

Optimal design of experiment: supercritical fluid extraction case

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Introduction

This study investigates the extraction of valuable components from biomass using supercritical carbon dioxide as a solvent. The interest is in essential oils extracted from chamomile flowers in cylindrical extractors operated in a semi-batch mode. The extraction process is described by a distributed-parameter model, and set of empirical correlations. This work aims to validate the empirical correlations by designing a new experiment with dynamically changing operating conditions.

Process Model

- One-dimensional
- Plug flow
- No pressure drop
- Uniform particle distribution
- Based on the two-film theory for a single component
- Peng-Robinson equation of state
- Decaying extraction kinetic
- Empirical correlations

$$\dot{x} = \frac{dx}{dt} = \begin{bmatrix} \frac{\partial c_f}{\partial t} \\ \frac{\partial c_s}{\partial t} \\ \frac{\partial (\rho_f h A_f)}{\partial t} \\ \frac{dy}{dt} \end{bmatrix} = \begin{bmatrix} -\frac{1}{\phi} \frac{\partial (c_f u)}{\partial z} + \frac{1-\phi}{\phi} \frac{\partial c_s}{\partial t} + \frac{1}{\phi} \frac{\partial}{\partial z} \left(D_e^M \frac{\partial c_f}{\partial z} \right) \\ D_i^R \exp \left(\Upsilon \left(1 - \frac{c_s}{c_{s0}} \right) \right) \\ - \frac{\partial (\rho_f h A_f)}{\partial z} + \frac{\partial (P A_f)}{\partial t} + \frac{\partial}{\partial z} \left(k_m \rho_f \right) \\ \frac{F}{\rho_f c_f} \Big|_{z=L} \\ G(x, t, \Theta; \Xi) \end{bmatrix}$$

c_f – Soluts concentration in the fluid phase
 c_s – Soluts concentration in the solid phase
 h – Enthalpy
 y – Extraction yield
 ρ_f – Density of fluid
 A_f – Cross-section of the bed
 u – Darcy velocity
 ϕ – Void fraction

D_e^M – Axial mass diffusivity
 D_i^R – Internal mass diffusivity
 Υ – Decaying factor
 ρ_s – Bulky density of solid bed
 k_m – Partition factor
 P – Pressure
 T – Temperature
 F – Mass flow rate

$$D_i^R = 0.190 - 8.188 \cdot Re + 0.620 \cdot F \times 10^5 \\ R^2 = 0.868$$

$$\Upsilon = 3.158 + 11.922 \cdot Re - 0.686 \cdot F \times 10^5 \\ R^2 = 0.823$$

