**ANSYS Fluent Rotating Machinery Modeling** 

**Workshop 02.1: Pump Simulation** 

Release 2020 R2



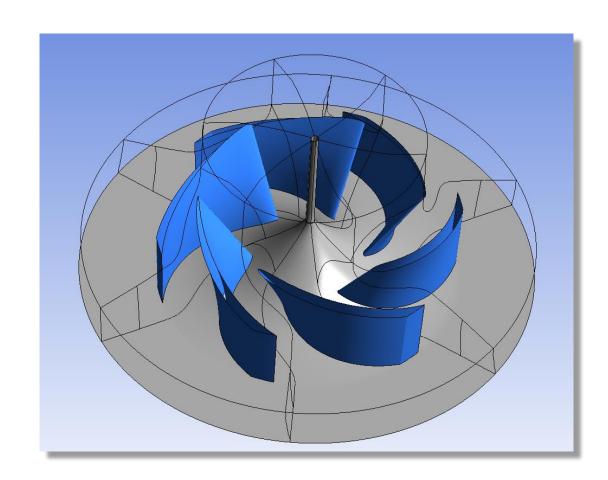
## Introduction

#### Workshop Description:

- This Workshop deals with the Fluent setup and solution for a pump impeller

#### Learning Aims:

- Setting up a single rotating component
  - Defining a rotating frame
  - Applying rotational periodicity
- Solving and monitoring convergence
- Visualizing the pressure distribution on the impeller walls





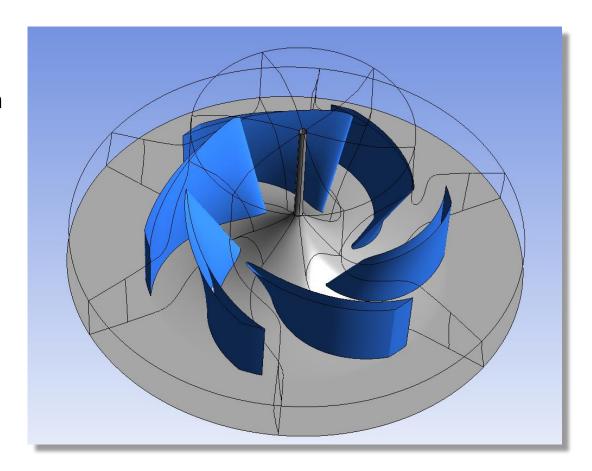
## Pump Model

#### Single rotating component

- A moving reference frame is used to solve rotating components
- As all blades are identical, we can reduce the problem size by modelling a single blade passage with periodic boundaries

#### Pump data

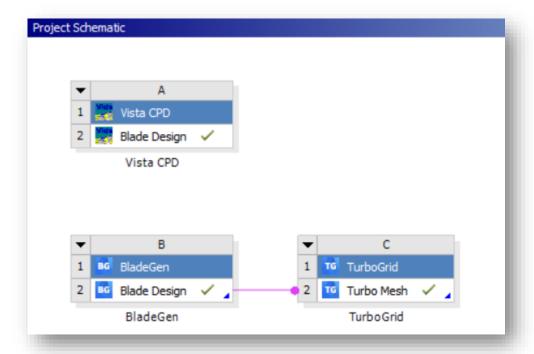
- Fluid = Water
- Speed = 2000 rpm
- Number of Blades = 6
- Flow Rate = 83.76 kg/s
  - Flow Rate for one passage = 83.76/6 kg/s= 13.96 kg/s
- Axis or rotation = z-axis





