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ELECTRICAL DOUBLE LAYER.

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**ADSORPTION AT THE MERCURY-AQUEOUS SOLUTION  
ELECTRICAL DOUBLE LAYER**

**Alan R. Sears**

**A Dissertation Presented to the Faculty  
of the Graduate School of Yale University  
in Candidacy for the Degree of  
Doctor of Philosophy**

**1971**

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## SUMMARY

The adsorption of KBr from  $x\text{MKBr} + (1-x)\text{MKF}$  and of  $x\text{M}_6\text{-amino-hexanoic} + 5\text{MKF}$  at the mercury aqueous solution interface has been investigated. The necessary data were obtained by determining the differential capacity curve, the streaming electrode potential and the surface tension at the point of zero charge. The adsorption of KBr from KBr + KF has been shown to be similar to KCl from KCl + KF if the data in the same range of specifically adsorbed charge are compared. The results at larger values of specifically adsorbed charge have not previously been observed for halide systems. They can be explained by assuming a standard free energy with both linear and quadratic terms and variable isotherm parameters. The bromide and chloride results imply that the simpler picture for the iodide ion is due to the limited range of surface charge which has been studied. Within the range of surface charge available, 6 amino-hexanoic acid is maximally adsorbed when the surface charge density is -6, with a quadratic standard free energy of adsorption. The expectation that this system would show some of the characteristics of ionic adsorption proved to be incorrect. The quadratic standard free energy, which implies the adsorption of a point dipole, indicates that in this system adsorption should be considered to occur in the entire double layer rather than only in the inner layer. This assumption is necessitated by the dipole being significantly larger than the inner layer.

### Glossary

The symbols occurring below are those which frequently are used in the text.

$\gamma$	surface tension
$\Gamma_X$	surface excess of X in Gibbs model
$\Gamma_{X,w}$	relative surface excess of X
$\Gamma^d$	surface concentration in the diffuse layer
$\Gamma^i$	surface concentration in the inner layer.
$q, q^M$	surface charge density on mercury
$q^s$	surface charge density in solution
$q^d$	surface charge density in diffuse layer
$q^l$	surface charge density of specifically adsorbed ions
$E^\pm$	potential of cell against a reversible electrode
$E, E_{ref}$	potential of cell against a reference electrode
$E_z$	potential of cell at the point of zero charge
$\phi^m$	potential in the mercury electrode
$\phi^1$	potential at the inner Helmholtz layer
$\phi^2$	potential at the outer Helmholtz layer
$\phi^{m-2}$	potential drop across the inner layer

C	capacity of the double layer
$C^d$	capacity of the diffuse layer
$C^i$	capacity of the inner layer
$\frac{dC^i}{dq}$	differential capacity at constant amount adsorbed.
$\frac{dC^i}{dq}^1$	differential capacity at constant charge
$\frac{K^i}{q}$	integral capacity at constant amount adsorbed
$\frac{1}{q} K^i$	integral capacity at constant charge
$x_1$	position of the inner Helmholtz layer
$x_2$	position of the outer Helmholtz layer
$\xi$	$\xi = \gamma + qE$
$E^b$	value of E for base solution
$C^b$	value of C for base solution
$\xi^b$	value of $\xi$ for base solution
$\Delta \frac{1}{C}$	$\frac{1}{C} - \frac{1}{C^b}$
$\Delta E$	$E - E^b$
$\Phi$	$\xi - \xi^b$ surface pressure
$\delta$	$q - q_{\max}$

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## I. THEORY OF THE ELECTRICAL DOUBLE LAYER

The region of the electrode solution interface is known as the electrical double layer. The generally accepted model of this interface consists of the metallic phase, the compact or inner layer and the diffuse layer as is shown in Figure 1. The compact layer is divided into two parts. The inner Helmholtz plane is the plane of closest approach of specifically adsorbed ions. An ion is specifically adsorbed if its adsorption can not be explained by diffuse layer theory. All adsorption of neutral molecules is therefore specific adsorption. The outer Helmholtz plane is the plane of closest approach of completely solvated ions. The diffuse layer begins at the outer Helmholtz plane and extends into the solution until the solution has its bulk concentration. The thermodynamic theory does not depend on the above model, but only on the existence of an interface and the absence of charge transfer across the interface. The Gouy-Chapman-Stern theory presupposes the model used and is applicable only to the diffuse layer. The thermodynamic derivation and that of the Guoy-Chapman-Stern theory are classical. The most complete discussion of both may be found in Mohilner's article.<sup>1</sup> The entire theory of the double layer is also discussed by Delahay.<sup>2</sup> The material discussed in Sections C and D is based on a method of analysis developed by Grahame and Parsons over the last twenty years. No single source is available in which the complete theory of the double layer is presented. A careful review of the theory was therefore considered advisable.

### A. The Thermodynamic Derivation of the Electrocapillary Equation

The system which I will first describe is represented by the

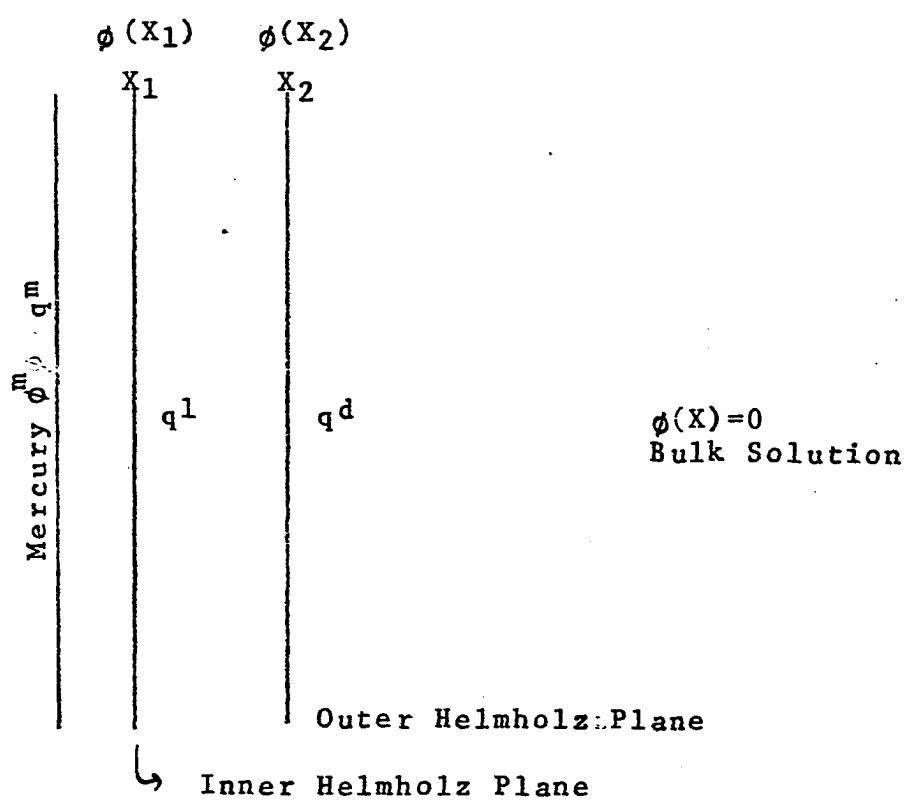
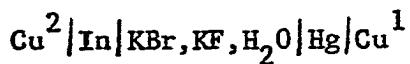


Figure 1. A Schematic Representation of The Electrical Double Layer

following cell:



The electrode In is a hypothetical  $\text{K}^+$  reversible electrode in contact with the solution. A  $\text{Br}^-$  or  $\text{F}^-$  reversible electrode could also be used in the derivation. It will later be shown that a constant potential electrode may always be used instead of a reversible electrode. We assume that if a potential is imposed across the cell, equilibrium is reached, and that no charge transfer occurs across the interface. We then get the Gibbs absorption equation for this system:

$$\begin{aligned} dy = - \Gamma_e d\bar{\mu}_e - \Gamma_{\text{Hg}}^+ 2d\bar{\mu}_{\text{Hg}^+} - \Gamma_{\text{K}^+}^+ d\bar{\mu}_{\text{K}^+} - \Gamma_{\text{F}^-}^- d\bar{\mu}_{\text{F}^-} \\ - \Gamma_{\text{Br}^-}^- d\bar{\mu}_{\text{Br}^-} - \Gamma_{\text{H}_2\text{O}}^+ d\bar{\mu}_{\text{H}_2\text{O}^+} \end{aligned}$$

The  $\mu$  are the electrochemical potentials in either mercury or the solution. The  $\Gamma$  are the surface excesses per unit area and will depend on the choice of the Gibbs plane.  $\gamma$  is the surface tension.

In the metallic phase

$$\bar{\mu}_{\text{Hg}} = \bar{\mu}_{\text{Hg}^+} + 2\bar{\mu}_{\text{e}^-}$$

and

$$\frac{\bar{\mu}_{\text{Hg}}}{\bar{\mu}_{\text{e}^-}} = \frac{\bar{\mu}_{\text{Cu}^1}}{\bar{\mu}_{\text{e}^-}}$$

therefore

$$\begin{aligned} - \Gamma_e d\bar{\mu}_e^{\text{Hg}} - \Gamma_{\text{Hg}^+}^+ d\bar{\mu}_{\text{Hg}^+} = - (\Gamma_e - 2\Gamma_{\text{Hg}^+}^+) d\bar{\mu}_e^{\text{Cu}^1} \\ - \Gamma_{\text{Hg}^+}^+ d\bar{\mu}_{\text{Hg}^+} \end{aligned}$$

Let  $q^M$  be the charge per unit area on the metal surface and  $d\mu_{Hg} = 0$  since we are restricting ourselves to constant T and P.

$$q^M = -F(\Gamma_e^- - 2\Gamma_{Hg+2})$$

and

$$d\gamma = \frac{q^M}{F} d\bar{\mu}_e^{-Cu^1} - \Gamma_K^+ d\bar{\mu}_K^+ - \Gamma_{Br}^- d\bar{\mu}_{Br}^- - \Gamma_F^- d\bar{\mu}_F^- - \Gamma_{Br}^- d\bar{\mu}_{Br}^- - \Gamma_{H_2O} d\bar{\mu}_{H_2O}$$

also

$$\mu_{KF} = \bar{\mu}_K^+ + \bar{\mu}_F^-$$

$$\mu_{KBr} = \bar{\mu}_K^+ + \bar{\mu}_{Br}^-$$

therefore

$$\begin{aligned} & -\Gamma_K^+ d\bar{\mu}_K^+ - \Gamma_F^- d\bar{\mu}_F^- - \Gamma_{Br}^- d\bar{\mu}_{Br}^- = \\ & -(\Gamma_K^+ - \Gamma_F^- - \Gamma_{Br}^-) d\bar{\mu}_K^+ - \Gamma_F^- d\bar{\mu}_{KF} - \Gamma_{Br}^- d\bar{\mu}_{KBr} \end{aligned}$$

Let  $q^S$  be the charge per unit area in the solution:

$$q^S = F(\Gamma_K^+ - \Gamma_F^- - \Gamma_{Br}^-)$$

therefore

$$\begin{aligned} d\gamma = & \frac{q^M}{F} d\bar{\mu}_e^{-Cu^1} - \frac{q^S}{F} d\bar{\mu}_K^+ - \Gamma_F^- d\bar{\mu}_{KF} \\ & - \Gamma_{Br}^- d\bar{\mu}_{KBr} - \Gamma_{H_2O} d\bar{\mu}_{H_2O} \end{aligned}$$

The indicator electrode is reversible to the  $K^+$  ion.

therefore

$$\bar{\mu}_K^{+In} + \bar{\mu}_{e^-}^{In} = \mu_K$$

and

$$d\bar{\mu}_{e^-}^{In} = d\bar{\mu}_K^{+In}$$

also

$$d\bar{\mu}_K^{+In} = d\bar{\mu}_K^+ (\text{solution})$$

$$d\bar{\mu}_{e^-}^{In} = d\bar{\mu}_{e^-}^{Cu^2}$$

and

$$q^M = - q^S$$

to preserve electroneutrality. Therefore

$$\frac{q}{F} d\bar{\mu}_{e^-}^{Cu^1} - \frac{q}{F} d\bar{\mu}_K^+ = + \frac{q}{F} d(\bar{\mu}_{e^-}^{Cu^1} - \bar{\mu}_{e^-}^{Cu^2})$$

but

$$\bar{\mu}_{e^-}^{Cu^1} = \mu_e - F\phi^{Cu^1}$$

$$\bar{\mu}_{e^-}^{Cu^2} = \mu_e - F\phi^{Cu^2}$$

therefore

$$\frac{q}{F} d(\bar{\mu}_{e^-}^{Cu^1} - \bar{\mu}_{e^-}^{Cu^2}) = - q \frac{M}{F} d(\phi^{Cu^1} - \phi^{Cu^2})$$

$$= - q \frac{M}{F} dE^+$$

where  $E^+$  is the potential of the cell with a cation reversible indicator electrode. The symbol  $q$  will now be used in place of  $q^M$  to designate the surface charge per unit area on the mercury surface.

We now have:

$$d\gamma = -qdE^+ - \Gamma_{Br}^- d\mu_{KBr} - \Gamma_F^- d\mu_{KF} - \Gamma_{H_2O} d\mu_{H_2O}$$

The Gibbs-Duhem gives us

$$d\mu_{H_2O} = -\frac{x_{KBr}}{x_{H_2O}} d\mu_{KBr} - \frac{x_{KF}}{x_{H_2O}} d\mu_{KF}$$

therefore

$$\begin{aligned} d\gamma = & -qdE^+ - (\Gamma_{Br}^- - \frac{x_{KBr}}{x_{H_2O}} \Gamma_{H_2O}) d\mu_{KBr} \\ & - (\Gamma_F^- - \frac{x_{KF}}{x_{H_2O}} \Gamma_{H_2O}) d\mu_{KF} \end{aligned}$$

or

$$d\gamma = -qdE^+ - \Gamma_{F,w}^- d\mu_{KF} - \Gamma_{Br,w}^- d\mu_{KBr}$$

The quantities  $\Gamma_{F,w}^-$ ,  $\Gamma_{Br,w}^-$  are called the relative surface excesses. They are the experimentally determined surface excesses and are independent of the position of the Gibbs surface. If we had used a fluoride reversible indicator electrode, we would get the equation:

$$d\gamma = -qdE^- - \Gamma_{K,w}^+ d\mu_{KF} - \Gamma_{Br,w}^- d\mu_{KBr}$$

If neutral molecules were present, terms such as  $-\Gamma_{N,w}^- d\mu_N$  must be added. The procedure could also be extended to include amalgam electrodes.

In interpreting a system we are actually interested in the quantities  $\Gamma^{OHP}$ ,  $\Gamma^d$ ,  $\Gamma^i$ .  $\Gamma^{OHP}$  is the surface excesses calculated at the outer Helmholtz plane.  $\Gamma^d$  is that part of the surface excess

which is in the diffuse layer.  $\Gamma^i$  is the surface concentration of specifically absorbed ions. As will be further discussed, compelling evidence indicates that KF is not specifically adsorbed, but is present only in the diffuse layer.  $\Gamma_{K^+}^{OHP}$  and  $\Gamma_K^d$  are equal and can be used to evaluate diffuse layer parameters. To use this approach one must assume that  $\Gamma_{F^-,w} = \Gamma_F^{OHP}$  which is equivalent to  $\frac{x_{KF}}{x_{H_2O}}$   $\Gamma_{H_2O}$  being negligible. The same situation arises in determining  $\Gamma^i$ . This approximation is only valid at low concentrations (1M and below).<sup>3</sup>

As was mentioned earlier, the use of a reversible electrode is not necessary. If a reference electrode, for example a calomel electrode, is used instead, the potential can be written:

$$E_{ref} = E_{Hg} - E_{cal}$$

$$E^+ = E_{Hg} - E_{In}$$

therefore

$$E_{ref} = E^+ + E_{In} - E_{cal}$$

For a  $K^+$  reversible half cell  $E_{In}$



$$E_{In} = E^o + \frac{RT}{F} \ln a_{K^+}$$

therefore

$$E_{ref} = E^+ + \frac{RT}{F} \ln a_{K^+} + \text{constant}$$

In evaluating data, only  $dE^+$  is used. If an experiment is run in which  $a_{K^+}$  varies, one simply calculates  $E^+$  from the above equation. The

only questionable but necessary practice is using  $a_{\pm}$  for  $a_K^{\pm}$ .

The general form for any system will be  $dy = - qdE - \Gamma_{x,w} \frac{du}{\mu} MX - \Gamma_{N,w} \frac{du}{\mu} N$  where MX is a salt and N a neutral molecule. The second derivative of  $\gamma$ , C

$$C = \left( \frac{\partial q}{\partial E} \right)_{\mu} = - \left( \frac{\partial^2 \gamma}{\partial E^2} \right)_{\mu}$$

is an experimentally available quantity known as the differential capacity. If C is measured as a function of E at constant  $\mu$ , the integration of the C - E curves will give  $\gamma$  and q. Two integration constants are needed and can be obtained either directly or from the base solution values in a region where there is no specific absorption. The directly available constants are  $E_z$ , the potential at which  $q = 0$ , which is obtained by use of the streaming electrode and  $\gamma$  at  $E_z$  which is obtained by using the capillary electrometer. It then follows that

$$q = \int_{E_z}^E CdE$$

$$\gamma - \gamma(E_z) = - \int_{E_z}^E \int_{E_z}^E CdEdE$$

If alternatively, the curves of C versus E are identical in a given region for two solutions of the same ionic strength in neither of which specific absorption occurs in that region, the values of C, q, E, and  $\gamma$  at a point in this region for one solution may be used to integrate the other solution. To check this procedure, one compares the back integrated value of  $E_z$  to the streaming electrode value.

Let us assume that the curve has been integrated such that values of  $\gamma$  and  $E$  are known at integral values of  $q$ . We now define the function of  $\xi = \gamma + qE$  which is a Legendre transformation of  $\gamma$ .

$$d\xi = Edq - \Gamma d\mu$$

If values of  $\xi$  at constant  $q$  are differentiated with respect to  $\mu$ ,  $\Gamma$  is obtained.  $\Gamma$  could also be found from the derivative of  $\gamma$  by  $\mu$  at constant  $E$ . The choice depends on whether you wish to further evaluate your data at constant  $q$  or constant  $E$ . The surface charge density  $q$  is directly related to the field in the interface. The potential difference across the cell  $E$  is a more complicated quantity. The choice of constant  $q$  is both intuitively satisfactory and leads to a somewhat easier analysis. Theoretical and experimental attempts to resolve this problem have been inconclusive.<sup>4,5</sup>

#### B. The Gouy-Chapman-Stern Theory of the Diffuse Double Layer

The G.C.S. theory deals only with the diffuse layer. We assume that the closest approach of an ion to the mercury surface is the outer Helmholtz plane,  $X_2$ . One assumes that the concentration at a distance  $X$  from the electrode surface is given by

$$C_i(X) = C_i^b \exp\left(-\frac{Z_i F \phi(X)}{RT}\right)$$

where  $Z_i$  is the charge,  $\phi(X)$  the potential at  $X$ , and  $C_i^b$  the bulk concentration. In the equations below  $\rho(X)$  is the charge density,  $\vec{D}$  the displacement vector and  $\vec{E}$  the electric field vector. It then follows from standard electromagnetic theory that

$$\nabla \cdot \vec{D} = \rho$$

$$\vec{D} = \epsilon \vec{E} = -\epsilon \nabla \phi$$

$$\nabla \cdot \epsilon \nabla \phi = -\rho(X)$$

$$\nabla^2 \phi = -\frac{\rho(X)}{\epsilon}$$

or

$$\frac{d^2 \phi(X)}{dx^2} = -\frac{1}{\epsilon} \sum_i z_i F C_i b \exp\left(-\frac{z_i F \phi(X)}{RT}\right)$$

if  $\phi$  is a function of  $X$  only and  $\epsilon$  is a constant. We now multiply both sides by  $2 \frac{d\phi(X)}{dx}$ .

$$2 \frac{d\phi}{dx} \frac{d^2 \phi}{dx^2} = \frac{d}{dx} \left( \frac{d\phi}{dx} \right)^2 = -\frac{2}{\epsilon} \sum_i z_i F C_i b \frac{d\phi}{dx} \exp\left(\frac{-z_i F \phi(X)}{RT}\right)$$

We now integrate and get the constant of integration from the fact that  $\frac{d\phi(X)}{dx}$  goes to zero as  $X$  goes to infinity.

$$\left( \frac{d\phi}{dx} \right)^2 = \left( \frac{2RT}{\epsilon} \right) \sum_i C_i b \left[ \exp\left(\frac{-z_i F \phi}{RT} - 1\right) \right]$$

$$\vec{E} = -\frac{d\phi}{dx} \hat{i} = \pm \left( \frac{2RT}{\epsilon} \right)^{\frac{1}{2}} \left( \sum_i C_i b \left[ \exp\left(\frac{-z_i F \phi}{RT} - 1\right) \right] \right)^{\frac{1}{2}} \hat{i}$$

Let  $X_2$  be the position of the outer Helmholtz plane.

$$E(X_2) = -\frac{d\phi(X)}{dx} \Big|_{X=X_2}$$

and

$$D(X_2) = q^M + q^L$$

where  $q^M$  is the charge density on the metal and  $q^1$  is the charge density of the specifically absorbed species. Therefore

$$q^M + q^1 = \pm (2RT\epsilon)^{\frac{1}{2}} \left( \sum c_i^b \left[ \exp - \frac{z_i F \phi}{RT} - 1 \right] \right)^{\frac{1}{2}}$$

For a 1-1 electrolyte or for a mixture of 1-1 electrolytes with one ion in common at constant ionic strength.

$$q^M + q^1 = (8RT\epsilon c)^{\frac{1}{2}} \sinh \frac{|z| F \phi^2}{2RT}$$

Since  $q^M$  and  $q^1$  are experimentally available, the capacity due to the diffuse layer is easily found.

$$C^d = \frac{\partial \phi^2}{\partial (q^M + q^1)} = \left( \frac{2|z|^2 F^2 \epsilon c^b}{RT} \right)^{\frac{1}{2}} \cosh \left( \frac{F \phi^2}{2RT} \right)$$

also

$$\phi^2 = \frac{2RT}{|z|F} \ln \left\{ \left( \frac{q^M + q^1}{2A} \right) + \left[ \left( \frac{q^M + q^1}{2A} \right)^2 + 1 \right]^{\frac{1}{2}} \right\}$$

where  $A = (2RT\epsilon c)^{1/2}$  and  $\phi^2$  is the potential at the outer Helmholtz plane. The surface excess due to the diffuse layer which is equivalent to the surface excess with the Gibbs surface at the outer Helmholtz plane is given by

$$\Gamma_i^d = c_i^b \int_{X_2}^{\infty} \left[ \exp \left( - \frac{z_i F \phi(X)}{RT} \right) - 1 \right] dx$$

and for a 1-1 electrolyte

$$\Gamma_+^d = \frac{A}{|z|F} \left( \exp \left( - \frac{|z| F \phi^2}{2RT} \right) - 1 \right)$$

$$\Gamma_-^d = \frac{A}{|z|F} \left( \exp \left( \frac{|z| F \phi^2}{2RT} \right) - 1 \right)$$

$$q_+^d = |z|F \Gamma_+^d \quad \text{and} \quad q_-^d = |z|F \Gamma_-^d$$

The general approach when dealing with absorption from a single salt solution is to find  $\Gamma_{+,w}$  from  $(\frac{\partial \sigma}{\partial \mu})_q$ . Unless the cation is one of the few which is absorbed,  $q_+$  can be completely assigned to the diffuse layer. Using the equation for  $q_+$ , one finds  $\phi^2$  and from it  $q_-^d$ . The amount of specifically adsorbed anion  $q_-^1$  then follows from

$$q_-^M = -q_-^S = - (q_-^1 + q_-^d + q_+^d)$$

It has already been pointed out that at high concentrations an error can result from equating  $\Gamma_{+,w}$  to  $\Gamma_+^{OHP}$ . Another source of error arises when there is weak specific adsorption. At positive surface charges  $\Gamma_+$  has the limiting value of  $-A$ , but  $\phi^2$  goes to infinity. It follows that a small error in  $\Gamma_{+,w}$  when  $\Gamma_{+,w} \approx -A$  will cause a large error in  $\phi^2$ . This makes the calculation of  $q_-^d$  and  $q_-^1$  suspect when  $\Gamma_{+,w}$  is near  $-A$ .<sup>6</sup>

### C. The Components of the Capacity

#### 1. No specific absorption

The potential drop across the cell with or without specific absorption may be written

$$E = (\phi^M - \phi^2) + \phi^2 - \phi^{\text{ref}}$$

In the absence of specific adsorption,  $\phi^2$  is a function of  $q$  only at constant  $\mu$ . Therefore

$$(\frac{\partial E}{\partial q})_\mu = (\frac{\partial (\phi^M - \phi^2)}{\partial q})_\mu + (\frac{\partial \phi^2}{\partial q})_\mu$$

or

$$\frac{1}{C} = \frac{1}{C^i} + \frac{1}{C^d}$$

$C^i$ , which is the capacity of the inner layer, may be obtained from measured values of  $C$  and computed values of  $C^d$ . With fluoride salts of unadsorbed cations  $C^i$ , Figure 2, is a function of charge only. The total capacity measured for any concentration, and that calculated using  $C^i$  values measured at another concentration and computed  $C^d$  values are in agreement.<sup>7</sup> Furthermore, plots of  $\frac{1}{C}$  versus  $\frac{1}{C^d}$  at constant  $q$  are linear. This affords strong support for the validity of G.C.S. theory and the assumption that fluoride ions are not adsorbed. No theory at present can satisfactorily predict the dependence of  $C^i$  on  $q$  even in the simplest case of fluoride salts. One point of particular controversy is the anodic peak in the  $C^i$  curve which is most evident with specific adsorption. In 1MKF at 25°C it is almost a plateau.<sup>8</sup> These peaks have been ascribed to specific adsorption peaks and to the reorientation of the solvent layer. The anodic rise which follows the peak has been associated with electrostriction and with specific adsorption. The situation is at present unresolved.

Another support for our assumption of no fluoride ion specific adsorption comes from the Esin-Markov effect. We begin with the function  $\xi$ .

$$d\xi = E^+ dq - \Gamma_{F^-, w} d\mu_{KF}$$

$$\left( \frac{\partial E^+}{\partial \mu} \right)_q = - \left( \frac{\partial \Gamma_{F^-, w}}{\partial q} \right)_\mu$$

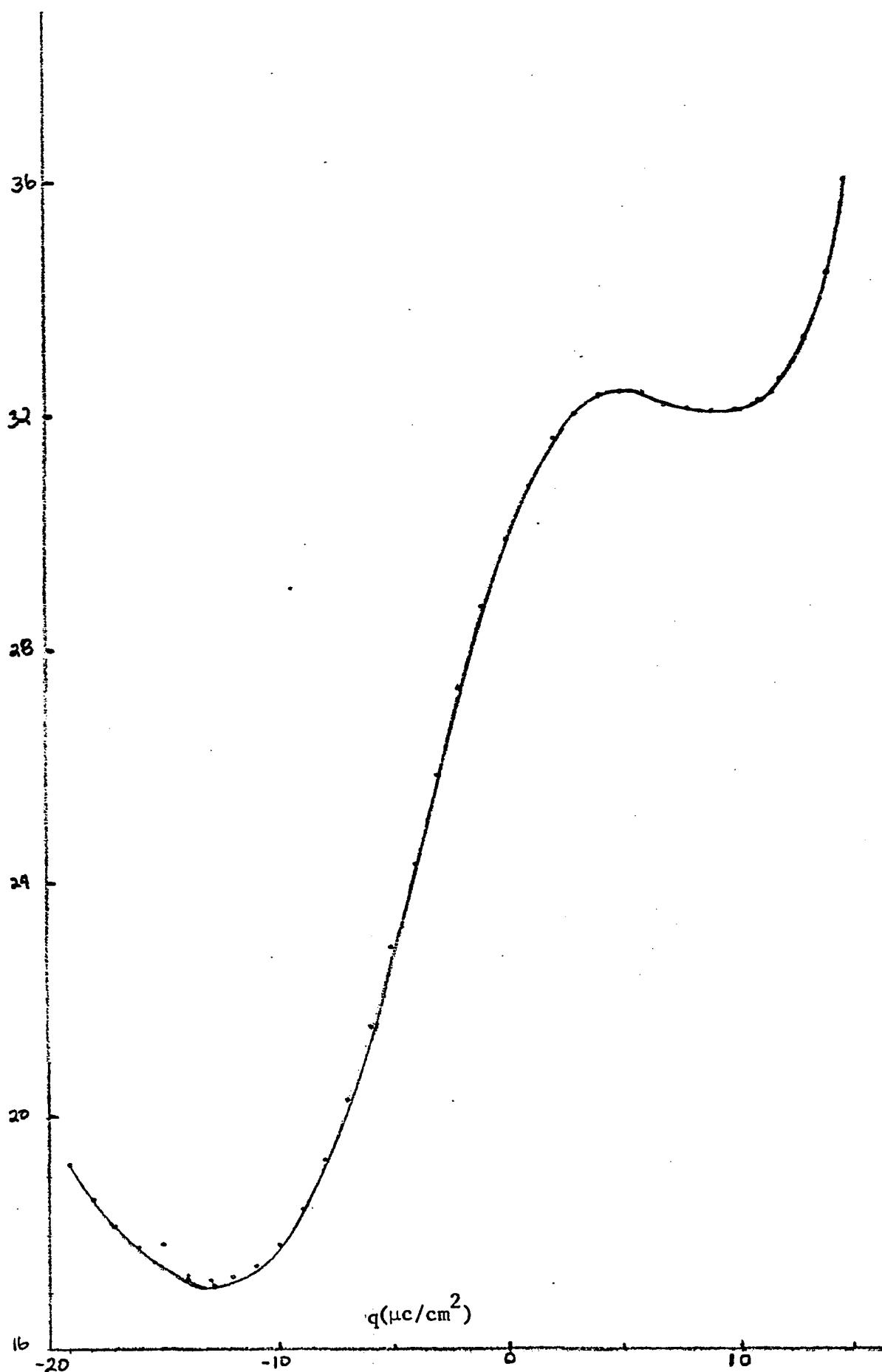


Figure 2. The Inner Layer Capacity of 1MKF Plotted as a Function of the Surface Charge Density

for a cation reversible electrode

$$E^+ = E_{\text{ref}} - \frac{RT}{2F} \ln a_+^2$$

and

$$q_F^- = - \frac{RT}{F} \Gamma_{F^-, w}$$

therefore

$$\left( \frac{\partial E_{\text{ref}}}{\partial \ln a_+^2} \right)_q = \frac{RT}{F} \left[ \left( \frac{\partial q_-^d}{\partial q} \right)_\mu + \frac{1}{2} \right]$$

where we have assumed that  $q_F^- = q_-^d$ .

