A Numerical Solution to the Convergent-Divergent Nozzle Using the McCormack Method

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Abstract

The problem of the Convergent-Divergent Nozzle is treated as a quasi-one dimensional flow problem. While a closed form solution exists for the problem, the aim will be to generate a sufficiently accurate numerical solution of a suitable form of the Navier–Stokes equations using a finite difference technique.

1 Problem Description

We consider an isentropic flow through a converging-diverging nozzle. The flow originates from a reservoir of large area A which results in a small value of velocity V, hence the pressure P_0 and temperature T_0 at the inlet are the stagnation values, the velocity here is in the subsonic region. The flow passes through the throat, where the flow is in a sonic state at the point of minimum cross-sectional area A^* , having pressure P^* and temperature T^* .

The flow now proceeds to the divergent part of the nozzle where the velocity of the flow is supersonic causing a shock. The flow exits with parameters, P_e , T_e , ρ_e . The variation is of the parameters with respect to space, at steady state is to be determined.

Anderson [1995] Anderson [1982]

2 Analytical Solution

The Analytical Solution is obtained using the Navier-Stokes equation, the equation of state and relation between enthalpy and temperature for a perfect gas. The area mach number relation (Equation 1) is used to determine the relation between flow speed and cross sectional area. Anderson [1982]

$$\left(\frac{A}{A^*}\right)^2 = \frac{1}{M^2} \left[\frac{2}{\gamma + 1} \left(1 + \frac{\gamma - 1}{2} M \right) \right]^{\frac{\gamma + 1}{\gamma - 1}} \tag{1}$$

$$\frac{P}{P_0} = \left(1 + \frac{\gamma - 1}{2}M^2\right)^{\frac{\gamma}{\gamma - 1}} \tag{2}$$

$$\frac{\rho}{\rho_0} = \left(1 + \frac{\gamma - 1}{2}M^2\right)^{\frac{-1}{\gamma - 1}} \tag{3}$$

$$\frac{T}{T_0} = \left(1 + \frac{\gamma - 1}{2}M^2\right)^{-1} \tag{4}$$

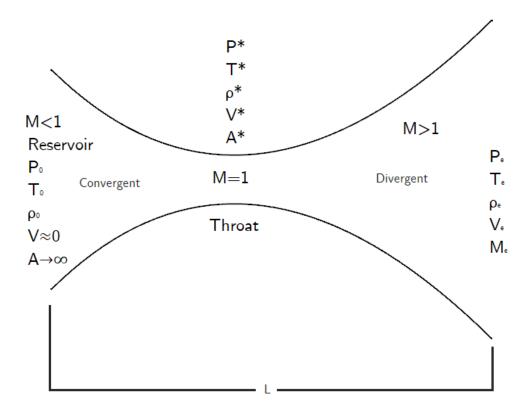


Figure 1: A Converging Diverging Nozzle.

3 Numerical Solution

The differential equations pertaining to the flow are derived using the integral form of the Navier-Stokes equations, the equation of state and the energy relation on a control volume of infinitesimal size. The obtained differential equations are further made dimensionless (Table 1).

Anderson [1995], Joseph W. Connolly

Note: a represents the speed of sound, a_0 represents the speed of sound in the reservoir.

The Dimensionless Differential Equations:

$$\frac{\partial \rho'}{\partial t'} = -\rho' \frac{\partial V'}{\partial x'} - \rho' V' \frac{\partial \ln A'}{\partial x'} - V' \frac{\partial \rho}{\partial x'}$$

$$\tag{5}$$

$$\frac{\partial V'}{\partial t'} = -V' \frac{\partial V'}{\partial x'} - \frac{1}{\gamma} \left(\frac{\partial T'}{\partial x'} + \frac{T'}{\rho'} \frac{\partial \rho'}{\partial x'} \right) \tag{6}$$

$$\frac{\partial T'}{\partial t'} = -V' \frac{\partial T'}{\partial x'} - (\gamma - 1)T' \left(\frac{\partial V'}{\partial x'} + V' \frac{\partial \ln(A')}{\partial x'} \right) \tag{7}$$

The McCormack Method: Anderson [1995]

The McCormack method is a conditionally stable explicit method to solve hyperbolic partial differential equations. It is accurate to the second order Consider a quantity u to be approximated, i represents the spatial coordinate while t represents the time coordinate.

