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# Thermodynamic descriptions of the Sb/Ge unary systems



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#### ABSTRACT

This paper focuses on the theoretical descriptions of the Gibbs energies concerning the unary systems of Antimony and Germanium. The Gibbs energy expressions of the vapor phase and the condensed phases are included in order to study the influences of temperature and pressure on the phase equilibrium status. The vapor phase is treated as a real solution of the constituent species by considering the fugacity coefficients of gas species in order to assure the reasonability of the P-T (Pressure-Temperature) diagrams at high pressure. The condensed phases are described in the light of the pressure dependent Murnaghan equation which is presented as a pressure dependent contribution G<sub>pres</sub> in the present work. The pressure correction factors for the condensed phases include the molar volume, the parameters of the variations of the thermal expansivity and the compressibility with temperature, and the variation of the bulk modulus with pressure. The related parameters of the vapor phase and all the condensed phases are thermodynamically optimized for Sb and Ge unary systems, on the basis of experimental measurements in literature. The calculated results of the P-T relations and the P-V (Pressure-Volume) curves agree well with the experimental data. The calculated slope of liquid-solid coexistence curve at the low pressure of the P-T phase diagram of Sb unary system follows Clausius-Clapeyron equation. The calculated heat capacity curves of condensed phases of Sb and Ge are analyzed and discussed to assure the reasonability of the thermodynamic models described in the paper. The present thermodynamic descriptions of both unary systems are of great benefit to the preparation process of the CoSb3-based thermoelectric materials, especially for the prevention of the volatilization of Sb containing vapor species and the determination of the sintering temperature under certain pressure.

# 1. Introduction

CoSb<sub>3</sub>-based Skutterudites refer to a certain kind of thermoelectric materials with a host of doping and substituting elements in the crystal lattice sites as well as in the cage-like intrinsic crystal voids. The substitution of Germanium for Antimony in the CoSb<sub>3</sub>-based Skutterudites may contribute to the enhancement of the thermoelectric properties [1–3]. In actual sintering process, the related pressure-temperature relations are greatly decisive to their phase equilibria and material preparation. At present, the thermodynamic parameters concerning the vapor phase and the condensed phases can be retrieved from PURE and SSUB databases of Thermo-Calc Software package, respectively [4]. However, the high pressure databases containing the pressure correction factors are relatively scarce according to the available literature reports.

This paper is intended to optimize the pressure-temperature phase diagrams for the unary systems of Sb and Ge, with the consideration of the pressure correction factors, so as to develop the related thermodynamic databases.

# 2. Thermodynamic models

# 2.1. The vapor phase

In terms of the vapor phases of Sb and Ge unary systems, the main species are Sb(g), Sb<sub>2</sub>(g), Sb<sub>3</sub>(g), Sb<sub>4</sub>(g) and Ge(g), Ge<sub>2</sub>(g), respectively [4]. In the present work, the real solution modeling is used for describing the Gibbs free energy of the vapor phase in order to assure the reasonability of the P-T diagram at high pressure, for the reason that the vapor phases will become thermodynamically stable at P > 10 GPa without considering the fugacity coefficients of vapor species for both unary systems. The Gibbs energy expression of the vapor phase is shown as the following:

$$G_m^{gas}(T) = \sum y_i [{}^{0}G_i^{gas}(T) + RT \ln(y_i) + RT \ln(f_i/P_0)]$$
 (1)

where  $y_i$  and  ${}^0G_i^{gas}(T)$  are the molar fraction and the molar Gibbs

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energy of the species i of the vapor phase taken from the SSUB substance database [4],  $P_0$  is the standard atmospheric pressure, R and T are the gas constant and temperature, and  $f_i = f_i(P,T)$  is the fugacity of vapor species i which can be several orders of magnitude higher than P when  $P > 1 \times 10^5$  Pa [5].

According to the previous literatures concerning the vapor fugacity, the fugacity coefficient  $\gamma = \frac{f}{p}$  and its relationship with pressure and temperature can be given as the following expression [5–7]:

$$ln\gamma = ln\left(\frac{f}{P}\right) = A \times \frac{P}{1 \times 10^5 Pa} + B \times \frac{P^2}{(1 \times 10^5 Pa)^2} (T \ge 298K)$$
 (2)

where A and B are parameters related to temperature, and the reasonable value of A and B should be relatively small in that f should infinitely approach to P at low pressures when  $P \le 1 \times 10^5$  Pa.

However, there exist no available literature report concerning the exact vapor species fugacity expressions of A and B of Sb, Sb<sub>2</sub>, Sb<sub>3</sub>, Sb<sub>4</sub> and Ge, Ge<sub>2</sub>. Particularly, the P-T relationships of Sb and Ge vapor phases are not reported at high pressures when  $P > 1 \times 10^5$  Pa and thus the related fugacities at high pressure are not available, either. So it is necessary to approximately estimate A and B of the fugacity expressions concerning the vapor species of Sb and Ge. Based on the fugacity study of nitrogen related systems [5–7], in the present optimization work, the expression form of A and B is taken from the aforementioned literatures:

$$M = \frac{M_1}{T} + \frac{M_2}{T^2} + \frac{M_3}{T^3} \tag{3}$$

where  $M_1$ ,  $M_2$  and  $M_3$  (M=A or B) are the undetermined coefficients on the basis of the experimental information of the vapor phase fugacity at high pressure. In terms of Sb and Ge unary systems, the following expressions are used for both Sb and Ge vapor species by analogy with nitrogen to reflect the variation of A and B with temperature approximately:

$$A = \frac{0.3926K}{T} - \frac{39.23K^2}{T^2} + \frac{2800K^3}{T^3}B = \frac{3.805 \times 10^{-6}K}{T} + \frac{0.00113K^2}{T^2} - \frac{0.07K^3}{T^3}$$
(4)

