

Week 6

Deviations from Ideality

6.1 Thermodynamics of the Rubber Band

2/14:

- Midterm:
 - Take for two hours, any two hours tomorrow.
 - Upload a single PDF file for your answer.
 - Do not discuss the questions with anybody.
- **Standard Gibbs free energy** (at T): The following energy, where $H^\circ(T)$ is the standard enthalpy at T and $S^\circ(T)$ is the standard entropy at T . Denoted by $G^\circ(T)$. Given by

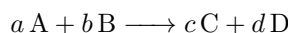
$$G^\circ(T) = H^\circ(T) - TS^\circ(T)$$

- It follows that since the enthalpy is taken at constant pressure and the entropy $S(T, P)$ at non-standard pressure is given by $S(T, P) = S^\circ(T) + R \ln P/P_0$ that the Gibbs free energy $G(T, P)$ at nonstandard pressure is

$$\begin{aligned} G(T, P) &= H^\circ(T) - TS(T, P) \\ &= H^\circ(T) - T \left(S^\circ(T) + R \ln \frac{P}{P_0} \right) \\ &= G^\circ(T) - RT \ln \frac{P}{P_0} \end{aligned}$$

- Gibbs free energy and equilibrium at constant T, P .

- If



is in equilibrium where A, B, C, D are ideal gases, then $\Delta G = 0$.

- This implies that

$$a\Delta G_a + b\Delta G_b = c\Delta G_c + d\Delta G_d$$

which is the **law of mass action**.

- Example of phase equilibrium ($G(T)$ for solid/liquid/gas phases).

- We have from the total differential of G that

$$\left(\frac{\partial G}{\partial T} \right)_P = -S$$

- Since $S \geq 0$ always, G is monotonically decreasing.

- During the liquid phase, there is a relatively constant slight negative slope in the $G(T)$ graph.
- During the gas phase, S is much bigger, so there is a larger negative slope in the $G(T)$ graph.
- Additionally, at the heats of vaporization and fusion, the system is in equilibrium (hence the energies are the same), so the graph is continuous.
- Rubber band temperature analysis.
 - A rubber band heats up when stretched:
 - We have that $dU = T dS + f dL$.
 - We want to show that $(\partial U / \partial L)_T = T(\partial S / \partial L)_T + f$.

$$\begin{aligned} dU &= T \left(\frac{\partial S}{\partial T} \right)_L dT + \left(\frac{\partial S}{\partial L} \right)_T dL + f dL \\ &= T \left(\frac{\partial S}{\partial T} \right)_L dT + \left[\left(\frac{\partial S}{\partial L} \right)_T + f \right] dS \end{aligned}$$

- All that's left is to show that $-(\partial S / \partial L)_T = (\partial f / \partial T)_L$, which we can do using Maxwell relations.

$$dA = -S dT + f dL$$

$$\left(\frac{\partial U}{\partial L} \right)_T = -T \left(\frac{\partial f}{\partial T} \right)_L + f$$

- Stating the equation of state for the “ideal” rubber band.

$$f = T\phi(L)$$

- It follows that $(\partial f / \partial T)_L = f/T$, and $(\partial U / \partial L)_T = -T \cdot f/T + f = 0$.
- We are now ready to answer the question of does it cool down or heat up when stretched adiabatically.

$$\begin{aligned} dU &= \left(\frac{\partial U}{\partial L} \right)_T dL + \left(\frac{\partial U}{\partial T} \right)_L dT = \delta q + f dL \\ \left(\frac{\partial U}{\partial T} \right)_L dT &= f dL \\ C_L dT &= f dL \\ dT &= \frac{f}{C_L} dL > 0 \end{aligned}$$

so since $dT > 0$, the rubber band heats up as it stretches.

- For intuitive motivation, PGS discusses Figure 17.1 of Labalme (2021).
- Building a statistical model of the rubber band.
 - Consider the rubber band to be made up of segments (you can think of each segment as part of a polymer). These segments can be oriented up or down. In a stretched rubber band, the polymers will be straight, i.e., all the segments will point the same way.
 - The difference in energy ΔE between a segment (of length ℓ_0) pointing up or down is $2f$.
 - Thus, the partition function for each segment is

$$q = e^{-f\ell_0/k_B T} + e^{f\ell_0/k_B T}$$

- Note that this is the same as the partition function for a paramagnet (which can also either be up or down) except that $f\ell_0$ becomes $\mu_B B_z$.

