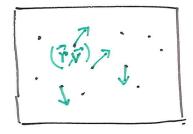
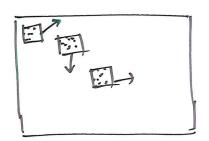
Plasma is a complex medium consisting of electrons, ions and neutrals which moves under the influence of electric, magnetic and collisional forces. To understand plasma and its basis of dynamics, we'll look into classical continuum mechanics for neutral fluid and gases.

For single particls: VECTOR QUANTITIES (7, V, F)

For Continuum Models: VECTOR AND SCALAR FIELDS
Instead of tracking individual particles, we study
fields which represent an ensamble of particles.



SINGLE



CONTINUUM/ FLUID

Space.

For continuum model, we'll consider density (P) instead of mass (m) unlike the single particle motion.

CHANGE IN DENSITY (P(r,t))

$$\overrightarrow{P}P = \left(\frac{\partial}{\partial x} \widehat{X} + \frac{\partial}{\partial y} \widehat{Y} + \frac{\partial}{\partial z} \widehat{z}\right) P$$

$$SPACE$$

RECALLING GAUSS THEOREM (DIVERGENCE THEOREM)

$$\int \int \overline{\nabla} \cdot \overline{u} \, dV = \iint \overline{u} \cdot \hat{n} \, dS$$

$$V \qquad \text{Field vector} \qquad S \qquad \text{Surface normal}$$

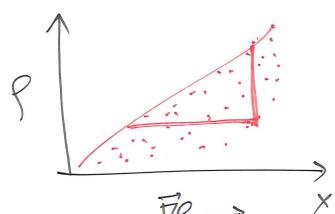
GAUSS LAW IN ELECTROSTATICS

$$\int \vec{E} \cdot d\vec{\zeta} = \frac{Q}{\epsilon_0}$$

$$\frac{1}{1} = \frac{1}{1} = \frac{1}$$

## DENSITY FIELD (GENERAL FLUID)

IN In:



DISCRETE APPROACH 1 is large.

Density Variation:

$$P(x+\Delta x) - P(x) = \Delta P$$

$$\Delta P > 0 \quad \text{or} \quad \Delta P < 0$$

For a stationary case where we only have spalial gradient.

2) Dynamic density (density moving)

$$V = \frac{3x}{4t}$$
Velocity
field
(Fluid flow)

FIXED POINT OBSERVER OR

LABORATORY FRAME OF REFERENCE

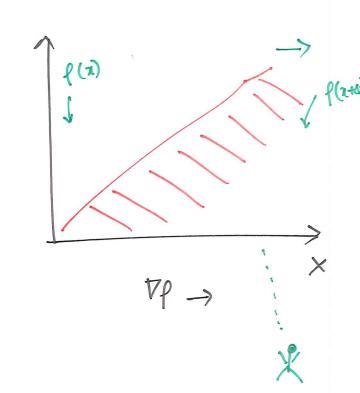
OR

STANDING OBSERVER

The observer will see - Ap in time

$$\frac{\Delta p}{\Delta t} = -u \frac{\Delta p}{\Delta x}$$

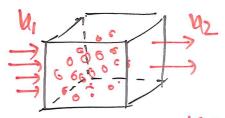
$$= \dot{\rho} = \dot{\rho} = -u \frac{\partial \rho}{\partial x}$$



FOR SITUATIONS WHEN WE HAVE CHANGE IN VELOCITY

ie. Pu to

means more parkele packed that together over time that together compressibility.



4>12

if more incoming flow them outgoing. there will be increase in density over time. NOTE: For compressibility, we need not to have  $\nabla f$ . Only  $\nabla u \neq 0$  should be enough.

$$u(x+\Delta x)-u(x)=\Delta u$$

For a fixed observer, du <0

$$\frac{\Delta \rho}{\Delta t} = -\rho \frac{\Delta u}{\Delta x} \qquad \text{conservation}$$

REMEMBER! For a fixed observer, (incoming field - outgoing field) to decide the sign.

#### CONSERVATION OF MASS IN ID

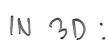
$$M = \rho \Delta x \qquad \Delta (\rho \Delta x) = (\rho u_{in} - \rho v_{out}) \Delta t$$

$$= \frac{\Delta \rho}{\Delta t} = -\rho \frac{\Delta u}{\Delta x}$$

IN GENERAL,

$$\frac{\partial P}{\partial t} = -\frac{\partial}{\partial x} (P u)$$

11× 13/0/2



CONTINUITY EQN:

$$\frac{\partial}{\partial t} + \nabla \cdot (\vec{u} + \vec{r}) = 0$$
 density is equal to: total change in massflux in space.