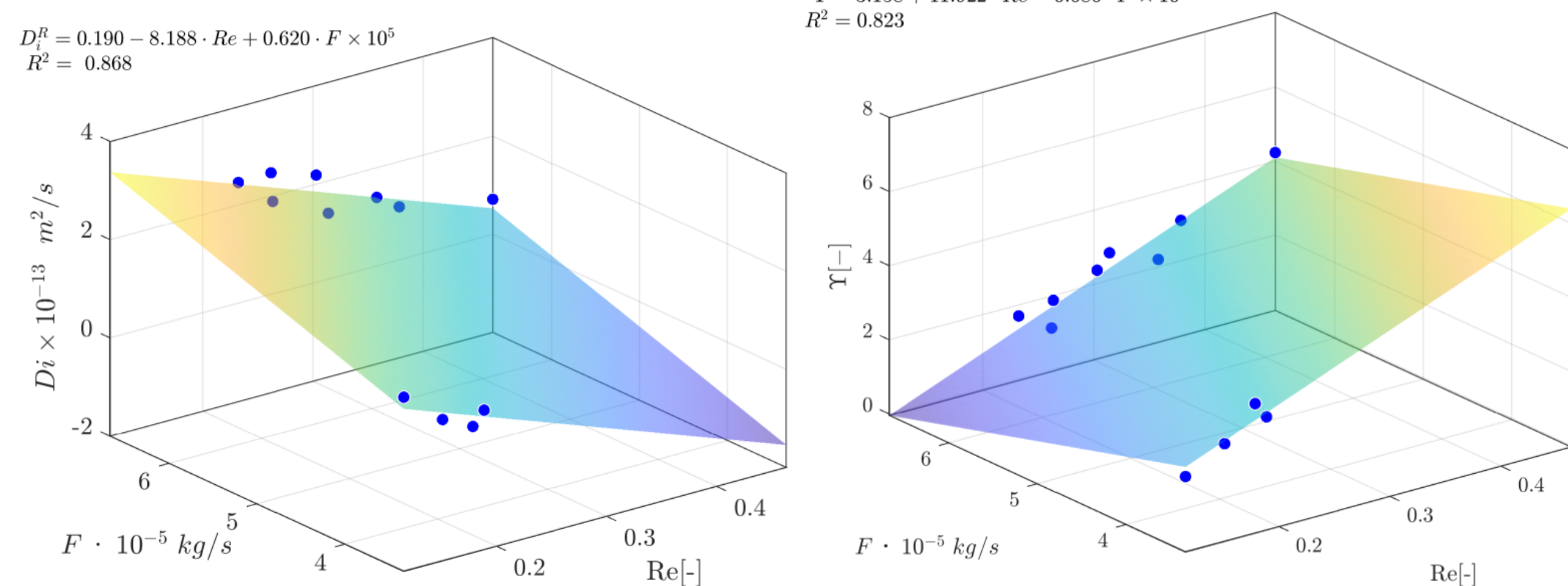


Figure 1: Empirical correlations

Model-based optimal design of experiment

Fisher information \mathcal{F} measures the amount of information that an observable random variable carries about an unknown parameter of a distribution that models the random variable. \mathcal{F} is defined as Hessian of the log-likelihood function with respect to the parameters Θ , given the covariance matrix Σ .

$$\mathcal{F}(t, \Theta; \Xi) = \frac{\partial y(t, \Theta; \Xi)}{\partial \Theta} \Sigma \frac{\partial y(t, \Theta; \Xi)}{\partial \Theta^T}$$

The optimal design of experiments is a concept that refers to planning an experiment, which allow parameters to be estimated without bias and with minimum variance. The D-optimality criterion is selected as the objective function, which leads to the minimisation of the volume of the ellipsoidal confidence region of parameter estimates given the experimental condition Ξ .

$$\begin{aligned} \Xi^* &= \arg \min_{T^{in}, F \in \Xi} \int_{t_0}^{t_f} -\ln \det \mathcal{F}(t, \Theta; \Xi) dt \\ \text{subject to} \quad &\dot{x} = G(x, t, \Theta; \Xi) \\ &T^0 = T^{in}(t=0) \\ &30^\circ C \leq T^{in}(t) \leq 40^\circ C \\ &3.33 \cdot 10^{-5} \text{ kg/s} \leq F(t) \leq 6.67 \cdot 10^{-5} \text{ kg/s} \\ &100 \text{ bar} \leq P(t) \leq 200 \text{ bar} \end{aligned}$$

This work aims to design a dynamic experiment to improve precision of correlation for D_i^R . The system is assumed to run for 300 min, with sampling time of 10 min. The set of decision variables consists of T^{in} and F , and each of them is manipulated every 15 min. Each of five analysed cases assumes that P is kept constant at 100, 125, 150, 175 and 200 bar, respectively.

Results

To identify the global solution, the optimization problem is solved multiple times, each starting from a random initial solution. Figure 2 compares the initial and final values of the cost function across multiple optimization runs for different cases of pressure value.

