

(1)

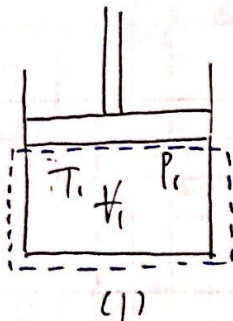
GIVEN

Piston-cylinder with refrigerant R-134a

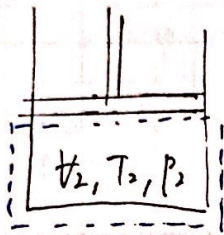
>> constant p process

* $P_1 = 4 \text{ bar} \rightarrow P_2, T_1 \rightarrow T_2 = 30^\circ\text{C}$

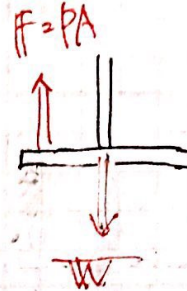
>> pF & kF negligible

FIND Show p-v diagram and find work, \dot{W} and \dot{Q} FFD

(1)



(2)

FFDASSUMP

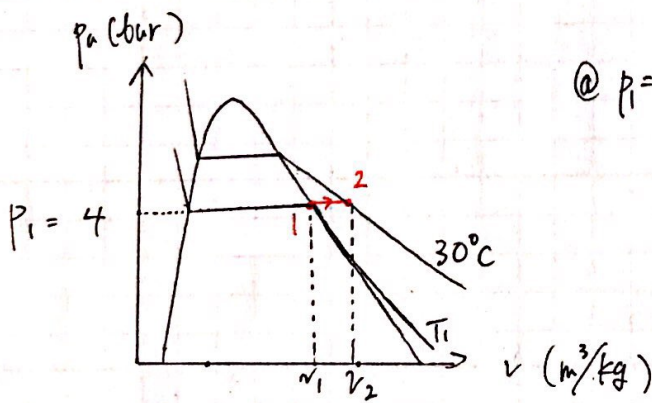
- closed sys.
- Quasi-equilibrium
- pF = kF = 0
- isobar

EQN

$$\frac{dm}{dt}|_{\text{sys}} = \dot{m}_{\text{in}} - \dot{m}_{\text{out}}$$

$$\cancel{\Delta pF} + \cancel{\Delta kF} + \Delta U = Q - W$$

$$W = \int p dV$$

SOLN

$$@ P_1 = 4.0 \text{ bar } T_{\text{sat}} = 8.9306^\circ\text{C}$$

the is all gas, and from SHV @ $P_1 = 4 \text{ bar}$ and state 1 is ($T_1 = T_{\text{sat}}$)

$$v_{g1} = 0.051207 \frac{\text{m}^3}{\text{kg}}$$

and at state 2 using same table $v_{g2} = 0.05680$

thus,

$$W_{12} = \int_{v_1}^{v_2} P dv = P_1 v_{g2} - P_1 v_{g1} = (4 \times 10^5 \text{ Pa})(0.05680 - 0.051207) \frac{\text{m}^3}{\text{kg}} \approx 2.237 \frac{\text{kJ}}{\text{kg}}$$

and from same table the internal energies are ($\frac{\text{kJ}}{\text{kg}}$)

$$u_1 = 235.09 \frac{\text{kJ}}{\text{kg}} \quad u_2 = 252.4 \frac{\text{kJ}}{\text{kg}}$$

$$\Delta u_{12} = u_2 - u_1 = (252.4 - 235.09) \frac{\text{kJ}}{\text{kg}} = 17.31 \frac{\text{kJ}}{\text{kg}}$$

therefore

$$\Delta q_{12} = \Delta u_{12} + \Delta w_{12}$$

$$= (17.31 \frac{\text{kJ}}{\text{kg}}) + (2.24 \frac{\text{kJ}}{\text{kg}})$$

$$= 19.55 \frac{\text{kJ}}{\text{kg}}$$

$$w_{12} = 2.24 \frac{\text{kJ}}{\text{kg}}$$

$$q_{12} = 19.6 \frac{\text{kJ}}{\text{kg}}$$

(ii)

GIVEN sys. w/ 1 kg of H₂O
 → Power cycle.

* Process 1-2: isovol \dot{Q}_{in} $P_1 = 5 \text{ bar}$, $T_1 = 160^\circ\text{C} \rightarrow P_2 = 10 \text{ bar}$, T_2

* Process 2-3: isobar $\dot{Q}_{out} \rightarrow T_3 = T_{sat3}$

* Process 3-4: isovol $\dot{Q}_{out} \rightarrow T_4 = 160^\circ\text{C}$

* Process 4-1: isotherm expansion w/ $Q_{in} = 815.8 \text{ kJ}$

FIND

- (a) sketch T-v & p-v diagrams
 (b) W & Q for each process.