Table 1: Substitution for the Dimensionless Differential Equation

Quantity	Substitution
T'	$\frac{T}{T_0}$
ho'	$\frac{\rho}{\rho}$
$egin{array}{c} ho' \ x' \end{array}$	$rac{\overline{T_0}}{\dfrac{ ho}{ ho_0}} rac{x}{L}$
a_0	$\sqrt{\gamma RT_0}$
V'	$\frac{V}{a_0}$
t'	$rac{\overline{a_0}}{t} \over L/a_0$
A'	$\frac{A}{A*}$

 $\left(\frac{\partial u}{\partial t}\right)_i^t$ is calculated from its differential differential equation using a **forward difference scheme**

$$\bar{u}_i^{t+\Delta t} = u_i^t + \left(\frac{\partial u}{\partial t}\right)_i^t \Delta t \tag{8}$$

 $\frac{\partial \bar{u_i}}{\partial t}^{t+\Delta t}$ is calculated using a rearward difference scheme

$$\left[\left(\frac{\partial u}{\partial t} \right)_i^t \right]_{avg} = 0.5 \left(\left(\frac{\partial u}{\partial t} \right)_i^t + \left(\frac{\partial \bar{u}}{\partial t} \right)_i^{t+\Delta t} \right) \tag{9}$$

Note: Consider $\left(\frac{\partial u}{\partial t}\right)_i^t$ and $\frac{\partial u_i^t}{\partial t}$ as equivalent notation

$$u_i^{t+\Delta t} = u_i^t + \left[\left(\frac{\partial u}{\partial t} \right)_i^t \right]_{avg} \Delta t \tag{10}$$

The above quantity is marched in time and the solution is updated until steady state is reached. The above method is applied to the density, the velocity and the temperature of our Nozzle simultaneously.

$$\frac{\partial \rho_i^t}{\partial t} = -\rho_i^t \frac{V_{i+1}^t - V_i^t}{dx} - \rho_i^t V_i^t \frac{\ln A_{i+1}^t - \ln A_{i-1}^t}{dx} - V_i^t \frac{\rho_i^t - \rho_{i-1}^t}{dx}$$
(11)

$$\frac{\partial V_i^t}{\partial t} = -V_i^t \frac{V_{i+1}^t - V_i^t}{dx} - \frac{1}{\gamma} \left(\frac{T_{i+1}^t - T_i^t}{dx} + \frac{T_i^t}{\rho_i^t} \frac{\rho_{i+1}^t - \rho_i^t}{dx} \right)$$
(12)

$$\frac{\partial T_i^t}{\partial t} = -V_i^t \frac{T_{i+1}^t - T_i^t}{dx} - (\gamma - 1)T_i^t \left(\frac{V_{i+1}^t - V_i^t}{dx} + V_i^t \frac{\ln A_{i+1}^t - \ln A_i^t}{dx} \right) \tag{13}$$

Naive Prediction:

$$\bar{\rho}_i^{t+\Delta t} = \rho_i^t + \left(\frac{\partial \rho}{\partial t}\right)_i^t \Delta t \tag{14}$$

$$\bar{V}_i^{t+\Delta t} = V_i^t + \left(\frac{\partial V}{\partial t}\right)_i^t \Delta t \tag{15}$$

$$\bar{T}_i^{t+\Delta T} = T_i^t + \left(\frac{\partial T}{\partial t}\right)_i^t \Delta t \tag{16}$$

