

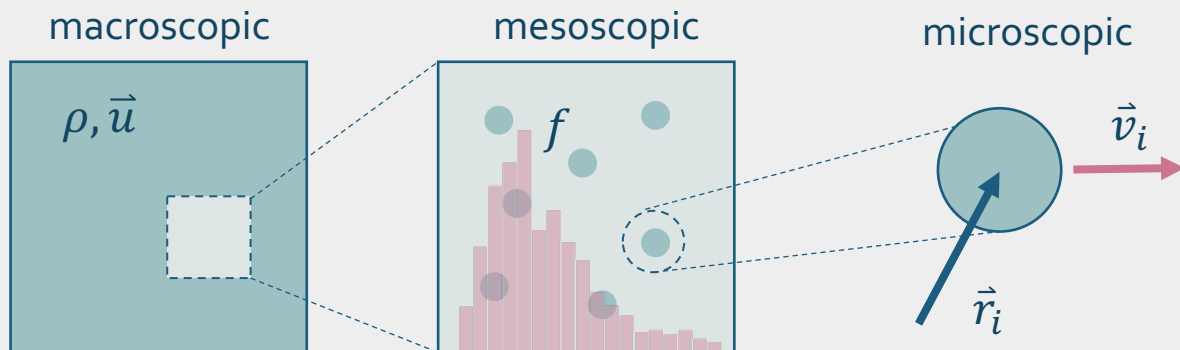
# Lattice Boltzmann Method

Rycroft Group Journal Club

Oct. 25, 2018

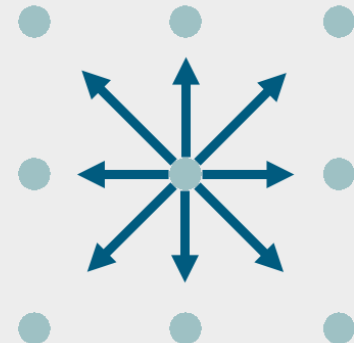
# Overview of lattice Boltzmann methods for fluids

- Replace a discretization of *macroscopic* continuum equations with a *mesoscopic* particle description which borrows from kinetic theory of gases
- Moments of particle distribution functions give back the macroscopic quantities such as density, velocity, etc.
- Particle transport governed by a discretized Boltzmann equation



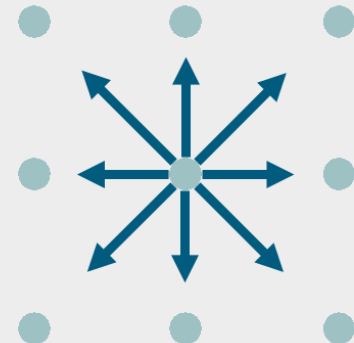
# Advantages

- Simpler and more efficient for multiphase/multicomponent flows, complex obstacles and boundaries, and inhomogeneous media than other approaches
- Highly parallelizable
- Interactions are local, which helps in managing memory constraints
- Not limited to fluids



# Challenges

- By design, limited to low Mach number flows
- Larger number of variables to keep track of
- Higher complexity required for methods beyond 2<sup>nd</sup> order accuracy

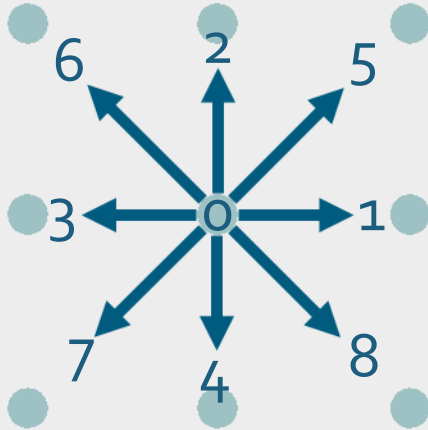


# From Boltzmann to Lattice Boltzmann



\*From Dr. Federico Toschi's lectures, courtesy of Vamsi

# 9-Bit Model



$\vec{e}_\alpha$	$e_x = -c$	$e_x = 0$	$e_x = c$
$e_y = c$	$(-c, c)$	$(0, c)$	$(c, c)$
$e_y = 0$	$(-c, 0)$	$(0, 0)$	$(c, 0)$
$e_y = -c$	$(-c, -c)$	$(0, -c)$	$(c, -c)$

$w_\alpha$			
	$\frac{\pi}{36}$	$\frac{\pi}{9}$	$\frac{\pi}{36}$
	$\frac{\pi}{9}$	$\frac{4\pi}{9}$	$\frac{\pi}{9}$
	$\frac{\pi}{36}$	$\frac{\pi}{9}$	$\frac{\pi}{36}$