## Load Workbench Project

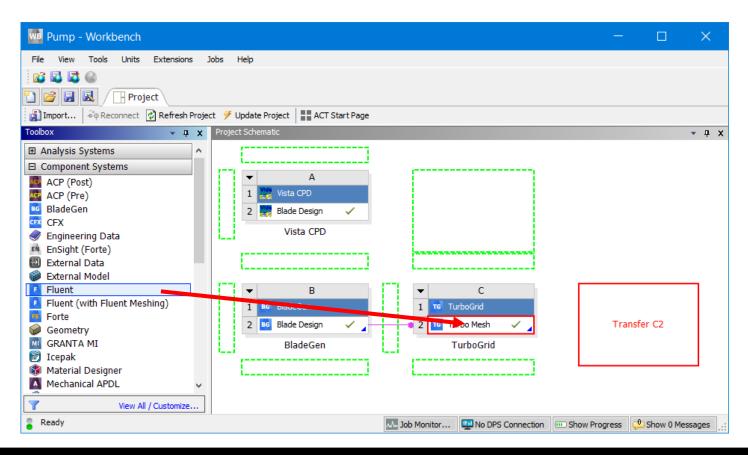
- The geometry has been created using Vista CPD and the mesh has been created using TurboGrid
- The geometry and mesh for the pump are provided in a Workbench archive
- Open Workbench
- In the Workbench main menu File > Open...
  - In the *Open* dialogue box *Browse to Pump\_mesh.wbpz* provided with the workshop inputs and click *Open*
  - In the Save As dialogue box edit the File Name to Pump.wbpj and click Save





## Create a Fluent Component

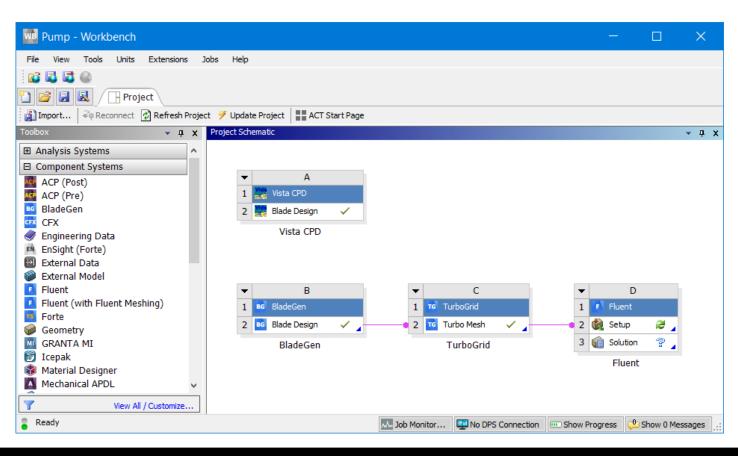
- Add a Fluent Component to Project Schematic
  - Find Fluent under Component Systems
  - Drag Fluent and drop it to cell C2 to transfer the TurboGrid mesh automatically to Fluent





