

Week 14

???

14.1 Kinetic Resolution and Related Asymmetric Processes

12/3:

- Announcements.
 - Today: Last Tuesday's lecture.
 - Next time: Electron Transfer.
 - Exam 2 tomorrow.
 - Format like the practice exam.
 - Administered remotely.
 - Work alone, and closed note (honor code).
 - Available for 48 hours: Start of Wednesday til end of Thursday.
 - Do the teaching evaluations for both Alex and Masha!!
- Today: Kinetic selectivities.
- Consider a starting material (SM) that can evolve to a product A or B.

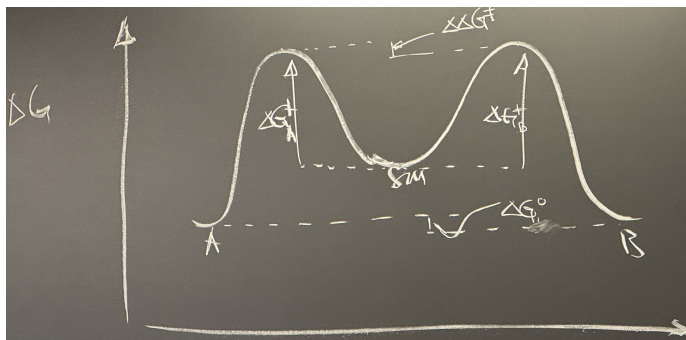


Figure 14.1: Thermodynamic vs. kinetic selectivity energy diagram.

- We can map this reaction onto a potential energy surface.
- If A and B are free to reversibly interconvert, then we can explain the product distribution in terms of the ΔG° between A and B.
 - In particular, $\Delta G = -RT \ln K_{eq}$ where $K_{eq} = [A]/[B]$.

- Today, we'll consider the case in which A and B do *not* reversibly interconvert.
 - In this case, what's important is the $\Delta\Delta G^\ddagger$ between the transition states.
 - Here, the selectivity is given as the ratio of the rate constants:

$$\text{selectivity} = \frac{[A]}{[B]} = \frac{k_A}{k_B} = \frac{e^{-\Delta G_A^\ddagger/RT}}{e^{-\Delta G_B^\ddagger/RT}} = e^{-\Delta\Delta G^\ddagger/RT}$$

- Note that $k_A/k_B = k_{\text{rel}}$. This quantity is important for determining dr's, er's, etc.
- A case in which kinetic selectivity is important: Catalytic kinetic resolution.

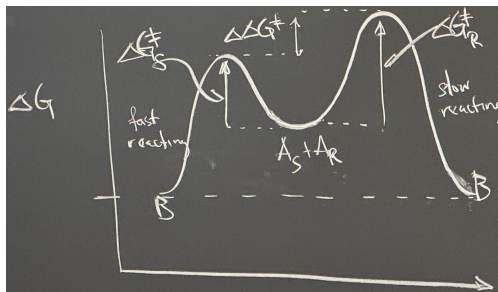


Figure 14.2: Catalytic kinetic resolution energy diagram.

- A is our starting material, a chiral racemic compound.
 - Thus, we can denote the starting materials as $A_S + A_R$.
 - As enantiomers, A_R and A_S have identical free energies.
- cat^* is a **homochiral** catalyst.
- Then resolution to a product B can happen two different ways: Through a transition state that consumes the (*S*)-enantiomer, and through a transition state that consumes the (*R*)-enantiomer.
- When a homochiral catalyst acts on two enantiomers, it forms two different, diastereomeric adducts: $A_S \cdot \text{cat}^*$ and $A_R \cdot \text{cat}^*$.
 - Unlike enantiomers, diastereomers *are* different compounds that may have two different energies.
- What we've indicated in Figure 14.2 is that the (*S*)-enantiomer is converted faster than the (*R*)-enantiomer.
- Thus,

$$k_{\text{rel}} = \frac{k_{\text{fast}}}{k_{\text{slow}}} = e^{-\Delta\Delta G^\ddagger/RT}$$

- In the literature, k_{rel} is sometimes referred to as an **S-factor** (for “selectivity factor”).
- Reference: Sheldon (2001).
- **Homochiral** (catalyst): A chiral catalyst of which we're using only a single enantiomer.
- There are many catalytic kinetic resolutions in the literature.
 - Radosevich developed one in grad school, when he was roughly our age!

- Example catalytic kinetic resolution.