- When we sum the energies, we multiply the component partition functions. Thus,

$$Q = q^N$$

- We know that

$$L = N(p + p_0 + p - (-p_0)) = Np_0(p + (-p)) = N\ell_0 \tanh\left(\frac{f\ell_0}{k_B T}\right)$$

6.2 Van der Waals Phase Transitions

2/16:

- Wrapping up the rubber band analysis.
- Note that we can approximate $\tanh x \approx x$ for small x . Thus,

$$L = N\ell_0 \cdot \frac{f\ell_0}{k_B T}$$

for small f .

- Therefore, statistical mechanics predicts the rubber band “ideal” equation of state, $f = T\phi(L)$, where f is the stretching force. Note that this is not at all like a mechanical spring constant; it is purely an entropy effect.

$$- dS = dS_{\text{orientation}} + dS_{\text{thermal}} = dS_{\text{orientation}} + C/T dT.$$

$$- dU = C dT + T dS = 0, \text{ implying that } dT = -T/C dS.$$

- Adiabatic stretching decreases orientation entropy and increases the temperature.
- The same model predicts the Curie law of paramagnetism, $M = CB/T$.
 - We have

$$M = N\mu \tanh \frac{\mu B}{k_B T}$$

$$M = \frac{N\mu^2}{k_B} \frac{B}{T}$$

where the second equation only holds for small B .

- Adiabatic demagnetization allows you to go from 4 K to 1 K using He_4 to He_3 liquefaction. Adiabatic demagnetization increases spin entropy and reduces the temperature.
 - To achieve 4 K, we let He_4 adiabatically expand, which makes it very cold. However, at temperatures below 4 K, He_4 is a liquid and it can no longer adiabatically expand like a gas.
 - To achieve temperatures lower than 4 K, you stick copper salt in a cryostat, subject it to a magnetic field, and cool it to 4 K with the above method. The magnet aligns the spins. When you take the salt out of the magnetic field, the spins will randomize entropically, but this takes energy. You use the lattice energy to raise the spin energy.
- The challenge of protein folding and structure determination.
 - We have $\Delta G = \Delta(H - TS)$.
 - Protein folding necessitates $\Delta S < 0$ (you are creating order). Thus, we must have $\Delta H < \Delta(TS) = T\Delta S$, i.e., the protein must adopt a very, very stable conformation.
 - Estimating ΔS :

$$\Delta S = k_B \ln W = k_B \ln 3^{100} = 914 \text{ J K}^{-1} \text{ mol}^{-1}$$

- Using **Levinthal's paradox**, we can estimate the number of possible configurations of a protein.
- Each segment (essentially a C–C bond) has about three dihedral angle possibilities for the segments at either end.
- Thus, for a protein that is 100 segments long, $W \approx 3^{100}$.
- At 300 K, $T\Delta S = 274 \text{ kJ/mol}$.
 - It doesn't take much of a temperature difference to alter or prevent protein folding.
- About 15 hydrogen bonds or a single disulfide bond is about 274 kJ/mol of energy, so we can find ways to stabilize proteins over the entropic barriers.
- Just recently, a UChicago grad student (who had been working with a UChicago professor who's been studying the protein folding problem for a long time) headed a team at Google that has an AI that looks like it will be able to solve the protein folding problem.
- **Levinthal's paradox:** The observation that finding the native folded state of a protein by a random search among all possible configurations can take an enormously long time. Yet proteins can fold in seconds or less.
- Real gases deviate from ideality due to molecular interactions.
- **Compressibility factor:** Denoted by z . Given by

$$z = \frac{P\bar{V}}{RT}$$

- The van der Waals equation of state (where \bar{V} is the molar volume):

$$\left(P + \frac{a}{\bar{V}^2}\right)(\bar{V} - b) = RT$$

- We can also rewrite this as

$$P = \frac{RT}{\bar{V} - b} - \frac{a}{\bar{V}^2}$$

- Note that $a, b \geq 0$.
- The compressibility is

$$z = \frac{\bar{V}}{\bar{V} - b} - \frac{a}{RT\bar{V}}$$

- The van der Waals equation of state is cubic in \bar{V} and can predict two different molar volumes (gas and liquid) for one pressure.

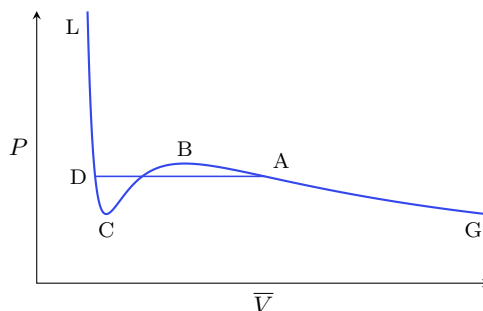


Figure 6.1: The van der Waals isotherm of CO_2 at 0°C .

