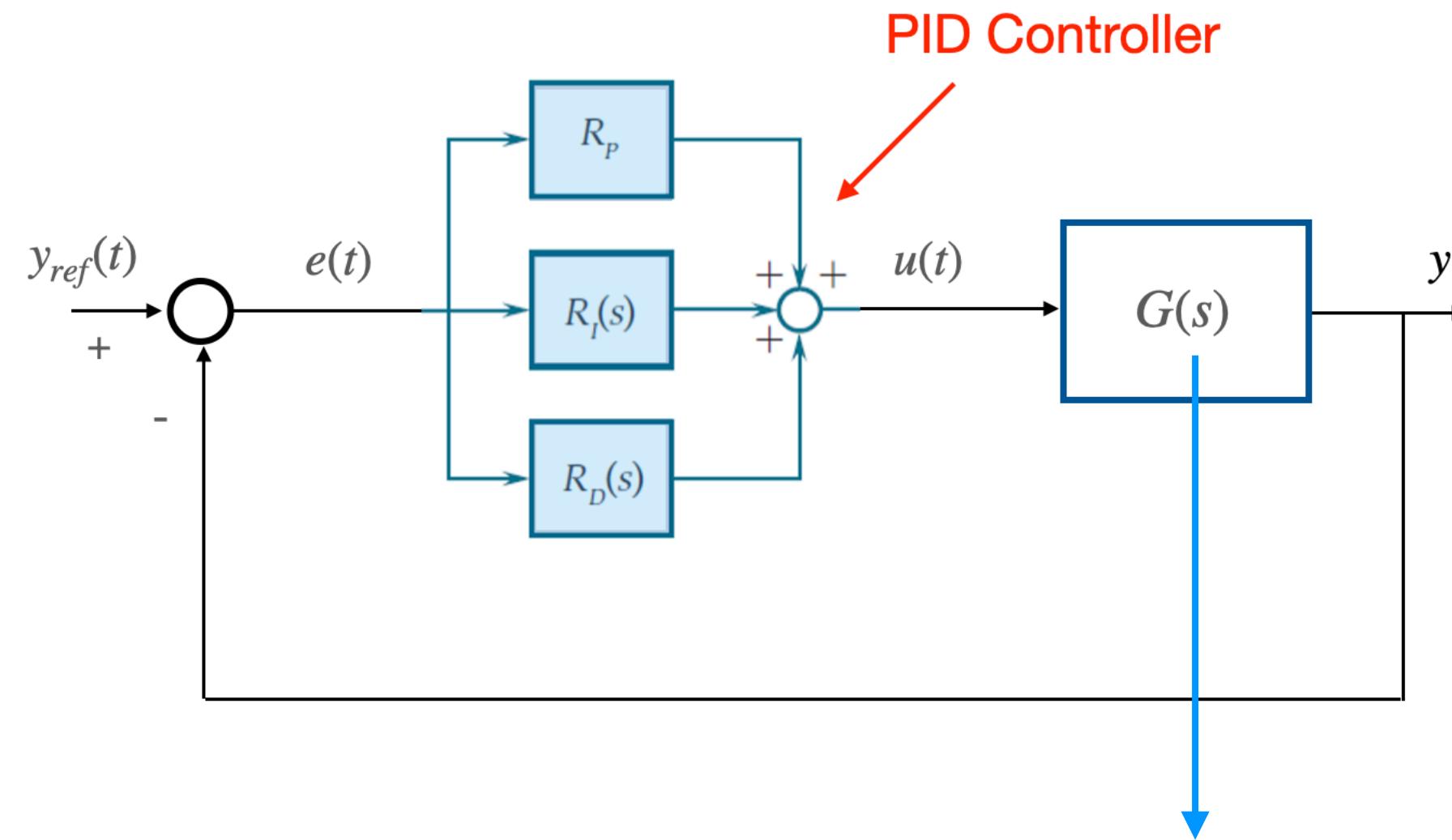
Approximate Model of the Process:

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$$R_{PID_{id}}(s) = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$



Practical Implementation of PID Controllers: Tuning Rules



Open-loop Internal Model Control (IMC) Method

	K_P	T_I	T_D
PI	$\frac{T}{\mu(\tau + T_f)}$	T	
PID	$\frac{T + 0.5\tau}{\mu(T_f + 0.5\tau)}$	$T + 0.5\tau$	$\frac{0.5\tau T}{T + 0.5\tau}$

Approximate Model of the Process:

$$G_a(s) = \frac{\mu e^{-\tau s}}{1 + Ts}$$

$$R_{PID_{id}}(s) = K_P \left(1 + \frac{1}{T_I s} + T_D s \right)$$

additional parameter: if T_f increases, then $\omega_{BW_{CL}}$ decreases and the phase and gain margins increase



Practical Implementation of PID Controllers: Tuning Rules

Comparison:

	φ_m	k_m	ω_c
Cohen - Coon	31°	7.9	0.74
IMC ($T_f = 0.4$)	45°	10.8	0.6
IMC ($T_f = 0.8$)	53°	12.8	0.5
IMC ($T_f = 1.2$)	59°	14.4	0.42

For system: $G(s) = \frac{1}{(1+s)^3}$ approximated as: $G_a(s) = \frac{e^{-0.8s}}{1+3.7s}$

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Note that: The IMC method produces more moderate control systems w.r.t. those obtained via the Cohen-Coon Method



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For system: $G(s) = \frac{1}{(1+s)^3}$ approximated as: $G_a(s) = \frac{e^{-0.8s}}{1+3.7s}$

Exercise:

Determine the Control Sensitivity Functions for a PI tuned using Cohen-Coon or the IMC in the table for the considered $G(s)$

Open-loop Internal Model Control (IMC) Method

	K_P	T_I	T_D
PI	$\frac{T}{\mu(\tau + T_f)}$	T	
PID	$\frac{T + 0.5\tau}{\mu(T_f + 0.5\tau)}$	$T + 0.5\tau$	$\frac{0.5\tau T}{T + 0.5\tau}$

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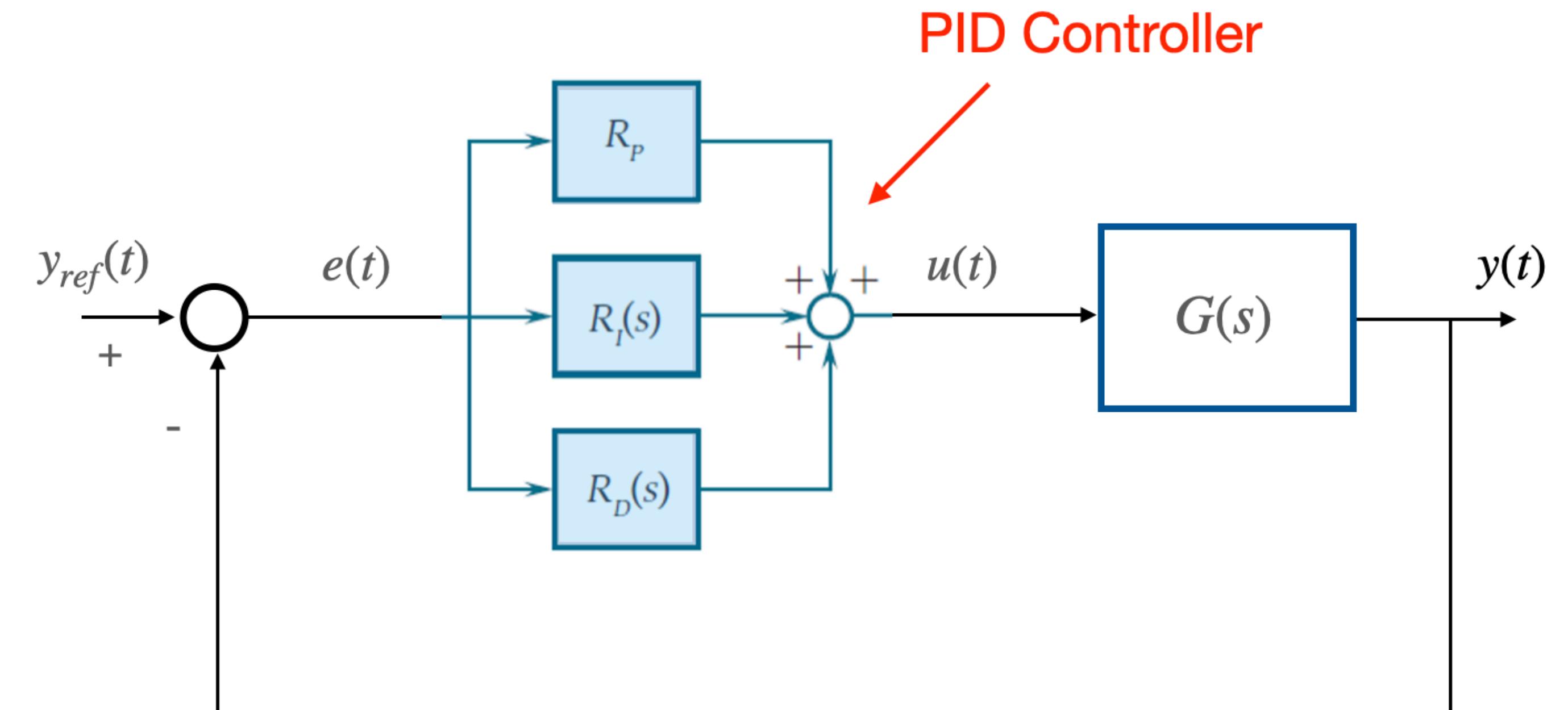
Practical Implementation of PID Controllers: Example

Process model:

$$G(s) = \frac{100}{(s + 10)(s + 30)(s + 5)}$$

```
/MATLAB Drive/PID_example1.m
1 %% System definition
2 s = tf('s');
3 G = 100 / ((s + 10)*(s + 30)*(s+5));
4
```

Control scheme:



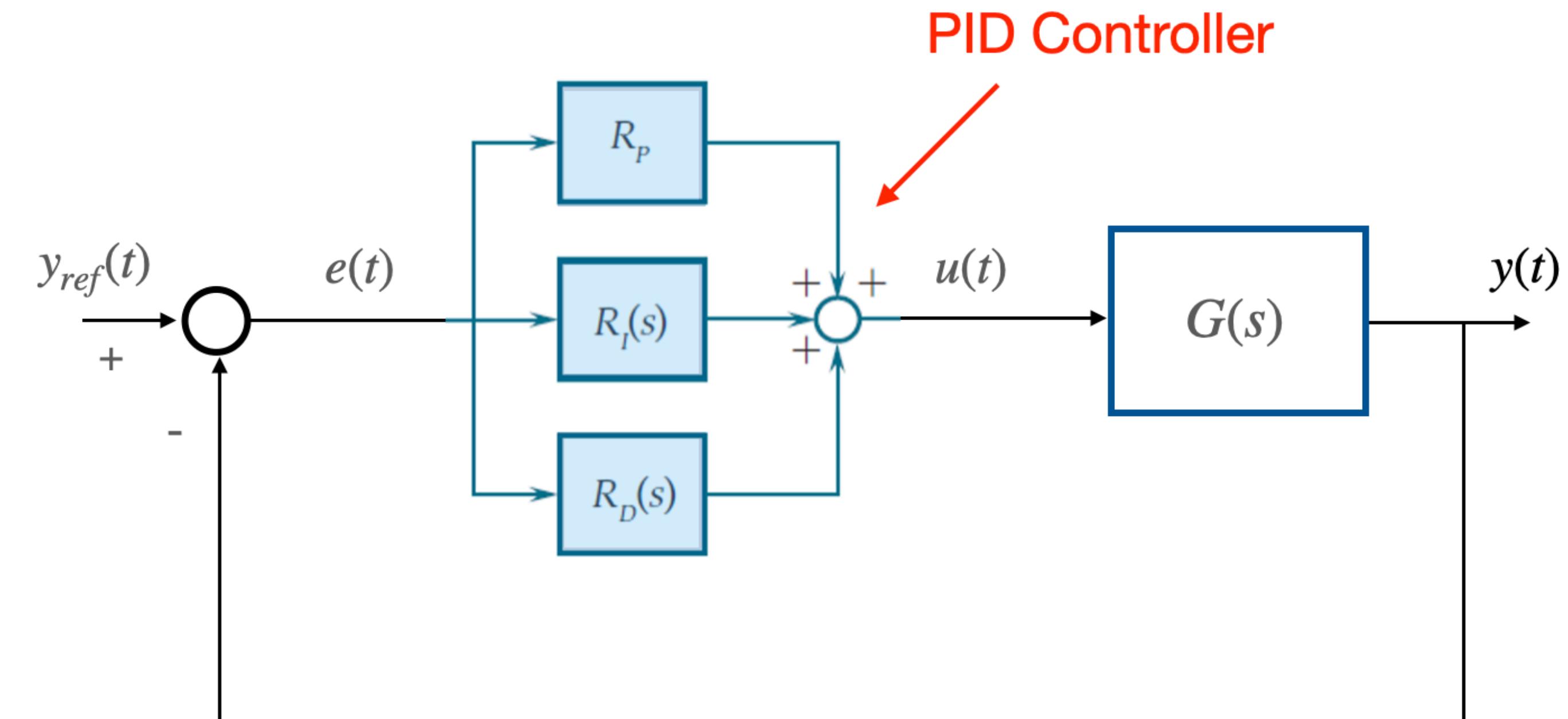
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Control scheme:



Objective: Compare the performance of the closed loop system with PID designed via CL Ziegler-Nichols rules and PID designed via OL Ziegler-Nichols rules



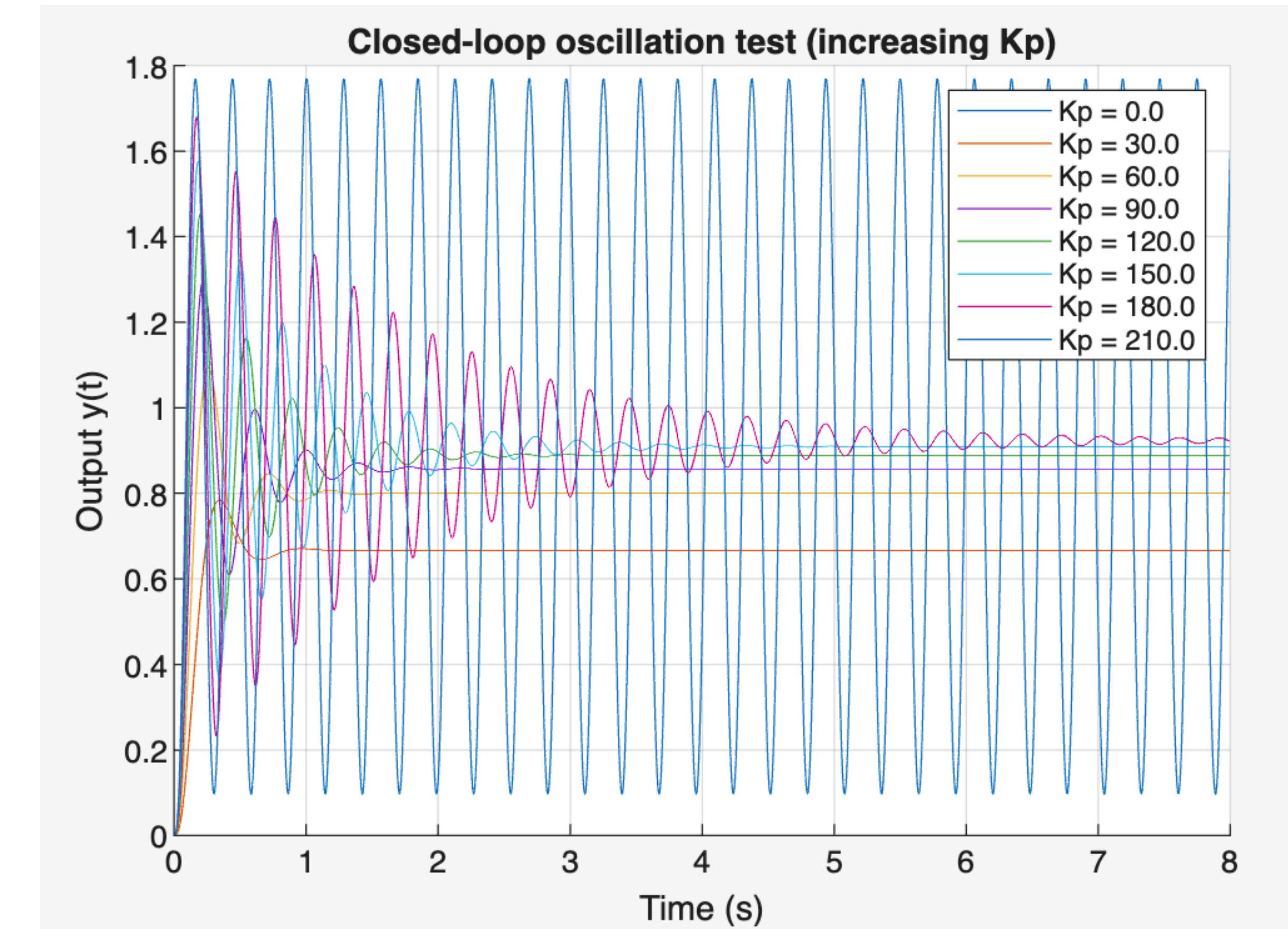
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Simulation for increasing K_P :



