

## 3.1 Description of the case

The second tutorial is based on the analysis of external flow. More specifically, the study encompasses the modelling of a bidimensional laminar flow around a circular cylinder. The analytical solution of the same case modeled with potential flow is known and easy to interpret; however the physical mechanism which rules real flow around a circular cylinder as well as its mathematical treatment are highly complex. Some examples are the boundary layer detachment and oscillatory effects that without a CFD study would be very difficult to determine either analytically or experimentally. The case includes simulations made with two different Reynolds numbers to observe the behaviour of the flow in such different regimes.

## 3.2 Hypotheses

- Incompressible flow
- Laminar flow
- Newtonian flow
- Bidimensional flow  $(\frac{\partial}{\partial z} = 0)$
- Negligible gravitatory effects

## 3.3 Physics of the problem

The problem encompasses a circular cylinder with a diameter of D=0.1 m submerged in a stream with an undisturbed speed of V=5 m/s and ambient pressure. The problem statement is shown at Figure 3.1.



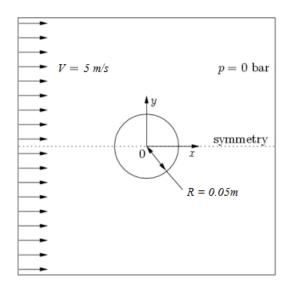


Figure 3.1: Flow around a circular cylinder

Unlike Chapter 2, in the current chapter there is no easy analytical solution to describe the behaviour of the fluid (except for potential flow, which is an ideal case). However, it is necessary to keep in mind the main equations and dimensionless numbers involved in the problem:

The continuity equation,

$$\nabla \cdot \mathbf{U} = 0 \tag{3.1}$$

The momentum equation,

$$\frac{\partial \mathbf{U}}{\partial t} + \mathbf{U} \cdot \nabla \mathbf{U} = -\frac{1}{\rho} \nabla p + \frac{\mu}{\rho} \nabla^2 \mathbf{U}$$
 (3.2)

The Reynolds number,

$$Re = \frac{D|\mathbf{U}|}{\nu} \tag{3.3}$$

The Strouhal number (which describes oscillating flow mechanisms),

$$St = \frac{wD}{2\pi |\mathbf{U}|} \tag{3.4}$$

The drag coefficient (dimensionless force parallel to the flow),

$$C_D = \frac{F_D}{\frac{1}{2}\rho |\mathbf{U}|^2 S} \tag{3.5}$$

The behaviour of the flow around a circular cylinder is very complex and highly de-



pendent on the Reynolds number. The boundary layer in laminar regimes detaches at an angle of  $\theta=82^{\rm o}$  as a consequence of the existence of an adverse pressure gradient. Furthermore, due to the symmetry of the cylinder, a curious phenomenon appears named  $von~K\'{a}rm\'{a}n~street$ , consisting of alternate vortices emitted by the cylinder. The vortices are detached periodically and their frequence is directly related to the Strouhal number.

For external flow, the transition from laminar regime to turbulent regime occurs at  $Re \approx 3 \times 10^5$ . However, the very complex structure of vortex shedding deserves special mention; the relation between the behaviour of the flow and the Reynolds number is shown at Figure 3.2:

	No separation. Creeping flow	Re < 5
-08>	A fixed pair of symmetric vortices	5 < Re < 40
-033	Laminar vortex street	40 < Re < 200
-033	Transition to turbulence in the wake	200 < Re < 300
-	Wake completely turbulent. A:Laminar boundary layer separation	300 < Re < 3×10 <sup>5</sup> Subcritical

Figure 3.2: Flow structure depending on the Reynolds number, extracted from [2]

As the simulation is going to be run with laminar flow, the Reynolds number is not going to be set higher than 195. This will allow to observe the von Kármán street and its transition while guaranteeing that the whole fluid domain remains laminar. Additionally, another simulation with Re = 30 will be run to check if the results of the CFD simulation adapt to the scheme shown at Figure 3.2.

The drag coefficient is a function of the Reynolds number and decreases when the regime turns to turbulent. It can be seen at Figure 3.3.



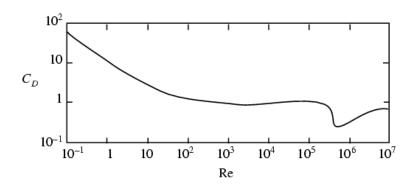


Figure 3.3: Drag coefficient as a function of the Reynolds number in an infinite circular cylinder

## 3.4 Pre-processing with Re = 195

The following codes contain the information to simulate the cylinder with Re = 195 using icoFoam. The case directory is named cylinder195 and will be located within FoamCases. Its structure of directories and subdirectories is very similar to the one used in Chapter 2.

## 3.4.1 Mesh generation

The mesh for the study of the cylinder is not going to be uniform. Some areas of the domain need to contain a higher cell density (mainly the walls of the cylinder and its prolongation). Consequently, it is necessary to divide the domain in different blocks as Figure 3.4 shows.

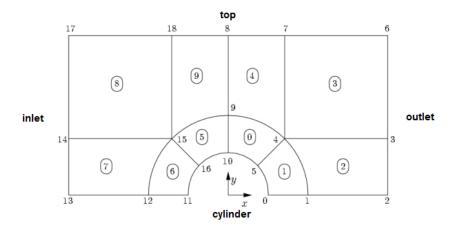


Figure 3.4: Half of the scheme used for the creation of the mesh, extracted from [1]

In Figure 3.4 there is only half of the mesh, which is contained between z = -0.05 m and z = 0.05 m. The numbers indicate the numbering used for the vertices and the blocks in the blockMeshDict file.