- We have that

$$\begin{aligned}
 RT &= \left(P + \frac{a}{\bar{V}^2} \right) (\bar{V} - b) \\
 &= P\bar{V} - bP + \frac{a}{\bar{V}} - \frac{ab}{\bar{V}^2} \\
 \frac{RT\bar{V}^2}{P} &= \bar{V}^3 - b\bar{V}^2 + \frac{a}{P}\bar{V} - \frac{ab}{P} \\
 0 &= \bar{V}^3 - \left(b + \frac{RT}{P} \right) \bar{V}^2 + \frac{a}{P}\bar{V} - \frac{ab}{P}
 \end{aligned}$$

- Since it is cubic in \bar{V} , this means we can have up to three different molar volumes for one pressure.
- This also reflects the fact that as we compress a gas, it behaves ideally for a while, and then pressure is constant as condensation takes hold, and then we must apply massive amounts of pressure to make the volume any smaller.
- On \overline{AG} , the system is a gas. On \overline{LD} , it is a liquid. On \overline{AD} , pressure is constant as we compress more and more because condensation takes hold, so highly compressed gas molecules become liquid, reducing the pressure.
- Drawing the line \overline{AD} : The points at which gas stops and liquid starts must be at the same pressure.
- We must also have the area above and below the line equal (**Maxwell equal area construction**).
 - Phase equilibrium (like we have along \overline{AD}) means that free energy does not change. Mathematically, $\Delta G(A) = \Delta G(D)$.
 - If A and D represent gas and liquids at the same temperature, they are in equilibrium and they must have the same molar Gibbs free energy.
 - We have $dG = -S dT + V dP$.
 - Since T is constant (this is an isotherm), $dG = V dP$.
 - Thus, we can integrate along the curve \overline{DA} to find an appropriate \overline{DA} such that the integral is zero.

$$\begin{aligned}
 0 &= \Delta G(A) - \Delta G(D) \\
 &= \int_D^A dG \\
 &= \int_D^A V dP
 \end{aligned}$$

- See Problem 23-46 for the “Maxwell equal area construction rule.”

6.3 More van der Waals Phenomena

- 2/18:
- The cubic vdW equation of state predicts a critical point at T_c at and above which only one P for (V, T) solution is possible.
 - The behavior of isotherms around the critical temperature.
 - For isotherms below the critical temperature, there will be a range of volumes where the gas and liquid phases are in equilibrium.
 - For isotherms above the critical temperature, we only have the gas phase, so there is no region of constant pressure as we compress the system.
 - This means that at the critical temperature $T = T_c$, there will only be a single volume V_c and hence pressure P_c at which the gas and liquid phases are in equilibrium. Mathematically, this means that each of the three roots of the cubic van der Waals equation exist at the same point V_c , i.e., that the equation is of the form $(V - \bar{V}_c)^3$.

- Expanding, we have

$$\begin{aligned} 0 &= \bar{V}^3 - \left(b + \frac{RT}{P}\right) \bar{V}^2 + \frac{a}{P} \bar{V} - \frac{ab}{P} \\ &= \bar{V}^3 - 3\bar{V}_c \bar{V}^2 + 3\bar{V}_c^2 \bar{V} - \bar{V}_c^3 \end{aligned}$$

- Thus, at T_c ,

$$b + \frac{RT_c}{P_c} = 3\bar{V}_c \qquad \frac{a}{P_c} = 3\bar{V}_c^2 \qquad \frac{ab}{P_c} = \bar{V}_c^3$$

- One immediate consequence is that

$$\begin{aligned} \bar{V}_c^3 &= \frac{a}{P_c} \cdot b \\ \bar{V}_c^3 &= 3\bar{V}_c^2 b \\ \bar{V}_c &= 3b \end{aligned}$$

- Thus, the critical volume is on the order of magnitude of the molecular volume.
- Note that we can't manipulate the first equation into a different relation between \bar{V}_c and b using the ideal gas law substitution because this is a van der Waals gas.
- It follows that

$$\begin{aligned} 3\bar{V}_c^2 &= \frac{a}{P_c} & b + \frac{RT_c}{P_c} &= 3\bar{V}_c \\ P_c &= \frac{a}{3(3b)^2} & b + RT_c \cdot \frac{27b^2}{a} &= 3(3b) \\ P_c &= \frac{a}{27b^2} & T_c &= \frac{8a}{27Rb} \end{aligned}$$