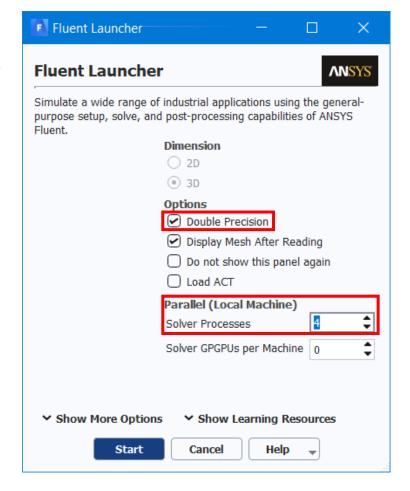
## Launch Fluent

• Double click on the *Setup* cell *D2* to launch Fluent



## Launch Fluent

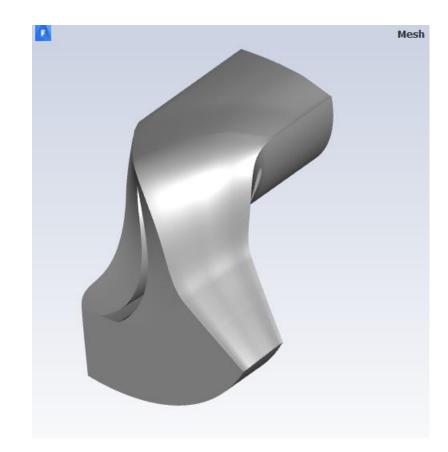
- In the Fluent Launcher select Double Precision
  - Double Precision is recommended in most turbomachinery simulations due to the usual high aspect ratios in the boundary layer (order 1000 and more...)
  - The Maximum Aspect Ratio for the given mesh is 1.18539e+03 (see next slide)
- Set the number of Processes for Parallel to 4
  - The mesh size for this case is approximately 250,000 cells (see next slide)
  - If you have enough Parallel licenses and more than 4 cores available, you may set up to 12 Processes (so that each Processor is solving for not less than 20,000 cells)

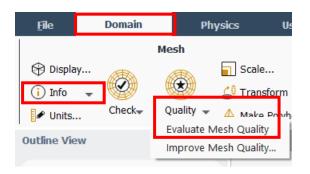




# Fluent

- In the Fluent window, you should see the single passage geometry of the pump as shown on the right
- The mesh corresponds to a 60-degrees sector of the complete domain
- It is always a good practice to check the mesh size and the mesh quality in the Mesh group of the Domain tab
  - Info > Size will give you the number of cells in the Fluent Console, which is approximately 250,000
  - Quality > Evaluate Mesh Quality will show you
     a Maximum Aspect Ratio of 1.18539e+03
    - This justifies the choice of starting Fluent in Double Precision



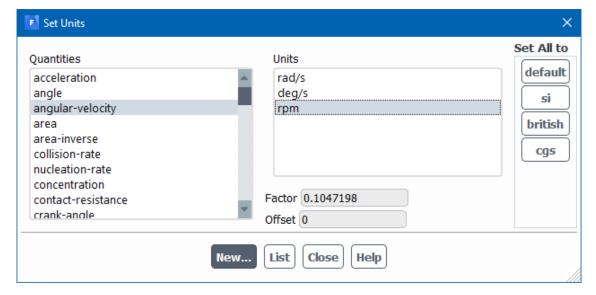




## General Settings

- The pump rotational speed is given in rpm
- Set the units for angular velocity to rpm
- Click Close



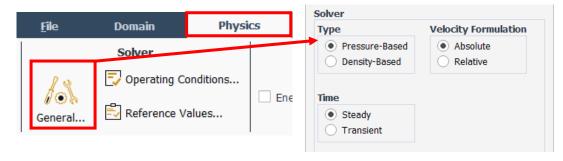




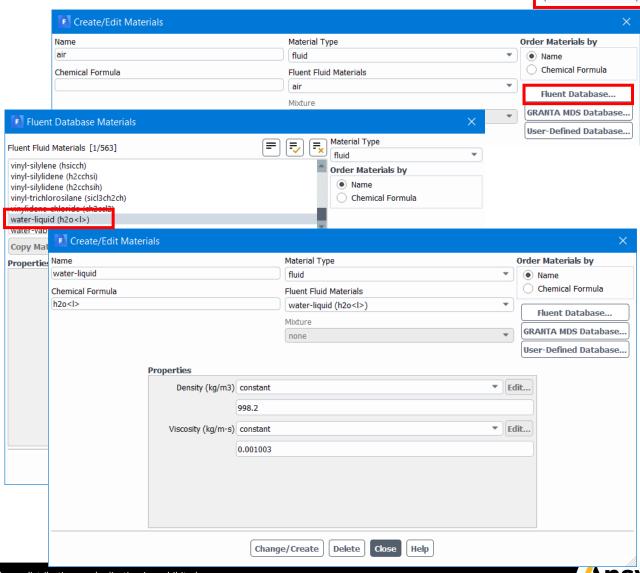
#### Physics: General Solver and Materials



 Retain the default solver settings of Pressure-Based solver with Absolute Velocity Formulation