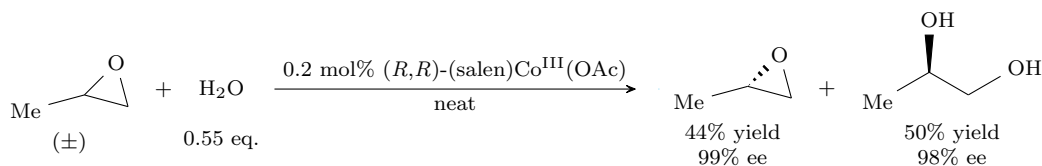


Figure 14.3: Hydrolytic kinetic resolution.

- Take propylene oxide (racemic) and 0.55 eq. of water.
- React them, neat, in the presence of a small amount of homochiral catalyst.
 - The structure of this complex is totally irrelevant to our aims, but we can look it up in the reference if we're curious.
 - This is our homochiral catalyst that will act on the two relatively inexpensive starting materials.
- We run this reaction neat, and recover one enantiomer of our starting material in nearly quantitative yield with near perfect ee.
- We also obtain a ring-opened *vic*-diol in nearly quantitative yield with near perfect ee.
- $k_{\text{rel}} \approx 500$ here!
- Reference: Tokunaga et al. (1997).
- This is a **hydrolytic kinetic resolution**.
 - This is a very useful reaction for the resolution of terminal epoxides — and access to terminal 1,2-diols — because there exists no method to synthetically prefer a single enantiomer.
 - Propylene is so small that even the best chiral epoxidation catalysts aren't very selective here, so it's better to do a racemic epoxidation and then this.
- Great atom economy.
- In a kinetic resolution like the above, the percent ee of both starting material and product is subject to change over time.
- To see this, let's build a theoretical model for a catalytic kinetic resolution.



- The net transformation involves the above two chemical reactions.
- We can write differential rate laws for each enantiomer

$$\frac{d[A_S]}{dt} = -k_{\text{fast}}[A_S][\text{cat}^*] \qquad \frac{d[A_R]}{dt} = -k_{\text{slow}}[A_R][\text{cat}^*]$$

- The consumption of the fast-reaction enantiomer will deplete [A].
- Assuming [cat*] is approximately constant throughout the reaction, each of these differential rate laws can be independently integrated to

$$\ln\left(\frac{[A_S]}{[A_S]_0}\right) = -k_{\text{fast}}[\text{cat}^*]t \qquad \ln\left(\frac{[A_R]}{[A_R]_0}\right) = -k_{\text{slow}}[\text{cat}^*]t$$

- Then, the key thing to note here is that for a racemic mixture, $[A_S]_0 = [A_R]_0$.
- Thus, we can make this substitution and divide the above two integrated rate laws to get

$$k_{\text{rel}} = \frac{k_{\text{fast}}}{k_{\text{slow}}} = \frac{\ln([A_S]/[A_S]_0)}{\ln([A_R]/[A_S]_0)}$$

- This is a useful result, but we can make it even better. We'll start with a couple of definitions.

- **Conversion:** The ratio of how much of a reactant has reacted. *Denoted by c . Given by*

$$c := 1 - \frac{[A_S] + [A_R]}{[A_S]_0 + [A_R]_0} = 1 - \frac{[A_S] + [A_R]}{2[A_S]_0}$$

- **Enantiomeric excess:** A measurement of the degree to which a sample contains one enantiomer in greater amounts than the other. *Denoted by ee . Given by*

$$ee := \frac{[A_S] - [A_R]}{[A_S] + [A_R]}$$

- We can now do some algebra.

- Indeed, it follows from the above definitions that

$$1 - ee = \frac{2[A_R]}{[A_S] + [A_R]} \qquad 1 + ee = \frac{2[A_S]}{[A_S] + [A_R]}$$

- Then we can derive the following interesting relationships.

$$\frac{[A_R]}{[A_S]_0} = (1 - c)(1 - ee) \qquad \frac{[A_S]}{[A_S]_0} = (1 - c)(1 + ee)$$

- We can now know the extent to which a reaction has evolved to consume one enantiomer or the other as a function of observables!

- Thus, we may define $S = k_{rel}$ as a function of conversion and ee .

- For recovered starting material,

$$S = \frac{\ln[(1 - c)(1 - ee)]}{\ln[(1 - c)(1 + ee)]}$$

- For the product,

$$S = \frac{\ln[(1 - c)(1 + ee)]}{\ln[(1 - c)(1 - ee)]}$$

- These relations allow us to relate conversion to ee for a catalyst of a given, set selectivity S . Specifically, we can parametrically plot ee as a function of conversion.
- Let's first do this for the percent ee in the recovered starting material.