$$\frac{\partial \bar{\rho}_{i}^{t}}{\partial t} = -\bar{\rho}_{i}^{t} \frac{\bar{V}_{i}^{t} - \bar{V}_{i-1}^{t}}{dx} - \rho_{i}^{t} \bar{V}_{i}^{t} \frac{\ln A_{i}^{t} - \ln A_{i-1}^{t}}{dx} - \bar{V}_{i}^{t} \frac{\bar{\rho}_{i}^{t} - \bar{\rho}_{i-1}^{t}}{dx}$$
(17)

$$\frac{\partial \bar{V}_i^t}{\partial t} = -\bar{V}_i^t \frac{\bar{V}_i^t - \bar{V}_{i-1}^t}{dx} - \frac{1}{\gamma} \left(\frac{\bar{T}_i^t - \bar{T}_{i-1}^t}{dx} + \frac{\bar{T}_i^t}{\bar{\rho}_i^t} \frac{\bar{\rho}_i^t - \bar{\rho}_{i-1}^t}{dx} \right) \tag{18}$$

$$\frac{\partial \bar{T}_{i}^{t}}{\partial t} = -\bar{V}_{i}^{t} \frac{\bar{T}_{i}^{t} - \bar{T}_{i-1}^{t}}{dx} - (\gamma - 1)\bar{T}_{i}^{t} \left(\frac{\bar{V}_{i}^{t} - \bar{V}_{i-1}^{t}}{dx} + \bar{V}_{i}^{t} \frac{\ln A_{i}^{t} - \ln A_{i-1}^{t}}{dx} \right)$$
(19)

Corrector:

$$\left[\left(\frac{\partial \rho}{\partial t} \right)_{i}^{t} \right]_{avq} = 0.5 \left(\frac{\partial \rho_{i}^{t}}{\partial t} + \frac{\partial \bar{\rho}_{i}}{\partial t}^{t+\Delta t} \right)$$
 (20)

$$\left[\left(\frac{\partial V}{\partial t} \right)_{i}^{t} \right]_{avq} = 0.5 \left(\frac{\partial V_{i}^{t}}{\partial t} + \frac{\partial \bar{V}_{i}^{t+\Delta t}}{\partial t} \right) \tag{21}$$

$$\left[\left(\frac{\partial T}{\partial t} \right)_{i}^{t} \right]_{avg} = 0.5 \left(\frac{\partial T_{i}^{t}}{\partial t} + \frac{\partial \bar{T}_{i}^{t+\Delta t}}{\partial t} \right)$$
 (22)

Final Update:

$$\rho_i^{t+\Delta t} = \rho_i^t + \left[\left(\frac{\partial \rho}{\partial t} \right)_i^t \right]_{avg} \Delta t \tag{23}$$

$$V_i^{t+\Delta t} = V_i^t + \left[\left(\frac{\partial V}{\partial t} \right)_i^t \right]_{ava} \Delta t \tag{24}$$

$$T_i^{t+\Delta t} = T_i^t + \left[\left(\frac{\partial T}{\partial t} \right)_i^t \right]_{avg} \Delta t \tag{25}$$

Determining The Time Step(Δt): The McCormack Method is conditionally stable and the time-step to be taken for stability is given by the Courant–Friedrichs–Lewy(CFL) condition. While the CFL criterion hold true for linear hyperbolic partial differential equations, it serves as a estimate for non-linear hyperbolic partial differential equations.

Anderson [1995]

On a given iteration at time t, the time-step to be taken is given by: In order to ensure stability at all spatial locations the common time-step taken is the minimum of the time-steps calculated at all the points.

$$\Delta t = \min(\Delta t_1^t, \Delta t_2^t, ..., \Delta t_n^t) \tag{26}$$

Where:

$$\Delta t_i^t = C \frac{\Delta x}{a_i^t + V_i^t}$$

C is the Courant Number, for a stable convergence, it is less than one .**The non-dimensional** speed of sound is given by \sqrt{T}

Boundary Conditions: Joseph W. Connolly

The area of the inlet of the nozzle is considered to be finite in our solution, this means that out

inlet is not a reservoir but rather a subsonic inlet. At the subsonic inlet two flow variables are kept constant while the velocity kept floating and is extrapolated along a characteristic line.