ASSUMP

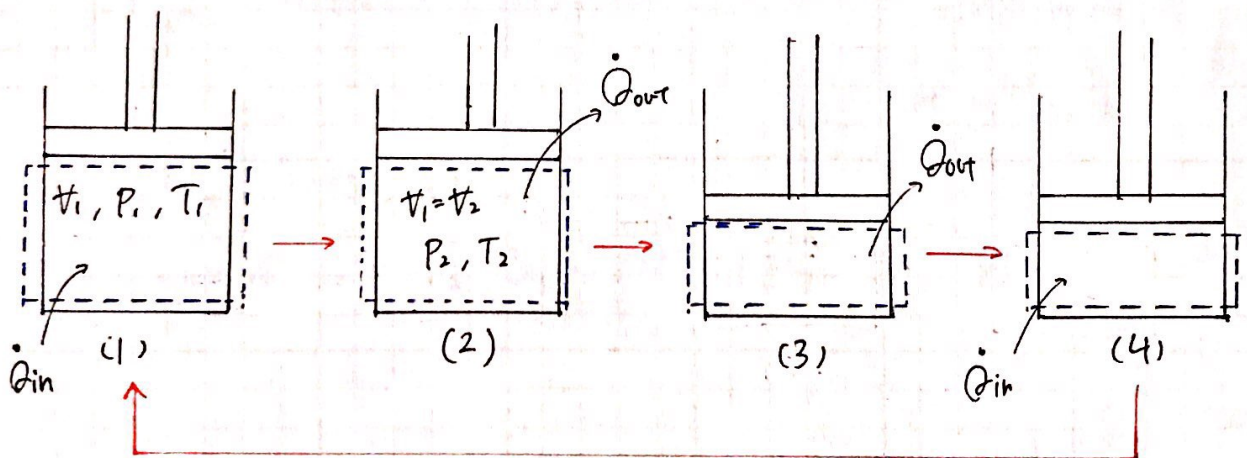
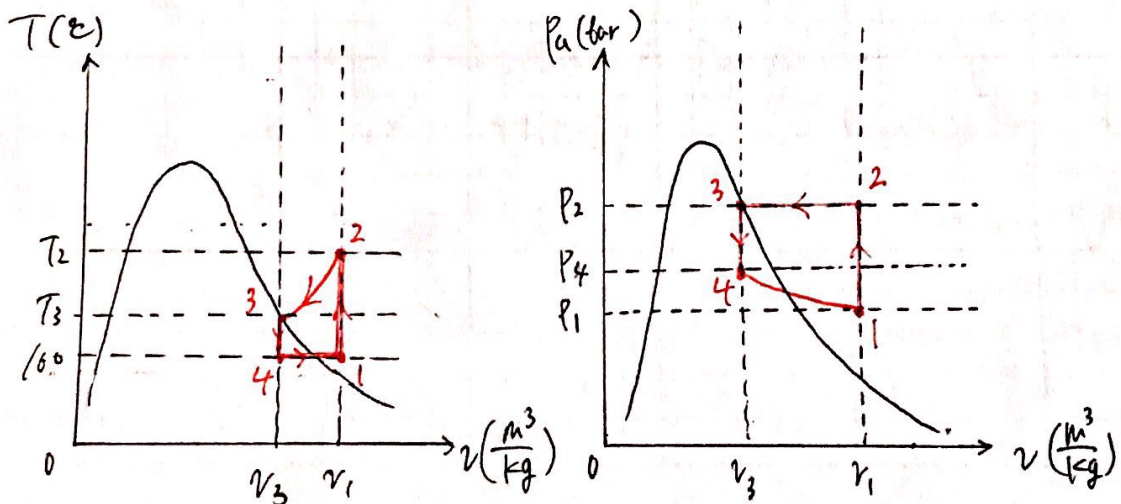
- Quasiequilibrium
- closed sys.
- PE = KE = 0

EQN

$$\frac{dm}{dt}|_{sys} = \dot{m}_{in} - \dot{m}_{out}$$

$$\Delta Q = \Delta U + \Delta W$$

$$W = \int P dV$$

EEDSOLN

from saturation table T_{sat} @ $p_1 = 5 \text{ bar}$ is $T_{sat1} = 151.83^\circ\text{C}$