Also

$$q_-^d = - A \left( \exp \left( \frac{RT\phi^2}{2F} \right) - 1 \right)$$

$$\phi^2 = \frac{2RT}{F} \sinh^{-1} q/2A$$

therefore

$$\left( \frac{\partial q_-^d}{\partial q} \right)_\mu = - \frac{1}{2} - \frac{1}{2} \left\{ \frac{q/2A}{[1 + (q/2A)^2]^{1/2}} \right\}$$

For  $q = 0$ , we find that

$$\left( \frac{\partial E_{\text{ref}}}{\partial \ln a_+^2} \right)_q$$

should equal zero. In other words  $E_z$  measured against a reference electrode is independent of concentration. Parsons found this to be the case with NaF solutions. Furthermore, he compared the experimental and theoretical values of  $\left( \frac{\partial E_{\text{ref}}}{\partial \ln a_+^2} \right)_q$  at different values of  $q$  and also found agreement.<sup>9</sup>

## 2. Specific adsorption present

In the presence of specific adsorption we may still write<sup>10,11</sup>

$$E = \phi^{m-2} + \phi^2 - \phi^{ref}$$

where  $\phi^{m-2}$  is the potential drop across the inner layer.

Also

$$\left(\frac{\partial E}{\partial q}\right)_\mu = \left(\frac{\partial \phi^{m-2}}{\partial q}\right)_\mu + \left(\frac{\partial \phi^2}{\partial q}\right)_\mu$$

but  $\phi^2$  is now a function of both  $q$  and  $q^1$

therefore

$$\left(\frac{\partial \phi^2}{\partial q}\right)_\mu = \left(\frac{\partial \phi^2}{\partial q}\right)_{d\mu} + \left(\frac{\partial q^d}{\partial q}\right)_\mu$$

$$q = -q^1 - q^d$$

$$\left(\frac{\partial \phi^2}{\partial q}\right)_\mu = \frac{1}{c^d} \left[ 1 + \left(\frac{\partial q^1}{\partial q}\right)_\mu \right]$$

so that

$$\frac{1}{c} = \frac{1}{c^i} + \frac{1}{c^d} \left[ 1 + \left(\frac{\partial q^1}{\partial q}\right)_\mu \right]$$

$c$ ,  $c^d$ , and  $\left(\frac{\partial q^1}{\partial q}\right)_\mu$  are known, which allows the computation of  $c^i$ .

$\phi^{m-2}$  may be expressed as

$$\phi^{m-2} = E - \phi^2 - Ez$$

where  $Ez$  is the potential at point of zero charge for KF in the same cell. This is essentially a method of putting all of the systems on

the same scale independent of the experimental design.  $\phi^{m-2}$  may be considered a function of  $q$  and  $q^1$ . Therefore

$$d\phi^{m-2} = \left( \frac{\partial \phi^{m-2}}{\partial q} \right)_q dq + \left( \frac{\partial \phi^{m-2}}{\partial q^1} \right)_q dq^1$$

$$\frac{1}{C^i} = \left( \frac{\partial \phi^{m-2}}{\partial q} \right)_\mu = \left( \frac{\partial \phi^{m-2}}{\partial q} \right)_q + \left( \frac{\partial \phi^{m-2}}{\partial q^1} \right)_q \left( \frac{\partial q^1}{\partial q} \right)_\mu$$

or

$$\frac{1}{C^i} = \frac{1}{q C^i} + \frac{1}{q^1 C^i} \left( \frac{\partial q^1}{\partial q} \right)_\mu$$

$$\frac{C^i}{q} = \left( \frac{\partial q}{\partial \phi^{m-2}} \right)_q \quad q^1 C^i = \left( \frac{\partial q^1}{\partial \phi^{m-2}} \right)_q$$

$\frac{C^i}{q}$  and  $q^1 C^i$  both have the dimensions of capacity.  $q^1 C^i$  can be obtained from the slope of a plot of  $\phi^{m-2}$  versus  $q^1$  at constant  $q$ .

Two other integral capacities can be obtained from this plot.

$$\frac{q^1 K^i}{q} = \frac{\Delta q^1}{\Delta \phi^{m-2}} \quad \text{at constant } q$$

$$\frac{K^i}{q} = \frac{\Delta q}{\Delta \phi^{m-2}} \quad \text{at constant } q^1$$

$\frac{q^1 K^i}{q}$  will equal  $\frac{q^1 C^i}{q}$  if the plots are linear.  $\frac{q^1 K^i}{q}$  is equal to the difference  $\Delta q$  between a  $q$  and  $q = 0$  curve divided by  $\Delta \phi^{m-2}$  for the same value of  $q^1$ . For  $q = 0$ ,  $\frac{q^1 K^i}{q} = \frac{q^1 C^i}{q}$ .  $\frac{q^1 C^i}{q}$  is obtained by solving the equation for  $1/C^i$ .  $\frac{q^1 K^i}{q}$  and  $\frac{q^1 C^i}{q}$  have both been interpreted as the capacities of two parallel plate capacitors.

$$q^{K^i} = \frac{\epsilon}{4\pi x_2} = \frac{q}{q^i \phi^{m-2}}$$

$$q^{1K^i} = \frac{\epsilon}{4\pi(x_2 - x_1)} = \frac{1}{q^1 \phi^{m-2}}$$

where  $x_1$  is the position of the inner Helmholtz layer,  $q^i \phi^{m-2}$  is the part of  $\phi^{m-2}$  due to the surface charges and  $q^1 \phi^{m-2}$  is the part of  $\phi^{m-2}$  due to the absorbed charges. The ratio

$$\frac{q^{K^i}}{q^{1K^i}} = \frac{x_2 - x_1}{x_2}$$

is known as the distance ratio. If the field in the inner layer is constant then we may write

$$\phi_1 = \phi^m - \alpha x$$

$$\phi_2 = \phi^m - \alpha x_1$$

$$\phi = \phi^m - \alpha x_2$$

$$\phi^{m-2} = \phi^m - \phi^2 = \alpha x_2$$

where  $\phi^1$  is the potential at the inner Helmholtz plane. A latter modification of this equation is

$$\phi^1 - \phi^2 = [(x_2 - x_1)/x_2] q^i \phi^{m-2} + \left[ \frac{\gamma}{\gamma + \beta} \right] q^1 \phi^{m-2}$$

$\gamma/\gamma+\beta$  will approach unity when  $q^1$  is large and most of the potential drop across the inner layer occurs between the inner and outer Helmholtz planes. At low values of  $q^1$ ,

$$\frac{\gamma}{\gamma+\beta} = \frac{x_2 - x_1}{x_2}$$

in order that

$$\phi^1 - \phi^2 = \frac{x_2 - x_1}{x_2} \phi^{m-2}$$

An adsorption isotherm may be used to obtain the value of  $\frac{x_2 - x_1}{x_2}$ .<sup>12</sup>  
For example, for KI + KCl, Parsons assumed the following:

$$q^1 = K^1 a_{\pm} \exp(\phi^1 F/RT)$$

where  $q^1 = |q^1|$  and  $K^1$  is a function of  $q$  only. Then

$$\ln q^1/a_{\pm} - \frac{\phi^2 F}{RT} = \ln K^1 + \frac{\phi^{m-2} F}{RT} \left( \frac{x_2 - x_1}{x_2} \right)$$

If we plot  $\phi^{m-2}$  versus the left side of the equation, the slope gives the distance ratio. More complicated isotherms and the modified expression for  $\phi^1 - \phi^2$  can also be used. The capacity ratio method was used for a number of systems, but recently situations where  $K^1$  is negative were found.<sup>13,14</sup> Since  $x_2$  must be greater than  $x_1$ , the interpretation cannot be meaningful for these systems. The earlier success was fortuitous since the physical situation in the inner layer does not correspond to two capacitors in series. The above equations are based on the assumption that

$$\phi^{m-2} = q \phi^{m-2} + \frac{q^1 \phi^{m-2}}{q}$$

or

$$\phi^{m-2} = \frac{q}{K^i} + \frac{q^1}{q^1 K^i}$$

This is not the equation for two capacitors in series or in parallel and its physical meaning is obscure. Values of the distance ratio determined by the isotherm method and those determined by the capacity ratio method have generally not been in agreement.

$q^C^i$  is theoretically an experimentally determinable quantity. We return to the equation

$$\frac{1}{C^i} = \frac{1}{q^C^i} + \frac{1}{q^1 C^i} \left( \frac{\partial q^1}{\partial q} \right)_u$$

At infinite frequency, the second term is zero and we are measuring  $q^C^i$ . This assumes that diffuse layer theory is still valid at infinite frequency.  $q^C^i$  is of particular importance in explaining the peaks in  $C^i$  versus charge curves. If the peak is due solely to specific adsorption, then  $q^C^i$  which is measured at constant  $q^1$  should not contribute to it. The fact that there are peaks in  $q^C^i$  suggests that solvent reorientation plays a part in peak formation.

#### D. Adsorption Isotherms and the Shape of the Capacity Curve.

Theoretically, the shape of the capacity versus charge curve can, under certain conditions, be directly predicted from the adsorption isotherm.<sup>15, 16, 17</sup> The determination of the isotherm also provides information on the charge or potential dependence of the free energy of adsorption. The constants of the isotherm give information concerning the interaction of adsorbed ions. The two isotherms which are most frequently used are the Frumkin and virial. The isotherms and equations of state are given below.

Frumkin:

$$\text{isotherm} \quad \ln \frac{a\beta}{\Gamma_S} = \ln \frac{\theta}{1-\theta} + A\theta$$

$$\text{equation of state} \quad \frac{\Phi}{kT\Gamma_S} = -\ln(1-\theta) + \frac{A}{2}\theta^2$$

Virial:

$$\text{isotherm} \quad \ln \Gamma + 2B\Gamma = \ln a\beta$$

$$\text{equation of state} \quad \Phi = kT(\Gamma + B\Gamma^2)$$

$\Phi$  is the surface pressure and for constant  $q$ ,  $\Phi = \xi - \xi^b$  where  $\xi$  is the base solution value of  $\xi$ .  $\beta$  equals  $\exp(-\Delta G/R\Gamma)$ ,  $\Gamma_S$  is the saturation concentration,  $a$  the activity,  $\theta = \Gamma/\Gamma_S$ , and  $A$  and  $B$  are isotherm constants. The problem of whether to study adsorption at constant  $q$  or  $E$  arises again at this point. As previously mentioned, it is unresolved.

The method of testing the Frumkin isotherm is to pick a value of  $A$ , allow  $\theta$  to vary from  $0 < \theta < 1$  and get a universal curve of  $\ln(\Phi/kT\Gamma_S)$  versus  $\ln(a\beta/\Gamma_S)$ . This curve is compared with an experimental curve of  $\ln \Phi$  versus  $\ln a$ . If the data fit a Frumkin isotherm, the two curves are superimpossible if the scale of  $\ln \Phi$  and  $\ln a$  are changed to  $\ln \Phi + C_1$  and  $\ln a + C_2$ . Obviously  $C_1 = -\ln kT\Gamma_S$  and  $C_2 = \ln \beta/\Gamma_S$ . The values of  $A$  and  $\Gamma_S$  can be adjusted to get the best fit of the experimental data. The virial isotherm is much easier to handle. One rearranges the isotherm into the form

$$\Gamma = \frac{1}{2B} \ln \frac{a}{\Gamma} + \frac{1}{2B} \ln \beta$$

The experimental values of  $\Gamma$  are plotted against  $\ln a/\Gamma$  and the slope gives  $\frac{1}{2B}$ , the intercept  $\ln \beta$ . The method used for the Frumkin isotherm can be used for any isotherm where  $K\bar{\Phi}$ ,  $K$  a constant, and  $\beta$  are functions only of  $\theta$  and any number of isotherm constants. In studying the adsorption of a single ion, the question arises whether to use the salt activity  $(a_{\pm}^2)$  or the ion activity  $a_{\pm}$  in the isotherm. It seems logical to use  $a_{\pm}$ , but this question is also unresolved.

The assumption which is necessary in order to relate the isotherm to the capacity curves is that  $\Gamma = \Gamma(\beta a)$ . This means that all isotherm constants are independent of the surface charge and the amount of specific adsorption. We begin with the differential form of  $\xi$ .

$$d\xi = Edq - \Gamma d\mu$$

$$\left( \frac{\partial E}{\partial \mu} \right)_q = - \left( \frac{\partial \Gamma}{\partial q} \right)_{\mu}$$

$$dE = - \int \left( \frac{\partial \Gamma}{\partial q} \right)_{\mu} d\mu \quad q = \text{constant}$$

but since

$$\Gamma = \Gamma(\beta a)$$

$$\frac{1}{\beta} \left( \frac{\partial \Gamma}{\partial a} \right)_{\beta} = \frac{1}{a} \left( \frac{\partial \Gamma}{\partial \beta} \right)_a$$

and

$$\left( \frac{\partial \Gamma}{\partial q} \right)_{\mu} = \left( \frac{\partial \Gamma}{\partial \beta} \right)_{\mu} \left( \frac{\partial \beta}{\partial q} \right)_{\mu}$$

therefore

$$dE = - \int \frac{a}{\beta} \left( \frac{\partial \Gamma}{\partial a} \right)_{\beta} \frac{\partial \beta}{\partial q} d\mu$$

and

$$\Delta E = E - E^b = - RT \left( \frac{\partial \ln \beta}{\partial q} \right) \Gamma \text{ at constant } q$$

$E^b$  is the value of  $E$  for the base solution at the same value of  $q$ .

If  $\ln \beta$  is linear in  $q$ , then plots of  $E - E^b$  versus  $\ln a$  should be part of the same curve if  $\ln \beta$  is added to  $\ln a$ . The isotherm and  $\frac{d \ln \beta}{dq}$  can be obtained directly from this type of plot.

More generally, we can now take the derivative of the equation for  $\Delta E$  by  $q$  at constant  $\mu$ .

$$\left( \frac{\partial E}{\partial q} \right)_\mu - \left( \frac{\partial E^b}{\partial q} \right)_\mu = - kT \frac{\partial}{\partial q} \left[ \frac{\partial \ln \beta}{\partial q} \cdot \Gamma \right]$$

or

$$\frac{1}{c} - \frac{1}{c^b} = - kT \left[ \left( \frac{\partial \ln \beta}{\partial q} \right)^2 \left( \frac{\partial \Gamma}{\partial \ln \beta} \right)_\mu + \Gamma \frac{\partial^2 \ln \beta}{\partial q^2} \right]$$

at any given value of  $q$ . Let us first assume that

$$\frac{d \ln \beta}{dq} = K$$

$$\frac{d^2 \ln \beta}{dq^2} = 0$$

Then

$$\Delta \frac{1}{c} = \frac{1}{c} - \frac{1}{c^b} = - kT K^2 \left( \frac{\partial \Gamma}{\partial \ln \beta} \right)_\mu$$

$\left( \frac{\partial \Gamma}{\partial \ln \beta} \right)_\mu$  is obtained from the isotherm. For a Frumkin isotherm

$$\frac{\partial \Gamma}{\partial \ln \beta} = \Gamma_S \left\{ \frac{1}{\theta(1-\theta)} + A \right\}^{-1}$$

and is symmetrical about  $\theta = .5$  where it is a maximum. A plot of  $-\frac{1}{C}$  versus  $\Gamma$  at constant charge should give a maximum at  $\theta = .5$ . When  $-\frac{1}{C}$  is a maximum  $C$  is also a maximum. Alternatively let us assume that a virial isotherm is obeyed.

$$\frac{1}{C} - \frac{1}{C^b} = - kT K^2 \left( \frac{\Gamma}{1+2B\Gamma} \right)$$

For large values of  $\Gamma$ ,  $-\frac{1}{C}$  reaches the limiting value of  $\frac{kT K^2}{2B}$  and this would be evident in plots of  $-\frac{1}{C}$  versus  $\Gamma$  at constant  $q$ . Plots of  $-\frac{1}{C}$  versus  $q$  at constant  $\mu$  will have the same characteristics if  $\frac{d^2 \ln \beta}{dq^2} = 0$ .

If we assume that  $\ln \beta$  is a quadratic function of  $q$ , we may write it as follows

$$\ln \beta = \ln \beta_{\max} - \frac{b}{2} \delta^2$$

where

$$\delta = q - q_{\max}$$

also

$$\frac{d \ln \beta}{dq} = - b \delta$$

$$\frac{d^2 \ln \beta}{dq^2} = - b$$

A quadratic standard free energy is based on the assumption that  $\Delta G$  is given by:

$$\Delta G = \Delta G^\circ + \frac{1}{2} q^2 \left[ \frac{1}{C^S} - \frac{1}{C^b} \right] + q \left[ \frac{\mu^b}{\epsilon^b} - \frac{\mu^S}{\epsilon^S} \right]$$

$\mu^S$ ,  $C^S$  and  $\epsilon^S$  are the dipole moment per unit volume, the capacity per unit area and the dielectric constant when the surface is saturated with absorbate;  $\mu^b$ ,  $C^b$ , and  $\epsilon^b$  are for the base solution.  $\Delta G^0$  is the non-electrical part of  $\Delta G$ . This equation may be rearranged to the form

$$\Delta G = \Delta G_{\max} + \frac{1}{2} b^1 \delta^2$$

by finding  $\Delta G_{\max}$  from the derivative  $\partial \Delta G / \partial \delta$  when it equals zero.  $\Delta G$  and  $\Delta G_{\max}$  are negative,  $b^1$  is positive. Since  $\beta = \exp(-\Delta G/RT)$

$$\ln \beta = \ln \beta_{\max} - \frac{1}{2} b^1 \delta^2$$

We then have for  $\Delta 1/C$  the following equation.

$$\frac{\Delta 1}{C} = kT \left[ \Gamma b - b^2 \delta^2 \left( \frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu} \right]$$

If we take the derivative of  $\frac{\Delta 1}{C}$  by  $\delta$  at constant  $\mu$  and set it equal to zero, we find the values at which  $\frac{\Delta 1}{C}$  is an extreme. This expression is

$$b^1 \delta^2 = \frac{3(\partial \Gamma / \partial \ln \beta)_{\mu}}{(\partial^2 \Gamma / \partial \ln \beta^2)_{\mu}}$$

There are three values of  $\delta$  which satisfy this equation. One is  $\delta = 0$ , independent of the isotherm chosen. This point corresponds to maximum adsorption since  $\ln \beta$  is a maximum at  $\delta = 0$ .  $\Delta \frac{1}{C}$  will be a maximum and  $C$  will have its minimum value. The other two values of  $\delta$  correspond to maxima in  $C$  and minima in  $\Delta \frac{1}{C}$ . They depend on the particular isotherm obeyed. As  $\delta$  goes to plus or minus infinity,  $\Delta \frac{1}{C}$  goes to

zero for any isotherm.  $C$  is then equal to  $C^b$  and there is complete desorption. Quadratic dependence is easily demonstrated by a plot of  $\Delta \frac{1}{C}$  versus  $q$  at constant  $\mu$ . Plots of  $\Delta 1/C$  versus  $\Gamma$  at constant  $q$  may be used as an alternative method of finding  $q_{\max}$ . The curve for  $q = q_{\max}$  should be linear and have the largest slope which will equal  $kT_b$ .

This analysis has been used to explain the shape of capacity curves with adsorption. It is truly rigorous only for the adsorption of neutral molecules. With ionic absorption one must decide whether to use  $\Delta \frac{1}{C}$  or  $\Delta \frac{1}{C^i}$ . The derivation necessitates the use of  $\Delta \frac{1}{C}$ , but unlike neutral adsorption the value of  $C^d$  for the base solution will not be the same as that for the solution with adsorption. Using  $\Delta 1/C^i$  solves this problem and is intuitively appealing, but without rigorous justification. Another problem arises with adsorption from a single salt solution, what do we use for the base solution values of  $C^b$ ? The values used in the literature are the  $C$  values for KF at the same concentration. Actually, the derivation indicates that the base solution is the solvent, and that the use of KF values needs further justification. These problems can be alleviated by working with a mixed electrolyte system at constant ionic strength such as  $xM\text{KBr} + (1 - x)M\text{KF}$ .  $C^d$  is then always large and makes a minor contribution to  $C$ . Equating the base solution to 1M KF is also justified in this type of system.

With single salt adsorption, the use of the surface pressure also becomes ambiguous.<sup>11,18</sup> We begin with

$$d\sigma^+ = Edq - (\Gamma_{\text{Br}^-}^d + \Gamma_{\text{Br}^-}^i) d\mu_{\text{KBr}}$$

We then assume that the surface pressure can be written as

$$\Phi = \xi^+ + I - \xi_0^+$$

where

$$I = \int_{-\infty}^{\mu} \Gamma_{Br}^d - d\mu_{KBr}$$

and  $\xi_0^+$  is the value of  $\xi$  when  $\mu = -\infty$  or

$$\Phi' = \xi^+ + I$$

$$I' = \int_{\mu_1}^{\mu_2} \Gamma_{Br}^d - d\mu_{KBr}$$

The magnitude of  $\Phi'$  will differ from  $\Phi$  by a constant at constant  $q$ . A significant problem in this approach is whether the surface pressure due to the anion is  $\Phi$  or  $\Phi/2$ . It is essentially the same problem of whether to use  $a_{\pm}^1$  or  $a_{\pm}^2$  in the isotherm.<sup>19</sup> Using  $\Phi$  implies that all of the effect is due to the anion, whereas  $\Phi/2$  implies that only half of the change is caused by the anion. Since the cation is also adsorbed, though not specifically, it must also have an effect on the surface pressure. A more basic difficulty, is whether the entire concept is valid in single salt solutions with varying ionic strength. This again reduces to the identification of the base solution. With organic adsorption, or adsorption from a solution of fixed ionic strength, this problem does not exist. Let us assume we have system governed by the equation:

$$d\xi = Edq - \Gamma_{N,w} d\mu_N - \Gamma_{F,w} d\mu_{KF}$$

$$d\mu_{KF} = 0$$

Then the surface pressure is given by

$$\Theta = \xi - \xi_0$$

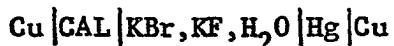
where  $\xi_0$  is the value of the KF solution in the absence of N and there is no ambiguity.

## II. EXPERIMENTAL PROCEDURE

Three separate experiments are needed in order to obtain the data required to interpret the structure of the electrical double layer. These are the determination of the potential ( $E_z$ ), and the interfacial tension ( $\gamma_{Ez}$ ) at the point of zero charge ( $q = 0$ ), and the determination of the differential capacity curve for each concentration of adsorbate studied. The potential and interfacial tension at the point of zero charge are the two constants needed to integrate the differential capacity curve.

### A. The Determination of $E_z$

Let us assume that we have the following cell:



CAL is a calomel reference electrode. A potentiometer is connected between the two copper leads. The mercury electrode consists of a capillary with its top in the solution connected to a mercury reservoir. The reservoir is in turn connected to a tank of nitrogen so that the pressure in the reservoir may be varied at will. The pressure on the mercury is then increased until a rate of flow is reached at which a stable potential exists between the reservoir and the calomel electrode. The pressure is then varied and the potential recorded as a function of pressure. As the pressure increases, the potential will become more negative, reach a plateau and then increase slightly. The potential in the plateau region is the potential of zero charge. The concept behind this experiment is that once an adequate rate of flow is reached, any excess charge on the mercury

will be carried off and furthermore the area of the electrode is effectively infinite. Therefore the surface charge density is zero. The slight rise in potential which occurs at large pressures was unexpected and remains unexplained. It has been observed in a sufficient number of systems that the nature of the adsorbate cannot be the cause. Grahame did an extensive amount of work on the determination of  $E_z$ , and found that this is the most reliable method.<sup>20</sup>  $E_z$  is reproducible to 1 mv or less and even this variation could be due to variations in the liquid junction potential. This method assumes that equilibrium has been reached at the electrode surface. If this is not the case,  $E_z$  must be determined by finding the maximum in the electrocapillary curve.

#### B. The Determination of $\gamma_{Ez}$

The capillary electrometer and its use for determining the electrocapillary curve were developed by Gouy early in this century. The same cell used to determine  $E_z$ , is used in this experiment, except that a much finer capillary is needed. A potential is applied across the cell. The capillary is connected to a mercury reservoir which can be varied in height above the capillary tip. The criterion for choosing a capillary is that it be able to support a column of mercury at least 60 cm high when  $E_z$  is the applied potential. The capillary is calibrated by using a solution whose electrocapillary curve is known. We apply a potential and measure the position of the mercury meniscus in the capillary. At the interface,

$$\Delta P = \frac{2\gamma}{r}$$

$\Delta P$  is computed from the height of the mercury and corrected for the solution height above the tip. Since  $\gamma$  is known, the radius of the capillary at a fixed position is also known. We now may use the capillary for any other solution. At each value of the imposed potential, the mercury reservoir is adjusted until the meniscus is at the calibrated position. We then compute  $\gamma$  using the known value of the radius. There are several possible sources of error in this experiment. We assume that the contact angle between the solution and the mercury is zero, and that we may accurately return the meniscus to the calibrated position. We have no choice concerning the contact angle since it cannot be measured, but the agreement of  $E_z$  values obtained from the electrocapillary curve and those obtained from the streaming electrode supports the zero contact angle assumption. The other problem depends on the capillary. If the radius is changing rapidly, then large errors will be made in positioning the meniscus, but if the radius changes too slowly, a definite equilibrium position is not easily achieved. If the results are reproducible, one may assume the taper of the capillary curve is correct. The potential at which the electrocapillary curve is a maximum is  $E_z$ . Unfortunately, the curve is quite flat in this region. This allows an accurate measurement of  $\gamma_{E_z}$ , but a poor measurement of  $E_z$ . The best procedure is to obtain  $E_z$  from the streaming electrode and  $\gamma_{E_z}$  from the electrocapillary curve.