# Simulation steps

1. If  $t = 0$ , initialize  $\rho, \vec{u}$  at grid points; otherwise compute from current  $f_\alpha$ 's
2. Apply boundary conditions to populate missing  $f_\alpha$ 's at boundaries
3. Compute equilibrium particle distributions  $f_\alpha^{eq}(\vec{r}_{ij}, t_n)$

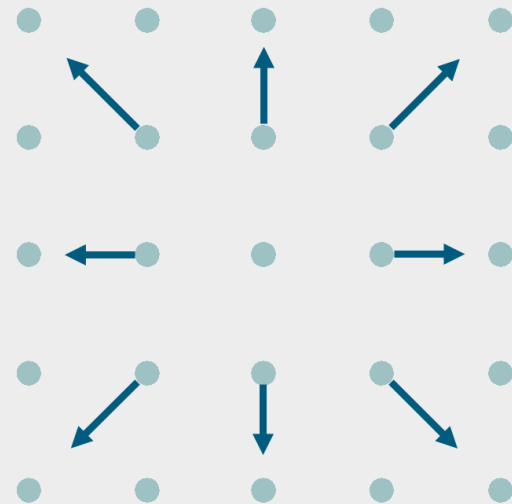
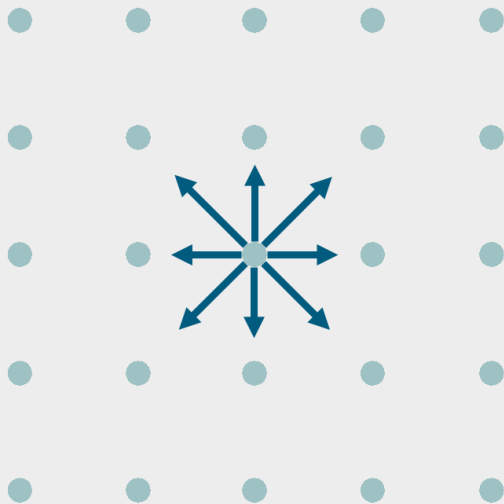
# Simulation steps

## 4. Collision step

$$f_{\alpha}^{+}(\vec{r}_{ij}, t_n) = f_{\alpha}(\vec{r}_{ij}, t_n) - \frac{1}{\tau} \left( f_{\alpha}(\vec{r}_{ij}, t_n) - f_{\alpha}^{eq}(\vec{r}_{ij}, t_n) \right)$$

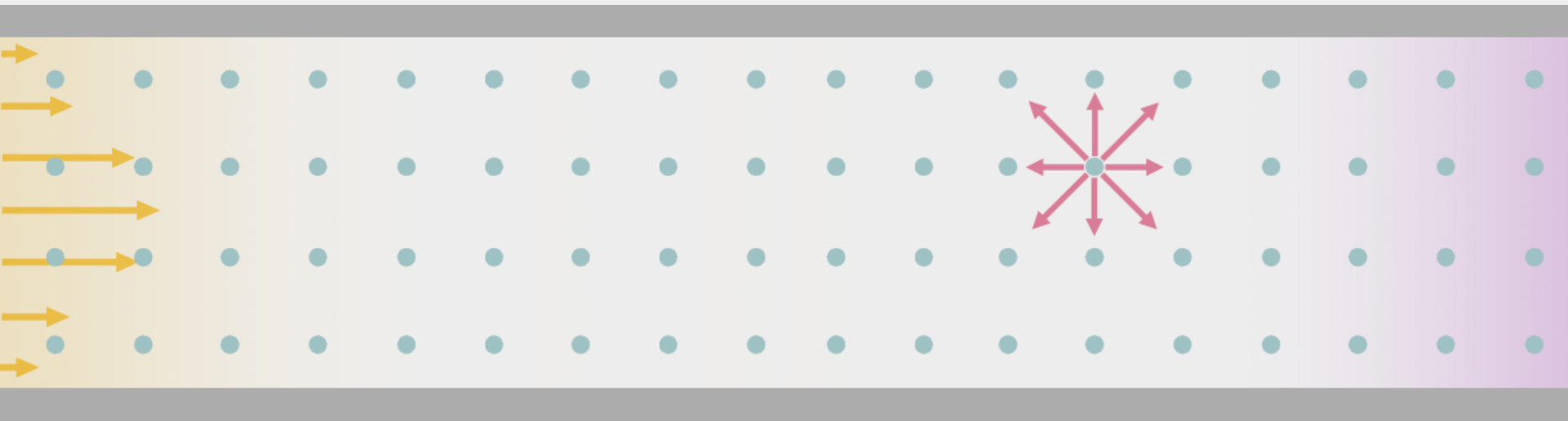
## 5. Streaming step

$$f_{\alpha}(\vec{r}_{ij} + \vec{e}_{\alpha} \delta_t, t_n + \delta_t) = f_{\alpha}^{+}(\vec{r}_{ij}, t_n)$$