MOISS flux

men production or When there is

> Change in mass density is equal massflux in space.

> > Divergence of mass flux.

TAKING Volume integral = ) muss conservation.

#### MOVING OBSERVER :

$$\frac{D}{Dt} = \frac{3}{3t} + \vec{u} \cdot \vec{\nabla}$$

Convective derivative

The variation in the flow due to Convection.

$$\frac{1}{2} = -\rho \vec{\nabla} \cdot \vec{u}$$

compresibility

Change in time movement of the system

### IF FLUID IS INCOMPRESSIBLE

$$\frac{D}{Dt} P = 0$$

FOR A COMOVING OBJERVER NO DENSITY GRADIENT.

TO EXPANSION OR COMPRESSION OF THE FLUID.

IF PRODUCTION OR LOSS

$$\frac{\partial}{\partial t} P + \overrightarrow{P} \cdot (\overrightarrow{u}P) = \angle - B$$

Production loss

For Plasma, (charge continuity)

$$\frac{\partial}{\partial t}(q.n) + P.\vec{J} = 0 \qquad \vec{J} = qn\vec{u}$$

FIXED POINT OBSERVER — ) EULERIAN APPROACHI
COMOVING OBSERVER — ) LAGRANGIAN APPROACH

NEWTON'S SELOND LAW \_\_\_\_ FOR SINGLE PARTICLE

$$m\vec{a} = \vec{F} = m \frac{d\vec{V}}{dt} \rightarrow velou'y$$

$$U = U (\overline{Y}, t)$$
 time

Function of time only

IN FLUID,

Velocity -> velocity field mass -> mass density field

Force density
$$\vec{f} = \frac{\vec{F}}{V} \quad \text{Force per volume}$$

This is valid if  $\vec{u}$  is const./homogeneous at t=0

LANGBANGIAN

CONSIDERING CHANGE IN MOMENTUM IN A SMALL VOLUME

$$\frac{d}{dt} \int P \vec{u} d\vec{r} = - \oint P \vec{u} \vec{u} \cdot \hat{n} dS + \int \vec{f} d\vec{r}$$

$$= \int_{V} \left[ \frac{\partial}{\partial t} (P\vec{u}) + \nabla \cdot P \vec{u} \vec{u} \right] d\vec{r}$$

$$= \int \left[ \overrightarrow{u} \frac{\partial}{\partial +} \rho + \rho \frac{\partial}{\partial t} \overrightarrow{u} + \nabla (\rho \overrightarrow{u}) \overrightarrow{u} + (\rho \overrightarrow{u}) \cdot (\rho \overrightarrow{u}) \right] d\overrightarrow{r}$$

(ONTINUITY EQN -) For mo production or loss -) O

$$= \int \left[ \int \frac{\partial \vec{u}}{\partial t} + (\int \vec{u}) \cdot \nabla \vec{u} \right] d\vec{r}$$

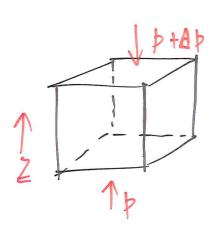
$$= \int \int \int \int \frac{d\vec{r}}{d\vec{r}} d\vec{r} + \vec{u} \cdot \nabla \vec{u} d\vec{r} = \int \int \frac{d\vec{r}}{d\vec{r}} d\vec{r}$$

AT THE POINT, WE HAVE TWO EQNS AND THREE UNKNOWNS (P, U, T)

$$\vec{f} = -\vec{\nabla} \vec{p}$$

$$\frac{F}{A \cdot az} = -\frac{4b}{4z} = -\overline{\nabla} p$$

$$=$$
)  $f = -\overrightarrow{p}p$ 



# RELEVANT FORM OF MOMENTUM EQN FOR FLUID

$$\int \left(\frac{\partial}{\partial t} \vec{u} + \vec{u} \cdot \vec{\nabla} \vec{u}^{T}\right) = -\nabla p + M \nabla^{T} \vec{u}^{T} + f$$
pressure viscosity

NEXT -> EQN OF STATE