Practical Implementation of PID Controllers: Example

Process model:

$$G(s) = \frac{100}{(s + 10)(s + 30)(s + 5)}$$

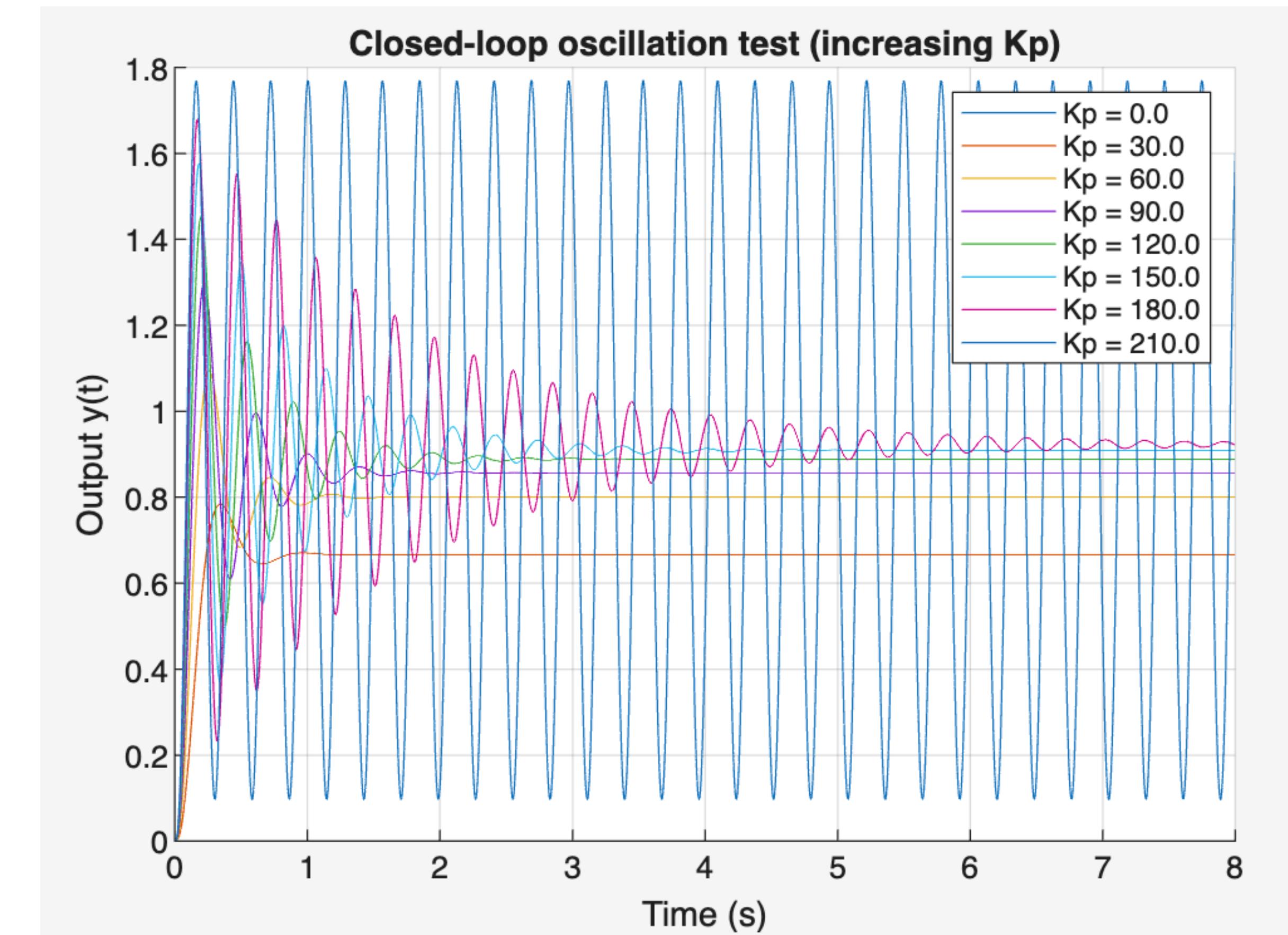
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```

PID calibration:

```
Estimated critical gain Kcr = 210.00
Estimated oscillation period Tcr = 0.281 s

Closed-loop ZN PID (with derivative filter, tau_f=1.000000e-02):
Kp = 126.000, Ti = 0.141, Td = 0.035
```

Simulation for increasing K_P :



Practical Implementation of PID Controllers: Example

Process model:

$$G(s) = \frac{100}{(s + 10)(s + 30)(s + 5)}$$

Approximate Model of the Process:

$$G_a(s) = \frac{\mu e^{-\tau s}}{1 + Ts}$$

$$\mu = 0.067 \quad \tau = 0.053 \quad T = 0.175$$



Practical Implementation of PID Controllers: Example

Process model:

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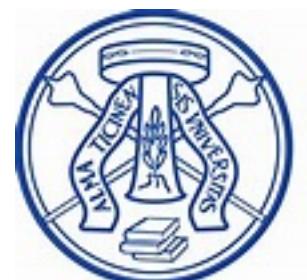
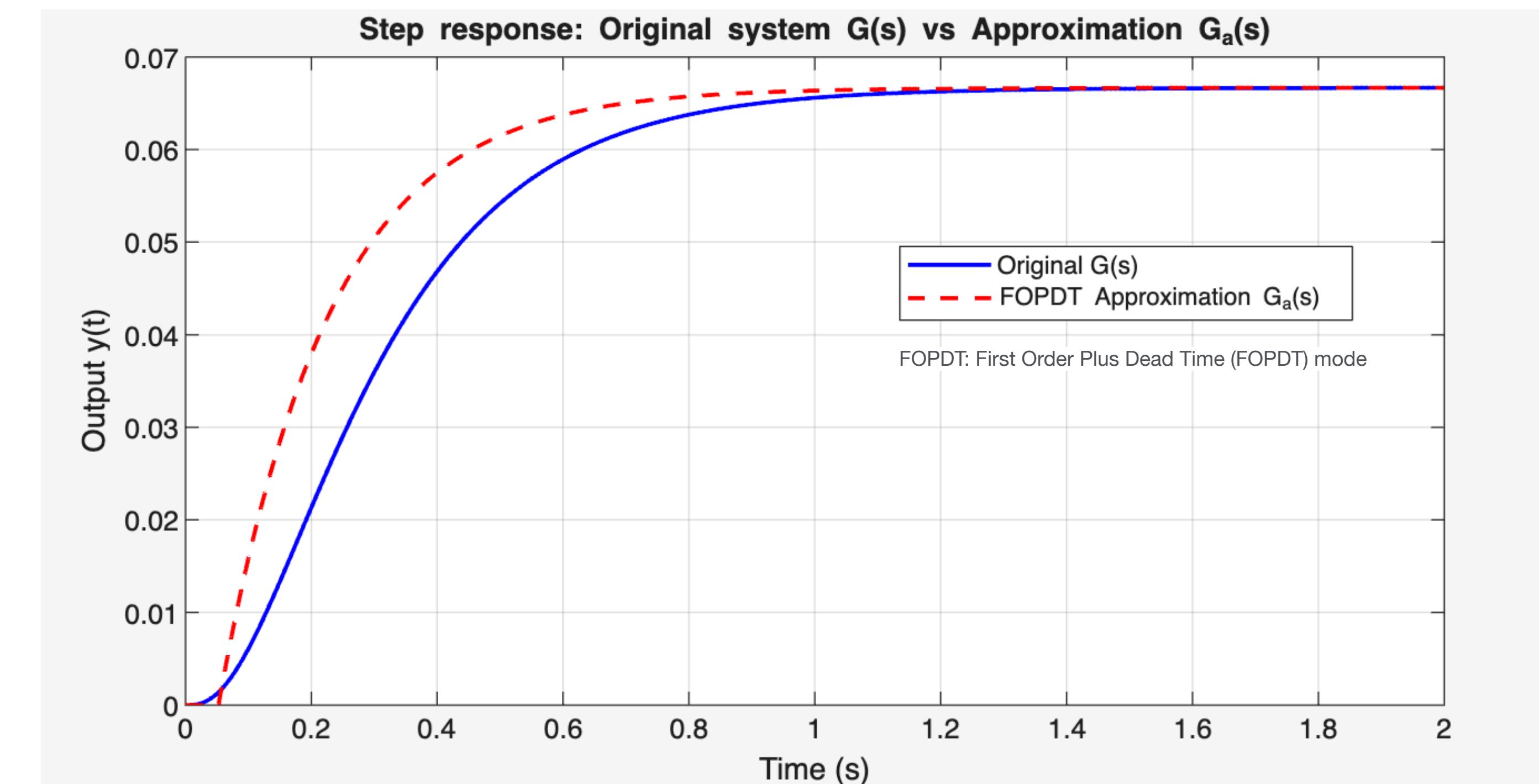
$$G_a(s) = \frac{\mu e^{-\tau s}}{1 + Ts}$$

