

$$\textcircled{b} \text{ COP}_H = \frac{\dot{Q}_H}{\dot{W}}$$

The following simplification can be used in the case of reversible heat pumps

$$\text{COP}_{H, \text{rev}} = \frac{T_H}{T_H - T_L}$$

$$\text{COP}_{H, \text{rev}} = \frac{297.15 \text{ K}}{297.15 \text{ K} - 280.15 \text{ K}}$$

$$\text{COP}_{H, \text{rev}} = 17.479$$

Then, input power needed for the heat pump is:

$$\dot{W} = \frac{\dot{Q}}{\text{COP}_{H, \text{rev}}}$$

$$\dot{W} = \frac{300 \text{ kW}}{17.479}$$

$$\dot{W} = 16.902 \text{ kW}$$

By 1<sup>st</sup> law of Thermodynamics, heat pump works at steady state and likewise heat released:

$$-\dot{Q}_H + \dot{W} + \dot{Q}_L = 0$$

$$\dot{Q}_L = \dot{Q}_H - \dot{W}$$

$$\dot{Q}_L = 300 \text{ kW} - 16.902 \text{ kW}$$

$$\dot{Q}_L = 283.098 \text{ kW}$$

from second law of thermodynamics, a rev. heat pump should have an entropy

generation rate equal to zero.

The second law for this;

$$\dot{S}_{in} - \dot{S}_{out} - \dot{S}_{gen} = 0$$

$$\dot{S}_{gen} = \dot{S}_{in} - \dot{S}_{out}$$

$$\dot{S}_{gen} = \frac{\dot{Q}_L}{T_L} - \frac{\dot{Q}_H}{T_H}$$

$$\dot{S}_{gen} = \frac{283.098 \text{ kW}}{280.15 \text{ K}} - \frac{300 \text{ kW}}{297.15 \text{ K}}$$

$$\dot{S}_{gen} = 9.318 \times 10^{-4} \text{ kW/K}$$

Albeit entropy generation rate is positive

(20)

from steam tables

At 2 MPa and 360°C

Interpolating b/w 350°C and 400°C

$$h_1 = 3137.7 + \frac{360 - 350}{400 - 350} \times [3248.4 - 3137.7]$$

$$h_1 = 3159.84 \text{ KJ/kg}$$

$$s_1 = 6.9583 + \frac{360 - 350}{400 - 350} \times [7.1292 - 6.9583]$$

$$s_1 = 6.99248 \text{ KJ/kg K}$$

It is a isentropic process so entropy remains constant  $s_1 = s_2$

At 100 kPa

$$s_f = 1.3028 \text{ KJ/kg K}$$

$$s_{fg} = 6.0562 \text{ KJ/kg K}$$

$$h_f = 417.51 \text{ KJ/kg}$$

$$h_{fg} = 2257.5 \text{ KJ/kg}$$

$$s_1 = s_2 = s_f + n s_{fg}$$

$$6.99248 = 1.3028 + n \times 6.0562$$

$$\eta = 0.93948$$

$$h_2 = h_f + \eta h_{fg}$$

$$h_2 = 417.51 + 0.93948 \times 2257.5$$

$$h_2 = 2538.3861 \text{ kJ/kg}$$

work produced  $w = h_1 - h_2$

$$w = (3159.84 - 2538.3861)$$

$$w = 621.4539 \text{ kJ/kg}$$

3) part (a)

$$T_{\text{Sat}} \rightarrow 140 \text{ kPa} = -18.77^\circ\text{C} \rightarrow 254.18 \text{ K}$$

we make a conversion  $^\circ\text{C} \rightarrow ^\circ\text{K}$

$$K = 273 + (-18.77^\circ\text{C}) \rightarrow 254.23 \text{ K}$$

the entropy change of cooled space

$$\Delta S_{\text{refrigerant}} = \frac{Q_{\text{in}}}{T_{\text{refrigerant}}}$$

we replace the values in the equation

$$\begin{aligned} \Delta S_{\text{refrigerant}} &= \frac{180 \text{ kJ}}{254.23 \text{ K}} \rightarrow \Delta S_{\text{refrigerant}} \\ &= 0.70754 \text{ kJ/K} \end{aligned}$$

part (b)

the entropy change of the cooled space

$$\Delta S_{\text{space}} = - \frac{Q_{\text{out}}}{T_{\text{space}}}$$

we replace the values in the equation

$$\Delta S_{\text{space}} = -\frac{180 \text{ KJ}}{262 \text{ K}} \rightarrow \Delta S_{\text{space}} = -0.6844 \frac{\text{KJ}}{\text{K}}$$

part (c)

the total entropy change for this process

$$\Delta S_{\text{total}} = \Delta S_{\text{refrid.}} + \Delta S_{\text{space}}$$

we replace the values in the eq<sup>n</sup>

$$\Delta S_{\text{total}} = 0.70754 \frac{\text{KJ}}{\text{K}} - 0.6844 \frac{\text{KJ}}{\text{K}}$$

$$\Rightarrow \Delta S_{\text{total}} = 0.02314 \text{ KJ/K}$$