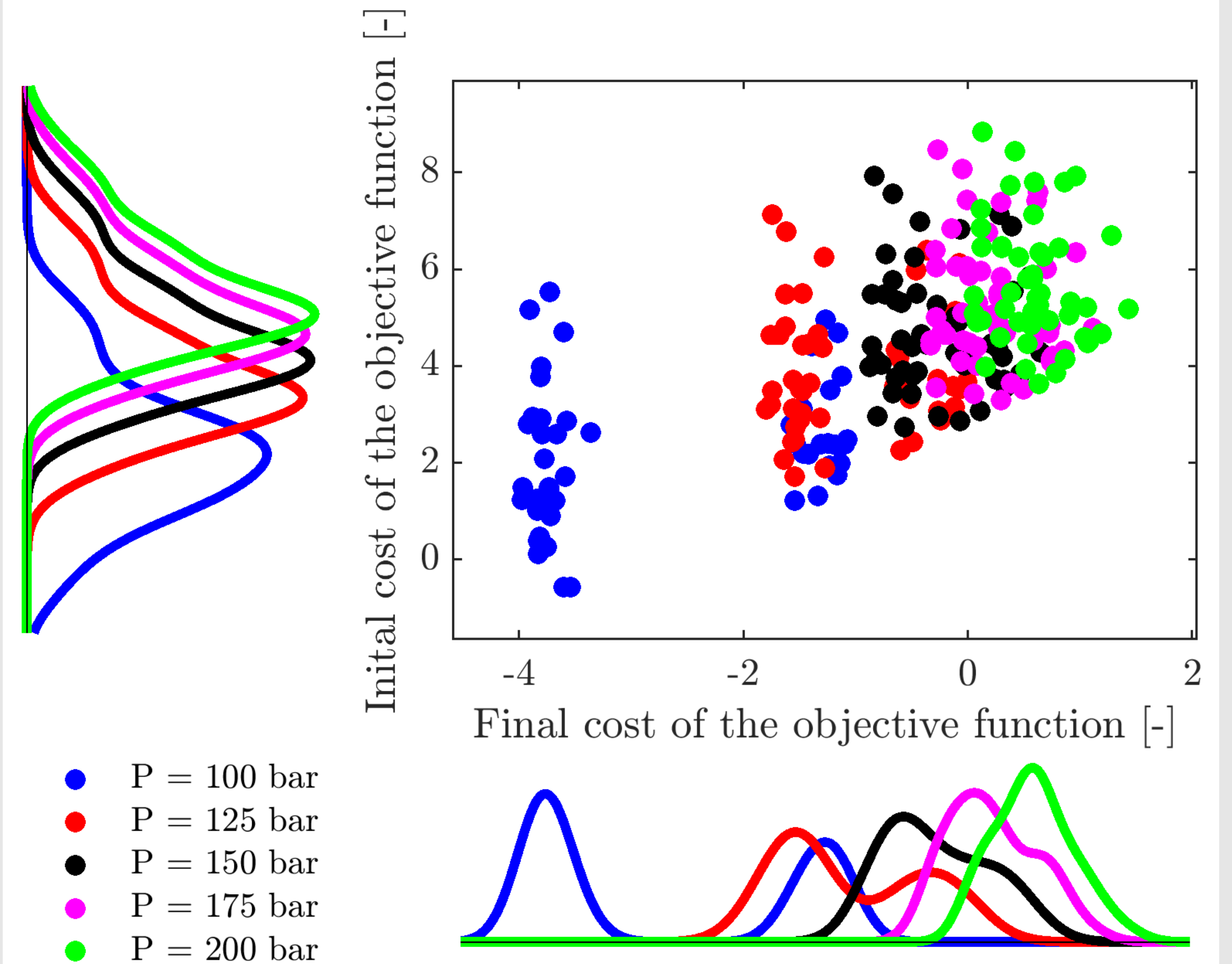


Figure 2: Values of the objective function

The optimal profiles of the inlet temperature and flow rates for each case are showed in Figure 3

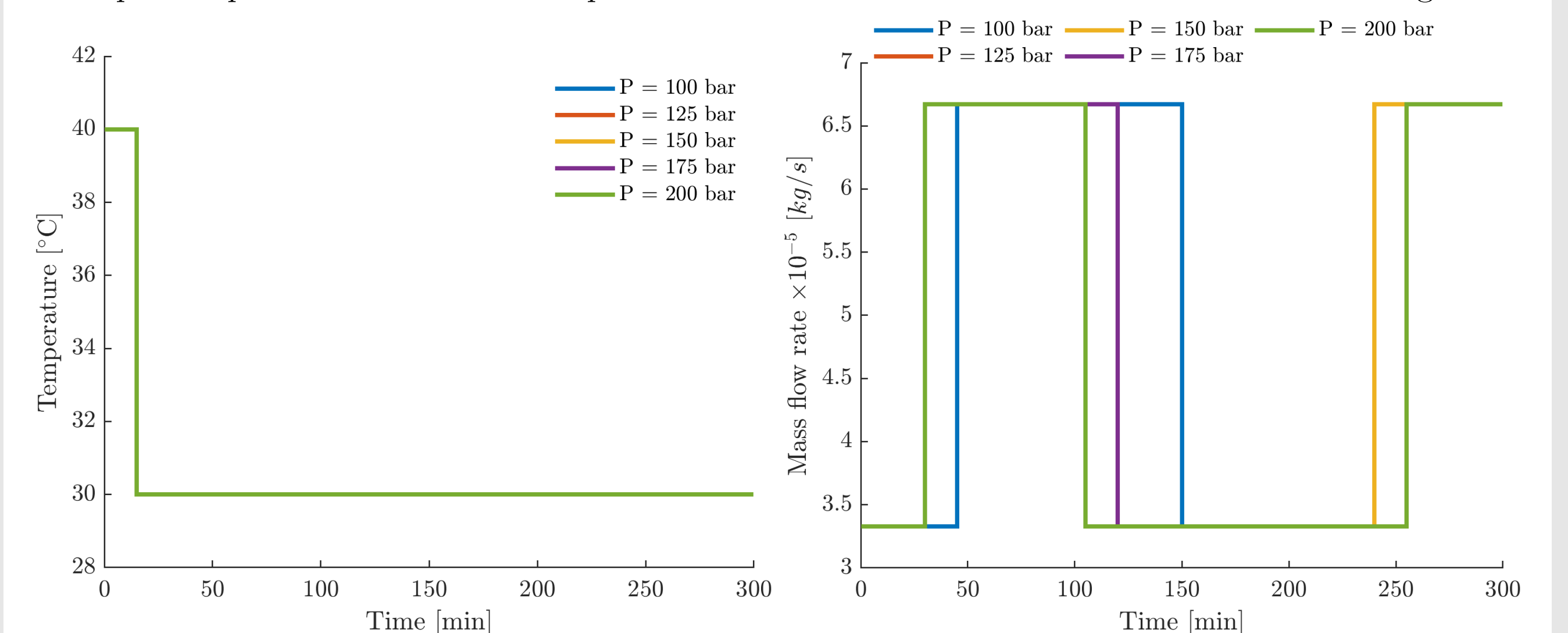


Figure 3: Optimal profiles

Conclusions

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Forthcoming Research

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References

- [1] A. B. Jones and J. M. Smith. Article Title. Journal title, 13(52):123–456, March 2013.
- [2] J. M. Smith and A. B. Jones. Book Title. Publisher, 7th edition, 2012.

Acknowledgements

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