# Optimization-based Real-time Operating Paradigms for Electric Arc Steelmaking

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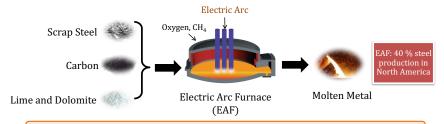
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#### Introduction



 $High\ energy\ intensive\ batch\ process, Low\ level\ of\ automation, Limited\ measurements$ 

#### **Objectives**

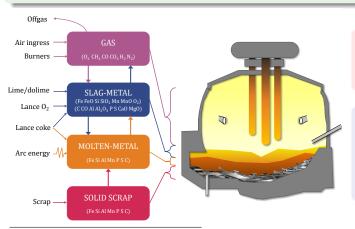
 Develop decision-support tool to determine economically optimal operating policies for EAF

#### **Approach**

- Develop dynamic model and rigorous optimization framework
- Collaborate with industrial partners for model validation, optimization problem formulation and in-plant evaluation

## Dynamic First Principles Model of EAF<sup>1</sup>

- Multi-zone System: Chemical equilibrium within slag-metal and gas zones (reactions limited by mass transfer)
- Mass and energy balances; diffusion and heat transfer relationships



Parameter estimation using plant data

Large scale DAE system: 28 differential & 518 algebraic variables

<sup>&</sup>lt;sup>1</sup>MacRosty, R. D. M. & Swartz, C. L. E. (2005). Ind.Eng.Chem.Res., 44, 8067-8083.

## Dynamic Optimization Application Paradigms

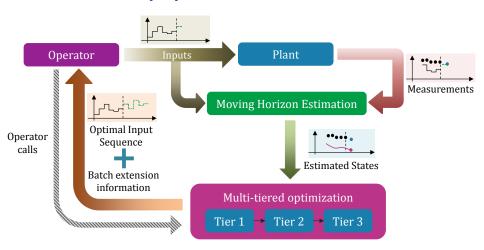


#### Key ingredients

- Dynamic model
- Dynamic optimization

- State estimation
- Novel initialization scheme

## Real-time Advisory System



- Model runs in parallel with the plant
- Multi-tiered optimization strategy handles end-point constraints

## Economics-based Dynamic Optimization Formulation

#### Objective function

$$\begin{split} \Phi(t_f) := c_0 M_{\text{steel}}(t_f) - \left( c_1 \int_{t_i}^{t_f} P dt + c_2 \int_{t_i}^{t_f} F_{CH_4, brnr} dt + c_3 \int_{t_i}^{t_f} F_{C_{lance}} dt \right. \\ + c_4 \int_{t_i}^{t_f} F_{C_{charge}} dt + c_5 \int_{t_i}^{t_f} (F_{O_2, Jetbox1} + F_{O_2, Jetbox2} + F_{O_2, Jetbox3}) dt \\ + c_6 \int_{t_i}^{t_f} F_{CaO} dt + c_7 \int_{t_i}^{t_f} F_{Dolomite} dt + c_8 \int_{t_i}^{t_f} (F_{1stCharge} + F_{2ndCharge}) dt \bigg) \end{split}$$

#### Constraints

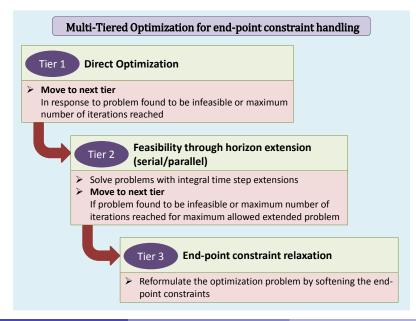
Model equations: 
$$\dot{\mathbf{x}}(t) = \mathbf{f}_{x}(\mathbf{x}(t), \mathbf{z}(t), \mathbf{u}(t)), \quad \mathbf{0} = \mathbf{f}_{z}(\mathbf{x}(t), \mathbf{z}(t), \mathbf{u}(t))$$
  
$$\mathbf{y}(t) = \mathbf{h}(\mathbf{x}(t), \mathbf{z}(t), \mathbf{u}(t))$$

Input constraints: 
$$P^{min}(t) \le P \le P^{max}(t)$$
,  $F_k^{min}(t) \le F_k \le F_k^{max}(t)$ 

Path constraints: 
$$T_{wall}(t) \leq T_{wall}^{max}$$
,  $T_{roof}(t) \leq T_{roof}^{max}$ 

