

Formuleo Turbomáquinas

Patricio Whittingslow — 55423

Ecuaciones 1 (Termodinámica) *Ecuaciones Cardinales:* $T ds = dh - v dp \parallel T ds = du + p dv$

Ecuaciones 2 (Modelo gas ideal) *Gas Ideales:* $\tilde{R} = 8,314[J/mol/K] \parallel \tilde{R} = \bar{M}R, \bar{M}[kg/mol] \parallel pV = mRT \parallel pv = RT \parallel pV = N\tilde{R}T \parallel a = \sqrt{\gamma \bar{R} T} \parallel T_0 = T \left(1 + \frac{k-1}{2} M^2\right) \parallel p_0 = p \left(1 + \frac{k-1}{2} M^2\right)^{\frac{k}{k-1}} \parallel \rho_0 = \rho \left(1 + \frac{k-1}{2} M^2\right)^{\frac{1}{k-1}}$

Procesos incompresibles: $s_2 - s_1 = \int_{T_1}^{T_2} \frac{c_v(T)}{T} dT$

Procesos compresibles isoentropicos: $\frac{T_2}{T_1} = \left(\frac{p_2}{p_1}\right)^{\frac{k-1}{k}} = \left(\frac{v_1}{v_2}\right)^{k-1} \parallel \left(\frac{T_2}{T_1}\right)^{\frac{k}{k-1}} = \frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^k \parallel \left(\frac{T_1}{T_2}\right)^{\frac{1}{k-1}} = \left(\frac{p_1}{p_2}\right)^{\frac{1}{k}} = \frac{v_2}{v_1}$

Procesos compresibles isoentropicos: $p_0 = cte = p + \frac{1}{2} \rho c^2 \parallel h_0 = h + \frac{1}{2} c^2$

Gas perfecto: $h = c_p T; c_p = kR/(k-1) \rightarrow T_0 = T + \frac{1}{2} c^2 / c_p \parallel s_x^0 = s_x - s_0 = \int_{T_0}^{T_x} \frac{c_p}{T} dT \rightarrow s_2 - s_1 = c_p \ln \frac{T_2}{T_1} - R \ln \frac{p_2}{p_1}$

Ecuaciones 3 (Fundamentales de turbomáquinas) $\frac{\dot{W}}{\dot{m}} = U_1 c_{\theta 1} - U_2 c_{\theta 2} = \left(\frac{w_2^2 - w_1^2}{2}\right) + \left(\frac{c_1^2 - c_2^2}{2}\right) + \left(\frac{U_1^2 - U_2^2}{2}\right) \parallel$

$\eta_{tob} = \frac{\text{Energía cinética actual de salida}}{\text{Energía cinética si el proceso fuera reversible}} = \frac{1 - T_2/T_{01}}{1 - T_{2s}/T_{01}} = \frac{\frac{1}{2} c_2^2}{\frac{1}{2} c_{2s}^2} = K_{tob}^2 \parallel \eta_{dif} = \frac{h_{2s} - h_1}{h_2 - h_1} = \frac{c_1^2 - c_{2s}^2}{c_1^2 - c_2^2} = \frac{(p_2/p_1)^{(k-1)/k} - 1}{[(p_{01}/p_{02})(p_2/p_1)]^{(k-1)/k} - 1}$

\parallel **Grado de reacción:** $R = \frac{\text{Salto entálpico en rotor}}{\text{Salto entálpico total en etapa (rotor + estator)}} = \frac{\Delta h_{rotor}}{\Delta h_{etapa}} \parallel$ **Maq. Hidraulicas:** $R = \frac{p_3 - p_2}{p_3 - p_1} \parallel$ **Pelton:** $F_x = \rho A (c - u)^2 (1 - \cos \theta) \parallel \eta_{generadora} = \frac{h_{02s} - h_{01}}{h_{02} - h_{01}} = \frac{\text{Trabajo adiabatico mínimo por seg.}}{\text{Trabajo adiabatico hecho por seg.}} \parallel$ **Turbinas:** $\eta_{motora} = \frac{h_{02} - h_{01}}{h_{02s} - h_{01}}$

