



# EN 410

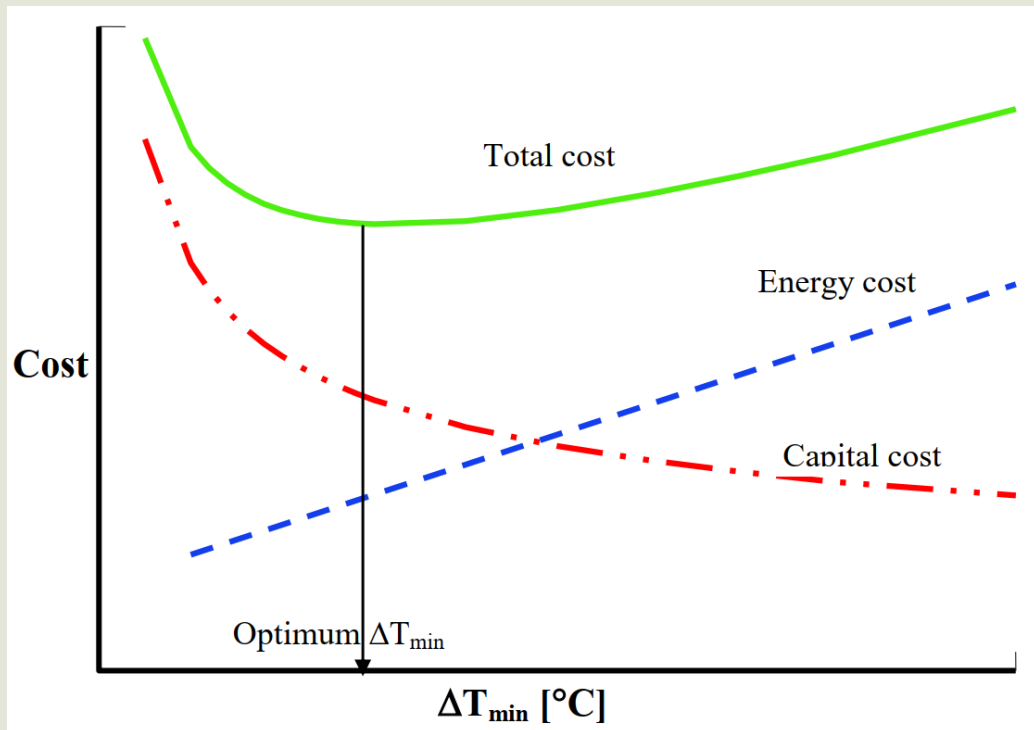
# Energy Management

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# Minimum temperature difference