#### C. The Differential Capacity Curve

The procedure for measuring the differential capacity was first developed by Grahame and improved by Hills and Payne.<sup>21</sup> A schematic of the apparatus is shown in Figure 3. The cell consists of three

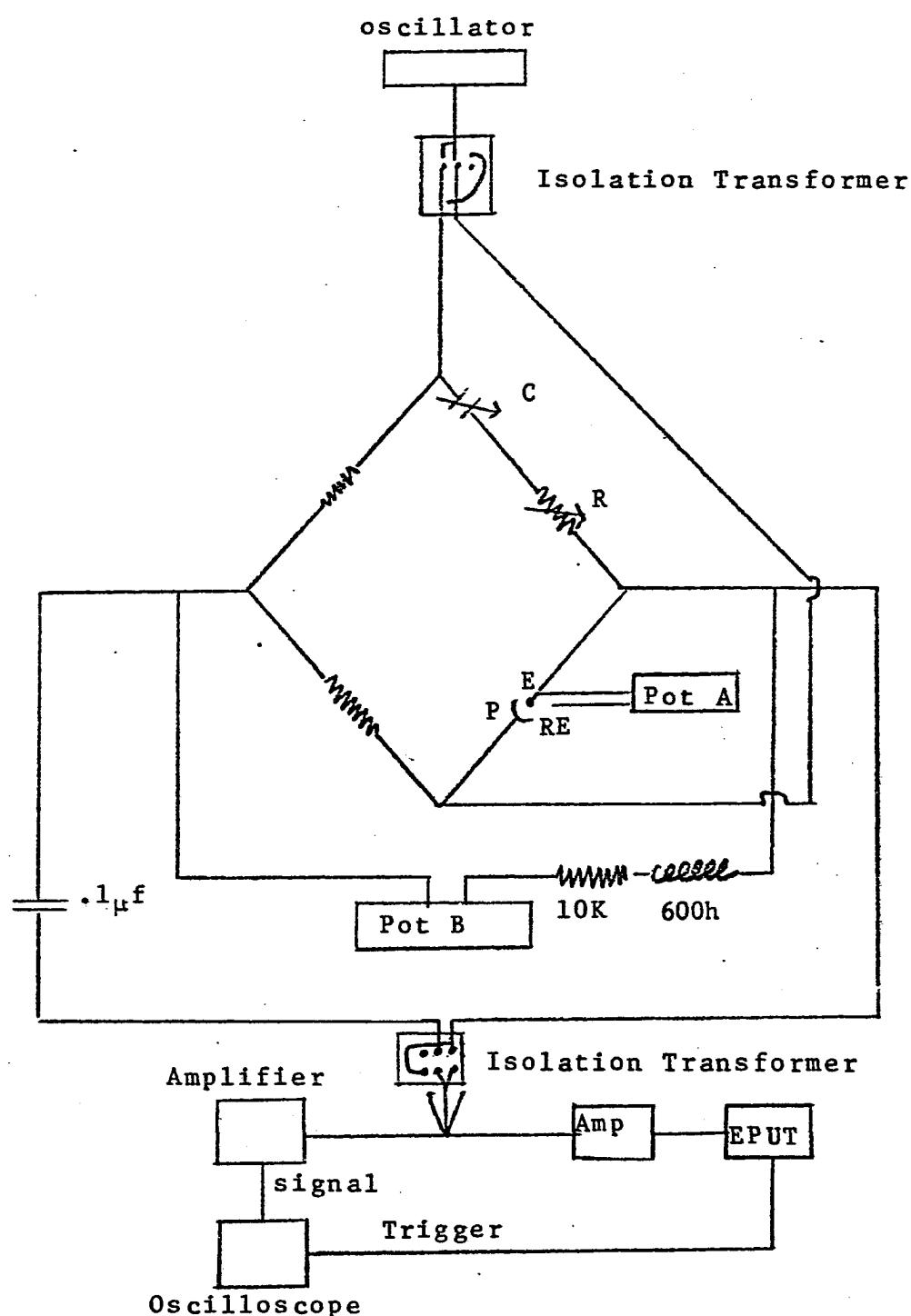


Figure 3. A Schematic Representation of the Apparatus Used to Determine The Differential Capacity

electrodes. A dropping mercury electrode (E) is attached to one terminal of the bridge. Its tip is inside a platinum mesh basket (P) which is attached to another terminal. Together they form one of the four bridge arms. The third electrode is a reference electrode (RE) which is separated by two stopcocks from the solution being measured. The closed stopcocks are ungreased allowing electrical contact but preventing the diffusion of chloride ions from the reference electrode into the solution. Potentiometer A measures the potential between the dropping electrode and the reference electrode. Potentiometer B imposes a constant potential across the entire bridge. The only direct current which flows is that to charge the capacitors. An alternating voltage of 10 mv is impressed across the bridge and the bridge output fed into two amplifiers. The first amplifier feeds the signal to the vertical plates of an oscilloscope. The second amplifier takes the signal to a modified Beckman EPUT meter. The maximum output of the bridge occurs when a drop falls off. At this point the bridge is completely out of balance. The EPUT meter has been modified in such a way that in the TIM mode it can be used both as a timer and as trigger pulse. One adjusts the EPUT meter so that it will not begin counting until a drop has fallen off. It then counts for 10 sec and provides a pulse which is used to trigger the scope. The scope is also calibrated so that the time it takes for a signal to get to the 5 cm line is known. The oscillator frequency is 1000 Hz and the scope sweep time about 1 sec/cm. The individual waves are therefore not resolved, rather they appear as a wedge shaped image on the screen. One adjusts the variable capacitor (C) and resistor (R) until the wedge goes to a minimum at the center of the screen. This means that at the time represented by the 5 cm line

the bridge is in balance. Since the electrical double layer is a pure capacity, the value of the variable capacitor is the capacity of the drop. The EPUT meter and scope repeat this sequence for each drop. The surface area of the drop is determined by measuring the flow rate of the mercury. From the flow rate we get:

$$V = \frac{4}{3}\pi r^3 = \frac{mt}{d}$$

where  $m$  is the flow rate,  $t$  the time in the life of the drop and  $d$  the density of mercury. It follows that

$$A = 4\pi r^2 = 4\pi^{2/3} \sqrt{\frac{3}{4\pi} \frac{mt}{d}}$$

The capacity per unit area is now determinable for each value of potential set by potentiometer B and read on potentiometer A.

The main source of error in this experiment lies in the improper choice and preparation of capillaries. The capillary must be thoroughly cleaned and then coated with dimethyl-dichloro-silane. This prevents the solution from getting inside the capillary. The tip of the capillary must be even. A sliver of glass projecting from the tip will effectively decrease the surface area of the drop. The flow rate must also vary during the course of the experiment since the interfacial tension is a function of potential and the actual pressure causing flow is  $(P - \frac{2\gamma}{r})$ . The variation in the rate of flow is not significant. It is also assumed in this experiment that the mercury surface is at equilibrium. At very low concentrations where this is not the case, an extrapolation must be made to the zero frequency value of the capacity.

### III. The Adsorption of Halide Ions

#### A. Review of Previous Work

The halide systems have received particular attention in the study of the electrical double layer. They exhibit a continuous variation between the non-specifically adsorbed fluoride ion and the strongly adsorbed iodide ion. Compared with most other anions studied, the halides have a simple structure which can, to a first approximation, be represented by a point charge. This removes the complication introduced by permanent dipole moments, and the further difficulty with polynuclear anions of several possible orientations relative to the mercury surface. The halide systems are then obviously the first place to begin looking for a coherent explanation of anionic specific adsorption.

##### 1. The fluoride ion

Grahame's work, which has been previously discussed, clearly shows that the fluoride ion is not specifically adsorbed.<sup>7,8</sup> It should be mentioned that the identity of the cation has a slight quantitative effect, but no qualitative significance. The remaining question is to explain the shape of the  $C^i$  versus  $q$  curve. Unfortunately an adequate theory is still not in existence. On Figure 2, the  $C^i$  versus  $q$  curve for LMKF is plotted. The slight anodic peak is clearly evident. For NaF, Grahame found that this peak disappears with increasing temperature and that the capacity at 85°C rises continuously as  $q$  becomes more positive. The shape of the curve was independent of concentration at constant charge and temperature. These results lend support to the belief that the peak is due to a local maximum in the dielectric constant of the inner layer. The maximum could be caused by the reorientation of the water dipole. If one assumes that the dipole is preferentially oriented with its positive side to the mercury,

then reorientation would occur at positive surface charges. In the region where reorientation is occurring, the dipole should be freer to rotate with the alternating field. This results in a larger dielectric constant. One could also explain the peak by a variation in the thickness of the inner layer, which in fact was Grahame's choice. Peaks which can not be ascribed to specific adsorption also occur in other solvents at both positive and negative surface charge densities.<sup>22</sup> This tends to support the dipole reorientation interpretation as opposed to a change in thickness. The remainder of the curve can be explained by a combination of electrostriction and dielectric saturation.

## 2. The chloride ion.

The adsorption of KCl was studied by Grahame and Parsons.<sup>12</sup> The isotherms at constant charge are definitely curved and would give a value of  $q^1 = -q$  at infinite dilution if the linearity at low concentration was maintained. This effect has been observed in the adsorption of the  $I^-$ ,  $Cl^-$ ,  $Br^-$ ,  $NO_3^-$  ions from single salt solutions.<sup>23</sup> At infinite dilution one would expect  $q^1$  to equal zero rather than  $-q$ . There is at present no reasonable explanation for this effect. The variation of  $q^1$  with  $q$  at constant concentration is similar to that for KI and KBr, and the linear portions have the same slope. The components of the capacity were obtained from plots of  $\phi^{m-2}$  versus  $q^1$  at constant surface charge. The points at constant surface charge were considered to lie on a straight line. Therefore  $q^1 C^i = q^1 K^i$  and  $q^1 K^i$  is a function of surface charge only. There are large systematic deviations from a straight line which cast doubt on the constancy of  $q^1 K^i$ . In any case, using the constant values, the other components of the capacity were derived.  $q^1 K^i$  decreases with increasing surface charge and  $q^1 K^i$  must therefore also vary with  $q^1$ . Parsons compared ✓

$q^1 K^i$  at  $q^1 = 0$  to the integral capacity of the inner layer in a KF solution and found reasonable agreement. The integral capacity is given by

$$K = \frac{1}{\phi^{m-2}} \int_0^\phi C^i d q$$

The distance ratio was calculated by both the isotherm and capacity ratio methods. The values obtained from the two methods are different, but in each case they are lower than those obtained for KI. On this basis it is assumed that  $X_1$  is larger for the chloride ion than for the iodide ion.

Payne has studied the adsorption of KCl from constant ionic strength solutions of KCl and KF.<sup>24</sup> The capacity curves have a distinct peak which becomes more prominent with increasing concentration. The peak remains when the inner layer capacity is determined and  $C^i$  is almost independent of concentration except at low concentrations. As in the pure KCl system,  $\frac{1}{q} C^i = \frac{1}{q} K^i$  and is a function of charge only. In contrast to pure KCl,  $\frac{1}{q} K^i$  increases with increasing surface charge. The fact that  $C^i$  is almost independent of concentration is due to a simultaneous decrease in  $\frac{1}{q} C^i$  and increase in  $\left| \frac{1}{q^1 K^1} \left( \frac{\partial q^1}{\partial q} \right)_\mu \right|$  as  $|q^1|$  increases. The adsorption was found to fit a virial isotherm with  $\ln \beta$  a non-linear function of the surface charge. Both the virial isotherm and the non-linear dependence of  $\ln \beta$  on  $q$  are supported by Payne's plots of  $-\Delta \frac{1}{C}$  versus  $q^1$  at constant surface charge. These plots approach a limiting value for each charge. The limiting values are different due to the second term in  $-\Delta \frac{1}{C}$ . When  $-\Delta \frac{1}{C}$  is plotted versus  $q$  at constant concentration, a peak occurred near  $q=6$ , and was followed by a decrease and approach to a limiting value. This is not true quadratic behavior in which the peak would be followed by a minimum and then another peak. Payne found that his isotherms could not be superimposed on the

pure KCl isotherms whether he used  $a_{\pm}$  or  $a_{\pm}^2$  for the activity.

### 3. The bromide ion.

Recently, the adsorption of the bromide ion has been studied as part of an experiment whose primary purpose was to compare the two distinct methods of investigating the electrical double layer.<sup>25</sup> These are the electrocapillary curve and the differential capacity curve. It was determined that neither a virial or Frumkin isotherm fit the data. A complete analysis of specific adsorption was not presented.

### 4. The iodide ion

Grahame performed the most complete study of the adsorption of KI in water.<sup>26</sup> He found that  $q^1$  was an approximately linear function of  $q$  at constant concentration except at quite negative values of  $q$ . The isotherms at constant charge were linear except at low concentrations where they begin to approach  $q^1 = -q$ . Grahame assumed this was due to experimental error and he used values of  $q^1$  obtained by extrapolating the linear part of the curve. In a latter paper, Parsons, using Grahame's data, found that iodide adsorption fits a virial isotherm with  $\ln \beta$  a linear function of the surface charge. It is not clear whether Parsons used Grahame's experimental data or his "corrected" data. The compounds of the capacity were then analyzed and  $\frac{1}{q} C^i$  was found to be a function of charge only.  $\frac{1}{q} C^i$  changes from  $83 \mu\text{f}/\text{cm}^2$  at  $q = -12$  to  $70 \mu\text{f}/\text{cm}^2$  at  $q = 16$ . There are systematic deviations from these constant values which he assumed to be within experimental error. The intercept for the  $q = 0$  line gave a value of  $E_z$  for KF which was 16 mv too cathodic. There must therefore be some curvature at low concentrations. Using his values of  $\frac{1}{q} C^i$ , he determined  $q C^i$ . The value of  $q C^i$  was independent of  $q^1$  and approximately equal to

$C^i$  for KF at the same value of  $q$ . The equivalence of  $C^i$  and  $\frac{C^i}{q}$  implies that the adsorbed ions do not have the same effect as the surface charges.

Dutkiewicz and Parsons studied the adsorption of KI from constant ionic strength solutions of KI in KF.<sup>28</sup> Parsons was able to fit the  $\Delta E$  versus  $\ln x$  curves to a single composite curve and found the  $\ln \beta$  was a linear function of the surface charge. The highest value of the surface charge used in this work appears to be  $q = -4$  and the largest value of  $q^1$  was -12. Presumably the rapid rise in the capacity at more positive charge did not allow accurate data to be obtained. Plots of  $\Delta \frac{1}{C}$  versus concentration indicate a Henry's law isotherm with  $\frac{\partial \ln \beta}{\partial q}$  a constant. Plots of  $\phi^{m^{-2}}$  versus  $q^1$  at constant charge were linear and parallel within experimental error.  $q^1 K^i$  was equal to  $89 \mu F/cm^2$ . The intercept found from these plots is quite different than that found from the pure KI data which should not be the case. The distance ratio is larger in KI+KF than in pure KI implying that  $X_1$  is smaller in KI+KF. The constant value of  $\partial \ln \beta / \partial q$  is supported by the  $\Delta E$  versus  $\ln x$  curves which can be fit to a single composite curve. If the adsorption isotherms at constant charge are plotted against the salt activity, the curves for KI and KF + KI can be superimposed. This can not be done if the anion activity is used. At the time this result appeared to resolve the question of which activity to use in the isotherm, but further work has shown it to be limited to the iodide system.

#### B. The adsorption of KBr from a constant ionic strength solution of KBr in KF .

##### Introduction

As should be obvious from the discussion of previous research, the adsorption of halide ions is not as simple as one would first expect. One of the main problems is to explain the different behavior of KCl and KI

when they are adsorbed from constant ionic strength solutions with KF. The difference between the iodide and chloride ion is much more pronounced in the mixed electrolyte systems than in the single salt systems. One possible explanation is that there are no qualitative differences, and that this would be apparent if iodide adsorption could be studied at positive surface charge densities. The bromide ion is intermediate in its strength of adsorption between the chloride and iodide, and the purpose of this experiment was to study its adsorption as compared to the other halides. The mixed electrolyte system was chosen for two main reasons: 1) The analysis can be more rigorously justified than that for a single salt. 2) The data for KI+KF and KCl+KF is more complete and probably more reliable than the earlier work on the single salt systems.

One of the benefits of choosing the mixed electrolyte system is a simplification which occurs in the electrocapillary equation and allows the specifically adsorbed charge to be determined without first determining the diffuse layer charge. We begin with the previously derived equation:

$$d\gamma = -q dE - \Gamma_{F,w}^- d\mu_{KF} - \Gamma_{Br,w}^- d\mu_{KBr}$$

We assume that the activity coefficients of KBr and KF are dependent only on the total ionic strength.

Therefore

$$d\mu_{KF} = R T d \ln m_{KF} = k T d \ln(1-x)$$

$$d\mu_{KBr} = R T d \ln m_{KI} = k T d \ln x$$

where x is the molarity of KBr, the total molarity being 1M. Substituting in the electrocapillary equation gives

$$d\gamma = -q dE - \left[ \Gamma_{Br,w}^- - \left( \frac{x}{1-x} \right) \Gamma_{F,w}^- \right] k T d \ln x$$

From diffuse layer theory and the assumption that the fluoride ion is not specifically adsorbed, one gets the relationship:

$$\frac{\Gamma_{Br}^d}{\Gamma_F^d} = \frac{x}{1-x}$$

also

$$\Gamma_{Br}^- = \Gamma_{Br}^i + \Gamma_{Br}^d$$

Therefore

$$dy = -q dE - \Gamma_{Br}^i k T d \ln x$$

and

$$d\xi = E d q - \Gamma_{Br}^i k T d \ln x$$

The specifically adsorbed charge is determined directly from the differentiation of  $\xi$  and  $y$ . The assumptions used here are more general than those needed for adsorption from a single salt. We are assuming that  $\Gamma_{Br}^d$  is proportional to  $x$ , whereas in the single salt system we would have to derive  $\Gamma_{Br}^d$  from a specific equation. The determination of the amount specifically adsorbed is therefore more reliable. Another simplification arises when isotherms are considered. In the mixed electrolyte system the choice of activity does not arise since the assumption that the activity coefficients are constant is equivalent to setting  $d \ln a_K^+ = 0$  in the following equation.

$$d \ln a_{KBr} = d \ln a_K^+ + d \ln a_{Br}^- = d \ln m$$

but

$$d \ln a_{Br}^- = d \ln m.$$

Either assumption leads to using  $x$  for the activity.

### Experimental

All experiments were performed with the previously discussed equipment. Reagent grade chemicals were used without further purification, but the water used was distilled from alkaline potassium permanganate. The reliability of the equipment and the absence of adsorbable impurities in the salts was confirmed by comparing our results for 1 MKF and 1MKBr with those previously reported in the literature. The capacity was measured at 50 mv intervals from at least -1.4v to the most positive voltage obtainable. This is usually -.2 volts. In the region where the capacity peak occurs, smaller voltage intervals were used. Five capacitance decades from  $1\mu F$  to  $.0001\mu F$  were available and balance was reproducible to  $\pm .0002\mu F$ , which represents .1% in the measured capacity. Streaming electrode potentials were as previously stated reproducible to within 1 mv.

### Results

The capacity of eleven solutions of  $x\text{MKBr} + (1 - x) \text{ MKF}$  were measured at  $25^\circ\text{C}$  and are shown in Figure 4. These curves are qualitatively similar to those found in  $\text{KCl} + \text{KF}$  in that a distinct peak occurs at higher concentrations. The peak in the KBr curves occurs at a higher value of the capacity and a more negative value of the potential than in KCl. It is also less pronounced. This shift in the peak height and position is due to the stronger adsorption of the bromide ion. The capacity curves are equivalent when the potential is less than -1.3 volts. This fact was used in integrating the curves. The capacity curve is integrated by fitting each successive set of three points to a parabola. The first integral gives  $q$  and the second  $\gamma$  and  $\xi$ . The values of  $q$ ,  $C$ ,  $E$ ,  $\gamma$ , and  $\xi$  are then

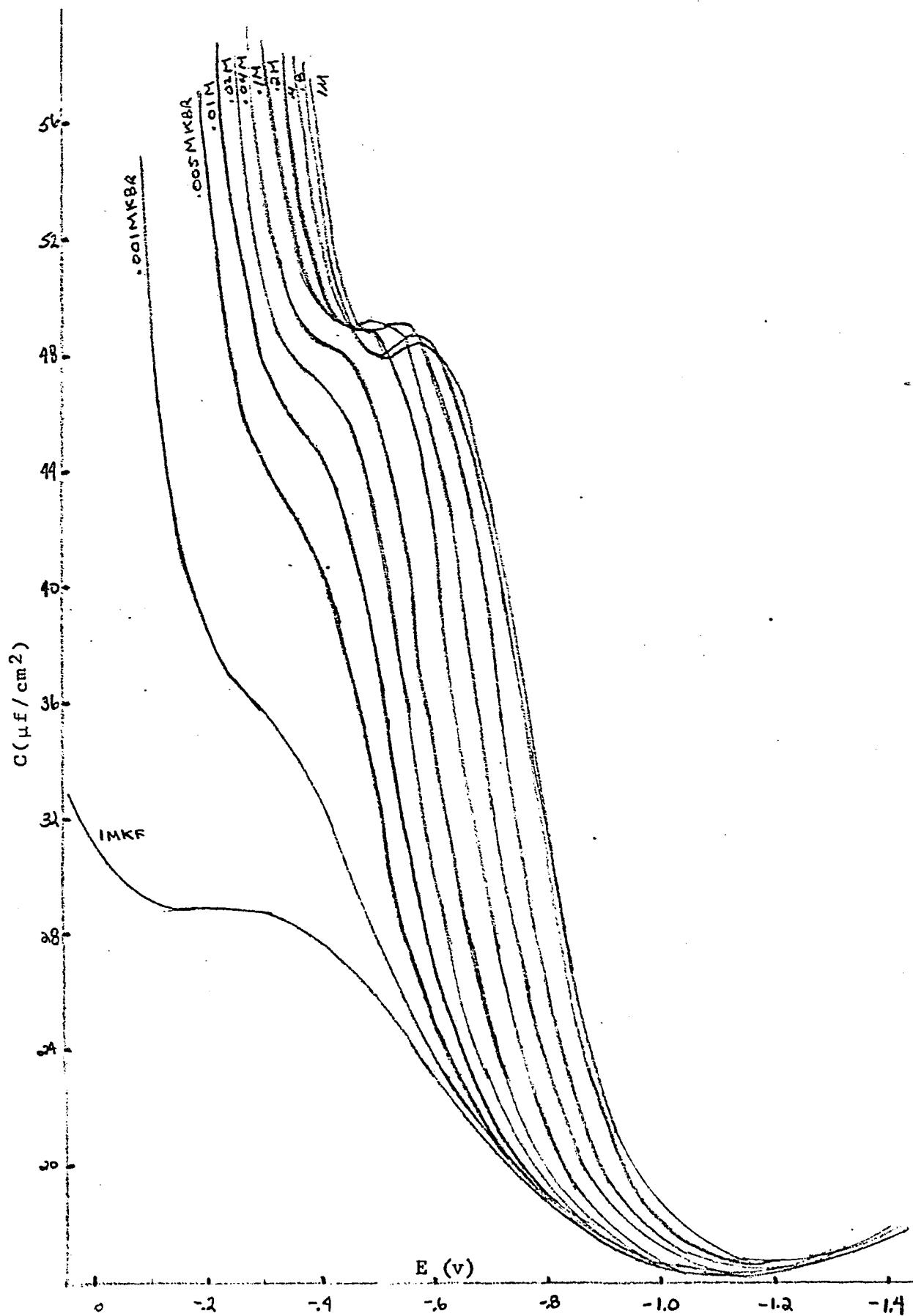


Figure 4. The Capacity of The Double Layer as a Function of Potential for  $x\text{MKBr} + (1-x)\text{MKF}$

found for all integral values of  $q$  which occur in the range covered by the three experimental capacity points. The program then reads another experimental point and uses the determined values of the second point for the integration constants. The program is discussed in more detail in the appendix. One set of integration constants is needed to use the program. These are usually  $E$ ,  $C$ ,  $\gamma$  at  $E = Ez$ . Due to the fact that all of the curves are equivalent at large negative values of the potential, we may avoid the determination of  $\gamma$ . We integrate the 1MKF curve assuming  $\gamma = 0$  at  $E = Ez$ , and obtain the value of  $\gamma$ ,  $C$ ,  $E$  at  $q = -19$ . The KBr + KF curves can now be integrated from  $q = -19$  using the 1MKF data for the integration constants. If this procedure is valid, the values of  $Ez$  computed by the integration and those directly determined by the streaming electrode method must be equivalent. The two sets of values are presented in Table 1.

Table 1

Solution	Concentration x	$Ez$ (Ex)	$Ez$ (Com)
1	0	- .4740	-
2	.001	- .4820	- .4828
3	.005	- .4996	- .4988
4.	.01	- .5130	- .5127
5	.02	- .5295	- .5300
6	.04	- .5486	- .5486
7	.1	- .5769	- .5776
8	.2	- .6004	- .6020
9	.4	- .6245	- .6252
10	.8	- .6477	- .6472
11	1	- .6550	- .6568

The agreement is well within the acceptable limits. The second program then takes the derivative of  $\xi$  by  $\ln x$  at constant  $q$  to give  $q^1$  since

$$d\xi = E d q + \frac{k T N}{F} q^1 d \ln x$$

The programs and data are presented in the appendix. In the course of evaluating the data, we decided not to use the .001M KBr set. It was decided that the results of the second program were more reliable if this set of data were excluded. It would be interesting to study the adsorption of KBr at low concentrations, but this would require the use of a frequency extrapolation of the capacity. The reliability of this procedure has not been demonstrated for ionic solutions. To show that the procedure was reliable, the equivalence of the twice integrated capacity curves and experimentally determined electrocapillary curves must be demonstrated. There is also the possibility that at very low concentrations the streaming electrode potential may not be the same as the potential at the point of zero charge. This will occur if equilibrium is not reached at the streaming electrode.

The specifically adsorbed charge is plotted against the surface charge at constant concentration in Figure 5 and the isotherms are plotted in Figure 6 at constant charge. The  $q^1$  versus  $q$  curves are similar to those for KCl + KF. The major difference is that they become almost linear at lower values of the surface charges. The effect of the stronger adsorption of  $\text{Br}^-$  than  $\text{Cl}^-$  is also evident in the isotherms. The isotherms for KCl + KF and KI + KF are similar in shape to the KBr + KF isotherms for  $q < 0$ . In the case of KI no data was taken above  $q = -4$ , for KCl the amount adsorbed at any concentration and charge is almost 40% less than for KBr. The change in the curvature of the isotherms has not been previously noted and at  $q > 12$  appears to indicate that saturation is being approached. An attempt was made to determine the isotherm and the charge dependence of the standard free energy. The surface pressure versus  $\ln x$  curves can not be superimposed on one common curve with the same accuracy

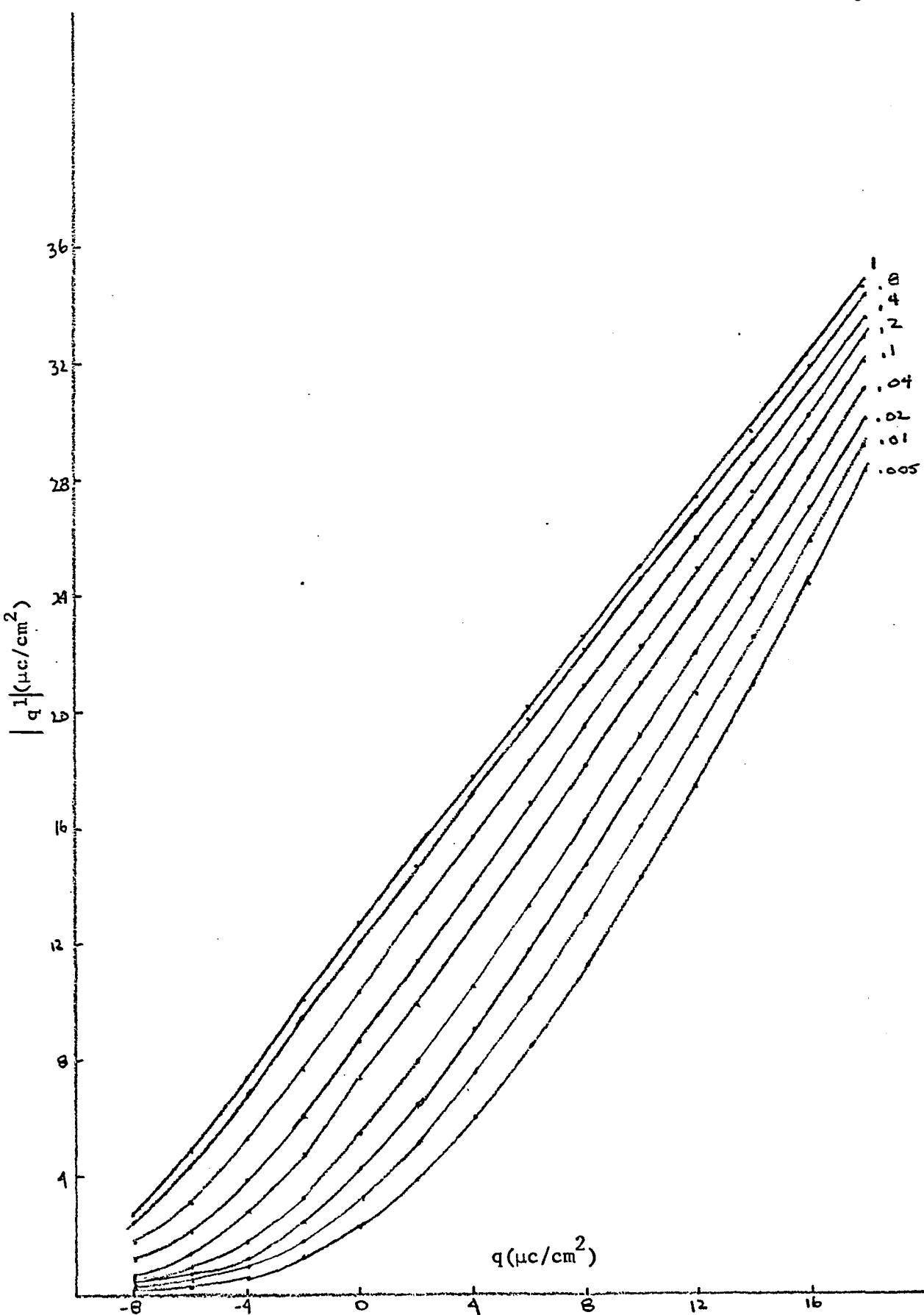


Figure 5. The Variation of The Amount Specifically Adsorbed with The Surface Charge Density at Constant Concentration for  $x$  MKBr +  $(1-x)$  MKF