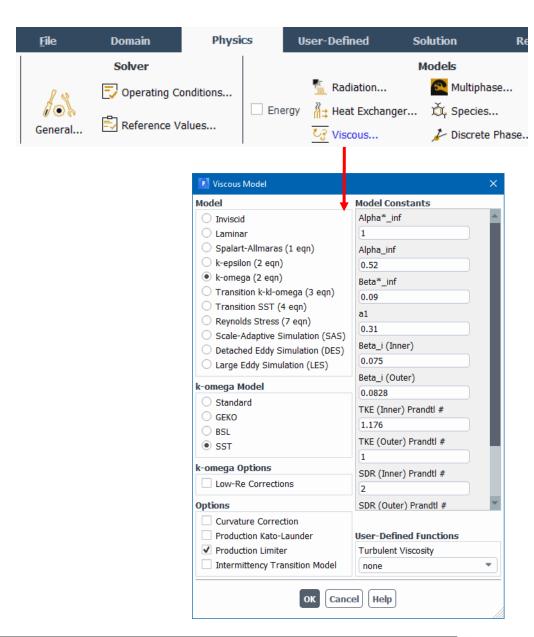
- Make Water material available:
  - From the *Fluent Database...* select water-liquid(h2o<l>) and click *Copy* and *Close*
  - Click *Change/Create* and close the *Create/Edit Materials* dialog box.





## Physics: Turbulence Model

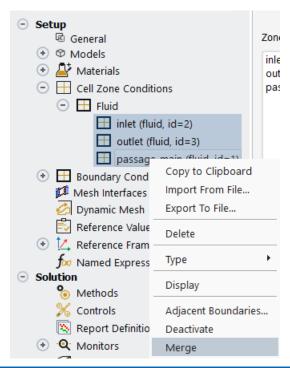
- Keep the default SST komega Viscous Model
- The SST k-omega model (default Viscous Model starting with 2020 R1) is the recommended turbulence model for turbomachinery simulations

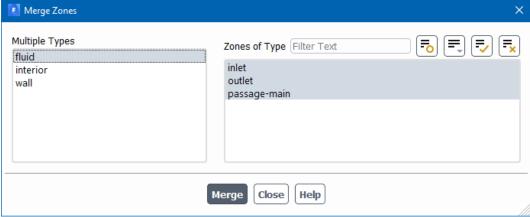




## Merge the 3 Cell Zones

- In the *Outline View* expand *Cell Zone Conditions* and then *Fluid* 
  - You can see three zones: *inlet, outlet,* and *passage-main*
  - These names were automatically created in Turbogrid
- Merge the three fluid zones into a single zone
  - Select all 3 zones (holding down Ctrl) and RMB > Merge
- You can see in the Outline View that now only a singe zone is present, inlet
- Rename it to impeller
  - *RMB* on the *inlet* cell zone in the *Outline*, *select Edit*, type in the new name and click *Apply*