- Thus,

$$z_c = \frac{P_c V_c}{RT_c} = \frac{3}{8}$$

- Indeed, the vdW equation predicts the compressibility at the critical point to be 3/8. The Redlich-Kwong predicts 1/3. The Peng-Robinson predicts 0.307. The experimental values are around 0.3. Water and ammonia deviate significantly: 0.23 and 0.24, respectively, due to their strong dipole moments/hydrogen bonding. Table 16.5 gives a lot of related data.
- Also, at T_c, V_c , we have that $(\partial P / \partial V)_T = 0$ and $\kappa \rightarrow \infty$ (recall that κ is the isothermal compressibility).
 - It follows from the vdW that $\kappa \propto (\bar{V} - \bar{V}_c)^{-1}$.
 - Experimental value: *Every* gas satisfies $\kappa \propto (\bar{V} - \bar{V}_c)^{-1.24}$.
 - The mystery was solved theoretically in the 1970s with renormalization group theory.
- Law of corresponding states.

- We define the relative pressure, volume, and temperature by

$$P_R = \frac{P}{P_c} \qquad V_R = \frac{V}{V_c} \qquad T_R = \frac{T}{T_c}$$

- Note that

$$\frac{RT}{P_c V_c} = \frac{RT_c}{P_c V_c} \frac{T}{T_c} = \frac{1}{z_c} \frac{T}{T_c} = \frac{8}{3} T_R$$

– Thus,

$$\begin{aligned} RT &= \left(P + \frac{a}{\bar{V}^2} \right) (\bar{V} - b) \\ &= \left(P + \frac{3\bar{V}_c^2 P_c}{\bar{V}_c^2} \right) \left(\bar{V} - \frac{\bar{V}_c}{3} \right) \\ \frac{RT}{P_c \bar{V}_c} &= \left(\frac{P}{P_c} + \frac{3\bar{V}_c^2}{\bar{V}} \right) \left(\frac{\bar{V}}{\bar{V}_c} - \frac{1}{3} \right) \\ \frac{8}{3} T_R &= \left(P_R + \frac{3}{\bar{V}_R^2} \right) \left(\bar{V}_R - \frac{1}{3} \right) \end{aligned}$$

- Virial expansion to experimentally determine the vdW coefficients a, b from the compressibility near ideal conditions.

– We let

$$z = 1 + \frac{B_{2V}(T)}{\bar{V}} + \frac{B_{3V}(T)}{\bar{V}^2} + \dots$$

where $B_{iV}(T)$ is the i^{th} **virial coefficient**.

– It follows that

$$\begin{aligned} \frac{P\bar{V}}{RT} &= \frac{\bar{V}}{\bar{V} - b} - \frac{a}{RT\bar{V}} \\ &= \frac{1}{1 - b/\bar{V}} - \frac{a}{RT\bar{V}} \\ &= 1 + \left(\frac{b}{\bar{V}} - \frac{a}{RT\bar{V}} \right) + \text{terms in } \frac{1}{\bar{V}^2} + \dots \end{aligned}$$

where we get from the second to the third line using the expansion

$$\frac{1}{1-x} = 1 + x + x^2 + \dots$$

– Thus,

$$B_{2V}(T) = b - \frac{a}{RT}$$

- Microscopic origin of the vdW coefficients from the interaction potential.

– Draws the interaction potential for a diatomic molecule.

■ The repulsion comes from the Fermi exclusion principle.

– Discusses dipole-induced dipole moments.

■ $-1/2 \propto E^2 \propto 1/r^6$.

– The origin of vdW (or London dispersion) interaction is quantum mechanical.

■ We use perturbation theory to calculate the interaction between two neighboring quantum dipoles.

$$\Delta E^{(1)} = \langle \psi_A^\circ \psi_B^\circ | H_{int} | \psi_A^\circ \psi_B^\circ \rangle = 0$$

■ Thus we need the second order correction:

$$\Delta E^{(2)} = - \sum_{ij} \frac{|\langle \psi_A^\circ \psi_B^\circ | H_{int} | \psi_A^i \psi_B^j \rangle|^2}{E_a^A + E_j^B - (E_0^A + E_0^B)} \approx - \frac{c}{r^6}$$

where $c \geq 0$.

6.4 Office Hours (PGS)

- Integrating along the curve in Figure 6.1?
 - Integrating along the curve with respect to P means (geometrically) that we take the area “under” (to the left of) the curve from A to C , then subtract the area under from C to B , and then add the area under from B to A . This calculation gets us overall the area of the bottom chunk as negative and the area of the top chunk as positive.