Ecuaciones 4 (Centrifugos) *Adimensionalizacion dinámica:* $\pi_1 = \frac{p_{02}}{p_{01}}, \pi_2 = \dot{m} \frac{\sqrt{RT_{01}}}{D^2 P_{01}}, \pi_3 = \frac{\Omega}{\sqrt{RT_{01}}}, \pi_4 = \eta_{iso} \parallel \tan \beta_1 = \frac{c_{a1}}{U_1}$

$\parallel \xi = \frac{c_{\theta d}}{c_{\theta}} = \frac{c_{\theta} - u_d}{c_{\theta}} \parallel D_{eddy} \simeq \frac{\pi D_2 \cos \beta_2}{Z} \parallel \frac{\dot{W}_d}{\dot{m}} = e_d = h_{02} - h_{01} = c_{\theta 2} U_2 - c_{\theta 1} U_1 = (\xi c_{\theta 2}) U_2 - c_{\theta 1} U_1 \parallel \frac{p_{03}}{p_{01}} = \left(\frac{T_{03s}}{T_{01}}\right)^{\frac{k}{k-1}} = \left[1 + \frac{\eta_{iso} (\xi c_{\theta 2} U_2 - c_{\theta 1} U_1)}{c_p T_{01}}\right]^{\frac{k}{k-1}} \parallel T_{03} - T_{01} = \frac{\xi c_{\theta 2} U_2 - c_{\theta 1} U_1}{c_p} \parallel M_1 = \frac{c_{a1}}{a} = \frac{c_{a1}}{\sqrt{kRT_1}} \parallel M_2 = \frac{c_{2d}}{\sqrt{\gamma kRT_2}} \parallel$ **Coef. Lift:** $C_L = \frac{L}{\frac{1}{2} \rho c^2 b t}; t$ es cuerda, b es long. de perfil

Ecuaciones 5 (Axiales) $\nu = \frac{r_{ext}}{r_{base}} \parallel \frac{\dot{W}}{\dot{m}} = U c_a (\cos \beta_2 - \cos \beta_1) \parallel$ **Isoentropico:** $h_3 - h_1 = \frac{p_3 - p_1}{\rho} = U (c_{\theta 3} - c_{\theta 1}) \parallel$

$\mu = \frac{\Delta T_{real}}{\Delta T_{euler}} \quad \text{tal que} \quad \dot{W}_{real} = \mu \dot{W} \parallel \frac{p_{03}}{p_{01}} = \left[1 + \frac{\eta_{iso} \mu U c_a (\tan \beta_1 - \tan \beta_2)}{c_p T_{01}}\right]^{\frac{k}{k-1}} \parallel R = \frac{h_2 - h_1}{h_3 - h_1} \rightarrow \rho = cte \Rightarrow R = \frac{p_3}{p_1}$

Ecuaciones 6 (Alternativos) $\varepsilon_{vol} = 1 - C(r_c^{\frac{1}{n}} - 1) = \frac{V_1 - V_4}{V_1 - V_3} \parallel r_{cmáx} = (1 + C^{-1})^n \parallel \varepsilon_{term} = T_{asp}/T_{int} \parallel \varepsilon_{pca} = \frac{P_{asp}}{P_{int}}$

$\parallel \varepsilon_{fugas} = \frac{1}{1+f} \parallel \eta_{vol} = \prod_i \varepsilon_i \parallel \dot{V} = \pi r^2 L_{carr} f_{hz} X \eta_{vol} \parallel \dot{m} = \frac{p \dot{V}}{Z_e R} \parallel p_{int} = p_e \frac{A_p}{A_v} - \frac{kx}{A_v} - \Delta p$

Ecuaciones 7 (Refrigeración) *Sin refrigeración:* $\dot{W}_{ad/rev} = \dot{m} \left[\frac{k}{k-1} R (T_{out} - T_{in}) \right] \parallel$

Refrig. intermedia: $\dot{W}_{pol/rev} = \dot{m} \left\{ \frac{n}{n-1} T_{in} R \left[\left(\frac{p_{out}}{p_{in}} \right)^{\frac{n-1}{n}} - 1 \right] \right\} \parallel$ *Refrig. máxima:* $\dot{W}_{isot/rev} = \dot{m} R T_{in} \ln \left(\frac{p_{out}}{p_{in}} \right)$