$$Q = AU \Delta T_{lm}$$

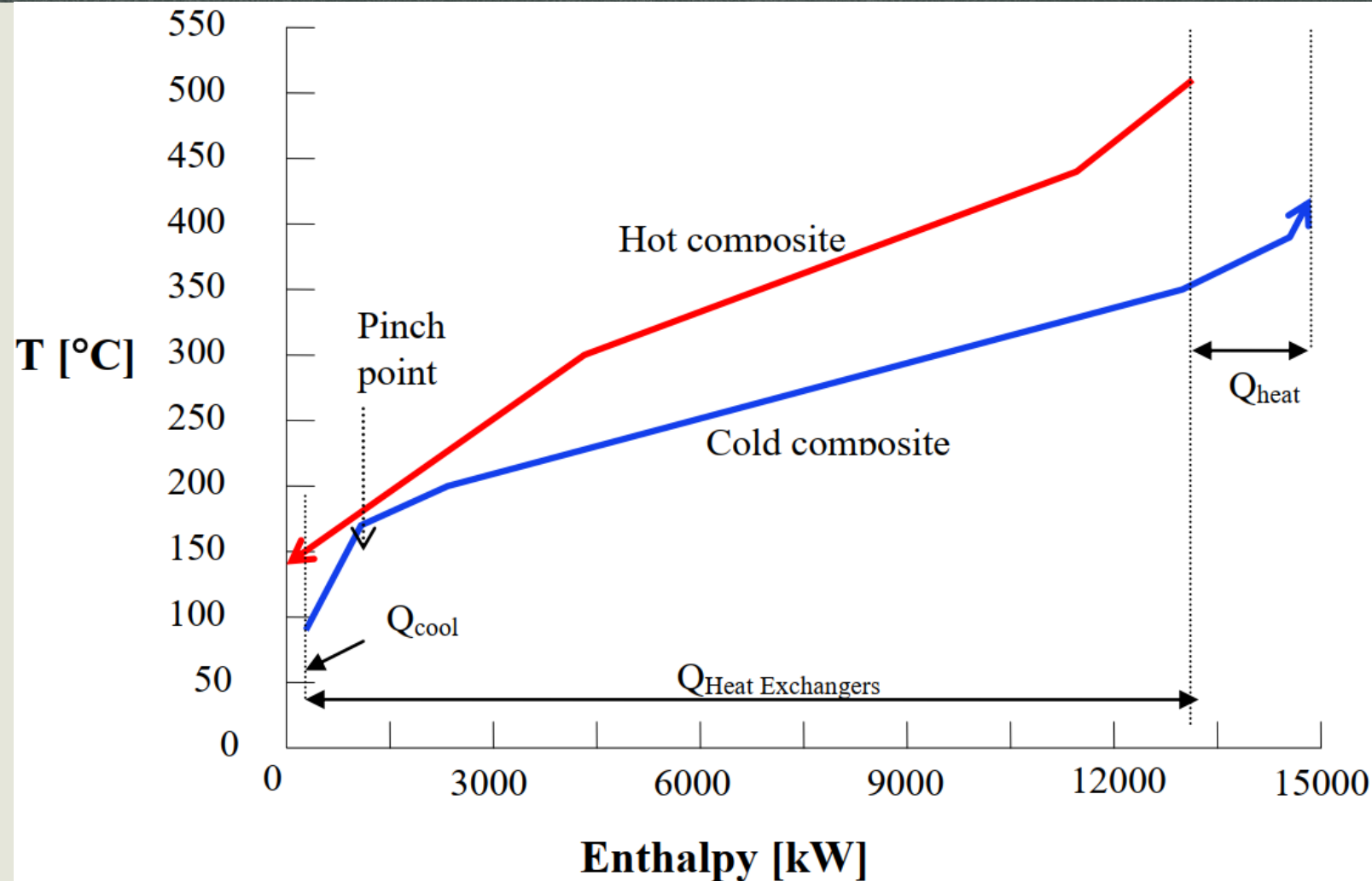
- Higher the  $\Delta T$  lesser the area, lesser the heat recovery, larger the external utilities
- Vice versa



Industrial Sector	Typical values for $\Delta T_{min}$
Low Temperature Process	3 – 5 °C
Chemical	10 – 20 °C
Petrochemical	10 – 20 °C
Oil Refinery	20 – 40 °C



# Composite curve for hot and cold streams



No heat transfer across pinch, otherwise the system needs more external utilities than the thermodynamic minimum

# Problem table approach

- $\Delta T_{\min} = 10^{\circ}\text{C}$
- Divide among the streams **or**
- Increase the cold stream temperature **or**
- **Decrease the hot stream temperature**

## 1. Estimate the new temp of streams

	Process stream type	Inlet temp	Outlet temp	Heat capacity rate	Q
	-	$^{\circ}\text{C}$	$^{\circ}\text{C}$	kW/K	kW
1	Cold	90	420	10	3300
2	Cold	170	350	32	5760
3	Cold	200	390	29	5510
4	Hot	440	140	27	8100
5	Hot	510	300	24	5040

	Process stream type	Inlet temp	Outlet temp	Heat capacity rate
	-	$^{\circ}\text{C}$	$^{\circ}\text{C}$	kW/K
1	Cold	90	420	10
2	Cold	170	350	32
3	Cold	200	390	29
4	Hot	430	130	27
5	Hot	500	290	24

# Problem table approach

## 2. Estimate the new temp intervals and Q

Interval Number	Temperature interval [°C]	Stream Numbers
1	500 – 430	5
2	430 – 420	4 + 5
3	420 – 390	1 + 4 + 5
4	390 – 350	1 + 3 + 4 + 5
5	350 – 290	1 + 2 + 3 + 4 + 5
6	290 – 200	1 + 2 + 3 + 4
7	200 – 170	1 + 2 + 4
8	170 – 130	1 + 4
9	130 – 90	1



# Estimate the energy availability

3. Estimate the excess energy in each interval

$$D_i = (T_i - T_{i+1}) \left[ \sum \left( \dot{m} C_p \right)_{cold} - \sum \left( \dot{m} C_p \right)_{hot} \right]$$