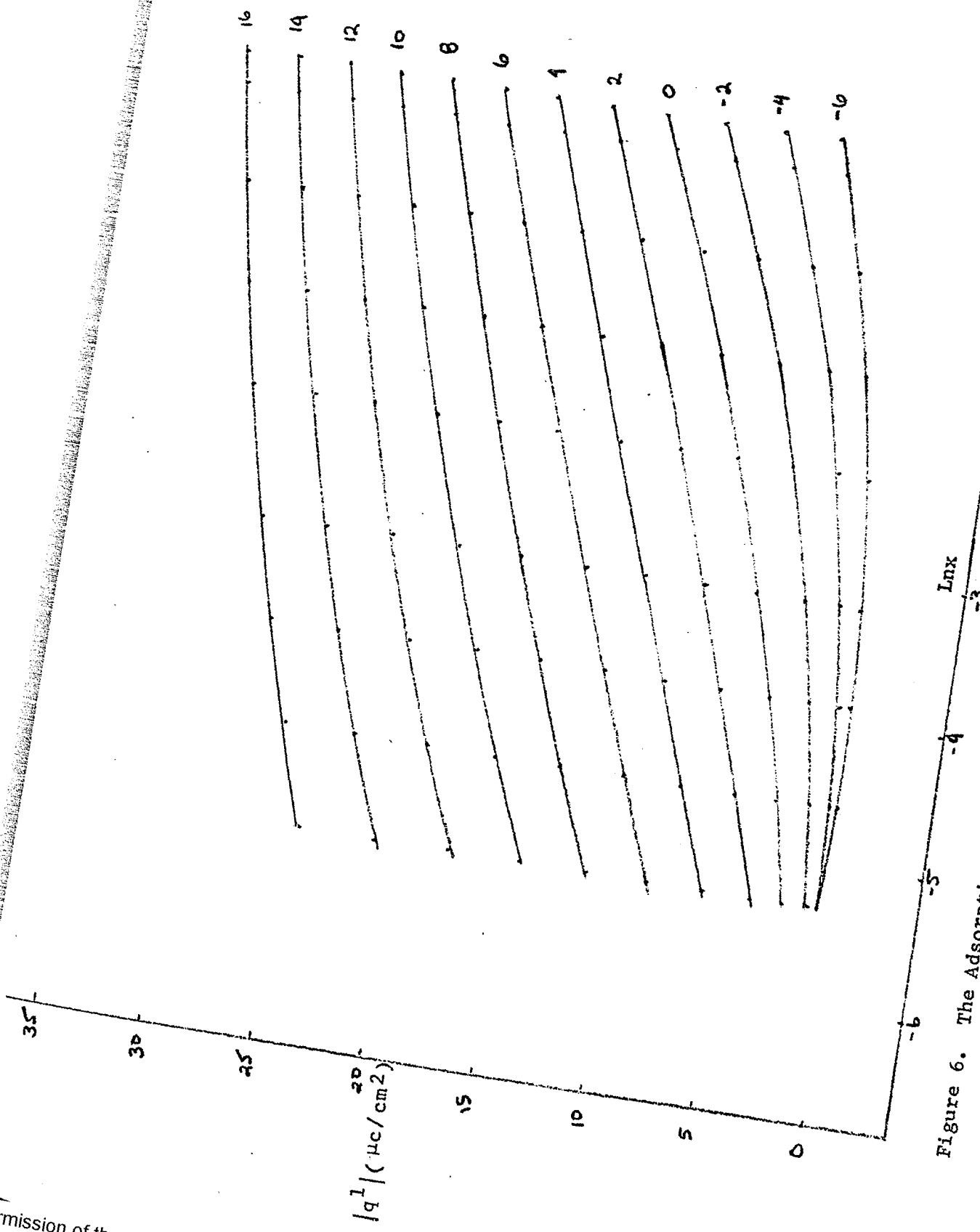


Figure 6. The Adsorption Isotherms at Constant Surface Charge for  $x \text{ KBr} + (1-x) \text{ KF}$

as in the KCl-KF system. Payne claims that his deviations from a common curve using a virial isotherm are no greater than .2 ergs/cm<sup>2</sup>. In this system deviations of up to 5 ergs/cm<sup>2</sup> occur at large  $q > 8$  if the best possible curve is drawn. One explanation is that the isotherm constants are a function of the surface charge. Another is that the surface pressure method is inaccurate due to the ambiguities in choosing 1MKF as the base solution. To avoid the surface pressure problem, the virial isotherm was checked by plotting  $\Gamma_{Br^-}$  versus  $\ln x/\Gamma_{Br^-}$  at constant  $q$ . As is evident in Figure 7, straight lines are not obtained. The low concentration values for  $q=-4$ ,  $q=-6$ , can be disregarded because of the small value of  $q^1$ . If a virial isotherm were obeyed, the curves should be both linear and parallel. If one assumes that virial isotherm is obeyed but that  $B$  is not constant, it follows from Figure 7 that  $B$  is increasing with  $q$  at constant  $q^1$  and increasing with  $|q^1|$  at constant  $q$ . The increase in  $B$  with  $|q^1|$  is quite reasonable and simply means that repulsion between adsorbed ions is occurring. The increase in  $B$  with increasing surface charge could only be explained by competitive adsorption of water. If it is harder for a bromide ion to displace a water molecule at large values of the surface charge than at low values,  $B$  will increase with the charge. Competitive adsorption results in a quadratic standard free energy and the fact that this system demonstrates quadratic behavior supports the above interpretation.

In Figure 8, the inner layer capacity is shown as a function of charge for several concentrations. The solutions not shown are virtually identical with the 1MKBr line. The concentration independence of  $C^i$  is also present in the KCl+KF system. In order to interpret the variation of  $C^i$  with  $q$ , the components of the capacity were determined. In Figure 9,  $\phi^{m-2}$  is plotted against  $q^1$  at constant  $q$  and the best straight line has been

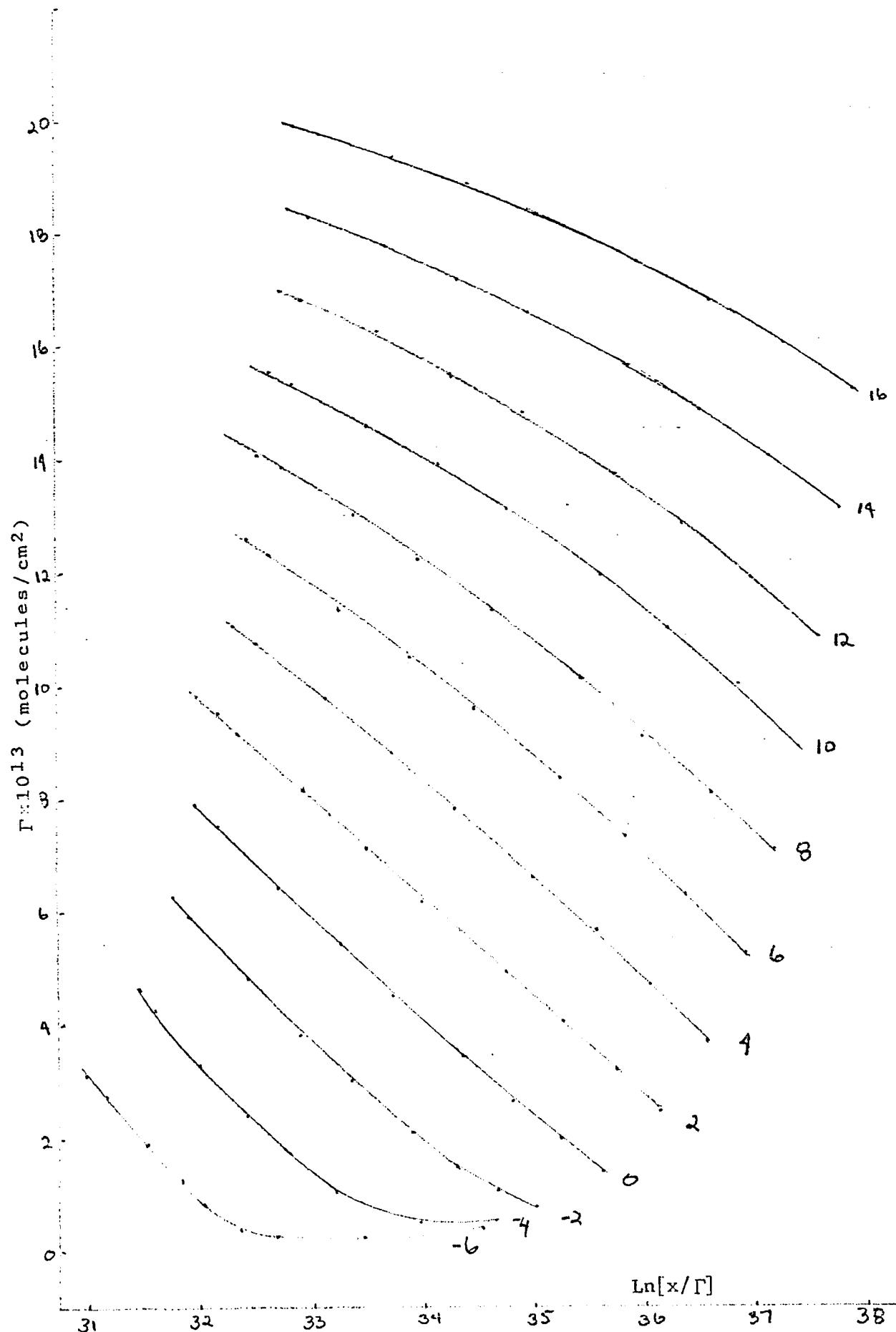


Figure 7. The Amount Specifically Adsorbed ( $\Gamma$ ) Plotted as a Function of  $\ln[x/\Gamma]$  for  $v_{MVR} + (1-v)_{MVE}$

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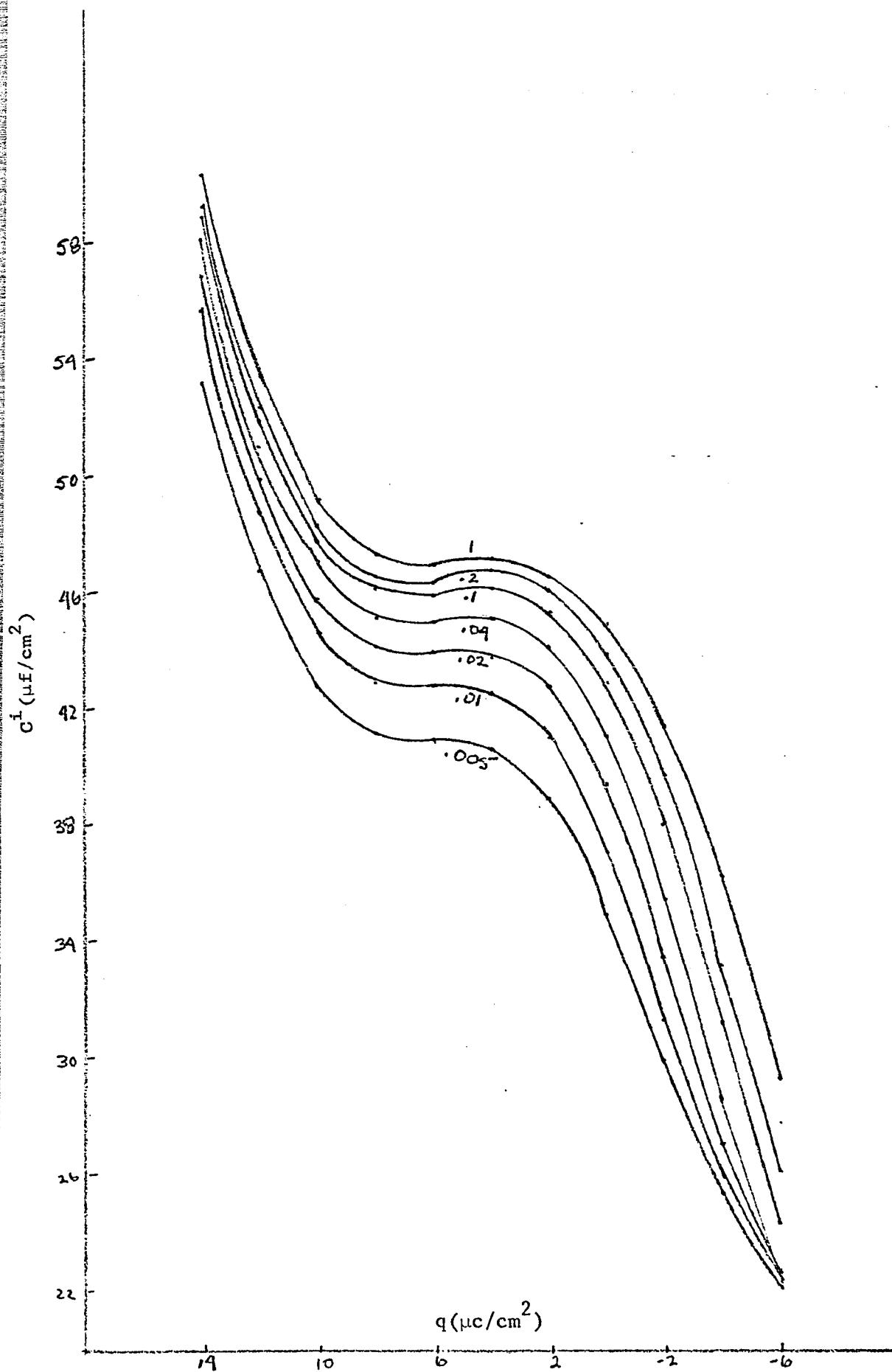


Figure 8. The Inner Layer Capacity of  $x\text{MKBr} + (1-x)\text{MKF}$  as a Function of Surface Charge Density

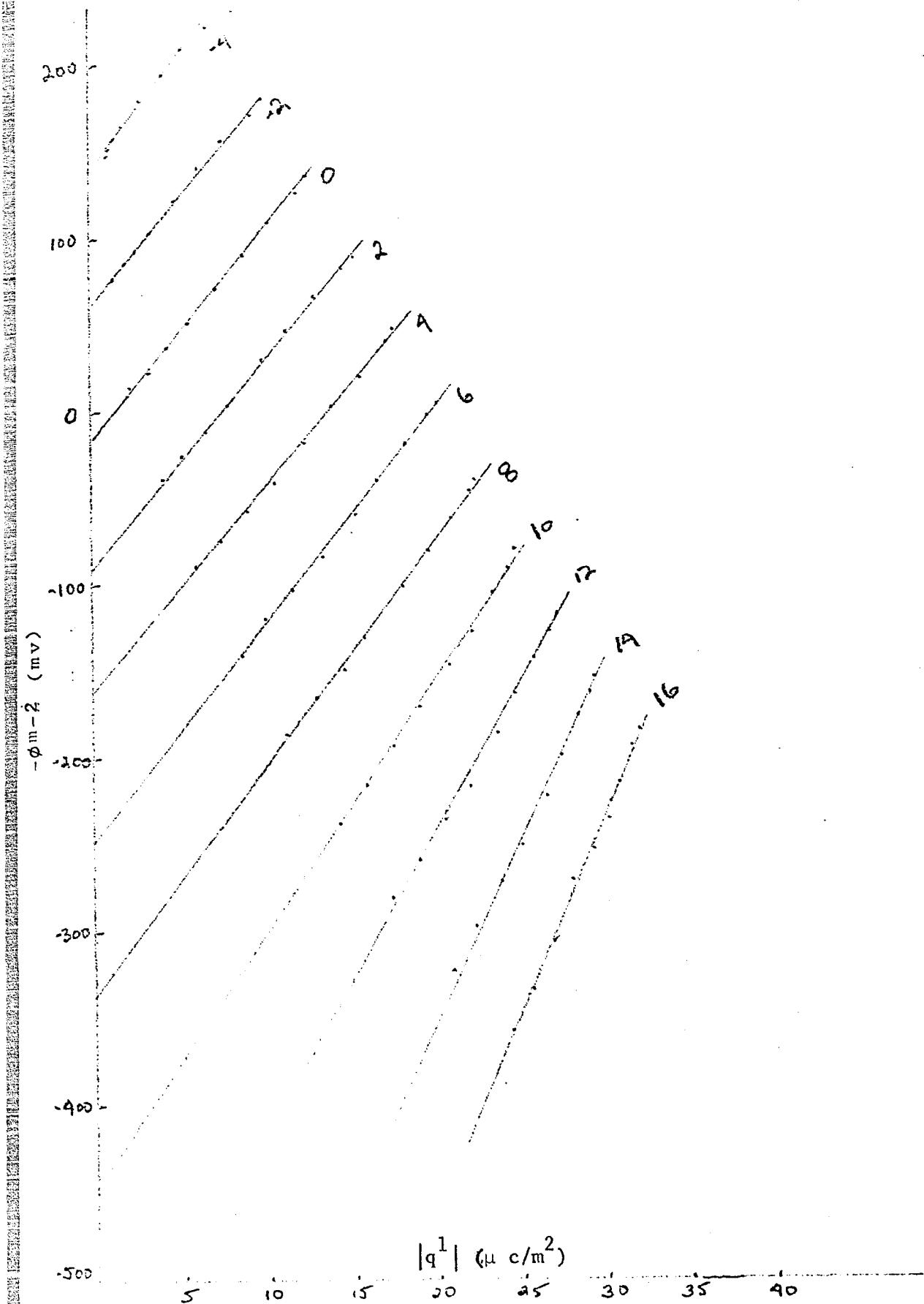


Figure 9. The Potential Across the Inner Layer Plotted as a Function of Specifically Adsorbed Cahrge for  $x\text{MKBBr} + (1-x)\text{MKF}$

drawn through the points. Though it is not apparent on this graph due to its scale, the points appear to lie on a parabola rather than a straight line. The equation for the components of the capacity is:

$$\frac{1}{c^i} = \frac{1}{q c^i} + \frac{1}{q^1 c^i} \left( \frac{\partial q^1}{\partial q} \right)_u$$

$\left( \frac{\partial q^1}{\partial q} \right)_u$  was obtained by fitting the  $q^1$  versus  $q$  data to a cubic equation and obtaining its shape. These values were checked against the graphically determined values.  $\frac{1}{q} c^i$  is obtained either from the inverse of the slope of the lines in Figure 9, in which case it is equal to  $\frac{1}{q} K^i$  or from the inverse of the slope of a quadratic equation giving  $\phi^{m-2}$  as a function of  $q^1$ . Both of these methods were used to evaluate  $\frac{1}{q} c^i$ . The values of  $\frac{1}{q} K^i$  obtained from the Figure 8 are presented in Table 2.

Table 2

$q$	$\frac{1}{q} K^i$
-6	84.7
-4	80.0
-2	84.8
0	86.8
2	85.0
4	83.8
6	80.4
8	74.1
10	66.3
12	60.3
14	52.1

The decrease in  $q^1 K^i$  with increasing charge would be explained by a decrease in  $\epsilon/(x_2 - x_1)$  according to the present model. A decrease in either  $\epsilon$  or  $x_1$  seems perfectly reasonable, but no distinction between the two is possible. The intercept of  $\phi^{m-2}$  at  $q^1 = 0$  are not the  $\phi^{m-2}$  values for 1MKF solution, so that if the model is valid, the lines must be curved at lower concentrations. The two sets of values for  $q^1 C^i$  were used to obtain  $q^1 C^i$ . Figure 10 shows  $q^1 C^i$  as a function of  $q$  for four concentrations where the linear value of  $q^1 C^i$  were used. In Figure 11, the quadratic values were used. The most important point is that independent of the method used,  $q^1 C^i$  has a distinct peak in the region  $q = 0$  to  $q = 4$ . This peak can not be due to specific adsorption since the peak height and position are virtually independent of concentration and therefore of specific adsorption. In Figure 11,  $q^1 C^i$  remains independent of the amount of specific adsorption even at large values of the surface charge whereas the curves in Figure 10 are different in this region. A peak in  $q^1 C^i$  which is independent of  $q^1$ , must be due to some alteration of the interaction between the electrode and the solvent. As mentioned previously,  $q^1 C^i$  is independent of concentration in KI solutions. In the KCl+KF system,  $q^1 K^i$  decreases as  $|q^1|$  increases at constant  $q$ . It follows that if  $q^1 K^i$  is plotted against  $q$  at constant concentration, the curves at higher concentrations are lower. In the KI system,  $q^1 K^i$  is independent of concentration and increases with increasing charge. In KBr+KF,  $q^1 K^i$  is independent of concentration when  $q < +4$ . At larger values of the surface charge,  $q^1 K^i$  eventually begins to increase depending on the concentration. The variation of  $q^1 K^i$  with surface charge at constant concentration is shown in Figure 12 for three concentrations. The increase in  $q^1 K^i$  with increasing  $q^1$  is evident from the vertical distance between the curves in the

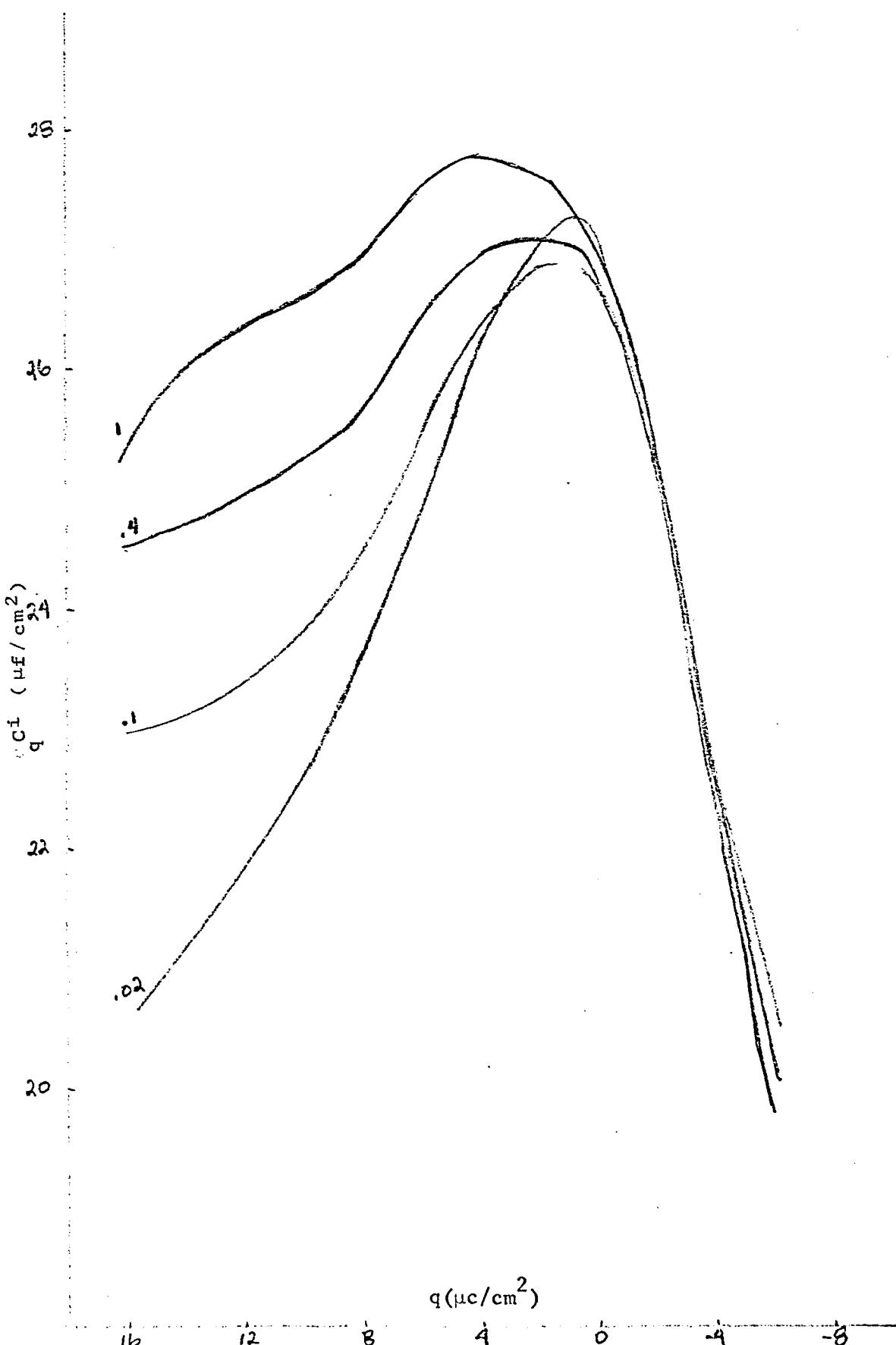


Figure 10. The Differential Capacity at Constant Amount Adsorbed as a Function of Surface Charge Density for  $x\text{MKBr} + (1-x)\text{MKF}$  Using Values of  $C_1$  Determined from Figure 9.

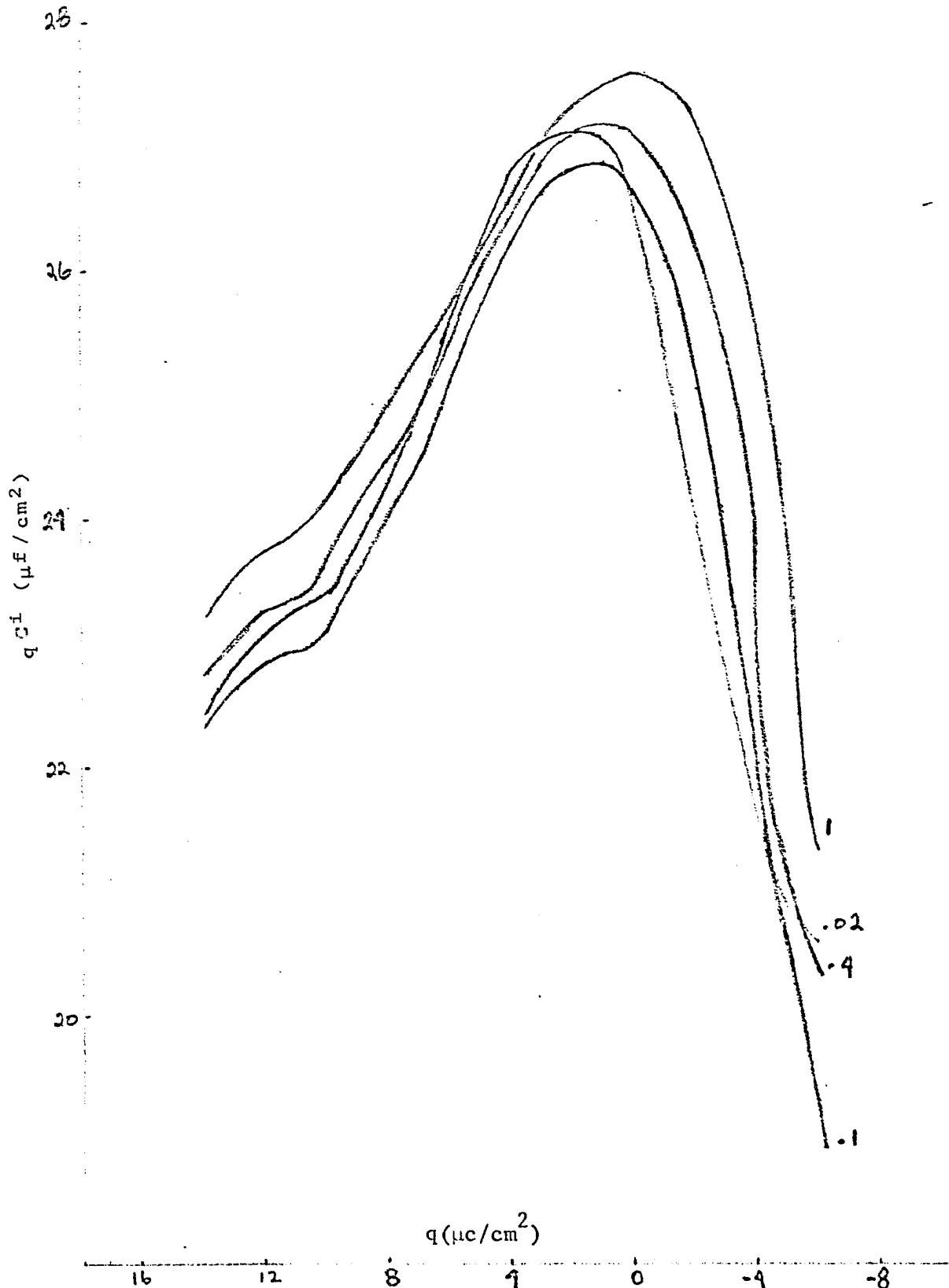


Figure 11. The Differential Capacity at Constant Amount Adsorbed as a Function of Surface Charge Density for  $x\text{MKBr} + (1-x)\text{MKF}$  Using values of  $1/c_1$  determined by Durrance et al.