In the bidimensional cylinder case, constant/blockMeshDict must contain the following instructions:

```
2
3
                      F ield
                                          OpenFOAM: The Open Source CFD Toolbox
                      O peration
                                          Version:
                                                      2.2.1
5
                      A nd
                                          Web:
                                                      www.OpenFOAM.org
6
                     M anipulation
7
8
      FoamFile
9
10
           version
                          2.0;
11
           format
                          ascii;
                          dictionary;
12
           class
           object
                          blockMeshDict;
13
14
15
16
      convertToMeters 0.1;
17
18
      vertices
19
20
          (0.5 \ 0 \ -0.5)
21
          (1 \ 0 \ -0.5)
22
          (10\ 0\ -0.5)
23
24
          (10\ 0.707107\ -0.5)
          (0.707107 \ 0.707107 \ -0.5)
25
26
          (0.353553 \ 0.353553 \ -0.5)
27
          (10\ 2\ -0.5)
          (0.707107 \ 2 \ -0.5)
28
          (0\ 2\ -0.5)
```



```
(0\ 1\ -0.5)
30
           (0 \ 0.5 \ -0.5)
31
32
           (-0.5 \ 0 \ -0.5)
33
           (-1 \ 0 \ -0.5)
34
           (-2 \ 0 \ -0.5)
35
           (-2 \ 0.707107 \ -0.5)
36
           (-0.707107 \ 0.707107 \ -0.5)
37
           (-0.353553 \ 0.353553 \ -0.5)
38
          (-2\ 2\ -0.5)
39
           (-0.707107 \ 2 \ -0.5)
40
41
           (0.5 \ 0 \ 0.5)
42
           (1 \ 0 \ 0.5)
43
           (10 \ 0 \ 0.5)
44
           (10\ 0.707107\ 0.5)
45
           (0.707107 \ 0.707107 \ 0.5)
46
           (0.353553 \ 0.353553 \ 0.5)
^{47}
           (10\ 2\ 0.5)
           (0.707107 \ 2 \ 0.5)
49
           (0\ 2\ 0.5)
51
           (0\ 1\ 0.5)
52
           (0 \ 0.5 \ 0.5)
53
          (-0.5 \ 0 \ 0.5)
54
           (-1 \ 0 \ 0.5)
55
          (-2 \ 0 \ 0.5)
56
          (-2 \ 0.707107 \ 0.5)
57
           (-0.707107 \ 0.707107 \ 0.5)
58
           (-0.353553 \ 0.353553 \ 0.5)
59
           (-2\ 2\ 0.5)
60
           (-0.707107 \ 2 \ 0.5)
61
62
63
           (10 -0.707107 -0.5)
64
            \begin{pmatrix} 0.707107 & -0.707107 & -0.5 \end{pmatrix} 
65
           (0.353553 -0.353553 -0.5)
66
67
           (10 -2 -0.5)
68
           (0.707107 -2 -0.5)
69
           (0 -2 -0.5)
70
           (0 -1 -0.5)
71
           (0 -0.5 -0.5)
72
           (-2 \quad -0.707107 \quad -0.5)
73
           (-0.707107 \ -0.707107 \ -0.5)
74
           (-0.353553 \ -0.353553 \ -0.5)
75
           (-2 \ -2 \ -0.5)
76
           (-0.707107 \ -2 \ -0.5)
77
78
           (10 -0.707107 0.5)
79
           (0.707107 -0.707107 0.5)
80
           (0.353553 -0.353553 \ 0.5)
81
           (10 -2 0.5)
82
           (0.707107 -2 0.5)
83
           (0 -2 0.5)
84
           (0 -1 0.5)
85
           (0 -0.5 0.5)
86
```



```
(-2 \ -0.707107 \ 0.5)
88
          (-0.707107 \ -0.707107 \ 0.5)
89
          (-0.353553 \ -0.353553 \ 0.5)
90
91
          (-2 \ -2 \ 0.5)
92
          (-0.707107 -2 0.5)
93
      );
94
      blocks
95
96
         hex (5 4 9 10 24 23 28 29) (80 20 1) simpleGrading (10 1 1)
97
          hex (0 1 4 5 19 20 23 24) (80 20 1) simpleGrading (10 1 1)
98
          hex (1 2 3 4 20 21 22 23) (200 20 1) simpleGrading (1 1 1)
99
          hex (4 3 6 7 23 22 25 26) (200 40 1) simpleGrading (1 1 1)
100
          hex (9 4 7 8 28 23 26 27) (20 40 1) simpleGrading (1 1 1)
101
102
          hex (16 10 9 15 35 29 28 34) (20 80 1) simpleGrading (1 10 1)
          hex (11 16 15 12 30 35 34 31) (20 80 1) simpleGrading (1 10 1)
103
          hex (12 15 14 13 31 34 33 32) (20 20 1) simpleGrading (1 1 1)
104
          hex (15 18 17 14 34 37 36 33) (40 20 1) simpleGrading (1 1 1)
105
          hex (9 8 18 15 28 27 37 34) (40 20 1) simpleGrading (1 1 1)
107
108
109
          hex (40 45 44 39 53 58 57 52) (20 80 1) simpleGrading (1 10 1)
          hex (0 40 39 1 19 53 52 20) (20 80 1) simpleGrading (1 10 1)
110
          hex (1 39 38 2 20 52 51 21) (20 200 1) simpleGrading (1 1 1)
111
          hex (39 42 41 38 52 55 54 51) (40 200 1) simpleGrading (1 1 1)
112
          hex (44 43 42 39 57 56 55 52) (40 20 1) simpleGrading (1 1 1)
113
          hex (48
                   47 44 45 61 60 57 58) (80 20 1) simpleGrading (10 1 1)
114
          hex (11 12 47 48 30 31 60 61) (80 20 1) simpleGrading (10 1 1)
115
          hex (12 13 46 47 31 32 59 60) (20 20 1) simpleGrading (1 1 1)
116
          hex (47 46 49 50 60 59 62 63) (20 40 1) simpleGrading (1 1 1)
117
           \text{hex } (44\ 47\ 50\ 43\ 57\ 60\ 63\ 56)\ (20\ 40\ 1)\ \text{simpleGrading}\ (1\ 1\ 1) 
118
119
      );
120
121
      edges
122
          arc 0 5 (0.469846 \ 0.17101 \ -0.5)
123
124
          arc 5 10 (0.17101 0.469846 -0.5)
          arc 1 4 (0.939693 \ 0.34202 \ -0.5)
125
          arc 4 9 (0.34202 0.939693 -0.5)
126
          arc 19 24 (0.469846 0.17101 0.5)
127
          arc 24 29 (0.17101 0.469846 0.5)
128
          arc 20 23 (0.939693 0.34202 0.5)