# Boundary conditions



Constant velocity

$$\vec{u} = \mathbf{0}$$

Wall

$$\vec{u} = (u_x(y), 0)$$

Inlet with fixed  
velocity profile

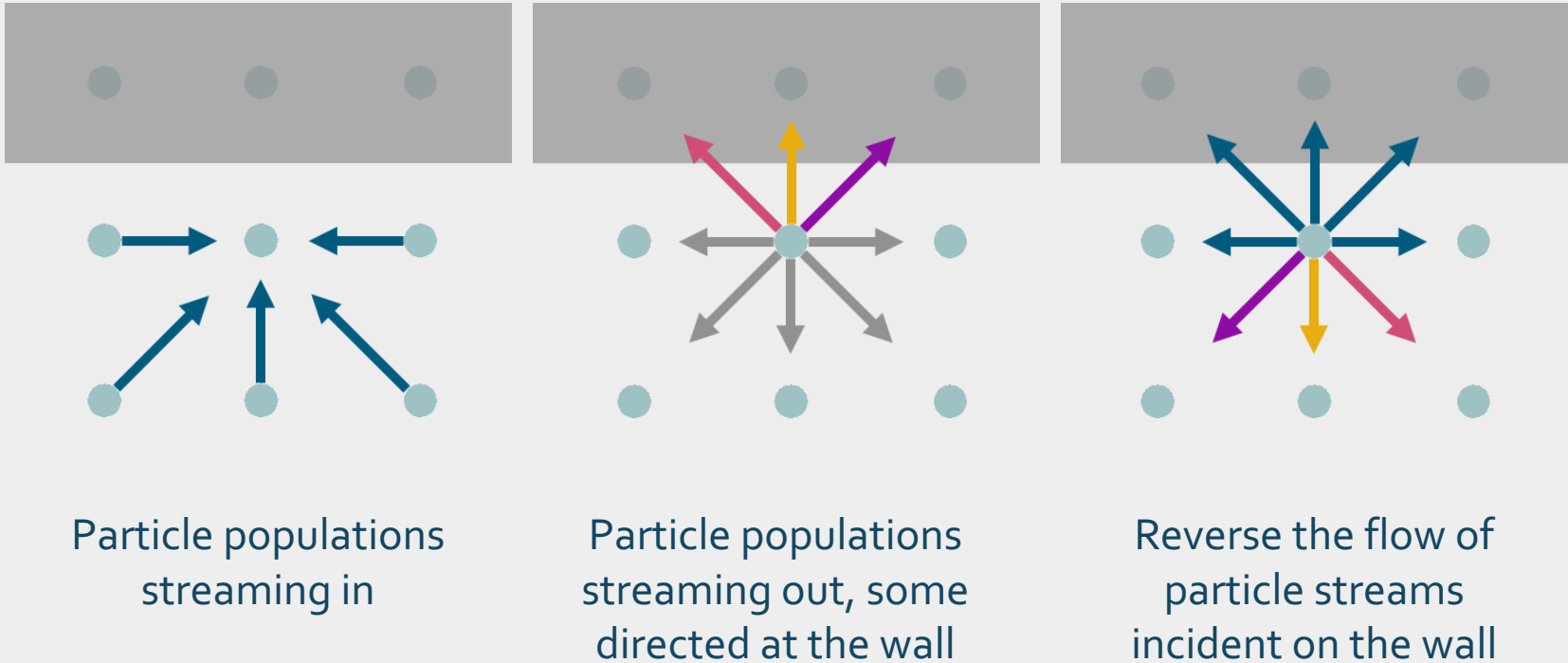
Constant density

$$\rho = \rho_o$$

Outlet with  
fixed pressure

$$\begin{aligned} &\rho(\vec{r}_{ij})u_y(\vec{r}_{ij}) \\ &= \rho(\vec{r}_{ij} \pm c\delta_t\hat{x})u_y(\vec{r}_{ij} \pm c\delta_t\hat{x}) \end{aligned}$$

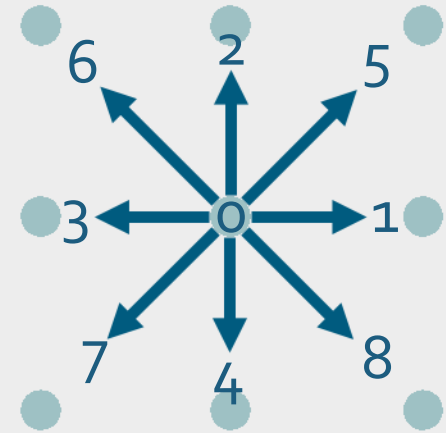
# Bounce-back



$$f_{\alpha}(\vec{r}_{ij}, t_n) = f_{-\alpha}^+(\vec{r}_{ij}, t_n - \delta_t)$$

# Corrector vector

$$f_{\alpha}(\vec{r}_{ij}, t_n) = f^* + \frac{w_{\alpha}}{c} \vec{e}_{\alpha} \cdot \vec{Q}$$