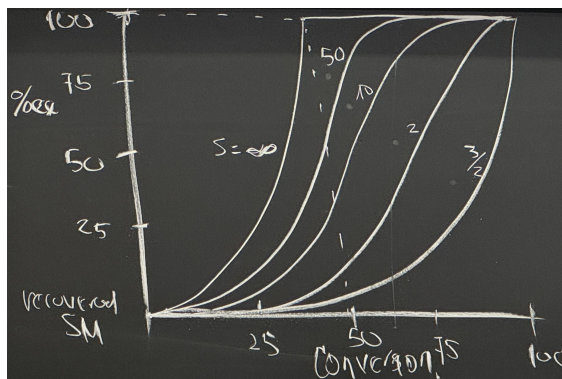


Figure 14.4: Starting material ee vs. conversion in a catalytic kinetic resolution.

- Consider first what happens in the limit that our selectivity factor is very large, i.e., that $\Delta\Delta G^\ddagger =$ large.
- If $S = \infty$, then 50% conversion will get us all we need.
 - This is because at this point, the enantiomer we don't want to recover will have been fully consumed.
- As the S-factor drops, we need higher conversions to get better ee's in the recovered starting material.
- What's cool about this is we can still get high ee's with bad catalysts... at the expense of conversion.
 - Essentially, with bad catalysts, we'll recover *less* enantiopure starting material (because some of it will have been consumed at higher conversions), but we *can* still recover essentially enantiopure starting material.
- For the product.

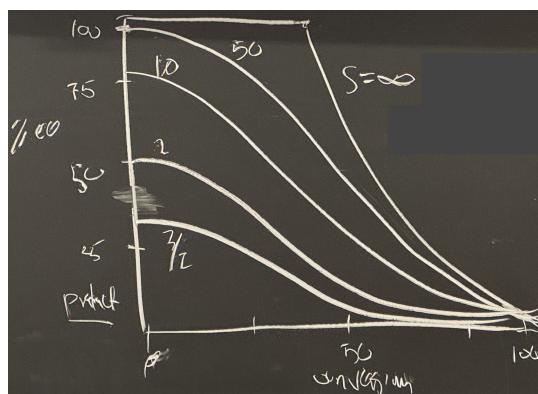


Figure 14.5: Product ee vs. conversion in a catalytic kinetic resolution.

- If $S = \infty$, the product will be enantiopure up until we begin converting some of the other enantiomer.
- If $S = 50$, we start at near-optimal purity, and then our bias will erode.
- What this implies is that for the purpose of kinetic resolution of the product, we need very good catalysts.
- That's what's remarkable about the Jacobsen catalyst: It's extremely selective for both the starting material *and* product.
- Let's now enter into some more complex kinetic regimes.

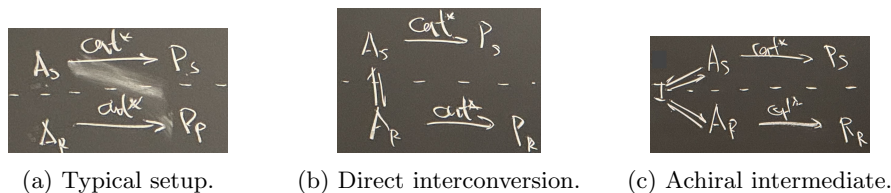


Figure 14.6: Dynamic kinetic resolution models.

- As we've depicted it in Figure 14.2, our starting materials are equal in energy and not interconverting.
 - We can conceptualize this scenario as having a mirror plane between our starting materials and products that we *never* cross (Figure 14.6a).
- But what about when the starting materials do interconvert?
 - There are two ways in which this can happen: We can cross the mirror plane directly (Figure 14.6b), or through an achiral intermediate (Figure 14.6c).
- The 50% mass balance limit that is otherwise imposed is now lifted!
- Now our catalyst can sample both enantiomers via the epimerization.
- A_S interconverts with A_R , subject to a kinetically selective catalyst.
- Enantiomers under fast equilibrium are still under kinetic control, but with 100% theoretical yield.

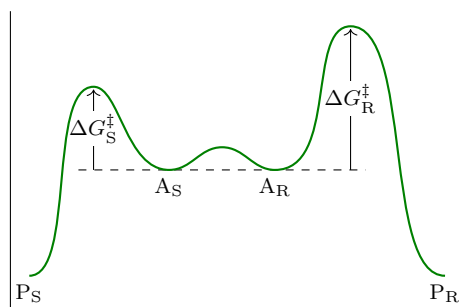


Figure 14.7: Dynamic kinetic resolution energy diagram.