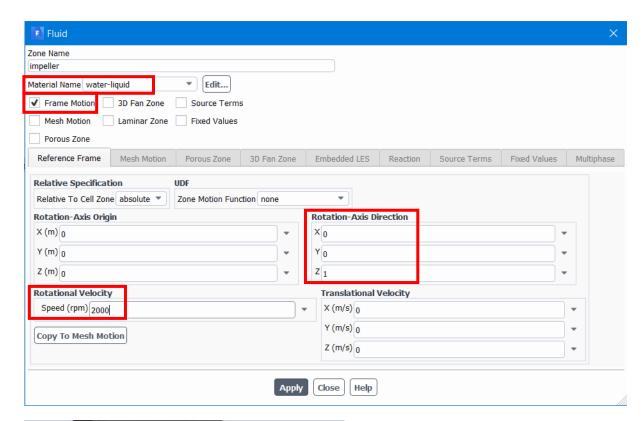


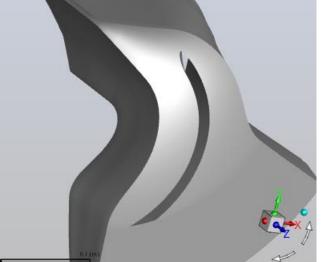




## **Physics: Cell Zone Conditions**

- Edit the *impeller* cell zone
  - Select water-liquid as Material Name
  - Enable Frame Motion
  - The default *Rotation-Axis Direction* is the z-axis and is suitable for this case
  - Set *Rotational Velocity* to 2000 (rpm)
    - Sign verification: If you place your right thumb to point as the z-axis, your fingers are curling (in this case) to the same direction with the rotation direction of the pump blade. Therefore, the Rotational Velocity was set to a positive number

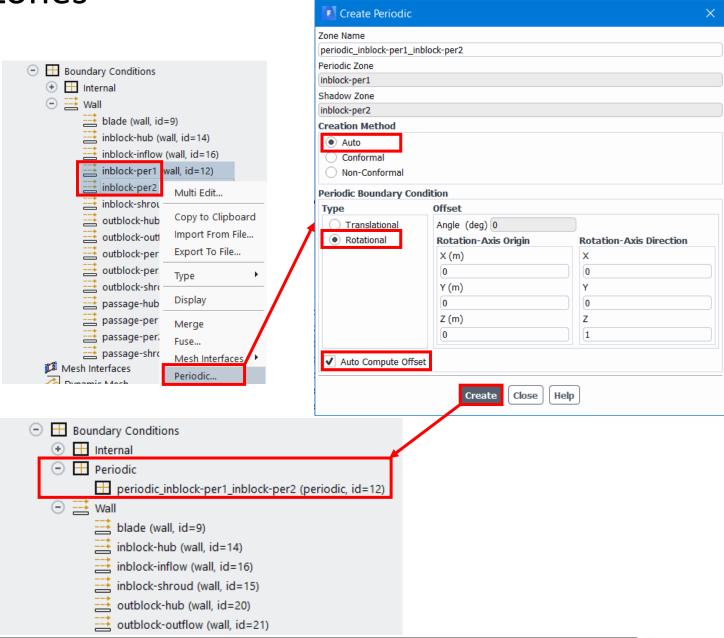






#### **Create Rotational Periodic Zones**

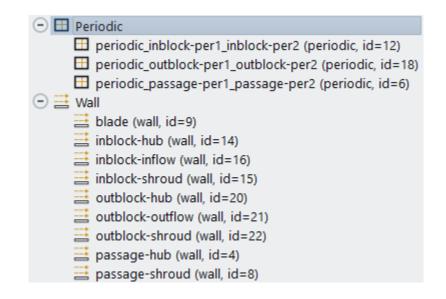
- In the *Outline View* expand the *Wall* branch
- Select inblock-per1 and inbloc-per2
  - Use *Ctrl* + *RMB* for multiple selections
- RMB > Periodic
- Select Rotational and leave all the rest to default values
  - Note that the Rotation-Axis Direction is set to the one defined in the cell zone Frame Motion
  - It is important to always first define the axis of rotation in the cell-zone conditions before creating the Rotational Periodic boundaries
  - Look for Console message:
     Zone 17 deleted
     Created a conformal periodic boundary.
- The periodic pair is placed under the newly created *Periodic* branch in the *Outline*





# Create Rotational Periodic Zones (2)

- In the same way Create Rotational Periodic Zones for:
- outblock-per1 and outblock-per2
- passage-per1 and passage-per2
  - This interface will fail using Auto Compute Offset
    - Error: Auto computation of Rotational Offset is not successful, please enter Angle.
  - Do a mesh check-
    - Remember, always do a mesh check after creating rotational periodic boundaries
    - This will give you a summary of all Periodic zones including the rotation angle and the axis of rotation
    - The two successfully created periodic zones show a rotation angle of -60.000 degrees
  - Manually give an offset of -60.000 degrees for this periodic boundary