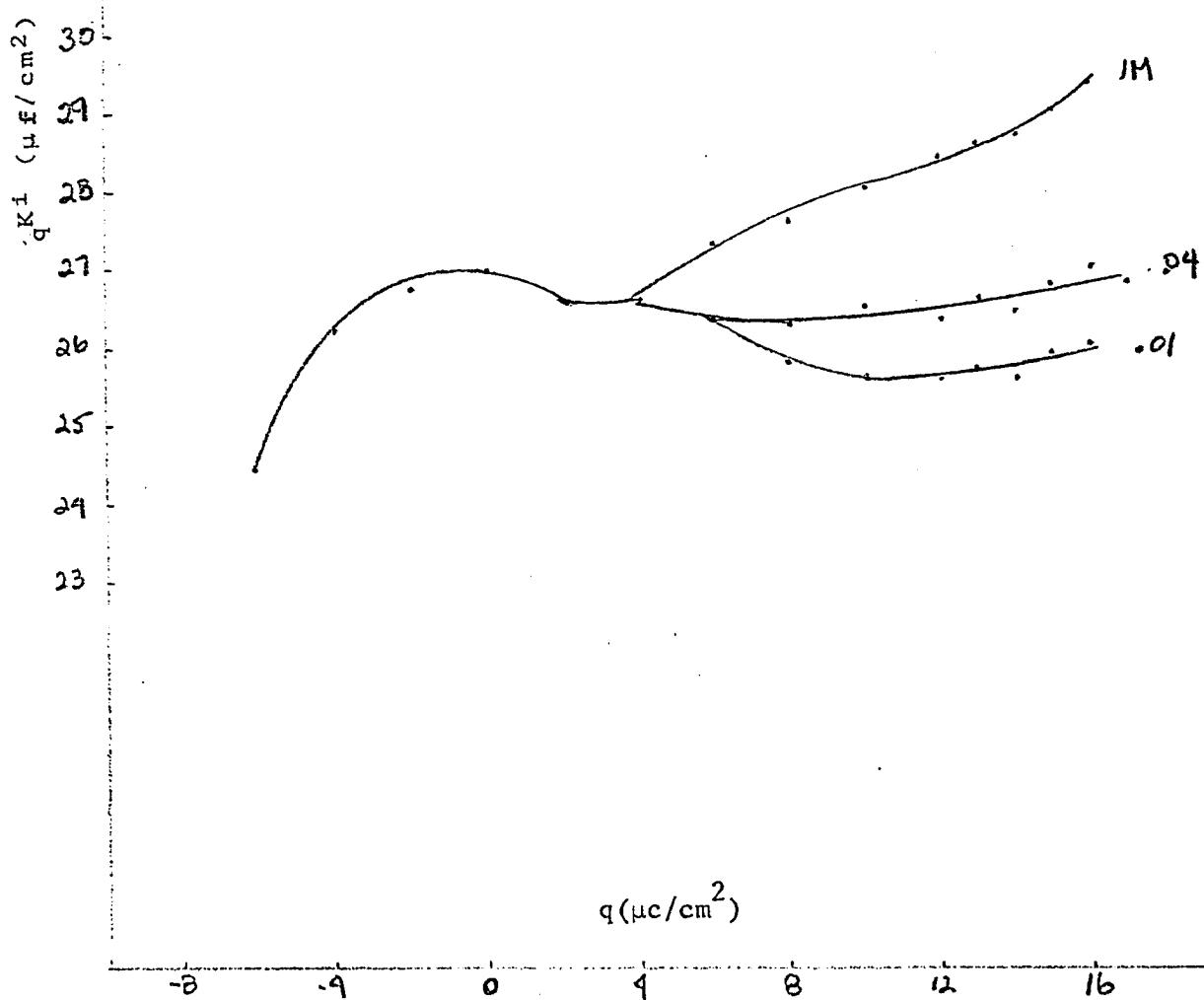


Figure 12. The Integral Capacity at a Constant Amount Adsorbed as a Function of Surface Charge Density for  $x\text{MKBBr} + (1-x)\text{MKF}$

anodic region. There is no convincing argument to explain the different behavior of the three systems.

As derived in the theoretical section, the equation relating the capacity to the isotherm is the following.

$$-\Delta \frac{1}{C_i} = -k T \left[ \left( \frac{\partial \ln \beta}{\partial q} \right)^2 \frac{\partial |q^1|}{\partial \ln \beta} + |\bar{q}^1| \frac{\partial^2 \ln \beta}{\partial q^2} \right]$$

We have also shown that  $-\Delta \frac{1}{C_i}$  should reach a limiting value for large values of  $\Gamma$  if a virial isotherm is obeyed. In Figure 13,  $-\Delta \frac{1}{C_i}$  has been plotted against  $|q^1|$  at constant charge. The curves for  $q > 6$  represent amounts of specific adsorption greater than those observed by Payne. Payne ascribed the decrease in the limiting value with increasing  $q$  to the neglect of the second term in the brackets which is negative. Let us assume  $\ln \beta$  may be written as follows:

$$\ln \beta = \ln \beta_{\max} + a q - \frac{b}{2} \delta^2$$

$$|a| \gg |b| \quad \delta = (q - q_0)$$

Our equation for  $-\Delta \frac{1}{C_i}$  is then

$$-\Delta \frac{1}{C_i} = k T \left[ a^2 \frac{\partial |q^1|}{\partial \ln \beta} - b |q^1| \right]$$

where we have set  $\frac{\partial \ln \beta}{\partial q} = a$  and  $q_0$  is a constant value of  $q$ . This equation will still give a limiting value of  $-\Delta \frac{1}{C_i}$  if  $|q^1|$  is not too large. The curves at higher  $q$  also appear to approach a limiting value, though now at progressively lower values of  $B$  if we assume  $a$  and  $b$  are constant. We have already shown that if a virial isotherm is assumed,  $B$  increases with increas-

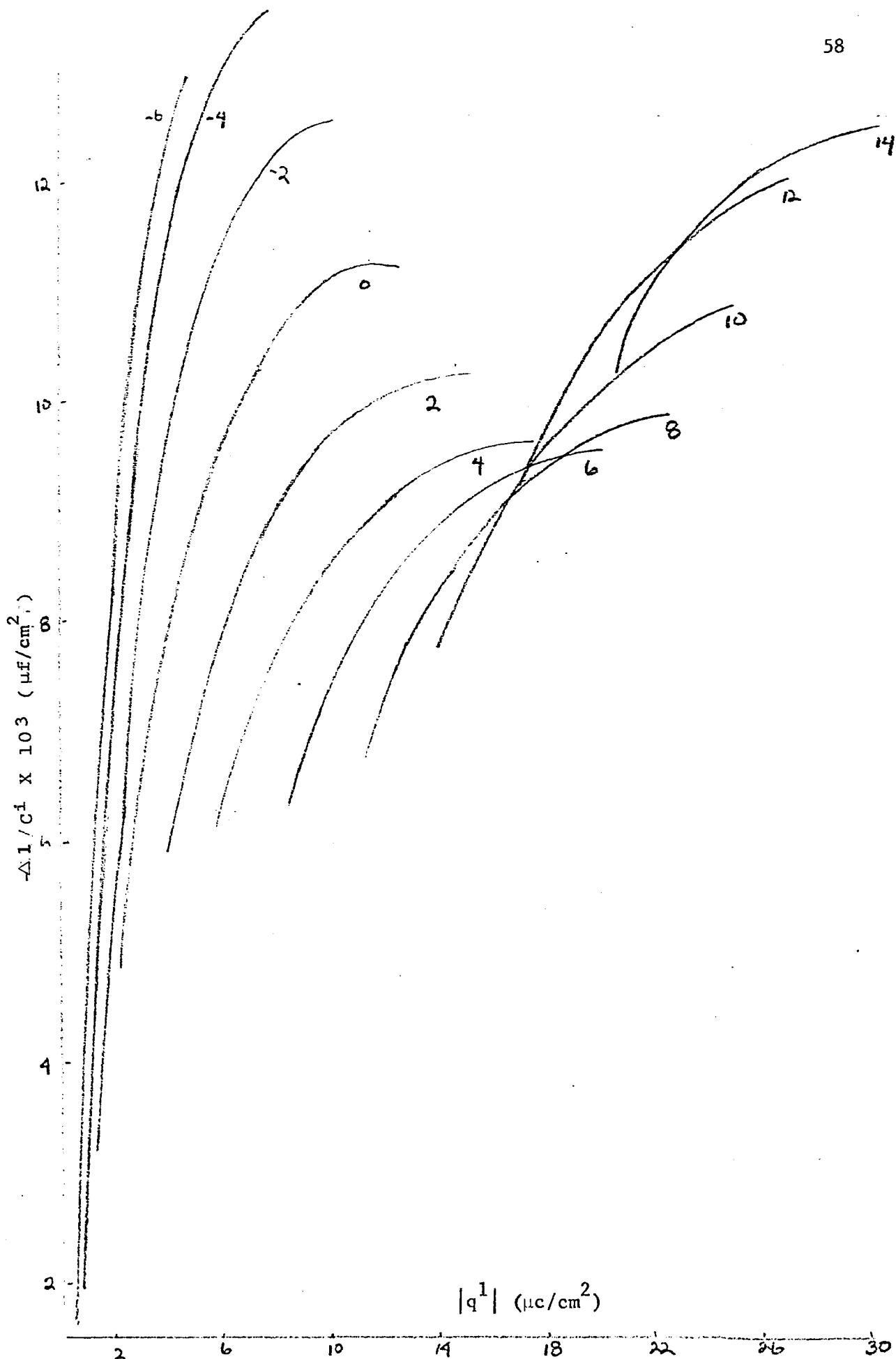


Figure 13.  $-\Delta 1/C^i \times 10^3$  Plotted Against the Amount Adsorbed at Constant Surface Charge Density

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ing charge. One could also assume that  $a$  increases faster with increasing charge than  $B$  which would give a higher value of  $-\Delta \frac{1}{C_i}$  at the limit since

$$-\Delta \frac{1}{C_i} = \frac{k T a^2}{2B}$$

We also investigated the possibility that at high values of  $q$ , the KBr + KF system might begin to behave like the KI - KF system. In the KI+KF system, a Henry's law isotherm is obeyed. That is, if we assume the following isotherm:

$$| q^{\frac{1}{2}} | = \beta C K$$

$C$  = concentration

$K$  = constant

$$\frac{\partial \ln \beta}{\partial q} = a$$

$$-\Delta \frac{1}{C} = k T a^2 K \beta C$$

In this case the curves are straight lines at constant charge when plotted against concentration and the slope increase with increasing charge. A plot of  $-\Delta \frac{1}{C_i}$  versus concentration for this system does not give straight lines except at high concentrations. Figure 14 is a plot of  $-\Delta \frac{1}{C}$  versus  $| q^{\frac{1}{2}} |$  at constant  $q$ . It is included to demonstrate that the choice between  $\Delta \frac{1}{C_i}$  and  $-\Delta \frac{1}{C}$  is not trivial and requires more justification than it has received. Figure 15 is a plot of  $-\Delta \frac{1}{C_i}$  versus  $q$  at constant concentration and Figure 16 a plot of  $-\Delta \frac{1}{C_i}$  versus  $| q^{\frac{1}{2}} |$  at constant concentration. The KCl + KF system shows the same behavior for  $q < 6$  except that the peak occurs at  $0 < q < 4$  depending on the concentration whereas here it occurs

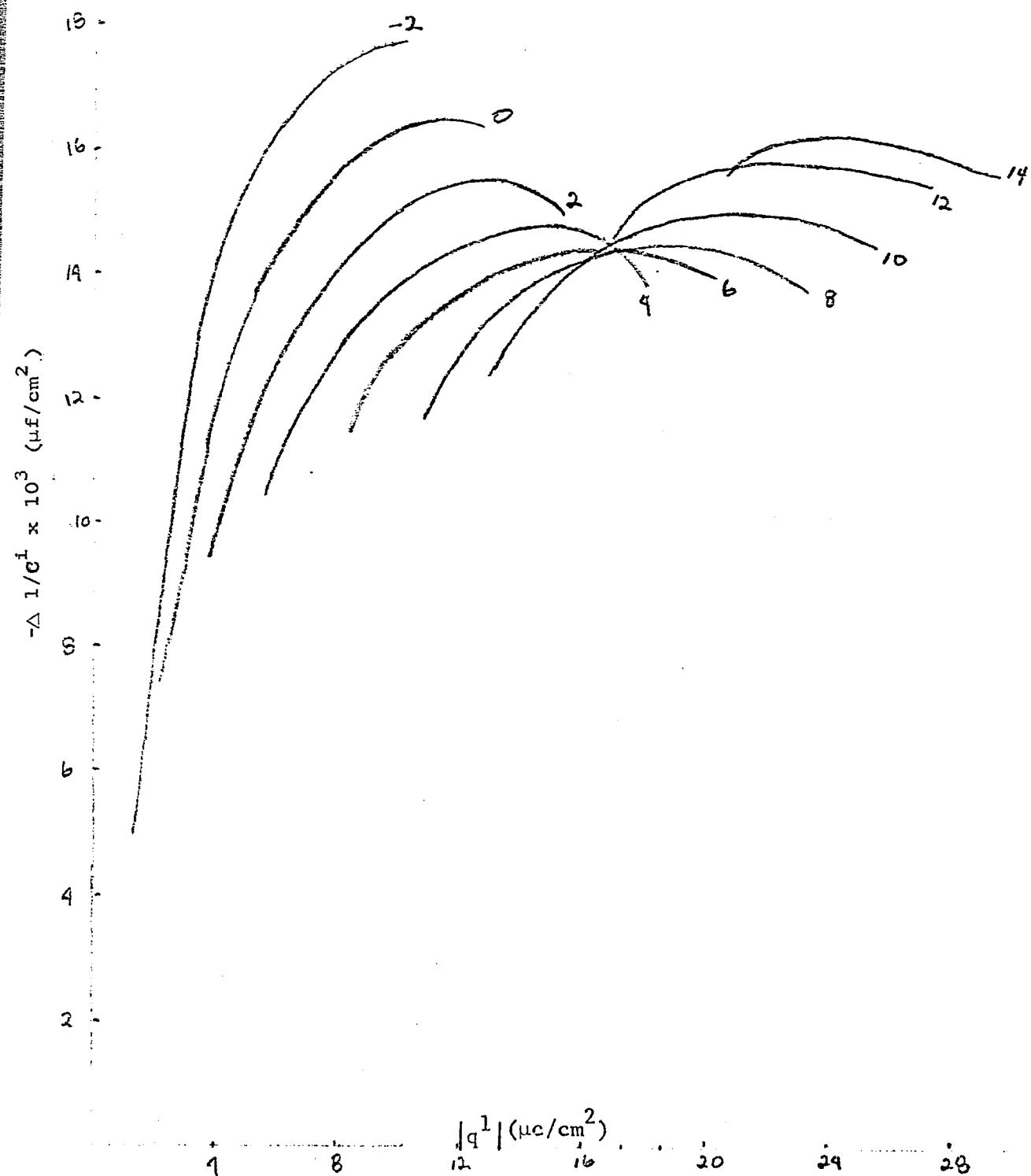


Figure 14.  $-\Delta 1/c_i^1 \times 10^3$  Plotted Against the Amount Adsorbed at Constant Surface Charge Density

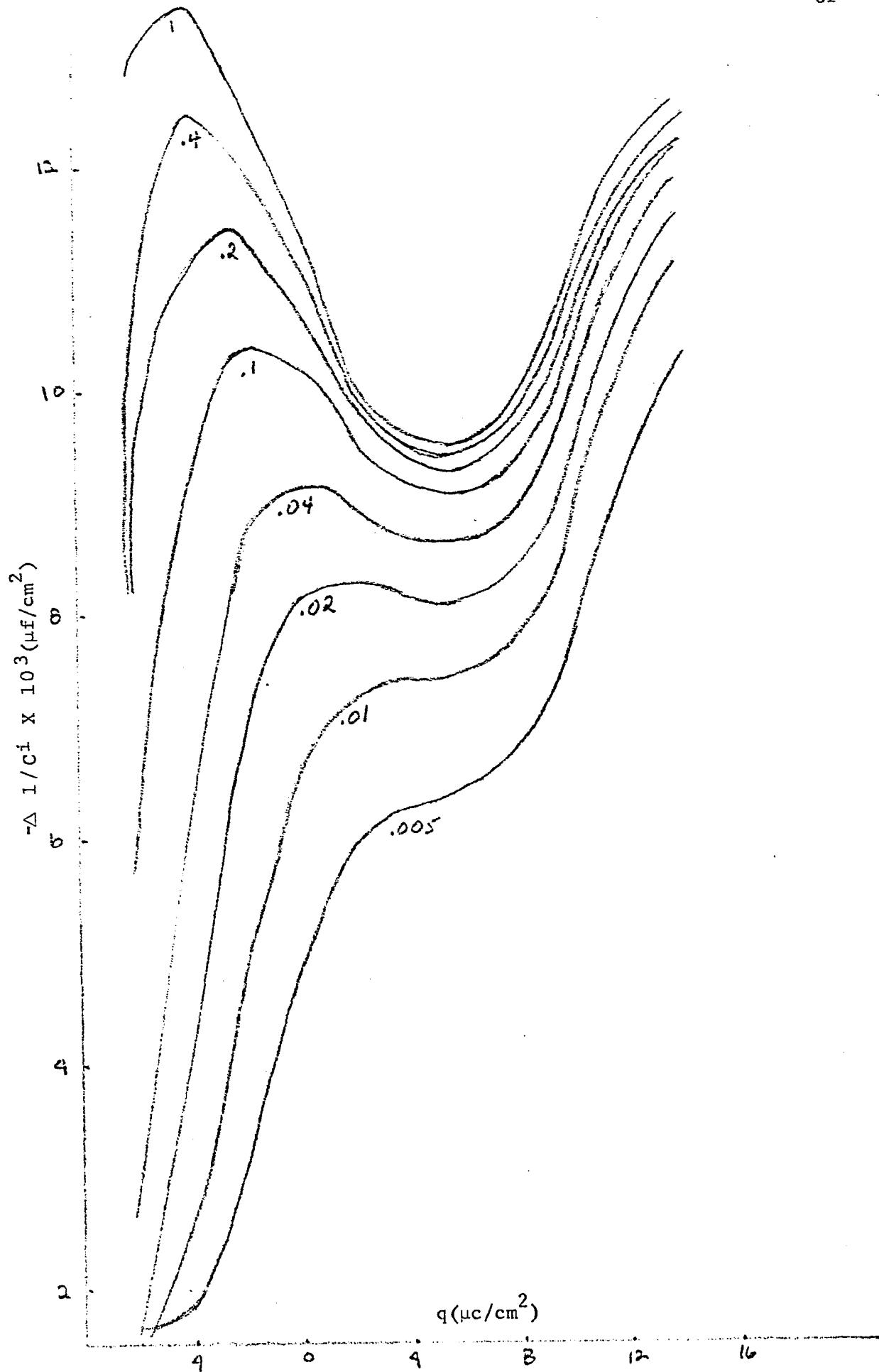


Figure 15.  $-\Delta 1/C^i \times 10^{-3}$  Plotted Against the Surface Charge Density at Constant Concentration.

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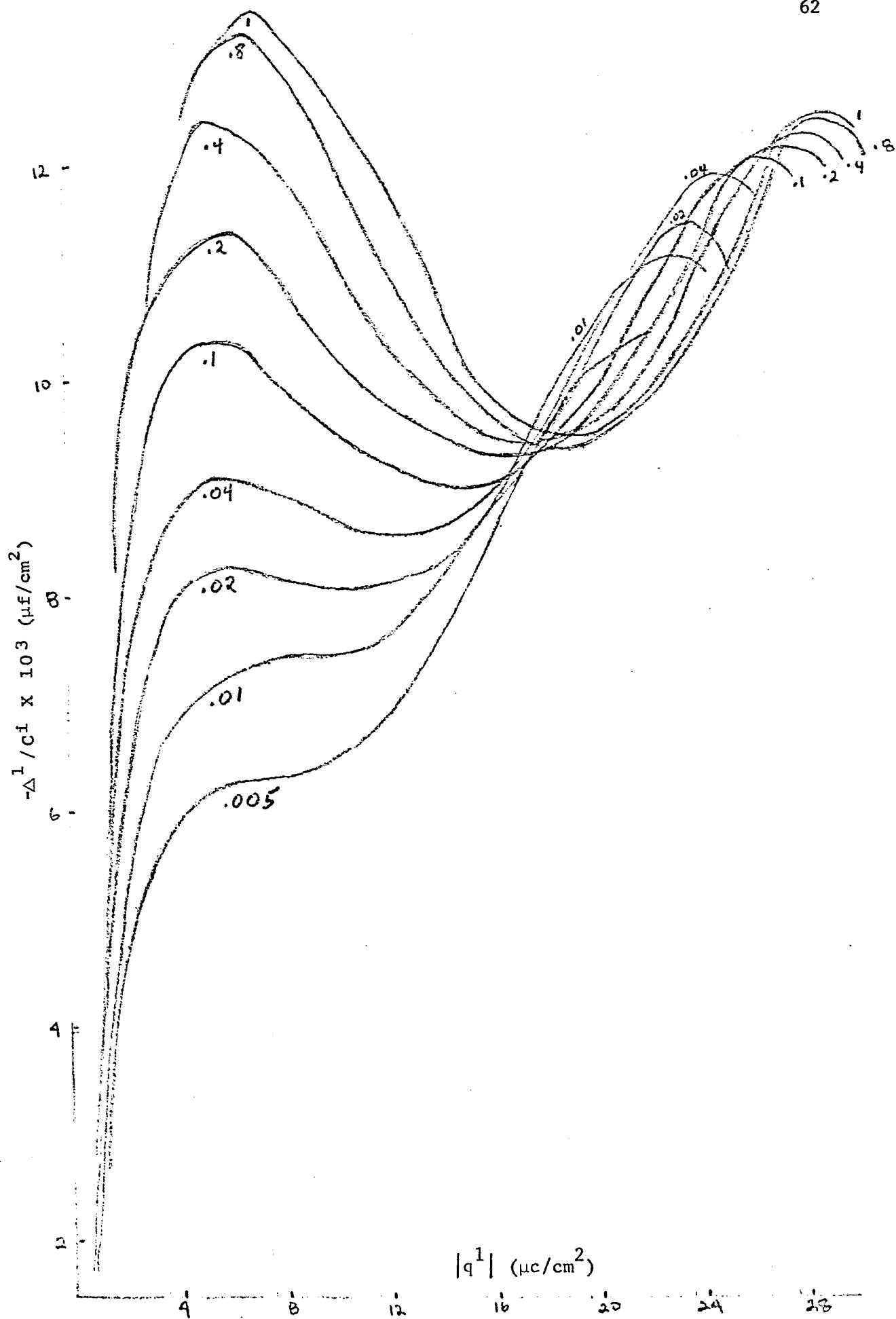


Figure 16.  $-\Delta 1/C^i \times 10^3$  Plotted Against the Amount Specifically Adsorbed at Constant Concentration for  $xMgBr + (1-x)MgCl_2$

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at  $-4 < q < 0$ . This is no doubt due to increased adsorption. The increase for  $q > 6$  or  $|q^1| > 18$  is not found in KCl + KF. As discussed previously, the existence of two peaks is indicative of a quadratic standard free energy of adsorption. For a purely quadratic  $\ln\beta$ ,  $-\Delta \frac{1}{C}$  must change sign which is not the case either here or with KCl + KF. Our equation for  $\ln\beta$  would result in two peaks and a minimum all at positive values of  $-\Delta \frac{1}{C}$ , but there really is very little justification in pushing the analysis any further.

#### Conclusion

The adsorption of KBr from KBr + KF has been shown to be similar to KCl from KCl + KF if the data in the same range of specifically adsorbed charge are compared. The results at large values of  $q^1$  have not previously been observed for halide systems. They can be explained by assuming a standard free energy with both a linear and quadratic terms and variable isotherm parameters. This obviously leaves much to be desired, but nothing further can be done with the present state of the theory. The bromide and chloride results strongly imply that the simpler picture for the iodide ion is due to the limited range of surface charge which was studied.

#### IV. THE ADSORPTION OF 6-AMINO-HEXANOIC ACID

##### Introduction

The adsorption of neutral molecules with permanent dipole moments have previously been studied. The most complete investigations have been for thiourea in aqueous solution,<sup>15,28</sup> and in formamide.<sup>29</sup> The sulfur in thiourea is strongly bound to the mercury surface at all but large negative surface charges. This gives the adsorption many of the characteristics of anion adsorption. The purpose of this experiment was to study the adsorption of a permanent dipole formed by two full charges which does not have a strong chemical interaction with mercury. Three amino acids: glycine, 4-amino-butyric acid, and 6-amino-hexanoic were chosen. All are zwitterions in neutral solutions. Preliminary work indicated that glycine and 4-amino-butyric acid are virtually unadsorbed. The electrocapillary curve for .3M glycine in 1MKF and the value of Ez(-.479v) indicated that adsorption was minimal. The differential capacity curve for 4-amino butyric acid (.15M4AB + .5MKF) also indicated very slight adsorption. For this reason the only system studied in detail was 6-amino-hexanoic acid.

##### Experimental

Eight solutions of  $xM6AH + .5MKF$  were investigated. The amino acid was purified by dissolving it in water and precipitating it with alcohol three times. The first precipitate to appear and that remaining after total precipitation were discarded. The differential capacity, the streaming electrode potential, and the surface tension at Ez were measured for each solution. This data is recorded in Table II of the appendix.

### Results

The differential capacity curves for xM6AH + .5MKF are presented in Figure 17. The inner layer capacity for .5MKF is shown in Figure 18. A comparison of Figures 2 and 18 or of Table III and IV confirms the lack of specific adsorption in KF solutions. The maximum difference in  $C^i$  is less than  $.3\mu\text{f}/\text{cm}^2$ . This is also the maximum difference between our values and Payne's and is probably due to using different capillaries. Programs I and II were used as discussed in the Appendix except that Program II was changed to a quadratic fit of  $\xi$  to  $\ln x$ , and values of  $\Gamma$  are not as reliable as the value of  $q^1$  in the previous system. This is due to the smaller total variation of  $\xi$  with  $\ln x$  at constant  $q$ . Our original assumption was that this system would show two regions of maximum adsorption. One would correspond to the positive end of the dipole being adsorbed at negative surface charges and the other to the negative end being adsorbed at positive surface charges. This did not turn out to be the case; rather the maximum adsorption at each concentration occurred at  $q = -6$ . Figure 19 shows the constant charge isotherm for several concentrations. The data do not fit a virial isotherm and the surface pressure values are too low to attempt to fit a Frumkin isotherm. The .01M values are not used in any of the figures, since Program II gave negative values of  $\Gamma$  for some values of  $q$ . This is due to  $\xi$  being almost constant at low concentration.