- This is known as a **dynamic kinetic resolution**.
- Example dynamic kinetic resolution: Interconversion of chiral β -ketoesters prior to asymmetric hydrogenation.

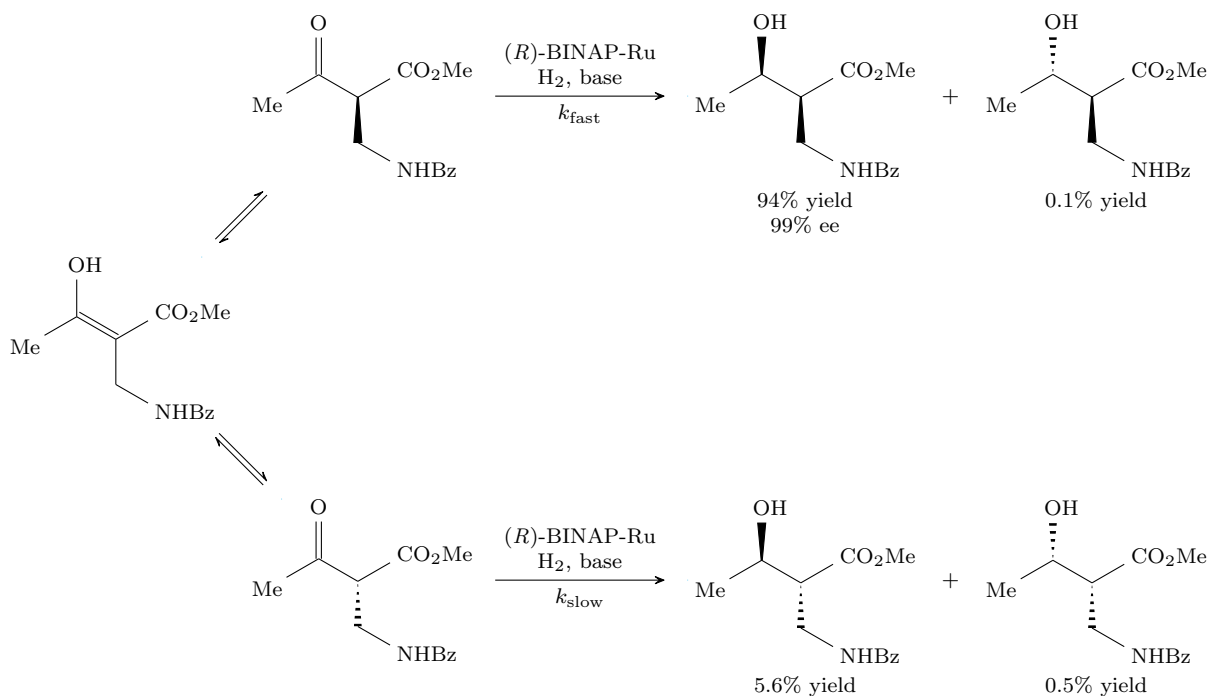


Figure 14.8: Noyori asymmetric hydrogenation.

- Consider a racemic sample of α -alkylated β -ketoester.
- Subject it to hydrogenation under **Noyori conditions**.
 - Both enantiomeric starting materials may become a *syn* or *anti* diastereomers.
 - Thus, in principle, you'd get a mess.
- Our mess is slightly alleviated by the fact that $k_{\text{fast}}/k_{\text{slow}} = 15$ for the ruthenium-BINAP catalyst.
 - This is about 2 kcal/mol of difference.
 - However, per Figure 14.5, this S-factor is not great.
- Our saving grace is the dynamic nature of this reaction.
 - When we actually run the experiment, we get fast enolization and interconversion through an achiral intermediate because of the base^[1] in solution and the acidic α -proton.
 - Indeed, if the rate of enolization/racemization is denoted by k_{rac} , we have $k_{\text{rac}}/k_{\text{fast}} \approx 100$!
- Thus, we get 94% yield of one stereoisomer in 99% ee.
- Reference: Noyori et al. (1995).
 - See Table 3, Figure 19, and the associated discussions.
 - The whole paper is a good review of this chemistry, though.
- **Noyori asymmetric hydrogenation:** The asymmetric hydrogenation of a ketone using a homochiral ruthenium-BINAP catalyst, hydrogen gas, and a base.
- A related kinetic selectivity: Curtin-Hammett kinetics.