Ecuaciones 8 (TdC) *Ecuación de calor:* $\nabla^2 T + \dot{q}_G = \rho c \frac{\partial T}{\partial t} \parallel q_k = -k \cdot A \frac{\Delta T}{\Delta x} \parallel$ *cilindricas:* $q_k = 2\pi L k \frac{\Delta T}{\ln \frac{r_o}{r_i}} \parallel$ *esféricas:* $q_k =$

$\left(\frac{\Delta T}{\frac{r_o - r_i}{4\pi k r_o r_i}} \right) \parallel$ *Resistencias:* $R_k = \frac{L}{kA}, \text{ cilindro: } R_k = \frac{\ln \frac{r_o}{r_i}}{2\pi L k}, \text{ esfera: } R_k = \left(\frac{r_o - r_i}{4\pi k r_o r_i} \right) \parallel$ *Aletas:* $\eta = \frac{q}{q_{max}} = \frac{q}{h P L \Delta T_{b\infty}} \parallel$

$\alpha = \frac{k}{\rho c_p} \parallel$ *Modelo resistencia despreciable:* $\frac{\Delta T_{t\infty}}{\Delta T_{0\infty}} = e^{BiFo} \parallel$ *Radiación:* $q_r = \sigma T^4 \parallel q_{r1 \leftarrow 2} = A_1 \mathcal{F}_{1,2} \sigma T^4; \mathcal{F}_{1,2} = f(\epsilon_2, \alpha_1, \text{forma})$

$\parallel \rho + \alpha + \epsilon = 1 \parallel$ *Wien:* $\lambda_{máx} T = 2,8976 \times 10^{-3} \parallel r_{crit} = \frac{k}{h}$

Ecuaciones 9 (Adimensionales) $Re = \frac{UL}{\nu} = \frac{\rho UL}{\mu} \parallel Nu = \frac{\tilde{h}_e L}{k_{fluido}} = \frac{\text{conveccion}}{\text{conduccion en fluido}}$

$Pr = \frac{\mu c_p}{k} = \frac{\nu}{\alpha} = \frac{\text{difusion cantidad cantidad movimiento}}{\text{difusion calor}} \parallel Bi = \frac{h \cdot L_c}{k} = \frac{R_k}{R_c} \parallel Fo = \frac{\alpha t}{L^2} \parallel Gr = \frac{g \beta (T_s - T_{\infty}) L^3}{\nu^2} = \frac{\text{conveccion natural}}{\text{conveccion viscosa}}$

Ecuaciones 10 (Correlaciones TdC) Correlaciones conveccion interna: $Turb: Nu_D = 0.023 Re_D^{4/5} Pr^n \rightarrow n = 0,4 \text{ heating}, n = 0,3 \text{ cooling} \parallel Lam: q'' = cte, Nu_D = 4,36 \rightarrow T_s = cte, Nu_D = 3,66 \parallel D_H = \frac{4 \cdot Seccion}{Perimetro \text{ mojado}}$
"Integrables" Capa Límite: $Re_{crit} \approx 5 \times 10^5$, $Laminar: Nu_x = \frac{h_x x}{k} = 0,332 Re_x^{1/2} Pr^{1/3} \parallel Turbulento: Nu_x = 0,0288 Pr^{1/3} Re_x^{0,8}$
 $\parallel Velocidad Altas Mach \gtrsim 1 T^* = T_\infty + 0,5(T_s - T_\infty) + 0,22(T_{as} - T_\infty)$ donde $T_{as}^{lam} = T_\infty + Pr^{1/2}(T_0 - T_\infty)$
 $T_{as}^{turb} = T_\infty + Pr^{1/3}(T_0 - T_\infty)$ *Hi-speed laminar:* $St_x^* = \left(\frac{h_{cx}}{c_p \rho U_\infty} \right)^* = 0,332 (Re_x^*)^{-1/2} (Pr^*)^{-2/3}$, *Hi-speed* $10^5 < Re_x^* < 10^7$:
 $St_x^* = 0,0288 (Re_x^*)^{-1/5} (Pr^*)^{-2/3} \parallel HiHi-speed 10^7 < Re_x^* < 10^9$: $St_x^* = \frac{2,46}{(\ln Re_x^*)^{2,584}} (Pr^*)^{-2/3}$