Provided that the fugacity coefficients of the vapor species of Sb and Ge are regarded as similar, Eq. (1) can be simplified as the following:

$$G_m^{gas}(T) = \sum_{i=1}^{n} y_i [{}^{0}G_i^{gas}(T) + RT \ln(y_i)] + RT \ln(f/P_0)$$
 (5)

After the approximate treatment of the parameters A and B for the Sb and Ge vapor phases, the P-T relationships are reasonable at both high and low pressure ranges. The precise expressions of A and B concerning the fugacity coefficients of Sb and Ge vapor species require further practical study and discussion in future research work.

# 2.2. The condensed phases

The Gibbs energy of a condensed phase containing a pure element depends on both temperature and pressure. The pressure dependence of the Gibbs energy can be expressed in the form of the Murnaghan equation [8]:

$$G_{pres} = \frac{A \exp(A_0 T + A_1 T^2 / 2 + A_2 T^3 / 3)}{(K_0 + K_1 T + K_2 T^2)(n - 1)} \{ [1 + nP(K_0 + K_1 T + K_2 T^2)]^{1 - 1/n} - 1 \}$$
(6)

where A represents the molar volume  $V_m = (\frac{\partial G_m}{\partial P})_T$  of the material at a temperature of 0 K and a pressure of 0 Pa; the parameters  $A_O$ ,  $A_I$ ,  $A_2$  and  $K_O$ ,  $K_I$ ,  $K_2$  indicate the variation of the volume thermal expansivity  $\alpha = \frac{1}{V_m}(\frac{\partial V_m}{\partial T})_P = A_0 + A_1T + A_2T^2$  and compressibility  $\kappa = -\frac{1}{V_m}(\frac{\partial V_m}{\partial P})_T = K_0 + K_1T + K_2T^2$  of the condensed phase as the functions of temperature at a pressure of 0 Pa; and the parameter n is the variation of the bulk modulus with pressure B(T,P) = B(T,0) + nP,

where B(T,P) represents the bulk modulus as the function of temperature and pressure and B(T,0) represents the bulk modulus at zero pressure. Taking the  $G_{pres}$  term into account, the Gibbs energy of a condensed phase containing a pure element can be expressed as the following:

$$G = a + bT + cT \ln(T) + dT^{2} + eT^{3} + fT^{-1} + gT^{7} + hT^{-9} + G_{pres}$$
 (7)

where a, b, c, d, e, f, g and h are the parameters of the Gibbs energy expression with no consideration of the pressure effect.

#### 3. Experimental data

#### 3.1. Antimony system

At  $P < 1 \times 10^5$  Pa, there exist Rhombo\_A7 Sb, liquid phase and vapor phase composed of Sb, Sb<sub>2</sub>, Sb<sub>3</sub> and Sb<sub>4</sub> in the Antimony system. In terms of the high pressure phase of Sb, there is an academic dispute over the crystal structure of this phase. Duggin [9] and Sasaki [10] suggested the crystal structure of the high pressure phase of Sb should be Tetragonal by analogy with As and Bi. Klement [11] determined the crystal structure of the high pressure phase of Sb and suggested the reasonable structure of this phase should be closely related to Bcc\_A2. However, most literatures [12–15] based on XRD method pointed out that the high pressure phase of Sb should be Monoclinic, which was derived from an orthorhombic SnS type structure. In the present optimization work, the crystal structure of the high pressure phase of Sb is regarded as Monoclinic.

The experimental data of the Antimony system is relatively abundant. Young [12] collected the unary phase diagram of Sb based on the experimental data from various literatures. Zhao [16] summarized the relationship between the saturated vapor pressure of Sb and temperature according to the original research reported by Russian experts. Besides, others [13,14,17-22] determined the phase boundaries of Rhombo\_A7 Sb, Monoclinic Sb and liquid by means of thermochemical analysis, including XRD (X-Ray Diffraction), ATD (Analysis of Thermal Desorption) and DSC (Differential Scanning Calorimeter). The triple point of the three-phase equilibrium of Rhombo\_A7, Monoclinic and liquid is 840 K at 5.7 GPa, while that of Rhombo\_A7, liquid and vapor is 903.7 K at 20.5 Pa [11,16]. Moreover, it is reported that the linear thermal expansivity and the compressibility data of Sb turn out to be 10.5×10<sup>-6</sup> /K and 23.535×10<sup>-12</sup> /Pa at 20 °C, respectively, and the molar volume of Rhombo\_A7 Sb at normal pressure and temperature is 1.75×10<sup>-5</sup> m<sup>3</sup>/ mol [23]. In terms of liquid Sb, similarly, the compressibility data of liquid Sb is 4.33×10<sup>-11</sup> /Pa at 1200 K according to sound velocity method [24]. These experimental data are used to evaluate the model parameters in the present work.

### 3.2. Germanium system

Germanium acts as a substitution element of Antimony in the  $CoSb_3$ -based materials. Compared with Sb, the experimental data of Ge are relatively scarce. There exist four phases in the Ge unary system, vapor phase, liquid phase, Diamond\_A4 Ge and Tetragonal Ge. The vapor phase is composed of species Ge and  $Ge_2[25]$ .