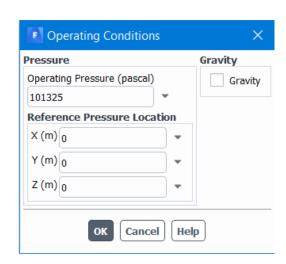


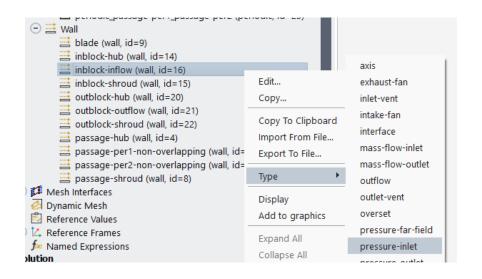


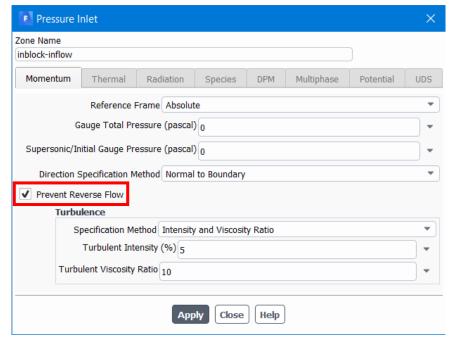
## Boundary Conditions: Inlet

- Set the boundary conditions for inblock-inflow zone
  - RMB on inblock-inflow and set Type to pressure-inlet
  - Check Prevent Reverse Flow
  - We will use a Gauge Total Pressure of 0 (pascal) at the inlet (default value)
  - Accept all remaining defaults and click Apply

Note for Operating Pressure:
This is an incompressible flow case. Therefore, the
Operating Pressure may be
left to the default value of
101325 (pascal) and the
Gauge Total Pressure at the
inlet is given as 0 (pascal)



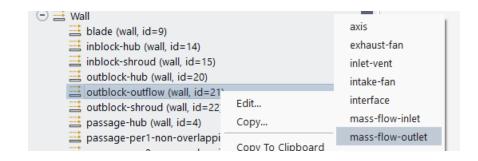


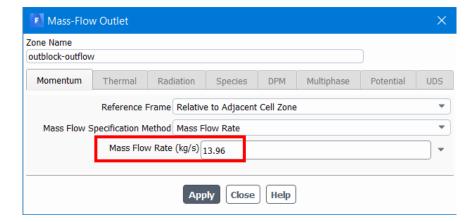




# **Boundary Conditions: Outlet**

- Set the boundary conditions for outblock-outflow zone
  - RMB on outblock-outflow and set Type to mass-flow-outlet
  - Set Mass Flow Rate = 13.96 (kg/s)
    - This value corresponds to the mass flow rate for one passaged and was given in slide 3



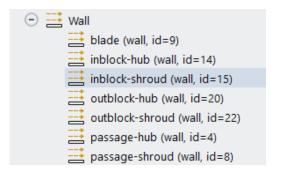


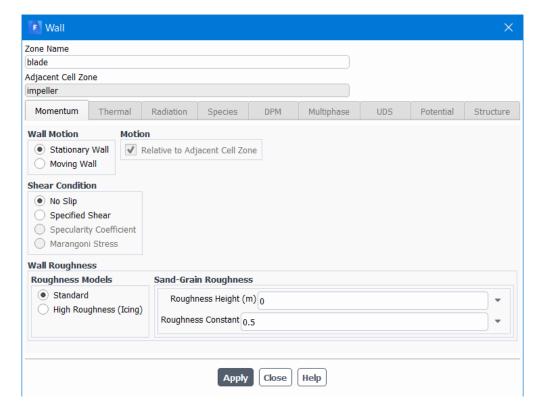


#### **Boundary Conditions: Walls**

- The remaining zones under Wall in the Outline View correspond to walls which are stationary in the Moving Reference Frame of the impeller cellzone
- Edit the boundary condition for *blade*
- The default settings of a No Slip, Stationary Wall, Relative to Adjacent Cell Zone is what we want No need to change this default setting for any of the walls for this case