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```

76 %% === COMPARE STEP RESPONSE: REAL G(s) vs APPROXIMATED G_a(s) ===
77 t_sim = 0:0.001:2;
78 [yG, tG] = step(G, t_sim);
79 [yGa, tGa] = step(G_a, t_sim);
80
81 figure;
82 plot(tG, yG, 'b', 'LineWidth', 1.5); hold on;
83 plot(tGa, yGa, 'r--', 'LineWidth', 1.5);
84 xlabel('Time (s)');
85 ylabel('Output y(t)');
86 title('Step response: Original system G(s) vs Approximation G_a(s)');
87 legend('Original G(s)', 'FOPDT Approximation G_a(s)');
88 grid on;
89

```



Practical Implementation of PID Controllers: Example

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Open-loop ZN PID:
 $K_p = 60.000, T_i = 0.105, T_d = 0.026$

Open-loop Ziegler-Nichols Method

	K_P	T_I	T_D
P	$\frac{T}{\mu\tau}$		
PI	$\frac{0.9T}{\mu\tau}$	3τ	
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Practical Implementation of PID Controllers: Example

Example:

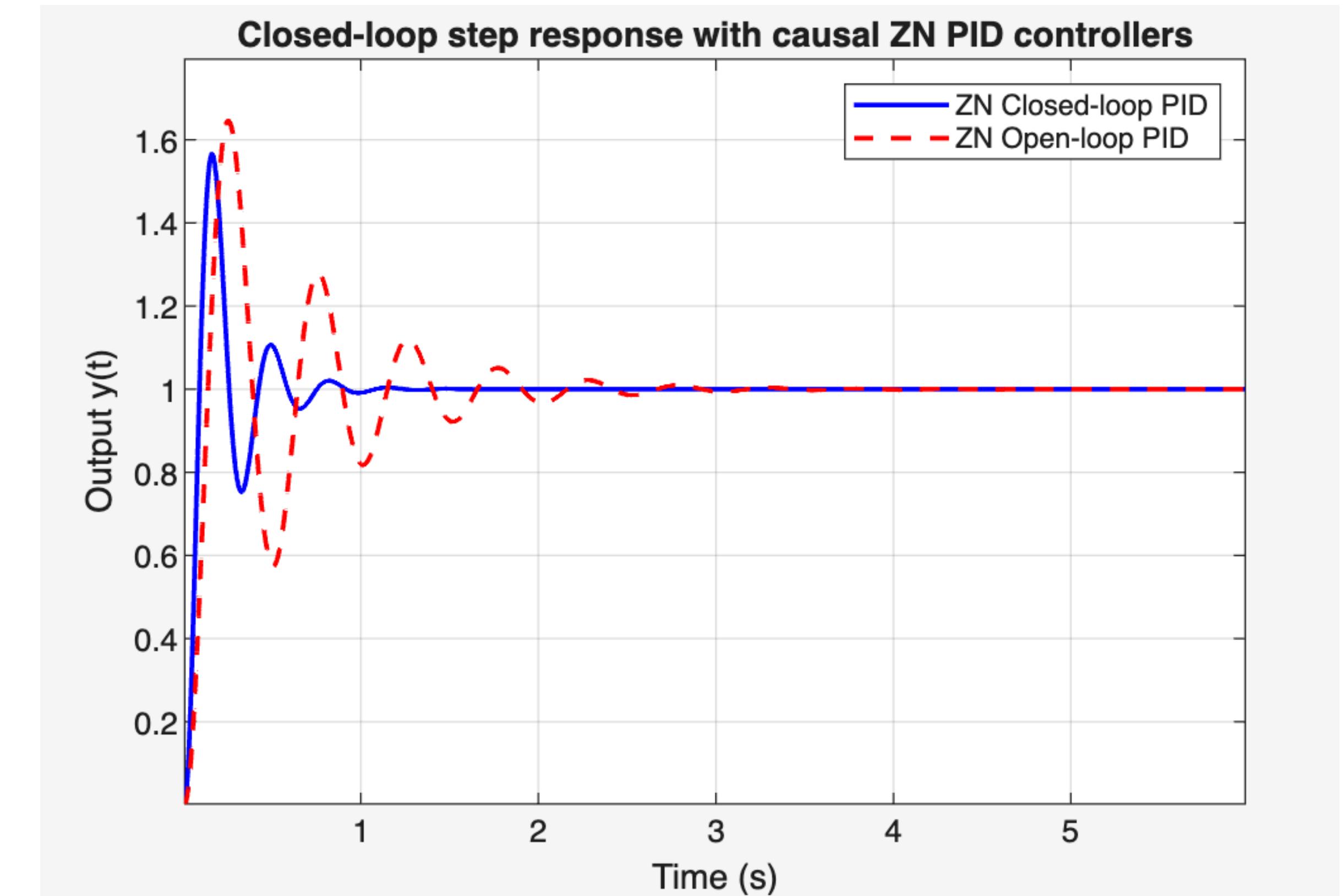
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Estimated critical gain Kcr = 210.00
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Closed-loop ZN PID (with derivative filter, tau_f=1.000000e-02):