Young [12] described the high pressure condensed phase diagram of Ge based on available experimental data from literature. Menoni et al. [26], Vaidya et al. [27], Bundy [28] and Vohra et al. [29] determined the phase boundaries of Diamond\_A4 Ge, Tetragonal Ge and liquid using the thermal analysis including adiabatic calorimetry, levitation method and drop calorimetry, as well as the physical measurements including elastic compression test and bulk modulus test. The triple point of the three-phase equilibrium of liquid, Diamond\_A4 Ge and Tetragonal Ge, however, has not got an unanimous conclusion according to the existing report. Jayaraman [30] and

Yang [31] summarized the equilibrium relationship of these three phases, and suggested the possible triple point should be 800 K at 10.2 GPa. Vechten [32] pointed out that this triple point is about 835 K at 10.2 GPa based on Quantum Dielectric Theory. Young [12], Bundy [28] and Vohra [29] suggested the triple point be 820 K at 10.2 GPa according to their academic research. Based on all the literature reports above, this triple point is taken as 820 K at 10.2 GPa in the present optimization. No triple point concerning the three-phase equilibrium of Diamond A4 Ge, liquid and vapor was reported. Besides, the linear thermal expansivity and the volume compressibility data are  $6.0 \times 10^{-6}$ K and 12.93×10<sup>-12</sup> /Pa at 20 °C, respectively, and the molar volume of Diamond A4 Ge at normal pressure and temperature is 1.26×10<sup>-5</sup> m<sup>3</sup>/ mol [23]. Moreover, it is reported that the compressibility data of liquid Ge is 2.525×10<sup>-11</sup> /Pa at 1200K by means of sound velocity method and static method [33,34]. Analogous to Sb, these experimental data are used in the present optimization of the Ge unary system.

#### 4. Optimization results

#### 4.1. The Sb system

As mentioned above, in the present work, the high pressure phase of Sb is treated as Monoclinic. It is generally recognized that the four phases, Rhombo\_A7 Sb, Monoclinic Sb, liquid and gas, constitute the unary system of Antimony [9-22,35]. However, there exists no Monoclinic Sb in the SGTE Database. Consequently the model of this phase was constructed with the consideration of the reasonable change trend of its heat capacity at high pressures and temperatures. The parameters of the Gibbs energy expression of Monoclinic Sb were optimized on the basis of the low temperature part of GHSER<sub>Sb</sub>, named as GHSER<sub>Sb</sub>\_Low [36] as listed in Table 1, to assure the heat capacity curve smooth at high temperature. Based on the available experimental data, the optimization work was carried out by means of Pandat 2016 software [37]. All the optimized model parameters are given in Table 1. The fugacity coefficients of gas species,  $\gamma$ , are regarded as the same for Sb(g), Sb<sub>2</sub>(g), Sb<sub>3</sub>(g) and Sb<sub>4</sub>(g) approximately.

### 4.2. The Ge system

The four phases, Diamond\_A4 Ge, Tetragonal Ge, the liquid phase and the vapor phase, constitute the unary system of Germanium. The SGTE database gives expressions of all the four phases under atmospheric pressure. Because of the scarcity of the experimental data and the dispersivity of the data points for the *P-T* diagram of Ge at high pressure, the data reported by Ref. [12] are given a larger weight for its comprehensiveness of the collected data. All the obtained model parameters are given in Table 2. Analogous to Sb, the fugacity coefficients of vapor species are set the same value as mentioned in Section 2.1.

# 5. Analysis and discussion

# 5.1. Antimony system

The optimization results of Sb unary system include the phase diagrams of both the high and the low pressure ranges. In order to present the whole phase diagram and the partial enlarged diagram clearly, the  $\lg(P)$ -T diagram and the P-T diagram are shown in Fig. 1(a) and (b), respectively. The consistent results are obtained between the calculated results and the experimental data. The optimization results show that the triple point of the three-phase equilibrium of Rhombo\_A7 Sb, Monoclinic Sb and liquid is about 840 K at 5.66 GPa; and that of Rhombo\_A7, liquid and vapor is about 903.7 K at 20.3 Pa.

The Pressure-Volume diagram,  $P-V_m$  diagram, is of great significance to evaluate the pressure correction factors in the present

optimization work. The expression of the P- $V_m$  relationship can be given in the following equation:

$$V_m = \left(\frac{\partial G_m}{\partial P}\right)_T = \frac{A \exp(A_0 T + A_1 T^2 / 2)}{(1 + nPK_0)^{1/n}}$$
(8)

As for the optimized parameters for the Gibbs energy expressions of the solid phases, the molar volume of Rhombo\_A7 Sb at 0 K and 0 Pa, A\_rho, is 1.65×10<sup>-5</sup> m<sup>3</sup>/mol, and the real molar volume of Rhombo\_A7 at normal temperature and pressure is 1.75×10<sup>-5</sup> m<sup>3</sup>/ mol, which is closely matched with the theoretical molar volume at 0 K and 0 Pa. The main contributor of the volume thermal expansivity of the Rhombo A7 Sb,  $A_0$  rho, turns out to be  $3.01 \times 10^{-5}$  /K, while the reported linear thermal expansivity at 298 K is 1.05×10<sup>-5</sup> /K. These data follow closely the empirical law that the volume expansivity is about three times of the linear expansivity. Similarly, the main contributor of the volume compressibility of the Rhombo\_A7 Sb,  $K_{0}$ \_rho, is  $2.13\times10^{-11}$  /Pa, while the literature reported compressibility at 293 K is  $2.3535\times10^{-11}$  /Pa. In terms of the liquid phase, the calculated compressibility is  $4.76 \times 10^{-11}$  /Pa , while the literature reported compressibility at 1200K is about 4.33×10<sup>-11</sup> /Pa. These data are also closely matched with each other. Based on the available pressure correction factors, the  $P\text{-}V_m$  diagram and the  $P\text{-}V/V_O$  diagram of Rhombo\_A7 Sb and Monoclinic Sb are given in Fig. 2. The calculated results fit the experimental data [15] well.