Conserved quantities

$$\rho = f_0 + f_1 + f_2 + f_3 + f_4 + f_5 + f_6 + f_7 + f_8$$

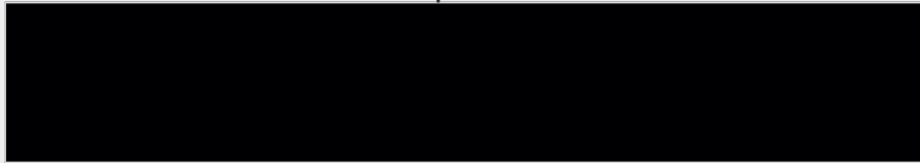
$$u_x = \frac{c}{\rho} (f_1 - f_3 + f_5 - f_6 - f_7 + f_8)$$

$$u_y = \frac{c}{\rho} (f_2 - f_4 + f_5 + f_6 - f_7 - f_8)$$

Zou-He:  $f^* = f_{-\alpha}(\vec{r}_{ij}, t_n)$

# Poiseuille Flow

Speed



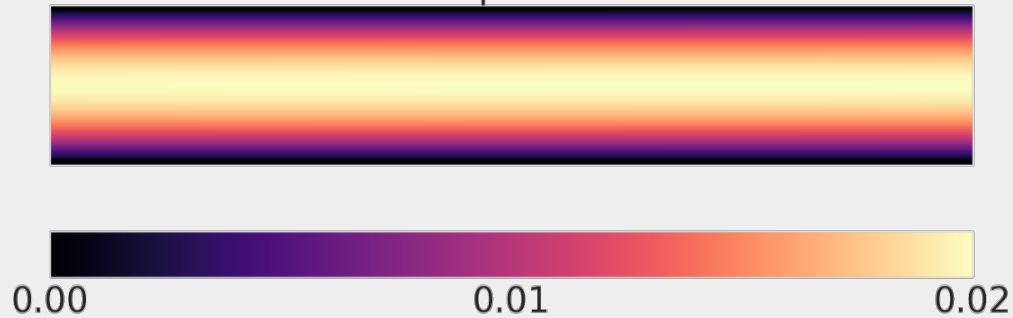
Density



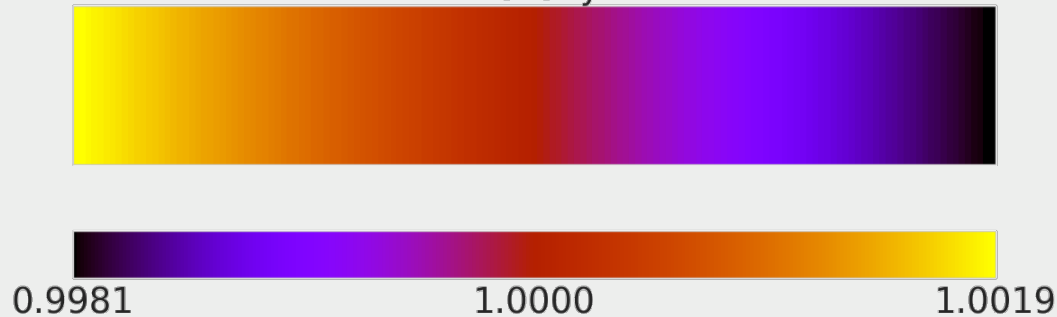
$$\begin{array}{lll} n_x = 151 & n_y = 26 & \text{Re} = 10 \\ L_x = 150 & L_y = 25 & \tau = 0.6 \end{array}$$