6.5 Chapter 16: The Properties of Gases

From McQuarrie and Simon (1997).

2/21:

- Outline:
 - Having studied ad nauseam the properties of individual atoms and molecules, we now turn our attention to systems consisting of large numbers of atoms and molecules.
 - The ideal gas equation is discussed, the van der Waals equation as the most famous extension of it, and then **virial expansions** as an even more systematic and accurate approach.
 - Relating virial coefficients to the intermolecular interaction energy reveals that deviations from ideal gas behavior provide great insight into molecular interactions.
- **Virial expansion:** An expression for the pressure of a gas as a polynomial in the density.
- **Ideal-gas equation of state:** An equation of state relating the pressure, volume, and temperature of a gas that is sufficiently dilute (i.e., with particles sufficiently far apart) for the intermolecular interactions to be negligible. *Given by*

$$PV = nRT$$

$$P\bar{V} = RT$$

- **Ideal gas:** A gas that obeys the ideal-gas equation of state.
 - All gases, regardless of the shape or size of the molecules or how the molecules interact with each other, obey behave ideally if they are sufficiently dilute.
 - “Experimentally, most gases satisfy [the ideal-gas equation of state] to approximately 1% at one atm and 0°C” (McQuarrie & Simon, 1997, p. 638).
- **Extensive quantity:** A quantity that is directly proportional to the size of the system in question. *Also known as* **extensive variable**.
- **Intensive quantity:** A quantity that does not depend on the size of the system in question. *Also known as* **intensive variable**.
- “If we divide an extensive quantity by the number of particles or the number of moles in a system, we obtain an intensive quantity” (McQuarrie & Simon, 1997, p. 638).
- **Liter:** A unit of volume. *Denoted by* **L**. *Given by*

$$1 \text{ L} = 1 \text{ dm}^3$$

- The SI unit of volume is m^3 , but liters are an acceptable unit of volume in the IUPAC system.
 - **Pascal:** The SI unit of pressure. *Denoted by* **Pa**. *Given by*
- $$1 \text{ Pa} = 1 \frac{\text{N}}{\text{m}^2} = 1 \frac{\text{kg}}{\text{m s}^2}$$
- “Pressure can be measured experimentally by observing how high a column of liquid (usually mercury) is supported by the gas” (McQuarrie & Simon, 1997, p. 638).

- If m is the mass of the liquid, g is the **gravitational acceleration constant**, A is the base area of the column, ρ is the density of the liquid, and h is the height of the column, then

$$P = \frac{F}{A} = \frac{mg}{A} = \frac{\rho h A g}{A} = \rho h g$$

- **Gravitational acceleration constant:** The acceleration of an object due to gravity at the surface of the Earth. *Denoted by g . Given by*

$$g = 9.8067 \frac{\text{m}}{\text{s}^2}$$

- The pressure exerted by a 76.000 cm column of mercury ($\rho(\text{Hg}) = 13.596 \text{ g cm}^{-3}$) is

$$\begin{aligned} P &= \rho g h \\ &= 1.0133 \times 10^6 \frac{\text{g}}{\text{cm s}^2} \\ &= 1.0133 \times 10^5 \frac{\text{kg}}{\text{m s}^2} \\ &= 1.0133 \times 10^5 \text{ Pa} \\ &= 101.33 \text{ kPa} \end{aligned}$$

- **Atmosphere:** The pressure that supports a 76.0 cm column of mercury. *Denoted by **atm**. Given by*

$$1 \text{ atm} = 101.325 \text{ kPa}$$

- **Bar:** The SI standard of pressure. *Denoted by **bar**. Given by*

$$1 \text{ bar} = 1 \times 10^5 \text{ Pa}$$

- **Torr:** The pressure that supports a 1.00 mm column of mercury. *Denoted by **torr**. Given by*