Furthermore, the heat capacities of liquid Sb, Rhombo\_A7 Sb and Monoclinic Sb are discussed in the present paper, in order to evaluate the reasonability of their pressure correction factors. The related heat capacity curves are shown in Fig. 3. For Rhombo\_A7 Sb and liquid, with the purpose of evaluating the influence of G<sub>pres</sub> terms, the heat capacity data retrieved from Pure module of Thermo-Calc software without G<sub>pres</sub> terms are listed as a comparison. It is apparent that the  $G_{\mathrm{pres}}$  term almost makes no difference concerning the heat capacities at standard atmospheric pressure. For Monoclinic Sb, it is imperative that the heat capacity should be thermodynamically meaningful at the discussed temperature and pressure scope. Meanwhile, the heat capacity curve of Monoclinic Sb should converge to the heat capacity of the liquid phase at high temperature, in order to be consistent with the SGTE standard. Consequently, we used a piecewise function to describe the characteristic of its heat capacity curve, and the curve strictly converges to the heat capacity of the liquid phase when  $P=1\times10^5$  Pa, the value of which is 31.38 J/(mol.K). To investigate the reasonability of the heat capacity of Monoclinic Sb, the heat capacities of both 1×105 Pa and 8 GPa are given as a reciprocal comparison. The slightly descending of the heat capacity curve at 8 GPa may rely on the sharp ascending of  $G_{\rm pres}$  term of Monoclinic Sb at high pressures, which influences the stability of Monoclinic Sb at corresponding conditions. The data mentioned above show the reasonability of the unary database of Sb.

It is worth noting that the data concerning the solidification curve of Rhombo\_A7 Sb at low pressure is rarely reported. In the present work, the slope of the two-phase equilibrium curve of liquid and Rhombo\_A7 Sb at low pressure,  $\frac{dp}{dT}$ , is estimated according to Clausius-Clapeyron equation

$$\frac{dp}{dT} = \frac{\Delta H}{T_m \Delta V_m} \tag{9}$$

where  $\Delta H$  is the latent heat of sublimation of Sb,  $T_m$  the melting temperature,  $\Delta V_m$  the molar volume change in the solidification process which can be approximately calculated as the following:

$$\Delta V_m = \frac{M_{Sb}}{\rho_{Sb}} \times c_{Sb} \tag{10}$$

where  $M_{Sb}$  is the molar atomic weight of Sb,  $\rho_{Sb}$  the density, and  $c_{Sb}$  the volume contraction percentage during the solidification process. According to the literature report [38],  $\Delta H$ =19875.784 J/mol,

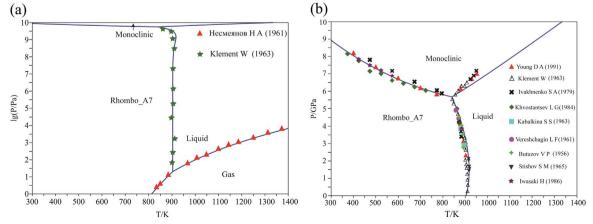
**Table 1**The optimized results of Antimony unary system.