At the exit of the nozzle the flow reaches supersonic conditions. Here all three flow variables are made to float and the exit values are extrapolated along the characteristic line.

4 Implementation

The above Numerical Method is implemented in MATLAB, with appropriate initialization to ensure a smoother convergence. The three flow variables under iteration are initialized as follows: Anderson [1995]

$$\rho = 1 - 0.3146x$$

$$T = 1 - 0.2314x$$

$$V = (0.1 + 1.09x)T^{\frac{1}{2}}$$

The area of the Nozzle:

$$A = 1 + 2.2(x - 1.5)^2$$

This function intitalizes the flow variables according to the above relations.

```
1 function[density,temperature,velocity] = initialize_flow_variables(spacesteps,
     timesteps,delta_x)
      %Create Placeholder
      density = zeros(timesteps, spacesteps);
      temperature = zeros(timesteps, spacesteps);
      velocity = zeros(timesteps, spacesteps);
5
6
      %Create intial values which help with better convergence
9
      for i = 1:spacesteps
          x = (i-1)*delta_x;
          density(1,i) = 1-(0.3146*x);
          temperature(1,i) = 1-(0.2314*x);
12
          velocity(1,i) = (0.1+(1.09*x)).*(temperature(1,i)).^0.5;
14
15
      end
```

This calculates the time-step to be taken on each iteration

```
%We try to calculate the timestep by which each iteration should march by
function[delta_t] = timestep(temperature_at_t,velocity_at_t,delta_x,C)

speed = sqrt(temperature_at_t);

delta_T = C*(delta_x)./(velocity_at_t + speed);

delta_t = min(delta_T);

end
```

This function implements the floating boundary conditions of the flow

```
1 function[density,temperature,velocity] = boundary_condition(density,temperature,
     velocity)
2
      "The reservoir has only one floating variable , the inlet density
      %and temperature are fixed
3
      density(:,1) = 1;
      temperature(:,1) = 1;
      velocity(:,1) = 2.*velocity(:,2) - velocity(:,3);
      %All the flow variables are floating at the exit
8
9
      density(:,end) = 2.*density(:,end-1) - density(:,end-2);
      temperature(:,end) = 2.*temperature(:,end-1) - temperature(:,end-2);
      velocity(:,end) = 2.*velocity(:,end-1) - velocity(:,end-2);
12
```