T_{sat} @ (3) is $T_{sat3} = 179.88^\circ\text{C}$

(I) Process 1 \rightarrow 2:

since isovol $w_{12} = 0$

and from SHV internal energies can be calculated using interpolation

$$u_1 = [(160 - 151.83)^\circ\text{C}] \cdot \frac{(2610.1 - 2560.8) \frac{\text{kJ}}{\text{kg}}}{(180 - 151.83)^\circ\text{C}} + 2560.8 \frac{\text{kJ}}{\text{kg}}$$

$$u_1 = 2575.1 \frac{\text{kJ}}{\text{kg}}$$

$$\therefore U_1 = (1.0 \text{ kg}) u_1 = 2575.1 \text{ kJ}$$

$$\text{also } v_1 = (1.0 \text{ kg}) v_1 = v_1 = \left\{ [(160 - 151.83)^\circ\text{C}] \cdot \frac{(0.40466 - 0.37484) \frac{\text{m}^3}{\text{kg}}}{(180 - 151.83)^\circ\text{C}} + 0.37484 \frac{\text{m}^3}{\text{kg}} \right\} (1.0 \text{ kg})$$

$$\approx 0.3835 \text{ m}^3$$

$$v_2 = v_1 \Leftrightarrow v_2 = v_1$$

so looking at SHV @ $p_2 = 10 \text{ bar}$, v_2

$$U_2 = (1.0 \text{ kg}) u_2 = (1.0 \text{ kg}) \left\{ [(0.3835 - 0.37295) \frac{\text{m}^3}{\text{kg}}] \cdot \frac{(3297.5 - 3193.3) \frac{\text{kJ}}{\text{kg}}}{(0.38347 - 0.37295) \frac{\text{m}^3}{\text{kg}}} + 3193.3 \frac{\text{kJ}}{\text{kg}} \right\}$$

$$\therefore U_2 = 3297.5 \text{ kJ}$$

$$\therefore Q_{12} = \Delta U_{12} = U_2 - U_1 = 3297.5 \text{ kJ} - 2575.1 \text{ kJ} = 722.4 \text{ kJ}$$

$$w_{12} = 0$$

$$Q_{12} = 722 \text{ kJ}$$

(II) PROCESS 2 \rightarrow 3

first find v_3 (@ $T_3 = 179.88^\circ\text{C}$ $p_3 = p_2 = 10 \text{ bar}$)

from saturation table $\rightarrow v_3 = 0.19436 \frac{\text{m}^3}{\text{kg}}$ $\therefore v_3 = 0.19436 \text{ m}^3$

then

$$w_{23} = \int_{v_2}^{v_3} p_2 dv = (10 \times 10^5 \text{ Pa}) (0.19436 - 0.3835) \text{ m}^3 = -189.140 \text{ kJ}$$

and using saturation table $u_3 = 2582.7 \frac{\text{kJ}}{\text{kg}} \Rightarrow U_3 = 2582.7 \text{ kJ}$

$$\therefore Q_{23} = \Delta U_{23} + w_{23} = (2582.7 - 3297.5) \text{ kJ} - 189.140 \text{ kJ}$$

$$= -900.94 \text{ kJ}$$

$$w_{23} = -189 \text{ kJ}$$

$$Q_{23} = -901 \text{ kJ}$$

(III) process 3 → 4

because isovol $W_{34} = 0$ and $V_4 = V_3$, $T_4 = 160^\circ$ from this we use SLTM to find u_4

$$\text{quality } x = \frac{v_4 - v_{f4}}{v_{g4} - v_{f4}} = \frac{0.19736 - 0.001102}{0.30678 - 0.001102} \approx 0.63223$$

thus,

$$\begin{aligned} u_4 &= (1-x)u_f + xu_g \\ &= 0.36777 \times 674.79 \frac{\text{kJ}}{\text{kg}} + 0.63223 \times 2567.8 \frac{\text{kJ}}{\text{kg}} \\ &\approx 1871.61 \frac{\text{kJ}}{\text{kg}} \end{aligned}$$

$$\therefore U_4 = 1871.61 \text{ kJ}$$

$$\therefore Q_{34} = \Delta U_{34} = U_4 - U_3 = (1871.61 - 2582.7) \text{ kJ} \approx -711.1 \text{ kJ}$$

$$W_{34} = 0$$

$$Q_{34} = -711 \text{ kJ}$$

(IV) Process 4 → 1

$$U_{41} = U_1 - U_4 = (2575.1 - 1871.61) \text{ kJ} \approx 703.5 \text{ kJ}$$

and because Q_{41} is given we know the work

$$Q_{41} = U_{41} + W_{41}$$

$$\therefore W_{41} = 815.8 - 703.5$$

$$\approx 112.3$$

$$W_{41} = 112 \text{ kJ}$$

↑
a bit off from

108 kJ

but for all calculations I
used scientific significant
figure operations.