Ecuaciones 11 (Intercambiadores) $U = \frac{1}{\sum_i \frac{1}{R_i}} = \frac{1}{\frac{1}{h_1} + \frac{t_1}{k} + \frac{1}{h_2} + \dots}$ $\parallel balance: \dot{U}_{VC} = \dot{W} = 0 \Rightarrow \dot{Q} = \dot{m} \Delta h = \rho u_\infty A c_p (T_2 - T_1)$
 $\parallel \dot{Q} = U A \cdot LMTD \parallel LMTD = \frac{\Delta T_A - \Delta T_B}{\ln \left(\frac{\Delta T_A}{\Delta T_B} \right)} \parallel \Delta T_B = T^{fluido1} \big|_{x=B} - T^{fluido2} \big|_{x=B} \parallel \beta_i = \frac{\dot{m}_i c_{p_i}}{U \ell_{i \text{ perimetro}}}$
 $(T_2 - T_1)|_x = (T_2 - T_1)|_{x=0} e^{-\left(\frac{1}{\beta_1} + \frac{1}{\beta_2}\right)x} \parallel T_1 = \text{efectividad: } \epsilon = \frac{T_{h,i} - T_{h,o}}{T_{h,i} - T_{c,i}}$

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Ecuaciones 12 (Fundamentalismos) *Euler:* $-\frac{\dot{W}}{\dot{m}} = \tau \cdot \Omega = -e = U_2 c_{\theta 2} - U_1 c_{\theta 1} = (h_{02} - h_{01}) = \left(\frac{c_2^2 - c_1^2}{2} \right) + \left(\frac{U_2^2 - U_1^2}{2} \right) + \left(\frac{w_1^2 - w_2^2}{2} \right)$
Primera Ley: $\dot{U} = \dot{Q} - \dot{W} - \dot{m} [(h_2 - h_1) + \frac{1}{2} (c_2^2 - c_1^2) + g(z_2 - z_1)]$ *Rend. de la instalación:* $\frac{\text{Potencia efectiva}}{\text{Potencia entregada a la instalación}}$
Ley de Coseno: $c^2 = a^2 + b^2 - 2ab \cos \theta_{\hat{a}\hat{b}}$

Ecuaciones 13 (T. Hidráulicas) *Pelton:* aprox $Dixon w_2 \approx U \rightarrow c_2 \approx 2U \sin \frac{\beta_2}{2}$ donde $\beta_2 = 180^\circ - \vartheta_2$ $\eta_h^{pelton} = \frac{U(c_1 - c_{\theta 2})}{gH}$
Kaplan: $c_{a1} = c_{a2} = \frac{Q}{\pi(r_{ext}^2 - r_{int}^2)} \parallel \eta_h^{kaplan} = \frac{\dot{W}/\dot{m}}{gH}$
Eficiencia Hidráulica = $\frac{\text{Potencia entregada al rotor}}{\text{Potencia que se puede entregar a la instalación (potencial)}}$