This function carries out the time-marching of the computation. The function returns the values of the flow variables at steady state and also the variation of parameters at the throat, with time.

```
2 function [density, velocity, temperature, pressure, mach, mass_flow_rate_memory,
      pressure_throat, density_throat, velocity_throat, temperature_throat, Mach_throat,
      iter] = McCormack(Nx,x,delta_x,A,gamma,throat_index,courant_number)
4 %We initialize the data
5 [density,temperature,velocity] = initialize_flow_variables(Nx,1,delta_x);
8 change = inf;
9 tolerance = 1e-11;
    iter = 1;
13
  % We march in time until our error metric is smaller than our tolerance
14
    while iter < 50000
16
17
      if change < tolerance
19
          break
20
      end
21
      density_old = density;
      velocity_old = velocity;
23
      temperature_old = temperature;
24
      mass_old = density_old.*A.*velocity_old;
26
       % Using the CFL criterion we predict the timestep to be taken
27
       [delta_t] = timestep(temperature, velocity, delta_x, courant_number);
28
29
      % Naive prediction
30
31
      for i = 2 : Nx-1
33
           diff1 = (density(i+1)-density(i))/delta_x;
34
           diff2 = (velocity(i+1)-velocity(i))/delta_x;
35
           diff3 = (log(A(i+1)) - log(A(i))) / delta_x;
36
           diff4 = (temperature(i+1)-temperature(i))/delta_x;
```

```
38
39
40
                        d_density(i) = (-density(i)*diff2) - ((density(i)*velocity(i))*diff3) - (
41
             velocity(i)*diff1);
42
43
                        d_velocity(i) = (-velocity(i)*diff2) - ((1/gamma)*((diff4)+((temperature(i
44
             )/density(i))*diff1)));
45
                        d_temperature(i) = (-velocity(i)*diff4) - ((gamma-1)*temperature(i))*(
47
             diff2 + (velocity(i)*diff3));
48
                        density(i) = density(i) + (d_density(i)*delta_t);
49
                        velocity(i) = velocity(i) + (d_velocity(i)*delta_t);
                        temperature(i) = temperature(i) + (d_temperature(i)*delta_t);
53
              end
54
              % We correct our naive prediction
              for i = 2 : Nx-1
56
                        diff1 = (density(i)-density(i-1))/delta_x;
                        diff2 = (velocity(i)-velocity(i-1))/delta_x;
                        diff3 = (temperature(i)-temperature(i-1))/delta_x;
60
                        diff4 = (log(A(i))-log(A(i-1)))/delta_x;
61
62
63
                        d_density_p(i) = (-density(i)*diff2) - ((density(i)*velocity(i))*diff4) -
64
              (velocity(i)*diff1);
65
66
                        d_{velocity_p(i)} = (-velocity(i)*diff2) - ((1/gamma)*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temperature))*((diff3)+((temp
67
              (i)/density(i))*diff1)));
68
                        d_temperature_p(i) = (-velocity(i)*diff3) - ((gamma-1)*temperature(i))*(
70
             diff2 + (velocity(i)*diff4));
              end
72
73
              % We take the average
74
75
              d_density_avg = 0.5*(d_density+d_density_p);
76
              d_velocity_avg = 0.5*(d_velocity+d_velocity_p);
77
              d_temperature_avg = 0.5*(d_temperature+d_temperature_p);
78
79
              \% Note the average arrays have size Nx-1 not Nx
80
              density = density_old + [d_density_avg*delta_t,0];
83
              velocity = velocity_old + [d_velocity_avg*delta_t,0];
84
               temperature = temperature_old + [d_temperature_avg*delta_t,0];
85
              % We ensure the floating conditions are implemented
86
               [density,temperature,velocity] = boundary_condition(density,temperature,
             velocity);
89
```

```
90
       mach = velocity./sqrt(temperature);
91
       mass_flow = density.*A.*velocity;
92
93
       pressure = density.*temperature;
94
       % We moniter what happens in the throat
95
96
       density_throat(iter) = density(throat_index);
97
       temperature_throat(iter) = temperature(throat_index);
       Mach_throat(iter) = mach(throat_index);
100
       velocity_throat(iter) = velocity(throat_index);
       pressure_throat(iter) = pressure(throat_index);
102
       change = max(abs(mass_flow-mass_old));
103
104
       %We put our flow variables into memory
105
106
       mass_flow_rate_memory(iter,:) = mass_flow;
107
108
       iter = iter+1;
109
110
111
112
   end
113
114
   end
115
```

5 Verification and Validation

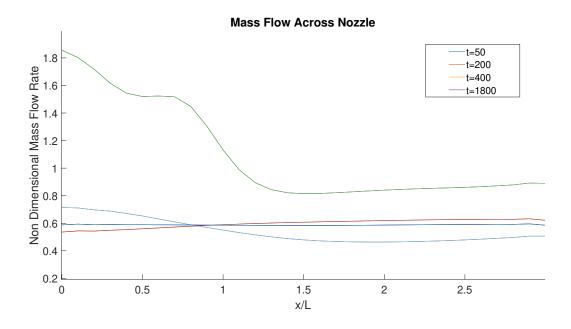


Figure 2: Conservation of mass.

As seen, the mass flow rate across the nozzle stabilizes with time to a constant value ensuring mass is conserved. The continuity equation is a direct consequence of mass conservation, hence it serves as a verification for the final solution.

