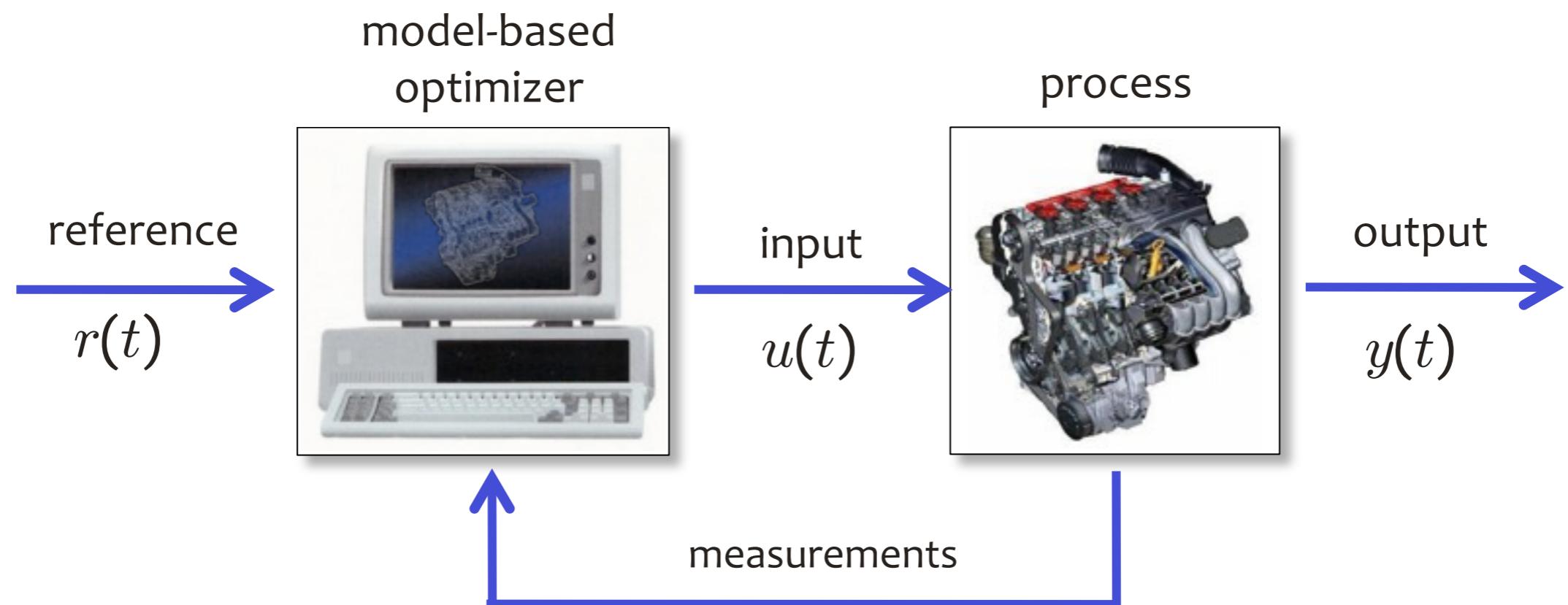


Model Predictive Control: Basic Concepts

Model Predictive Control (MPC)

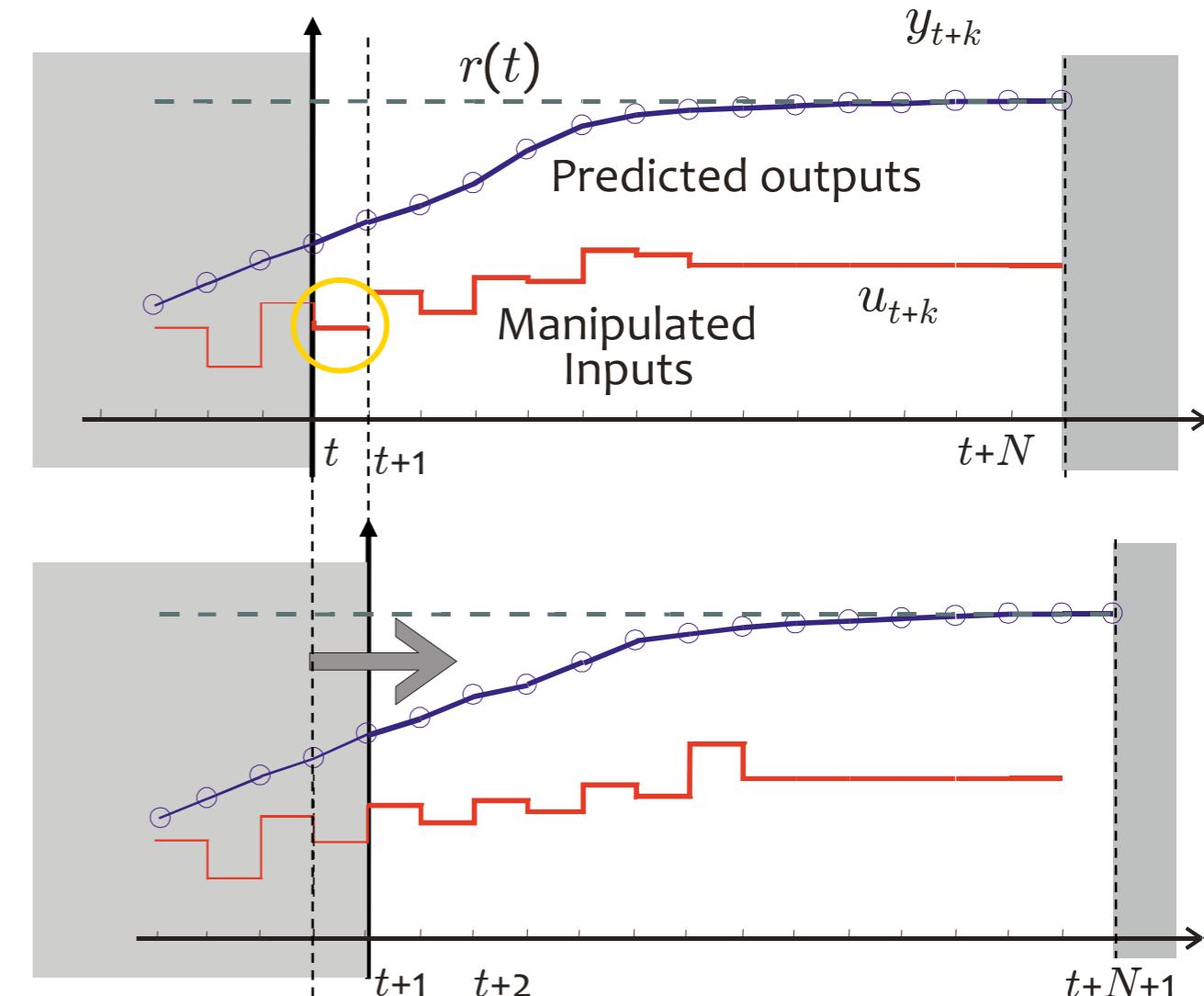


A **model** of the process is used to **predict** the future evolution of the process to optimize the **control** signal

Receding horizon philosophy

- At time t : solve an **optimal control** problem over a finite future horizon of N steps:

$$\begin{aligned} \min_{u_t, \dots, u_{t+N-1}} \quad & \left\{ \sum_{k=0}^{N-1} \|y_{t+k} - r(t)\|^2 + \right. \\ & \left. \rho \|u_{t+k} - u_r(t)\|^2 \right\} \\ \text{s.t.} \quad & x_{t+k+1} = f(x_{t+k}, u_{t+k}) \\ & y_{t+k} = g(x_{t+k}, u_{t+k}) \\ & u_{\min} \leq u_{t+k} \leq u_{\max} \\ & y_{\min} \leq y_{t+k} \leq y_{\max} \\ & x_t = x(t), \quad k = 0, \dots, N-1 \end{aligned}$$

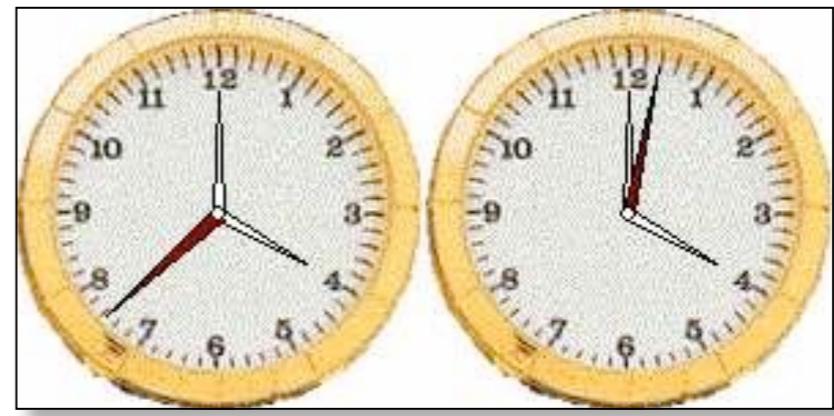
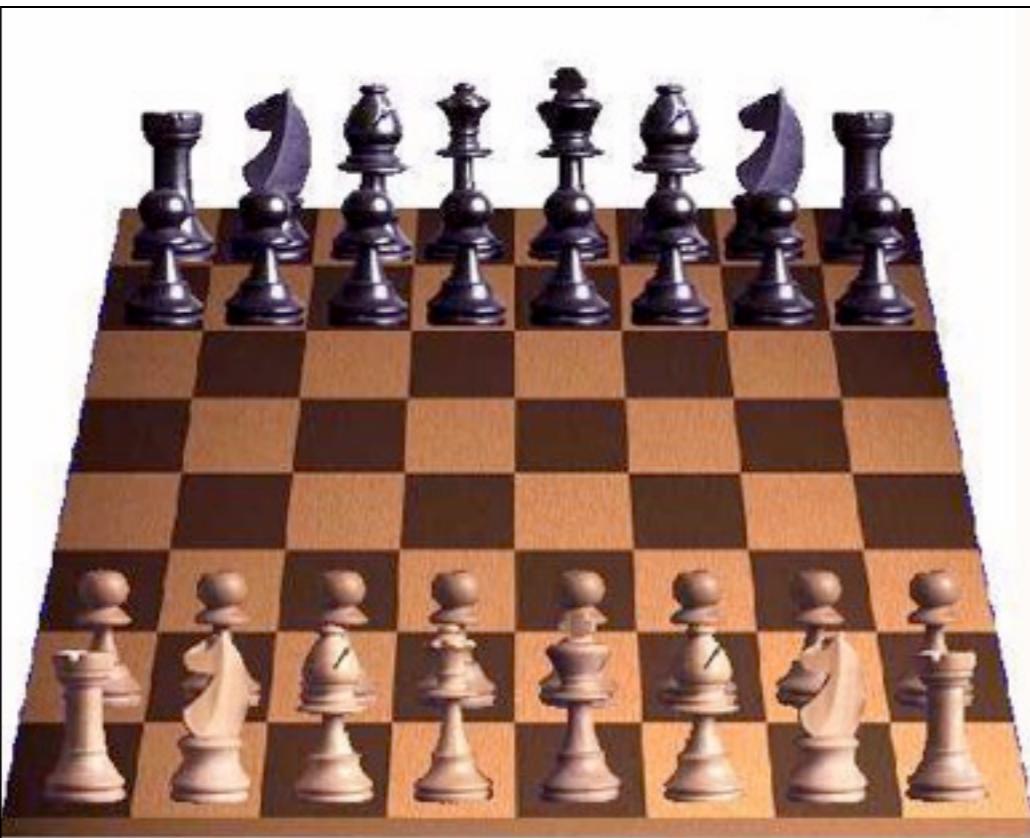


- Only apply the first optimal move $u^*(t)$
- At time $t+1$: Get new measurements, repeat the optimization. And so on ...

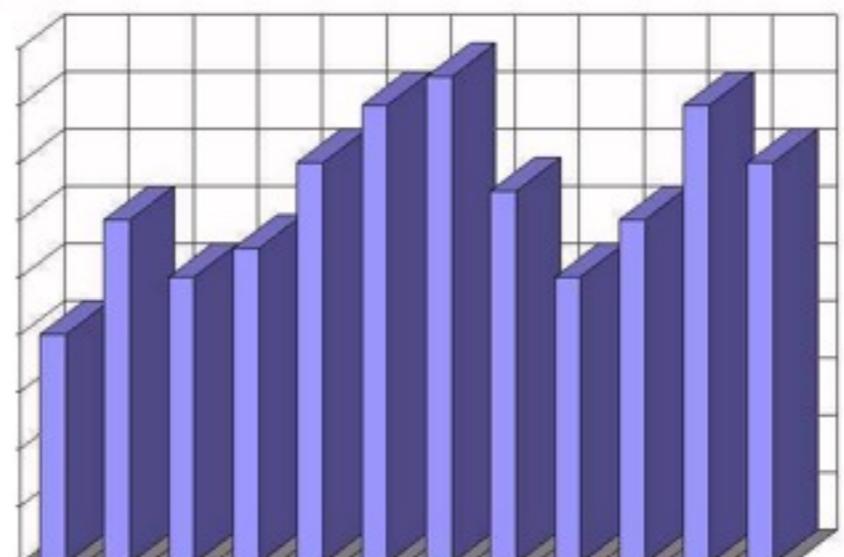
Advantage of repeated on-line optimization: **FEEDBACK!**

Receding Horizon - Examples

- MPC is like **playing chess** !



- “Rolling horizon” policies are also used frequently **in finance**



Receding Horizon - Examples

- prediction model how vehicle moves on the map

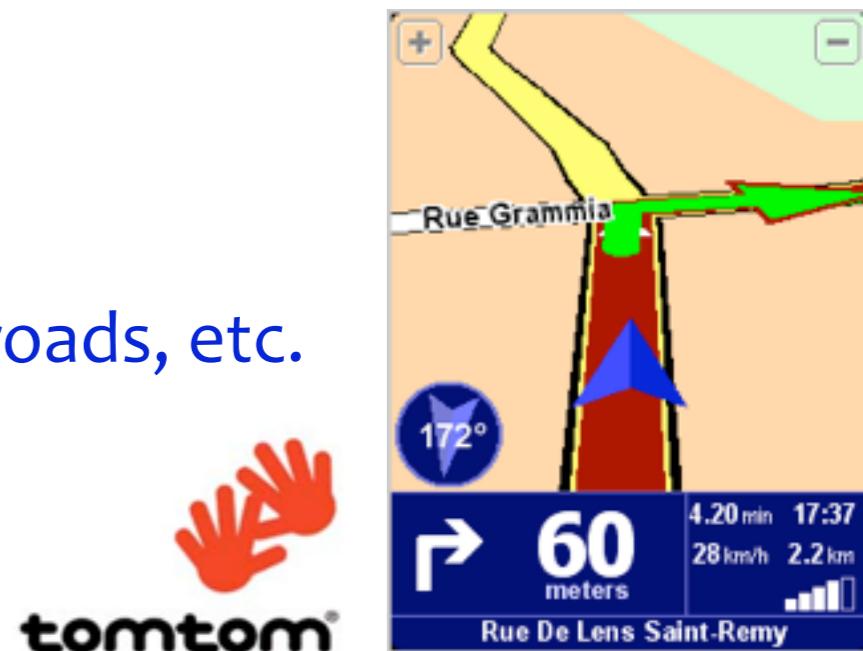
- constraints drive on roads, respect one-way roads, etc.

- disturbances mainly driver's inattention !

- set point desired location

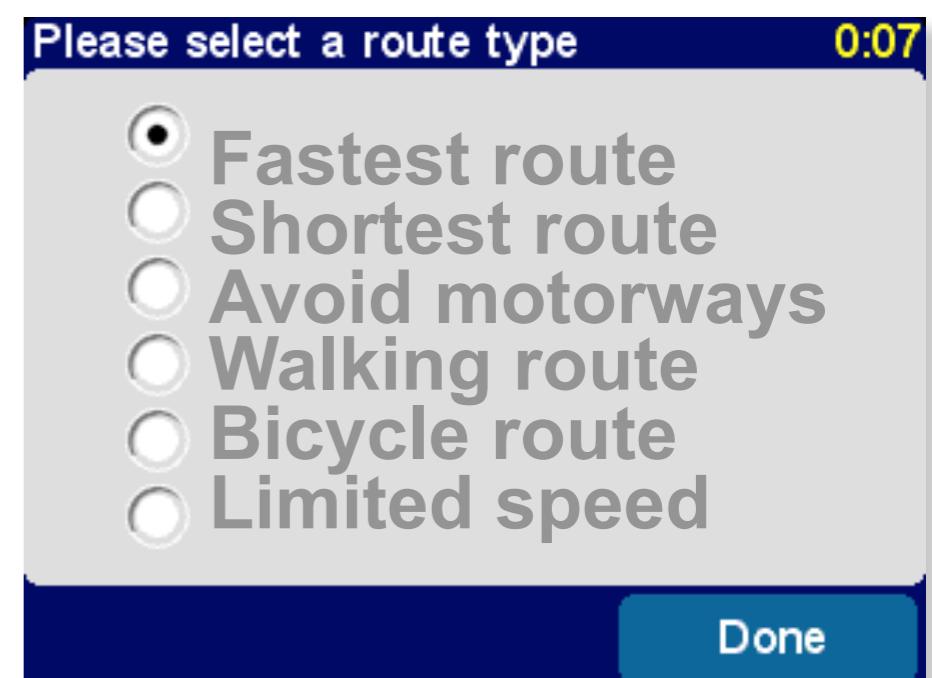
- cost function minimum time,
minimum distance, etc.