Further analysis of the data is in line with maximum adsorption occurring at  $q = -6$  and with a quadratic free energy of adsorption. We will begin with the equation for  $-\Delta 1/C$ .

$$-\Delta \frac{1}{C} = -kT[\Gamma b - b^2 \delta^2 \left( \frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu}]$$

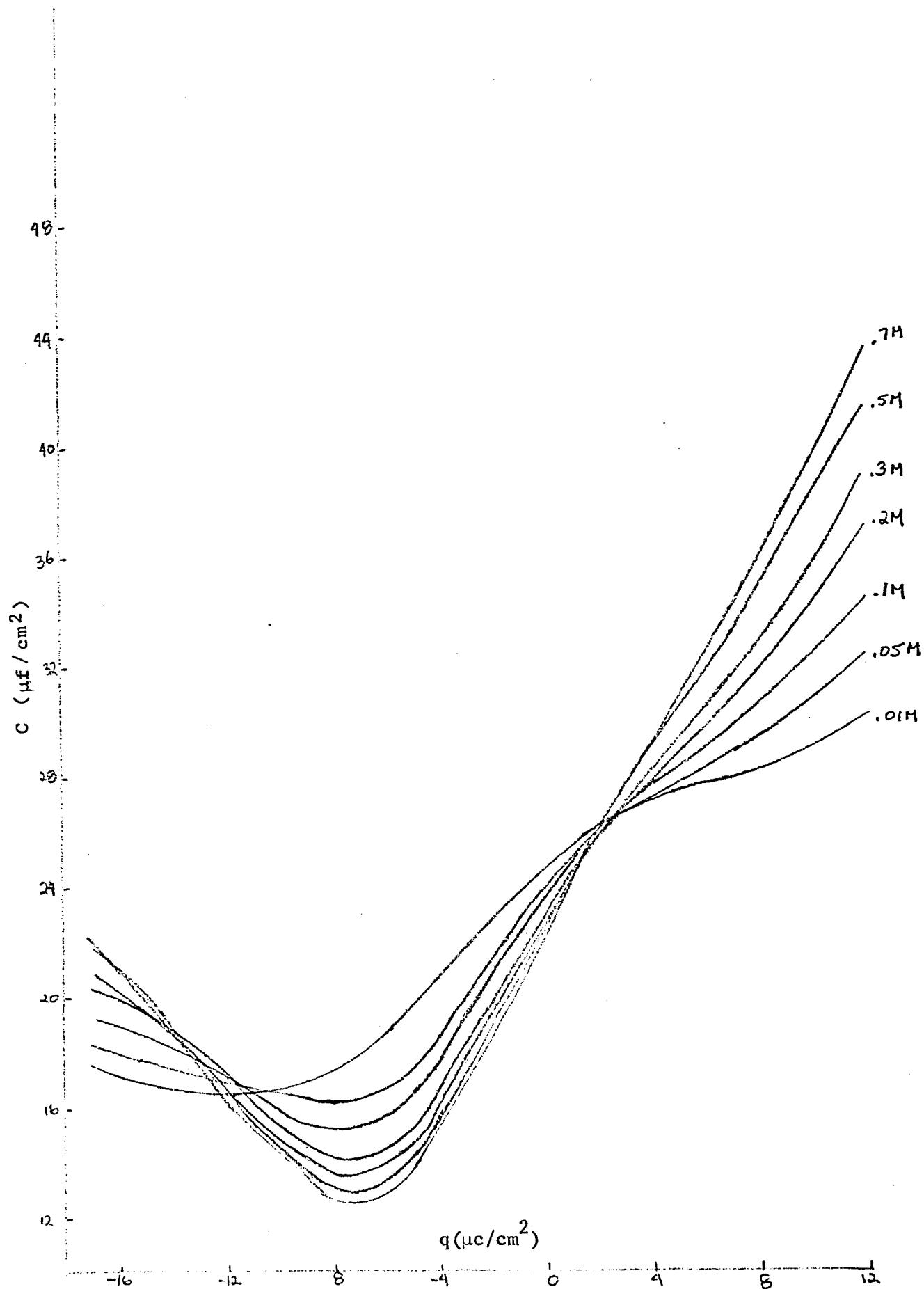


Figure 17. The Differential Capacity of  $x$  M 6-amino Hexanoic + .5MKF Acid Plotted as a Function of the Surface Charge Density

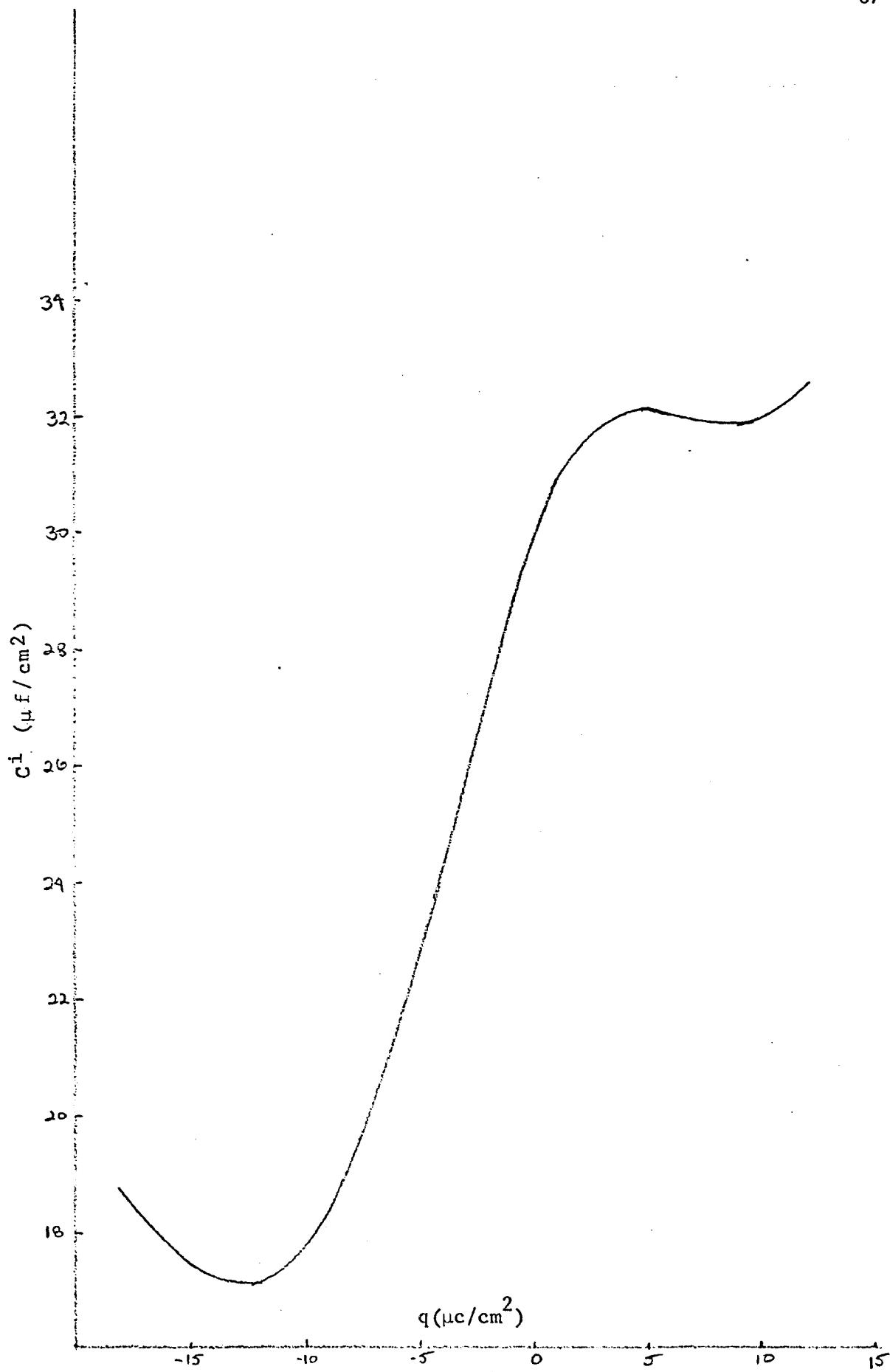


Figure 18. The Inner Layer Capacity of .5MKF Plotted as a Function of The Surface Charge Density

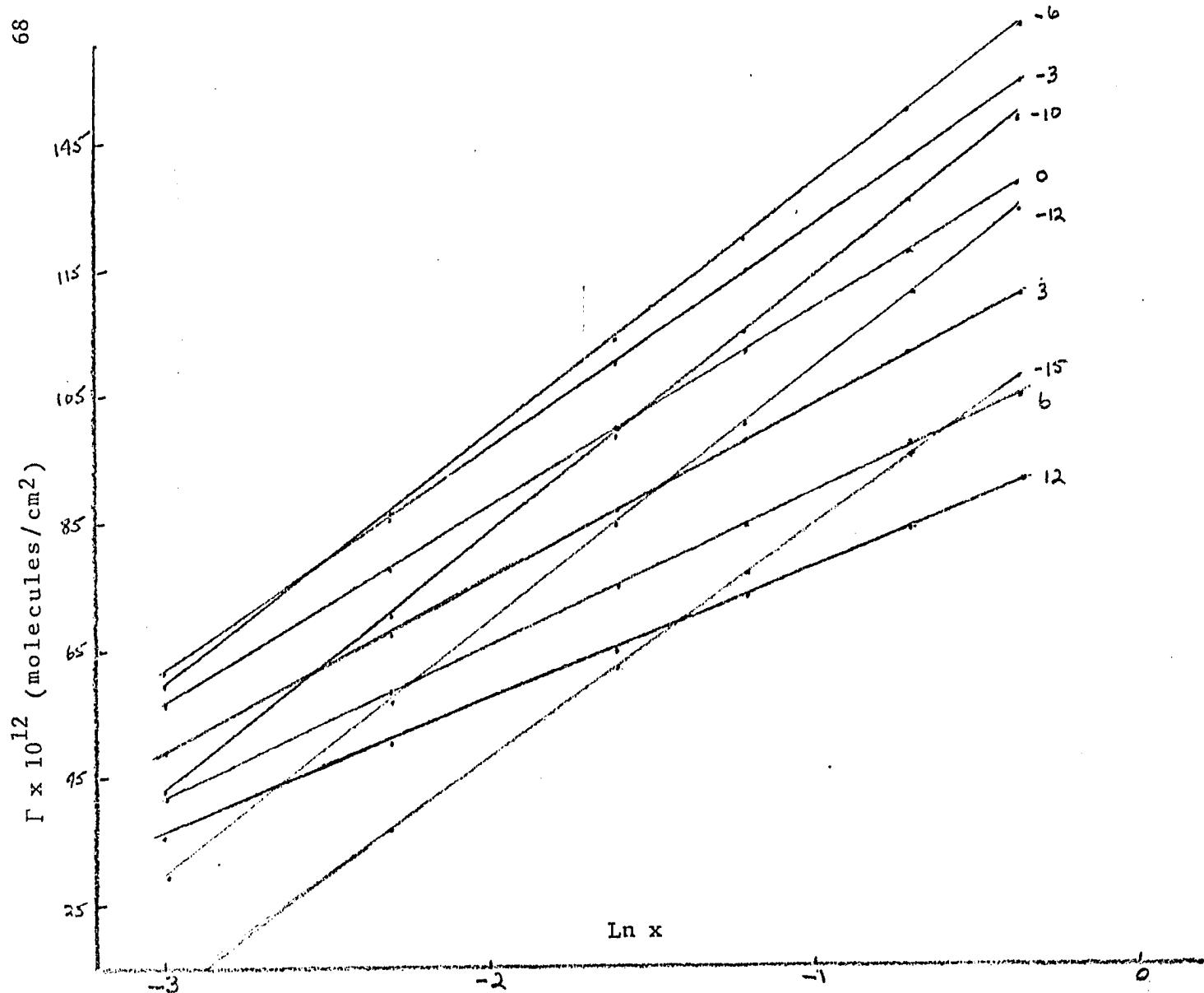


Figure 19. The Amount of xM6-Amino Hexanoic Acid ( $\Gamma \times 10^{12}$ ) Plotted as a Function of  $\ln x$  at Constant Surface Charge

assuming

$$\ln \beta = \ln \beta_{\max} - \frac{b}{2} \delta^2$$

$$\delta = q - q_{\max}$$

In Figure 20,  $-\Delta 1/C$  is plotted against  $q$  for four different concentrations. In this system there is no ambiguity concerning  $C$  since  $C^d$  is the same in the base solution as in the mixed solution at constant  $q$ .  $\Delta \frac{1}{C}$  therefore equals  $\Delta 1/C^i$ . As the equation for  $\Delta 1/C$  predicts, the minimum occurs at  $q = -6$ ,  $\delta = 0$  and becomes more negative with increasing  $\Gamma$ . In the range of charge available, desorption is not complete so that the curves do not return to  $\Delta \frac{1}{C} = 0$  but are still part of the desorption peaks. Figure 21 is a plot of  $-\Delta 1/C$  versus  $\Gamma$  at constant  $q$ . As expected, the curve at  $q = -6$  has the minimum slope which will equal  $-kT_b$ . The quadratic form of  $\ln \beta$  is again supported by the plots of  $\phi^{m-2}$  versus  $\Gamma$  in Figure 22. We begin by recognizing that for the adsorption of a neutral compound<sup>30</sup>

$$\phi^{m-2} = E - E^b \quad q = \text{const}$$

since

$$E = \phi^{m-2} + \phi^2 - \phi^{\text{ref}}$$

$$E^b = \phi_b^{m-2} + \phi_b^2 - \phi_b^{\text{ref}}$$

and

$$\phi^2 = \phi_b^2$$

$$E - E^b = \phi^{m-2} - \phi_b^{m-2} \quad q = \text{constant}$$

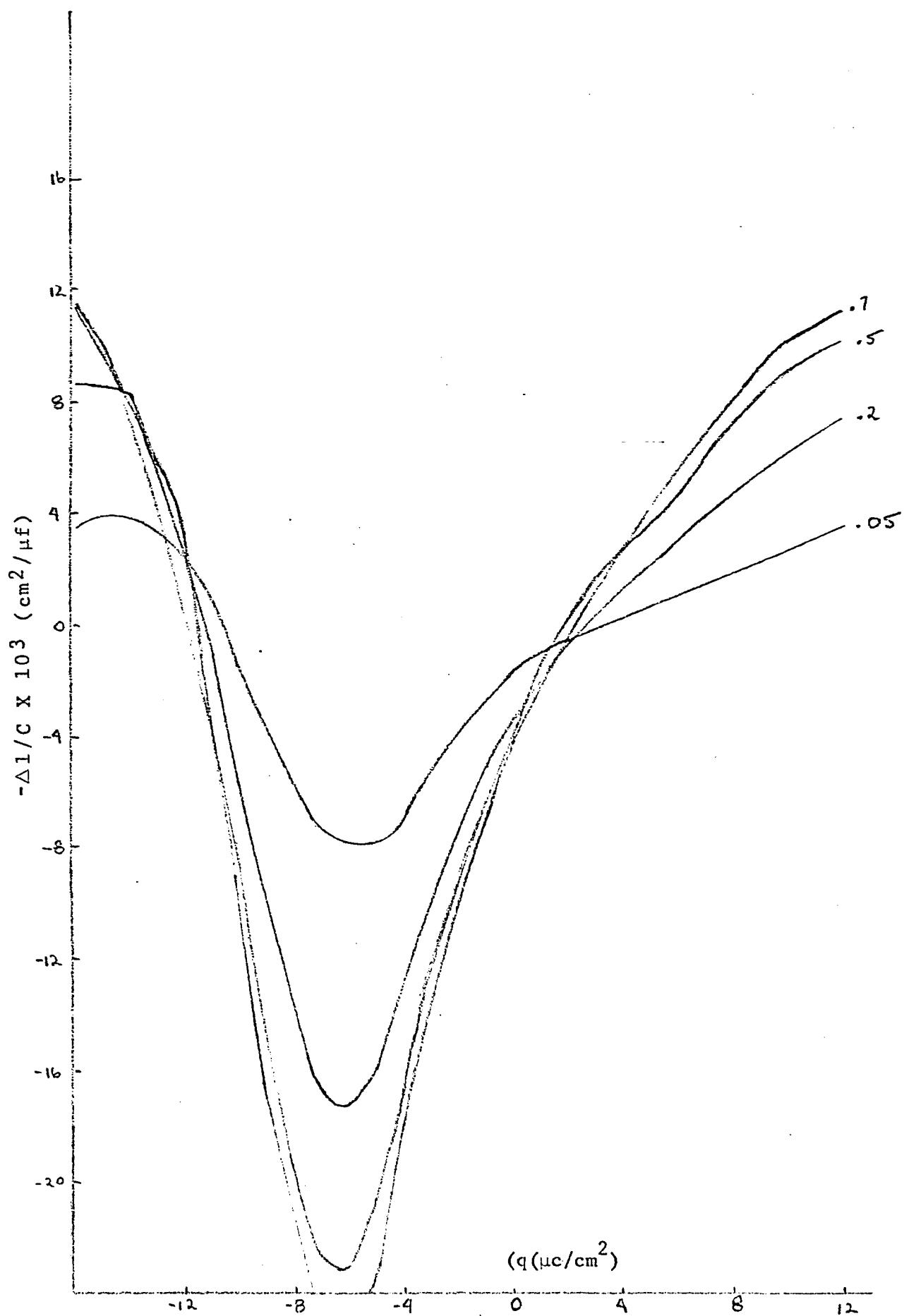


Figure 20.  $-\Delta 1/C \times 10^3$  Plotted as a Function of The Surface Charge at Constant Concentration for  $xM$  6-amino Acid + .5MKF

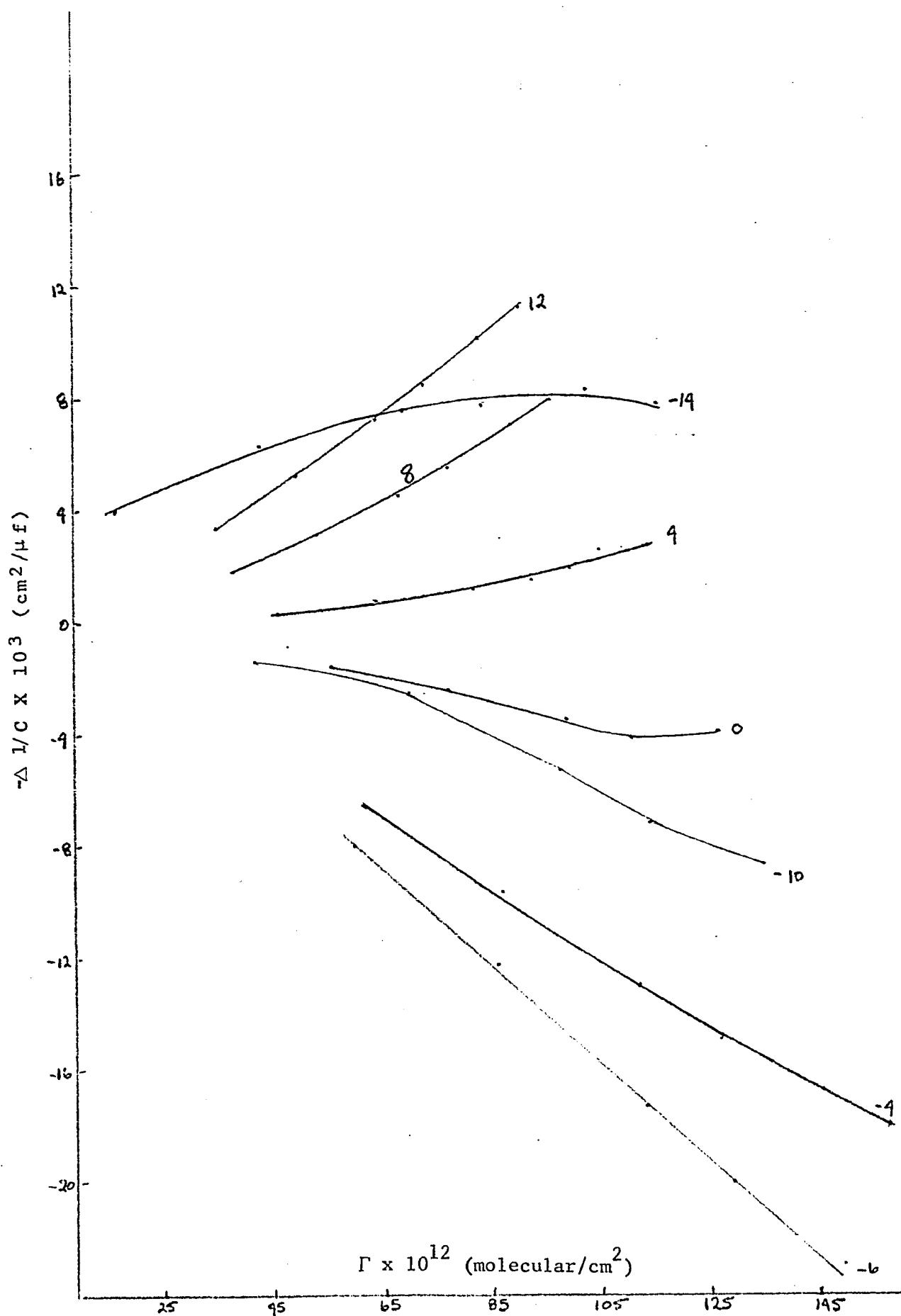


Figure 21.  $-\Delta 1/C \times 10^3$  Plotted as a Function of The Amount Adsorbed at Constant Surface Charge for  $xM$  6-amino Hexanoic Acid + .5MFe

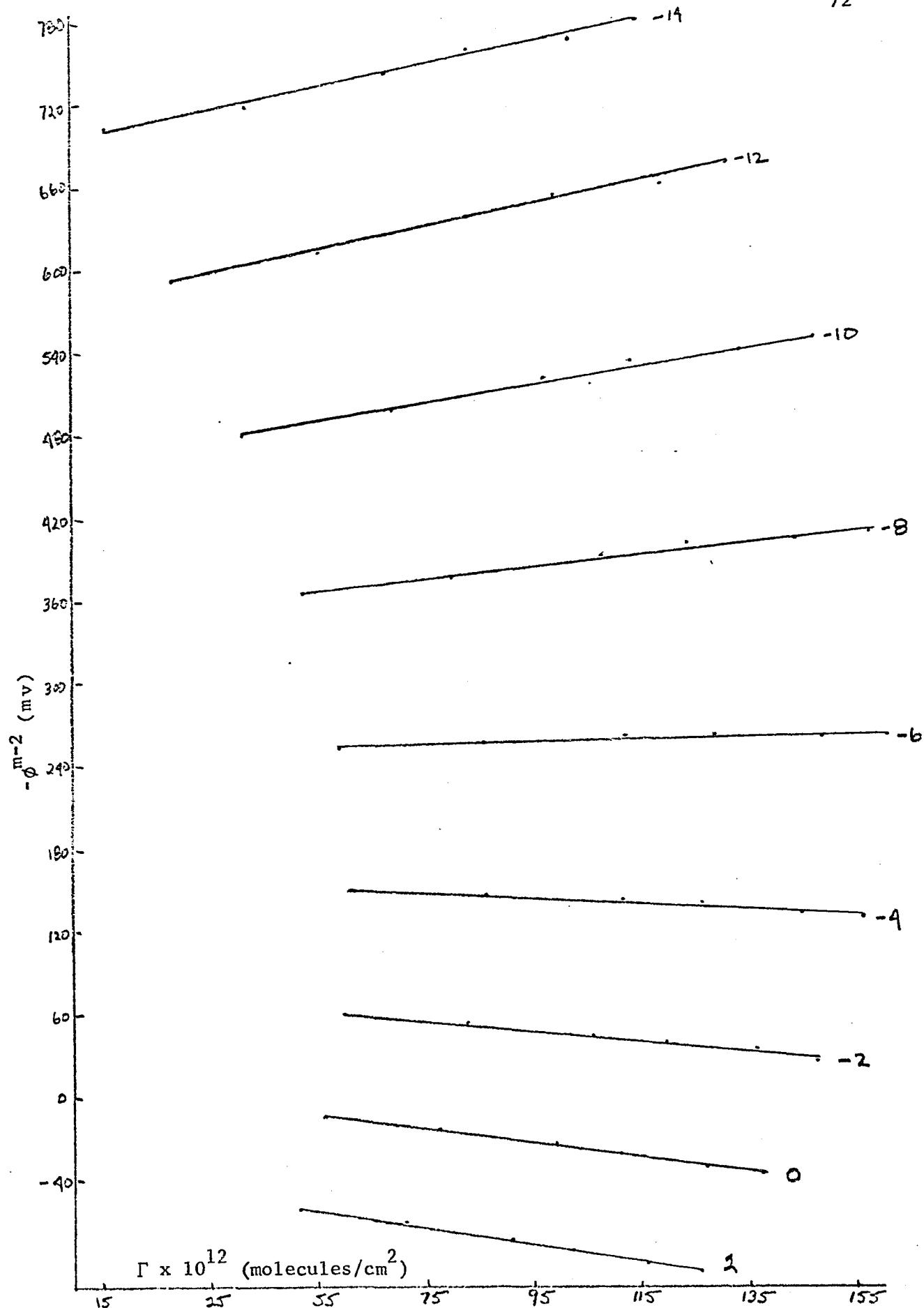


Figure 22. The Potential Across the Inner Layer ( $-\phi_m^{-2}$ ) Plotted as a Function of the Amount Adsorbed ( $\Gamma$ ) at Constant Surface Charge

Parsons neglects  $\phi_b^{m-2}$  which will change with  $q$ . This is justifiable if  $\phi^{m-2}$  can be separated into two terms.

$$\phi^{m-2} = \phi_T^{m-2} + \phi_b^{m-2}$$

$\phi_T^{m-2}$  is that part of  $\phi^{m-2}$  due to adsorption. We have previously shown that

$$\Delta E = E - E^b = -kT\Gamma \frac{\partial \ln \beta}{\partial q}$$

therefore

$$\phi^{m-2} = -kT\Gamma \frac{\partial \ln \beta}{\partial q}$$

$$\left( \frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = -kT \frac{\partial \ln \beta}{\partial q}$$

In Figure 22,  $\left( \frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = 0$  at  $q = -6$ .

Assuming

$$\delta = q + 6$$

$$\left( \frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = kTb(\delta)$$

This model is correct except at large positive values of  $q$  where either  $b$  is getting smaller or one of the other assumptions is no longer tenable. Actually if  $b$  is not constant, we do not have congruent isotherms and the analysis is no longer rigorous.

### Conclusion

Within the range of surface charge available, 6-amino-hexanoic acid is maximally adsorbed at  $q = -6$  with a quadratic standard free

energy of adsorption. A quadratic standard free energy of adsorption is to be expected for a point dipole. In this case, the distance between the amino and carboxyl groups is much larger than the inner layer which is only  $3\text{-}5 \text{ \AA}$ . It was therefore expected that the system would demonstrate the characteristics of ionic adsorption. It was our expectation that adsorption would be maximal at large absolute values of the surface charge density and that the molecule would reorient itself in the vicinity of the point of zero charge. The quadratic charge dependence implies that adsorption should be considered to occur in the entire double layer rather than be restricted to the inner layer for only then does the point dipole model make sense. The entire double layer for a .5MKF solution has a thickness of  $40\text{-}50 \text{ \AA}$ . In line with the quadratic charge dependence, one must assume that water is preferentially adsorbed as  $|q + 6|$  becomes large.

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VI. APPENDIX

Table I and Table II consist of the experimental data for the KF + KBr and .5MKF + 6-amino-hexanoic acid system respectively. The procedure for handling both sets of data is identical in all but two respects. All of the diffuse layer cards must be changed since  $q^1 = 0$  in the 6-amino hexanoic system and the total ionic concentration is .5M. Care must also be taken not to exceed the maximum permissible exponent in programs where powers of  $\Gamma$  appear. These differences are trivial and the programs and data will be discussed only for the KBr + KF system.

The purpose of Program I is to integrate the experimental capacity versus potential curve. The input for this program consists of Table I. The first and second cards are the title. The second card was always blank since the title was short. The third card gives the initial values of  $q$ ,  $\gamma$ ,  $E$ ,  $C$ , and the concentration, and indicates the direction of integration and whether specific adsorption is assumed. Provision is made to correct  $E$  values to  $E^+$  if necessary. For 1MKF, this card consists of experimentally determined values. For all of the  $x$ MKBr + (1-X)MKF sets, this card consists of the  $q = -19$  values for 1MKF. The following cards in each set consist of the experimentally determined potential and capacity values arranged according to the direction of integration. The program is capable of interpolating the value of  $C$  at  $q = 0$ , but this was not used, rather  $C$  was found directly. The program fits the first three points to a parabola and finds all integral values of  $q$  which lie between the endpoints. It then drops the first point, reads another point and repeats the process using the previously computed values of the second point as the integration constants. This

procedure is repeated until all of the points have been read. The output consists of  $E$ ,  $C$ ,  $\gamma$ ,  $\xi$  at integral values of  $q$ . If no specific adsorption is present,  $C^d$ , and  $C^i$  and  $\phi^{m-2}$  are also determined. Specific adsorption is assumed absent for KF. This program is a modified version of one originally developed by Payne. Tables III and IV are the output for 1MKF and .5MKF respectively.

Table V consists of the output cards of the first program for  $q = +4$ . The second card is the 1MKF card and the next nine are the KBr + KF cards. With the control card, this forms the input for Program II. The second program fits  $\xi$  to a cubic equation  $iskTN/F \ln x$ , the derivative of which is  $q^1$ . It also calculates  $\Phi$ ,  $C^d$ ,  $-\Delta 1/C$ ,  $\Delta E$ ,  $\phi^2$ ,  $\phi^{m-2}$ . Table VI contains the printed output of Program II for  $q = +4$ .

Program III obtains  $q^1 C^i$  from a quadratic fit of  $\phi^{m-2}$  to  $q^1$ . Program IV obtains  $(\frac{dq}{dq})_u^1$  from a cubic fit of  $q^1$  to  $q$ . The input cards for both programs are the output cards of Program II. In the first case they are arranged at constant charge and in the second at constant concentration. Program V evaluates  $C^i$ ,  $q^1 C^i$  and  $-\Delta 1/C^i$  using the output of Programs II, III, and IV. It can be easily modified to use the constant values of  $q^1 C^i$  obtained from Figure 9. The input cards for Program V are shown in Table VII. The first nine cards are the output of Program III. The next card is the 1MKF output card from Program I. The next nine cards are the output of Program IV, and the last nine are the output of Program II. All cards are for  $q = +4$ . Table VIII consists of the printed output of Program V.

Programs VI, VII, and VIII are used to determine whether the data will fit a Frumkin isotherm. Program VI iterates  $A$  and  $\theta$  to give universal plots of  $\ln \Phi/kT\Gamma_S$  versus  $\ln a\beta/\Gamma_S$ . Programs VII and VIII

iterate A and  $\Gamma_S$  and use experimental values of  $\Gamma$  and a to determine the best values of A and  $\Gamma_S$  once a rough fit of A is made. The input cards for Programs VII and VIII consist of the output cards of Program II at constant charge (J indicates the number of such sets). The fineness of the iteration can easily be varied. Program IX simply gives  $\Gamma$  and  $\ln a/\Gamma$  which are used to check for a virial isotherm. This would have been included in Program II except that there was not enough space left to print it out.