# Poiseuille Flow

Speed



Density



$$n_x = 151$$

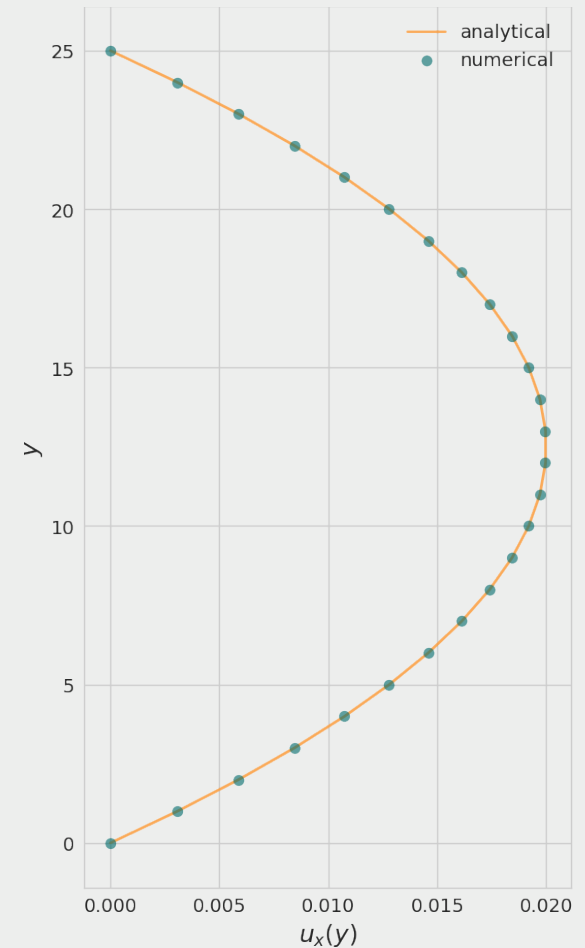
$$n_y = 26$$

$$\text{Re} = 10$$

$$L_x = 150$$

$$L_y = 25$$

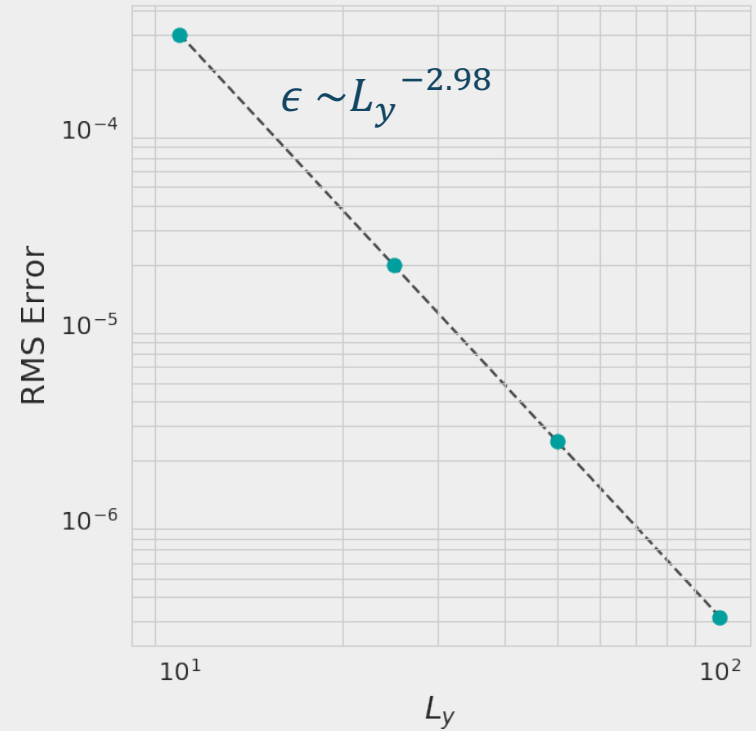
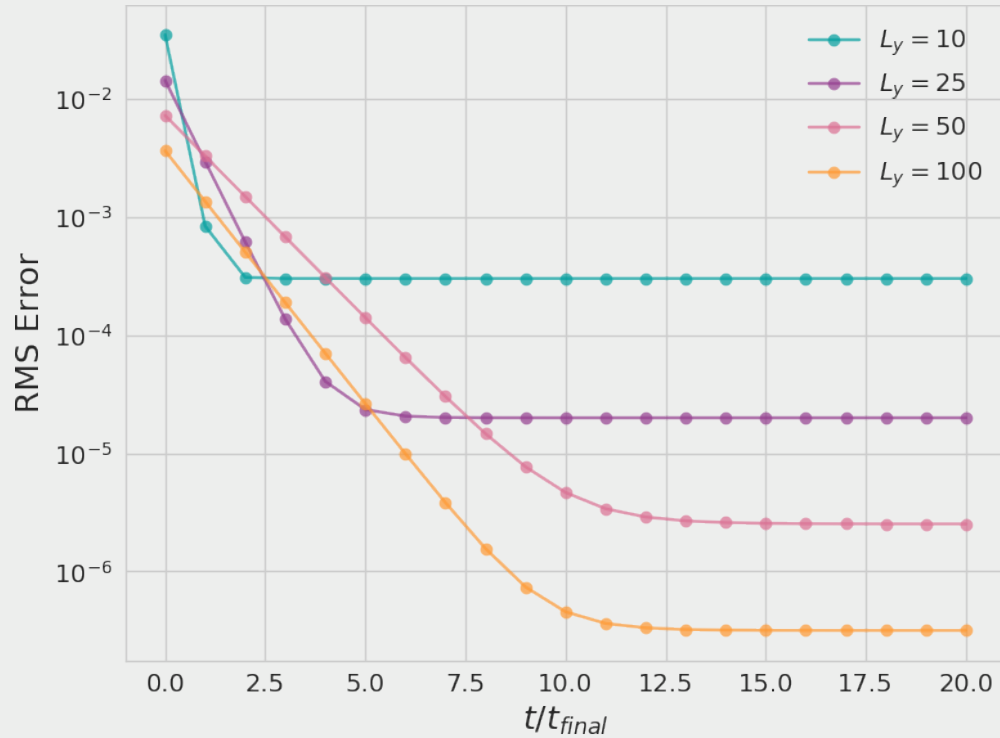
$$\tau = 0.6$$