- receding horizon mechanism
event-based
(optimal route re-planned when path is lost)



x = GPS position

u = navigation commands



Good Models for (MPC) Control

Note: computational **complexity** and theoretical properties (e.g. stability) depend on chosen model/objective/constraints

Good models for MPC:

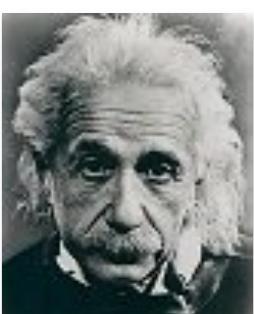
- **Descriptive** enough to capture the most significant dynamics of the system



- **Simple** enough for solving the optimization problem

“Make everything as simple as possible, but not simpler.”

— Albert Einstein



MPC in Industry

- History: Computer control (“Manual” MPC)



Fluid catalytic cracking
(courtesy of Shell / M. Morari)

Fluid catalytic cracking (FCC) is the most important conversion process used in petroleum refineries. It is widely used to convert the high-boiling hydrocarbon fractions of petroleum crude oils to more valuable gasoline, olefinic gases and other products

(http://en.wikipedia.org/wiki/Catalytic_cracking)

MPC in Industry

- History: 1979 Dynamic Matrix Control (DMC) by Shell
(Motivation: multivariable, constrained)

- Present Industrial Practice

- linear impulse/step response models
- sum of squared errors objective function
- executed in supervisory mode

- Particularly suited for problems with

- many inputs and outputs
- constraints on inputs, outputs, states
- varying objectives and limits on variables
(e.g. because of faults)

DMCplus™



New Generation Controller

DMCplus is the “new generation” multivariable control product devel-

The new GUI-based system makes DMCplus easy to use.

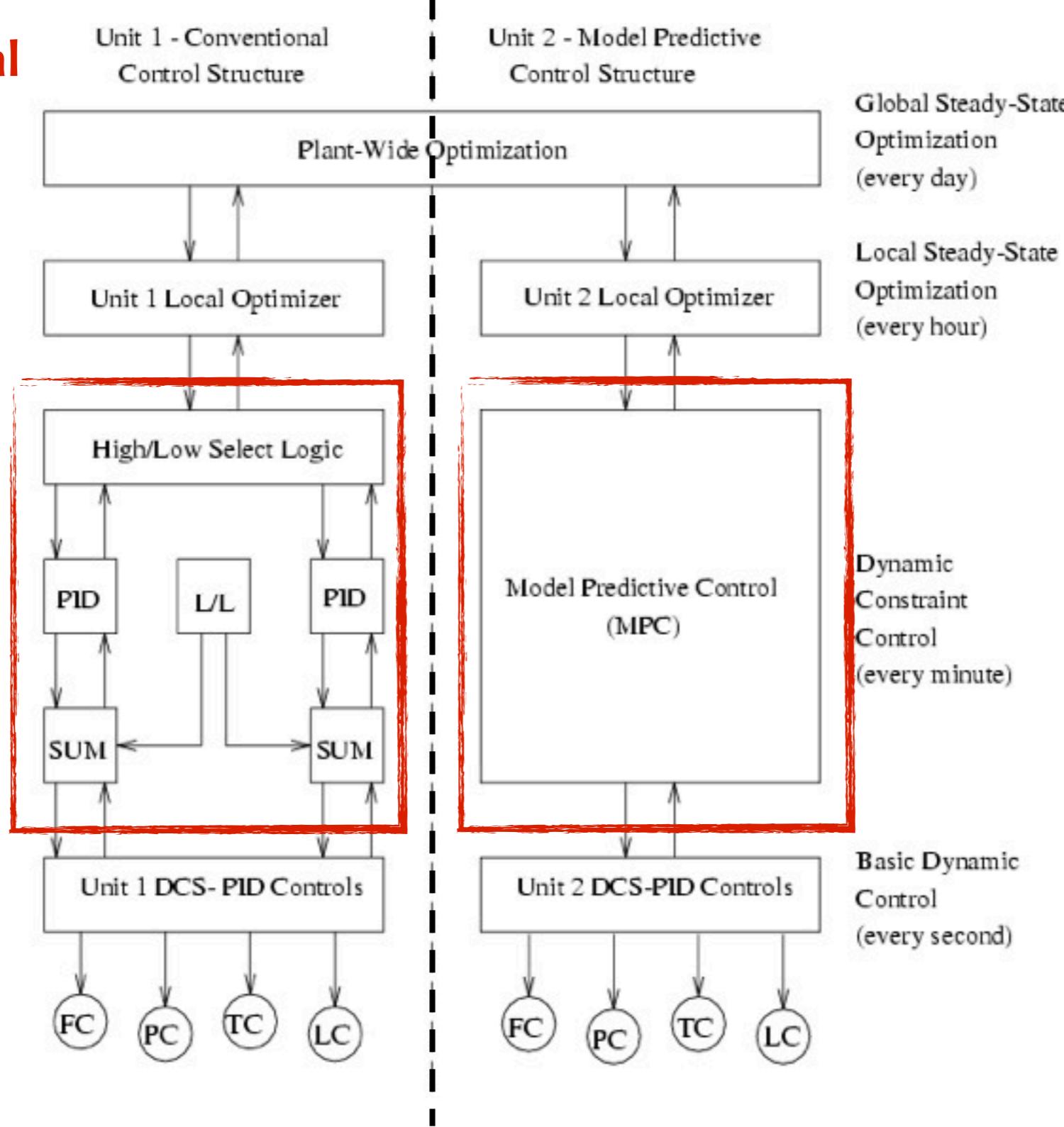
AspenTech's installed base of model predictive control represents over 50% of the world's applications.

optimization technology and thus also for AspenTech's plant-wide optimiza-

MPC in Industry

Hierarchy of control system functions:

Conventional



MPC

(Qin, Badgwell, 1997)

MPC in Industry

Area	Aspen Technology	Honeywell Hi-Spec	Adersa ^b	Invensys	SGS ^c	Total
Refining	1200	480	280	25		1985
Petrochemicals	450	80	—	20		550
Chemicals	100	20	3	21		144
Pulp and paper	18	50	—	—		68
Air & Gas	—	10	—	—		10
Utility	—	10	—	4		14
Mining/Metallurgy	8	6	7	16		37
Food Processing	—	—	41	10		51
Polymer	17	—	—	—		17
Furnaces	—	—	42	3		45
Aerospace/Defense	—	—	13	—		13
Automotive	—	—	7	—		7
Unclassified	40	40	1045	26	450	1601
Total	1833	696	1438	125	450	4542
First App.	DMC:1985 IDCOM-M:1987 OPC:1987	PCT:1984 RMPCT:1991	IDCOM:1973 HIECON:1986	1984	1985	
Largest App.	603 × 283	225 × 85	—	31 × 12	—	

(snapshot survey conducted in mid-1999)

(Qin, Badgewell, 2003)

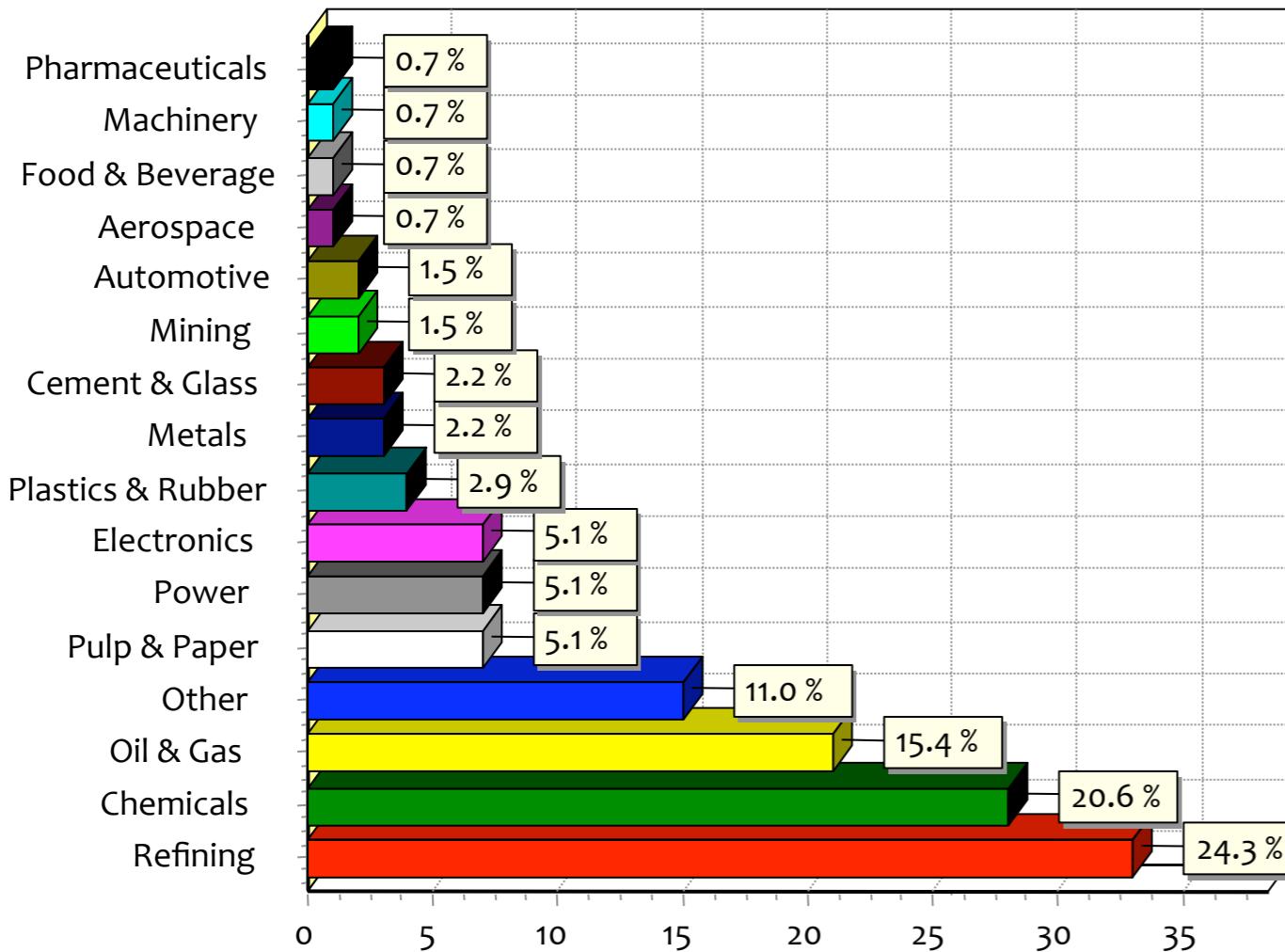
“For us multivariable control is predictive control ”

Tariq Samad, Honeywell (IEEE Control System Society, President) (1997)

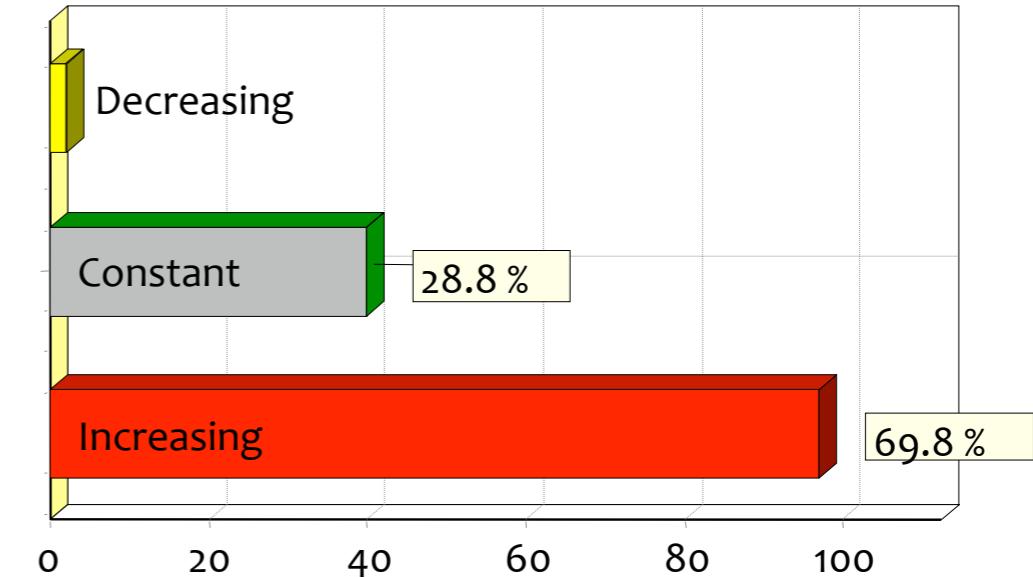
MPC in Industry

Results from a recent survey (November 7, 2005) about the use of MPC techniques / real-time optimization in a set of US industries:

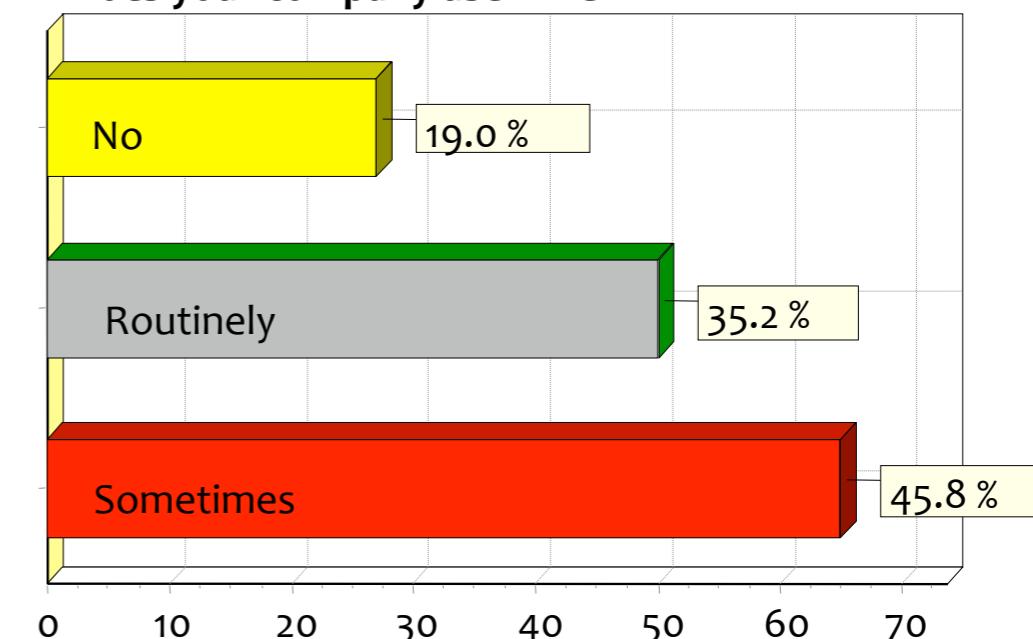
Industrial area of respondents to the survey:



Do you see your use of MPC accelerating, staying constant, or declining?

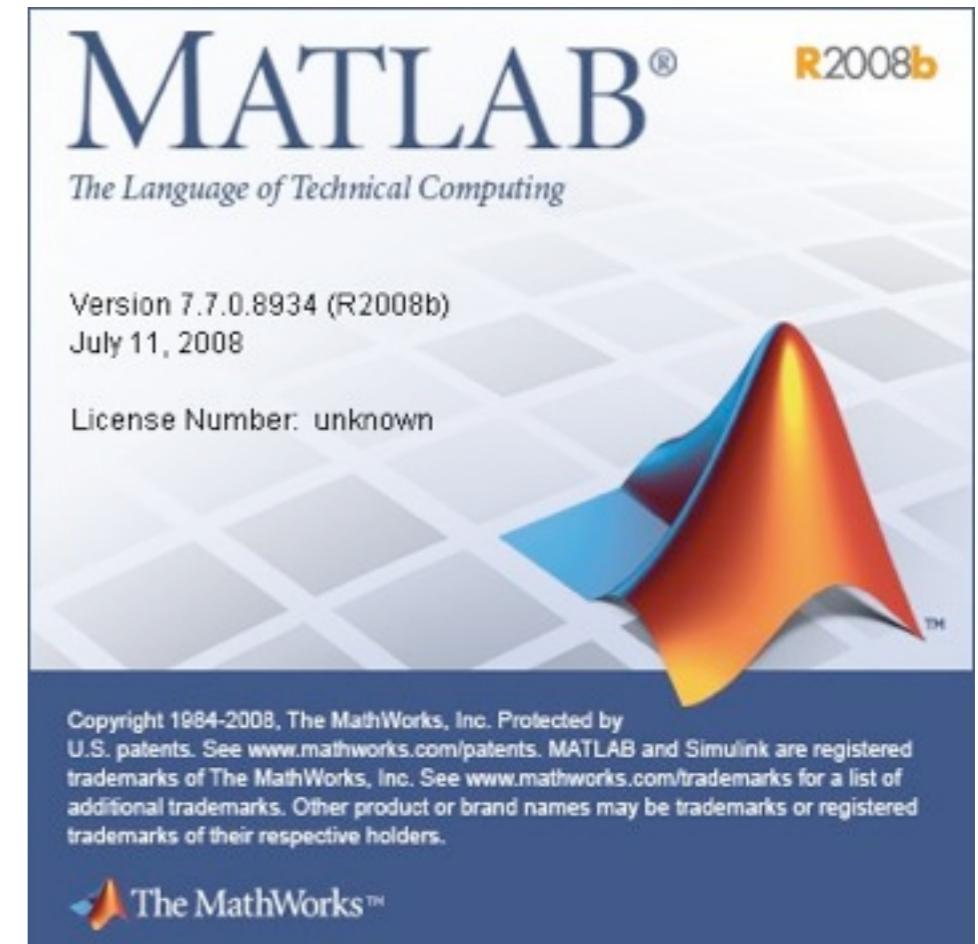


Does your company use MPC ?