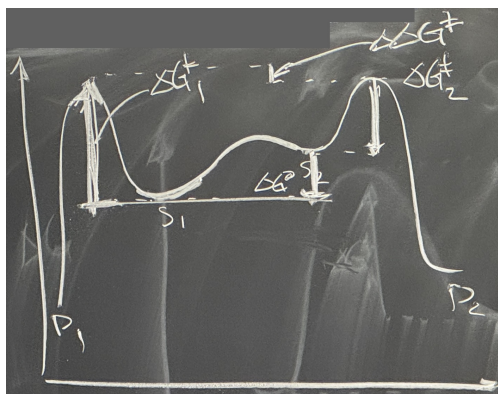


Figure 14.9: Curtin-Hammett selectivity derivation.

- Instead of (*R*)- and (*S*)-enantiomers, which rigorously have the same energy, we can consider other interconverting species with different energies.
- We can quantitate — with rate laws — the formation of the products.

$$\frac{d[P_1]}{dt} = k_1[S_1] \qquad \frac{d[P_2]}{dt} = k_2[S_2]$$

- Then taking a ratio gives

$$\frac{d[P_1]}{d[P_2]} = \frac{k_1[S_1]}{k_2[S_2]}$$

- Note that

$$\frac{[S_1]}{[S_2]} = K_{\text{eq}}$$

so

$$\frac{d[P_1]}{d[P_2]} = \frac{k_1}{k_2} K_{\text{eq}}$$

¹It appears from the paper that there may not be a base; this may just be keto-enol tautomerization.

- Thus, with Arrhenius,

$$\frac{d[P_1]}{d[P_2]} = \frac{e^{-\Delta G_2^\ddagger/RT}}{e^{-\Delta G_1^\ddagger/RT}} e^{-\Delta G^\circ/RT} = e^{(\Delta G_1^\ddagger - \Delta G_2^\ddagger - \Delta G^\circ)/RT}$$

- And then referencing Figure 14.9, we can see pictorially that

$$\Delta G_1^\ddagger - \Delta G_2^\ddagger - \Delta G^\circ = \Delta \Delta G^\ddagger$$

- Thus,

$$\frac{d[P_1]}{d[P_2]} = e^{\Delta \Delta G^\ddagger/RT}$$

if we have a fast equilibrium $S_1 \rightleftharpoons S_2$ (10 times faster than P_1 or P_2 formation).

- Essentially, if we have this fast starting equilibrium, then the product ratio is under kinetic control.
- Now suppose we drop S_2 down in free energy and leave the rest of the diagram unperturbed.
 - This change in one variable is compensated for by a change in the other variable, and we remain under kinetic control.
- Alex briefly discusses kinetic quench.
- Curtin-Hammett example 1 (Figure 6.4a).
 - P_1 is kinetically favored.
 - $[S_1] > [S_2]$.
 - Here, the S_1/S_2 ratio is irrelevant to product formation. This is “invisible” C/H kinetics. Mathematically,

$$\frac{[S_1]}{[S_2]} \neq \frac{[P_1]}{[P_2]}$$
- Curtin-Hammett example 2 (Figure 6.4b).
 - P_1 is kinetically favored.
 - $[S_1] < [S_2]$.
 - This is “classic” C/H kinetics.
 - Great example of this in Landis and Halpern (1987).
 - This scenario is actually pretty common.
- Curtin-Hammett example 3 (Figure 6.4c).
 - Here, $\Delta G_1^\ddagger = \Delta G_2^\ddagger$.
 - This scenario is pretty uncommon, but it is possible.
 - In this case, the equilibrium ratio *does* reflect the product ratio.
- Takeaway: It is far more likely that your equilibrium ratio of intermediates has no bearing on your ratio of products.

14.2 Exam 2 Review Sheet

12/4:

- Noncovalent interactions.
 - Quadrupoles preferentially bind hard, positively charged ions.
 - The strongest hydrogen bonds have short bond lengths and are nearly linear; vice versa for weak.
 - There is an energetic penalty to mixing polar and nonpolar solvents. The penalty is mostly entropic, because putting a hydrophobic link in the water disrupts the water's ability to randomly hydrogen bond to itself. Less H-bonding means more ordered, less entropic water.
- Transition states are first-order saddle points on a hypersurface defined by vibrational DOFs.
 - $\Delta G = -RT \ln K_{\text{eq}}$.
 - $\Delta G^\ddagger = -RT \ln k$.
 - $\Delta \Delta G^\ddagger = -RT \ln(k_A/k_B)$

- **van't Hoff analysis:** Experimental determination of ΔH° and ΔS° .

$$-RT \ln K_{\text{eq}} = \Delta H^\circ - T\Delta S^\circ$$

$$R \ln K_{\text{eq}} = -\Delta H^\circ \left(\frac{1}{T} \right) + \Delta S^\circ$$

- Fragmentations give 9 kcal/mol, or 30 e.u. at 300 K.
- Transition state theory.