Kp = 126.000, Ti = 0.141, Td = 0.035

Approximate FOPDT model parameters:
mu = 0.067, tau = 0.053, T = 0.175

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Practical Implementation of PID Controllers: Example

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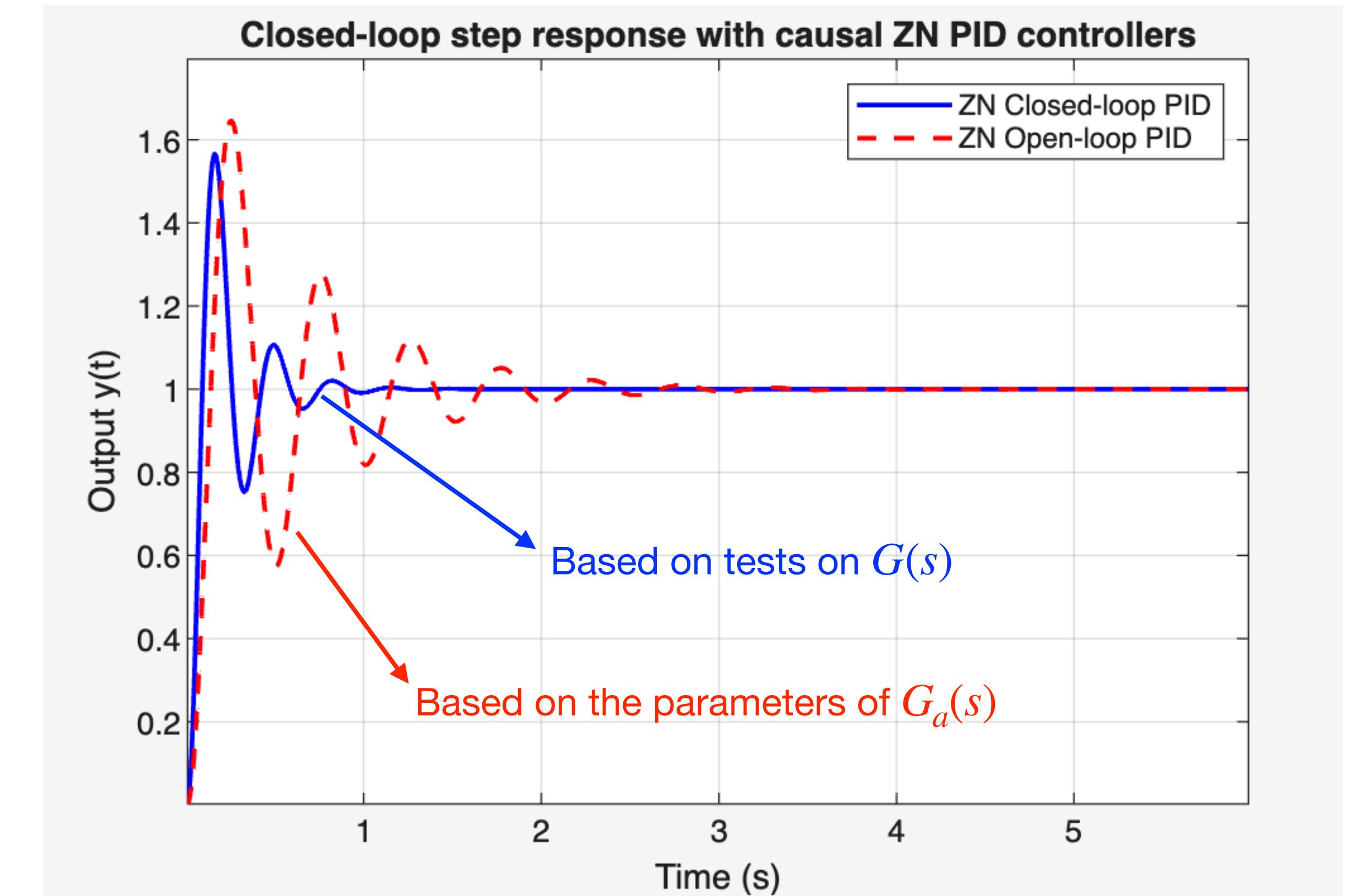
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Practical Implementation of PID Controllers: Example

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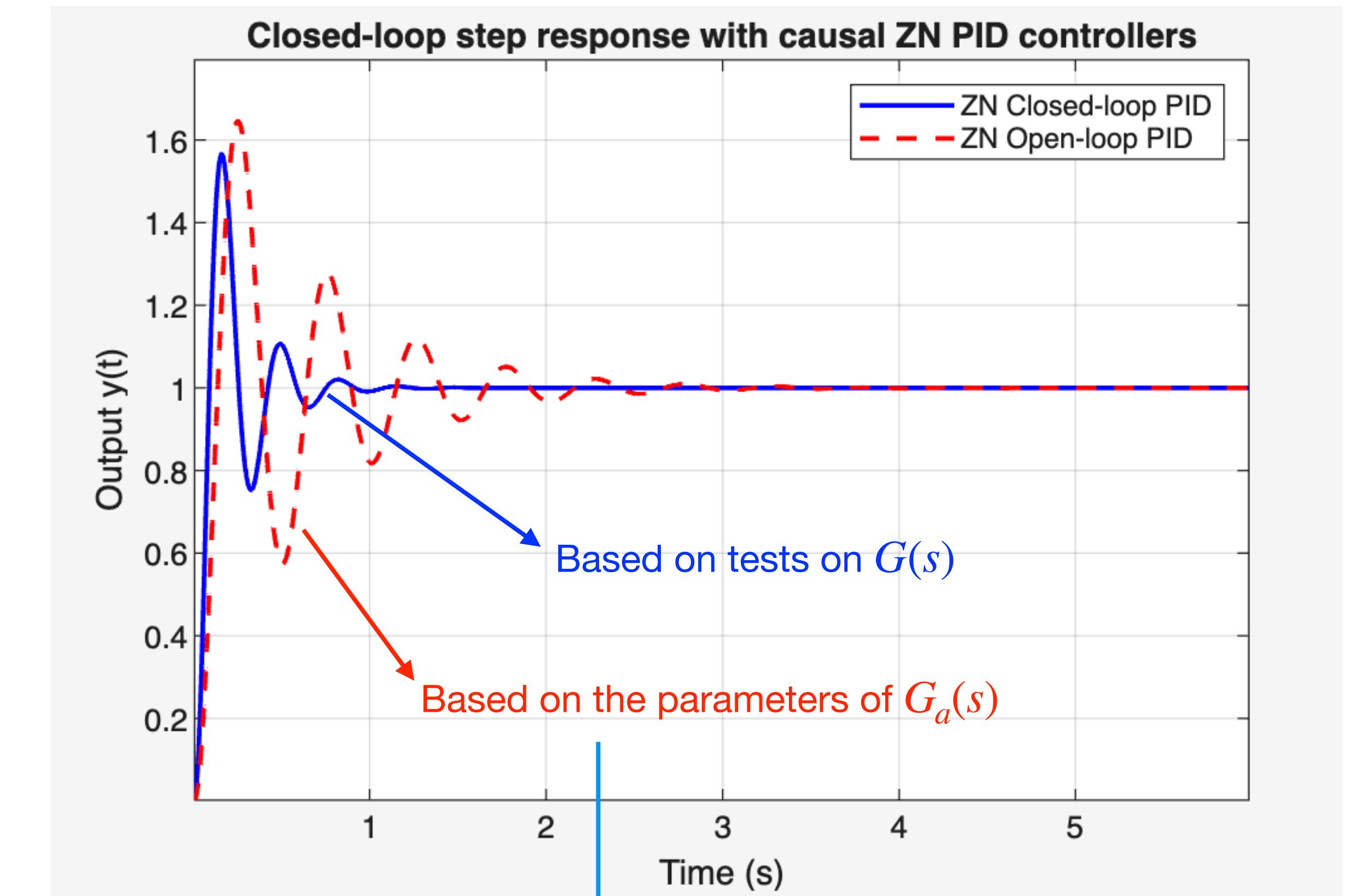
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```



in the example we are approximating a 3rd order system with a first order system with delay!



Practical Implementation of PID Controllers: Example

Process model:

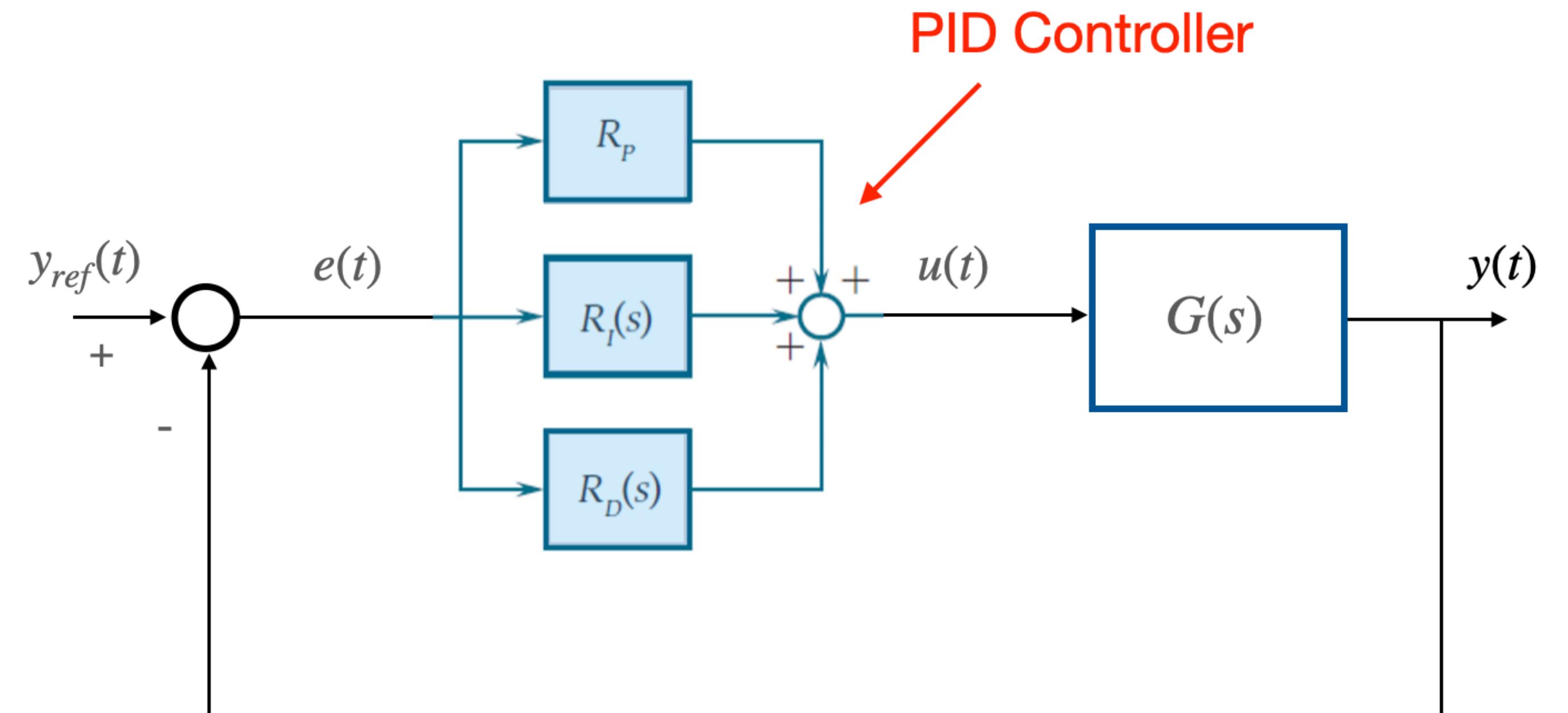
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Approximate Model of the Process:

$$G_a(s) = \frac{\mu e^{-\tau s}}{1 + Ts}$$

$$\mu = 0.067 \quad \tau = 0.053 \quad T = 0.175$$

Control scheme:



Practical Implementation of PID Controllers: Example

Process model:

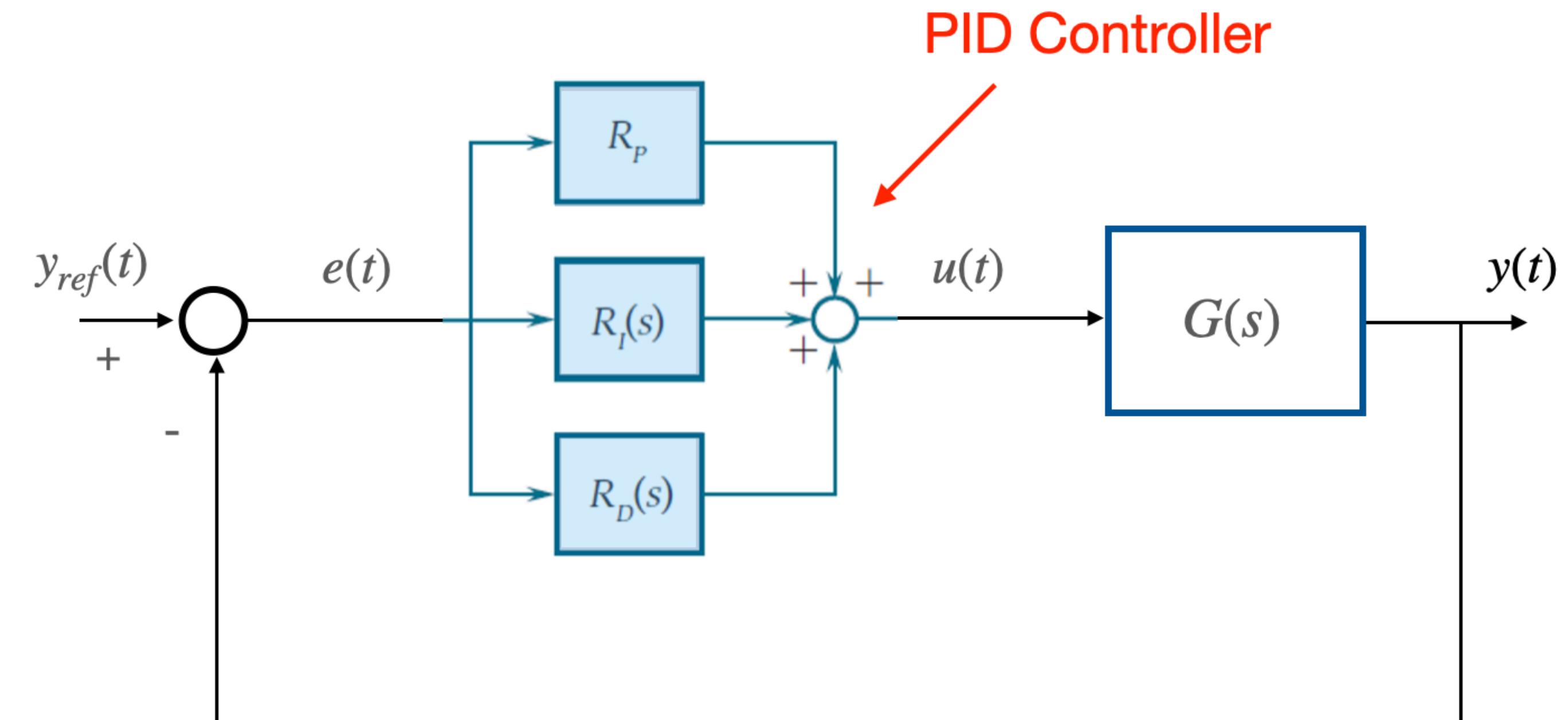
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Control scheme:



Objective: Compare the performance of the closed loop system with PID designed via Cohen-Coon rules and PID designed via the IMC method



Practical Implementation of PID Controllers: Example

Process model:

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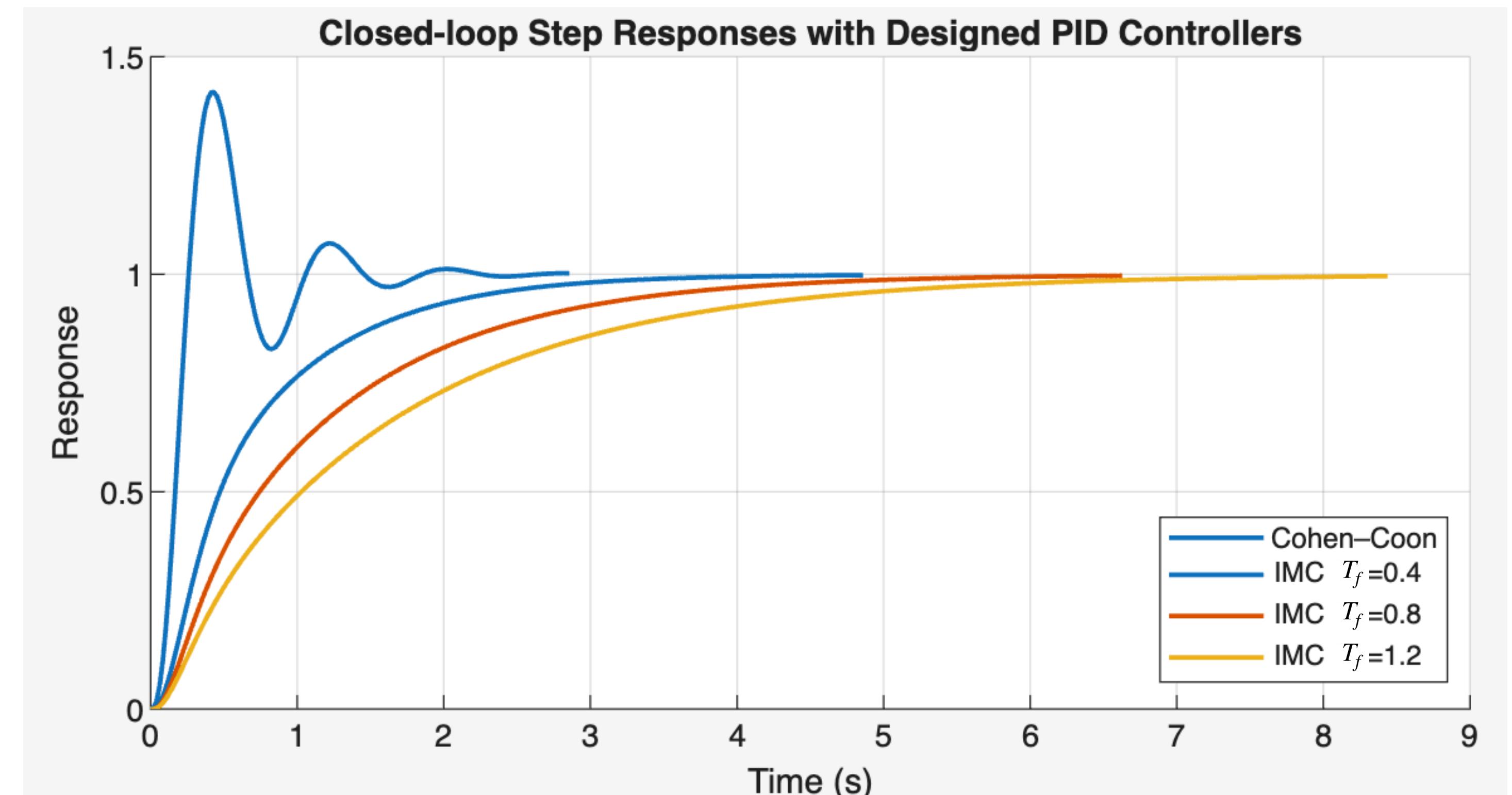
$$\mu = 0.067 \quad \tau = 0.053 \quad T = 0.175$$

Cohen-Coon PID (with derivative filter, $\tau_f=0.01$):
 $K_p = 23.4620, K_i = 169.5603, K_d = 0.4321$

IMC PID ($T_f = 0.4, \tau_f=0.01$):
 $K_p = 6.8182, K_i = 20.4545, K_d = 0.6136$

IMC PID ($T_f = 0.8, \tau_f=0.01$):
 $K_p = 4.4118, K_i = 13.2353, K_d = 0.3971$

IMC PID ($T_f = 1.2, \tau_f=0.01$):
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Practical Implementation of PID Controllers: Example

Process model:

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Approximate Model of the Process:

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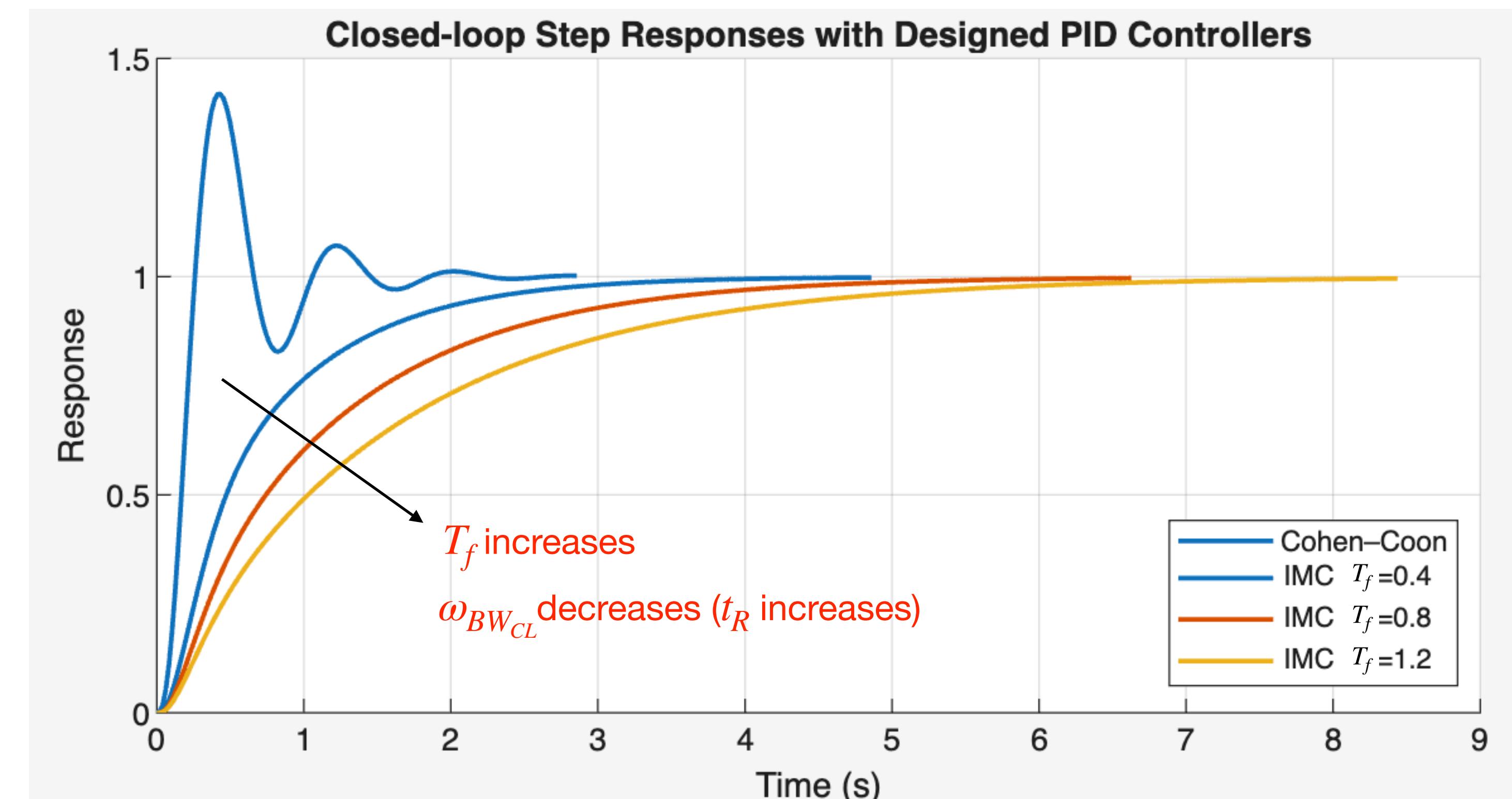
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Practical Implementation of PID Controllers: Example

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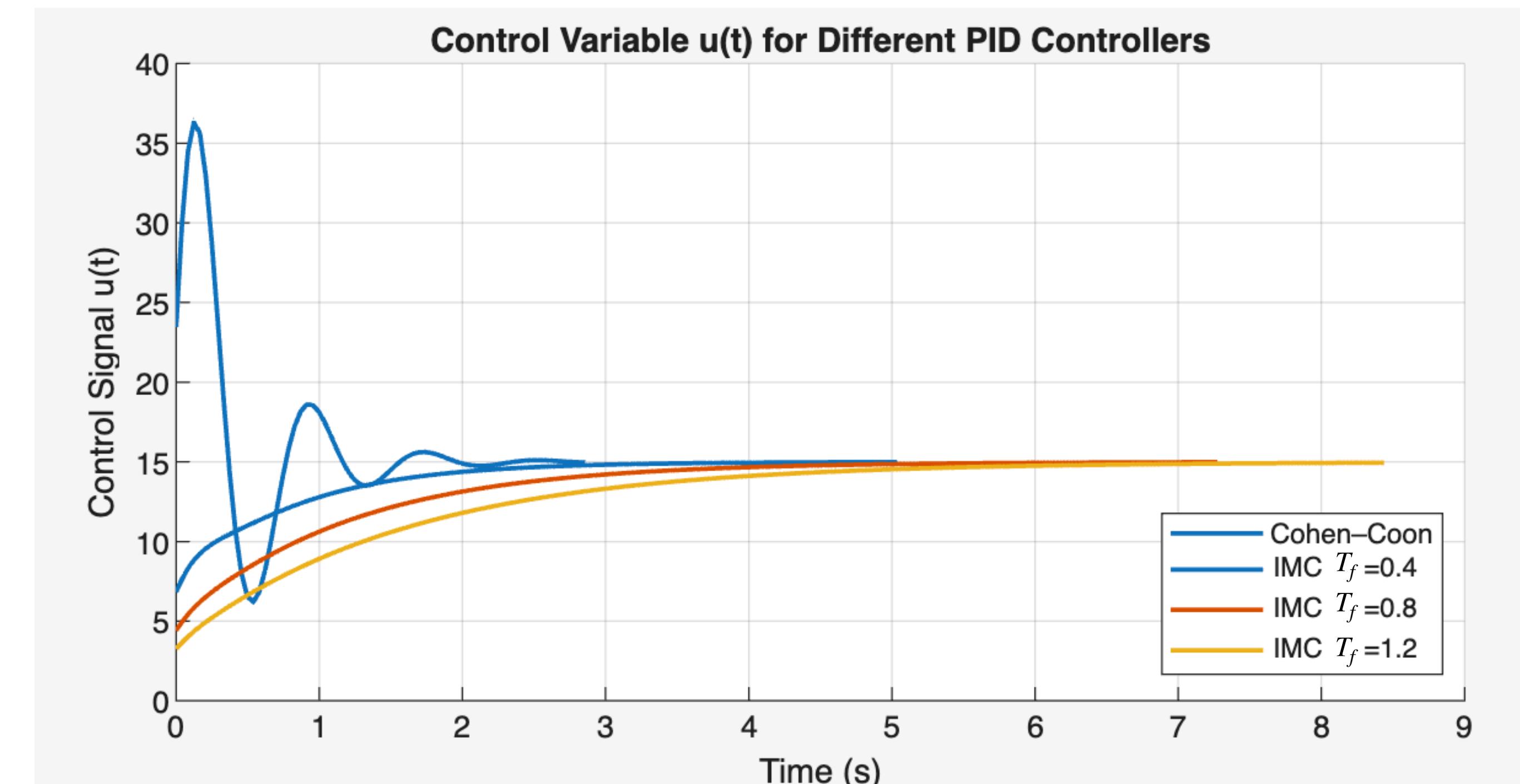