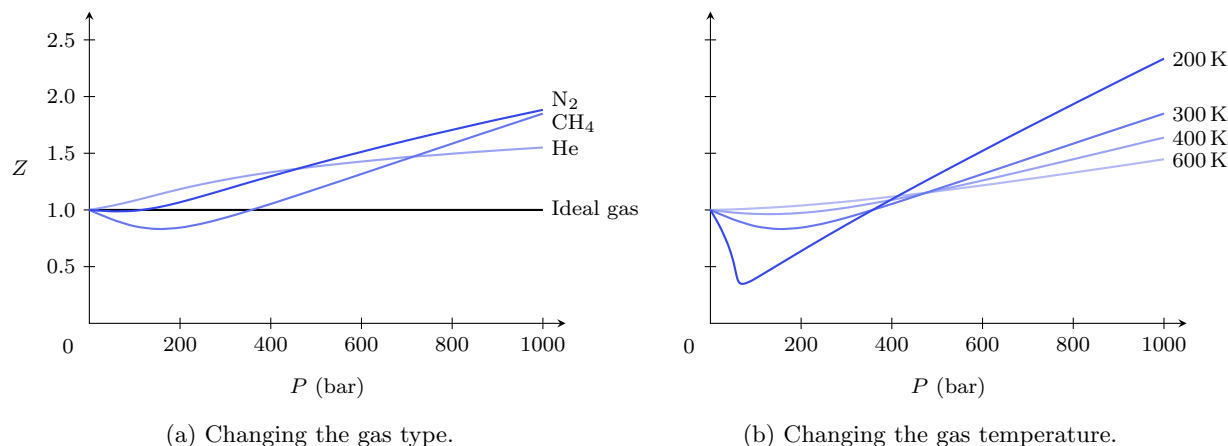
$$1 \text{ torr} = \frac{1}{760} \text{ atm}$$

- “Because we are experiencing a transition period between the widespread use of atm and torr on the one hand and the future use of bar and kPa on the other hand, students of physical chemistry must be proficient in both sets of pressure units” (McQuarrie & Simon, 1997, p. 639).
- Temperatures as low as $1 \times 10^{-7} \text{ K}$ and as high as $1 \times 10^8 \text{ K}$ have been achieved in the laboratory.
- **Triple point:** The point (P, V, T) at which all three of a given substance’s phases are in equilibrium.
- **Kelvin:** The SI unit of temperature, defined as $1/273.16$ of the temperature of the triple point of water. *Denoted by **K**.*
- “We will use the lower case t for $^{\circ}\text{C}$ and the upper case T for K ” (McQuarrie & Simon, 1997, p. 640).
- **Room temperature:** The temperature $25^{\circ}\text{C} = 298.15 \text{ K}$.
- If we plot $P\bar{V}$ vs. P for several gases at $T = 273.15 \text{ K}$, all the data can be extrapolated to a common value of $P\bar{V} = 22.414 \text{ L atm}$ as $P \rightarrow 0$. Thus,

$$\begin{aligned} R &= \frac{P\bar{V}}{T} = \frac{22.414 \text{ L atm}}{273.15 \text{ K}} = 0.082058 \frac{\text{L atm}}{\text{mol K}} \\ &= 8.3145 \frac{\text{J}}{\text{mol K}} \\ &= 0.083145 \frac{\text{L bar}}{\text{mol K}} \end{aligned}$$

- **Compressibility factor:** The following quantity. *Denoted by **Z**. Given by*

$$Z = \frac{P\bar{V}}{RT}$$



(a) Changing the gas type.

(b) Changing the gas temperature.

Figure 6.2: Plots of the compressibility factor vs. pressure.

- We use the compressibility factor, which is constant at 1 for an ideal gas, to visualize deviations from ideality for different gases (Figure 6.2a) at different temperatures (Figure 6.2b).
- At lower temperatures, intermolecular attraction takes hold, reducing the true volume and making $Z < 1$.
- At higher temperatures, molecules are moving fast enough to make negligible their attractions. Here, only repulsions due to their nonzero volume take hold at higher pressures.
- “The closer the gas is to the point at which it begins to liquify, the larger the deviations from ideal behavior will be” (McQuarrie & Simon, 1997, p. 642).
- **Van der Waals equation:** The most well known of the gaseous equations of state which account for intermolecular interactions. *Given by*

$$\left(P + \frac{a}{\bar{V}^2}\right)(\bar{V} - b) = RT$$

- Note that as $\bar{V} \rightarrow \infty$, the van der Waals equation becomes the ideal-gas equation of state.
- The van der Waals equation is also commonly written in the following form.

$$P = \frac{RT}{\bar{V} - b} - \frac{a}{\bar{V}^2}$$

- **Van der Waals constants:** The constants a, b in the van der Waals equation, whose value depend upon the particular gas.
 - We will see later that “the value of a reflects how strongly the molecules of a gas attract each other and the value of b reflects the size of the molecules” (McQuarrie & Simon, 1997, p. 643).
 - Table 16.3 lists van der Waals constants for various substances.
- The van der Waals equation approximates the behavior depicted in Figure 6.2 since

$$Z = \frac{P\bar{V}}{RT} = \frac{\bar{V}}{\bar{V} - b} - \frac{a}{RT\bar{V}}$$

- At high pressures ($\bar{V} \rightarrow 0$), the first term above dominates because $\bar{V} - b$ gets really small.
- At low pressures, the second term dominates.
- Notice that this also relates to the previously mentioned roles of a, b (e.g., at high pressures, the size of the molecules [and b] becomes significant).