$$u_x(y) = \frac{6 \text{ Re } \nu}{L_y} y(1 - y)$$

# Poiseuille Flow

Convergence with varying grid resolution



$Re = 10$   
 $\tau = 0.6$

RMS Error: 
$$\epsilon = \sqrt{\frac{1}{n_x n_y} \sum_{i=1}^{n_x n_y} \|\vec{u}_{num} - \vec{u}_{ana}\|^2}$$

# Flow past a cylinder

$$\begin{array}{ll} n_x = 601 & n_y = 101 \\ L_x = 600 & L_y = 100 \end{array}$$

$$\begin{array}{l} \text{Re} = 80 \\ \tau = 0.6 \end{array}$$

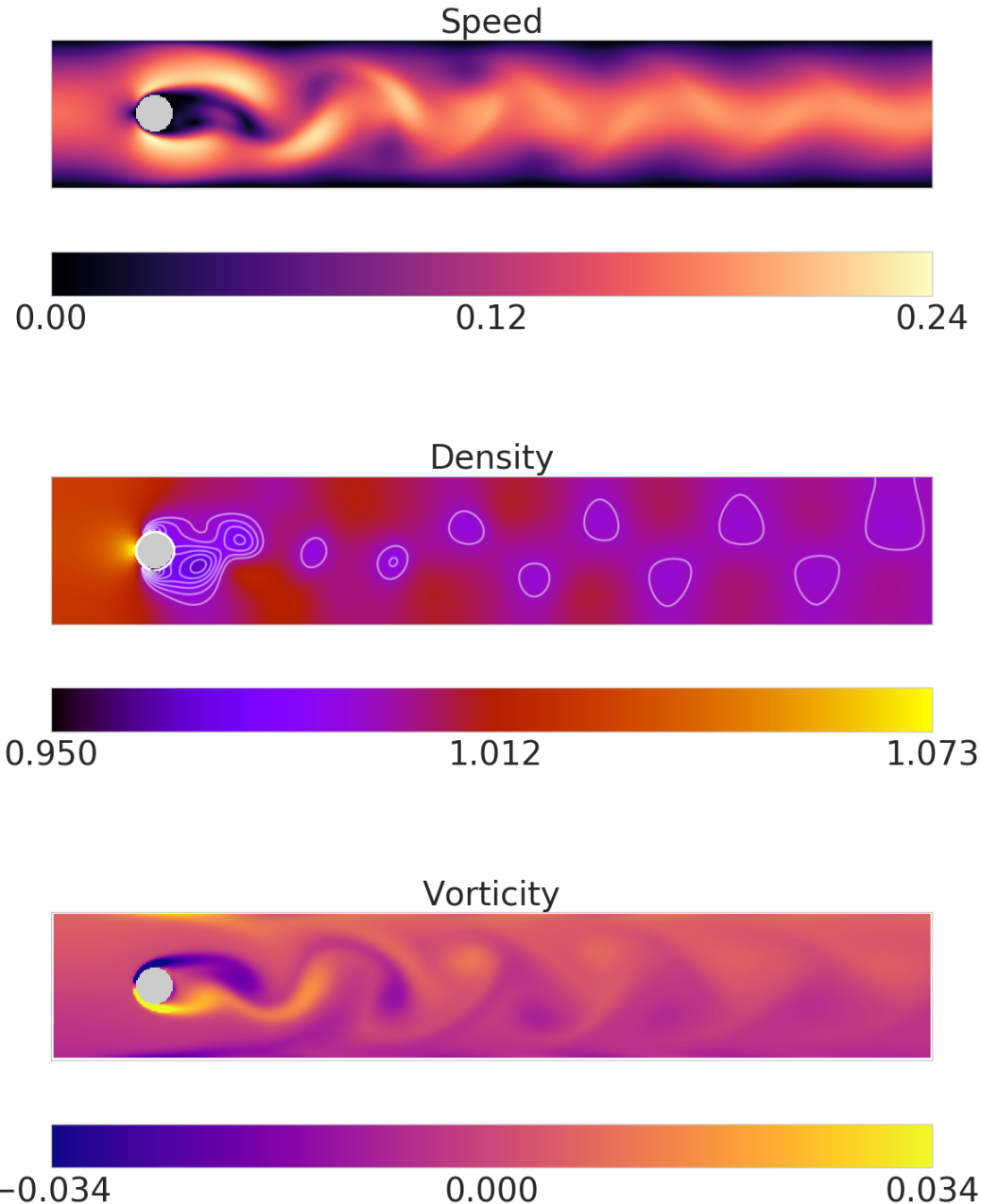
## Boundary conditions

- Inlet: steady state Poiseuille velocity profile