Phase	Thermodynamic function	Pressure term/correction factor
Gas	$\ln \gamma = A \times \frac{P}{1 \times 10^5 Pa} + B \times \frac{P^2}{(1 \times 10^5 Pa)^2} (T \ge 298  K)$	
	· · · · · · · · · · · · · · · · · · ·	
	$A = \frac{0.3926K}{T} - \frac{39.23K^2}{T^2} + \frac{2800K^3}{T^3}B = \frac{3.805 \times 10^{-6}K}{T} + \frac{0.00113K^2}{T^2} - \frac{0.07K^3}{T^3}$	
	$\begin{cases} = +260807.82 - 37.9550038T - 21.27672T \ln T \end{cases}$	${}^{0}G_{Sb}^{Gas} = GGASSB + RT \ln(10^{-5} \times P) + RT \ln$
	$+5.524195 \times 10^{-4} \times T^2 - 1.05228767 \times 10^{-7} \times T^3$	
	$+9996.235 \times T^{-1}(298K < T < 1500K)$ $= +277520.519 - 132.229974T - 8.970999T \ln T$	
	$-0.0030704565T^2 + 5.21558333 \times 10^{-8} \times T^3$	
	$-3997436T^{-1}(1500K < T < 3200K)$	
	$GGASSB \begin{cases} = +220721.423 + 26.8449864T - 27.71232T \ln T \\ -7.8024 \times 10^{-4} \times T^2 + 2.46637333 \times 10^{-8} \times T^3 \end{cases}$	
	$ + 25565705T^{-1}(3200K < T < 5700K) $	
	$= +181935.295 + 193.241235T - 48.14252T \ln T$	
	$+0.0028203175T^2 - 8.119545 \times 10^{-8} \times T^3$	
	$+ 25871630T^{-1}(5700K < T < 9000K)$ = + 1141367.55-1326.1236T + 119.631T ln T	
	$-0.010240775T^2 + 1.09708933 \times 10^{-7} \times T^3$	
	$-1.0049905 \times 10^9 \times T^{-1}(9000K < T < 10000K)$	
Phase	Thermodynamic function	Pressure term/correction factor
	$ = + 225644.034 - 1.64062093T - 38.03868T \ln T $	${}^{0}G_{Sb2}^{Gas} = GGASSB2 + RT \ln(10^{-5} \times P) + RT \ln \gamma$
	$+5.08568 \times 10^{-4}T^{2} - 1.31408217 \times 10^{-7} \times T^{3} +60968.15T^{-1}(298K < T < 1700K)$	-
	$= +231514.886 - 6.69092891T - 38.05471T \ln T$	
	$+ 0.00253181T^2 - 4.26984 \times 10^{-7} \times T^3$	
	$GGASSB2$ $-2451004T^{-1}(1700K < T < 3400K)$	
	$= +569974.061 - 1288.56295T + 120.7968T \ln T  -0.030603185T^2 + 8.68664667 \times 10^{-7} \times T^3$	
	$-1.376966 \times 10^8 \times T^{-1}(3400K < T < 5700K)$	
	$= -689327.546 + 1714.84499T - 228.6644T \ln T$	
	$ + 0.012556505T^2 - 1.31793767 \times 10^{-7} \times T^3 $ $ + 7.14668 \times 10^8 \times T^{-1}(5700K < T < 6000K) $	
	$GGASSB3 = +277165.227 + 46.0530737T - 58.19257T \ln T$	O Gas
	$-2.0866265 \times 10^{-6} \times T^2 + 8.316025 \times 10^{-11} \times T^3$	${}^{0}G_{Sb_{3}}^{Gas} = GGASSB3 + RT \ln(10^{-5} \times P) + RT \ln r$
	$+\ 43601.08 \times T^{-1}(298K < T < 6000K)$	
	$GGASSB4 = +192849.585 + 194.765811T - 83.12392T \ln T$	${}^{0}G_{Sb4}^{Gas} = GGASSB4 + RT \ln(10^{-5} \times P) + RT \ln g$
	$-5.116865 \times 10^{-6} \times T^2 + 2.043415 \times 10^{-10} \times T^3 + 115767.85T^{-1}(298K < T < 6000K)$	
Liquid	$= + 19822.328 - 21.923164T + GHSER_{Sb}$	$Aliq = 1.636 \times 10^{-5}$
		•
	$ {}^{0}G_{Sb}^{Liq} = \begin{cases} -1.74847 \times 10^{-20} \times T^{7} + G_{pres}liq(298K < T < 903.7K) \\ = +8175.359 + 147.455986T - 31.38T \ln T \\ +G_{pres}liq(903.7K < T < 2000K) \end{cases} $	
	$\left( - \frac{1}{2000 \text{ K}} \right)$	$A_0 liq = 6.965 \times 10^{-5}$
		$A_1 liq = 6.915 \times 10^{-10}$
		$K_0 liq = 4.76 \times 10^{-11}$
		Nliq = 8
Rhombo_A7	${}^{0}G_{Sb}^{R \text{hom } boA7} = GHSER_{Sb} + G_{pres}rho$	$Arho = 1.65 \times 10^{-5}$
		$A_0 rho = 3.01 \times 10^{-5}$
		$A_1 rho = 1.26 \times 10^{-10}$
		$K_0 rho = 2.13 \times 10^{-11}$ N rho = 10
		11770 - 10
Monoclinic	$GHSER_{Sb}Low = -9242.858 + 156.154689T - 30.5130752T \ln T + 0.007748768T^2 - 3.003415 \times 10^{-6}T^3$	
	$+ 100625T^{-1} (298.15K < T < 6000K)$	
	$= +23056 - 56.96T + 4.86T \ln T$	$Amon = 1.675 \times 10^{-5}$
	$+8.56 \times 10^{-3}T^2 - 1.66 \times 10^{-7}T^3$	
	$G_{Sb}^{Monoclinic} \begin{cases} +300001 + 9.00 \times 10^{-27} + GHSER_{Sb}Low \\ +G_{pres}mon(298K < T < 1875K) \end{cases}$	
	${}^{0}G_{Sb}^{Monoclinic} = \begin{cases} +8.56 \times 10^{-3}T^{2} - 1.66 \times 10^{-7}T^{3} \\ +36000T^{-1} + 9.06 \times 10^{23}T^{-9} + GHSER_{Sb}Low \\ +G_{pres}mon(298K < T < 1875K) \\ = -1505.221457 + 170T - 31.38T \ln T \\ +G_{pres}mon(1875K < T < 5000K) \end{cases}$	
	( Spression (1010h 11 5000h)	$A_0 mon = 1.56 \times 10^{-5}$
		$A_1 mon = 8.62 \times 10^{-9}$
		$K_0 mon = 1.21 \times 10^{-10}$
		Nmon = 8