- To solve the van der Waals equation for a molar volume given the other state variables, we must find the roots of a cubic equation via Newton's method.

$$\bar{V}^3 - \left(b + \frac{RT}{P}\right)\bar{V}^2 + \frac{a}{P}\bar{V} - \frac{ab}{P} = 0$$

- **Redlich-Kwong equation:** A relatively simple equation of state that is much more accurate than the van der Waals equation. *Given by*

$$P = \frac{RT}{\bar{V} - B} - \frac{A}{\bar{V}(\bar{V} + B)\sqrt{T}}$$

- Table 16.4 lists Redlich-Kwong parameters for various substances.
- As a cubic equation (Problem 16-26):

$$\bar{V}^3 - \frac{RT}{P}\bar{V}^2 - \left(B^2 + \frac{BRT}{P} - \frac{A}{P\sqrt{T}}\right)\bar{V} - \frac{AB}{P\sqrt{T}} = 0$$

- **Peng-Robinson equation:** Another relatively simple equation of state that is much more accurate than the van der Waals equation. *Given by*

$$P = \frac{RT}{\bar{V} - \beta} - \frac{\alpha}{\bar{V}(\bar{V} + \beta) + \beta(\bar{V} - \beta)}$$

- α is a somewhat complicated function of temperature, so α, β values are not listed.
- Problem 16-28 gives the Peng-Robinson equation as a cubic.
- As a general rule, the van der Waals equation fails beyond 200 bar while the Redlich-Kwong and Peng-Robinson equations remain nearly quantitative all the way into regions where the gas liquifies.
 - Additionally, the Peng-Robinson equation is better in the liquid-vapor phase transition region, and the Redlich-Kwong equation is better at higher pressures (these equations were actually constructed for these purposes).
- There exist many more sophisticated equations of state, some containing 10+ parameters, that can quantitatively reproduce experimental data over a wide range of state variables.
- A note on the drawing of Figure 6.2.
 - The curves in the figure were plotted with the Redlich-Kwong equation of state (since it is the one that most accurately depicts reality at high pressures).
 - To plot said curves, we need $Z(P)$. Much like with the van der Waals equation, we can write that

$$Z = \frac{P\bar{V}}{RT} = \frac{\bar{V}}{\bar{V} - B} - \frac{A\bar{V}}{RT\bar{V}(\bar{V} + B)\sqrt{T}}$$

- However, the above equation expresses Z as a function of \bar{V} , not P . Fortunately, we can solve the Redlich-Kwong equation for P using Cardano's formula.
- Comparing the cubic form of the Redlich-Kwong equation to the general cubic $ax^3 + bx^2 + cx + d = 0$ yields

$$a = 1 \quad b = -\frac{RT}{P} \quad c = \frac{A}{P\sqrt{T}} - \frac{BRT}{P} - B^2 \quad d = -\frac{AB}{P\sqrt{T}}$$

- We now depress $ax^3 + bx^2 + cx + d = 0$ into $t^3 + pt + q = 0$ via the substitutions

$$t = x + \frac{b}{3a} \quad p = \frac{3ac - b^2}{3a^2} \quad q = \frac{2b^3 - 9abc + 27a^2d}{27a^3}$$

- Since $4p^3 + 27q^2 > 0$ for all $P \in (0, 1000]$ (as we can verify graphically), the depressed cubic $t^3 + pt + q = 0$ has the real root

$$t = \sqrt[3]{-\frac{q}{2} + \sqrt{\frac{q^2}{4} + \frac{p^3}{27}}} + \sqrt[3]{-\frac{q}{2} - \sqrt{\frac{q^2}{4} + \frac{p^3}{27}}}$$

- It follows by returning the substitution for x that the original cubic has the real root

$$x = -\frac{b}{3a} + \sqrt[3]{-\frac{q}{2} + \sqrt{\frac{q^2}{4} + \frac{p^3}{27}}} + \sqrt[3]{-\frac{q}{2} - \sqrt{\frac{q^2}{4} + \frac{p^3}{27}}}$$

i.e., that the above equation provides values \bar{V} that make the Redlich-Kwong equation true for arbitrary P . In other words, the above equation equals $\bar{V}(P)$.

- It is a simple matter then to consider $Z(\bar{V}(P))$.