## PROGRAM I

## INTEGRATION OF THE CAPACITIY

```

C      INTEGRATION OF DOUBLE LAYER CAPACITY
C      L = 1 NO SPECIFIC ADSORPTION
C      K = 1 ANODIC INTEGRATION K = 2 CATHODUC
100 READ(5,20)
20 FORMAT (55H
          READ(5,21)
21 FORMAT(55H
          READ(5,30)K,CORR,Q1,G1,E1,C1,CON,L
30 FORMAT(I2,8X,6F10.0,12)
          WRITE(6,40)
40 FORMAT(37H1 INTEGRATION OF DOUBLE LAYER CAPACITY//)
          WRITE(6,20)
          WRITE(6,21)
          IF(L)404,404,402
402 WRITE(6,51)
51 FORMAT(1H ,4HE(V),5X,9HQ(MC/CM2),2X,10HG(ERG/CM2),2X,11HXI(ERG/CM2
1),2X,9HC(MF/CM2),4X,3HI/C,10X,2HCD,11X,2HCI,11X,4H)/CI/)
          GOTO403
404 WRITE(6,50)
50 FORMAT(1H,4HE(V),5X,9HQ(MC/CM2),2X,10HG(ERG/CM2),2X,11HXI(ERG/CM2
1),2X,9HC(MF/CM2),4X,3H1/C/)
403 IF(C1)22,22,24
22 READ(5,70)EP,CP
70 FORMAT(2F10.0)
          READ(5,70)E2,C2
          READ(5,70)E3,C3
          D2=E2-EP
          D3=E3-EP
          A2=C2-CP
          A3=C3-CP
          R=(A3/D3-A2/D2)/(D3-D2)
          S=(A2*D3/D2-D2*A3/D3)/(D3-D2)
          C1=R*(E1-EP)**2+(E1-EP)+CP
          GOTO23
24 READ(5,70)E2,C2
          READ(5,70)E3,C3
23 E=E1
          CE=C1
          QE=Q1
          GE=G1
          XN1=0.0
1 EC=E+CORR
          CR=1./CE
          XIE=GE+QE*EC*10.0
          KE=QE
          IF(L)65,65,400
400 F=11.72

```

```

PH12=2.*.02569*ALOG((QE/F)+SQRT((QE/F)**2+1.))
CD=228.5*COSH(19.46*PH12)
CI=(CE*CD)/(CD-CE)
B=1./CI
PHIM2=E+0.4750-PHI2
WRITE(6,61)E,KE,GE,XIE,CE,CR,CD,CI,B,PHIM2
61 FORMAT(1H0,F7.4,2X,13,8X,F7.2,5X,F7.2,6X,6(E11.4,2X))
WRITE(7,63)QE,XIE,EC,CE,CI
63 FORMAT(F5.1,F8.2,F7.4,2E11.4)
GOTO401
65 WRITE(6,60)E,KE,GE,XIE,CE,CR
60 FORMAT(1H0,F7.4,2X,13,8X,F7.2,5X,F7.2,6X,E11.4,2X,E11.4)
WRITE(7,62)QE,XIE,CON,EC,CE
62 FORMAT(F5.1,F8.2,2F7.4,E11.4)
401 IF(QE-Q1)11,2,11
2 IF(K-1)3,3,4
3 QE=QE+1.0
GOTO200
4 QE=QE-1.0
200 D2=E2-E1
D3=E3-E1
A2=C2-C1
A3=C3-C1
R=(A3/D3-A2/D2)/(D3-D2)
S=(A2*D3/D2-D2*A3/D3)/(D3-D2)
5 XN=XN1+1.0/C1
N=0
6 XN1=XN-(R*XN**3/3.+S*XN**2)/2.+C1*XN-(QE-Q1))/(R*XN**2+S*XN+C1)
Y=ABS(XN1-XN)
IF(Y.LT.0.00001)GOTO8
XN=XN1
N=N+1
GOTO(6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,7),N
7 WRITE(6,80)
25 READ(5,70)E4,C4
IF(E4-999.99)25,15,15
8 Z=ABS(XN1)
Z3=ABS(D3)
IF(Z-Z3)9,10,10
9 E=XN1+E1
CE=R*XN1**2+S*XN1+C1
GE=-10.* (R*XN1**4/12.+S*XN1**3/6.+C1*XN1**2/2.+Q1*XN1)+G1
GOTO1
10 READ(5,70)E4,C4
G1=-10.* (R*D2**4/12.+S*D2**3/6.+C1*D2**2/2.+Q1*D2)+G1
Q1=R*(E2-E1)**3/3.+S*(E2-E1)**2/2.+C1*(E2-E1)+Q1
IF(E4-999.99)300,15,15
300 E1=E2
E2=E3
E3=E4
C1=C2
C2=C3
C3=C4

```

```
GOTO200
11 IF(K-1)12,12,13
12 QE=QE+1.
    GOTO14
13 QE=QE-1.
14 GOTO5
15 GOTO100
80 FORMAT(32H NO SOLUTION AFTER 20 ITERATIONS)
END
```

Program II - Determination of  $q^1$ 

```

----- SPUFF VERSION 3/1/68 -----
C  CURVE FIT FCP XI = A+BX+CX2+DX3
C  QE XIE CE CI BASE SOLUTION VALUES
C  DIMENSION D(4,4),V(6),Y(15),C(15),X(15),E(15),D(15),SP(1)      56437
151,A(15),ACON(15),CS(15)                                         56437
201,READ(5,10)IN,Q,EZ
1C9,FORMAT(13,F5.1,F7.4)
READ(5,402)JOE,X16,EC,CE,C1
402,FORMAT(5.1,F9.2,F7.4,2E1.4)
150,D12001,N
200,READ(5,110)Y(11),CON(11),E(11),CS(11)
110,FORMAT(5X,F6.2,F7.4,E11.4)
D(8)=1,N
8  X(1)=.2569*ALOG(CN(1))                                         56542
A(1)=1
J=1
SX=0.0
SX2=0.0
SX3=0.0
SX4=0.0
SX5=0.0
SX6=0.0
SY=0.0
SXY=0.0
SX2Y=0.0
SX3Y=0.0
D(1,30)L=1,N
SX=SX+X(L)
SX2=SX2+X(L)*X(L)
SX3=SX3+X(L)*X(L)*X(L)
SX4=SX4+X(L)*X(L)*X(L)*X(L)
SX5=SX5+X(L)*X(L)*X(L)*X(L)*X(L)
SX6=SX6+X(L)*X(L)*X(L)*X(L)*X(L)*X(L)
SY=SY+Y(L)
SXY=SXY+X(L)*Y(L)
SX2Y=SX2Y+(X(L)**2)*(Y(L))
30 SX3Y=SX3Y+(X(L)**3)*(Y(L))
D(1,1)=AN
D(2,1)=SX
D(3,1)=SX2
D(4,1)=SX3
D(1,2)=SX
D(2,2)=SX2
D(3,2)=SX3
D(4,2)=SX4
D(1,3)=SX
D(2,3)=SX3
D(3,3)=SX5
D(4,3)=SX5
D(1,4)=SX3
D(2,4)=SX4
D(3,4)=SX5
D(4,4)=SX6
----- 35,67,T0=(2*4*4*46748,50),T,J
42 V(L,J)=(L*(L,1)*(L,2,2)*D(3,3)*D(4,4)+D(2,3)*D(3,4)*D(4,2)+      57003
15*(2,2)*D(3,2)*D(4,3)-D(2,3)*D(3,2)*D(4,4)-D(4,2)*D(3,3)*D(2,4)+      57007
2-(D(2,2)*D(3,4)*D(4,3))-((D(1,2)*D(2,1)*D(3,3)*D(4,4)+      57042
3*D(1,2)*D(3,2)*D(4,1))+D(2,4)*D(3,1)*D(4,3))-D(2,3)*D(3,1)*D(4,4))      57063
----- 57111

```

```


$$\begin{aligned}
& 4 \cdot D(2,4) \cdot D(3,2) \cdot D(4,1) - D(2,1) \cdot D(3,4) \cdot D(1,3) \cdot D(2,1) \\
& 6 \cdot D(2,2) \cdot D(4,4) \cdot D(4,1) + D(2,2) \cdot D(3,4) \cdot D(4,1) \\
& 6 \cdot D(2,2) \cdot D(4,1) + D(2,4) \cdot D(4,1) - D(2,4) \cdot D(3,2) \cdot D(4,1) \\
& 7H = ((D(1,2) \cdot (D(2,1) \cdot D(3,2) \cdot D(4,3) + D(2,2) \cdot D(3,3) \cdot D(4,1)) \\
& 8 \cdot D(2,3) \cdot D(3,1) \cdot D(4,2) - D(2,2) \cdot D(3,1) \cdot D(4,3)) \\
& 9 \cdot D(2,5) \cdot D(3,3) \cdot D(4,2))) \\
J = J + 1
\end{aligned}$$


$$I F (J=6) 3575752$$

44 D(1,1) = SY
D(2,1) = SXV
D(3,1) = SXV
D(4,1) = SXV
G0 TO 42
46 D(1,2) = SV
D(2,2) = SXV
D(3,2) = SXV
D(4,2) = SXV
G0 TO 42
48 D(1,3) = SY
D(2,3) = SXV
D(3,3) = SX2Y
D(4,3) = SX3Y
D(1,2) = SX
D(2,2) = SX2
D(3,2) = SX3
D(4,2) = SX4
GC TO 42
50 D(1,4) = SY
D(2,4) = SXV
D(3,4) = SX2Y
D(4,4) = SX3Y
D(1,3) = SX2
D(2,3) = SX3
D(3,3) = SX5
D(4,3) = SX5
G0 TO 42
52 CONTINUE
A = V(2) / V(1)
B = V(3) / V(1)
C = V(4) / V(1)
P = V(5) / V(1)
WRITE(5,200)0
300 FORMAT(B,H1CHARGE=,F5.1)
WRITE(6,301)A,B,C,P
301 FORMAT(5H0X=((E11.4,4H)+(E11.4,4H))X+(E11.4,3H)X3)
WRITE(6,303)
303 FORMAT(1H0,3HCON,6X,5HLCN,4X,3HOSA,5X,2HSP,7X,3HLSP,6X,2HXI,7X,4
1HDIFF,5X,2HCD,11X,2HDC,11X,2HDE,7X,4HPHM=2)
IF(ECI<0,501,400
501 0J5021=1,N
DE(1)=0,0
DC(1)=0,0
SP(1)=0,0
AS(1)=0,0
SC2 CUNTINUE
GOT0500
57526
57527

```

```

4CO 004031=1,N
  DE(I) EC-EIT
    DC(I)=(1./CF)-11./CS(I))
    SP(I)=X(F-Y(I))
    IF(SP(I)<-.005)403,404
    404  ASPI=ALOG(SP(I))
    403  CONTINUE
    5CO -003021,I,0
      XC=A+B*X(I)+C*X(I)**2+P*X(I)**3
      QSA=B+C*X(I)+3.0*X(I)**2
      5750
      57541
      57547
      57552
      57557
      57562
      57566
      57600
      57615
      57616
      57621
      57661
      57706
      57710
      57741
      57750
      57756
      57771
      60006
      60055
      60074
      60074
      60142
      60143

      XC=A+B*X(I)+C*X(I)**2+P*X(I)**3
      QSA=B+C*X(I)+3.0*X(I)**2
      F=11.*I2
      PHI=2.0*02569*ACOG((1.0+QSA)/F)+SQR(((1.0+QSA)/F)*#2*I2)
      PHIE(I)=E(I)-EZ-PHI2
      DIFF=XIC-Y(I)
      CD=228.5*COSH(19.46*PHI2)
      AC(I)=ALOG(CD(I)))
      ARIY(I)=304(CUN(I)),QSA,SP(I),ASPI(I),Y(I),DIFF,CD,DC(I),DE(I)
      LIT,PHI2,PHIN,X(I)
      3C4  FORMAT(1H0,2(F7.4,2X),F6.2,2X,F7.2,2X,2(F7.2,2X),2(E11.4,2
      -1X),4(F7.4,2X))
      4RITE(7,406)CUN(I),QSA,SP(I),CD,DC(I),DE(I),CS(I),Q,PHIN
      4C6  FORMAT(7.4,F6.2,F7.2,E11.4,F7.4,E11.4,F5.1,E11.4)
      302  C JNITUE
      CNTN21
      END

```

卷之三

**Program III - Determination of  $\left(\frac{\partial q}{\partial \phi}\right)_{m-2}$**

```

112 261=5X2
20 261=6X2
52 CONTINUE
A = V(1,1)*M(1,1)
H = V(1,1)/M(1,1)
C = V(1,2)*M(1,1)
WRITE(6,0010)
200 FORMAT(1H1,2ME,5E,1)
WRITE(6,0) H,B,C
201 FORMAT(1H2,5ME,11,4,3H05A,114,511,4,6H05A,4,2)
WRITE(6,002)
502 L=1DO 51 M=6X2+1,6X2+5X2-1,6X2+5X2-2,6X2+5X2-1
51 M=M+1
D=L*2+1,M*2+1,51*2+1,51*2+2
DPI=PI*2.0*X*C*S(A(J))
CSP=PI*E*B*S(B(J))
WRITE(6,0010) L,M,DPI,CSP
204 FORMAT(1H1,2ME,5E,1)
WRITE(7,0) C,V(1,1)*M(1,1)
205 FORMAT(1H2,5ME,11,4,3H05A,114,511,4,6H05A,4,2)
503 CONTINUE
504 TO 201
END

```

## Program IV.—Determination of $\left(\frac{\partial \ln k}{\partial T}\right)_{P, \text{constant}}$ .

1

89

```

ED(2*3)*D(3,1)*D(3,1)*D(4,2)*D(4,2)*D(2,1)*D(2,1)*D(3,1)*D(3,1) = D(2,2)*D(3,1)*D(4,1)
J = J + 1
1F (J-6) 3655252
L4 D(1,1) = SY
D(2,1) = SX
D(3,1) = SY
D(4,1) = SX2Y
62 TC 42
L6 S(1,2) = SY
S(2,2) = SYV
D(2,2) = SY2Y
S(3,2) = SYAV
D(3,2) = AN
D(4,2) = SX
D(3,1) = SY2
D(4,1) = SX3
60 TO 42
L8 D(1,3) = SY
D(2,3) = SX
D(3,3) = SY2Y
D(4,3) = SYAV
D(1,2) = SY
D(2,2) = SX2
D(3,2) = SX2
D(4,2) = SX4
60 TO 42
50 D(1,4) = SY
D(2,4) = SYV
D(3,4) = SX2Y
D(4,4) = SYV
D(1,2,2) = SY2
D(2,2,2) = SY2
D(3,2,2) = SY3
D(4,2,2) = SY4
60 TO 42
52 CONTN,F
A = VLL(2) / VLL(1)
L = VLL(3) / VLL(1)
C = VLL(4) / VLL(1)
P=VL(5) / VL(1)
E11E12E13CUN
803 FORMAT(1H0,1H0,1H0,6X,1H0$AC*4X+5X*4HQ$AC)
804 FORMAT(1H0,1H0,1H0,6X,1H0$AC*4X+5X*4HQ$AC)
PCB012,N
$OSAC=A$C*(1)+C*$C*(1)**2+P*$C*(1)**3
$SSAC=B$C*(2,0)*(1$C*(1))**2,0*$P$C*(1))**2,
WHITE(1,806)$OSAC*5*(1),CON
B05 ECPMNL2,LAE2,LAE1,5
WHITE(1,807)$OSAC*11,CON
WHITE(1,807)$OSAC*11,CON
B07 FORMALDO,EGO,2X,3IE6,2,2X),
B05 CONTN,F
END

```

Program V - Determination of the Components of Capacity -

-EXCEDE-

## Program VI

```

      1 ID-----CHX201-2701-305,30LU,200 SEARS
      2 SPUFF
      3 C...FRIMKIN-ISOTERM
      4 READ(5,1)A,N
      5 DO6 J=1,N
      6 THETA=0.0
      7 IF(J>5.0)11 GOT012
      8 A=4+0.5*(J-1)
      9 WRITE(6,4)
     10 4 FORMAT(1H1,16HFRIJKIN ISOTHERM)
     11 WRITE(6,5)A
     12 5 FORMAT(1H0,2HAE,F5.1)
     13 WRITE(6,7)
     14 7 FORMAT(1H0,5SHFTA,2X,3HPHI,6X,4HAPHI,5X,1HB)
     15 DCA=1.2
     16 IF(J>4.5)5 GOT014
     17 IF(J>TA=0.0718*14,14
     18 5 GOT019*10,11),1
     19 6 THETA=0.01
     20 7 GOT012
     21 8 THETA=0.03
     22 9 GOT012
     23 10 THETA=0.07
     24 11 THETA=0.07
     25 12 GOT012
     26 13 D=1
     27 14 THETA=(D-3.0)*0.05
     28 15 PHI=1.0* ALOG(1.0-THETA)+(A/2.0)*(THETA**2)
     29 16 APHI=ALG(1PHI)
     30 17 B=ALCG(1(THETA)/1.0-THETA)+A*THETA
     31 18 WRITE(6,2)THETA,PHI,APHI,B
     32 19 2 FORMAT(1H0,F5.2,X,3(F7.2,2X))
     33 20 3 CONTINUE
     34 21 6 CONTINUE
     35 22 END
     36 23 SDATA

```

CARD COUNT 6037

## Program VII

```

      10  CHM201-2701,205,303,290, SEARS
      SPUFFT
      C,FROMKIN,LSCFTERM,
      DIMENSION,CON(10),SA(10),SP(10),Q(10),GAM(10),ASP(10)
      D012 J=1,2
      D014 i=1,5
      READ(5,1)CCN(I),QSAT(I),SP(I),011
      1 FORMAT(F7.4,F6.2,F7.2,F6.5,B.1)
      14 GAM(I),R4=1.0)*QSAT(I)*0.60232E+24/U.964935E+11
      D015 L=1,5
      PEL
      A=7.5+0.1*P
      D015 K=1,21
      R=<
      GAMS=0.1480E+15+0.0020E+15*R
      G=0.1
      WRITE(6,6)A*GAMS,F
      6 FCPVAT(1H1,2HA,F5.1,5HGAMS,E11.4,5X,2HQ=,F5.1)
      WRITE(6,7)
      7 FCPVAT(1H0,3HCON,6X,3HGAN,1LX,3HOSA,6X,2HSP,7X,4HDIFF,5X,5HSRC,6X,
      14 ASPC*5X,3HSP,6X,3HPER)
      D016 N=1,9
      META=GAM(R)/GAMS
      IF (UTFTA.GE.1.0)GOTO 9
      STOP
      9 PH1=0.0
      APHI=0.0
      ASP(M)=ALOG(SP(M))
      SOT010
      6 PR=-1.0*ALOG(1.0-THETA)+(A/2.0)*(THETA**2)
      PHI=0.133042E-15*298.12*GAMS*PR
      ASP(M)=ALOG(SP(M))
      APHI=ALOG(PHI)
      10 DIFFSP(M)-PHI
      PER=DIFF/SP(M)*1CO.0
      WRITE(6,2)CON(M),GAM(M),GSA(M),SP(M),DIFF,PHI,APHI,ASP(M),PER
      2 FORMAT(1H0,F7.4,2X,E11.4,2X,7(F7.2,2X))
      16 CONTINUE
      15 CONTINUE
      18 CONTINUE
      13 CONTINUE
      END
      SDATA
      CARD COUNT 0044

```

## Program VIII

```

$ID      CHM201-2/01,303,303+200 - SEARS
$PUFF    C-FRUNKIN ISOTHERM
DIMENSION CON(10),QSA(10),SP(10),Q(10),GAM(10),ASP(10)
DC13J=1,1
DO14J=1,9
READ 5,1ICON(1),QSA(1),SP(1),Q(1)
1 FORMAT(F7.4,F6.2,F7.2,40X,F5.1)
14 GAM(1)=1.0*QSA(1)*0.60232E+24/0.964935E+11
DO18L=1,15
PL
A=4.0+0.2*P
DO15K=1,16
R=X
GAMS=0.1600E+15+0.0U20E+15*R
F=C(1)
WRITE 6,1A,GAMS,F
6 FORMAT(1H1,2H=A,F2.1,2H=GAMS,F11.4,5X,2H0=,F5.1)
WRITE (6,7)
7 FORMAT(1H0,3HCON,6X,3HGAM,10X,3HOSA,6X,5HSHAETA)
DO16N=1,9
THETA=GAM(N)/GAMS
IF (THETA.GE.1.0)GOTO9
GOTO8
9 ABETA=0.0
GOTO10
8 ABETA=-1.0*ALOG(CON(M))+ALOG(GAMS)+ALOG(THETA/(1.0-THETA))+A*THETA
10 ARITE(6,2)CON(M)*GAM(M)*QSA(M)*ABETA
12 FORMAT(1H0,F7.4,2X,E11.4,2X,F7.2,2X,E11.4)
16 CONTINUE
15 CONTINUE
18 CONTINUE
13 CONTINUE
END
EDATA

```

CARD COUNT 0036

## Program IX

```

$PUFF VERSIN 3/1/68
C      VIRTUAL ISOTH=PM
12 WRITE(6,1)
1  FORMAT(1H1,15HVIPIAL TSO/TERM)
APITE(6,2)
2 FORMAT(1HO,3HCN,6X,3HOSA,5X,3+SAM,10X,1HQ,5X,12HLCN)7(GAM)
DC11=1,9
3 FADDS,A)CON,QSA,Q
SAM=(-1.0*QSA)*10.6023E+24/(0.9549E+11)
IF(GAM)4,4,6
4 SOTO9
5 F=ALOC((CN)-ALOC((GAM))
6 APITE(6,1)CN=A$A,GAM,Q,F
10 F02MAT(1HO,F7.4,2,X,F6.2,?X,F11.4,2X,F5.1,2X,F8.3)
11 CONTINUE
SOTO12
END

```

\*\*\* EXECUTION

**Table I: Experimental Data for xMKBr + (1- $\nu$ )MKP Arranged As Used For Input of Program I.**

1	1NKF 25 DEG	-0.4750	26.36	1.0	1
-0.4119	27.01				
-0.4119	27.61				
-0.3855	28.01				
-0.3516	28.35				
-0.3214	28.58				
-0.2905	28.69				
-0.2606	28.76				
-0.2307	28.77				
-0.2007	28.81				
-0.1703	28.80				
-0.1404	28.90				
-0.1106	29.04				
-0.0808	29.48				
-0.0524	30.44				
+0.0247	32.33				
+0.0009	33.96				
995.99	1NKF 25 DEG				
2	1NKF 25 DEG	-0.4750	26.38	1.0	1
-0.5225	25.77				
-0.5226	24.41				
-0.6034	23.04				
-0.5533	21.60				
-0.7041	20.47				
-0.7514	19.42				
-0.8012	18.55				
-0.8487	17.83				
-0.8777	17.24				
-0.9491	16.80				
-1.0014	16.52				
-1.0514	16.47				
-1.1022	16.30				
-1.1504	15.94				
-1.2015	16.46				
-1.2517	16.88				
-1.3007	16.89				
-1.3511	17.18				
-1.4021	17.53				
-1.4525	17.94				
-1.4971	18.35				
995.99	1NKF 25 DEG				
1	1NKF 25 DEG	-19.0	-103.053	-1.4514	10.23
-1.4546	1b.04				
-1.4067	17.59				
-1.3542	17.25				
-1.3045	16.95				
-1.2540	16.70				
-1.2042	16.50				
-1.1549	16.30				
-1.1041	16.25				
-1.0545	16.20				
-1.0023	16.54				
-0.9527	16.81				
-0.9240	17.23				

-0.8537 17.79  
 -0.8040 18.53  
 -0.7535 19.46  
 -0.7040 20.61  
 -0.6539 21.04  
 -0.5042 23.52  
 -0.5526 25.45  
 -0.530 27.2  
 -0.6724 29.08  
 -0.425 29.67  
 -0.4127 32.18  
 -0.3821 33.61  
 -0.3524 34.69  
 -0.3225 35.45  
 -0.2720 45.20  
 -0.2227 37.37  
 -0.1727 40.41  
 -0.1230 47.61  
 -0.0732 64.80  
 -0.0696 99.63  
 969.99  
 .005M KBR 25 DEG  
 1 19.0 -103.053 -14914 -10.293 .005  
 -1.4515 17.97  
 -1.4021 17.55  
 -1.3518 17.20  
 -1.3024 16.91  
 -1.2520 16.66  
 -1.2023 16.46  
 -1.1520 16.34  
 -1.1023 16.30  
 -1.0519 16.35  
 -1.0023 16.52  
 -0.9518 16.80  
 -0.9023 17.23  
 -0.8521 17.63  
 -0.8029 16.65  
 -0.7526 19.68  
 -0.7030 21.04  
 -0.6527 22.86  
 -0.6031 25.31  
 -0.5526 28.64  
 -0.5228 31.12  
 -0.4522 33.91  
 -0.4127 44.12  
 -0.4329 39.13  
 -0.4030 41.09  
 -0.3719 42.39  
 -0.3422 43.28  
 -0.4625 36.69  
 -0.2625 45.43  
 -0.2326 50.12  
 -0.1817 61.35  
 -0.1324 487.07  
 -0.0836 179.00  
 969.99  
 .01 M KBR IKDEG

<b>.024 KBR - 25 DEG.</b>	
-1.4520	17.97
-1.4018	17.50
-1.3511	17.22
-1.3011	16.92
-1.2503	16.68
-1.2003	16.48
-1.1507	16.37
-1.1006	16.31
-1.0502	16.38
-1.0046	16.55
-0.9506	16.85
-0.9005	+17.31
-0.8496	17.96
-0.8016	18.82
-0.7513	20.02
-0.7013	21.67
-0.6507	24.06
-0.6009	27.47
-0.5509	32.04
-0.5150	35.96
-0.4840	39.15
-0.4539	41.93
-0.4239	43.90
-0.3837	45.34
-0.3440	46.55
-0.2835	49.44
-0.2338	57.08
-0.1824	74.39
-0.1341	118.40
9.99	99
<b>.024 KBR - 25 DEG.</b>	
<b>.02 -19.0. +18.293</b>	
-1.4538	16.06
-1.4041	17.65
-1.3537	17.29
-1.3041	16.98
-1.2537	16.73
-1.2039	16.53
-1.1535	16.37
-1.1039	16.14
-1.0534	16.39
-1.0035	16.57
-0.9529	16.86
-0.9030	17.38
-0.8513	18.12
-0.8012	19.13
-0.7506	20.62
-0.7006	22.64
-0.6501	25.14
-0.6022	30.68
-0.5517	36.59
-0.5251	35.92
-0.5019	42.25
-0.4504	45.91
-0.4006	47.12
-0.3501	46.00
-0.3024	51.09

•04M KBR 25 DEG		-19.0	-103.053	-1.4914	1b.293	.04
1	1.4501	18.01				
	-1.4018	17.61				
	1.2512	17.24				
	-1.3013	16.96				
	1.2507	16.70				
	-1.2019	16.53				
	1.1515	16.40				
	-1.1018	16.37				
	1.0513	16.43				
	-1.0019	16.64				
	0.9513	17.00				
	-0.9015	17.56				
	0.8512	16.41				
	-0.8014	19.70				
	0.7509	21.64				
	-0.7013	24.67				
	0.6512	29.14				
	-0.6016	32.08				
	0.5793	37.62				
	-0.5513	41.40				
	0.5209	43.70				
	-0.5018	46.02				
	0.4758	47.14				
	-0.4515	46.03				
	0.4303	46.23				
	-0.4020	46.42				
	0.3802	46.04				
	-0.3524	49.76				
	0.3031	52.04				
	-0.2732	67.27				
	0.2043	93.04				
	99.79					
0.1	1.4501	-2.5 - 26.6				
	-1.4018	-19.0				
	1.2512	-1.4914				
	-1.3013	-103.053				
	1.2507	-1.4914				
	-1.2019	-103.053				
	1.1515	-1.4914				
	-1.1018	-103.053				
	1.0513	-1.4914				
	-1.0019	-103.053				
	0.9513	-1.4914				
	-0.9015	-103.053				
	0.8512	-1.4914				
	-0.8014	-103.053				
	0.7509	-1.4914				
	-0.7013	-103.053				
	0.6512	-1.4914				
	-0.6016	-103.053				
	0.5793	-1.4914				
	-0.5513	-103.053				
	0.5209	-1.4914				
	-0.5018	-103.053				
	0.4758	-1.4914				
	-0.4515	-103.053				
	0.4303	-1.4914				
	-0.4020	-103.053				
	0.3802	-1.4914				
	-0.3524	-103.053				
	0.3031	-1.4914				
	-0.2732	-103.053				
	0.2043	-1.4914				
	99.79					



10XER 25 DEG.		10XER 25 DEG.		10XER 25 DEG.		10XER 25 DEG.	
-1.100	15.66	-1.4518	18.07	-1.4518	18.07	-1.4518	18.07
-1.020	16.34	-1.4020	17.70	-1.4020	17.70	-1.4020	17.70
-1.0023	17.42	-1.3524	17.36	-1.3524	17.36	-1.3524	17.36
-0.9517	18.36	-1.3026	17.68	-1.3026	17.68	-1.3026	17.68
-0.9013	19.22	-1.2529	16.88	-1.2529	16.88	-1.2529	16.88
-0.8512	20.25	-1.2035	16.76	-1.2035	16.76	-1.2035	16.76
-0.8010	21.25	-1.1536	16.81	-1.1536	16.81	-1.1536	16.81
-0.7512	22.01	-1.1042	16.96	-1.1042	16.96	-1.1042	16.96
-0.7013	22.50	-1.0544	17.36	-1.0544	17.36	-1.0544	17.36
-0.6512	22.60	-1.0048	18.09	-1.0048	18.09	-1.0048	18.09
-0.6013	23.57	-0.9549	19.43	-0.9549	19.43	-0.9549	19.43
-0.5512	24.00	-0.9058	21.60	-0.9058	21.60	-0.9058	21.60
-0.5013	24.90	-0.8556	24.90	-0.8556	24.90	-0.8556	24.90
-0.4512	25.57	-0.8067	25.57	-0.8067	25.57	-0.8067	25.57
-0.4013	25.33	-0.7577	25.33	-0.7577	25.33	-0.7577	25.33
-0.3512	24.19	-0.7072	24.19	-0.7072	24.19	-0.7072	24.19
-0.3013	23.82	-0.6614	23.82	-0.6614	23.82	-0.6614	23.82
-0.2512	23.81	-0.6257	23.81	-0.6257	23.81	-0.6257	23.81
-0.2013	23.76	-0.6317	23.76	-0.6317	23.76	-0.6317	23.76
-0.1512	23.66	-0.6080	24.12	-0.6080	24.12	-0.6080	24.12
-0.1013	23.51	-0.5815	24.47	-0.5815	24.47	-0.5815	24.47
-0.0512	23.67	-0.5579	24.42	-0.5579	24.42	-0.5579	24.42
-0.0013	23.94	-0.5320	24.19	-0.5320	24.19	-0.5320	24.19
0.0512	23.52	-0.5084	24.12	-0.5084	24.12	-0.5084	24.12
0.1013	23.99	-0.4818	24.31	-0.4818	24.31	-0.4818	24.31
0.1512	24.30	-0.4584	24.19	-0.4584	24.19	-0.4584	24.19
0.2013	24.21	-0.4002	23.67	-0.4002	23.67	-0.4002	23.67
0.2512	24.30	-0.3523	23.94	-0.3523	23.94	-0.3523	23.94
0.3013	24.30	-0.3066	23.52	-0.3066	23.52	-0.3066	23.52
0.3512	24.30	-0.2699	23.99	-0.2699	23.99	-0.2699	23.99

-1	4.032	17.83
-1	3.578	17.51
-1	3.165	17.27
-1	3.062	17.19
-1	2.642	17.05
-1	2.577	17.00
-1	2.542	17.00
-1	2.641	17.91
-1	1.552	17.92
-1	1.051	17.17
-1	0.943	17.63
-1	0.040	18.52
-1	0.930	20.11
-1	0.629	22.62
-1	0.624	24.37
-1	0.623	31.44
-1	0.7516	37.32
-1	7019	42.96
-1	6730	46.42
-1	6514	46.41
-1	6267	47.93
-1	5016	46.42
-1	5736	46.35
-1	5512	46.25
-1	5226	46.09
-1	5015	48.20
-1	4731	48.04
-1	4513	50.05
-1	4034	55.68
-1	3540	67.93
-1	3025	51.05
	999.99	

CARD COUNT 0390

Table II: Experimental Data for xM6-Amino Hexanoic Acid  
Arranged as Used for Input of Program I.