Model Predictive Control Toolbox

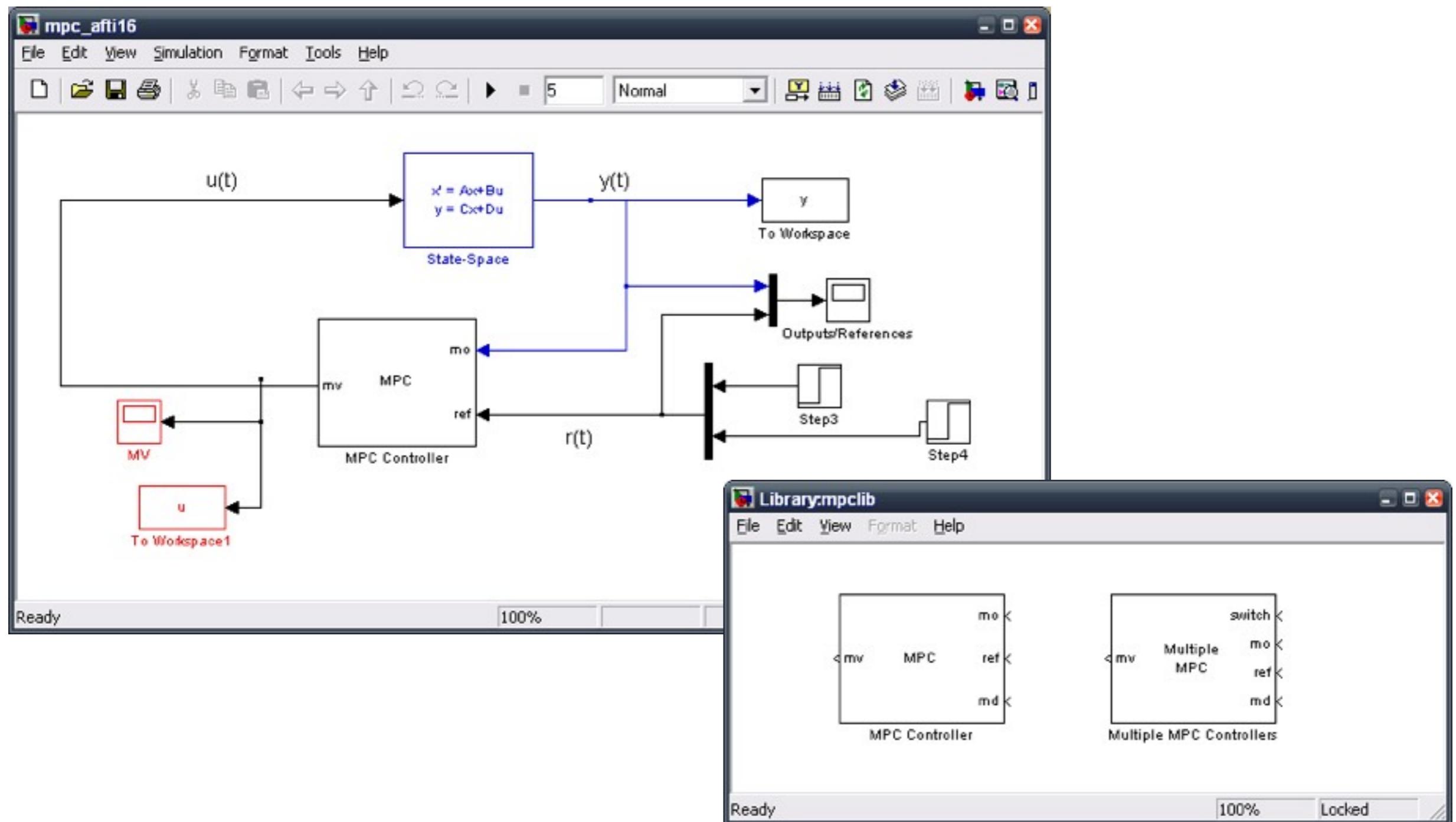
- **MPC Toolbox 3.0** (Bemporad, Ricker, Morari, 1998-today):
 - Object-oriented implementation (MPC object)
 - MPC Simulink Library
 - MPC Graphical User Interface
 - RTW extension (code generation)
[xPC Target, dSpace, etc.]
 - Linked to OPC Toolbox v2.0.1



Only linear models are handled

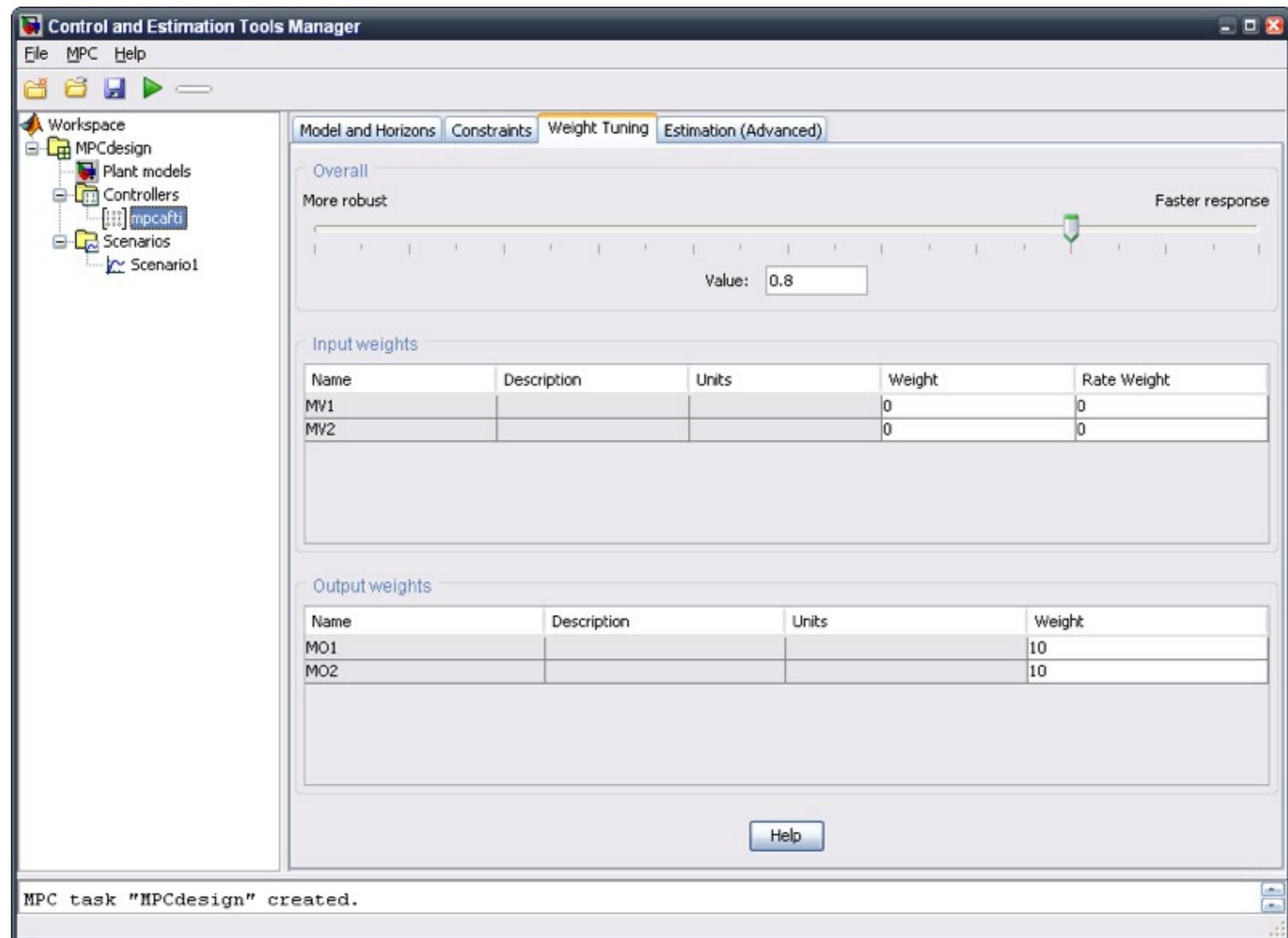
<http://www.mathworks.com/products/mpc/>

MPC Simulink Library

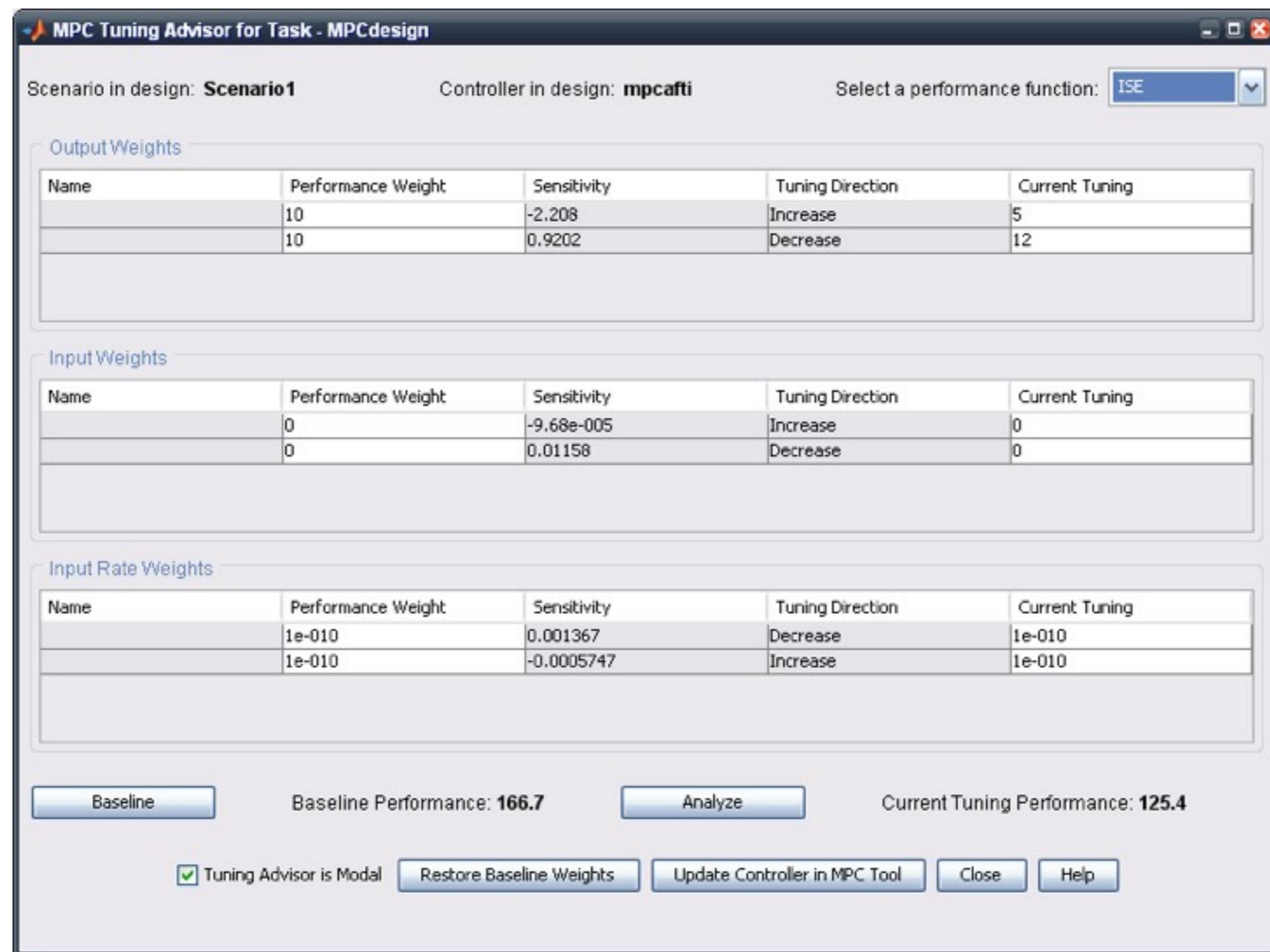


- Single MPC and multiple switched MPC blocks supported
- Reference/disturbance preview and time-varying limits supported

MPC Graphical User Interface



MPC Tuning Advisor

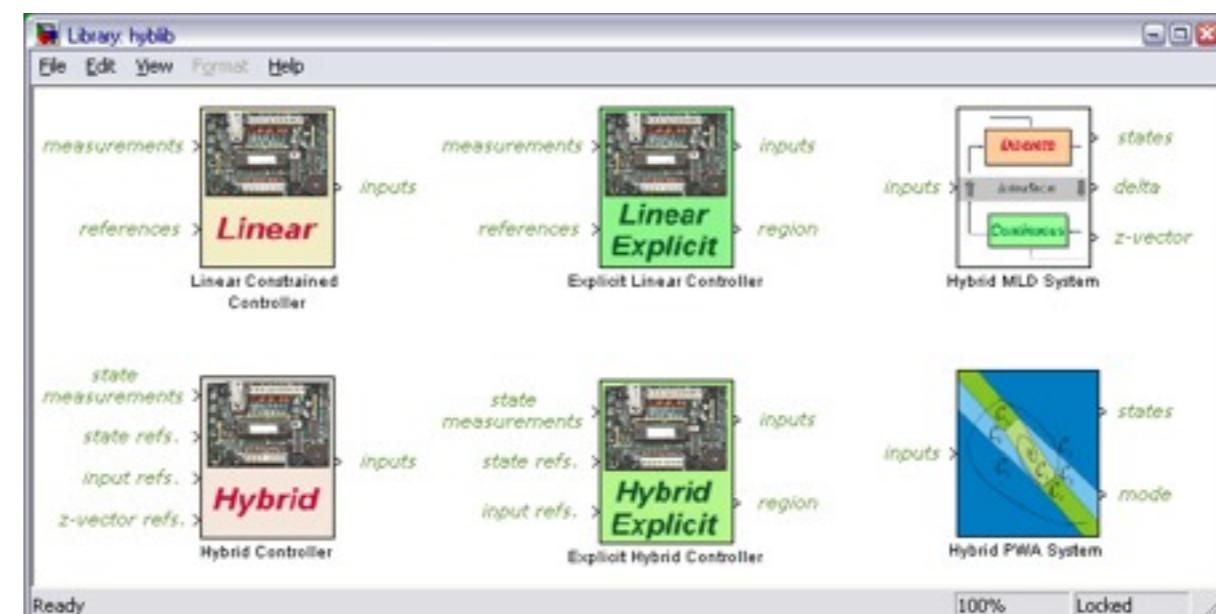
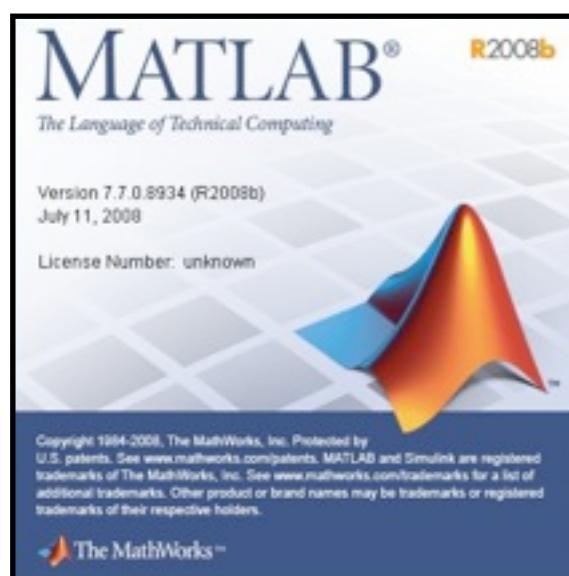


Hybrid Toolbox for MATLAB

Features:

(Bemporad, 2003-2009)

- Hybrid models: design, simulation, verification
- Control design for linear systems w/ constraints and hybrid systems (on-line optimization via QP/MILP/MIQP)
- Explicit MPC control (via multi-parametric programming)
- C-code generation
- Simulink library



2450+ download requests
since October 2004

<http://www.dii.unisi.it/hybrid/toolbox>

Basics of Constrained Optimization

Mathematical Programming

$$\begin{array}{ll} \min & f(x) \\ x & \\ \text{s.t.} & g(x) \leq 0 \end{array}$$

$$\left(\begin{array}{ll} \max & f(x) \\ x & \\ \text{s.t.} & g(x) \leq 0 \end{array} \right)$$

$x \in \mathbb{R}^n, f : \mathbb{R}^n \rightarrow \mathbb{R}, g : \mathbb{R}^n \rightarrow \mathbb{R}^m$

$$f(x) = f(x_1, \dots, x_n) \quad x = \begin{bmatrix} x_1 \\ x_2 \\ \vdots \\ x_n \end{bmatrix} \quad g(x) = \begin{bmatrix} g_1(x_1, \dots, x_n) \\ g_2(x_1, \dots, x_n) \\ \vdots \\ g_m(x_1, \dots, x_n) \end{bmatrix}$$