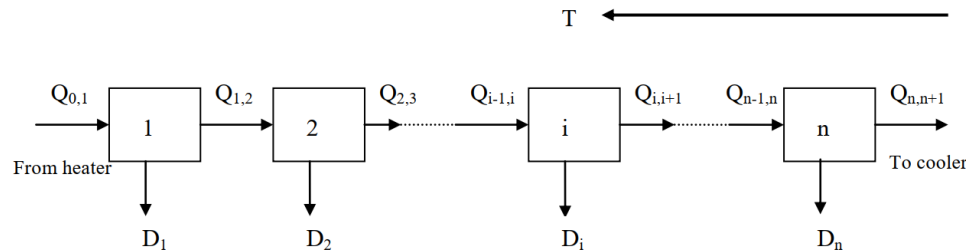
$D_i < 0 \Rightarrow$  need for cooling  
 $D_i > 0 \Rightarrow$  need for heating

Interval Number	Temperature interval [°C]	Stream Numbers	$D_i$
1	500 – 430	5	-1680
2	430 – 420	4 + 5	-510
3	420 – 390	1 + 4 + 5	-1230
4	390 – 350	1 + 3 + 4 + 5	-480
5	350 – 290	1 + 2 + 3 + 4 + 5	1200
6	290 – 200	1 + 2 + 3 + 4	3960
7	200 – 170	1 + 2 + 4	450
8	170 – 130	1 + 4	-680
9	130 – 90	1	400

	Process stream type	Heat capacity rate
	-	kW/K
1	Cold	10
2	Cold	32
3	Cold	29
4	Hot	27
5	Hot	24

# Estimate the sequential balance

4. Estimate the supplied heat to the each interval



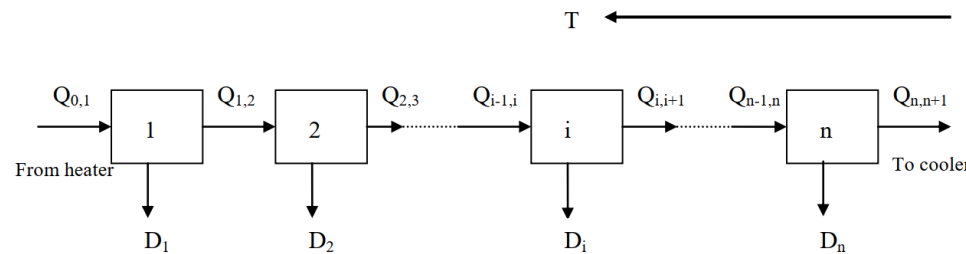
$$\dot{Q}_{i,i+1} = \dot{Q}_{i-1,i} - D_i$$

			Sequential Balance	
Interval	Temp. limits	$D_i$	$\dot{Q}_{i-1,i}$	$\dot{Q}_{i,i+1}$
1	500 – 430	-1680	0	1680
2	430 – 420	-510	1680	2190
3	420 – 390	-1230	2190	3420
4	390 – 350	-480	3420	3900
5	350 – 290	1200	3900	2700
6	290 – 200	3960	2700	-1260
7	200 – 170	450	-1260	-1710
8	170 – 130	-680	-1710	-1030
9	130 – 90	400	-1030	-1430

Minimum utility load which must be added to the network to avoid any deficit at lower intervals

# Problem table approach

5. Estimate the new supplied heat to the each interval, 1710 kW as load input in the interval 1



$$\dot{Q}_{i,i+1} = \dot{Q}_{i-1,i} - D_i$$

Interval	Temp. limits	$D_i$	Sequential Balance		Max Table	
			$\dot{Q}_{i-1,i}$	$\dot{Q}_{i,i+1}$	$\dot{Q}_{i-1,i}$	$\dot{Q}_{i,i+1}$
1	500 – 430	-1680	0	1680	<b>1710</b>	3390
2	430 – 420	-510	1680	2190	3390	3900
3	420 – 390	-1230	2190	3420	3900	5130
4	390 – 350	-480	3420	3900	5130	5610
5	350 – 290	1200	3900	2700	5610	4410
6	290 – 200	3960	2700	-1260	4410	450
7	200 – 170	450	-1260	-1710	450	<b>0</b>
8	170 – 130	-680	-1710	-1030	<b>0</b>	680
9	130 – 90	400	-1030	-1430	680	<b>280</b>

- Pinch temperature = 170°C (for cold = 170°C, hot = 180°C)
- Minimum heating utility = 1710 kW
- Minimum cooling utility = 280 kW



# Composite curve for hot and cold streams