.5M - KF

1	425.7	-0.4740	25.10
-0.4515	25.56		
-0.4018	26.35		
-0.3513	26.92		
-0.3016	27.34		
-0.2514	27.58		
-0.2018	27.81		
-0.1516	28.04		
-0.1020	28.42		
-0.0518	28.97		
-0.0024	29.76		
999.99			

.5M - KE

2	425.7	-0.4740	25.10	1
-0.5010	24.61			
-0.5515	23.54			
-0.6017	22.42			
-0.6515	21.30			
-0.7024	20.26			
-0.7523	19.22			
-0.8046	18.27			
-0.8549	17.57			
-0.9042	17.13			
-0.9537	16.71			
-1.0038	16.42			
-1.0534	16.26			
-1.1036	16.21			
-1.1532	16.24			
-1.2032	16.36			
-1.2528	16.52			
-1.3028	16.78			
-1.3527	17.08			
-1.4022	17.43			
-1.4575	17.98			
999.99				

.01M - 6AH

1	424.1	-0.4656	24.96	0.01
-0.4516	25.14			
-0.4018	26.05			
-0.3518	26.72			
-0.3020	27.20			
-0.2520	27.57			
-0.2022	27.93			
-0.1523	28.36			
-0.1025	28.95			
-0.0525	29.76			
-0.0021	30.95			
999.99				

.01M - 6VH

2	424.1	-0.4656	24.96	0.01
-0.5016	24.06			
-0.5516	42.97			
-0.6024	21.64			
-0.6543	40.46			

-0.7042	19.45			
-0.7542	16.59			
-0.8041	17.81			
-0.8540	17.34			
-0.9041	16.94			
-0.9540	16.65			
-1.0041	16.49			
-1.0537	16.42			
-1.1038	16.41			
-1.1537	16.47			
-1.2037	16.59			
-1.2537	16.78			
-1.3038	17.05			
-1.3538	17.32			
-1.4039	17.62			
-1.4562	16.13			
99.99	0.054...6AH			
		1.	421.6	0.05
		-0.4515	24.17	
		-0.4016	25.48	
		-0.3915	26.54	
		-0.3915	27.41	
		-0.2514	28.12	
		-0.2014	28.80	
		-0.1213	29.61	
		-0.1014	30.59	
		-0.0516	31.97	
		-0.0019	32.82	
		99.59	0.05W...6AH	
			2.	421.6
		-0.5017	22.74	
		-0.5516	21.24	
		-0.6021	19.84	
		-0.6522	18.63	
		-0.6954	17.66	
		-0.7506	16.49	
		-0.8508	16.42	
		-0.8509	16.12	
		-0.8010	16.05	
		-0.7512	16.09	
		-1.0013	16.27	
		-1.0464	16.49	
		-1.1001	16.77	
		-1.1505	12.05	
		-1.2008	17.25	
		-1.2510	17.56	
		-1.3015	17.78	
		-1.3506	18.04	
		-1.4011	18.30	
		-1.4463	18.61	
		-1.4860	18.95	
		99.99	0.1V 6AH	
			1.	421.3
			-0.45C6	23.60
			-0.6023	25.12

-0.3519	26.46
-0.3050	27.62
-0.2518	28.60
-0.2022	29.56
-0.1520	30.69
-0.1023	32.06
-0.0532	33.79
-0.0033	36.04
29.965	
1N 6AH	
2	
-0.4119	23.59
-0.3024	24.96
-0.2021	20.23
-0.1502	18.51
-0.1025	17.57
-0.0740	16.54
-0.0750	15.83
-0.0805	15.38
-0.0868	15.17
-0.0939	15.18
-0.09470	15.35
-1.0016	15.74
-1.0012	16.19
-1.0116	16.62
-1.1613	17.21
-1.2615	12.72
-1.2112	18.17
-1.3015	18.54
-1.3512	18.87
-1.4017	19.17
-1.4214	19.44
-1.4917	19.61
999.95	
C.2E -6AH	
2	
-0.4040	24.38
-0.3537	26.01
-0.3043	27.49
-0.2540	28.53
-0.2047	30.16
-0.1544	31.80
-0.1050	33.68
-0.0549	35.92
-0.0058	38.72
-999.92	
.2N 6AH	
2	
-0.4534	22.67
-0.5037	20.89
-0.532	19.29
-0.6034	17.80
-0.6528	16.47
-0.7050	15.41
-0.7538	14.70
-0.8040	14.26
-0.8235	14.02



-0.2017	-21.69
-0.1517	-34.43
-0.1018	37.30
-0.0520	-60.30
-0.0022	44.24
0.99999	
0.5N	6AH
2	
-0.4004	-41.61
-0.3007	19.93
-0.2006	-18.20
-0.1011	16.61
-0.0510	-15.29
-0.0010	14.27
-0.7411	-12.58
-0.6013	12.18
-0.5013	-13.02
-0.9015	12.09
-0.5015	-13.02
-1.0017	12.74
-1.0017	-14.30
-1.0004	12.96
-1.1008	-15.79
-1.2010	16.74
-1.2516	-17.74
-1.3001	18.75
-1.3507	-19.82
-1.4014	20.85
-1.4518	-21.71
-1.4825	22.17
0.99999	
0.7V	6AH
1	
-0.4013	-23.24
-0.3513	25.32
-0.3012	-27.57
-0.2512	29.42
-0.2012	-32.11
-0.1512	35.03
-0.1016	-35.46
-0.0517	42.25
-0.0021	-46.79
0.99999	
0.7V	6AH
2	
-0.4512	21.24
-0.5012	-19.35
-0.5512	17.68
-0.6012	-16.21
-0.6511	14.85
-0.7010	-13.43
-0.7510	13.17
-0.8012	-12.80
-0.8511	12.57
-0.9011	-12.57
-0.9510	13.62
-1.0010	-13.62

-1.0509 12.63  
-1.1008 14.48  
-1.1508 15.27  
-1.2010 16.13  
-1.2510 17.14  
-1.3012 18.24  
-1.3513 19.39  
-1.4015 20.54  
-1.4523 21.6d  
-1.4927 22.7d  
999.00

CARD COUNT 0311

Table III: INTEGRATION OF DOUBLE LAYER CAPACITY FOR IMKF

1MKF	25 DEG	$\frac{q}{E(V)}$	$\frac{Y}{C(MC/CR2)}$	$\frac{\xi}{G(ERG/CR2)}$	$\frac{C}{C(MF/CM2)}$	$\frac{1/C}{1/C}$	$\frac{d}{CD}$	$\frac{c}{CI}$	$\frac{1/c}{1/CI}$	$\frac{\phi}{\phi_{IMF}}$
-0.4756	-5	-0.	0.	0.2638E-02	0.3791E-01	0.2285E-03	0.2982E-02	0.3353E-01	0.	
-0.4376	1	-2.19	-4.56	0.2708E-02	0.3692E-01	0.2293E-03	0.3071E-02	0.3256E-01	0.3304E-01	
-0.4012	2	-2.73	-8.76	0.2778E-02	0.3600E-01	0.2318E-03	0.3156E-02	0.3169E-01	0.6510E-01	
-0.3554	3	-1.52	-12.59	0.2820E-02	0.3546E-01	0.2359E-03	0.3203E-02	0.3122E-01	0.9655E-01	
-0.3202	4	-2.66	-16.07	0.2852E-02	0.3506E-01	0.2414E-03	0.3235E-02	0.3092E-01	0.1276E-00	
-0.2852	5	-4.43	-19.19	0.2868E-02	0.2487E-01	0.2484E-03	0.3242E-02	0.3084E-01	0.1584E-00	
-0.2504	6	-5.34	-21.97	0.2876E-02	0.3477E-01	0.2561E-03	0.3239E-02	0.3087E-01	0.1893E-00	
-0.2257	7	-8.40	-24.40	0.2877E-02	0.3475E-01	0.2661E-03	0.3226E-02	0.3100E-01	0.2202E-00	
-0.1909	8	-10.21	-26.48	0.2881E-02	0.3471E-01	0.2766E-03	0.3216E-02	0.3109E-01	0.2513E-00	
-0.1552	9	-14.16	-28.22	0.2883E-02	0.3469E-01	0.2881E-03	0.3204E-02	0.3121E-01	0.2824E-00	
-0.1216	10	-17.45	-29.61	0.2890E-02	0.3460E-01	0.3004E-03	0.3208E-02	0.3117E-01	0.3136E-00	
-0.0973	11	-21.26	-30.62	0.2911E-02	0.3433E-01	0.3134E-03	0.3222E-02	0.3104E-01	0.3447E-00	
-0.0732	12	-24.97	-31.36	0.2960E-02	0.3379E-01	0.3270E-03	0.3254E-02	0.3073E-01	0.3757E-00	
-0.0497	13	-29.15	-31.72	0.3026E-02	0.3305E-01	0.3412E-03	0.3321E-02	0.3012E-01	0.4061E-00	
0.0261	14	-32.55	-31.75	0.3134E-02	0.3191E-01	0.3559E-03	0.3436E-02	0.2910E-01	0.4358E-00	
0.0041	15	-38.08	-31.47	0.3289E-02	0.3041E-01	0.3711E-03	0.3609E-02	0.2771E-01	0.4643E-00	

## INTEGRATION OF DOUBLE LAYER CAPACITY

IMMF	25	DEC	E(V)	G(C1/CM2)	G(EFG/CM2)	X1(ERG/CM2)	C1MF/CM2)	1/C	CD	C1	1/C1	PHM2
-0.4750	-0	-0	0.	0.2638E 02	0.3791E-01	0.2288E 03	0.2982E 02	0.3353E-01	0.			
-0.5135	-1	-0.19	4.94	0.2550E 02	0.2922E-01	0.2293E 03	0.2869E 02	0.3486E-01	-0.3415E-01			
-0.5537	-2	-0.80	10.28	0.2438E 02	0.4101E-01	0.2318E 03	0.2725E 02	0.3677E-01	-0.6993E-01			
-0.5957	-3	-1.85	16.02	0.2324E 02	0.4303E-01	0.2359E 03	0.2578E 02	0.3877E-01	-0.1076E 00			
-0.6354	-4	-3.40	22.20	0.2205E 02	0.4535E-01	0.2414E 03	0.2427E 02	0.4121E-01	-0.1476E 00			
-0.5865	-5	-5.50	28.83	0.2080E 02	0.4790E-01	0.2488E 03	0.2279E 02	0.4387E-01	-0.1902E 00			
-0.7357	-6	-8.21	35.93	0.1976E 02	0.5061E-01	0.2577E 03	0.2141E 02	0.4671E-01	-0.2354E 00			
-0.7377	-7	-12.59	43.55	0.1376E 02	0.5330E-01	0.2661E 03	0.2018E 02	0.4954E-01	-0.2836E 00			
-0.6422	-8	-15.68	51.70	0.1792E 02	0.5580E-01	0.2766E 03	0.1916E 02	0.5218E-01	-0.3344E 00			
-0.8292	-9	-20.53	60.40	0.1722E 02	0.5806E-01	0.2881E 03	0.1832E 02	0.5459E-01	-0.3878E 00			
-0.9551	-10	-26.13	69.69	0.1674E 02	0.5974E-01	0.3004E 03	0.1773E 02	0.5641E-01	-0.4434E 00			
-1.0184	-11	-32.69	79.57	0.1646E 02	0.6077E-01	0.3134E 03	0.1737E 02	0.5758E-01	-0.5004E 00			
-1.0795	-12	-39.48	90.06	0.1632E 02	0.6127E-01	0.3270E 03	0.1718E 02	0.5821E-01	-0.5583E 00			
-1.1405	-13	-47.15	101.16	0.1632E 02	0.6126E-01	0.3412E 03	0.1714E 02	0.5833E-01	-0.5167E 00			
-1.2015	-14	-55.39	112.87	0.1646E 02	0.6075E-01	0.3559E 03	0.1726E 02	0.5794E-01	-0.5749E 00			
-1.2616	-15	-64.05	125.19	0.1691E 02	0.5912E-01	0.3711E 03	0.1772E 02	0.5643E-01	-0.7319E 00			
-1.3205	-16	-73.24	138.11	0.1697E 02	0.5992E-01	0.3866E 03	0.1775E 02	0.5633E-01	-0.7885E 00			
-1.3791	-17	-82.04	151.61	0.1736E 02	0.5759E-01	0.4025E 03	0.1815E 02	0.5510E-01	-0.8441E 00			
-1.4360	-18	-92.40	165.68	0.1779E 02	0.5620E-01	0.4197E 03	0.1858E 02	0.5381E-01	-0.8986E 00			
-1.4914	-19	-102.05	180.32	0.1829E 02	0.5464E-01	0.4352E 03	0.1910E 02	0.5237E-01	-0.9517E 00			
*#0**												
EOF READ ON UNIT 00005 --- EXECUTION TERMINATED												

Table IV: Integration of Double-Layer-Capacity For .5 MKF

$\sigma_{5M}$	KF	$E(V_B)$	$Q(MC/CM2)$	$G(ERG/CM2)$	$X(TERG/CM2)$	$C(MF/CM2)$	$1/C$	$1/G$	$c_d$	$c_i^1$	$1/c_i^1$	$\sigma_{m-2}^{m-2}$
-0.4740	-9	425.70	425.70	0.2510E.02	0.3984E-01	0.1616E.03	0.2972E.02	0.3365E-01	0.	0.	0.	0.
-0.4348	-1	425.51	425.51	0.2588E.02	0.3854E-01	0.1627E.03	0.3078E.02	0.3249E-01	0.	0.	0.	0.
-0.2966	-2	426.93	417.00	0.2642E.02	0.3785E-01	0.1662E.03	0.3141E.02	0.3183E-01	0.	0.	0.	0.
-0.2592	-3	423.99	413.22	0.2695E.02	0.3725E-01	0.1718E.03	0.3102E.02	0.3143E-01	0.	0.	0.	0.
-0.3220	-4	422.70	409.82	0.2719E.02	0.3679E-01	0.1794E.03	0.3204E.02	0.3121E-01	0.	0.	0.	0.
-0.2854	-5	421.05	406.78	0.2744E.02	0.3545E-01	0.1887E.03	0.3211E.02	0.3115E-01	0.	0.	0.	0.
-0.2490	-6	419.05	406.11	0.2759E.02	0.3624E-01	0.1995E.03	0.3202E.02	0.3123E-01	0.	0.	0.	0.
-0.2129	-7	415.70	401.80	0.2776E.02	0.3602E-01	0.2115E.03	0.3195E.02	0.3130E-01	0.	0.	0.	0.
-0.1770	-8	414.01	399.85	0.2792E.02	0.3581E-01	0.2246E.03	0.3189E.02	0.3136E-01	0.	0.	0.	0.
-0.1413	-9	410.97	398.25	0.2811E.02	0.3559E-01	0.2385E.03	0.3186E.02	0.3139E-01	0.	0.	0.	0.
-0.1059	-10	407.61	387.93	0.2839E.02	0.3523E-01	0.2532E.03	0.3197E.02	0.3128E-01	0.	0.	0.	0.
-0.0708	-11	403.93	396.14	0.2874E.02	0.3479E-01	0.2685E.03	0.3219E.02	0.3107E-01	0.	0.	0.	0.
-0.0363	-12	395.61	392.96	0.2920E.02	0.3425E-01	0.2843E.03	0.3254E.02	0.3073E-01	0.	0.	0.	0.

## INTEGRATION.OE\_DOUBLE\_LAYER\_CAPACITY

$\cdot 5M$	$KF$	$\cdot 0(MC/CM2)$	$G(ERG/CM2)$	$X(ITERG/CM2)$	$C(MF/CM2)$	$1/C$	$CD$	$CT$	$1/CT$	$PRIM2$
-0.4740	-2	425.70	425.70	0.2510E 02	0.3984E-01	0.1616E 03	0.2972E 02	0.3365E-01	0.	
-0.5144	-1	425.50	420.64	0.2436E .02	0.4104E-01	0.1627E 03	0.2863E..02	0.3490E-01	-0.3423E-01	
-0.5552	-2	424.87	435.93	0.2344E .02	0.4257E-01	0.1662E 03	0.2728E..02	0.3665E-01	-0.5999E-01	
-0.5998	-3	423.78	441.77	0.2246E .02	0.4452E-01	0.1718E 03	0.2584E..02	0.3870E-01	-0.1076E 03	
-0.6454	-4	422.18	448.00	0.2144E .02	0.4665E-01	0.1794E 03	0.2435E..02	0.4107E-01	-0.1475E..00	
-0.6922	-5	420.03	454.69	0.2039E .02	0.4903E-01	0.1887E 03	0.2287E..02	0.4372E-01	-0.1899E 00	
-0.7425	-6	417.26	461.87	0.1939E .02	0.5157E-01	0.1995E 03	0.2149E..02	0.4655E-01	-0.2350E..00	
-0.7964	-7	413.82	469.57	0.1849E .02	0.5407E-01	0.2115E 03	0.2027E..02	0.4934E-01	-0.2830E..00	
-0.8517	-8	409.67	477.81	0.1771E .02	0.5645E-01	0.2246E 03	0.1923E..02	0.5201E-01	-0.3336E..00	
-0.9092	-2	404.78	486.61	0.1708E .02	0.5854E-01	0.2365E 03	0.1840E..02	0.5435E-01	-0.3868E..00	
-0.9686	-10	399.13	496.00	0.1661E .02	0.6020E-01	0.2532E 03	0.1778E..02	0.5625E-01	-0.4422E..00	
-1.0294	-11	392.75	505.98	0.1633E .02	0.6124E-01	0.2685E 03	0.1739E..02	0.5752E-01	-0.4991E..00	
-1.0909	-12	385.68	516.59	0.1621E .02	0.6163E-01	0.2843E 03	0.1719E..02	0.5817E-01	-0.5570E..00	
-1.1525	-13	377.97	527.80	0.1624E .02	0.6158E-01	0.3005E 03	0.1717E..02	0.5825E-01	-0.6152E..00	
-1.2139	-14	369.69	529.64	0.1633E .02	0.6105E-01	0.3171E 03	0.1727E..02	0.5789E-01	-0.6733E..00	
-1.2745	-15	360.90	552.08	0.1662E .02	0.6016E-01	0.3341E 03	0.1749E..02	0.5717E-01	-0.7309E..00	
-1.3341	-16	351.67	565.12	0.1697E .02	0.5894E-01	0.3512E 03	0.1783E..02	0.5610E-01	-0.7875E..00	
-1.3924	-17	342.05	578.75	0.1736E .02	0.5761E-01	0.3687E 03	0.1822E..02	0.5490E-01	-0.8420E..00	
-1.4492	-18	332.11	592.97	0.1739E .02	0.5591E-01	0.3863E 03	0.1876E..02	0.5332E-01	-0.8972E..00	
* * 0 *	*	EOF PREAD ON UNIT 00005	---	EXECUTION TERMINATED						

Table V: Input Cards for Program II.

-4.0	-4.0	-4.0	-4.0
4.0	-16.0	-8.0	-3.302
4.0	-1b.0	-2b.0	0.0020
4.0	-19.47	0.0100	-0.3932
4.0	-21.03	0.0200	-0.4150E
4.0	-22.63	0.0400	-0.4381
4.0	-25.36	0.1000	-0.4606
4.0	-27.95	0.2000	-0.4782E
4.0	-30.52	0.4000	-0.4922E
4.0	-33.17	0.8000	-0.4990E
6.0	-34.57	1.0000	-0.4846E
			CARD COUNT J024

Table VI: Output of the Program III.

CHARGE= 4.0

	$X_1 = -0.3441E-021 + (-0.1771E-02)X + (-0.4309E-01)X^2 + (-0.4577E-02)X^3$	$\ln X$	$q$	$\ln \phi$	$\phi$	$C_d$	$\frac{1}{\Delta G}$	$E-E_b$	$\phi^2$	$\phi^{m-2}$	$x(i)$
CON	L'CON	QSA	SP	LSP	X1	DIFF	CD	DE	PH12	PHIM-2	
0.0050	-5.2983	-6.00	2.19	0.7839	-18.26	-0.02	0.2318E-03	0.1101E-01	0.0630	-0.0087	0.0905 -1.3611
0.0100	-4.6052	-7.53	3.40	1.2238	-19.47	-0.01	0.2386E-03	0.1252E-01	0.0845	-0.0153	0.0756 -1.1831
0.0200	-3.9120	-9.06	4.96	1.6014	-21.03	0.07	0.2489E-03	0.1352E-01	0.1079	-0.0216	0.0585 -1.0050
0.0400	-3.2189	-10.59	6.56	1.8810	-22.63	-0.08	0.2621E-03	0.1415E-01	0.1304	-0.0276	0.0420 -0.8269
0.1000	-2.3026	-12.62	9.29	2.2289	-25.36	-0.08	0.2836E-03	0.1462E-01	0.1629	-0.0350	0.0169 -0.5915
0.2000	-1.6094	-14.15	11.88	2.4749	-27.95	0.12	0.3022E-03	0.1475E-01	0.1887	-0.0402	-0.0037 -0.4135
0.4000	-0.9163	-15.68	14.45	2.6707	-30.52	0.04	0.3226E-03	0.1469E-01	0.2122	-0.0452	-0.0222 -0.2354
0.8000	-0.2231	-17.21	17.12	2.8402	-33.19	-0.22	0.3443E-03	0.1443E-01	0.2336	-0.0498	-0.0390 -0.0573
1.0000	0.	-17.71	18.50	2.9178	-34.57	0.16	0.3516E-03	0.1440E-01	0.2430	-0.0512	-0.0470 0.
**0**	EOF READ ON UNIT 00005 --- EXECUTION TERMINATED										

Table VII: Input Cards for Program V.

0.00050 -4.0 -94.39
0.0100 4.0 91.60
0.0200 -4.0 -db.97
0.0400 4.0 86.48
0.1000 -4.0 83.39
0.2000 4.0 81.21
0.4000 -4.0 79.14
0.6000 4.0 77.16
1.0000 -4.0 76.56
4.0 -16.0 -0.3302 0.2852E 02 0.3235E 02
1.0135 -4.0 0.0050
1.02260 4.0 0.0100
1.02390 -4.0 -0.0200
1.03448 4.0 0.0400
1.03671 -4.0 0.1000
1.03752 4.0 0.2000
1.03182 -4.0 -0.4000
1.02266 4.0 0.8000
1.02209 -4.0 1.0000
0.00050 -6.0 0 2.19 0.2318E 03 0.0101E-01 C.0.0630 0.415BE 02 4.0 0.9054E-01
0.0100 -7.53 -3.40 0.2386E 03 0.1252E-01 0.0845 0.4439E 02 4.0 0.7556E-01
0.0200 -9.06 4.96 0.2489E 03 0.1352E-01 0.1079 0.4642E 02 4.0 0.5844E-01
0.0400 -10.59 -6.36 -0.2621E 03 0.1415E-01 0.1304 0.4782E 02 4.0 0.4196E-01
0.1000 -12.62 9.29 0.2826E 03 0.1462E-01 0.1629 0.4852E 02 4.0 0.1690E-01
0.2000 -14.15 11.38 0.3022E 03 0.1475E-01 0.1861 0.4922E 02 4.0 -0.4657E-02
0.5000 -12.68 14.42 0.3226E 03 0.1468E-01 0.2122 0.4905E 02 4.0 -0.2224E-01
0.8000 -17.21 -14.12 0.3445E 03 0.1442E-01 0.2336 0.4846E 02 4.0 -0.3903E-01
1.0000 -17.71 16.20 0.3210E 03 0.1440E-01 0.2430 0.4791E-01 CARD COUNT 0041

Table VIII. Printed Output of Program V.

$\Omega = 4.0$	$c^d$	$c^1$	$(\frac{\partial q}{\partial \phi_m})_1$	$(\frac{\partial q}{\partial \phi_m})_2$	$(\frac{\partial q}{\partial \phi_m})_3$
CON C	DO SA	CI	DOPHI	DOSPHI	DCI
0.0050 0.4158E-02	0.2318E-02	-0.1132E-01	0.4061E-02	0.2730E-02	0.9439E-02
0.0100 0.4435E-02	0.2396E-03	-0.1229E-01	0.4254E-02	0.2708E-02	0.9160E-02
0.0200 0.4642E-02	0.2489E-03	-0.1299E-01	0.4397E-02	0.2678E-02	0.8897E-02
0.0400 0.4782E-02	0.2621E-03	-0.1345E-01	0.4499E-02	0.2647E-02	0.8648E-02
0.1000 0.4892E-02	0.2836E-03	-0.1367E-01	0.4601E-02	0.2623E-02	0.8339E-02
0.2000 0.4922E-02	0.3022E-03	-0.1355E-01	0.4653E-02	0.2619E-02	0.8121E-02
0.4000 0.4909E-02	0.3226E-03	-0.1318E-01	0.4682E-02	0.2631E-02	0.7914E-02
0.8000 0.4846E-02	0.3443E-03	-0.1257E-01	0.4677E-02	0.2655E-02	0.7716E-02
1.0000 0.4830E-02	0.3516E-03	-0.1231E-01	0.4690E-02	0.2674E-02	0.7654E-02
** 0**	EOF READ ON UNIT 00005	EXECUTION TERMINATED			