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Macro P. Chem.

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Reading HW #7

7.1.) Real Gases and Ideal Gases

real gases cannot be compressed to a volume less than the total molecular volume \rightarrow $P-V-T$ always related regardless of ideal or real

7.2.) Equations of State for Real Gases and Their Range of Applicability

Vander Waals equation

$$P = \frac{RT}{V_m - b} - \frac{a}{V_m^2} = \frac{nRT}{V - nb} - \frac{n^2 a}{V^2}$$

Predict P-V behavior

Redlich-Kwong equation

$$P = \frac{RT}{V_m - b} - \frac{a}{\sqrt{T} V_m (V_m + b)} = \frac{nRT}{V - nb} - \frac{n^2 a}{\sqrt{T} V (V + nb)}$$

7.3.) The Compression Factor

$\lim_{P \rightarrow 0} (Z - 1) = 0$
then $T \leq T_B$

$$Z = \frac{V_m}{V_{m,ideal}} = \frac{P V_m}{RT}$$

Boyle temperature

different for each gas

$$T_B = \frac{a}{Rb}$$

a & b \rightarrow substance dependent

7.4.) The Law of Corresponding States

$$\text{Error} = 100\% \frac{Z - 1}{Z}$$

$$P_r = \frac{8 T_r}{3 V_{mr} - 1} - \frac{3}{V_{mr}^2}$$

without reference to parameters a & b

7.5.) Fugacity and the Equilibrium Constant for Real Gases

effective pressure that a real gas exerts

$$\mu(T, P) = \mu^\circ(T) + RT \ln \frac{f}{f^\circ}$$

$$\gamma(P, T) P = f$$

γ = fugacity coefficient

8.1.) What Determines the Relative Stability of the Solid, Liquid & Gas Phases?

μ decreases as temperature increases

$$\left(\frac{\partial \mu}{\partial T}\right)_P = -S_m$$

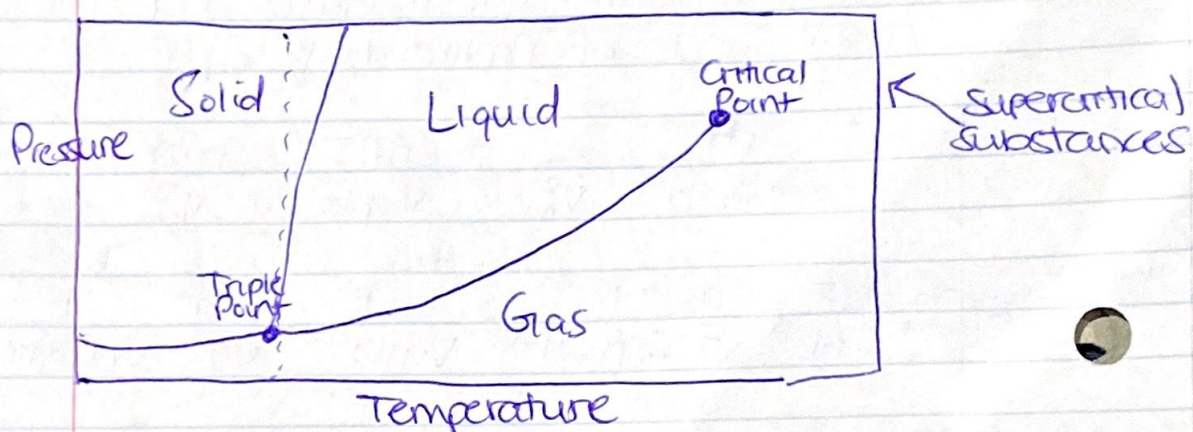
$\left(\frac{\partial \mu}{\partial P}\right)_T = V_m$

$S_m^{\text{gas}} > S_m^{\text{liq}} > S_m^{\text{sol}}$

V_m range for

always positive

8.2 The Pressure-Temperature Phase Diagram



every substance is different

$$\Delta H = \Delta H_{\text{sublimation}} = \Delta H_{\text{fusion}} + \Delta H_{\text{vaporization}}$$

8.3.) The Phase Rule

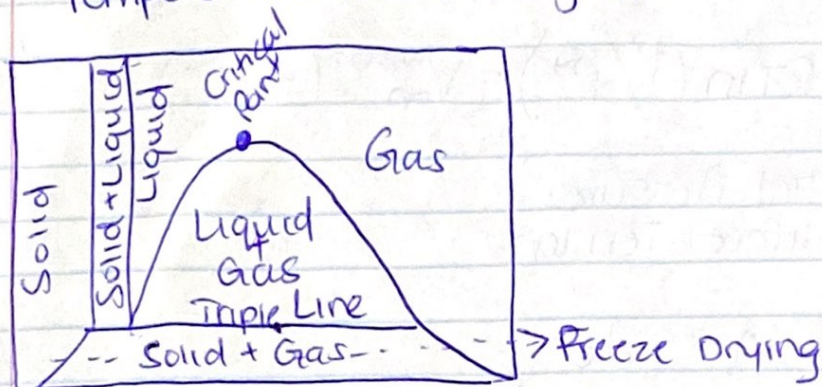
$$\mu_a(T, P) = \mu_b(T, P) = \mu_g(T, P)$$

a system of pure substance has two degrees of freedom

$$F = 3 - P$$

of phases

8.4.) The Pressure - Volume and Pressure - Volume - Temperature Phase Diagrams



8.5.) Providing a Theoretical Basis for the P-T Phase Diagram

$$\left(\frac{dP}{dT}\right)_{\text{vaporization}} = \frac{\Delta S_{\text{vap}}}{\Delta V_{\text{vap}}} \approx 4.8 \times 10^{-2} \text{ bar K}^{-1}$$

$$\text{Fusion} \rightarrow \approx \pm 55 \text{ bar K}^{-1}$$

$$\text{Trautman's Rule} \rightarrow \Delta S_{\text{vap}} \approx 90 \text{ J mol}^{-1} \text{ K}^{-1}$$

8.6.) Using the Clausius-Clapeyron Equation to Calculate Vapor Pressure as a Function of T

$$\int_{P_i}^{P_f} \frac{dP}{P} = \frac{\Delta H_{\text{vap}}}{R} \times \int_{T_i}^{T_f} \frac{dT}{T^2}$$

$\Delta H_{\text{vaporization}}$
can be
substituted for
 $\Delta H_{\text{sublimation}}$

$$\ln \frac{P_f}{P_i} = -\frac{\Delta H_{\text{vap}}}{R} \times \left(\frac{1}{T_f} - \frac{1}{T_i} \right)$$

8.7.) The Vapor Pressure of a Pure Substance Depends on the Applied Pressure

$$\uparrow RT \ln(P/P^*) = V_m^{\text{liquid}} (P - P^*)$$

8.8.) Partial Pressure
↳ Surface Tension

$$dA = \gamma d\sigma$$

Capillary rising
or depression

$$P_{\text{inner}} = P_{\text{outer}} + \frac{2\gamma}{r} \rightarrow \text{goes from } 0 \rightarrow \infty$$

↳ pressure differential across a curved surface