In general, problem is difficult to solve



use software tools

Optimization Software

- Taxonomy of most known solvers, for different classes of optimization problems:

<http://www-fp.mcs.anl.gov/otc/Guide/SoftwareGuide/>

- Network Enabled Optimization Server (NEOS) for remotely solving optimization problems:

<http://neos.mcs.anl.gov/neos/solvers/>

- Comparison on benchmark problems:

<http://plato.la.asu.edu/bench.html>

- Good open-source optimization software

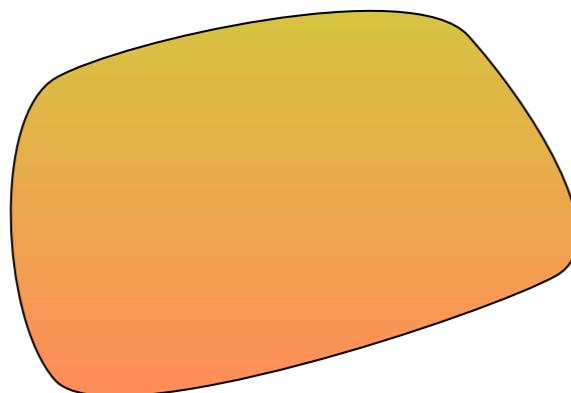
<http://www.coin-or.org/>

Convex sets

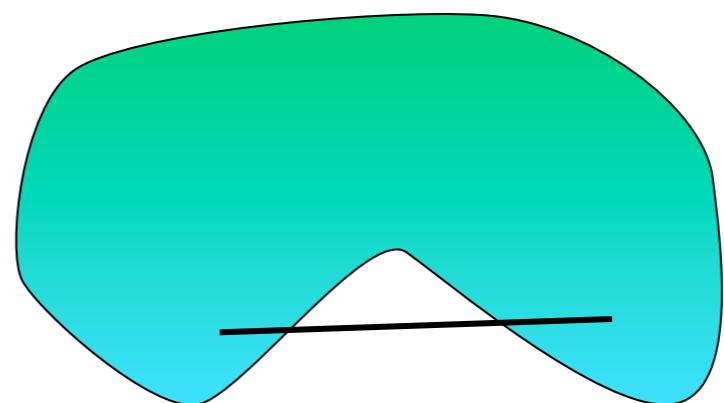
A **set** $S \in X$ is convex if for all $x_1, x_2 \in S$

$$\lambda x_1 + (1 - \lambda)x_2 \in S, \text{ for all } \lambda \in [0, 1]$$

Convex set



Nonconvex set

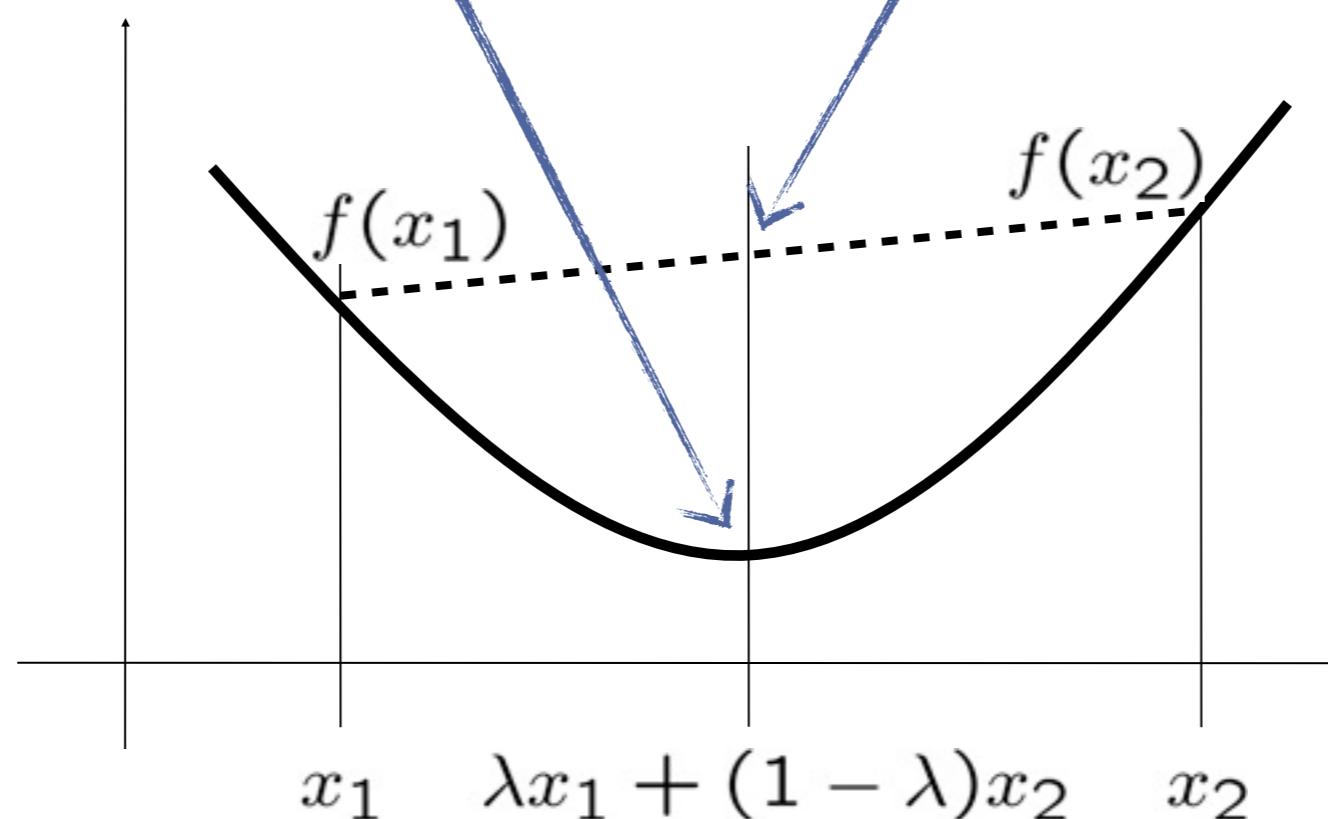


Convex function

A **function** $f : S \rightarrow \mathbb{R}$ is convex if S is convex and

$$f(\lambda x_1 + (1 - \lambda)x_2) \leq \lambda f(x_1) + (1 - \lambda)f(x_2)$$

for all $x_1, x_2 \in S, \lambda \in [0, 1]$



Convex Optimization Problem

$$\begin{array}{ll} \text{minimize} & f(x) \\ \text{subject to} & x \in C \end{array}$$

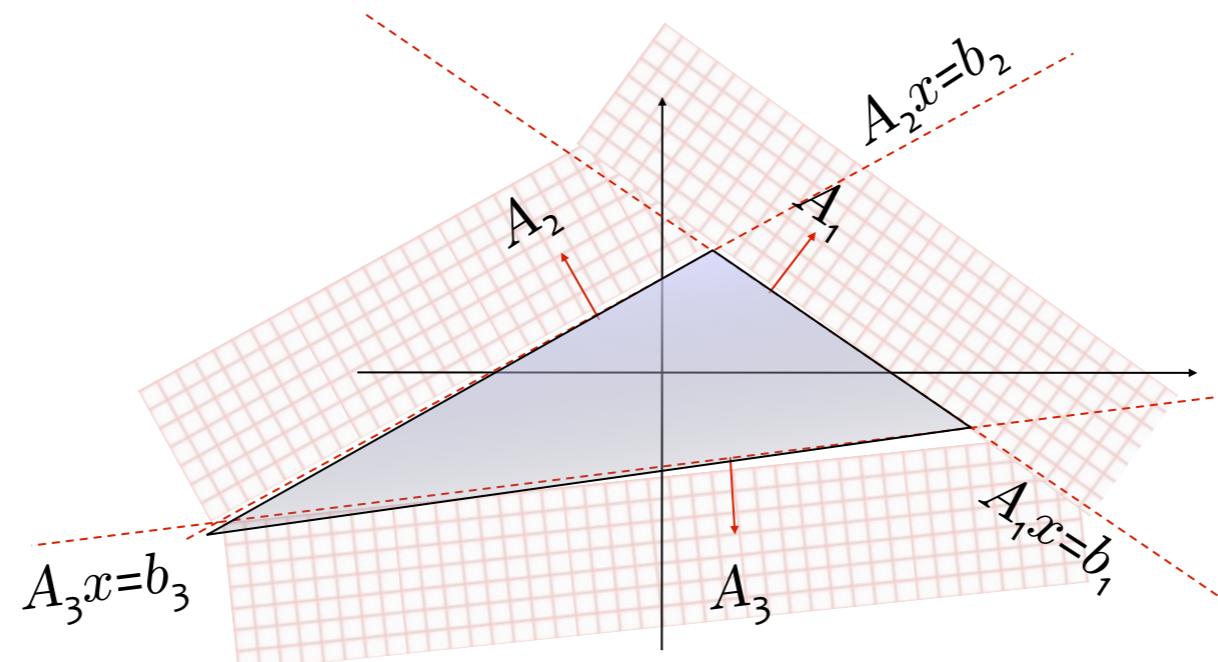
f and C convex

- Very efficient numerical algorithms exist
- Global solution attained
- Extensive useful theory
- Often occurring in engineering problems
- Tractable in theory and practice

Excellent reference textbook: “Convex Optimization” by S. Boyd
and L. Vandenberghe <http://www.stanford.edu/~boyd/cvxbook/>

Polyhedra

- A convex **polyhedron** is the intersection of a finite set of halfspaces of \mathbb{R}^d
- A convex **polytope** is a bounded convex polyhedron



- Hyperplane representation:

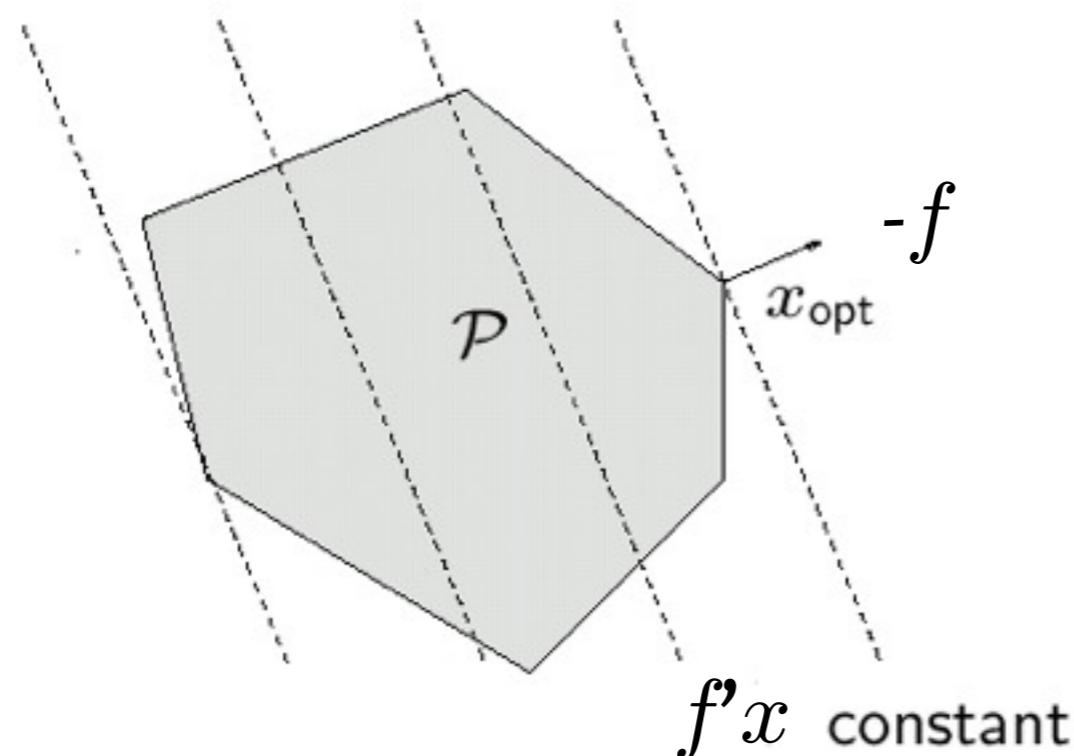
$$Ax \leq b$$

Linear Program



George Dantzig
(1914 - 2005)

$$\begin{aligned} \min \quad & f'x \\ \text{s.t.} \quad & Ax \leq b, \quad x \in \mathbb{R}^n \end{aligned}$$



Standard form:

$$\begin{aligned} \min \quad & f'x \\ \text{s.t.} \quad & Ax = b \\ & x \geq 0, \quad x \in \mathbb{R}^n \end{aligned}$$

Slack variables

$$\sum_{j=1}^N a_j x_j \leq b$$



$$\sum_{j=1}^N a_j x_j + s = b, \quad s \geq 0$$

Linear Program

trasformation
from max to min:

$$\max_x c^T x = - \left(\min_x -c^T x \right)$$

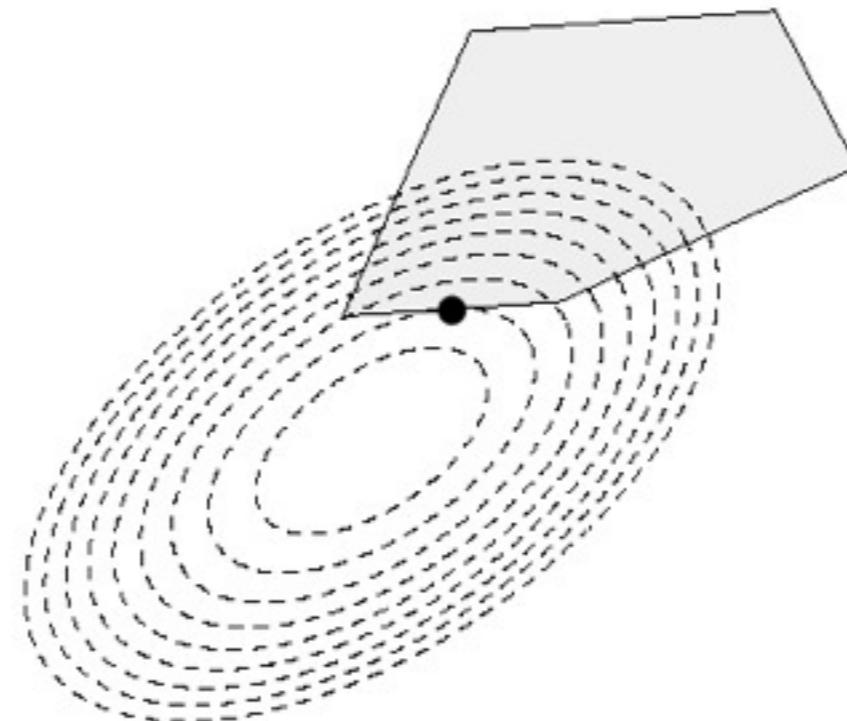
Change inequality
direction:

$$\sum_{j=1}^N a_{ij}x_j \geq b_i \quad \rightarrow \quad \sum_{j=1}^N -a_{ij}x_j \leq -b_i$$

It is always possible to formulate LP problems
using “min” and “ \leq ” inequalities

Quadratic Program

$$\begin{aligned} \min \quad & \frac{1}{2} x' P x + f' x \\ \text{s.t.} \quad & A x \leq b, \quad x \in \mathbb{R}^n \end{aligned}$$



- Convex optimization if $P \succeq 0$
- Hard problem if $P \not\succeq 0$

Mixed-Integer Linear Program

$$\begin{aligned} \min \quad & f'x + d'\delta \\ \text{s.t.} \quad & Ax + B\delta \leq c \\ & x \in \mathbb{R}^n, \quad \delta \in \{0, 1\}^m \end{aligned}$$

- Some variables are continuous, some are discrete (0/1)
- In general, it is a NP-hard problem
- Rich variety of algorithms/solvers available

Modeling languages

- **MOSEL**, associated with commercial package Xpress-MP
- **OPL** (Optimization Programming Language), associated with commercial package Ilog-CPLEX
- **AMPL** (A Modeling Language for Mathematical Programming)
most used modeling language, supports several solvers
- **GAMS** (General Algebraic Modeling System) is one of the first modeling languages
- **LINGO**, modeling language of Lindo Systems Inc.
- **GNU MathProg**, a subset of AMPL associated with the *free* package GLPK (GNU Linear Programming Kit)
- **FLOPC++ open source** modeling language (C++ class library)
- **CVX** matlab-based modeling language (from Stanford)
- **YALMIP** another matlab-based modeling language

Linear MPC

Unconstrained Optimal Control

- Linear model:

$$\begin{cases} x(t+1) = Ax(t) + Bu(t) \\ y(t) = Cx(t) \end{cases}$$

$$x \in \mathbb{R}^n, u \in \mathbb{R}^m$$
$$y \in \mathbb{R}^p$$

- Goal: find $u^*(0), u^*(1), \dots, u^*(N-1)$

$$J(x(0), U) = \sum_{k=0}^{N-1} [x'(k)Qx(k) + u'(k)Ru(k)] + x'(N)Px(N)$$

$$U = [u'(0) \ u'(1) \ \dots \ u'(N-1)]'$$

$u^*(0), u^*(1), \dots, u^*(N-1)$ is the input sequence that steers the state to the origin “optimally”