129
          arc 23 28 (0.34202 0.939693 0.5)
130
          arc 11 16 (-0.469846 \ 0.17101 \ -0.5)
131
          arc 16 10 (-0.17101 \ 0.469846 \ -0.5)
132
          arc 12 15 (-0.939693 \ 0.34202 \ -0.5)
133
          arc 15 9 (-0.34202 \ 0.939693 \ -0.5)
134
          arc 30 35 (-0.469846 \ 0.17101 \ 0.5)
135
          arc 35 29 (-0.17101 0.469846 0.5)
136
          arc 31 34 (-0.939693 \ 0.34202 \ 0.5)
137
          arc 34 28 (-0.34202 0.939693 0.5)
138
139
140
          arc 0 40 (0.469846 -0.17101 -0.5)
141
          arc 40 45 (0.17101 -0.469846 -0.5)
142
          arc 1 39 (0.939693 -0.34202 -0.5)
143
```



```
arc 39 44 (0.34202 -0.939693 -0.5)
144
          arc 19 53 (0.469846 -0.17101 0.5)
145
          arc 53 58 (0.17101 -0.469846 0.5)
146
          arc 20 52 (0.939693 -0.34202 0.5)
147
          arc 52 57 (0.34202 -0.939693 0.5)
148
          arc 11 48 (-0.469846 -0.17101 -0.5)
149
          arc 48 45 (-0.17101 -0.469846 -0.5)
150
          arc 12 47 (-0.939693 -0.34202 -0.5)
151
          arc 47 44 (-0.34202 -0.939693 -0.5)
152
          arc 30 61 (-0.469846 -0.17101 0.5)
153
          arc 61 58 (-0.17101 -0.469846 0.5)
154
          arc 31 60 (-0.939693 -0.34202 0.5)
155
          arc 60 57 (-0.34202 -0.939693 0.5)
156
157
158
       boundary
159
160
161
162
          top
163
               type symmetryPlane;
164
165
               faces
166
               (
                    (7 \ 8 \ 27 \ 26)
167
                    (6 \ 7 \ 26 \ 25)
168
                    (8 18 37 27)
169
                    (18 \ 17 \ 36 \ 37)
170
               );
171
          }
172
173
          bottom
174
175
               type symmetryPlane;
176
               faces
177
178
                   (49 50 63 62)
179
                   (50 43 56 63)
180
                   (43 \ 42 \ 55 \ 56)
181
182
                   (42 \ 41 \ 54 \ 55)
183
               );
184
          }
185
          inlet
186
187
               type patch;
188
               faces
189
190
                    (14\ 13\ 32\ 33)
191
                    (17 \ 14 \ 33 \ 36)
192
193
                    (46\ 13\ 32\ 59)
194
                    (46 49 62 59)
195
               );
196
          }
197
198
           outlet
199
200
```



```
201
                  type patch;
202
                   faces
                   (
203
                        (2 \ 3 \ 22 \ 21)
204
                        (3 6 25 22)
205
206
                        (38 \ 51 \ 21 \ 2)
207
                        (41 54 51 38)
208
                   );
209
            }
210
211
             cylinder
212
213
                   type wall;
214
                   faces
215
216
                        (10 \ 5 \ 24 \ 29)
217
                        (5 \ 0 \ 19 \ 24)
218
                        (16\ 10\ 29\ 35)
219
                        (11 \ 16 \ 35 \ 30)
220
221
222
                        (48 \ 11 \ 30 \ 61)
223
                        (45 \ 48 \ 61 \ 58)
224
                        (40 \ 45 \ 58 \ 53)
225
                        (0 \ 40 \ 53 \ 19)
226
                   );
            }
227
228
            front And Back\\
229
230
231
                   type empty;
                   faces
232
                   (
233
                       (5\ 10\ 9\ 4)
234
                       (24 \ 23 \ 28 \ 29)
235
                       (0 \ 5 \ 4 \ 1)
236
                       (19 \ 20 \ 23 \ 24)
237
238
                       (1 \ 4 \ 3 \ 2)
239
                       (20\ 21\ 22\ 23)
240
                       (4 \ 7 \ 6 \ 3)
241
                       (23 \ 22 \ 25 \ 26)
242
                       (4 \ 9 \ 8 \ 7)
243
                       (28 \ 23 \ 26 \ 27)
244
                       (16 \ 15 \ 9 \ 10)
^{245}
                       (35 29 28 34)
                       (12\ 15\ 16\ 11)
246
                       (31 \ 30 \ 35 \ 34)
^{247}
                       (13 \ 14 \ 15 \ 12)
248
                       (32\ 31\ 34\ 33)
249
                       (14 \ 17 \ 18 \ 15)
250
                       (33 \ 34 \ 37 \ 36)
251
                       (15 18 8 9)
252
                       (34\ 28\ 27\ 37)
253
254
                       (45 \ 40 \ 39 \ 44)
255
                       (58 57 52 53)
256
                       (40 \ 0 \ 1 \ 39)
257
```



```
(53 \ 52 \ 20 \ 19)
258
                  (39 \ 1 \ 2 \ 38)
259
                  (52 \ 51 \ 21 \ 20)
260
261
                  (39 38 41 42)
262
                  (52 \ 55 \ 54 \ 51)
263
                  (44 39 42 43)
                  (57 \ 56 \ 55 \ 52)
264
265
                  (47 \ 48 \ 45 \ 44)
                  (60 57 58 61)
266
                  (12\ 11\ 48\ 47)
267
                  (31 60 61 30)
268
                  (13\ 12\ 47\ 46)
269
                  (32 59 60 31)
270
                  (49 \ 46 \ 47 \ 50)
271
                  (62 63 60 59)
272
                  (50 \ 47 \ 44 \ 43)
273
                  (63 \ 56 \ 57 \ 60)
274
              );
275
276
277
278
279
       mergePatchPairs
280
       (
281
282
283
```

