

Ideal gases equation has assumed to be accurate to describe P-V-T relationship for a real gas

Real gas cannot be compressed to a volume that is less than the total molecular volume.

↑ Density ↓ Temp → molecular interaction can't be neglected.

2.2.1. Equations of State for Real Gases and Their Range of Applicability

Real gas equations

→ Van der Waals equation of state

$$p = \frac{RT}{V_m - b} - \frac{a}{V_m^2} = \frac{nRT}{V - nb} - \frac{n^2 a}{V^2}$$

Redlich-Kwong equation of state

$$p = \frac{RT}{V_m - b} - \frac{a}{\sqrt{T} V_m(V_m + b)} = \frac{nRT}{V - nb} - \frac{n^2 a}{\sqrt{T} V(V + nb)}$$

Beattie-Bridgeman equations take.

$$P = \frac{RT}{V_m^2} \left(1 - \frac{c}{V_m T^3} \right) (V + B) - \frac{A}{V_m^2}$$

$$A = A_0 \left(1 - \frac{a}{V_m} \right) \text{ and } B = B_0 \left(1 - \frac{b}{V_m} \right)$$

Virial equation of state.

$$P = RT \left[\frac{1}{V_m} + \frac{B(T)}{V_m^2} \right]$$

Critical Temperature \rightarrow range of V_m has
shrunk to a single value $\rightarrow T_c$.

$P_c \} V_c \rightarrow$ Critical Constants \rightarrow
describe the phase diagram of
pure substance.

Maxwell Construction - generate isotherms

2.3 | The Compression Factor

- Compression Factor $z = \frac{V_m}{V_{m, \text{ideal}}} = \frac{PV_m}{RT}$

Boyle temperature T_b

$$T_b = \frac{a}{Rb}$$

7.4 | The law of corresponding states

law of corresponding states - If 2 gases have the same values of T_r , P_r , and V_{mr} , they are corresponding states.

$$\frac{P_r}{27b^2} = \frac{8aT_r}{27b(8bV_{mr}-b)} - \frac{9}{9b^2V_{mr}^2}$$

$$P_r = \frac{8T_r}{3V_{mr}-1} - \frac{3}{V_{mr}^2}$$

7.5 | Fugacity and Equilibrium Constant for real gases

$$N(T, P) = N^0(T) RT \ln \frac{f}{f^0}$$

$f \rightarrow$ Fugacity of the gas.

\hookrightarrow Effective pressure that a real gas exerts.

$$\ln f = \ln P + \int_0^P \frac{z-1}{P'} dP$$

$$\text{or } f = P \exp \left[\int_0^P \frac{z-1}{P'} dP \right]$$

$$\text{or } f = \gamma(P, T) P.$$

Equation coefficient \rightarrow f and P are related proportionally factor γ .

Q.1] What determines the Relative Stability of solid, liquid and gas phases?

phase \rightarrow A form of matter that is uniform with respect to chemical composition and the state of aggregation

$$\left(\frac{\partial M}{\partial T}\right)_P = -S_m \text{ and } \left(\frac{\partial U}{\partial P}\right)_T = V_m$$

$$S_m^{\text{gas}} > S_m^{\text{liquid}} > S_m^{\text{solid}}$$

$V_m^{\text{gas}} \gg V_m^{\text{liquid}} > V_m^{\text{solid}} \gg 0$, $\uparrow P$ leads to boiling point elevation

$\uparrow P$ leads to freezing point elevation if $V_m^{\text{liquid}} > V_m^{\text{solid}}$ and to freezing point depression if $V_m^{\text{liquid}} < V_m^{\text{solid}}$

thermodynamically favored with respect to the solid \rightarrow Gel formation at high pressure

Solid Sublimes and the transition temperature T_s is called the Sublimation temperature.

The P, V_m, T for this point specifies the triple point.

8.2) The ^{pressure -} temperature phase diagram.

Phase diagram - it displays the information graphically.

P, V, T construct phase diagrams

$P-T$ phase diagram \rightarrow Stability regions for a pure substance as a function of pressure and temperature.

All P, T points for the same 2 phases coexist at equilibrium fall on a curve \rightarrow coexistence curve.

Standard boiling temp - temp. at which the vapor pressure of the substance is 1 bar.

Normal boiling temp - temp. at which the vapor of the substance is 1 atm.

Along 2-phase curves in which one of the coexisting phases is the gas. P_v refers to the vapor pressure.

liquid-solid coexistence curve extends indefinitely. liquid-gas curve ends at the critical point $\rightarrow T = T_c \ \& \ P = P_c$

$T > T_c \ \& \ P > P_c$ are Supercritical fluids

8.3 / Phase Rule

$$N_g(T, P) = N_0(T_0) = N_1(T, P)$$

$T \ \& \ P$ can be varied independently. In a single region a system of pure substance has 2 degrees of freedom.

Phase rule \rightarrow links the # of degrees of freedom to the # of phases in a system.

8.4] The pressure-volume and pressure-volume-Temp. phase diagrams.

P-T phase diagram with a P-V phase diagram \rightarrow combine two representations into a P-V-T. Phase diagram.
↳ 3 Dimensions

8.5] Providing a Theoretical Basis for the P-T. phase diagram.

Clayton equation:
$$\frac{dP}{dT} = \frac{\Delta S_m}{\Delta V_m}$$

Trouton's rule - $\Delta S_{\text{vaporization}} \approx 90 \text{ J/mol.K}$ for liquids.

8.6] Using the Clausius-Clayton Equation to calculate vapor pressure as a function of T.

Clausius-Clayton equation.

$$\frac{dP}{dT} = \frac{\Delta S_{\text{vap}}}{\Delta V_{\text{vap}}} \approx \frac{\Delta H_{\text{vap}}}{TV_m} = \frac{P \Delta H_{\text{vap}}}{RT^2}$$

$$\frac{dP}{P} = \frac{\Delta H_{\text{vap}}}{R} \frac{dT}{T^2}$$

8.7 | The vapor pressure of a pure substance depends on the applied pressure

$$\mu_{li}(T, P) = \mu_{gas}(T, P)$$

$$\left(\frac{\mu_{li}(T, P)}{P} \right)_T = \left(\frac{\mu_{gas}(T, P)}{P} \right)_T \left(\frac{dP}{P} \right)$$

$$\frac{RT}{P} dP = V_m^{liq} dP \quad \text{or} \quad RT \int_P^P \frac{dP}{P}$$

$$= V_m^{liq} \int_P^P dP$$

$$\rightarrow RT \ln \left(\frac{P}{P^*} \right) = V_m^{liq} (P - P^*)$$

8.8 | Surface Tension

$$dA = r d\sigma$$

Surface Tension \rightarrow energy/area or J/m^2

$$\sigma = 4\pi r^2 \quad \text{do: } 8\pi r dr$$

$$F = 8\pi r$$

$$4\pi r^2 \text{ Portent } 8\pi r = 4\pi r^2 \text{ Portent } \rightarrow \text{Pinch } \rightarrow \text{Labor } \frac{2\sigma}{r}$$

Capillary rise and capillary depression
are consequences of the pressure
difference across a curved surface.

$$h = \frac{2\gamma}{\rho g r}$$

Liquid-surface is characterized by
the contact angle, θ .

Complete wetting corresponds to

$\theta = 0^\circ$ and complete non wetting

corresponds to $\theta = 180^\circ$

$P_{inner} = P_{outer} + \frac{2\gamma \cos \theta}{r}$ and

$$h = \frac{2\gamma \cos \theta}{\rho g r}$$