Table 2
The optimized results of Germanium unary system

Phase	Thermodynamic function	Pressure term/correction factor
Gas	$\ln \gamma = A \times \frac{P}{1 \times 10^5 Pa} + B \times \frac{P^2}{(1 \times 10^5 Pa)^2} (T \ge 298 K)$ $A = \frac{0.3926K}{T} - \frac{39.23K^2}{T^2} + \frac{2800K^3}{T^3}$ $B = \frac{3.805 \times 10^{-6} K}{T} + \frac{0.00113K^2}{T^2} - \frac{0.07K^3}{T^3}$	
	$GGASGE \begin{cases} = + 354205.659 + 120.562507T - 43.82842T \ln T \\ + 0.01399744T^2 - 1.669525 \times 10^{-6} \times T^3 \\ + 250845.65T^{-1}(298K < T < 1100K) \\ = + 373131.148 - 56.1903326T - 18.6573T \ln T \\ - 0.001064157T^2 + 4.18049833 \times 10^{-8} \times T^3 \\ - 2447580T^{-1}(1100K < T < 4900K) \\ = + 296853.328 + 145.237519T - 42.445872T \ln T \\ + 0.0023340125T^2 - 5.148525 \times 10^{-8} \times T^3 \\ + 44812690T^{-1}(4900K < T < 10000K) \end{cases}$	$^{0}G_{Ge}^{Gas} = GGASGE + RT \ln(10^{-5} \times P) + RT \ln \gamma$
	$GGASGE2 \begin{cases} = + 452821.305 + 129.510905T - 58.27585T \ln T \\ + 0.01555048T^2 - 2.367595 \times 10^{-6} \times T^3 \\ + 381719.4T^{-1}(298K < T < 900K) \\ = + 466026.197 - 21.0297748T - 36.10521T \ln T \\ - 0.0011553605T^2 + 1.43478617 \times 10^{-8} \times T^3 \\ - 1107859T^{-1}(900K < T < 4000K) \\ = + 448161.895 - 8.64280187T - 36.8412T \ln T \\0021332445T^2 + 8.26510333 \times 10^{-8} \times T^3 \\ + 14926150T^{-1}(4000K < T < 6000K) \end{cases}$	${}^{0}G_{Ge2}^{Gas} = GGASGE2 + RT \ln(10^{-5} \times P) + RT \ln \gamma$
Liquid	${}^{0}G_{Ge}^{Liq} \left\{ \begin{array}{l} = +\ 37141.49 - 30.687043T + GHSER_{Ge} \\ +\ 8.56632 \times 10^{-21} \times T^{7} + G_{pres}liq (298K < T < 900K) \\ = +\ 37141.489 - 30.687044T + GHSER_{Ge} \\ +\ 8.56632 \times 10^{-21} \times T^{7} + G_{pres}liq (900K < T < 1211.4K) \\ = +\ 27243.473 + 126.324186T - 27.6144T \ln T \\ +\ G_{pres}liq (1211.4K < T < 3200K) \end{array} \right.$	$Aliq = 9.676 \times 10^{-6}$ $A_0 liq = 3.56 \times 10^{-6}$ $A_1 liq = 6.01 \times 10^{-10}$ $K_0 liq = 2.61 \times 10^{-11}$ $N liq = 6$
Phase	Thermodynamic function	Pressure term/correction factor
Tetragonal	$\begin{cases} = +19313.847 + 149.135573T - 29.5337682T \ln T \end{cases}$	$Atet = 9.9 \times 10^{-6}$

Phase	Thermodynamic function	Pressure term/correction factor
Tetragonal	$ \begin{cases} = + 19313.847 + 149.135573T - 29.5337682T \ln T \\ + 0.00556829TT^2 - 1.513694 \times 10^{-6}T^3 \\ + 163298T^{-1} + G_{pres}tet(298K < T < 900K) \\ = + 23110.761 + 86.3608TT - 19.8536239T \ln T \\ - 0.003672527T^2 + G_{pres}tet(900K < T < 1211.4K) \\ = + 19251.796 + 140.208024T - 27.6144T \ln T \\ - 8.59809 \times 10^{28}T^{-9} + G_{pres}tet(1211.4K < T < 3000K) \end{cases} $	$Atet = 9.9 \times 10^{-6}$ $A_0tet = 1.27 \times 10^{-5}$ $A_1tet = 5.69 \times 10^{-9}$ $K_0tet = 5.56 \times 10^{-11}$ $Ntet = 5$
Diamond_A4	${}^{0}G_{Ge}^{Diamond} = GHSER_{Ge} + G_{pres}dia$	$Adia = 1.049 \times 10^{-5}$ $A_0 dia = 1.86 \times 10^{-5}$ $A_1 dia = 1.86 \times 10^{-9}$ $K_0 dia = 1.36 \times 10^{-11}$ $N dia = 5$



 $\textbf{Fig. 1.} \ \, \textbf{The optimized phase diagram of Sb system compared with experimental data: (a) The <math>\lg(P/Pa)-T/K$  global diagram; (b) The enlarged partial diagram.}

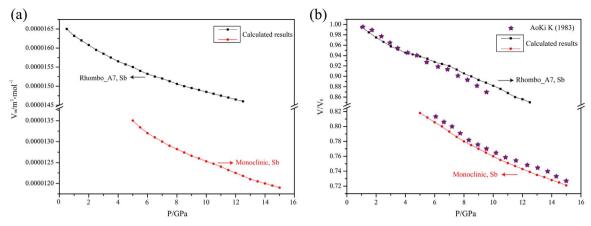


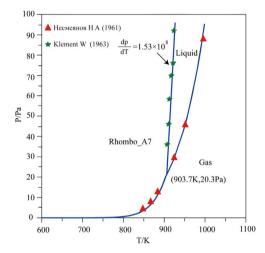
Fig. 2. The calculated Pressure-Volume diagrams of Rhombo\_A7 Sb and Monoclinic Sb: (a) The calculated  $P-V_m$  diagram; (b) The calculated  $P-V/V_O$  diagram compared with experimental data.