It can be seen that as the cylinder has curved edges, it is necessary to use the arc instruction to obtain the circular geometry. This instruction must be followed by the labels of the connected vertices and an interpolation point contained in the trajectory of the arc.

In the current *blockMeshDict* there are four different types of patches: *wall*, *empty*, *symmetryPlane* and *patch*. All were used in the *plane-parallel plates* case except *symmetryPlane*, which is used in the top and bottom patches of the current case to indicate that there are no physical walls in the top and bottom borders; the flow must behave as if the domain would extend infinitely in the *y*-direction.

After running blockMesh and checking the results with checkMesh it is possible to observe the mesh with ParaView.

#### Caution:

It is necessary to have the majority of the required files for the simulation within the case directory to create the mesh. Wait until the three main directories (0, constant and system) and their files are ready to run blockMesh. Otherwise, it is also possible to use a solved case as a dummy file to run blockMesh



The mesh of cylinder195 is shown at Figures 3.5, 3.6 and 3.7:

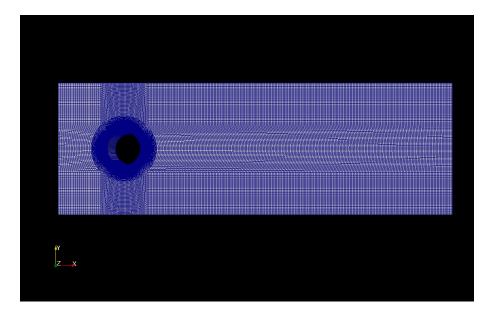


Figure 3.5: Mesh of the  $bidimensional\ cylinder\ case$ 

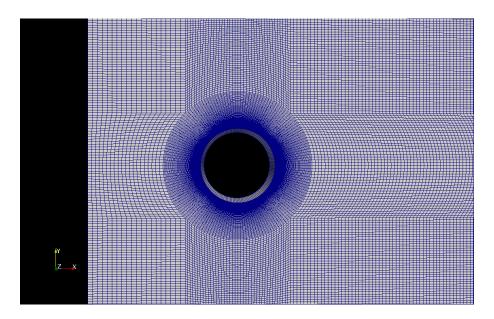


Figure 3.6: Detail of the mesh of the bidimensional cylinder case



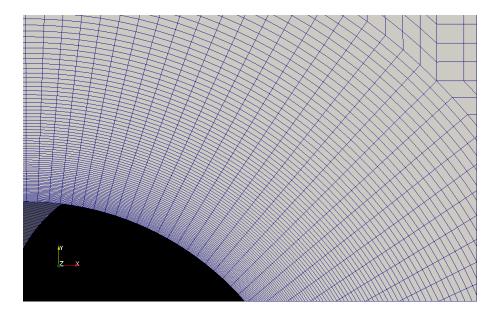


Figure 3.7: Detail of the mesh gradation on the walls of the bidimensional cylinder case

#### Advice:

On the walls and downstream the cylinder it is necessary to have a high refined mesh. It will allow the user to compute the drag coefficient and to observe the von Kármán street both with high accuracy. However, if the simulation is too much time-consuming or it is done with a Reynolds number such that no vortices are generated, it is recommended to reduce the refinement of the mesh

## 3.4.2 Boundary and initial conditions

The files (located in  $\theta$ ) containing the information related to the pressure and the velocity fields are the following:

```
2
                  F ield
                                  | OpenFOAM: The Open Source CFD Toolbox
                  O peration
                                  | Version: 2.2.1
                  A nd
                                  | Web:
                                            www.OpenFOAM.org
5
                  M anipulation
6
     FoamFile
9
         version
                      2.0;
10
11
         format
                      ascii;
         class
                      volScalarField;
```



```
object
13
14
15
16
17
                            [0 \ 2 \ -2 \ 0 \ 0 \ 0 \ 0];
18
       internalField
                           uniform 0;
19
20
      boundaryField
21
22
           top
23
24
                                symmetry Plane \, ;
25
                type
26
27
           bottom
28
^{29}
           {
                                symmetry Plane \, ;
30
                type
31
32
           inlet
33
34
           {
35
                type
                                 free stream Pressure \, ;
36
37
           outlet
38
39
           {
                                 freestream Pressure;
40
                type
41
42
           front And Back\\
43
44
45
                                empty;
                type
46
47
           cylinder
48
49
                                {\tt zeroGradient};
50
                type
51
52
53
1
2
                                         | OpenFOAM: The Open Source CFD Toolbox
                      F ield
3
                                         | Version: 2.2.1
                       O peration
4
                                         | Web:
                       A nd
                                                        {\it www.} OpenFOAM. org
5
                      M anipulation
6
 7
      FoamFile
8
9
                          2.0;
10
           {\tt version}
11
           format
                           ascii;
                          volVectorField\ ;
12
           class
13
           object
```



```
14
15
16
17
       dimensions
18
       internalField
                                   uniform (5 0 0);
19
20
       boundaryField
21
22
            top
23
24
                                        symmetryPlane;
                _{
m type}
25
26
27
            bottom
28
^{29}
                                        symmetry Plane \, ;
30
                _{\rm type}
31
32
33
            inlet
34
            {
35
                                        freestream;
36
                freestream Value\\
                                        uniform (5 \ 0 \ 0);
37
38
            outlet
39
40
            {
                                        freestream;
41
                                        uniform (5 \ 0 \ 0);
                freestream Value\\
42
43
44
            cylinder
45
46
                                        fixedValue;
                type
47
                                        uniform (0 \ 0 \ 0);
                value
48
49
50
            front And Back\\
51
52
53
               _{
m type}
                                        empty;
54
55
56
```

The freestreamPressure condition is acting as zeroGradient but with a more accurate physical behaviour. freestream acts as fixedValue when the flow is ingoing, and as zeroGradient when it is outgoing. This kind of boundary conditions are widely used for external flow simulations.