Ecuaciones 14 (T. de Vapor) *Trabajo:* $de = \frac{1}{\rho} dp + d\frac{1}{2}c^2 + dq \parallel Tobera: \eta_{iso}^{tobera} = \frac{c_2^2/2}{c_1^2/2}; K_f = \frac{c_1}{c_{1s}} \parallel Rotor: dp = 0: \eta_{iso}^{rotor} = \frac{\dot{W}/\dot{m}}{c_1^2/2}$ con $K_m = \frac{w_2}{w_1} \parallel$ *Eficiencia interna de etapa:* $\eta_i = \eta_{iso}^{tobera} \cdot \eta_{iso}^{rotor} \cdot \dots = \frac{\dot{W}/\dot{m}}{\Delta h_s}$ *Eficiencia maxima:* $\frac{U}{c_1} = \frac{\cos \alpha_1}{2m \cdot (1-R)}$
Escalonamiento de reacción. Fijo: $c_{2s} = \sqrt{2\Delta h_s(1-R)} + c_1^2$ *Movil:* $w_{2s} = \sqrt{2\Delta h_s R} + w_1^2$ donde $K_m = \frac{w_2}{w_{2s}}$
Perdidas tobera: $Y_{tob.} = \dot{m}(c_{1s}^2/2 - c_1^2/2)$ *Perdidas movil:* $Y_m = \dot{m}(w_1^2/2 - w_{2s}^2/2)$ *Perdidas roz. entre fijo/movil:* $k_{axial} = 0,009$
 $k_{radial} = 0,027: Y_{roz.} = k \rho n_{Hz}^3 D_m^5 [W] \parallel$ *Perdidas ventil. ε es grado adm. l es largo alabes en cm, D_m es diametro medio y k depende del nro. de ruedas* $k_1 = 3,8; k_2 = 4,5; k_3 = 6 \rightarrow Y_{vent.} = (1 - \varepsilon) k \rho n^3 D_m^4 l [W]$. donde $\varepsilon = \frac{\text{Long arco inyeccion}}{\text{circunferencia media (U/omega)}}$
donde $\ell_a = \frac{\dot{m}}{\rho h c_0}$ para una ÚNICA tobera cuadrada $A = \ell_a \cdot h$
Etapas acción: $c_0 \approx 0$ para tobera. *Rend. Maximo de UNA etapa accion (c₁ salida tobera):* $\eta_{m\acute{a}x} = \frac{\dot{W}/\dot{m}}{c_{1s}^2/2} = K_f^2 \cdot \frac{\cos^2(\alpha_1)}{2} \cdot (1 + K_m \frac{\cos \beta_1}{\cos \beta_2})$

Ecuaciones 15 (T.Gas) Valores: $c_{p \text{ comb}} \approx 1,15 [kJ/kg]; k_{comb.} \approx 1,33; \eta_{comb} = \frac{FAC_t}{FAC_c}$
Relacion de compresion (Segun Hilal): $r_c = \frac{p_2}{p_1}$ *Potencia eff donde w = Δh*
 $\dot{W}_e = (\dot{m}_{air} + \dot{m}_{comb.}) \cdot |w_{turb.}| - \dot{m}_{air} \cdot |w_{comp.}|$ donde $w_t = h_{in} - h_{out} = c_{p \text{ cte}}(T_{in} - T_{out})$
Eficiencias Internas: $\eta_{int}^{turb.} = \frac{\text{Potencia ciclo indicado}}{\text{Potencia ciclo ideal}} = \frac{\Delta h_s}{\Delta h_s}$ *Efic. mecánicas(al revés para bombas):* $\eta_m^{turb.} = \frac{\text{Potencia entregada}}{\text{Potencia indicada}} = \frac{w_t}{w_t^{ind}}$
Optimo ζ: $r_c^* = \left(\frac{T_3}{T_1} \eta_c \eta_t \frac{c_{34}}{c_{12}} \right)^{\left(\frac{k}{2(k-1)} \right)}$ *Regeneración:* $\sigma = \frac{T_A - T_2}{T_4 - T_2}, \zeta = \frac{T_2}{T_1}, \vartheta = \frac{T_3}{T_1}, \eta_{regen} = \frac{\zeta - 1}{\vartheta - \zeta - \sigma \frac{\vartheta - \zeta}{\sigma}} \parallel$ *Poder Calorico del combustible (PCI) [J/kg]* *Consumo específico* $C_e = \frac{\dot{m}_{comb.}}{P_e} \rightarrow \eta_{instalacion} = \frac{\dot{W}_e}{\dot{m}_{comb.} \cdot PCI} = \frac{1}{C_e \cdot PCI}$

Ecuaciones 16 (Ciclo combinado) *Rankine:* $\eta = \frac{\dot{W}_t/\dot{m} - \dot{W}_b/\dot{m}}{\dot{Q}_{in}/\dot{m}} = \frac{|\Delta h_{turb.}| - |\Delta h_{bomba}|}{\Delta h_{cald}} = 1 - \frac{|\Delta h_{cond.}|}{\Delta h_{cald}} \parallel BWR = \frac{\dot{W}_b/\dot{m}}{\dot{W}_t/\dot{m}} = \frac{\Delta h_{bomba}}{|\Delta h_{turb.}|}$
 \parallel *Turb/bomba (b al revés):* $\eta_t = \frac{\Delta h_{turb}}{(\Delta h_{turb.})_s}$ 