Note: In some cases a wall in a rotating zone can be stationary in the absolute frame. Example, the shroud casing wall of an unshrouded impeller. Such a wall is seen as a "counter-rotating wall" in the reference frame of the rotating zone. You will learn how to set up such walls in a next workshop

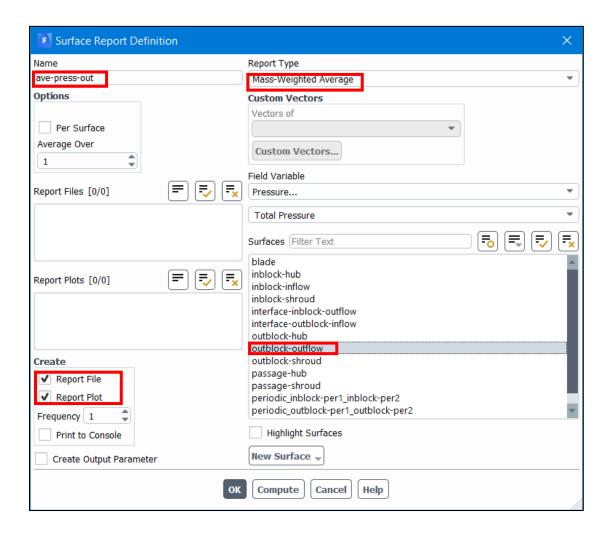






# Solution: Report Definition

- In the Solution tab create a new Mass-Weighted Average Surface Report Definition with the following settings:
  - Name = ave-press-out
  - Field Variable = Total Pressure
  - Surfaces = outblock-outflow
  - Report File = checked
  - Report Plot = checked

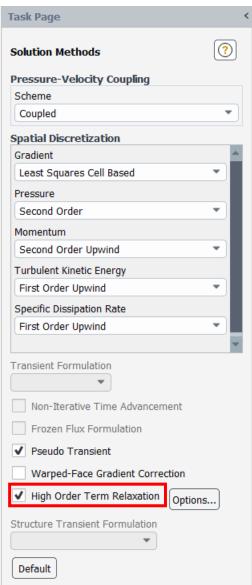




## Solution: Solution Methods

- Always use the default Coupled "Pseudo-Transient" Solver
  - If for any reason the Solution method is set to some *Scheme* other than *Coupled*, click the *Default* button at the bottom of the panel
- Turn on High Order Term Relaxation (more stable)