- Outlet: constant density
- Walls and cylinder: zero velocity

## Completing $f_\alpha$ 's

- Inlet/Outlet/Walls: Zou-He
- Cylinder: Bounce-back

(see movies folder)



# Flow past airfoil

$$\begin{aligned} n_x &= 1201 & n_y &= 301 \\ L_x &= 1200 & L_y &= 300 \end{aligned}$$

$$\begin{aligned} \text{Re} &= 600 \\ \tau &= 0.6 \end{aligned}$$

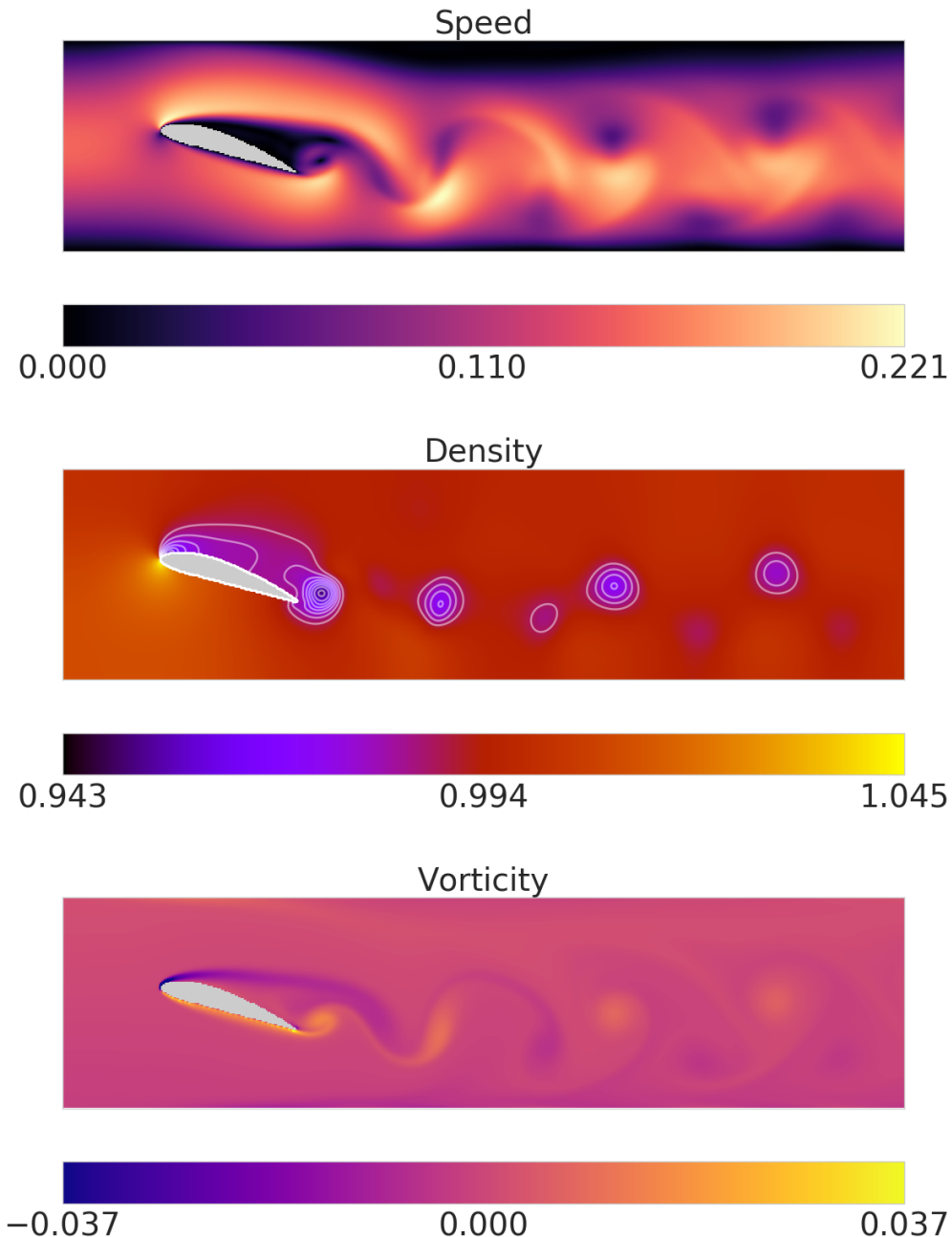
## Boundary conditions

- Inlet: steady state Poiseuille velocity profile
- Outlet: constant density
- Walls and cylinder: zero velocity