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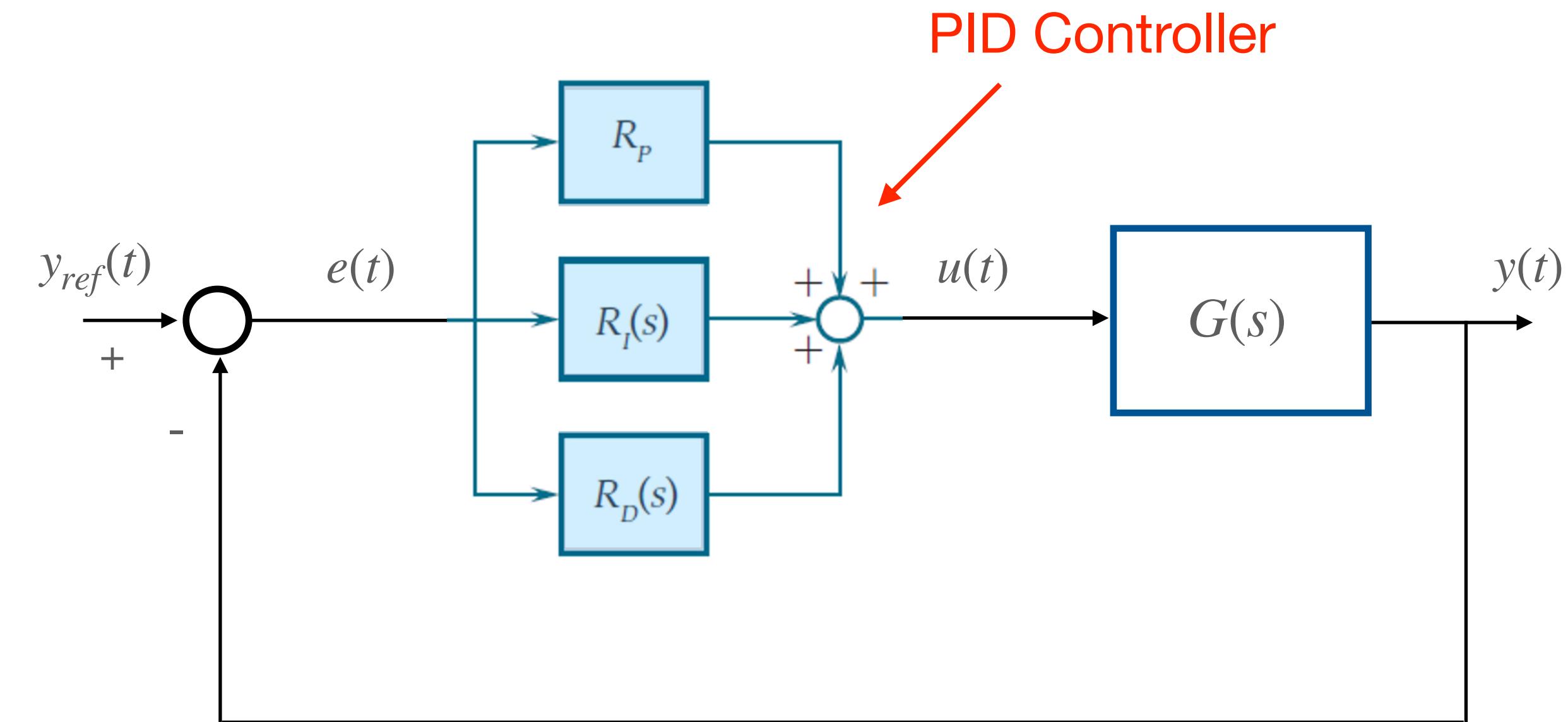
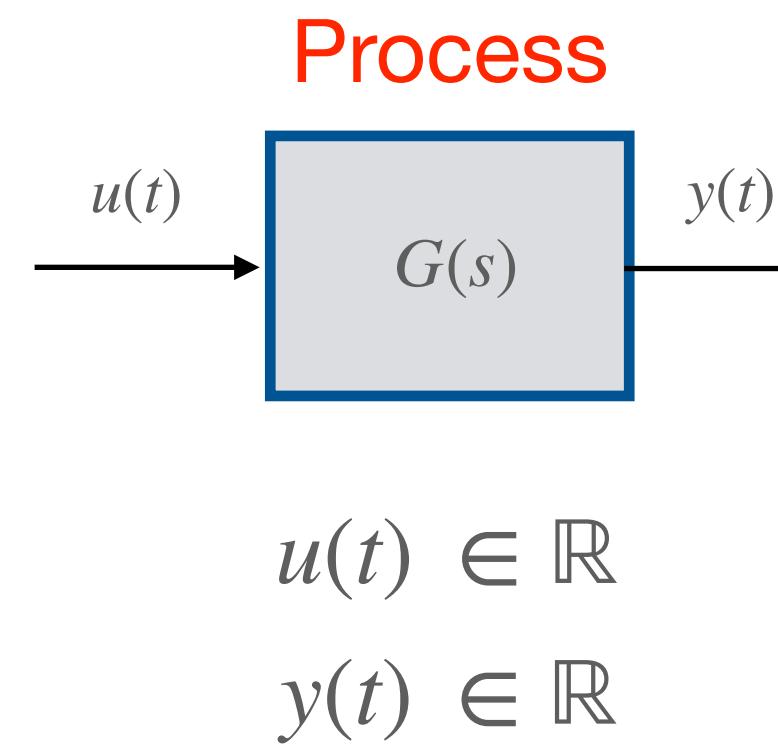
IMC PID ($T_f = 1.2$, $\tau_f=0.01$):
 $K_p = 3.2609$, $K_i = 9.7826$, $K_d = 0.2935$



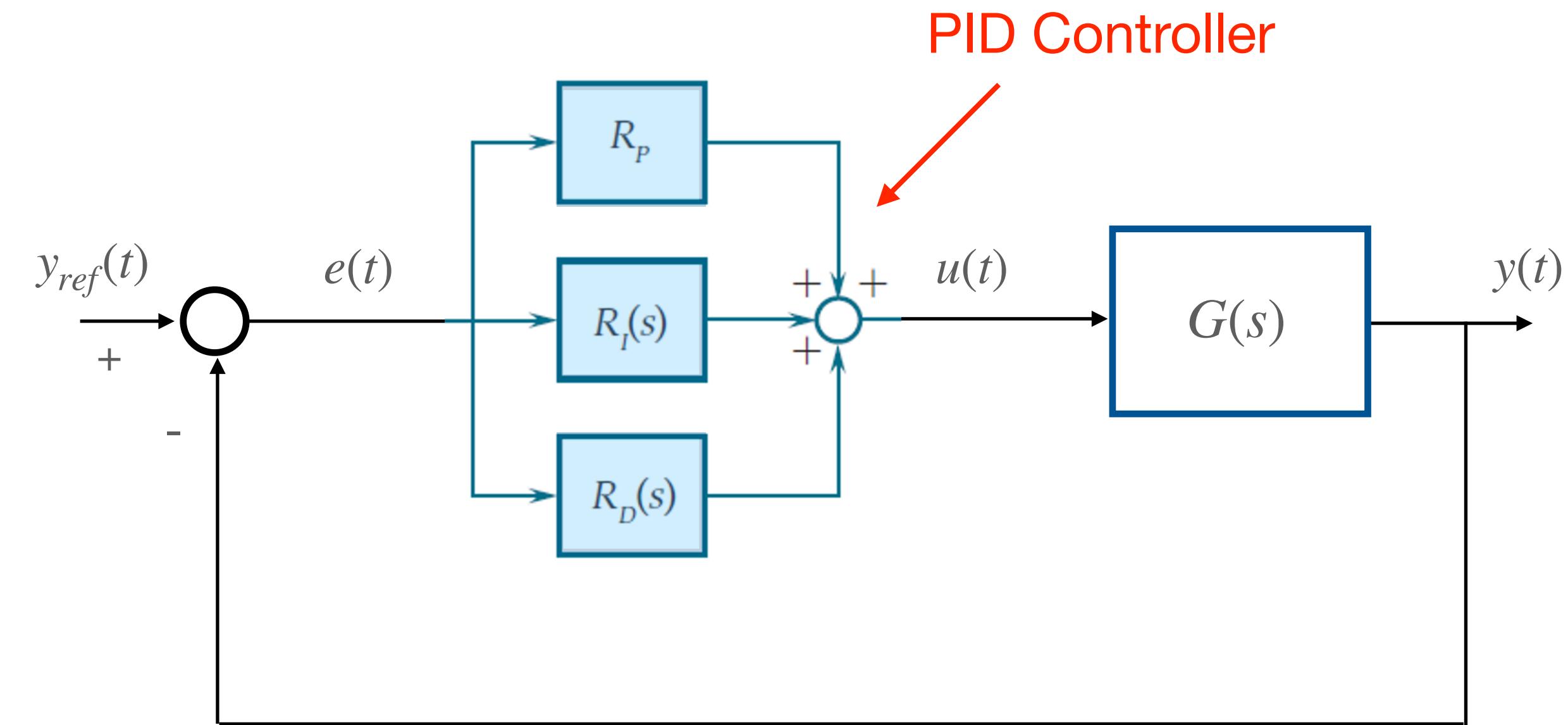
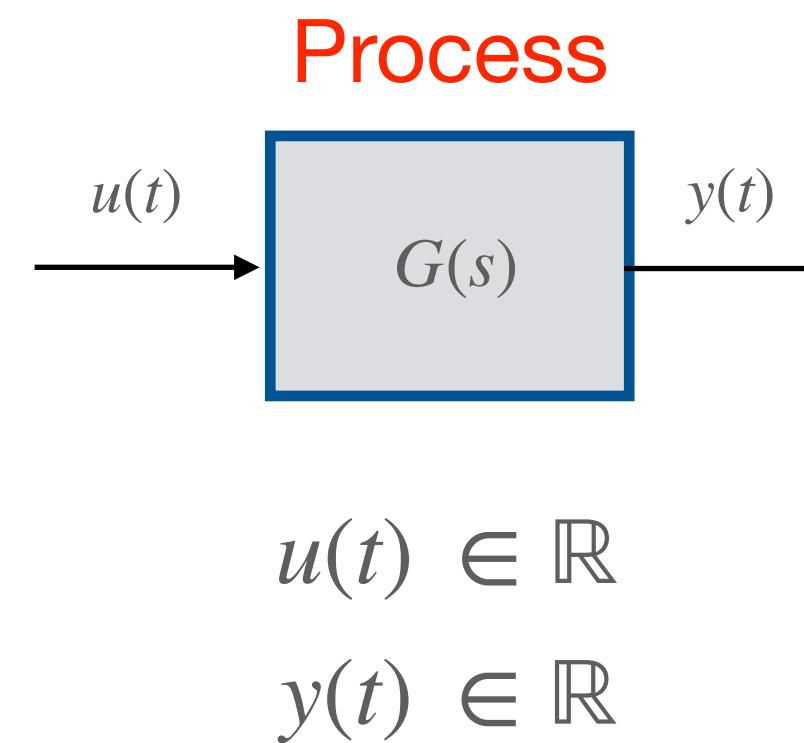
Note that: The IMC method produces more moderate control systems w.r.t. those obtained via the Cohen-Coon Method



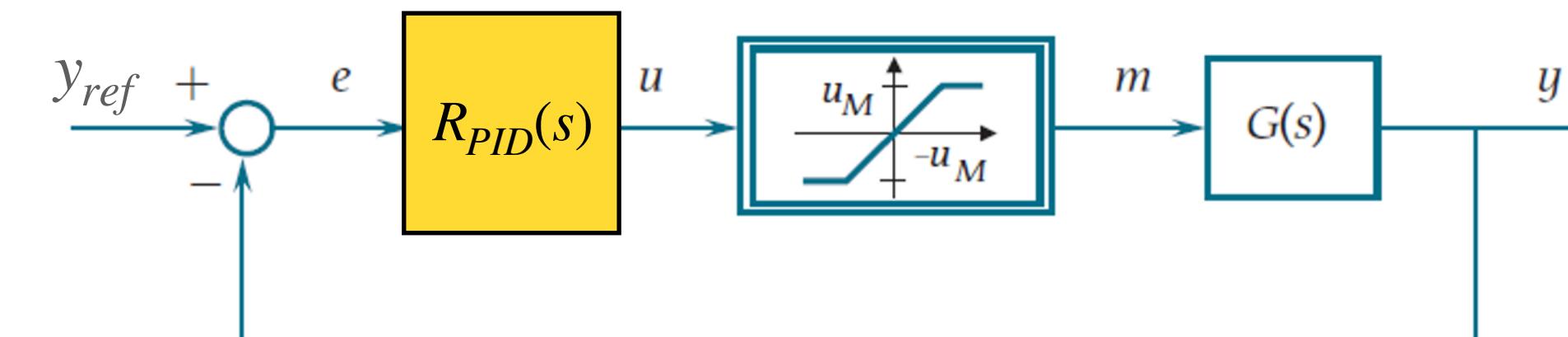
PID Controllers: Wind-up Effect



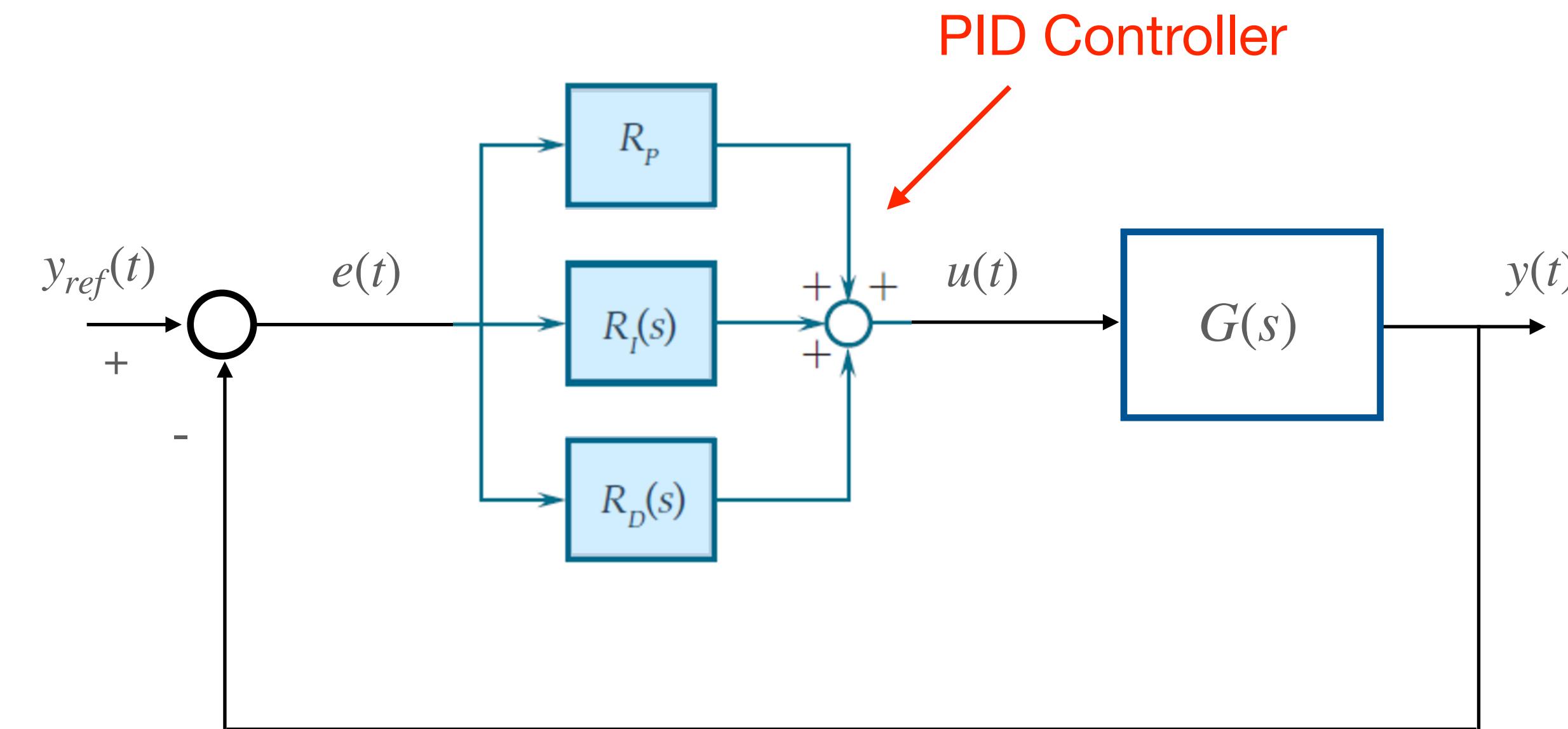
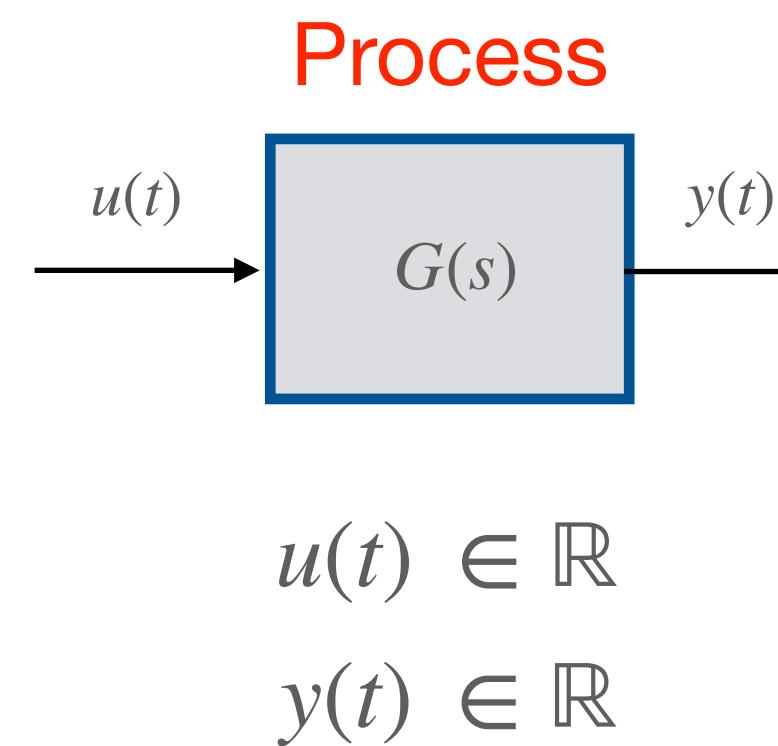
PID Controllers: Wind-up Effect



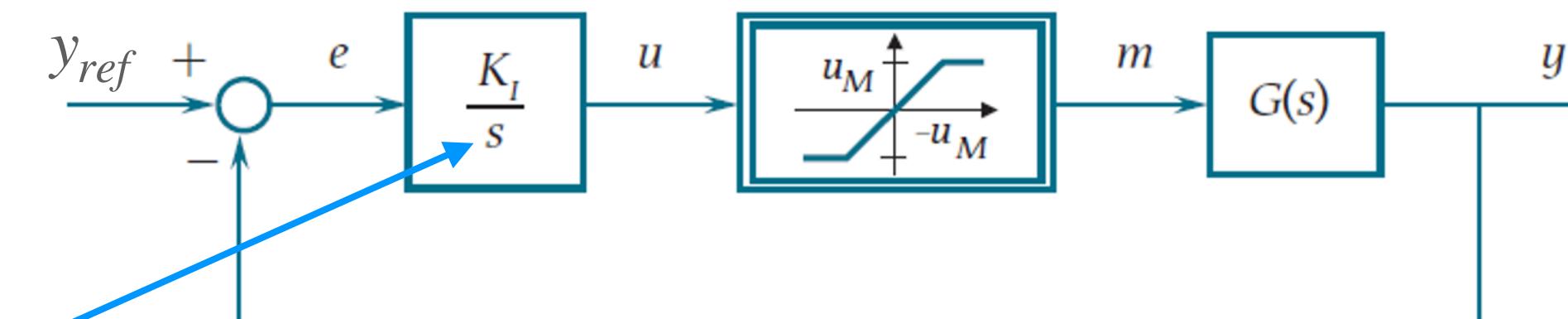
Realistic situation



PID Controllers: Wind-up Effect



Realistic situation

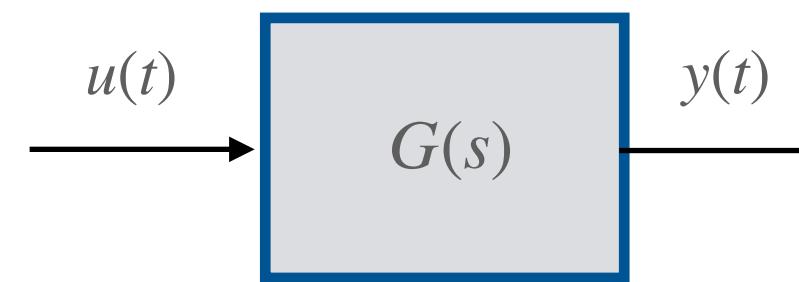


Only the integral component is considered

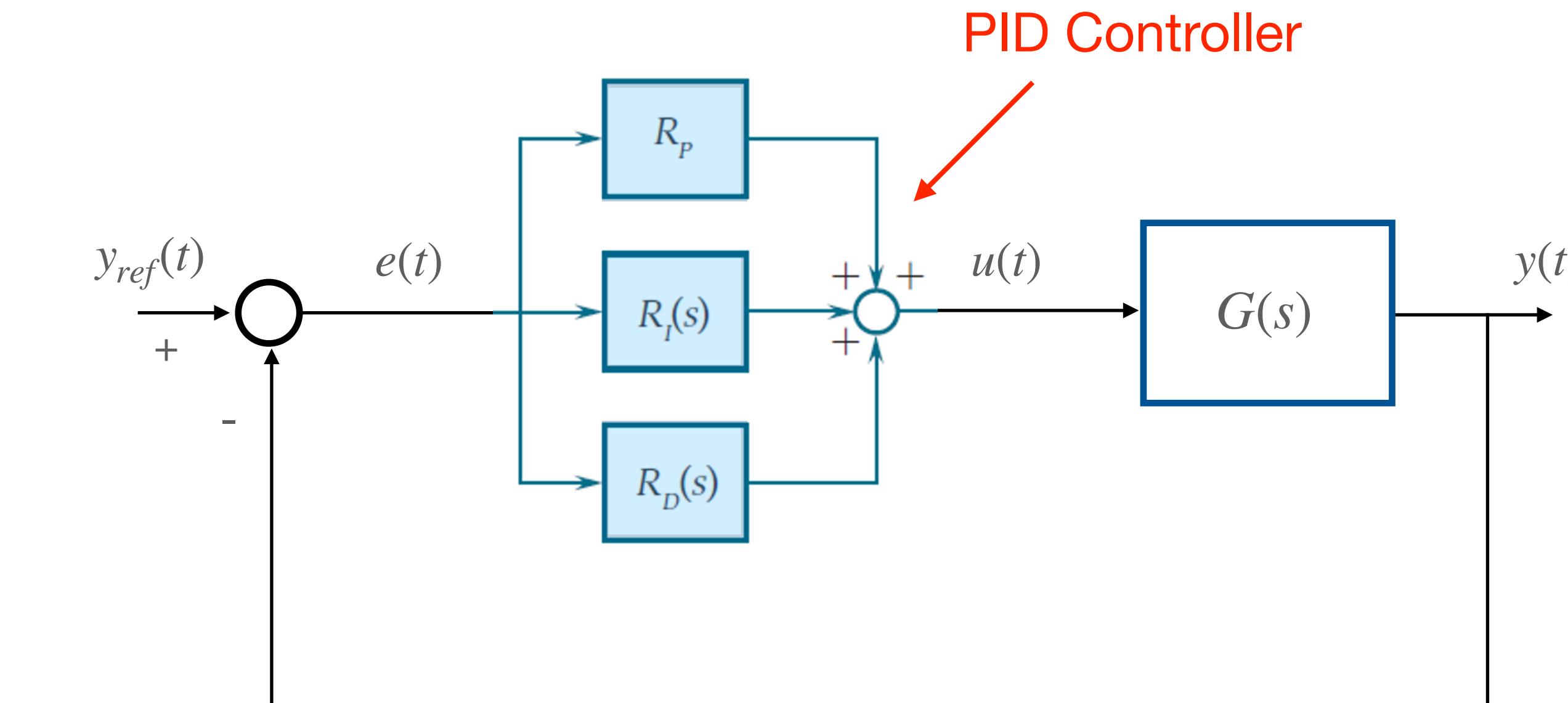
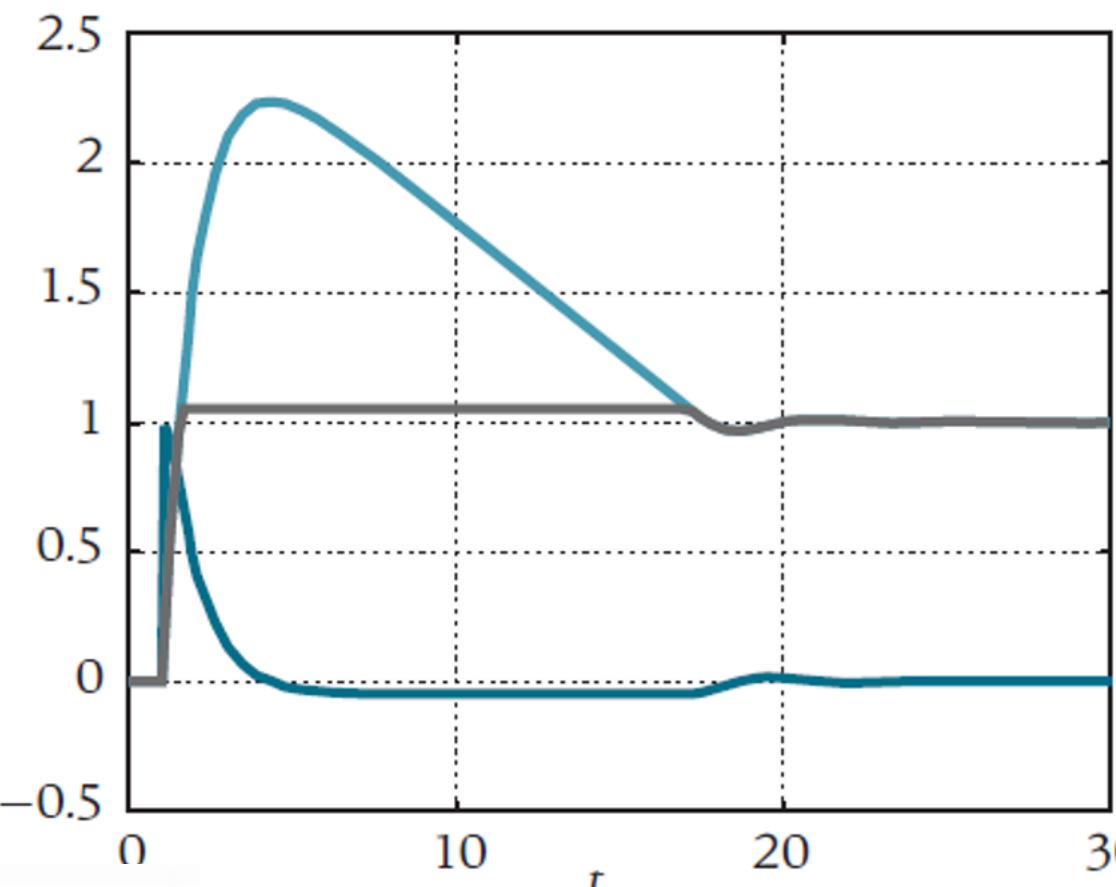


PID Controllers: Wind-up Effect

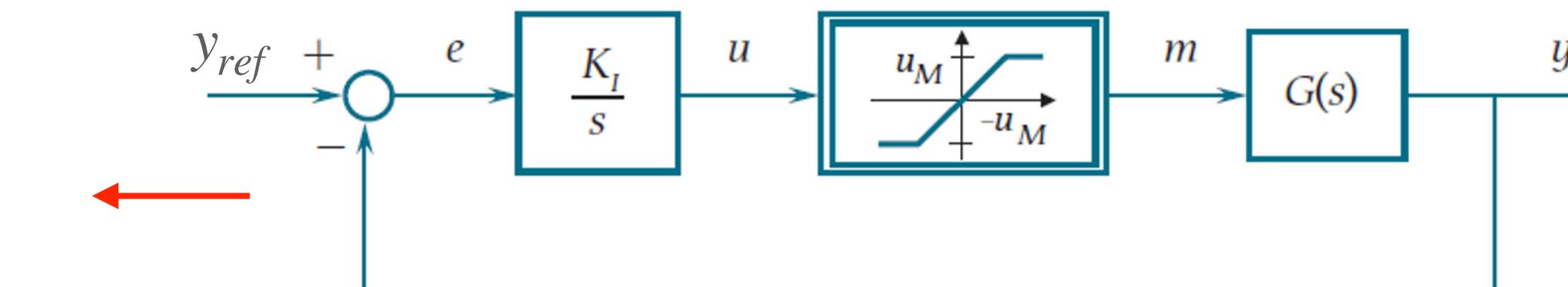
Process



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$

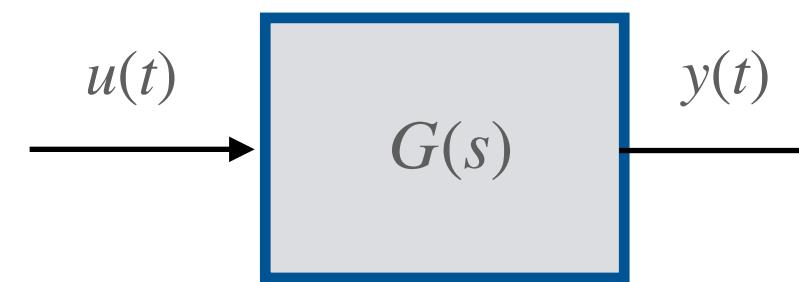


Realistic situation