End-point constraints: 
$$m_{ss}(t_f) \le \delta_{ss}$$
,  $y_{carbon}(t_f) \le Y_c^{max}$ 

## Multi-tiered Optimization



## Multi-rate MHE<sup>2,3</sup> (w/ Batch MHE)



$$\begin{aligned} \min_{\mathbf{x}_{i-N},\mathbf{w}_{k}} \ \sum_{k=i-N}^{i-1} & ||\mathbf{w}_{k}||_{Q^{-1}}^{2} + \sum_{k=i-N}^{i} & ||\mathbf{v}_{k}^{F}||_{(R^{F})^{-1}}^{2} \\ & + \sum_{k=i-N}^{i} & ||\mathbf{v}_{k}^{SF}||_{(R^{SF})^{-1}}^{2} + ||\mathbf{x}_{i-N} - \hat{\mathbf{x}}_{i-N}||_{S_{i}^{-1}}^{2} \\ & + \sum_{k=i-N}^{i} & ||\mathbf{v}_{k}^{SF}||_{(R^{SF})^{-1}}^{2} + ||\mathbf{x}_{i-N} - \hat{\mathbf{x}}_{i-N}||_{S_{i}^{-1}}^{2} \end{aligned}$$

Subject to: 
$$\mathbf{x}_{k+1} = \mathbf{f}(\mathbf{x}_k, \mathbf{u}_k) + \mathbf{w}_k,$$
  
 $\mathbf{y}_k^F = \mathbf{h}^F(\mathbf{x}_k) + \mathbf{v}_k^F, \quad k \in \mathbb{I}_F;$   
 $\mathbf{x}^{LB} \leq \mathbf{x}_k \leq \mathbf{x}^{UB}, \quad \mathbf{w}_k \in W$   
 $\mathbf{y}_k^{SF} = \mathbf{h}^{SF}(\mathbf{x}_k) + \mathbf{v}_k^{SF}, \quad k \in \mathbb{I}_{SF}$ 

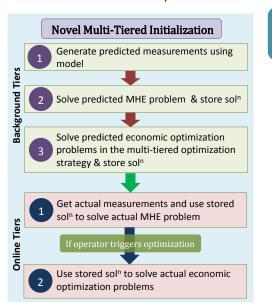
Tuning matrices:

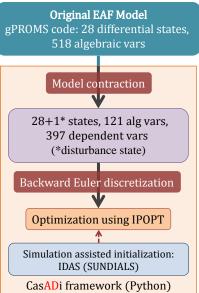
$$Q, R \text{ and } S_i \ \left( S_{i+1} = Q + A_i [S_i - S_i C_i^T (R + C_i S_i C_i^T)^{-1} C_i S_i] A_i^{-1} \right)$$

<sup>&</sup>lt;sup>2</sup>Rao, C.V., Rawlings, J.B. and Lee, J.H., (2001). Automatica, 37(10), 1619-1628.

<sup>&</sup>lt;sup>3</sup>Lopez-Negrete R. and Biegler, L.T., (2012). Journal of Process Control, 22(4), 677-688

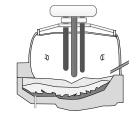
## Initialization and implementation





## Case Study 1

- Length of batch process: 60 minutes
- Estimation horizon: 6 min
- Advisory system's ability demonstrated in presence of
  - ► Plant-model mismatch
  - Unknown initial conditions of states
  - ► Measurement noise
- Structure of slow and fast measurements:



Time (min)	042	43	44 46	47	4860
Number of measured variables	6	13	6	8	6

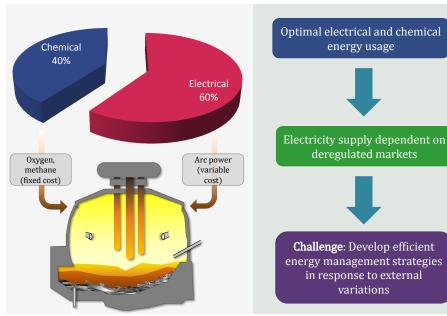
Off-gas compositions (CO, CO <sub>2</sub> , O <sub>2</sub> , H <sub>2</sub> ), $T_{roof}$ , $T_{wall}$	Every 1 min
Slag compositions (FeO, Al <sub>2</sub> O <sub>3</sub> , SiO <sub>2</sub> , MgO, CaO)	t=43 min
Molten-metal temperature and carbon content	t=43 & 47 min