- General form.



- Postulates.

1. Activated complex is in quasi-equilibrium with starting material.
2. Any molecule that makes its way to the transition state will then proceed onto the product barrierlessly ($\kappa = 1$).

- The number of times a starting material appears in the TS is it's order in the rate law.
- Eyring equation:

$$k = \kappa \left(\frac{k_B T}{h} \right) e^{-\Delta G^\ddagger / RT}$$

- Linearization (for experimental determination of ΔH^\ddagger and ΔS^\ddagger):

$$\ln \left(\frac{k h}{\kappa k_B T} \right) = -\frac{\Delta H^\ddagger}{R} \left(\frac{1}{T} \right) + \frac{\Delta S^\ddagger}{R}$$

- Hammond postulate.

- Isotope effects.

- QMech foundation:

$$E_n = h\nu \left(n + \frac{1}{2} \right) \qquad \nu = \frac{1}{2\pi} \sqrt{\frac{k}{\mu}}$$

- C-D lower by 1.5 kcal/mol.
- Equilibrium isotope effect:

$$\frac{K_H}{K_D}$$

- C–D bonds hold onto their electrons more tightly.
- Kinetic isotope effect.

$$\text{KIE} = \frac{k_{\text{H}}}{k_{\text{D}}}$$

- Asymmetric stretch is the reaction coordinate.
 - Symmetric stretch is the important orthogonal vector.
 - Under thermoneutral conditions with identical atoms on either side, KIE = max because the symmetric stretch has no isotopic sensitivity.
- Bent transition states have more contributions from bending mode isotopic sensitivities, but smaller overall sensitivities (1.5-3.5).
- Quantum tunnelling can give anomalously large KIEs.
- Secondary isotope effects at the α -position largely governed by out-of-plane bending modes.
 - Going to a slacker potential: Normal 2° KIE.
 - Going to a stiffer potential: Inverse 2° KIE.
- Secondary isotope effects at the β -position governed by hyperconjugation, or actually primary because involved (e.g., E₂).
- Experimental determination.
 - Independent absolute rate measurement.
 - Intramolecular competition experiment.
 - Correction: If

$$C := \frac{[\text{P}_{\text{H}}]}{[\text{SM}_{\text{H}}]_0} \quad R := \left(\frac{[\text{SM}_{\text{D}}]}{[\text{SM}_{\text{H}}]} \right)_t \quad R_0 := \left(\frac{[\text{SM}_{\text{D}}]}{[\text{SM}_{\text{H}}]} \right)_0$$

then

$$\text{KIE} = \frac{k_{\text{H}}}{k_{\text{D}}} = \frac{\ln(1 - C)}{\ln \left[(1 - C) \cdot \frac{R}{R_0} \right]}$$

- Intramolecular competition can probe post-rate-determining steps.
 - Extract KIE from the product ratio at *any* conversion.
- Heavy-atom KIEs.
 - Extracted at high conversions.
 - Choose a reference atom, take NMRs at high conversion, plug into conversion formula to get KIEs.
 - Can tell you what sites are involved in the RDS!
 - Conversion-*dependent* isotopic enrichment is affiliated with the RDS.
 - Conversion-*independent* isotopic enrichment is affiliated with post-RDS steps.
- Rate laws.
 - Zeroth-order, first-order, and second-order integrated rate laws.
 - k_{obs} vs. swamping concentrations to determine k .
 - SSA.
 - If A is more stable than B, the SSA is valid.
 - If I is depleted faster than it is formed, the SSA is valid.
 - QEA.
 - Only valid when $k_{-1} > k_2$.
 - Limiting cases.

- The saturation regime.
- Defining the total concentration of the catalyst is often useful.
- Michaelis-Menten kinetics.
- Blackmond's work.
 - Same-excess experiment and visual overlay.
 - Different excess experiment.
- Kinetic resolution.
 - Relations between conversion and ee.
 - Dynamic kinetic resolution: Going through an intermediate or other interconversion.
 - Curtin-Hammett kinetics.