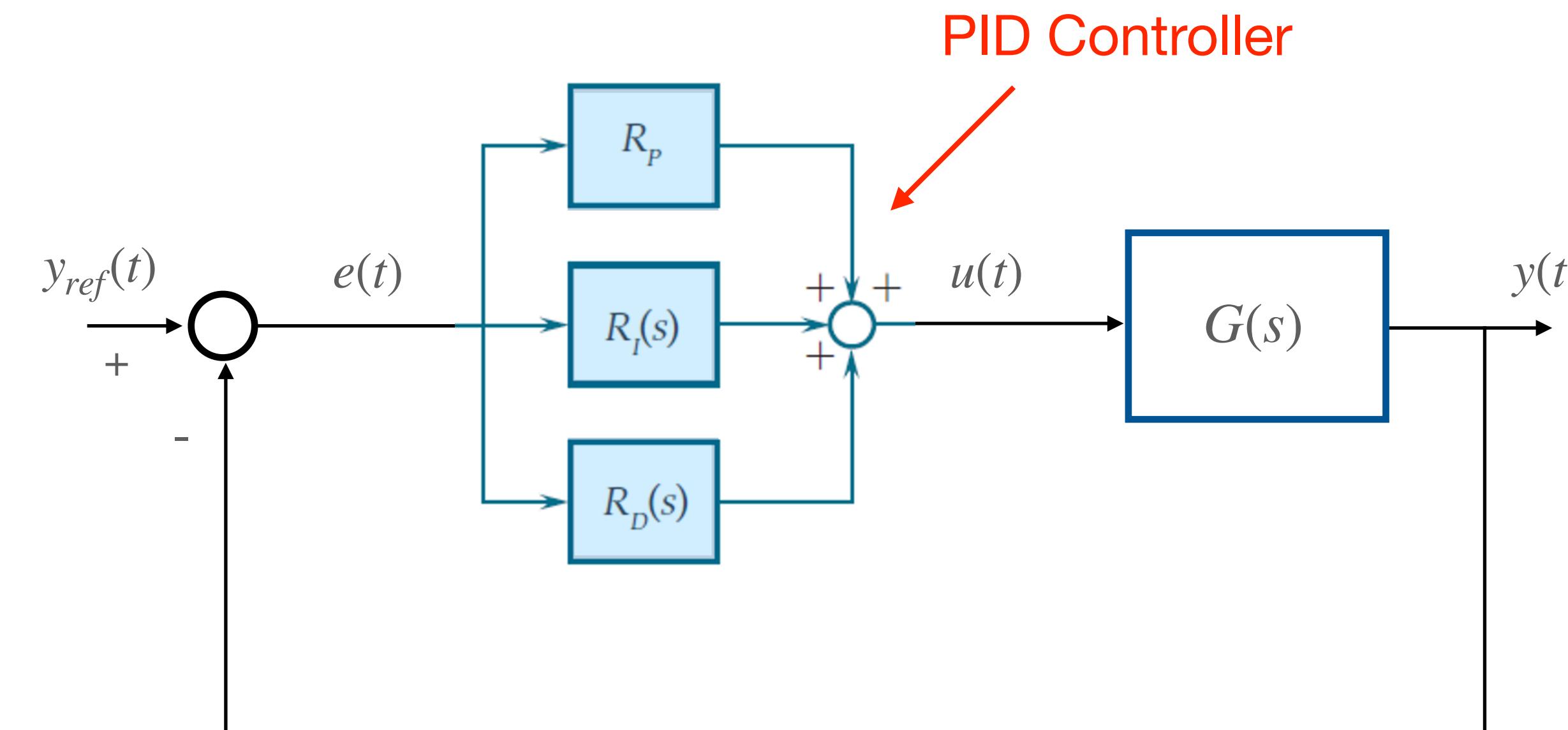
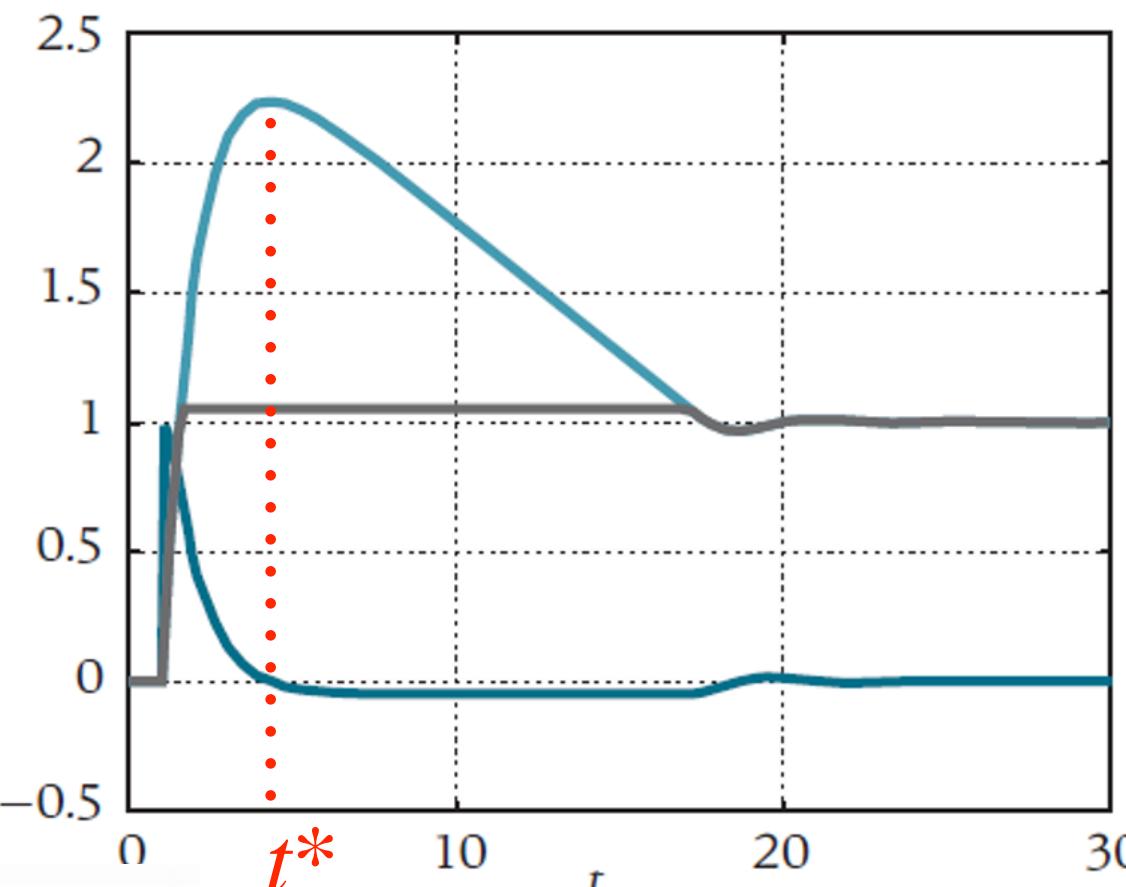


PID Controllers: Wind-up Effect

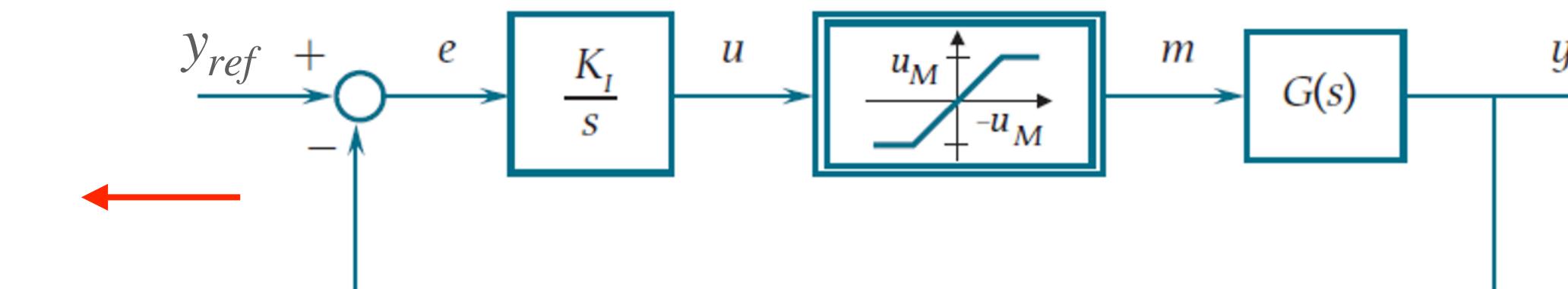
Process



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$

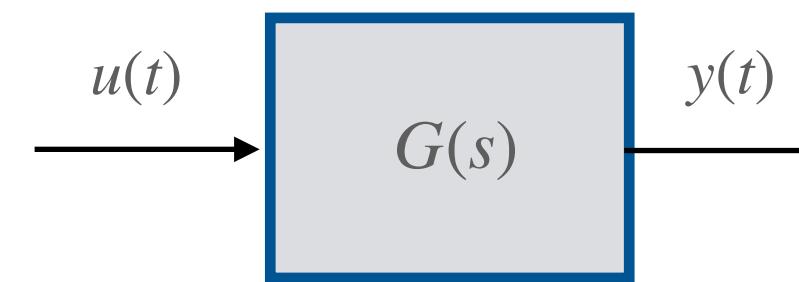


Realistic situation

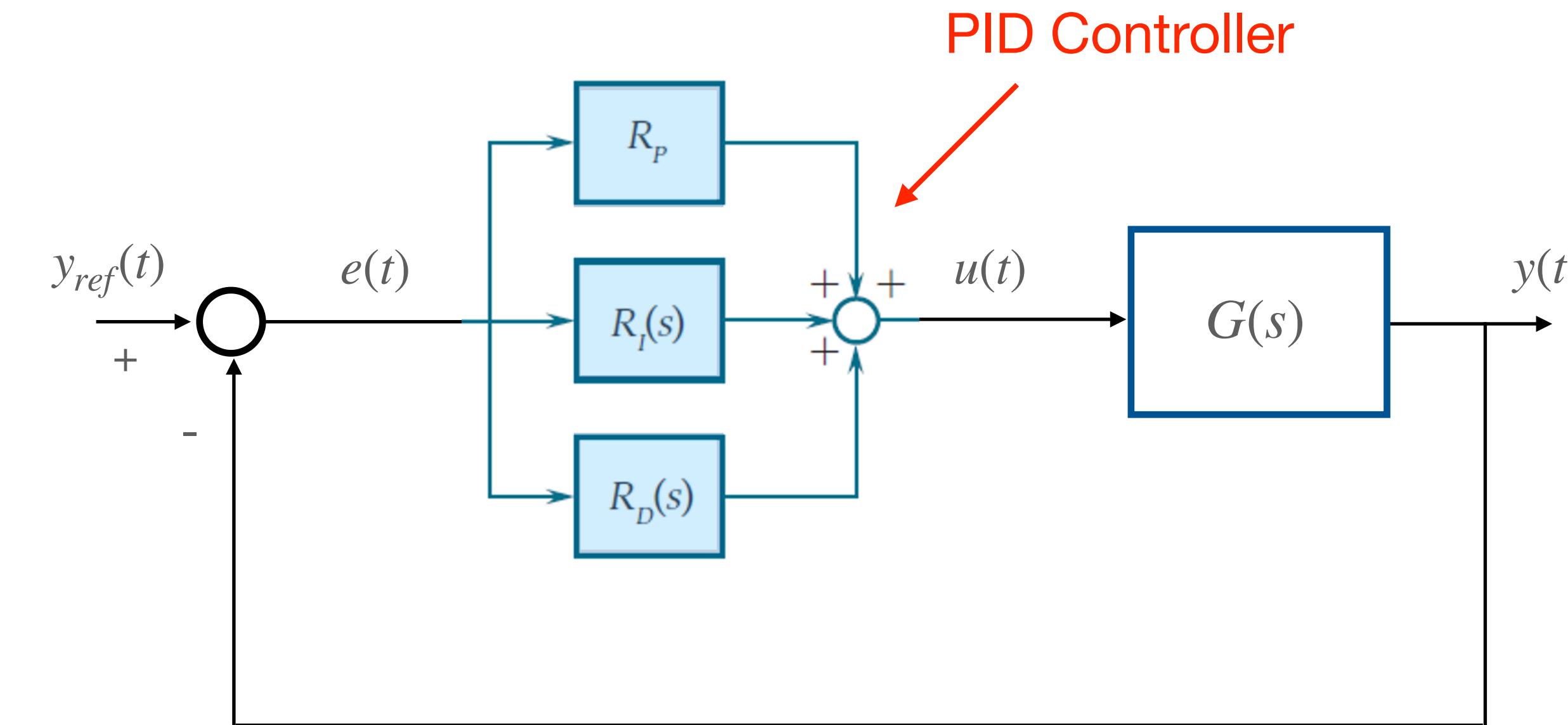


PID Controllers: Wind-up Effect

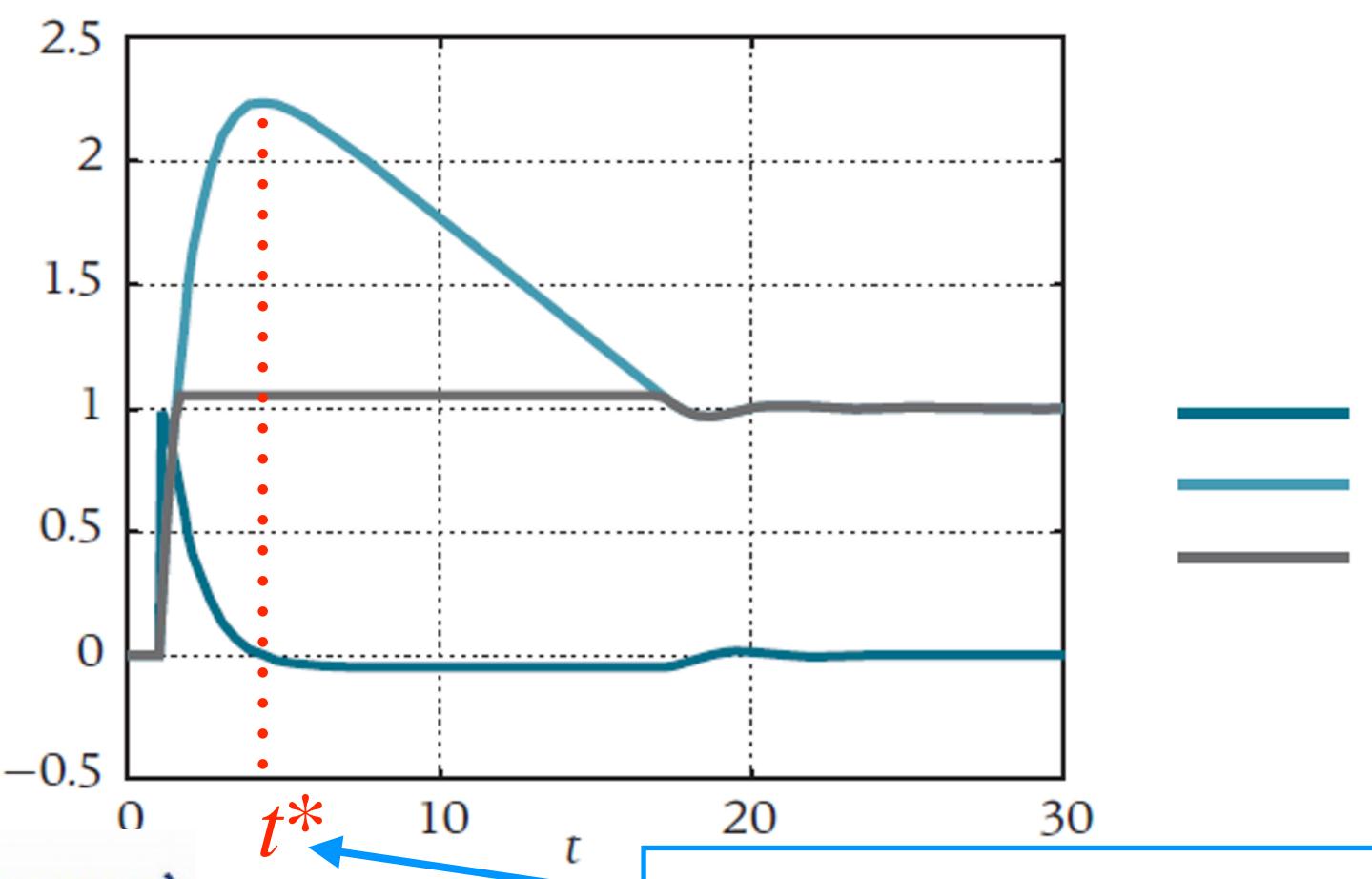
Process



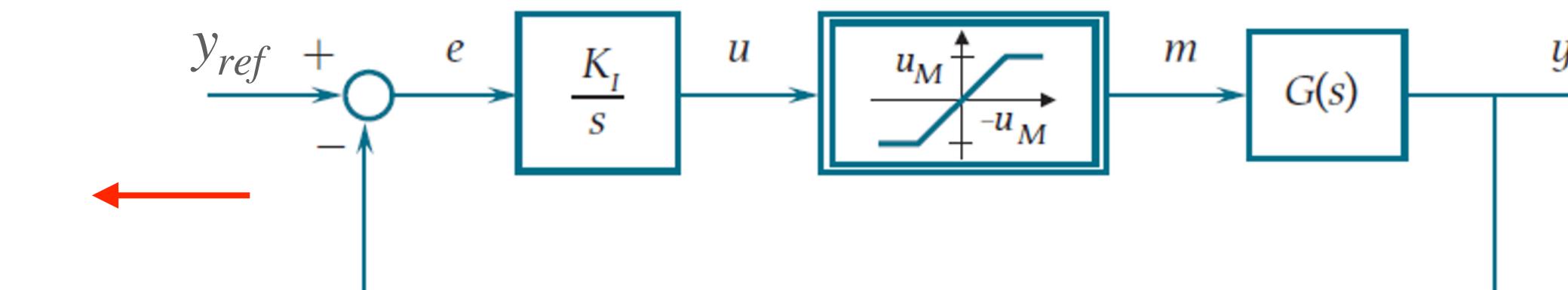
$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



PID Controller

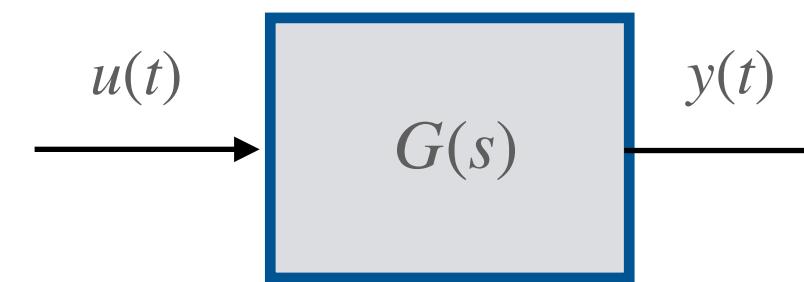


Realistic situation

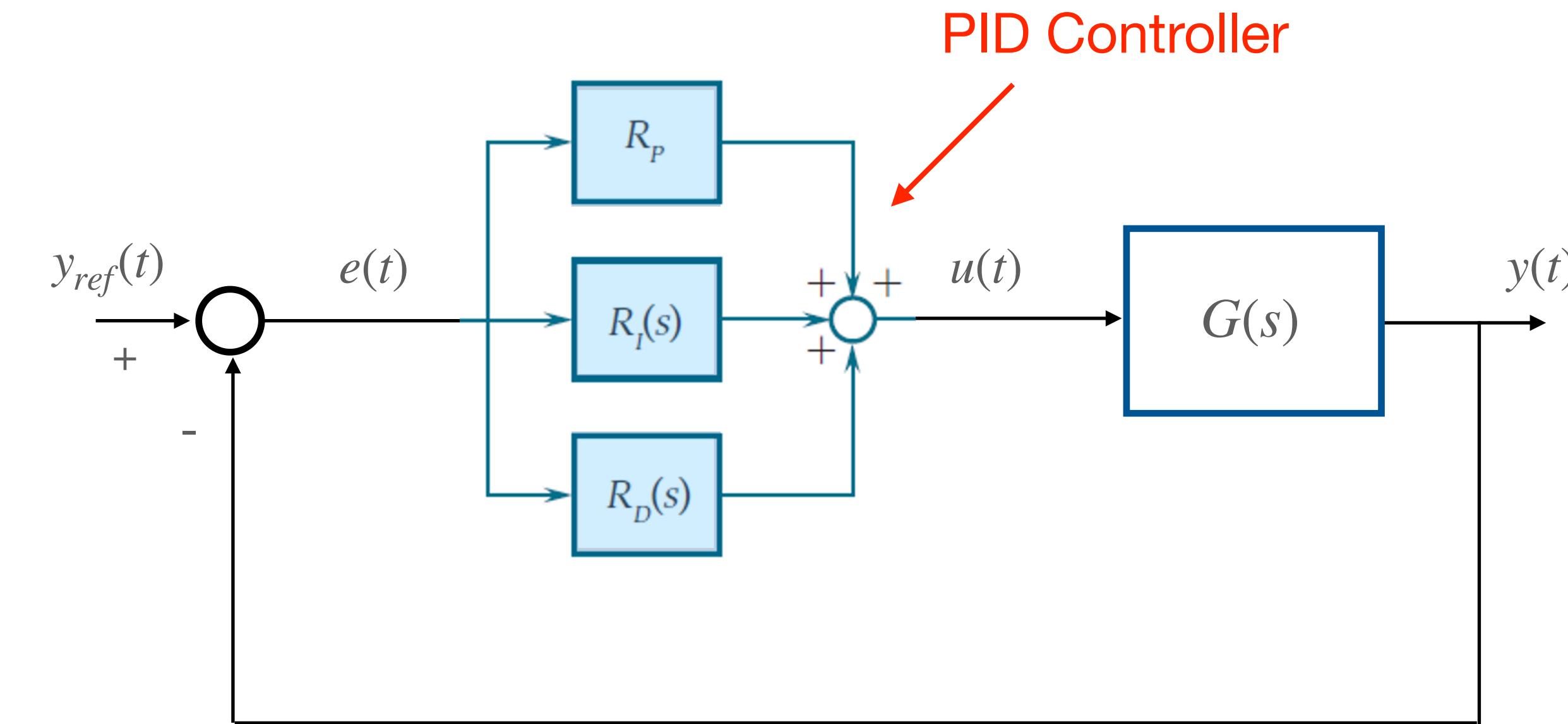


PID Controllers: Wind-up Effect

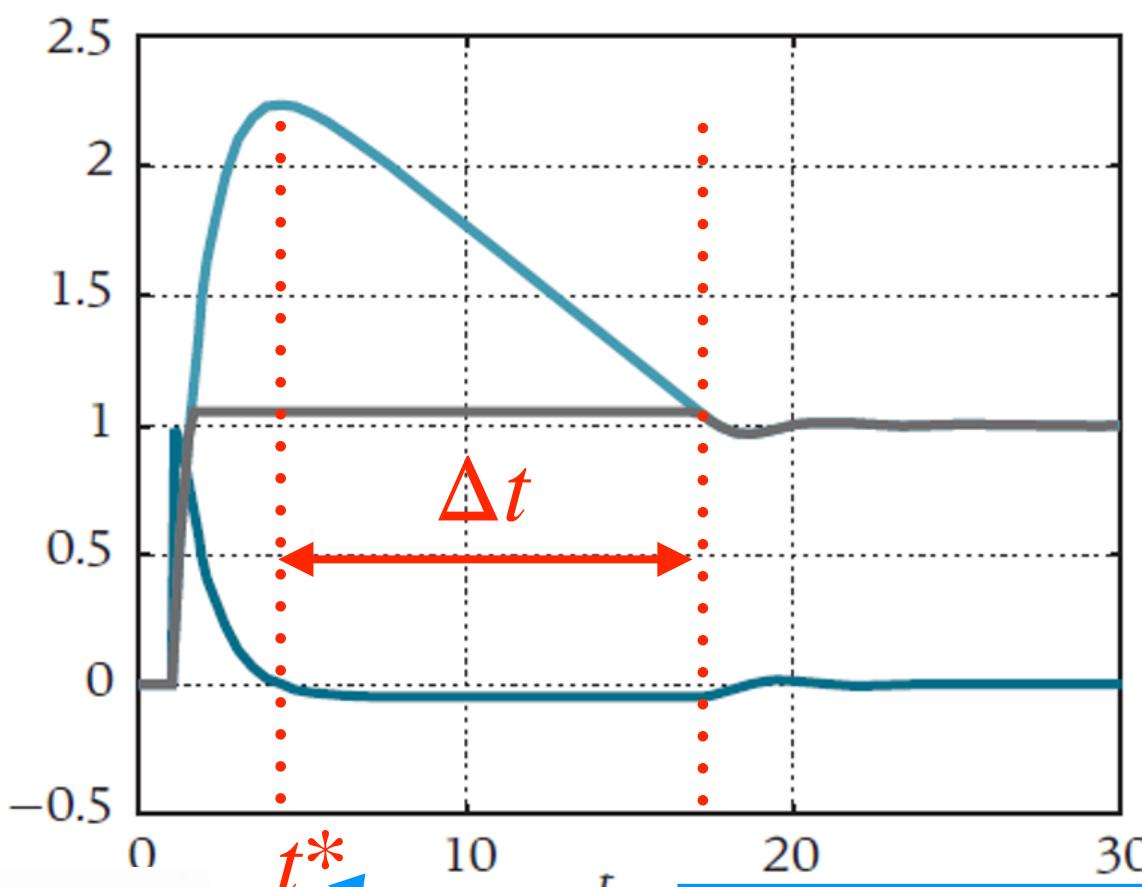
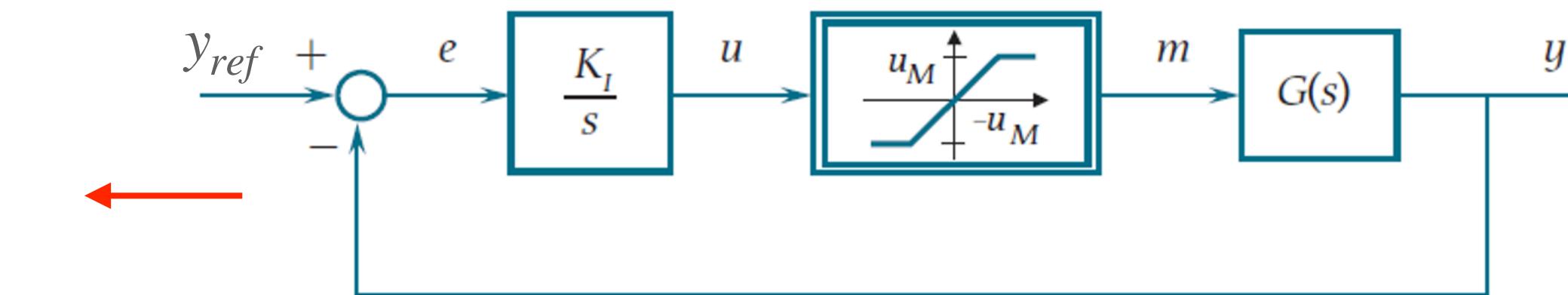
Process



$$\begin{aligned} u(t) &\in \mathbb{R} \\ y(t) &\in \mathbb{R} \end{aligned}$$



Realistic situation

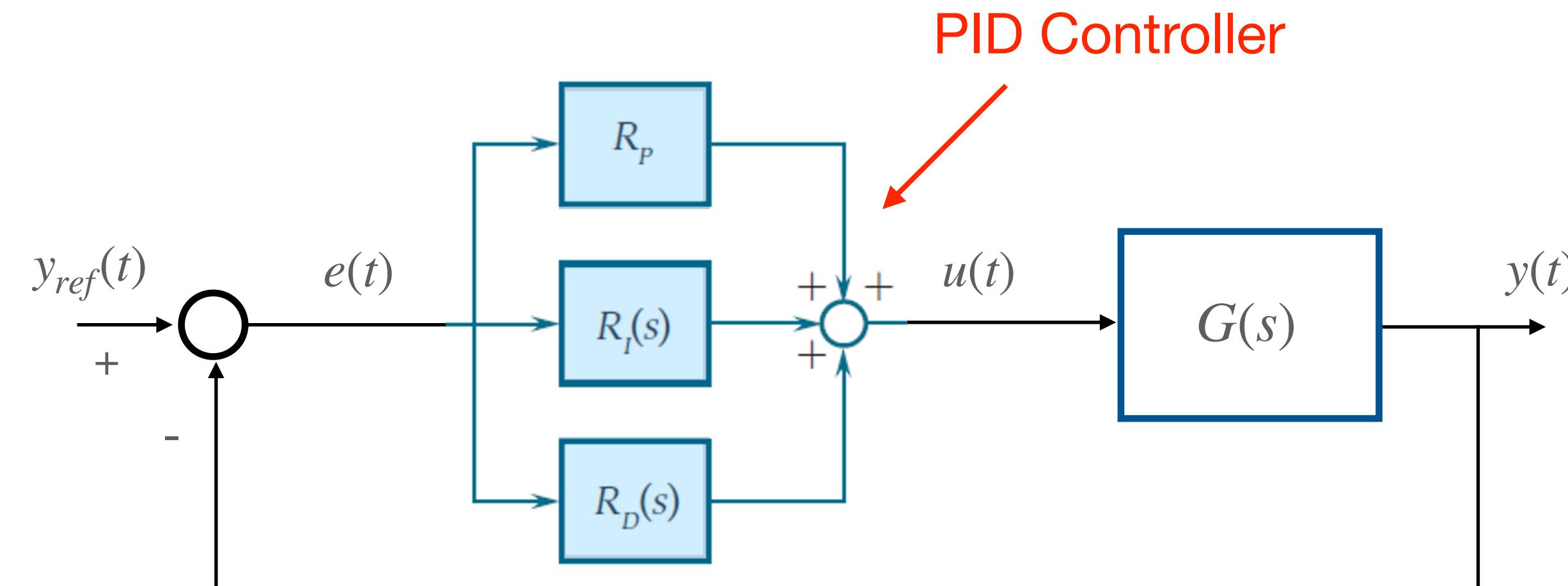


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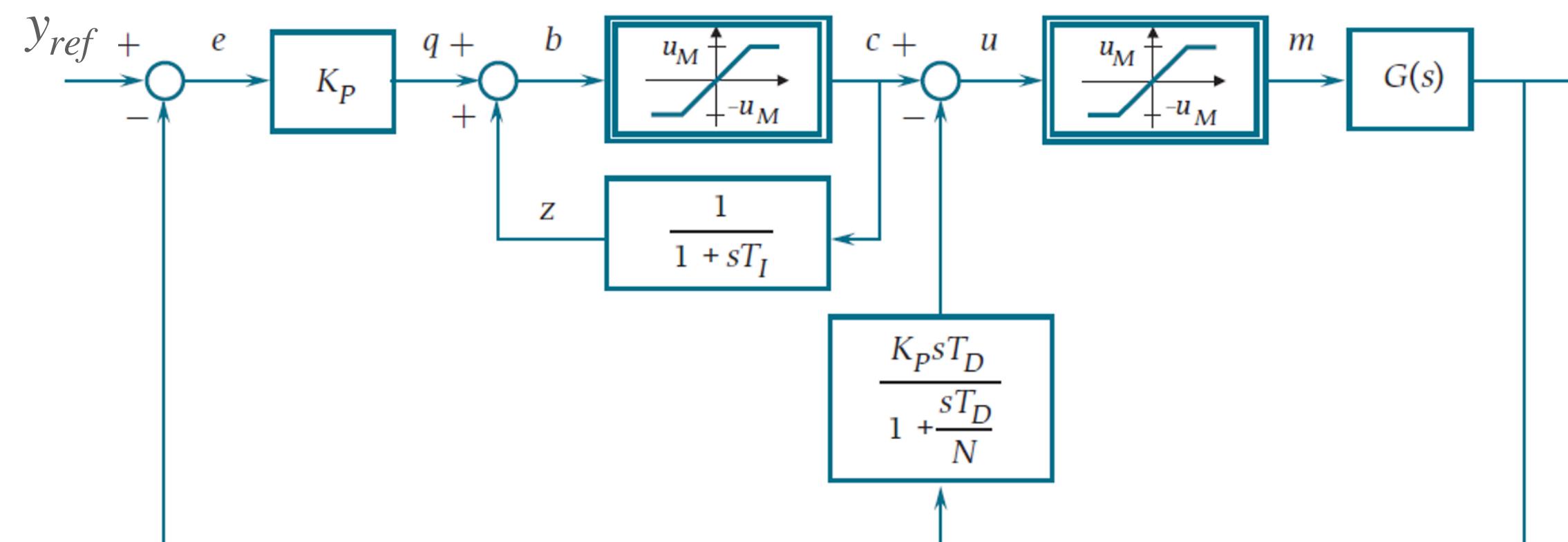
Ideal situation: the control action exits the saturation mode when e changes its sign (no useless waiting time due to wind-up)



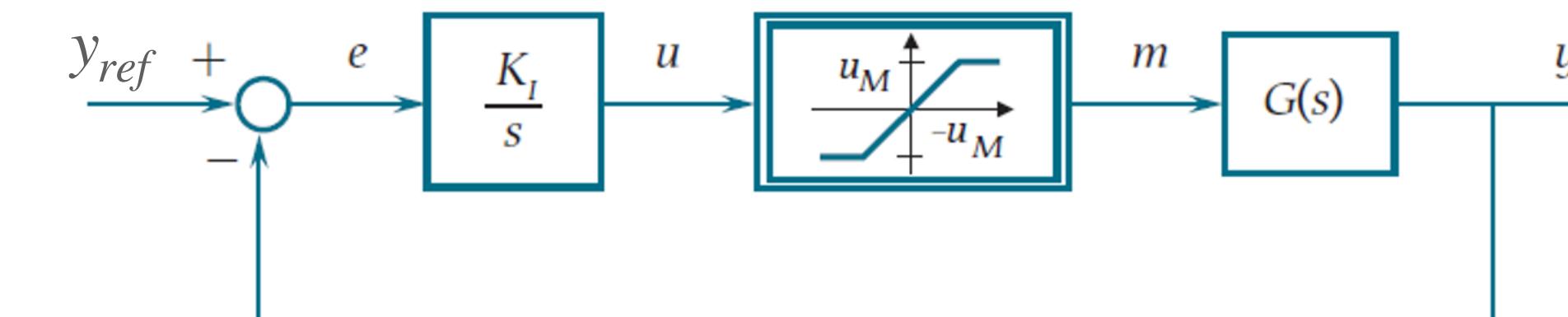