## 3.4.3 Physical properties

Within constant one finds the information related to the kinematic viscosity and the RASProperties file to compute the wall shear stress or other utilities requesting the RAS dictionary.

```
-*- C++ -*-
2
                               | OpenFOAM: The Open Source CFD Toolbox
      //
                 F ield
3
                 O peration
                               | Version: 2.2.1
                               | Web:
                 A nd
                                          www.OpenFOAM.org
5
                 M anipulation
6
7
     FoamFile
9
10
         version
                    2.0;
11
        format
                    ascii;
12
                    dictionary;
        location
                    "constant";
13
                    transportProperties;
14
15
16
17
     transportModel Newtonian;
18
19
                    nu \begin{bmatrix} 0 & 2 & -1 & 0 & 0 & 0 \end{bmatrix} 2.564103e-03;
20
21
                       22
1
2
                               | OpenFOAM: The Open Source CFD Toolbox
                 F ield
3
                               | Version: 2.2.1
                 O peration
4
                               Web:
                 A nd
                                          www.OpenFOAM.org
5
                 M anipulation
6
         \\/
7
     FoamFile
8
9
                    2.0;
10
        version
11
        format
                    ascii;
12
        class
                    dictionary;
13
        location
                    "constant";
14
        object
                    RASProperties;
15
16
^{17}
18
     RASModel
                    laminar;
19
20
     turbulence
                    off;
21
22
     printCoeffs
23
     24
```



#### 3.4.4 Control

```
1
2
                 F ield
                                | OpenFOAM: The Open Source CFD Toolbox
3
                  O peration
                                | Version: 2.2.1
                                | Web:
                                            www.OpenFOAM.org
                  A nd
5
                 M anipulation
6
7
     FoamFile
8
9
         version
                     2.0;
10
                     ascii;
11
         format
                     dictionary;
12
         class
                     "system";
         location
14
         object
                     controlDict;
15
16
17
     application
                         icoFoam;
18
19
     startFrom
                         startTime;
20
21
     startTime
22
                         0;
23
     stopAt
                         endTime;
24
25
     endTime
                         1.75;
26
27
     deltaT
                         0.00001;
28
29
     writeControl
                         timeStep;
30
31
     writeInterval
                         1000;
32
33
     purgeWrite
34
35
     writeFormat
                         ascii;
36
37
     writePrecision
38
39
     writeCompression
                         off;
40
41
     timeFormat
                         general;
42
43
     timePrecision
                         6;
44
45
     {\tt runTimeModifiable}
46
                         true;
47
     48
```

Advice:



The case reaches steady before  $t=1.75~\mathrm{s}$ . Despite it, endTime has been set to 1.75 to widely appreciate the von Kármán street and its periodical distribution. As the mesh is very refined and the solver is transitory, the simulation may be very slow

## 3.4.5 Discretization and linear-solver settings

```
*- C++ -*
2
                                        OpenFOAM: The Open Source CFD Toolbox
                     F ield
                                       Version: 2.2.1
                     A nd
                                        Web:
                                                   www.OpenFOAM.org
                    M anipulation
7
      FoamFile
8
9
          version
                        2.0;
10
11
          format
                        ascii;
          class
                        dictionary;
12
          location
                        "system";
13
          object
                        fvSchemes;
14
15
16
17
      ddtSchemes
18
19
           default
                             Euler;
20
^{21}
22
      gradSchemes
23
24
           default
                             Gauss linear;
25
                             Gauss linear;
26
          grad(p)
27
28
      divSchemes
29
30
           default
                             none;
31
          div (phi,U)
                             Gauss linear;
32
      }
33
34
      laplacianSchemes
35
36
           default
37
                            none;
          laplacian(nu,U) Gauss linear orthogonal;
38
          laplacian((1|A(U)),p) Gauss linear orthogonal;
39
      }
40
41
42
      interpolation Schemes \\
43
44
           default
                               linear;
45
          interpolate(HbyA) linear;
46
47
```



```
snGradSchemes
48
49
50
          default
                          orthogonal;
51
52
     fluxRequired
53
54
          default
                          no;
55
56
57
58
     59
                                          *- C++ -*-
                                   | OpenFOAM: The Open Source CFD Toolbox
3
                   O peration
                                   | Version: 2.2.1
                   A nd
                                   | Web:
                                               www.OpenFOAM.org
5
           \\/
                   M anipulation
6
7
     FoamFile
8
9
          version
                      2.0;
10
                      ascii;
         format
11
          class
                      {\tt dictionary}\ ;
12
         location
                      "constant";
13
          object
                      transport Properties \ ;
14
15
16
17
     solvers
18
19
20
         р
21
          {
                              PCG;
22
              {\tt solver}
              preconditioner
                              DIC;
23
              tolerance
                               1e - 06;
24
              relTol
                               0;
25
         }
26
27
         U
28
29
                              PBiCG;
              solver
30
              preconditioner
                              DILU;
31
              tolerance
                              1e - 05;
32
              relTol
                               0;
33
34
         }
     }
35
36
     PISO
37
38
          n\,Correctors
                          2;
39
40
          n Non Orthogonal Correctors \ 3;\\
          pRefCell
41
                          0;
          pRefValue
42
                           0;
43
     }
```



Advice:

As it can be seen, the instruction nNonOrthogonalCorrectors has been set to 3 instead of 0 (as it was in the plane-parallel plates case). It is so because when checking the mesh with checkMesh, it is possible to observe that there are mesh non-orthogonalities. Although globally the mesh is OK to be run, it helps in obtaining more physically accurate results