## Completing $f_\alpha$ 's

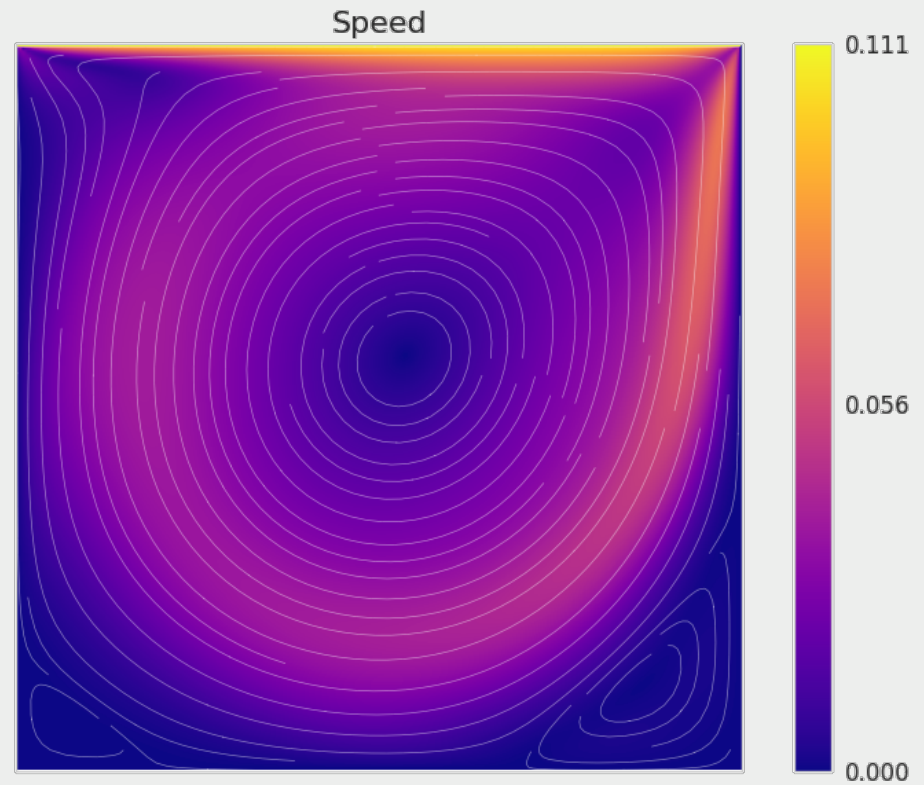
- Inlet/Outlet/Walls: Zou-He
- Airfoil: Bounce-back

(see movies folder)

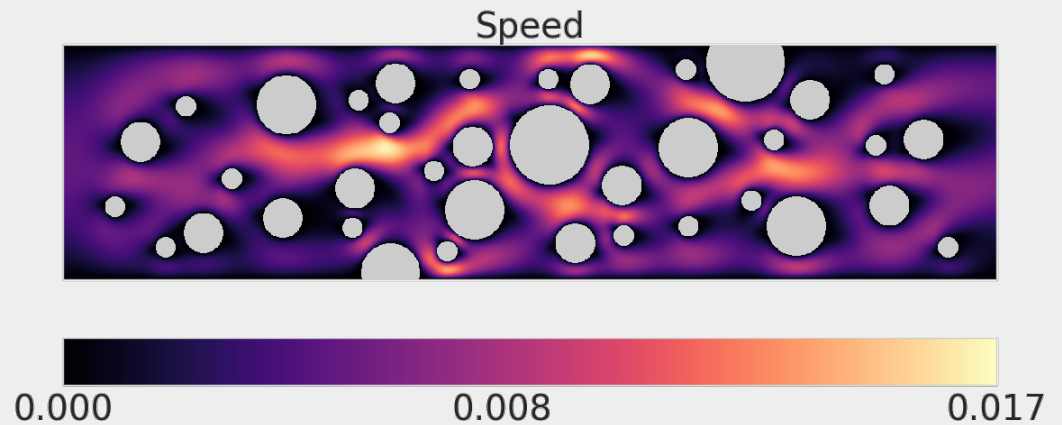




Lid-driven  
cavity flow



Flow through a  
porous medium



# References

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