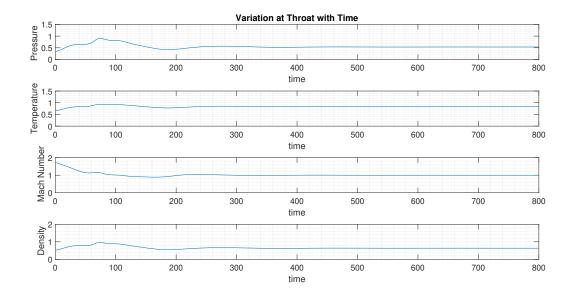


Figure 3: Convergence.

The above graphs shows the status of the flow variables at the nozzle with time, as can be seen after 300 time steps the solution has reached steady state. Hence the convergence of the solution is observed.

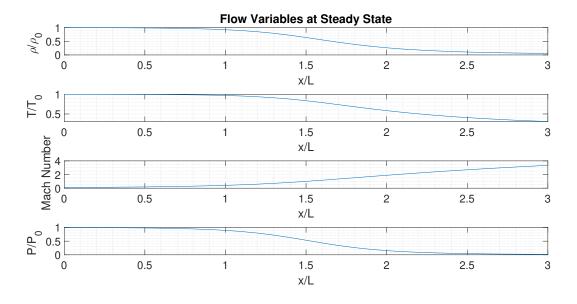


Figure 4: Steady State.

The above graph shows the profile of the Nozzle at Steady State, as can be seen the Nozzle Mach Number is 1.

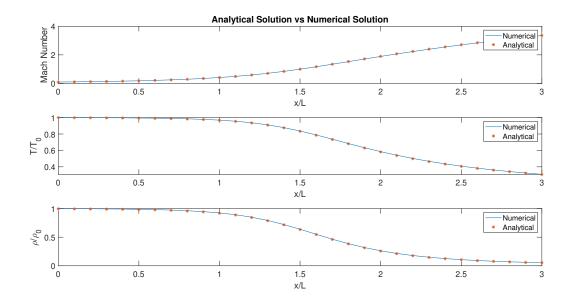


Figure 5: Comparing the solutions.

The flow variables vary in a manner consistent with the Analytical Solution. Thus validating the numerical solution.

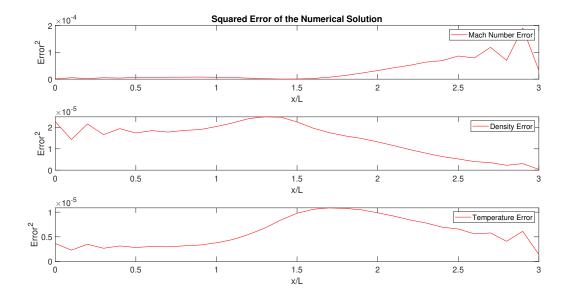


Figure 6: Evaluating the Error.

Overall the error is very small (order $10^{-4} - 10^{-5}$), however there is marginal variation along the nozzle, the errors seem to peak near the throat of the nozzle. A possible explanation for this could be the fact that the flow experience a sharp change in velocity across the throat which results in the propagation of a larger error.

The mean squared errors:

Mach Number: 3.0799E-05Density: 1.4859E-05Temperature: 5.9295E-06

Table 2: Comparing Values from Both the Solutions at The Throat

rable 2. Comparing values from Both the Solutions at The Throat				
	M at throat	ρ at throat	T at throat	Time Taken by solver
Numanical	0.0004	0.6297	0.0265	0.2561
Numerical	0.9994	0.6387	0.8365	0.3561
Analytical	1	0.6339	0.8333	0.2012

6 Conclusion

As seen an accurate numerical solution solution has been developed, the errors which appear are caused due to truncation. Also we have an inbuilt error at the inlet where we assume stagnation values, however if we consider it to be a reservoir inlet the Mach Number would be 0 and mass flow would be absent, which is in contradiction to the floating boundary condition assumed at the inlet. The solution can be made further accurate by using a finer mesh until a situation of mesh independence is attained with appropriate adjustments in the courant number.

A complete version of the implementation is available in the following repository.

References

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