At the end of the pre-processing, the structure of directories and subdirectories within cylinder195 should be as follows:

$$\begin{cases} 0 & \begin{cases} p \\ U \end{cases} \\ constant & \begin{cases} polyMesh \\ blockMeshDict \end{cases} \\ transportProperties \\ RASProperties \end{cases}$$
 
$$\begin{cases} controlDict \\ fvSchemes \\ fvSolutions \end{cases}$$

## 3.5 Post-processing

#### **3.5.1** Results of the simulation with Re = 195

The evolution over time of the velocity is as follows:

Jordi Casacuberta Puig 79



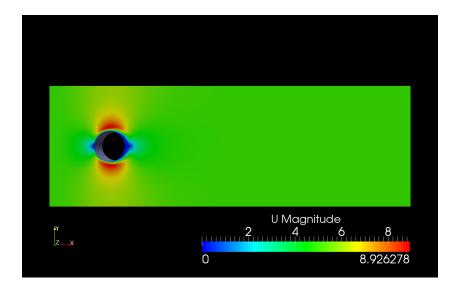


Figure 3.8: Velocity field around the bidimensional cylinder at t = 0.01 s (m/s)

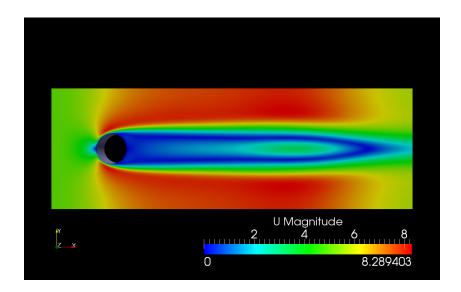


Figure 3.9: Velocity field around the bidimensional cylinder at t = 0.6 s (m/s)

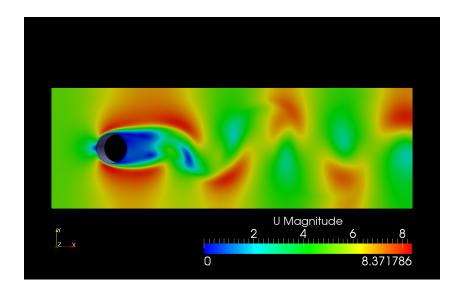


Figure 3.10: Velocity field around the bidimensional cylinder at t = 1.13 s (m/s)

The evolution over time of the pressure is as follows:

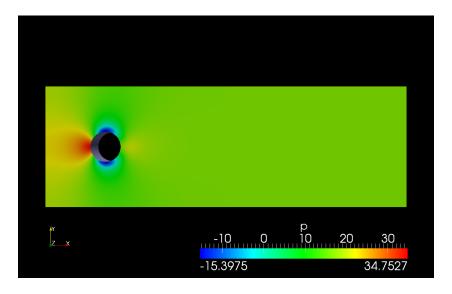


Figure 3.11: Pressure field around the bidimensional cylinder at t = 0.01 s  $(m^2/s^2)$ 



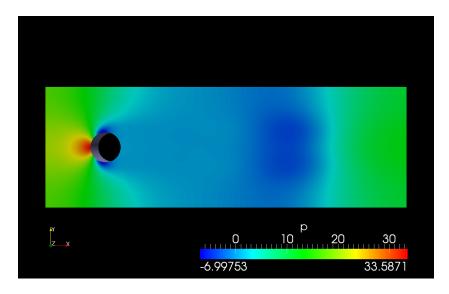


Figure 3.12: Pressure field around the bidimensional cylinder at t = 0.6 s  $(m^2/s^2)$ 

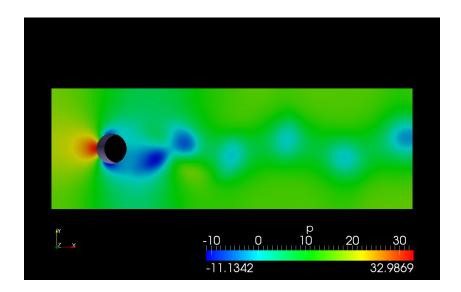


Figure 3.13: Pressure field around the bidimensional cylinder at  $t=1.13~\mathrm{s}~(m^2/s^2)$ 

The evolution over time of the streamlines is as follows:

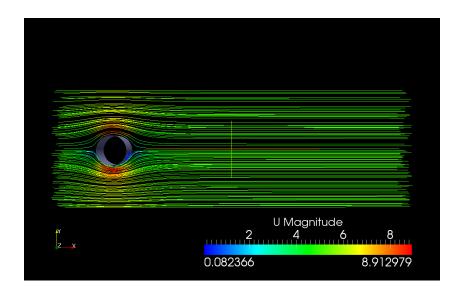


Figure 3.14: Streamlines around the bidimensional cylinder at t = 0.01 s (m/s)

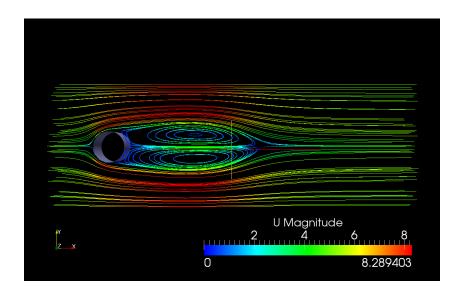


Figure 3.15: Streamlines around the bidimensional cylinder at t = 0.4 s (m/s)



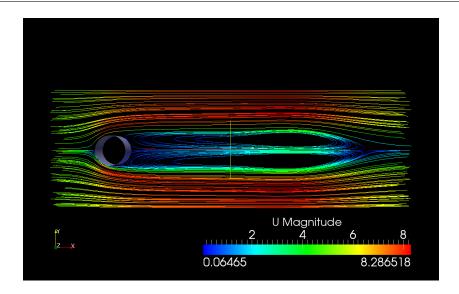


Figure 3.16: Streamlines around the bidimensional cylinder at t = 0.6 s (m/s)