2/24:

- Equations of state that can be written as cubic equations in \bar{V} describe both the gaseous and the liquid regions of a substance.
- *PV*-diagram terminology. *Figure 16.7.*
- **Isotherm:** An experimentally determined plot of P as a function of \bar{V} at constant T .
- **Coexistence curve:** The curve on a *PV* diagram such that any point within the curve corresponds to liquid and gas coexisting in equilibrium with each other and any point on or outside the curve corresponds to only one phase.
- **Critical temperature:** The temperature above which a gas cannot be liquefied, regardless of the pressure. *Denoted by T_c .*
- **Critical point:** The point along the curve $P(\bar{V}, T_c)$ at which $\partial P / \partial \bar{V} = 0$.
 - The global maximum of the coexistence curve.
- **Critical pressure:** The pressure at the critical point. *Denoted by P_c .*
- **Critical volume:** The volume at the critical point. *Denoted by \bar{V}_c .*
- **Critical density:** The density of the system at the critical point.
- McQuarrie and Simon (1997) describes how pressure remains constant during a phase transition at a subcritical temperature.
- At the critical point, the meniscus between liquid and vapor disappears and both take on the same critical density.
- The spurious loops obtained from the van der Waals and Redlich-Kwong equation for $T < T_c$ (see Figure 6.1) result from the approximate nature of these equations of state.
 - However, the segment AB is a metastable region corresponding to the superheated vapor, the segment CD corresponds to the supercooled liquid, and the segment BC signifies an unstable region not observed for equilibrium systems.
- The **Maxwell equal-area construction** will be justified in Chapter 23.
- The three roots of the equations of state along isotherms for $T < T_c$.
 - A is the molar volume of the vapor in equilibrium.
 - D is the molar volume of the liquid in equilibrium.
 - The third root in the middle has no physical meaning.

- We can thus use our cubic equations of state to calculate the molar volume of the liquid and gas phases of a given substance.
 - Note that since it was designed to behave the best in the liquid region, the Peng-Robinson equation gives the best result here.
- Since the critical point is an inflection point along the isotherm corresponding to the critical temperature, we have that

$$\left(\frac{\partial P}{\partial \bar{V}}\right)_T = 0 \qquad \left(\frac{\partial^2 P}{\partial \bar{V}^2}\right)_T = 0$$

at it.

- We can use these conditions to derive the critical constants in terms of a and b .
- An easier way to derive said expressions, though, is to note that the cubic van der Waals equation has three real roots for $T < T_c$ and one real root (plus two complex roots) for $T > T_c$, so at $T = T_c$, all three of its roots merge into one, i.e., the equation is of the form $(\bar{V} - \bar{V}_c)^3 = 0$.
 - It follows by expanding the trinomial and comparing coefficients with the van der Waals equation written as a cubic that

$$3\bar{V}_c = b + \frac{RT_c}{P_c} \qquad 3V_c^2 = \frac{a}{P_c} \qquad \bar{V}_c^3 = \frac{ab}{P_c}$$

- It follows that

$$\bar{V}_c = 3b \qquad P_c = \frac{a}{27b^2} \qquad T_c = \frac{8a}{27bR}$$

- For the Redlich-Kwong equation,

$$\bar{V}_c = 3.8473B \qquad P_c = 0.029894 \frac{A^{2/3} R^{1/3}}{B^{5/3}} \qquad T_c = 0.34504 \left(\frac{A}{BR}\right)^{2/3}$$

- From the above equations, we can show that

$$\frac{P_c \bar{V}_c}{RT_c} = 0.375 \qquad \frac{P_c \bar{V}_c}{RT_c} = 0.333$$

where the left estimate is provided by the van der Waals equation and the right by the Redlich-Kwong equation.

- The significance is that both equations of state predict that the compressibility factor at the critical point is the same for all substances (there is no a, b or A, B dependence in the terms on the right of the equalities). However, there is a slight disparity in the predicted value of Z .
- While neither prediction is particularly quantitative (that of the Peng-Robinson is a bit more so), all three equations of state predict a constant Z . This prediction is borne out reasonably well by experimental data.
- **Law of corresponding states:** The properties of all gases are the same if we compare them under the same conditions relative to their critical point.
 - In particular, this means that gas properties are identical when their **reduced quantities** are equal.
- Note that in practice, the van der Waals and Redlich-Kwong constants are obtained from data at the critical point, not the other way around.
 - Also note that there is some ambiguity in how we do so, since there are three pieces of data (P_c, \bar{V}_c, T_c) describing a gas at the critical point but only two constants a, b or A, B .