 $T_m$ =903.7 K,  $M_{Sb}$ =0.12175 kg/mol,  $\rho_{Sb}$ =6697 kg/m³, and  $c_{Sb}$ =0.79%, the calculated result shows that the slope of the two-phase equilibrium curve of the liquid and Rhombo\_A7 Sb is 1.53×10<sup>8</sup> Pa/K. This value is supported by the related literature [11] and is very close to the present calculation using the optimized thermodynamic parameters, as shown in Fig. 4.

#### 5.2. Germanium system

The experimental data of Ge unary system from literature are merely confined to high pressure ranging from 1 to 20 GPa. The  $\lg(P)$ -T and the P-T phase diagrams are shown in Fig. 5(a) and (b), respectively. The triple point of the three-phase equilibrium of Diamond\_A4 Ge, Tetragonal Ge and liquid is about 818 K at 10.1 GPa according to the present optimization result.

According to the optimized results, the molar volume of Diamond\_A4 Ge at 0 K and 0 Pa, A\_dia, is  $1.049\times10^{-5}\,\mathrm{m}^3/\mathrm{mol}$ , and the real molar volume of Diamond\_A4 Ge at normal temperature and pressure is  $1.26\times10^{-5}\,\mathrm{m}^3/\mathrm{mol}$ . The two values are approximate with each other. The main contributor of the volume thermal expansivity of Diamond\_A4 Ge, A\_dia, is  $1.86\times10^{-5}$  /K, while the reported linear thermal expansivity at 293 K is  $6.0\times10^{-6}$  /K, close to 1/3 of the volume thermal expansivity. Meanwhile, the main contributor of the compressibility of Diamond\_A4 Ge, K\_dia, is  $1.36\times10^{-11}$  /Pa, while the literature reported value of volume compressibility at 293 K is  $1.293\times10^{-11}$  /Pa. For liquid Ge, the calculated compressibility is  $2.61\times10^{-11}$  /Pa , while the literature reported compressibility at 1200 K is about  $2.525\times10^{-11}$  /Pa. With the available pressure correction factors, the  $P\text{-}V_m$  diagram and the  $P\text{-}V/V_O$  diagram of



 $\textbf{Fig. 4.} \ \textbf{The $P$-$T$ phase diagram of Sb at low pressure compared with experimental data}.$ 

Diamond\_A4 Ge and Tetragonal Ge are given in Fig. 6. The calculated results fit the experimental data [26,39] well.

Analogous to Sb, the heat capacities of liquid, Diamond\_A4 Ge and Tetragonal Ge are discussed in the present work, in order to evaluate the reasonability of the pressure correction factors concerning these three phases. The related heat capacity curves are shown in Fig. 7, in which the  $G_{\rm pres}$  term almost makes no difference concerning the heat capacities of liquid and Diamond\_A4 Ge at standard atmospheric pressure. In terms of Tetragonal Ge, the heat capacities of both  $1\times10^5$  Pa and 16 GPa are given in Fig. 7(b). The calculated results

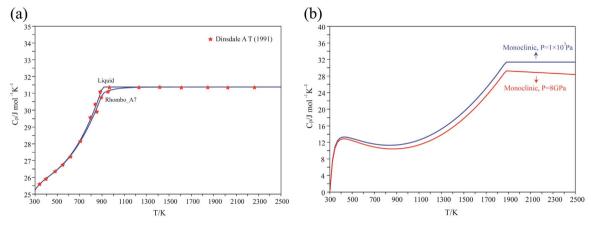


Fig. 3. The calculated heat capacity curves of liquid, Rhombo\_A7 Sb and Monoclinic Sb: (a) The calculated heat capacities of Rhombo\_A7 Sb and liquid Sb compared with model input; (b) The calculated heat capacities of Monoclinic Sb at P=1×10<sup>5</sup> Pa and 8 GPa.

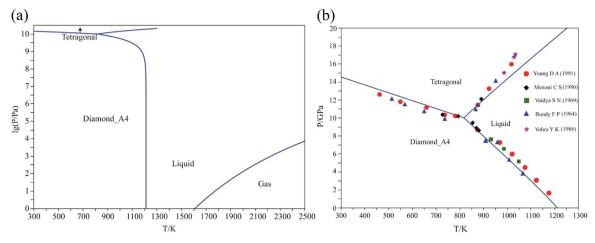


Fig. 5. The optimized phase diagram of Ge system compared with experimental data: (a) The lg(P/Pa)-T/K global diagram; (b) The enlarged partial diagram.

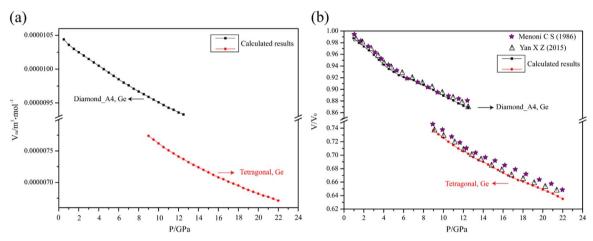


Fig. 6. The calculated Pressure-Volume diagrams of Diamond\_ A4 Ge and Tetragonal Ge: (a) The calculated P- $V_m$  diagram; (b) The calculated P- $V/V_O$  diagram compared with experimental data.