PID Controllers: Wind-up Effect

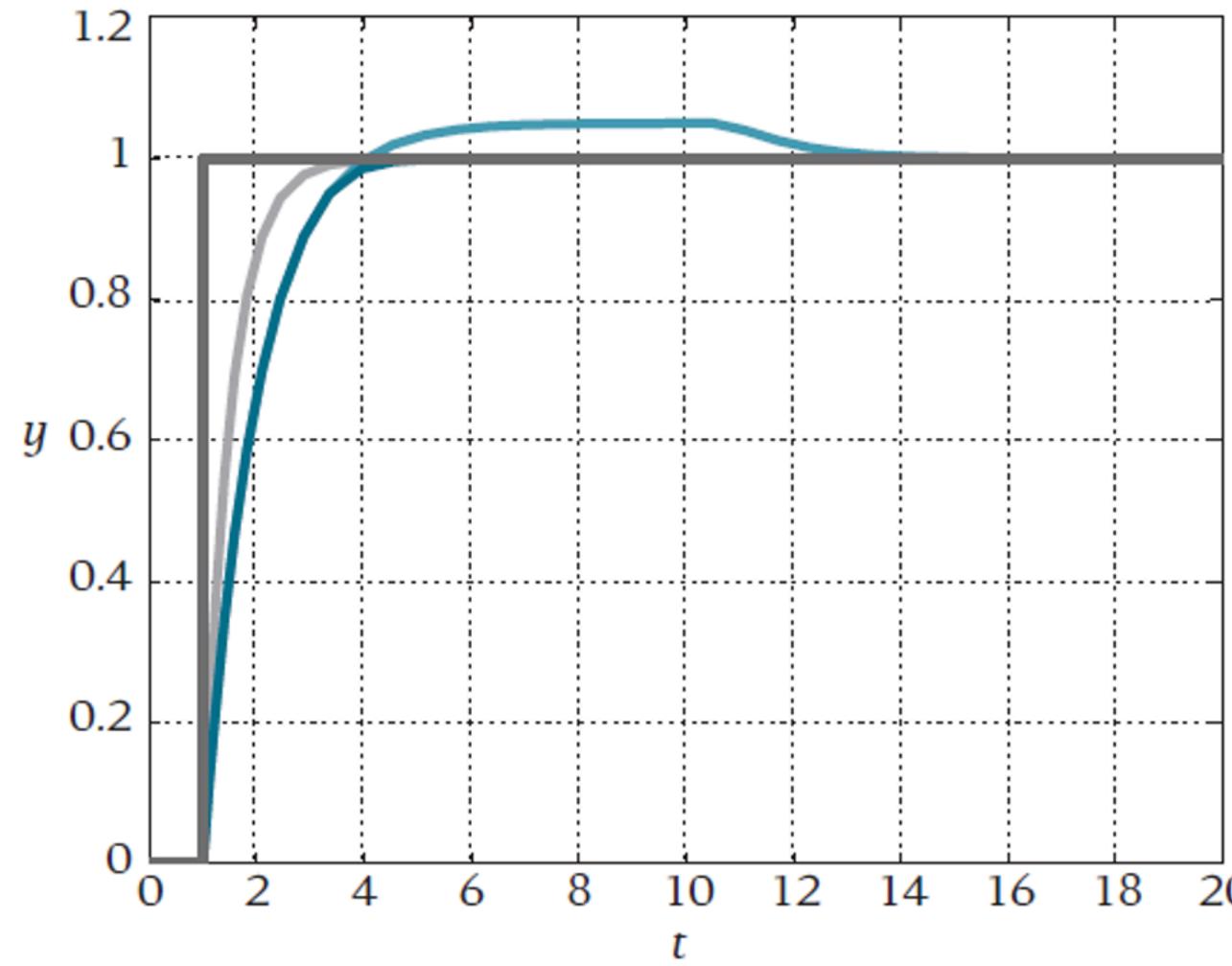


Solution: Anti-wind-up scheme

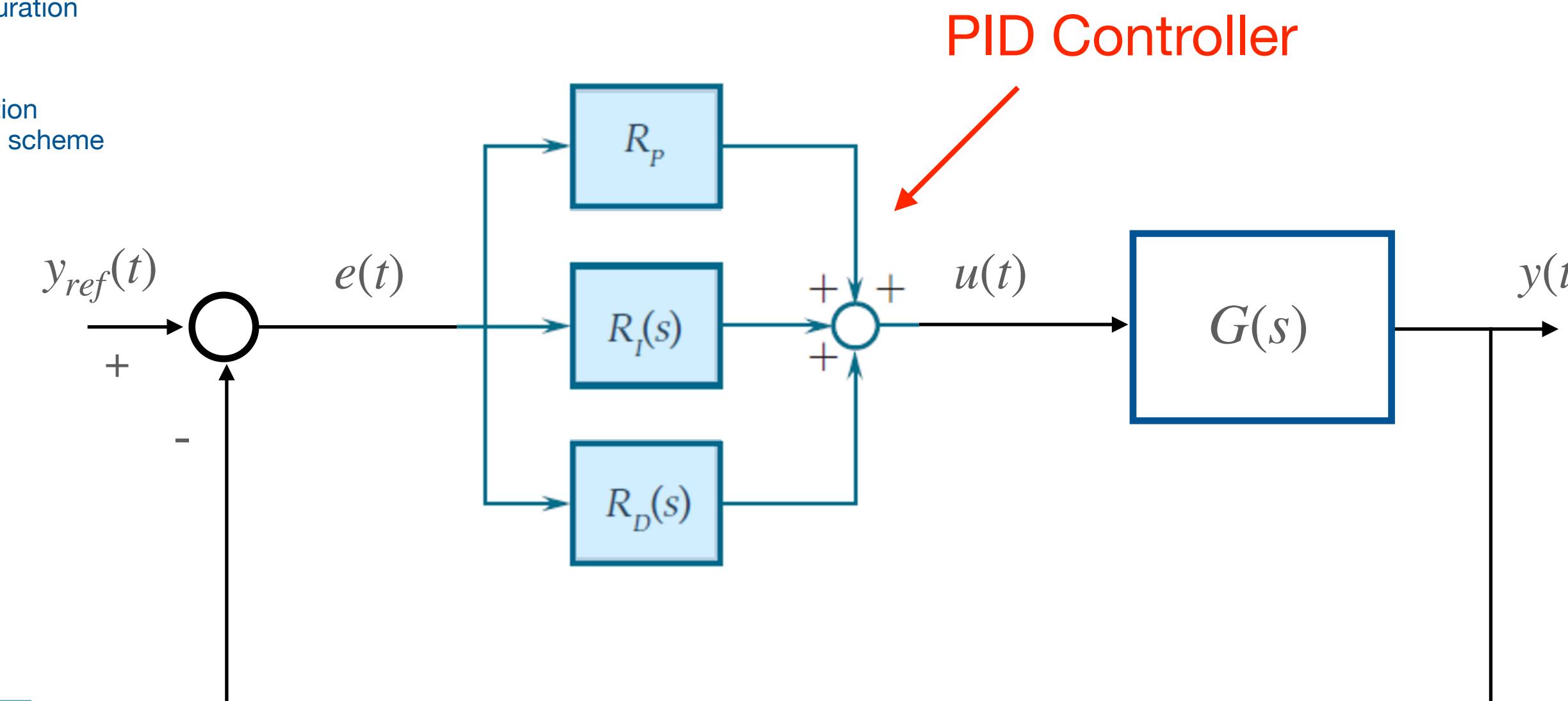


Realistic situation

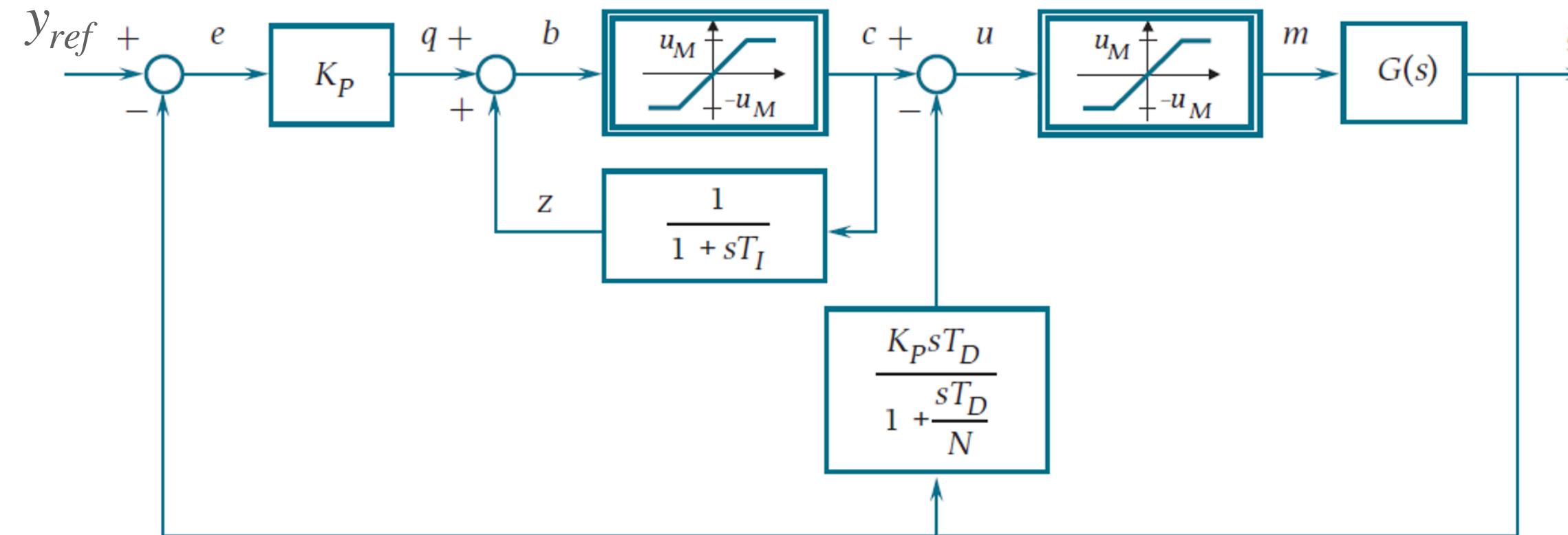




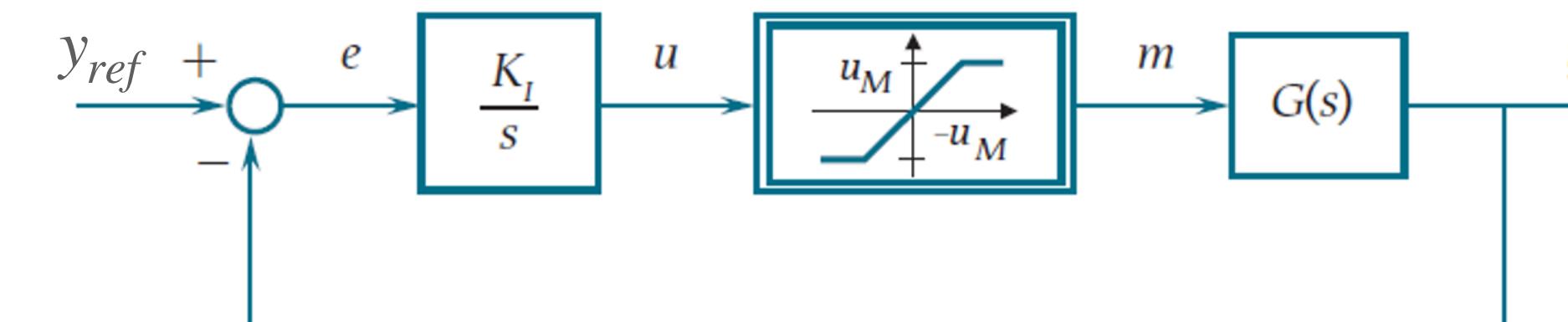
PID Controllers: Wind-up Effect



Solution: Anti-wind-up scheme



Realistic situation

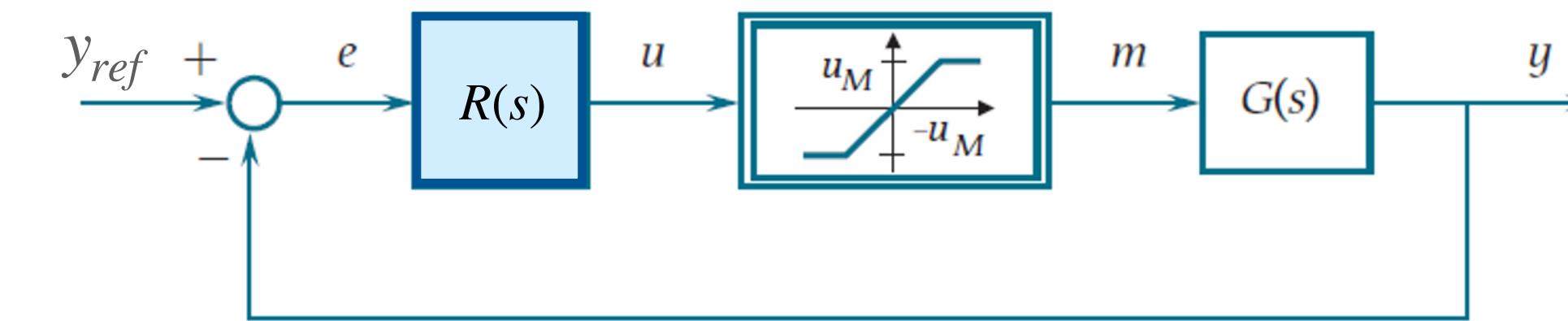


PID Controllers: Wind-up Effect

Generic integral controller

$$R(s) = \frac{N_R(s)}{D_R(s)}, \quad D_R(0) = 0$$

Realistic situation

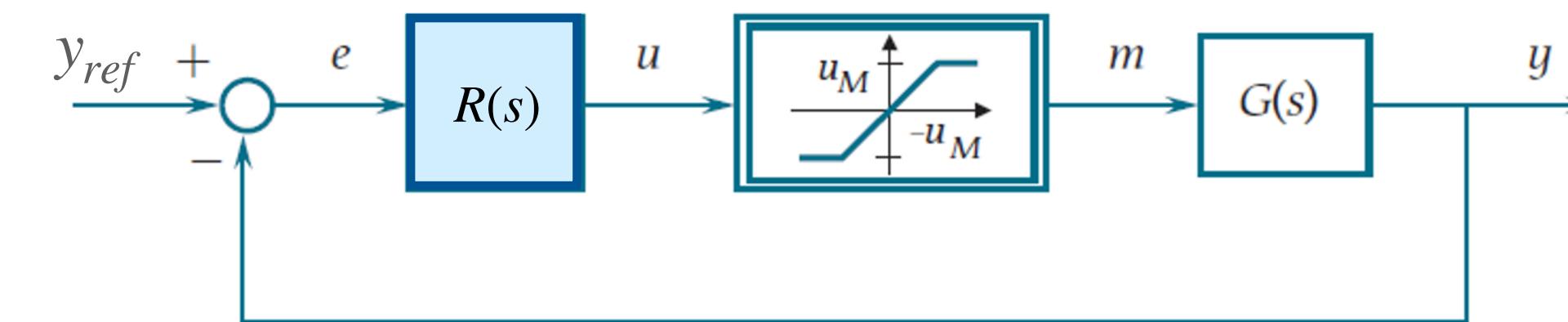


PID Controllers: Wind-up Effect

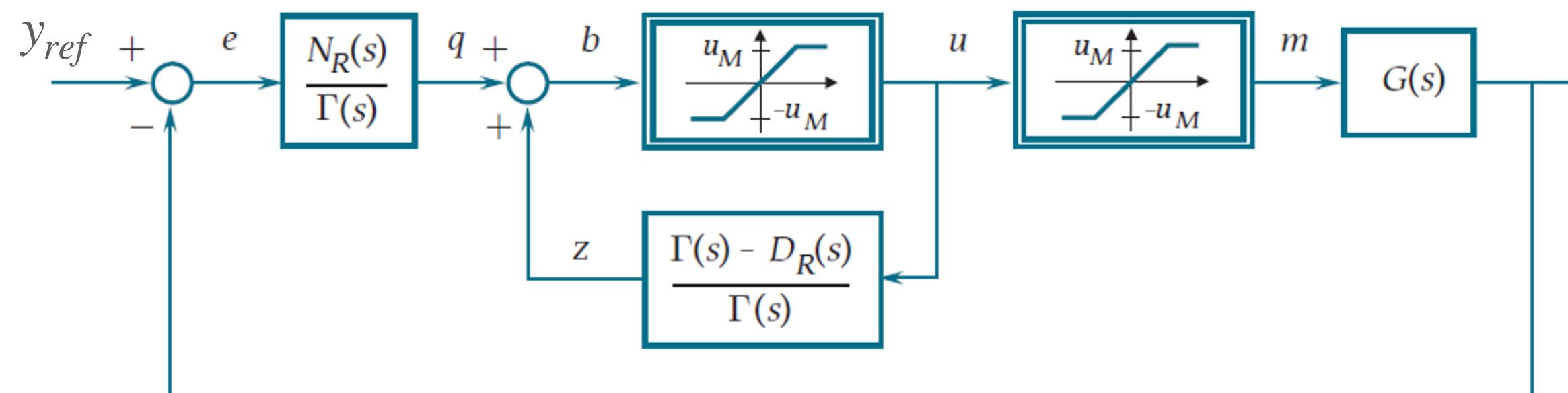
Generic integral controller

$$R(s) = \frac{N_R(s)}{D_R(s)}, \quad D_R(0) = 0$$

Realistic situation



Solution: Anti-wind-up scheme for generic integral controller

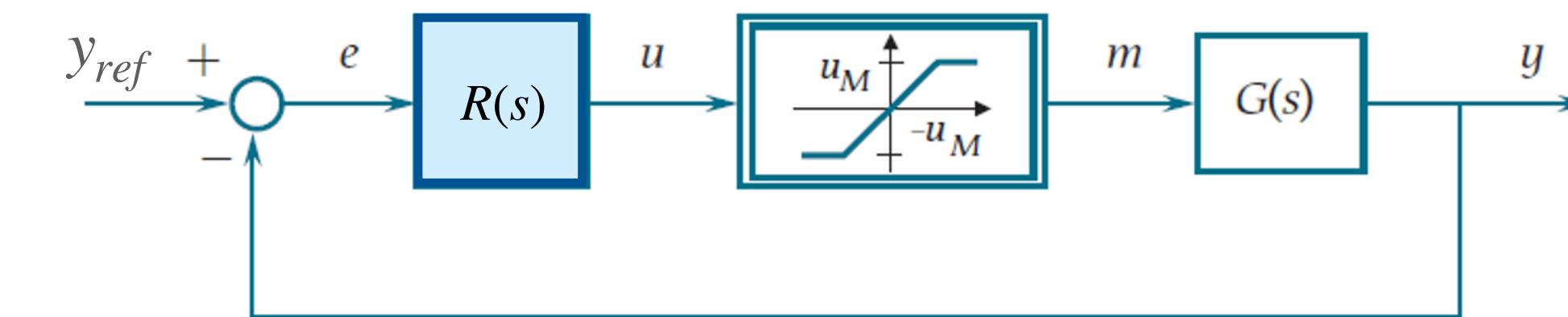


PID Controllers: Wind-up Effect

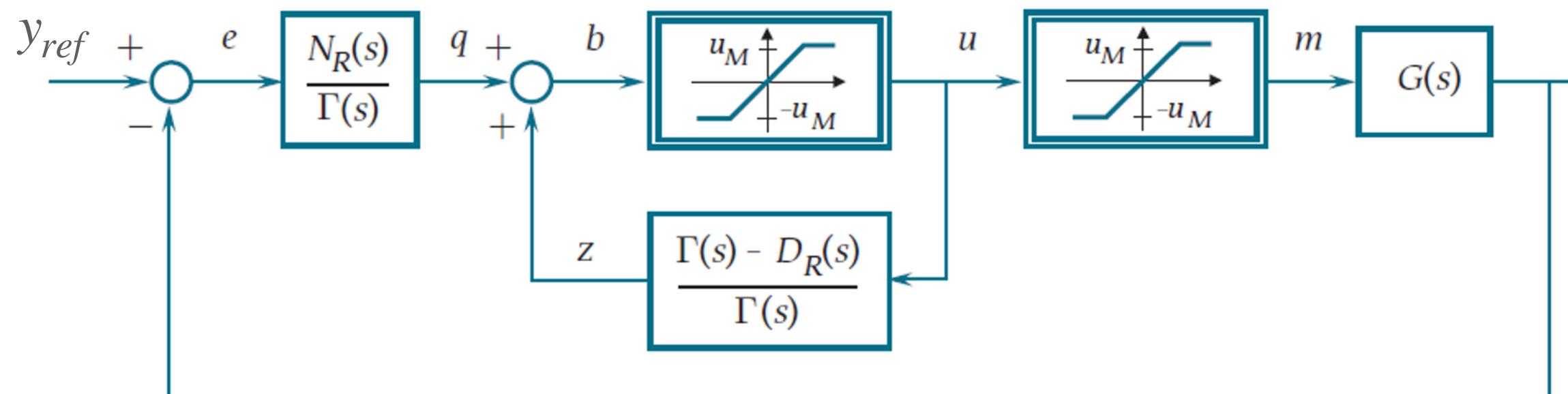
Generic integral controller

$$R(s) = \frac{N_R(s)}{D_R(s)}, \quad D_R(0) = 0$$

Realistic situation



Solution: Anti-wind-up scheme for generic integral controller



Alternative (accessible signal downstream of saturation)