[computation of cost function]

$$J(x(0), U) = x'(0)Qx(0) + \left[x'(1) \ x'(2) \ \dots \ x'(N-1) \ x'(N) \right] \underbrace{\begin{bmatrix} Q & 0 & 0 & \dots & 0 \\ 0 & Q & 0 & \dots & 0 \\ \vdots & \vdots & \ddots & \ddots & \vdots \\ 0 & \dots & 0 & Q & 0 \\ 0 & 0 & \dots & 0 & P \end{bmatrix}}_{\bar{Q}} \cdot \begin{bmatrix} x(1) \\ x(2) \\ \vdots \\ x(N-1) \\ x(N) \end{bmatrix} + \left[u'(0) \ u'(1) \ \dots \ u'(N-1) \right] \underbrace{\begin{bmatrix} R & 0 & \dots & 0 \\ 0 & R & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & R \end{bmatrix}}_{\bar{R}} \begin{bmatrix} u(0) \\ u(1) \\ \vdots \\ u(N-1) \end{bmatrix}$$

$$\begin{bmatrix} x(1) \\ x(2) \\ \vdots \\ x(N) \end{bmatrix} = \underbrace{\begin{bmatrix} B & 0 & \dots & 0 \\ AB & B & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ A^{N-1}B & A^{N-2}B & \dots & B \end{bmatrix}}_{\bar{S}} \begin{bmatrix} u(0) \\ u(1) \\ \dots \\ u(N-1) \end{bmatrix} + \underbrace{\begin{bmatrix} A \\ A^2 \\ \vdots \\ A^N \end{bmatrix}}_{\bar{T}} x(0)$$

$$J(x(0), U) = x'(0)Qx(0) + (\bar{S}U + \bar{T}x(0))' \bar{Q}(\bar{S}U + \bar{T}x(0)) + U' \bar{R}U$$

$$= \frac{1}{2} U' \underbrace{2(\bar{R} + \bar{S}' \bar{Q} \bar{S})}_{H} U + x'(0) \underbrace{2\bar{T}' \bar{Q} \bar{S}}_{F} U + \frac{1}{2} x'(0) \underbrace{2(Q + \bar{T}' \bar{Q} \bar{T})}_{Y} x(0)$$

Unconstrained Optimal Control

$$J(x(0), U) = \frac{1}{2}U' H U + x'(0) F U + \frac{1}{2}x'(0) Y x(0)$$

$$U = [u'(0) \ u'(1) \ \dots \ u'(N-1)]'$$

The optimum is obtained by zeroing the gradient

$$\nabla_U J(x(0), U) = HU + F'x(0) = 0$$

and hence

$$U^* = \begin{bmatrix} u^*(0) \\ u^*(1) \\ \vdots \\ u^*(N-1) \end{bmatrix} = -H^{-1}F'x(0)$$

**batch least
squares**

Alternative approach: use dynamic programming to find U^*
(Riccati iterations)

Constrained Optimal Control

- Linear model:
$$\begin{cases} x(t+1) = Ax(t) + Bu(t) \\ y(t) = Cx(t) \end{cases} \quad x \in \mathbb{R}^n, u \in \mathbb{R}^m \\ y \in \mathbb{R}^p$$
- Constraints:
$$\begin{cases} u_{\min} \leq u(t) \leq u_{\max} \\ y_{\min} \leq y(t) \leq y_{\max} \end{cases}$$
- Constrained optimal control problem (quadratic performance index):

$$\begin{aligned} & \min_{u(0), \dots, u(N-1)} \sum_{k=0}^{N-1} [x'(k)Qx(k) + u'(k)Ru(k)] + x'(N)Px(N) \\ \text{s.t. } & u_{\min} \leq u(k) \leq u_{\max}, \quad k = 0, \dots, N-1 \\ & y_{\min} \leq y(k) \leq y_{\max}, \quad k = 1, \dots, N \end{aligned}$$

$$Q = Q' \succeq 0, \quad R = R' \succ 0, \quad P \succeq 0$$

Constrained Optimal Control

- Optimization problem:

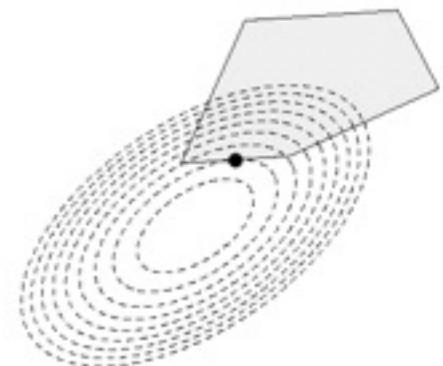
$$V(x(0)) = \frac{1}{2}x'(0)Yx(0) + \min_U \frac{1}{2}U'HU + x'(0)FU$$

$$\text{s.t. } GU \leq W + Sx(0)$$

(quadratic)

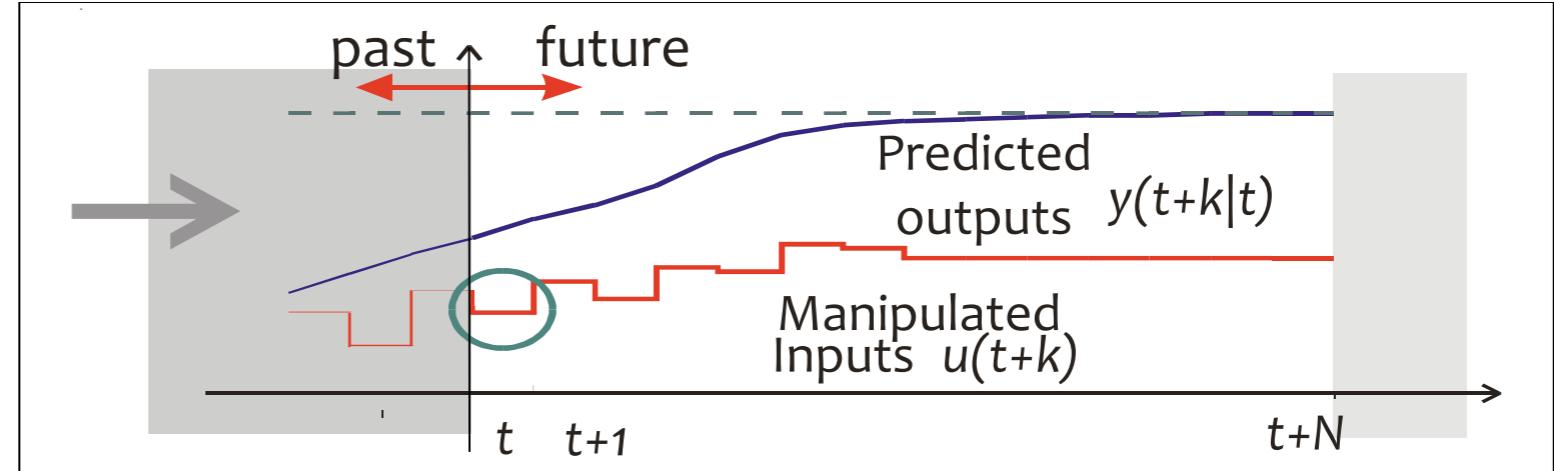
(linear)

Convex QUADRATIC PROGRAM (QP)



- $U \triangleq [u'(0) \dots u'(N-1)]' \in \mathbb{R}^s$, $s \triangleq Nm$, is the optimization vector
- $H = H' \succ 0$, and H, F, Y, G, W, S depend on weights Q, R, P , upper and lower bounds $u_{\min}, u_{\max}, y_{\min}, y_{\max}$, and model matrices A, B, C

Linear MPC Algorithm



At time t :

- Get/estimate the current state $x(t)$
- Solve the QP problem

$$\begin{aligned} \min_U \quad & \frac{1}{2} U' H U + x'(t) F U \\ \text{s.t.} \quad & G U \leq W + S x(t) \end{aligned}$$

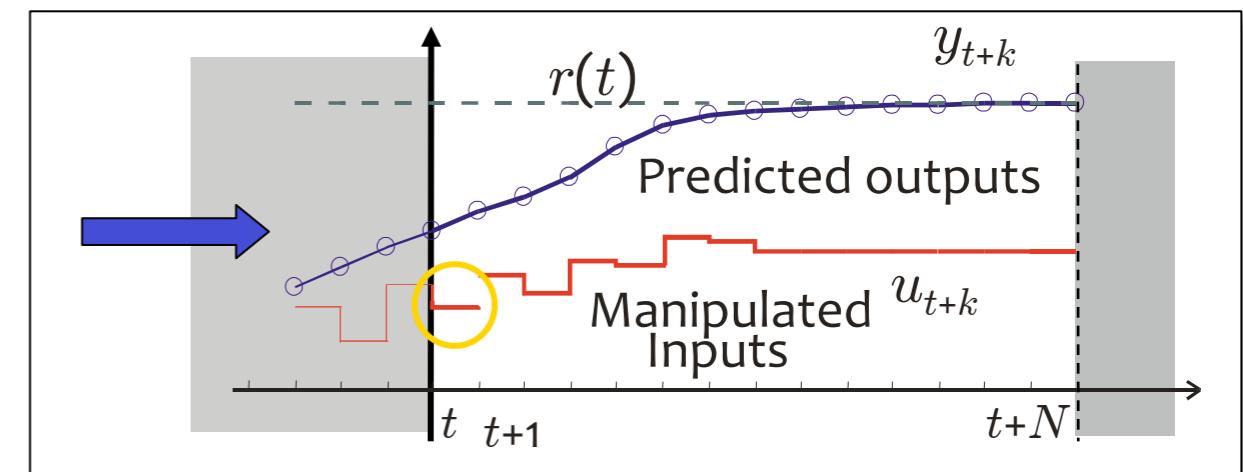
and let $U = \{u^*(0), \dots, u^*(N-1)\}$ be the solution
(=finite-horizon constrained open-loop optimal control)

- Apply only $u(t) = u^*(0)$ and discard the remaining optimal inputs
- Repeat optimization at time $t+1$. And so on ...

Unconstrained Linear MPC

- Assume no constraints
- Problem to solve on-line:

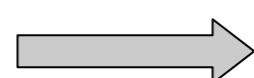
$$\min_U J(x(t), U) = \frac{1}{2} U' H U + x'(t) F U$$



- Solution: $\nabla_U J(x(t), U) = HU + F'x(t) = 0$

$$\longrightarrow U^* = -H^{-1}F'x(t)$$

$$U = \begin{bmatrix} u_0 \\ u_1 \\ \vdots \\ u_{N-1} \end{bmatrix}$$



$$u(t) = -[I \ 0 \ \dots \ 0]H^{-1}Fx(t) \triangleq Kx(t)$$

Unconstrained linear MPC is nothing else than a standard linear state-feedback law !

Double Integrator Example

- System: $y(\tau) = \frac{1}{s^2}u(\tau)$ ➡ $x(t+1) = \begin{bmatrix} 1 & 1 \\ 0 & 1 \end{bmatrix}x(t) + \begin{bmatrix} 0 \\ 1 \end{bmatrix}u(t)$
 $y(t) = \begin{bmatrix} 1 & 0 \end{bmatrix}x(t)$
sampling + ZOH
 $T_s=1\text{ s}$

- Constraints: $-1 \leq u(\tau) \leq 1$

- Control objective: $\min \left(\sum_{k=0}^1 y^2(k) + \frac{1}{10}u^2(k) \right) + x'(2) \begin{bmatrix} 1 & 0 \end{bmatrix} x(2)$

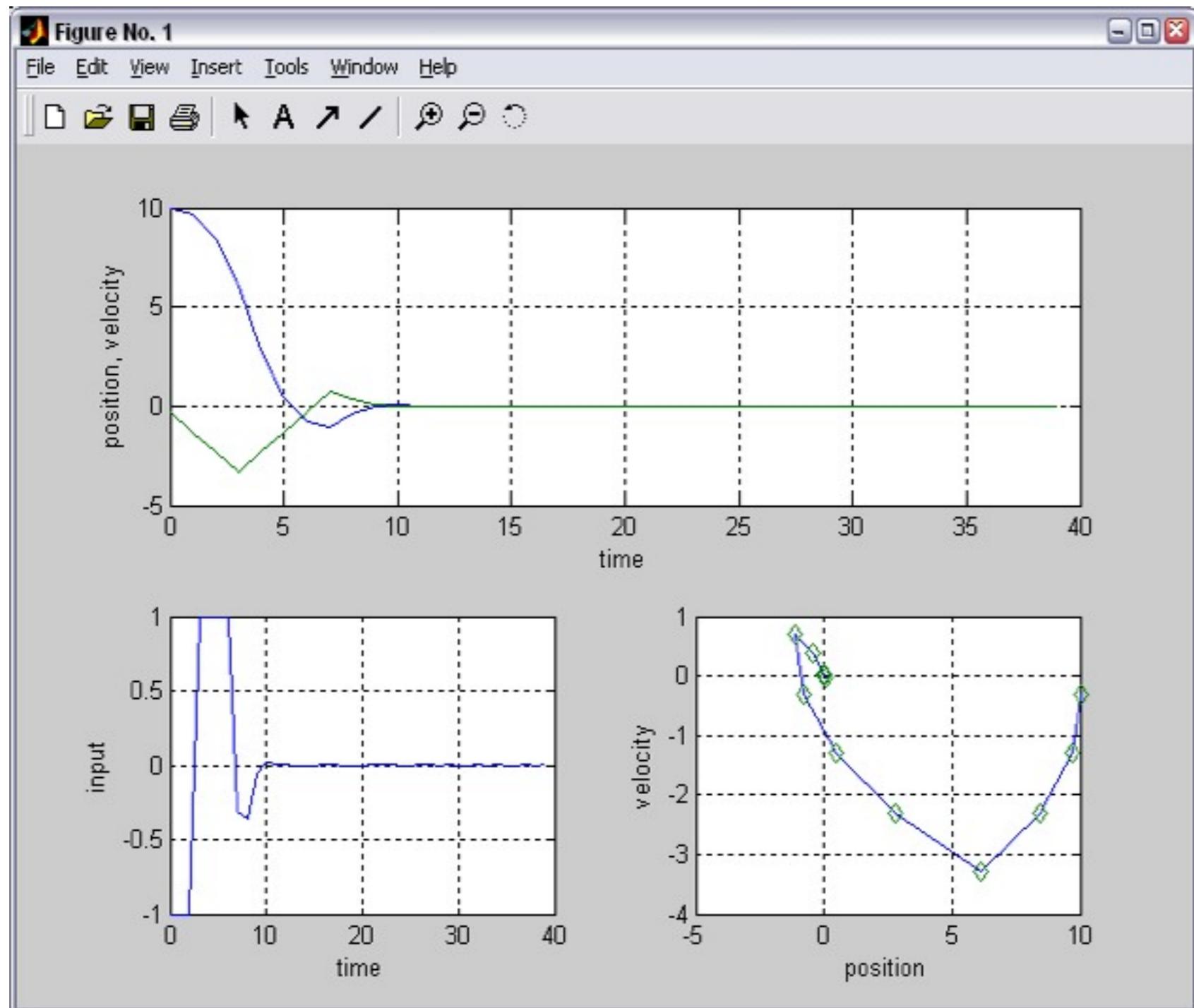
- Optimization problem matrices:

$$H = \begin{bmatrix} 4.2 & 2 \\ 2 & 2.2 \end{bmatrix}, \quad F = \begin{bmatrix} 2 & 0 \\ 6 & 2 \end{bmatrix}, \quad Y = \begin{bmatrix} 4 & 6 \\ 6 & 12 \end{bmatrix}$$
$$G = \begin{bmatrix} 1 & 0 \\ -1 & 0 \\ 0 & 1 \\ 0 & -1 \end{bmatrix}, \quad W = \begin{bmatrix} 1 \\ 1 \\ 1 \\ 1 \end{bmatrix}, \quad S = \begin{bmatrix} 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \end{bmatrix}$$

cost: $\frac{1}{2}U'HU + x'(t)FU + \frac{1}{2}x'(t)Yx(t)$

constraints: $GU \leq W + Sx(t)$

Double Integrator Example



go to demo **/demos/linear/doubleint.m**

(Hyb-Tbx)

see also **mpcdoubleint.m**

(MPC-Tbx)