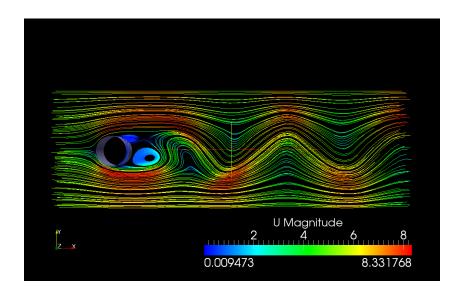


Figure 3.17: Streamlines around the bidimensional cylinder at t = 1.13 s (m/s)

A detail of the vector field near the wall of the cylinder is shown to appreciate the boundary layer detachment:

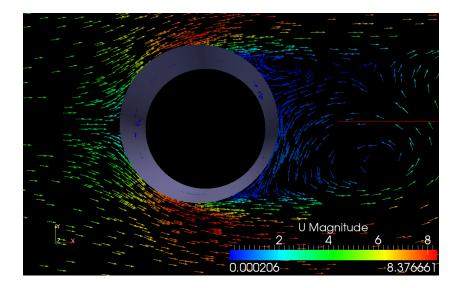


Figure 3.18: Velocity vectors around the bidimensional cylinder at t = 1.13 s (m/s)

#### Advice:

A way to introduce the shape of the cylinder to provide more realism to the results is shown in Section 3.6.5

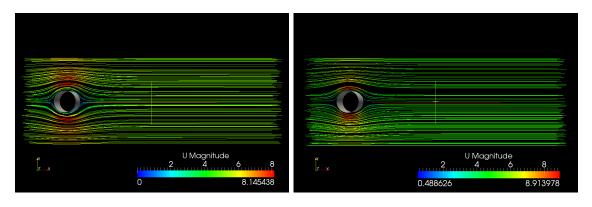
## **3.5.2** Comparative between cases with Re = 30 and Re = 195

Additionally, the simulation has been done for another different Reynolds number (Re = 30). The only instruction that needs to be changed in the  $OpenFOAM^{\mathbb{R}}$  code is for instance the kinetic viscosity in constant/transportProperties. According to Equation 5.3, by maintaining the value of the inlet velocity while increasing the kinetic viscosity it is possible to simulate the bidimensional cylinder in such regime (case cylinder30):

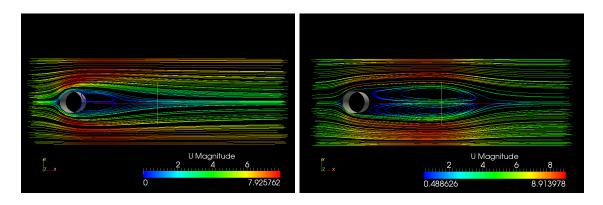


Re = 30

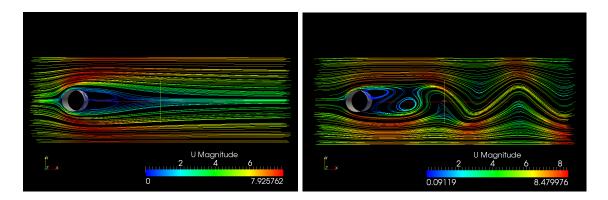
Re = 195



 $t=0.01~\mathrm{s}$ 



 $t=0.4~\mathrm{s}$ 



 $t=1 \mathrm{\ s}$ 

As it was shown in Section 3.3, for Re = 30 the alternate vortices are not detached.



## 3.6 Additional utilities

## 3.6.1 Vorticity

As with the computation of the flow rate and the wall shear stress, it is also possible to compute the vorticity in the fluid field by using  $OpenFOAM^{\textcircled{R}}$  utilities. The vorticity is a pseudovector field that describes the local spinning motion of a fluid near some point, as would be seen by an observer located at that point and traveling along with the fluid. Mathematically, the vorticity is the curl of the velocity field:

$$\vec{w} = \nabla \times \mathbf{U}$$

The vorticity of a two-dimensional flow is always perpendicular to the plane of the flow. It plays a relevant role in the current chapter due to the existence of vortices generated by the cylinder forming the von Kármán street.

To execute it, type within the case directory

#### vorticity

Within the directories of each time step it has appeared a new file. Then, to observe the vorticity field, open ParaView and select it by clicking the vorticity box contained within Volume Fields. For the cylinder195 case, the results are:

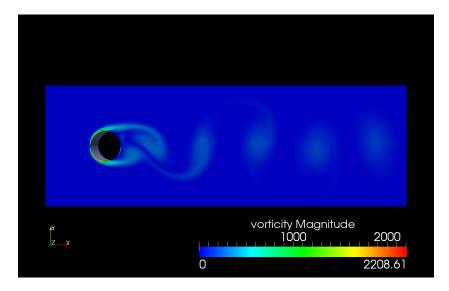


Figure 3.19: Vorticity field around the bidimensional cylinder at t = 1.75 s

Jordi Casacuberta Puig



It offers a clear-cut representation of the von Kármán vortices at Re = 195.

## 3.6.2 Computation of the aerodynamic coefficients

One of the main interests when studying external flows is the computation and analysis of the aerodynamic forces that the fluid exerts to solid objects. The drag is the force parallel to the flow velocity and the lift is the force perpendicular to the flow velocity. The dimensionless drag force is presented in Equation 5.6 and for an infinite circular cylinder its dependence on the Reynolds number is shown at Figure 3.3.

