Week 4

1/31:

Entropy and the Second Law of Thermodynamics

4.1 Entropy Equations

• We define a new state function S by $dS = \delta q_{rev}/T$ and call it **entropy**.

- See notes from last time for why this is a state function.

• Verify that the same definition of entropy is a state function for any system.

 Consider an ideal gas system in thermal equilibrium with an arbitrary system and drive the ideal gas system along a loop.

- Around the cycle: $\Delta S_{\text{total}} = 0$.

- Ideal gas:

$$\Delta S_{\text{total}} = \Delta S_1 + \Delta S_2$$

$$= \int \frac{\delta q_{\text{rev}_1}}{T} - \int \frac{\delta q_{\text{rev}_1}}{T}$$

$$= \int \frac{\delta q_{\text{rev}_1}}{T} + \int \frac{\delta q_{\text{rev}_2}}{T}$$

• We must devise a reversible process to calculate the entropy changes for an irreversible process leading to the same final state.



Figure 4.1: Two linked containers.

- Imagine two linked containers, one filled with n moles of gas and the other vacuumed.

- Opening the two containers to each other results in an adiabatic expansion. All vibrational/rotational energy of the molecules is consumed and used for translation.
- Measuring the temperature with spectroscopy (the Maxwell-Boltzmann distribution of each spectral line, plus only the ground rovibrational states are occupied now) shows a drastic drop in temperature.

- We have $\delta q = 0$ and $\delta w = 0$ so that dU = 0 and $\Delta T = 0$ overall?

- An isothermal expansion is a reversible process leading to the same final state.

- dU = 0 implies $\delta q_{rev} = -\delta w = P dV$.
- We have that

$$\Delta S = \int \frac{\delta q_{\rm rev}}{T} = \int_{V_0}^{2V_0} \frac{P \, dV}{T} = \int_{V_0}^{2V_0} \frac{nRT}{V} \frac{1}{T} \, dV = nR \ln 2$$

• Using entropy as a state function to predict the vapor pressure in equilibrium with its liquid, from the enthalpy at boiling and the boiling temperature.

Figure 4.2: Vapor pressure thermodynamic loop.

- Consider the above thermodynamic loop, where T is the temperature of the water and P is the pressure above the water.
- We have that

$$\Delta S_1 = \int_T^{T_b} \frac{C_{P_l}}{T} \, \mathrm{d}T \qquad \Delta S_2 = \frac{\Delta H_{\mathrm{vap}}}{T_b} \qquad \Delta S_3 = nR \ln \frac{P_0}{P} \qquad \Delta S_4 = \int_{T_b}^T \frac{C_{P_g}}{T} \, \mathrm{d}T$$

and that

$$\Delta S_0 = \frac{\Delta H_{\text{vap}}}{T}$$

– We know that ΔS around the loop is zero since S is a state function. We neglect the heat capacity effect. Thus,

$$\begin{split} \frac{\Delta H_{\mathrm{vap}}}{T_b} + nR \ln \frac{P_0}{P} - \frac{\Delta H_{\mathrm{vap}}}{T} &= 0 \\ \ln \frac{P_0}{P} &= \frac{\Delta H_{\mathrm{vap}}}{nR} \left(\frac{1}{T} - \frac{1}{T_b} \right) \\ P &= P_0 \mathrm{e}^{-\Delta H_{\mathrm{vap}}/nR(1/T - 1/T_b)} \end{split}$$

- The above equation gives the vapor pressure at T in terms of the vapor pressure P_0 at T_b .
- Trouton's rule: The statement that

$$\frac{\Delta H_{\rm vap}}{T_b} \approx 85 \pm 5 \, \mathrm{J} \, \mathrm{mol}^{-1} \, \mathrm{K}^{-1}$$

- Discovered this rule as an undergrad after an afternoon's manipulation of data from a book of tables.
- This rule reflects the fact that

$$\frac{\Delta H_{\text{vap}}}{T_b} = \Delta S_{\text{vap}}$$

and implies that ΔS_{vap} is approximately a constant.

• Example of entropy change: The direction of heat flow between two systems (1 and 2) only in thermal contact.

- We have

$$\delta q_{\text{rev}_1} = \delta q_{\text{rev}_2}$$

$$C_{V_1} \, dT_1 = -C_{V_2} \, dT_2$$

- Thus,

$$dS = dS_1 + dS_2$$

$$= \frac{\delta q_{\text{rev}_1}}{T_1} + \frac{\delta q_{\text{rev}_2}}{T_2}$$

$$= \frac{C_V dT_1}{T_1} - \frac{C_V dT_1}{T_2}$$

$$= C_V dT_1 \left(\frac{1}{T_1} - \frac{1}{T_2}\right)$$

- The conclusion is that if $dT_1 > 0$, then dS > 0. This is the spontaneous direction, the direction that nature chooses, the one in which entropy increases.
- The maximum of S is the equilibrium temperature between the two systems.
- Entropy change of the isothermal mixing of two ideal gases at the same temperature.
 - Consider the same two-container setup from Figure 4.1.
 - We have that

$$\Delta S = Rn_1 \ln \frac{V_1 + V_2}{V_1} + Rn_2 \ln \frac{V_1 + V_2}{V_2}$$

$$= R(n_1 + n_2) \left(\frac{n_1}{n_1 + n_2} \ln \frac{V_1 + V_2}{V_1} + \frac{n_2}{n_1 + n_2} \ln \frac{V_1 + V_2}{V_2} \right)$$

$$= R(n_1 + n_2) (-y_1 \ln y_1 - y_2 \ln y_2)$$

$$= R(n_1 + n_2) [-y_1 \ln y_1 - (1 - y_1) \ln(1 - y_1)]$$

- Note that $y_1 = n_1/(n_1 + n_2) = V_1/(V_1 + V_2)$ is the mole fraction, and similarly for y_2 .
- The conclusion is that $\Delta S > 0$.
- The maximum of ΔS is at $y_1 = y_2 = 1/2$.
- **Gibb's paradox**: Suppose you have the same gas on both sides of the containers. Then $\Delta S = nR \ln 2$ for an indistinguishable gas.
 - This is wrong.
 - Resolved by knowing that the gases *must* be distinguishable.