Double Integrator Example

- Add a state constraint:

$$x_2(k) \geq -1, \quad k = 1$$

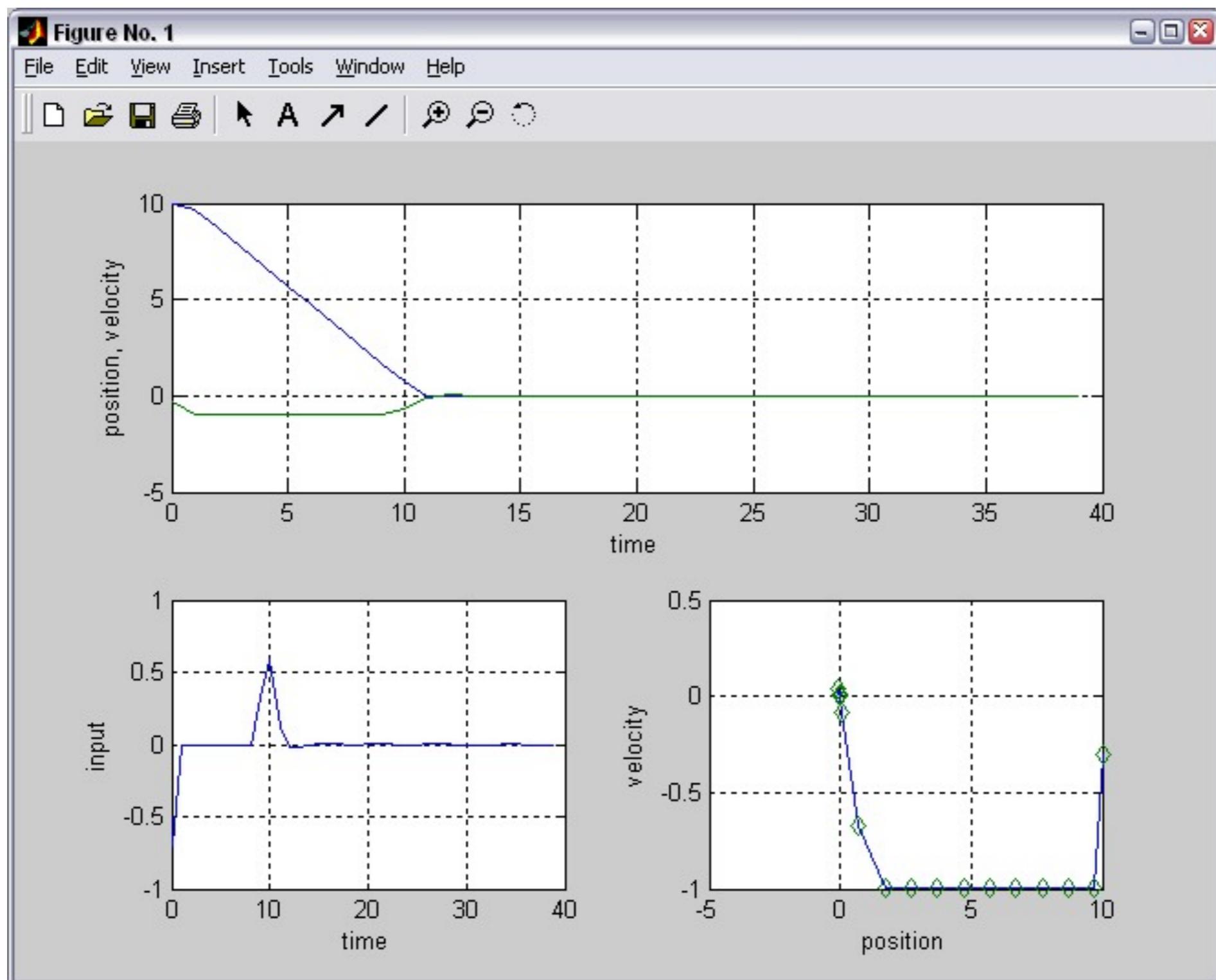
- Optimization problem matrices:

$$H = \begin{bmatrix} 4.2 & 2 \\ 2 & 2.2 \end{bmatrix}, \quad F = \begin{bmatrix} 2 & 0 \\ 6 & 2 \end{bmatrix}, \quad Y = \begin{bmatrix} 4 & 6 \\ 6 & 12 \end{bmatrix}$$
$$G = \begin{bmatrix} -1 & 0 \\ 1 & 0 \\ -1 & 0 \\ 0 & 1 \\ 0 & -1 \end{bmatrix}, \quad W = \begin{bmatrix} 1 \\ 1 \\ 1 \\ 1 \\ 1 \end{bmatrix}, \quad S = \begin{bmatrix} 0 & 1 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \end{bmatrix}$$

cost: $\frac{1}{2}U'HU + x'(t)FU + \frac{1}{2}x'(t)Yx(t)$

constraints: $GU \leq W + Sx(t)$

Double Integrator Example



Linear MPC - Tracking

- Objective: make the output $y(t)$ track a reference signal $r(t)$
- Idea: parameterize the problem using input increments

$$\Delta u(t) = u(t) - u(t-1) \quad \Rightarrow \quad u(t) = u(t-1) + \Delta u(t)$$

- Extended system: let $x_u(t) = u(t-1)$

$$\begin{cases} x(t+1) = Ax(t) + Bu(t-1) + B\Delta u(t) \\ x_u(t+1) = x_u(t) + \Delta u(t) \end{cases}$$



$$\begin{cases} \begin{bmatrix} x(t+1) \\ x_u(t+1) \end{bmatrix} = \begin{bmatrix} A & B \\ 0 & I \end{bmatrix} \begin{bmatrix} x(t) \\ x_u(t) \end{bmatrix} + \begin{bmatrix} B \\ I \end{bmatrix} \Delta u(t) \\ y(t) = \begin{bmatrix} C & 0 \end{bmatrix} \begin{bmatrix} x(t) \\ x_u(t) \end{bmatrix} \end{cases}$$

Again a linear system with states $x(t)$, $x_u(t)$ and input $\Delta u(t)$

Linear MPC - Tracking

- Optimal control problem (quadratic performance index):

$$\begin{aligned} \min_{\Delta U} \quad & \sum_{k=0}^{N-1} \|W^y(y(k+1) - r(t))\|^2 + \|W^{\Delta u}\Delta u(k)\|^2 \\ & [\Delta u(k) \triangleq u(k) - u(k-1)] \\ \text{subj. to} \quad & u_{\min} \leq u(k) \leq u_{\max}, \quad k = 0, \dots, N-1 \\ & \Delta u_{\min} \leq \Delta u(k) \leq \Delta u_{\max}, \quad k = 0, \dots, N-1 \\ & y_{\min} \leq y(k) \leq y_{\max}, \quad k = 1, \dots, N \end{aligned}$$

optimization vector:

$$\Delta U = \begin{bmatrix} \Delta u(0) \\ \Delta u(1) \\ \vdots \\ \Delta u(N-1) \end{bmatrix}$$

- Note: $\|Wz\|^2 = (Wz)'(Wz) = z'(W'W)z = z'Qz$



same formulation as before (W =Cholesky factor of weight matrix Q)

- Optimization problem:

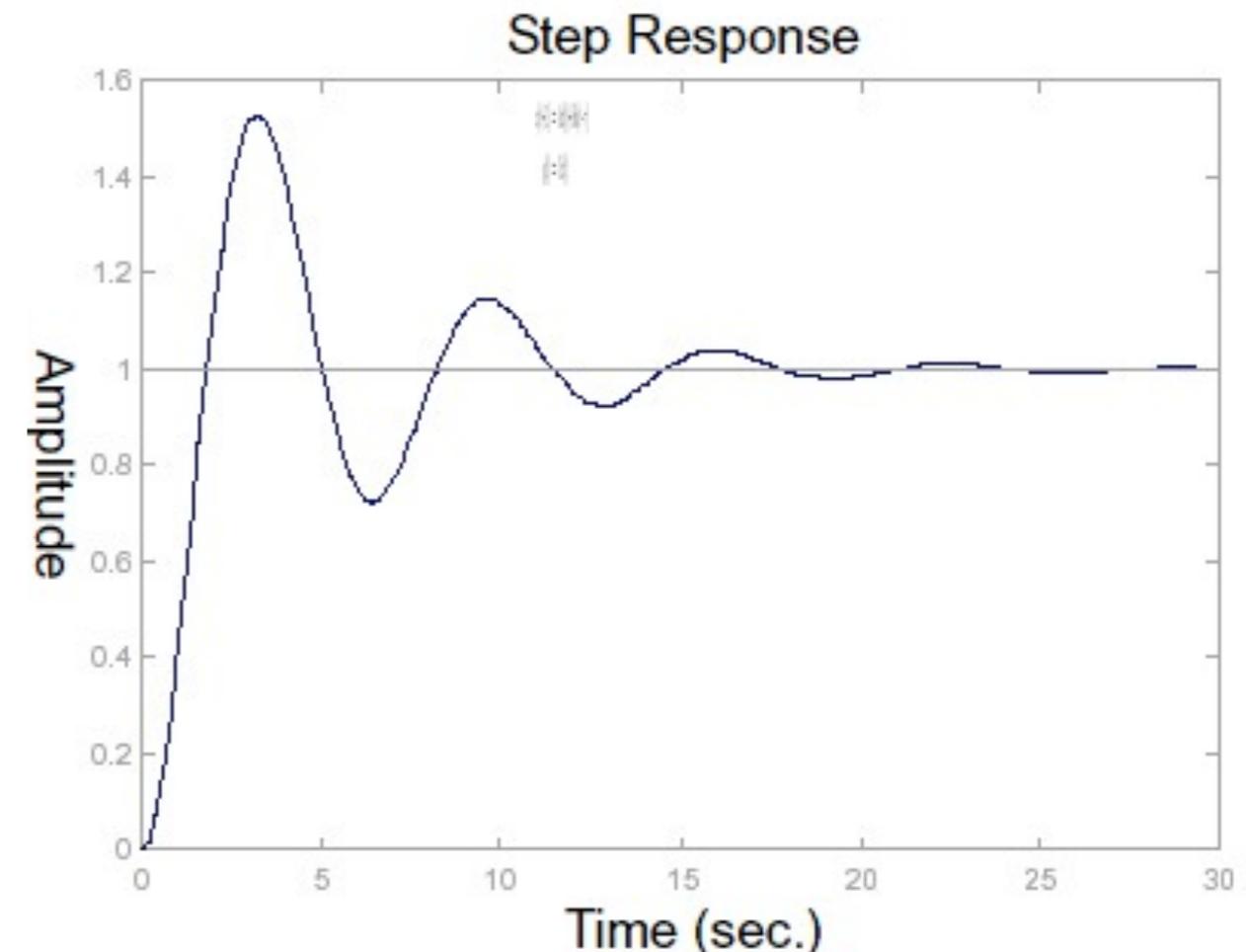
Convex
Quadratic
Program (QP)

$$\begin{aligned} \min_{\Delta U} \quad & J(\Delta U, x(t)) = \frac{1}{2} \Delta U H \Delta U + [x'(t) \ r'(t) \ u'(t-1)] F \Delta U \\ \text{s.t.} \quad & G \Delta U \leq W + S \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix} \end{aligned}$$

Linear MPC - Example

- Plant: $G(s) = \frac{1}{s^2 + 0.4s + 1}$

- Sampling time: $T_s = 0.5$ sec.



- Model:

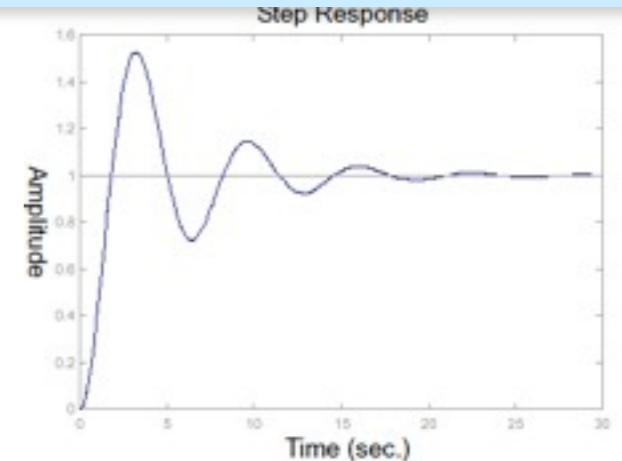
$$\begin{cases} x(t+1) = \begin{bmatrix} 1.597 & -0.4094 \\ 2 & 0 \end{bmatrix} x(t) + \begin{bmatrix} 0.5 \\ 0 \end{bmatrix} u(t) \\ y(t) = \begin{bmatrix} 0.2294 & 0.1072 \end{bmatrix} x(t) \end{cases}$$

go to demo **linear/example3.m** (Hyb-Tbx)

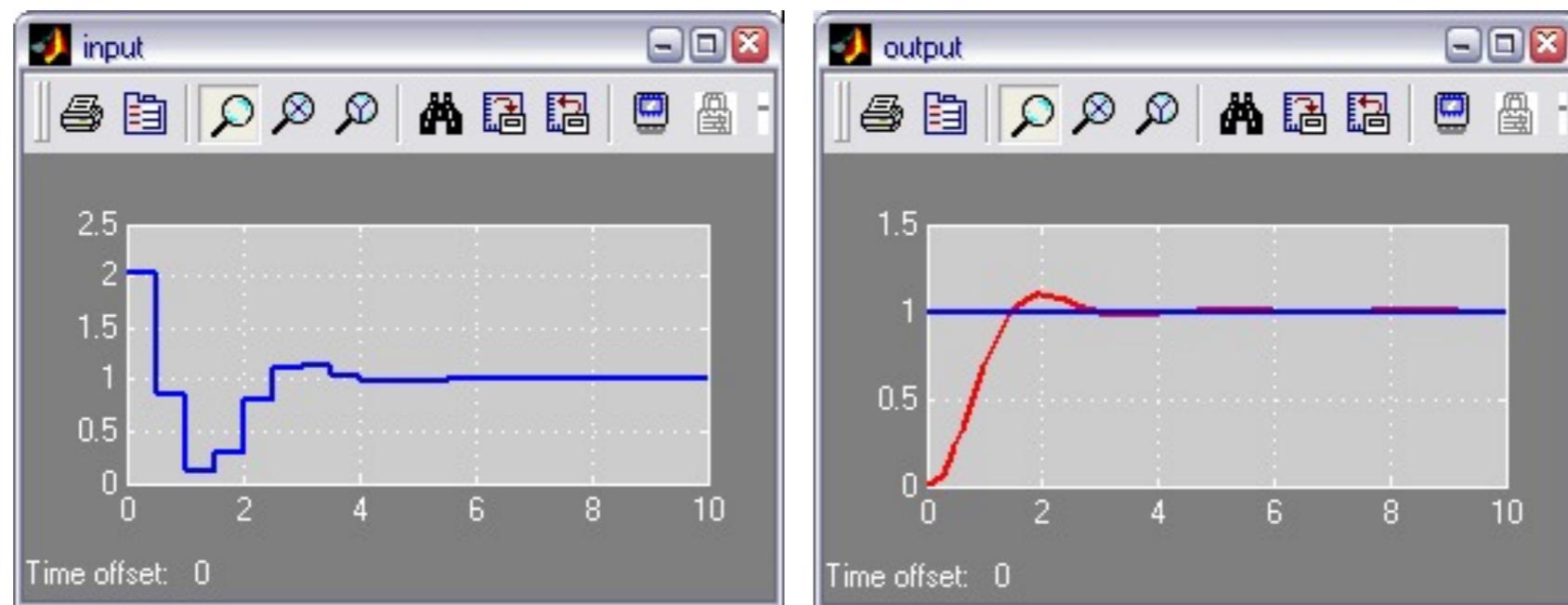
Linear MPC - Example

- Performance index:

$$J(U, t) \triangleq \sum_{k=0}^9 [y(t + k + 1|t) - r(t)]^2 + 0.04\Delta u^2(t)$$



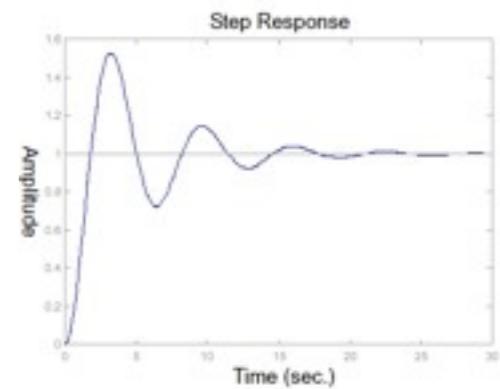
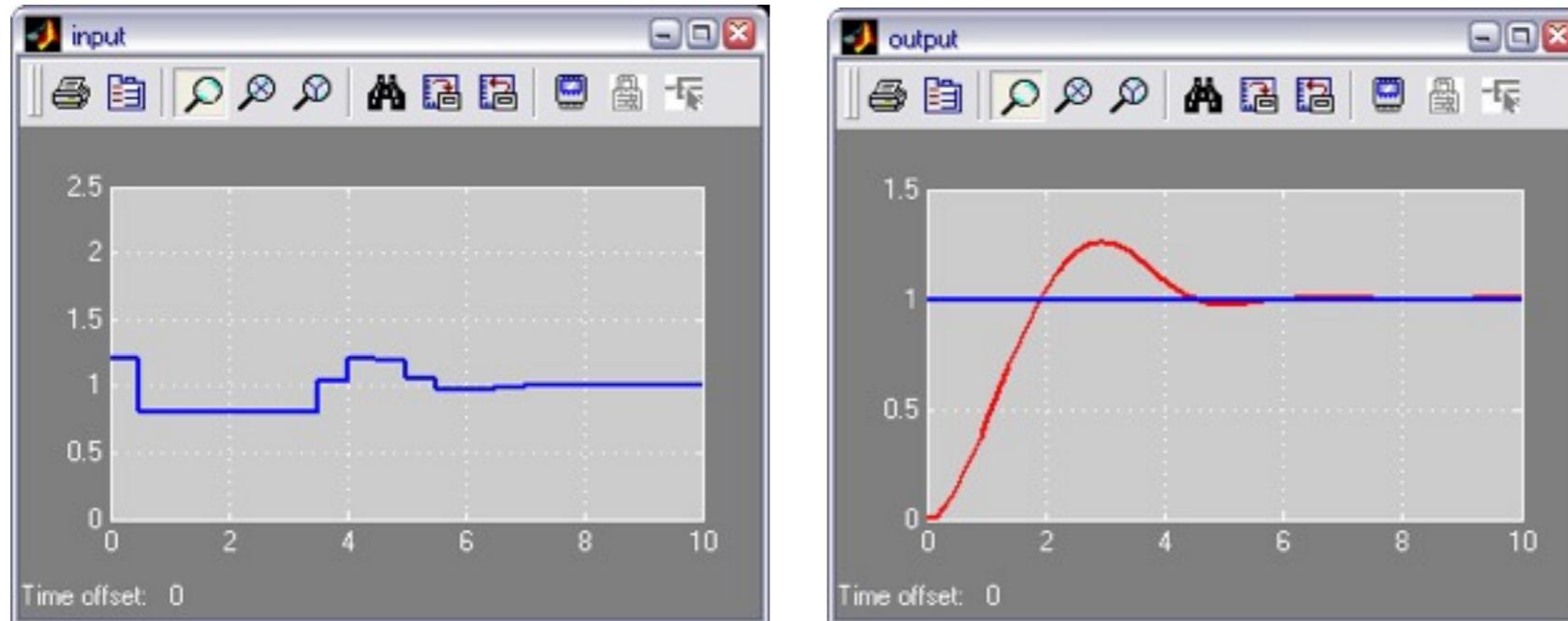
- Closed-loop MPC:



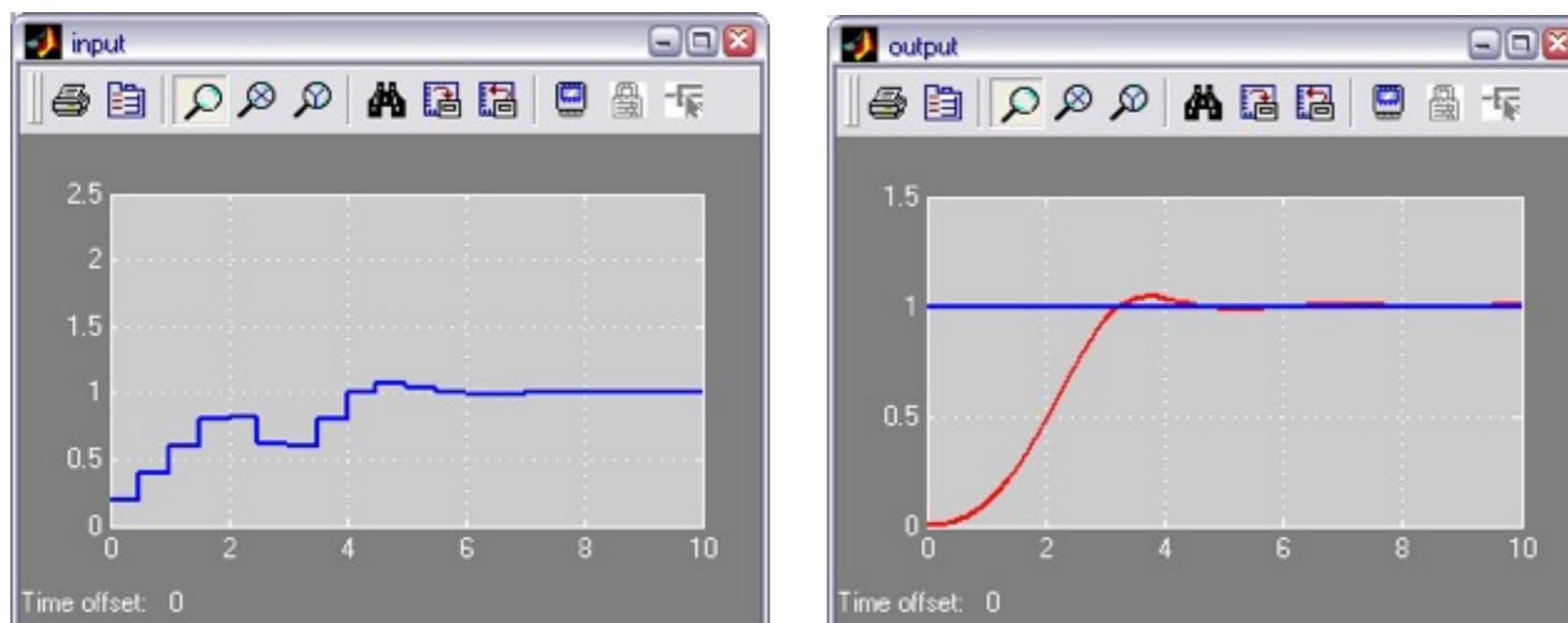
go to demo **linear/example3.m** (Hyb-Tbx)

Linear MPC - Example

- Constraint $0.8 \leq u(t) \leq 1.2$ (amplitude)



- Constraint $-0.2 \leq \Delta u(t) \leq 0.2$ (slew-rate)

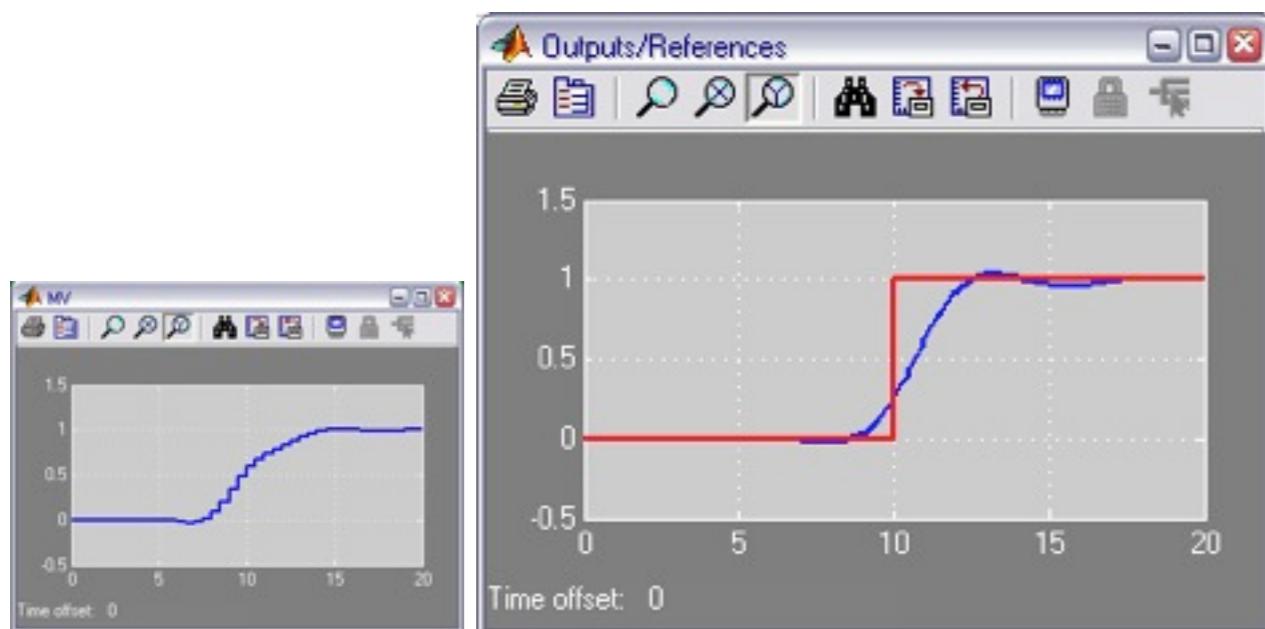


Anticipative Action

$$\min_{\Delta U} \sum_{k=0}^{N-1} \|W^y(y(k+1) - r(t+k+1|t))\|^2 + \|W^{\Delta u} \Delta u(k)\|^2$$

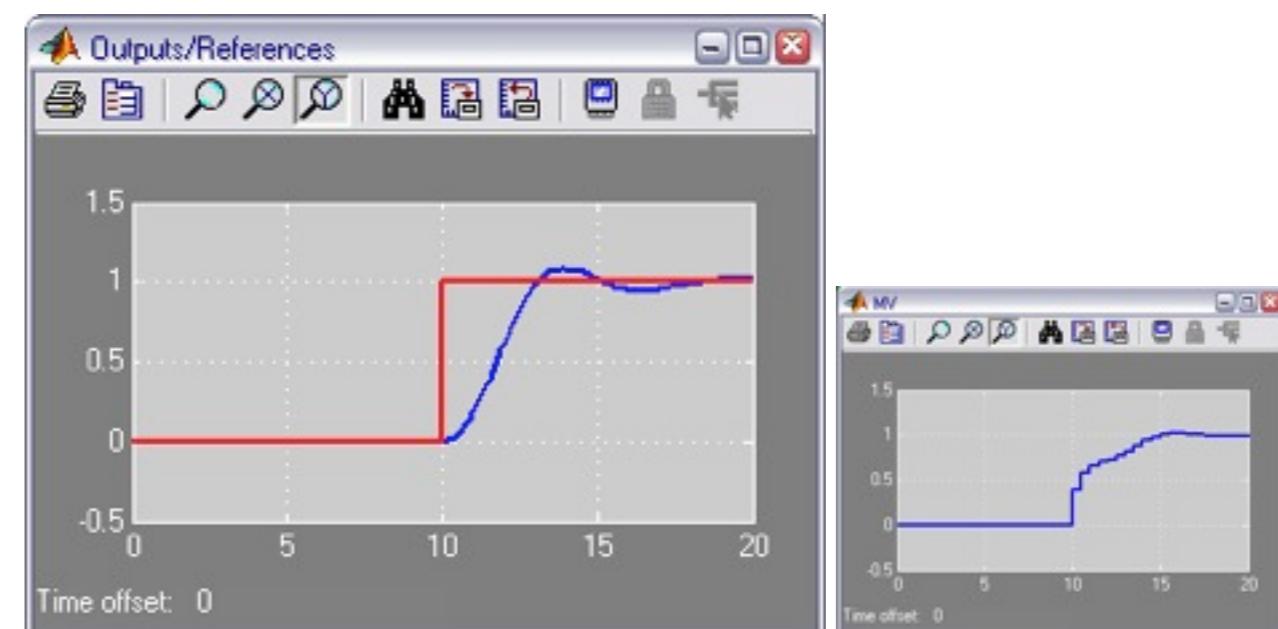
- Future reference samples (partially) known in advance (anticipating action):

$$r(t+k|t) = \begin{cases} r(t+k) & \text{if } k = 0, \dots, N_r \\ r(t+N_r) & \text{if } k > N_r \end{cases}$$



- Reference not known in advance (causal):

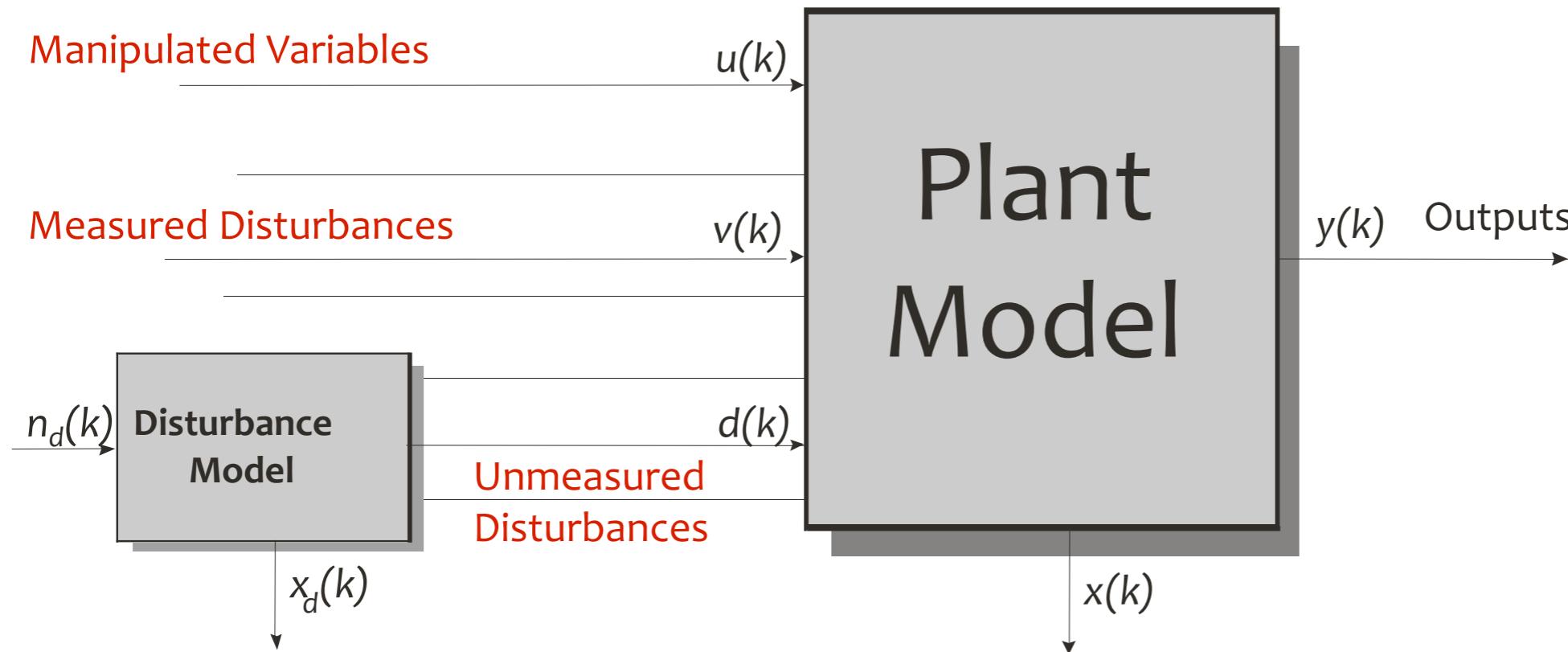
$$r(t+k|t) \equiv r(t), \forall k \geq 0$$



go to demo `mpcpreview.m`

(MPC-Tbx)

Measured and Unmeasured Disturbances



Linear model
for MPC
optimization

$$\begin{cases} x(k+1) = Ax(k) + B_u u(k) + B_v v(k) + B_d d(k) \\ y(k) = Cx(k) + D_v v(k) + D_d d(k) \end{cases}$$
$$\begin{cases} x_d(k+1) = \bar{A}x_d(k) + \bar{B}n_d(k) \\ d(k) = \bar{C}x_d(k) + \bar{D}n_d(k). \end{cases}$$

($n_d(k)$ = white Gaussian noise, $n_d(t+k|t)=0$ over the prediction horizon)

more details about disturbance models later on ...

Soft Constraints

- To prevent QP infeasibility, relax output constraints:

$$\min_z \quad \sum_{k=0}^{N-1} \|W^y(y(t+k+1|t) - r(t))\|^2 + \|W^{\Delta u}\Delta u(t)\|^2 + \rho_\epsilon \epsilon^2$$

subj. to $u_{\min} \leq u(t+k) \leq u_{\max}, \quad k = 0, \dots, N-1$

$\Delta u_{\min} \leq \Delta u(t+k) \leq \Delta u_{\max}, \quad k = 0, \dots, N-1$

$y_{\min} - \epsilon V_{\min} \leq y(t+k|t) \leq y_{\max} + \epsilon V_{\max}, \quad k = 1, \dots, N$

ϵ = “panic” variable

$$z = [\Delta u'(0) \ \Delta u'(1) \ \dots \ \Delta u'(N-1) \ \epsilon]'$$

$$\rho_\epsilon \gg W^y, W^{\Delta u}$$

V_{\min}, V_{\max} = vectors with entries ≥ 0 (the larger the entry, the relatively softer the corresponding constraint)

- Infeasibility can be due to:

- modeling errors
- disturbances
- wrong MPC setup (e.g., prediction horizon is too short)

Delays – Method 1

- Linear model w/ delays:

$$x(t+1) = Ax(t) + Bu(t-\tau)$$

$$y(t) = Cx(t)$$

- Map delays to poles in $z=0$:

$$x_k(t) \triangleq u(t-k) \Rightarrow x_k(t+1) = x_{k-1}(t) \quad k = 1, \dots, \tau$$

$$\begin{bmatrix} x \\ x_\tau \\ x_{\tau-1} \\ \vdots \\ x_1 \end{bmatrix}(t+1) = \begin{bmatrix} A & B & 0 & 0 & \dots & 0 \\ 0 & 0 & I_m & 0 & \dots & 0 \\ 0 & 0 & 0 & I_m & \dots & 0 \\ \vdots & \vdots & \vdots & \ddots & \vdots & \vdots \\ 0 & 0 & 0 & 0 & \dots & 0 \end{bmatrix} \begin{bmatrix} x \\ x_\tau \\ x_{\tau-1} \\ \vdots \\ x_1 \end{bmatrix}(t) + \begin{bmatrix} 0 \\ 0 \\ 0 \\ \vdots \\ I_m \end{bmatrix} u(t)$$

- Apply MPC to the extended system

Delays – Method 2

- Linear model w/ delays:

$$x(t+1) = Ax(t) + Bu(t-\tau)$$

$$y(t) = Cx(t)$$

- Delay-free model:

$$\bar{x}(t+1) = A\bar{x}(t) + Bu(t)$$

$$\bar{x}(t) \triangleq x(t+\tau)$$

$$\bar{y}(t) = C\bar{x}(t)$$

- Design MPC for delay-free model:

$$u(t) = f_{\text{MPC}}(\bar{x}(t))$$

- Compute the predicted state

$$\bar{x}(t) = x(t+\tau) = A^\tau x(t) + \sum_{j=0}^{\tau-1} A^j B u(t-1-j)$$

- Compute MPC action accordingly:

$$u(t) = f_{\text{MPC}}(\bar{x}(t+\tau))$$

For better closed-loop performance one can predict $x(t+\tau)$ with a much more complex model than (A, B, C) !