With  $OpenFOAM^{\textcircled{R}}$ , to compute the aerodynamic forces that a fluid exerts on solid walls, add the following code after the last instruction of controlDict:

```
functions
1
2
3
     forces
     type forces;
6
     functionObjectLibs ("libforces.so");
     patches (cylinder); // Patch where the force exerted by the fluid is calculated
8
     pName p;
     UName U;
     rhoName rhoInf;
10
     rhoInf 1000; // Reference density of the fluid
11
     CofR (0 0 0); // Origin for moment calculations
12
     outputControl timeStep; // Time criterion used to print the results
13
     outputInterval 100; // How often (according to outputControl) the results are
14
         printed
     }
15
     forceCoeffs
16
17
     type forceCoeffs;
18
     functionObjectLibs ("libforces.so");
19
     patches (cylinder); // Patch where the force exerted by the fluid is calculated
20
     pName p;
21
     UName U;
22
     rhoName rhoInf;
23
     rhoInf 1000; // Reference density of the fluid
24
     CofR (0 0 0); // Origin for moment calculations
25
     liftDir (0 1 0);
26
     dragDir (1 0 0);
27
     pitchAxis (0 0 1);
28
     magUInf 5; // Free stream velocity
29
     lRef 0.1; // Reference length (diameter of the cylinder)
30
     Aref 0.01; // Reference area (cross sectional area of the cylinder)
31
     outputControl timeStep; // Time criterion used to print the results
32
     outputInterval 100; // How often (according to outputControl) the results are
33
         printed
34
```



35 );

Advice:

For incompressible cases, the value of rholnf is irrelevant for the computation of the dimensionless coefficients

Now, when the case is rerun, a new directory named *postProcessing* appears next to 0, *constant* and *system*. This directory contains two subdirectories with information concerning the evolution of the aerodynamic forces and moments and their dimensionless coefficients.

## 3.6.3 Plotting the results with Gnuplot

Once the aerodynamic forces have been computed with the instruction shown in Section 3.6.2, it is useful to plot the results. Besides showing the behaviour of the forces with time, it allows an understanding of the convergence (or divergence) of the case. For the *bidimensional cylinder* case, it is possible to claim that if the drag coefficient converges then the case converges too.

First of all the user has to have **Gnuplot** installed. It is a portable command-line driven graphing utility for Linux, MS Windows, OSX and many other platforms. It is widely used to plot data obtained with  $OpenFOAM^{\textcircled{R}}$ . First, access the file containing the required data:

cd FoamCases/cylinder195/postProcessing/forceCoeffs/0

Secondly, execute Gnuplot by typing:

gnuplot

Finally plot the values of the drag coefficient (third column) in front of the time (first column) by typing:

plot './forceCoeffs.dat' u 1:3 w 1

The plot is:



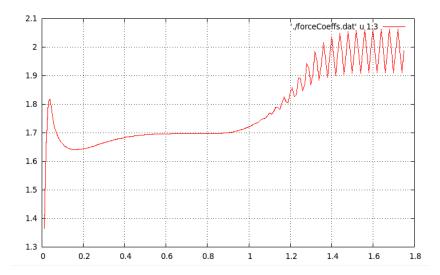


Figure 3.20: Drag coefficient (ordinate axis) of the bidimensional cylinder at Re = 195 in front of time (abscissa axis)

It is also possible to plot the values of the lift coefficient (fourth column) in front of the time (first column) by typing:

The plot is:

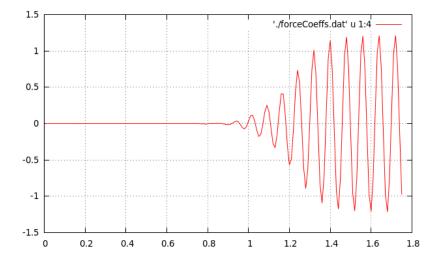


Figure 3.21: Lift coefficient (ordinate axis) of the bidimensional cylinder at Re = 195 in front of time (abscissa axis)



## 3.6.4 Computation of the stream function

As it was explained in Section 2.6.2, the streamlines offer a clear understanding of the behaviour of the flow; they represent the trajectories of particles in steady fluids. Related to it, there exists a scalar function (stream function) such that the flow velocity components can be expressed as the derivatives of this function, also being used to plot the streamlines. Mathematically it is related to the velocity as:

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}$$

Since streamlines are tangent to the velocity vector of the flow, the value of the stream function must be constant along a streamline.

To obtain the stream function of the velocity, type:

#### streamFunction

To view the results with ParaView, it is necessary to select the streamFunction box located within Point Fields. Here are the results:

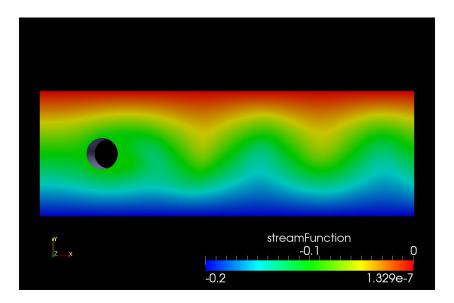


Figure 3.22: Stream function of the velocity of the bidimensional cylinder case for Re = 195 at t = 1.75 s

As it can be seen, it follows the same trend as the streamlines but with a continuous appearance. The colour indicates the value of the stream function in a particular point (note that this utility generates a point field), taking the  $\psi = 0$  streamline as



the one at the top patch of the domain.

It can be proved that the volumetric flow rate between two streamlines is equal to the difference between their stream functions. This helps in the validation of the streamFunction utility. At the inlet:

$$Q = V \cdot S = 5 \cdot 0.4 \cdot 0.1 = 0.2 \ m^3/s$$
$$Q = \psi_n - \psi_0 = 0.2 \ m^3/s$$

#### 3.6.5 Convertion to VTK

It is possible to convert data from  $OpenFOAM^{\textcircled{R}}$  to VTK format. For instance, access cylinder195 and type:

#### foamToVTK

A new directory appears within the case containing the VTK data. Since it is a worldwide used format, it is also possible to open it with ParaView.

Example: Once in ParaView, click on the "open" icon, access the VTK directory of the case and click on "cylinder". Within the Pipeline Browser, a new module has appeared. It is the cylinder patch whose shape can be used to give more realism to the results of the simulation. This same procedure can be carried out for each one of the defined patches of the case.