## Case Study 1 Results

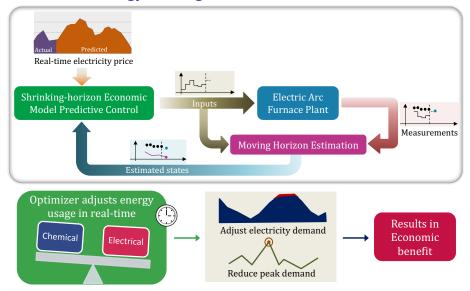
	Scenario 1	Scenario 2	Scenario 3	Scenario 4	
Times at which advisory system was called (min)	0	0,30	0, 30, 40	0, 30, 40, 50, 58	
Number of re- optimizations	0	1	2	4	
Economic objective function value (\$)	9,100	9,360	9,484	9,585	
Actual scrap left at 60th minute (kg)	2.8	2.5	2.3	1.0	

- Scenario 4 has 5.3% more profit compared to scenario 1.
- End point target achieved without extension when more reoptimizations carried out

## Energy Management for Electric Arc Furnace



## Real-Time Energy Management



Key idea: Offset high price electricity with chemical energy

#### **Economic Model Predictive Control**

## Objective function (with time varying cost coefficients)

$$\max_{\mathbf{u}(t)} c_{0}M_{steel}(t_{f}) - \left( \int_{t_{i}}^{t_{f}} c_{1}(t)Pdt + c_{2} \int_{t_{i}}^{t_{f}} F_{CH_{4},brnr}dt + c_{3} \int_{t_{i}}^{t_{f}} (F_{O_{2},Jetbox1} + F_{O_{2},Jetbox2} + F_{O_{2},Jetbox3})dt \right)$$

#### Constraints

Model equations

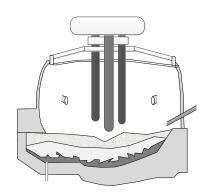
Input constraints:

$$P^{min}(t) \le P \le P^{max}(t), \quad F_k^{min}(t) \le F_k \le F_k^{max}(t)$$

u: P (Electrical arc power),  $F_k$  (Flow rates of natural gas and oxygen)

## Case Study 2

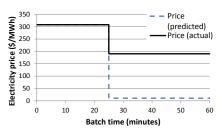
- Realistic electricity price data considered
- Real-Time market (price change every 1 hour)
- Ontario wholesale market



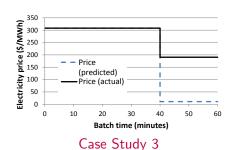
#### Compare two closed loop results:

- NMPC<sup>nominal</sup>: Price profile not updated and forecast price continued to be used even after the change occurs
- NMPC<sup>update</sup>: Price profile updated to reflect actual price obtained from wholesale market

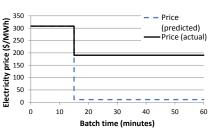
#### Price Profiles for Case Studies



Case Study 1



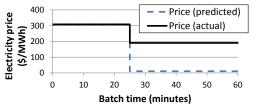
Case Study 2



Case Study 4

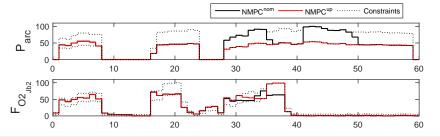
## Case Study 2

#### Peak price decrease with price change at 25th minute



## Compare NMPC<sup>update</sup> & NMPC<sup>nominal</sup>:

Profit increase	4.6%
Decrease in electricity use	23%
Increase in other input use	1.6%
Reduction in peak electricity demand	45%



Average CPU time to solve (sec): 2.6 (novel initialization), 11.2 (nominal)

#### Conclusions and Future Work

- Introduced real-time dynamic optimization-based advisory system
- Real-time energy management strategy to reduce energy requirements
  - ▶ Optimal energy use while exploiting changing electricity price
- Case studies demonstrate major economic benefit for both the application paradigms

Average Solve Time



#### Current and Future Work

- Variable batch length problem
  - Explore possibility of contraction in batch duration
- Real-time energy management strategy for 5 and 15 minute market
  - Construct NMPC problem to minimize the peak demand

### **Acknowledgments**



MCMASTER STEEL RESEARCH CENTRE