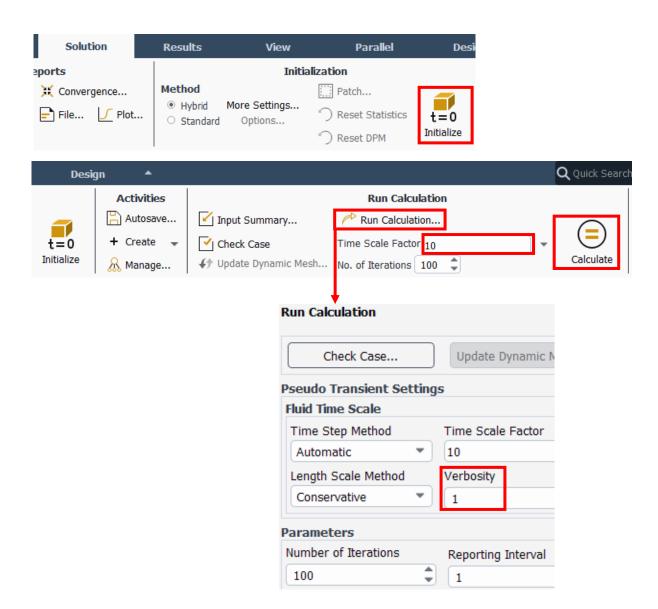






## Solution: Initialize Solution and Run the Solver

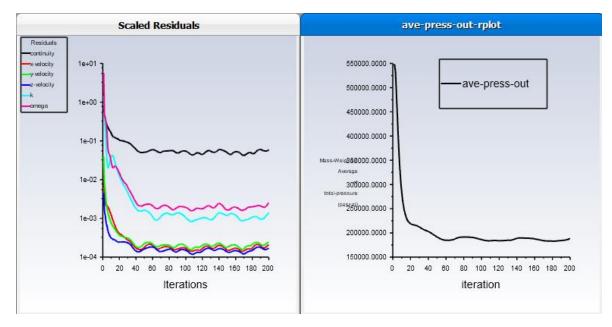
- Perform a default *Hybrid Initialization* 
  - This works fine for this case. A best practice initialization procedure will be used in the next workshops of this course
- Click on Run Calculation...
  - Set *Verbosity* to 1
    - This will produce a more detailed runtime solver output, including the time step used by the pseudo-transient solver
- Set Time Scale Factor to 10
- Set *No. of Iterations* to 100
- Click Calculate
- Click OK in any Warning popup about Mesh and settings have changed

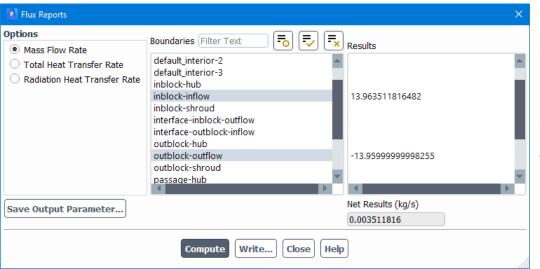




## Solver Convergence

- As the solution progresses we can see that the residuals reduce somewhat; however the case ends after 100 iterations with the residuals and the report plot for average outlet pressure showing a bouncy behaviour
- Running 100 iterations further the convergence behavior is similar
- The mass Flow Rate Flux report shows an imbalance of 0.025 %
- This case is not well converged
- In workshop 03.1 "Pump Analysis using CFD-Post" we will examine why this is happening using CFD-Post



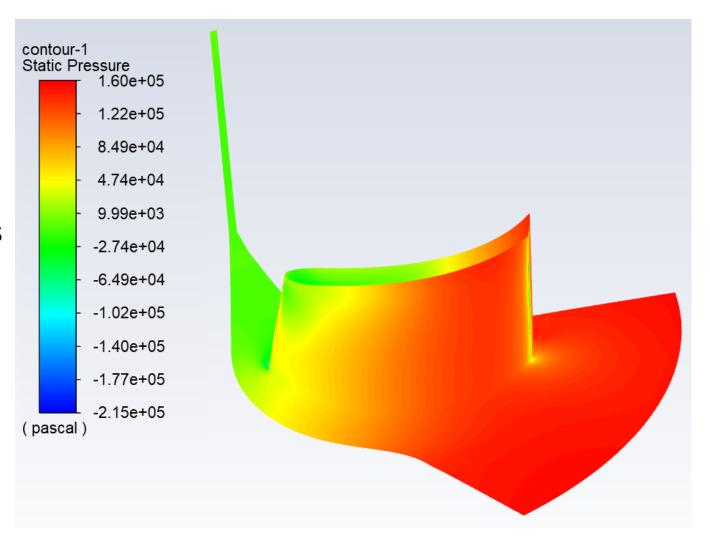


Note: Residuals and monitor plots may differ between two computers or Ansys releases



#### **Results: Pressure Contours**

- Create a contour plot on the blade and hub walls
- The pressure increases through the impeller passage, as expected
- Additional post-processing of this case will be carried out in workshop 03
- When done, save the Workbench project and exit Fluent





## Summary

- This workshop has covered:
  - Setting up a single rotating component
    - Defining a rotating frame
    - Applying rotational periodicity
  - Solving and monitoring convergence
  - Visualizing the pressure distribution on the impeller walls





**End of presentation** 