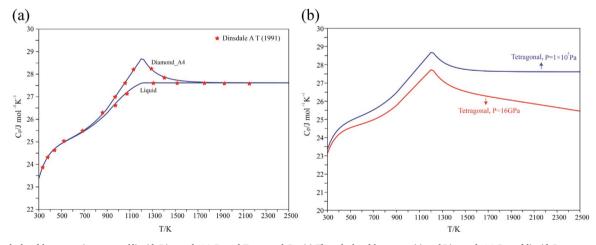


Fig. 7. The calculated heat capacity curves of liquid, Diamond\_A4 Ge and Tetragonal Ge: (a) The calculated heat capacities of Diamond\_A4 Ge and liquid Ge compared with model input; (b) The calculated heat capacities of Tetragonal Ge at P=1×10<sup>5</sup> Pa and 16 GPa.

mentioned above show the reasonability of the unary database of Ge.

# 5.3. The discussion of the application of the databases

The volatilization of Sb shows a prominent influence on the preparation of  $CoSb_3$ -based thermoelectric materials [40]. In the sintering process of the  $CoSb_3$ -based Skutterudites, the pressure condition is nearly vacuum or argon filled, and the temperature range

is controlled from 873 to 973 K or even lower [41–43] in case of the oxidation of the metal substrate. In the present work, the contributions of  $G_{\rm pres}$  of the condensed phases to the corresponding total Gibbs Energies are calculated, as shown in Figs. 8 and 9. Fig. 8 gives the variation of  $G_{\rm pres}$  with pressure at 298.15 and 2000 K, showing that when  $P < 10^8$  Pa, the  $G_{\rm pres}$  term is relatively small, while when P becomes to  $10^8$  Pa or even higher, the  $G_{\rm pres}$  term contributes so significantly that it can no longer be neglected. Fig. 9 gives the variation

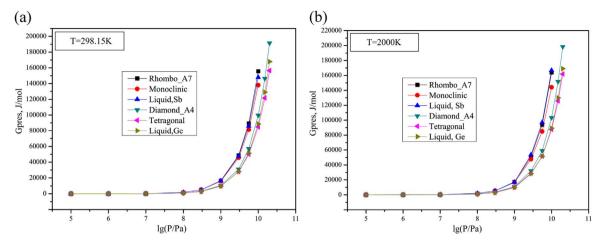


Fig. 8. The G<sub>pres</sub>-lg(P) relationship of Sb and Ge: (a) T=298.15 K; (b) T=2000 K.

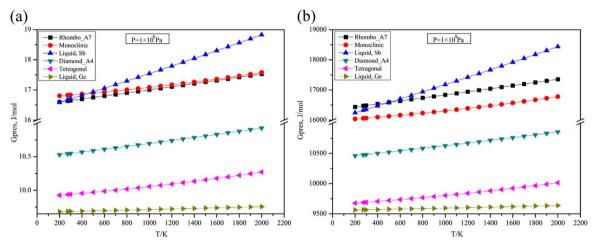


Fig. 9. The  $G_{\rm pres}$ -T relationship of Sb and Ge: (a)  $P=10^6$  Pa; (b)  $P=10^9$  Pa.

of  $G_{\rm pres}$  with temperature at  $10^6$  and  $10^9$  Pa, and it can be noticed that the influence of T on  $G_{\rm pres}$  term takes on a monotone increasing trend with the increase of temperature. Taking account of both P and T, it can draw a conclusion that the  $G_{\rm pres}$  term can no longer be neglected when P and T become high enough.

It is the theoretical law that the saturated vapor pressure of a certain substance increases with the ascending of temperature. For this reason, the sintering temperature cannot be set too high to reach a high saturated vapor pressure and a high pyrolysis of the substance. However, the sintering temperature cannot be set too low either to increase the difficulty caused by atomic diffusion and reaction kinetics to merely guarantee the high vacuum during the sintering process. Thus, it can be suggested that a number of Sb particles be added when the CoSb<sub>3</sub>-based Skutterudites are sealed in the closed environment. The Sb particles may decompose and volatilize, and the vapor species, Sb(g), Sb<sub>2</sub>(g), Sb<sub>3</sub>(g) and Sb<sub>4</sub>(g), may contribute to the increase of the system pressure and to the prevention of the volatilization of Sb in the CoSb<sub>3</sub>-based substrate. Containing the Gibbs energy parameters of Sb and Ge for the vapor phase and the condensed phases, the thermodynamic database of the CoSb<sub>3</sub>-based materials will be helpful to calculate the added amount of Sb particles in the sintering process, and be more important to analyze the phase equilibrium relations under different temperatures and pressures as well.

#### 6. Conclusions

The Gibbs energy expressions of the unary systems of Antimony and Germanium including the fugacity coefficients of the vapor phases

and the pressure correction factors for the condensed phases are thermodynamically optimized. The experimental results, especially the data concerning the molar volume, the volume thermal expansivity and compressibility of both elements, serve as the vital reference basis in the optimization process. Using the thermodynamic data obtained in the present work, the two-phase equilibrium curves, the three-phase equilibrium points and the P-T phase diagrams are calculated. The calculated slope of the two-phase equilibrium curve of liquid and Rhombo\_A7 Sb at low pressure follows Clausius-Clapeyron equation. The calculated phase diagrams and the Pressure-Volume curves agree well with the experimental phase equilibrium data. Meanwhile, the heat capacities of the calculation results are thermodynamically meaningful at the discussed temperature and pressure scope. The thermodynamic data of the unary systems of Sb and Ge can provide an essential basis for the thermodynamic database of the CoSb<sub>3</sub>-based thermoelectric materials. In addition, the form of  $G_{\mathrm{pres}}$  model used in the present work can be widely used when other unary systems associated with the pressure dependent condensed phases are concerned.

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#### Appendix A. Supplementary material

Supplementary data associated with this article can be found in the online version at http://dx.doi.org/10.1016/j.calphad.2016.11.007.

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