MPC vs. Conventional Control

Single input/single output control loop w/ constraints:

equivalent performance can be obtained with other simpler control techniques (e.g.: PID + anti-windup)

HOWEVER

MPC allows (in principle) **UNIFORMITY**
(i.e. same technique for wide range of problems)

- reduce training
- reduce cost
- easier design maintenance

Satisfying control specs and walking on water is similar ...

both are not difficult if frozen !



MPC Features

- Multivariable constrained “non-square” systems
(i.e. #inputs and #outputs are different)
- Delay compensation
- Anticipative action for future reference changes
- “Integral action”, i.e. no offset for step-like inputs

Price to pay:

- Substantial on-line computation
- For simple small/fast systems other techniques dominate
(e.g. PID + anti-windup)
- New possibilities for MPC: **explicit** piecewise linear forms

- **Historical Goal:** Explain the success of DMC
- **Present Goal:** Improve, simplify, and extend industrial algorithms
- **Areas:**
 - **Linear MPC:** linear model
 - **Nonlinear MPC:** nonlinear model
 - **Robust MPC:** uncertain (linear) model
 - **Hybrid MPC:** model integrating logic, dynamics, and constraints
- **Issues:**
 - Feasibility
 - Stability (Convergence)
 - Computations

(Mayne, Rawlings, Rao, Scokaert, 2000)

Feasibility

$$\min_{\Delta U} \sum_{k=0}^{N-1} \|W^y(y(t+k+1|t) - r(t))\|^2 + \|W^{\Delta u}\Delta u(k)\|^2$$

subj. to $u_{\min} \leq u(t+k) \leq u_{\max}, k = 0, \dots, N-1$
 $\Delta u_{\min} \leq \Delta u(t+k) \leq \Delta u_{\max}, k = 0, \dots, N-1$
 $y_{\min} \leq y(t+k|t) \leq y_{\max}, k = 1, \dots, N$

**QUADRATIC
PROGRAM (QP)**

- **Feasibility:** Guarantee that the QP problem is feasible at all sampling times t
- Input constraints only: no feasibility issues !
- Hard output constraints:
 - When $N < \infty$ there is no guarantee that the QP problem will remain feasible at all future time steps t
 - $N = \infty \rightarrow$ infinite number of constraints !
 - **Maximum output admissible set theory:** $N < \infty$ is enough
(Gilbert, Tan, IEEE TAC, 1991), (Kerrigan, Maciejowski, CDC, 2000),
(Chmielewski, Manousiouthakis, Sys. Cont. Letters, 1996)

Stability

$$\begin{aligned} & \min_{u(0), \dots, u(N-1)} \sum_{k=0}^{N-1} [x'(k)Qx(k) + u'(k)Ru(k)] + x'(N)Px(N) \\ \text{s.t. } & u_{\min} \leq u(k) \leq u_{\max}, \quad k = 0, \dots, N-1 \\ & y_{\min} \leq y(k) \leq y_{\max}, \quad k = 1, \dots, N \end{aligned}$$

$$Q = Q' \succeq 0, \quad R = R' \succ 0, \quad P \succeq 0$$

- Stability is a complex function of the MPC parameters $N, Q, R, P, u_{\min}, u_{\max}, y_{\min}, y_{\max}$
- **Stability constraints** and weights on the terminal state can be imposed over the prediction horizon to ensure stability of MPC

Convergence Result

Theorem 1 Consider the linear system

$$\begin{cases} x(t+1) = Ax(t) + Bu(t) \\ y(t) = Cx(t) \end{cases}$$

and the MPC control law based on

$$\begin{aligned} \min_U J(U, x(t)) &= \sum_{k=0}^{N-1} \{x'(t+k|t)Qx(t+k|t) + u'(t+k|Ru(t+k)\} \\ \text{subj. to} \quad y_{min} &\leq y(t+k) \leq y_{max} \\ u_{min} &\leq u(t+k) \leq u_{max} \\ x(t+N|t) &= 0 \end{aligned}$$

Assume that the optimization problem is feasible at time $t = 0$. Then, for all $R > 0$, $Q > 0$,

$$\begin{aligned} \lim_{t \rightarrow \infty} x(t) &= 0, \\ \lim_{t \rightarrow \infty} u(t) &= 0, \end{aligned}$$

and the constraints are satisfied at all time instants $t \geq 0$.

(Keerthi and Gilbert, 1988)(Bemporad et al., 1994)

Proof: Use value function as Lyapunov function

Convergence Proof

- Let \mathcal{U}_t^* denote the optimal control sequence @ t $\{u_t^*(0), \dots, u_t^*(N-1)\}$
- Let $V(t) \triangleq J(\mathcal{U}_t^*, x(t))$ = value function \rightarrow Lyapunov function
- By construction, $\mathcal{U}_1 = \{u_t^*(1), \dots, u_t^*(N-1), 0\}$ is feasible @ $t+1$, and hence

$$V(t+1) = J(\mathcal{U}_{t+1}^*, x(t+1)) \leq J(\mathcal{U}_1, x(t+1)) = V(t) - x'(t)Qx(t) - u'(t)Ru(t)$$

- $V(t)$ is decreasing and lower-bounded by 0 $\Rightarrow \exists V_\infty = \lim_{t \rightarrow \infty} V(t) \Rightarrow V(t+1) - V(t) \rightarrow 0$, which implies $x'(t)Qx(t), u'(t)Ru(t) \rightarrow 0$
- Since $R, Q > 0$, $u(t), x(t) \rightarrow 0$

Global optimum is not needed to prove convergence !

Convergence Result (a little more general)

Theorem 1 Consider the linear system

$$\begin{cases} x(t+1) = Ax(t) + Bu(t) \\ y(t) = Cx(t) \end{cases}$$

and the MPC control law based on

$$\begin{aligned} \min_U J(U, x(t)) &= \sum_{k=0}^{N-1} \{y'(t+k|t)Qy(t+k|t) + u'(t+k|Ru(t+k)\} \\ \text{subj. to} &\quad y_{min} \leq y(t+k) \leq y_{max} \\ &\quad u_{min} \leq u(t+k) \leq u_{max} \end{aligned}$$

Assume that the optimization problem is feasible at time $t = 0$. Then, for either $N \rightarrow \infty$ or with the extra constraint $x(t+N|t) = 0$, for all $R > 0$, $Q \geq 0$,

$$\begin{aligned} \lim_{t \rightarrow \infty} y(t) &= 0, \\ \lim_{t \rightarrow \infty} u(t) &= 0, \end{aligned}$$

while fulfilling the constraints. Moreover, provided that $(Q^{\frac{1}{2}}C, A)$ is a detectable pair, $\lim_{t \rightarrow \infty} x(t) = 0$.

(Keerthi and Gilbert, 1988)(Bemporad et al., 1994)

Proof: Use value function as Lyapunov function

Convergence Proof

- Assume we set the terminal constraint $x(t + N|t) = 0$
- Let \mathcal{U}_t^* denote the optimal control sequence @ t $\{u_t^*(0), \dots, u_t^*(N - 1)\}$
- Let $V(t) \triangleq J(\mathcal{U}_t^*, x(t))$ = value function \rightarrow Lyapunov function
- By construction, $\mathcal{U}_1 = \{u_t^*(1), \dots, u_t^*(N - 1), 0\}$ is feasible @ $t + 1$, and hence

$$\begin{aligned} V(t + 1) &= J(\mathcal{U}_{t+1}^*, x(t + 1)) \leq J(\mathcal{U}_1, x(t + 1)) = \\ &= V(t) - y'(t)Qy(t) - u'(t)Ru(t) \end{aligned}$$

- $V(t)$ is decreasing and lower-bounded by 0 $\Rightarrow \exists V_\infty = \lim_{t \rightarrow \infty} V(t) \Rightarrow V(t + 1) - V(t) \rightarrow 0$, which implies $y'(t)Qy(t), u'(t)Ru(t) \rightarrow 0$
- Since $R > 0$, $u(t) \rightarrow 0$
- Assume for simplicity that $C = I$ (i.e., $y(t) = x(t)$) and $Q > 0$. Then also $x(t) \rightarrow 0$.

Global optimum is not needed to prove convergence !

Convergence Proof

If $Q \geq 0$ and/or $C \neq I$:

- For all $\forall k = 0, \dots, n - 1$, we have

$$\lim_{t \rightarrow \infty} y'(t+k)Qy(t+k) = \lim_{t \rightarrow \infty} \|Q^{\frac{1}{2}}C(A^kx(t) + \sum_{j=0}^{k-1} A^jBu(t+k-1-j))\|^2 = 0$$

- As $u(t) \rightarrow 0$, also $Q^{\frac{1}{2}}CA^kx(t) \rightarrow 0$, and hence $\Theta x(t) \rightarrow 0$, where Θ is the observability matrix of $(Q^{\frac{1}{2}}C, A)$.
- If $(Q^{\frac{1}{2}}C, A)$ is observable, this also implies $x(t) \rightarrow 0$.
- If $(Q^{\frac{1}{2}}C, A)$ is only detectable, through a canonical decomposition one can observe that, as $u(t) \rightarrow 0$, unobservable modes go to zero spontaneously.

Convergence Proof

- Similar argument for infinite prediction horizon $N = \infty$:
 - Let \mathcal{U}_t^* denote the infinite optimal control sequence @ t $\{u_t^*(0), u_t^*(1) \dots\}$
 - Let $V(t) \triangleq J(\mathcal{U}_t^*, x(t))$ = value function (\Rightarrow Lyapunov function)
 - Because constraints were checked up to $t+k = \infty$, $\mathcal{U}_1 = \{u_t^*(1), u_t^*(2), \dots\}$ is feasible @ $t+1$ by construction.
 - Hence

$$\begin{aligned} V(t+1) &= J(\mathcal{U}_{t+1}^*, x(t+1)) \leq J(\mathcal{U}_1, x(t+1)) = \\ &= V(t) - y'(t)Qy(t) - u'(t)Ru(t) \end{aligned}$$

- Repeat same arguments as before

Stability Constraints

1. No constraint, infinite output horizon:

(Keerhi and Gilbert, 1988) (Rawlings and Muske, 1993)

$$N \rightarrow \infty$$

2. End-point constraint:

(Kwon and Pearson, 1977) (Keerhi and Gilbert, 1988)

$$x(t + N|t) = 0$$

3. Relaxed terminal constraint:

(Scokaert and Rawlings, 1996)

$$x(t + N|t) \in \Omega$$

4. Contraction constraint:

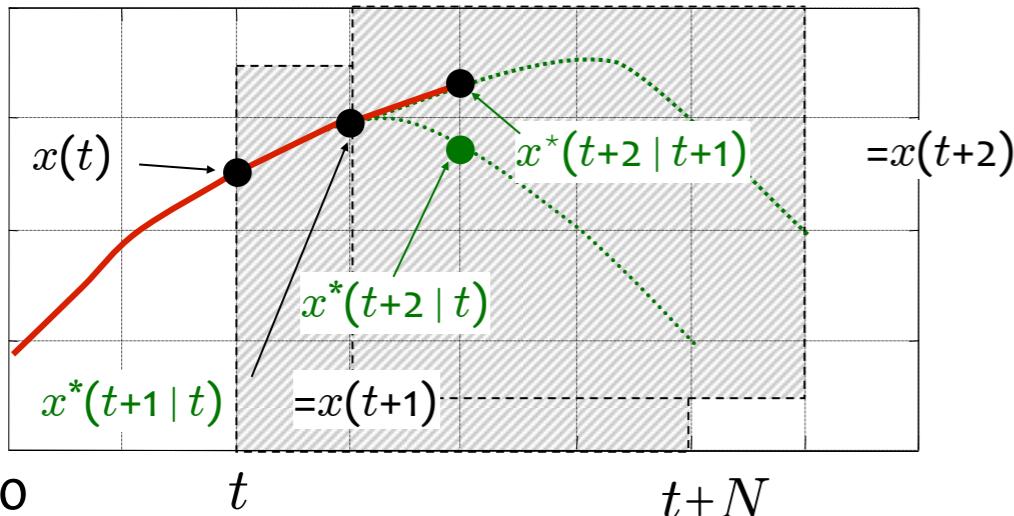
(Polak and Yang, 1993) (Bemporad, 1998)

$$\|x(t + 1|t)\| \leq \alpha \|x(t)\|, \quad \alpha < 1$$

All the proofs in (1,2,3) use the value function $V(t) = \min_U J(U, t)$ as a Lyapunov function

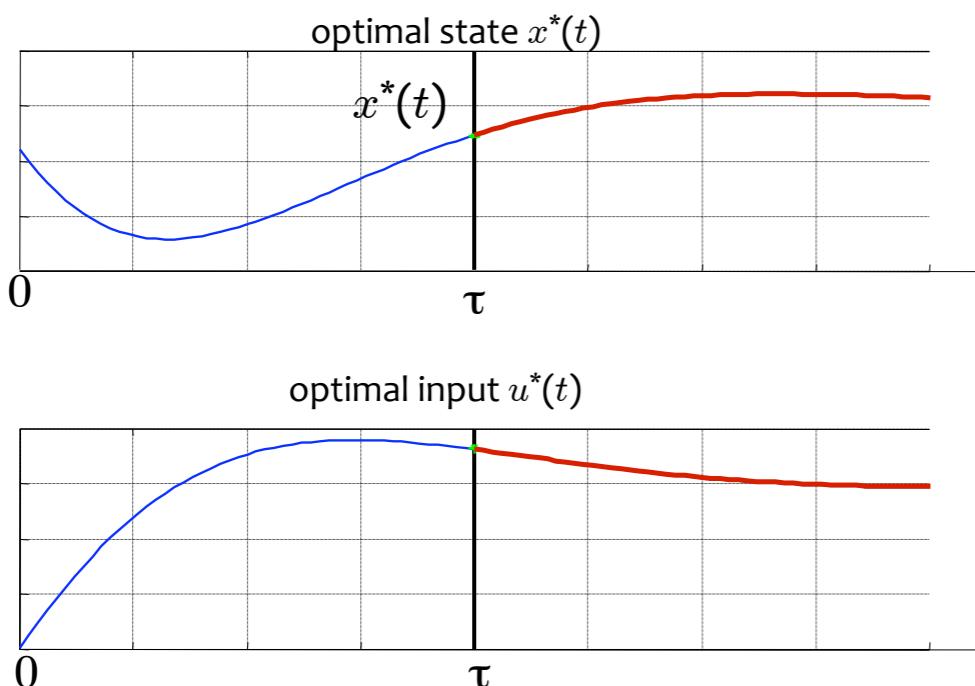
Predicted and Actual Trajectories

- Even assuming perfect model & no disturbances:



predicted open-loop trajectories may be different from **actual** closed-loop trajectories

- Special case: for **infinite horizon**, open-loop trajectories and closed-loop trajectories coincide. This follows by Bellman's principle of optimality.



Richard Bellman
(1920 - 1984)

Input and Output Horizons

$$\min_{\Delta U} \sum_{k=0}^{N-1} \|W^y(y(t+k+1|t) - r(t))\|^2 + \|\Delta u\|^2$$

$$\text{subj. to } u_{\min} \leq u(t+k) \leq u_{\max}, \quad k = 0, \dots, N-1$$

$$\Delta u_{\min} \leq \Delta u(t+k) \leq \Delta u_{\max}, \quad k = 0, \dots, N_u-1$$

$$y_{\min} \leq y(t+k|t) \leq y_{\max}, \quad k = 1, \dots, N$$

$$\Delta u(t+k) = 0, \quad k = N_u, \dots, N-1$$

- Input horizon N_u can be shorter than output horizon N
- $N_u < N$ = less degrees of freedom, and hence:
 - Loss of performance
 - Decreased computation time (QP is smaller)
 - Feasibility still maintained (constraints are still checked up to N)

typically $N_u=1\div 10$



- Consider the MPC control law:

$$\begin{aligned} \min_U J(U, t) = & \quad x'(t + N|t)Px(t + N|t) + \\ & \sum_{k=0}^{N-1} \left\{ x'(t + k|t)Qx(t + k|t) + u'(t + k)Ru(t + k) \right\} \end{aligned}$$

Jacopo Francesco
Riccati (1676 - 1754)

$R = R' > 0$, $Q = Q' \geq 0$, and P satisfies the Riccati equation

$$P = A'PA - A'PB(B'PB + R)^{-1}B'PA + Q$$

(Unconstrained) MPC = LQR

MPC and LQR

- Consider the MPC control law:

$$\begin{aligned} \min_U J(U, t) = & \quad x'(t + T|t)Px(t + T|t) + \\ & \sum_{k=0}^{N-1} \left\{ x'(t + k|t)Qx(t + k|t) + u'(t + k)Ru(t + k) \right\} \end{aligned}$$

subj. to

$$y_{min} \leq y(t + k|t) \leq y_{max}, \quad k = 1, \dots, N$$

$$u_{min} \leq u(t + k) \leq u_{max}, \quad k = 0, \dots, N - 1$$

$$u(t + k) = Kx(t + k|t), \quad k = N_u, \dots, N - 1$$

$R = R' > 0$, $Q = Q' \geq 0$, and P , K satisfy the Riccati equation

$$\begin{aligned} K &= -(R + B'PB)^{-1}B'PA \\ P &= (A + BK)'P(A + BK) + K'RK + Q \end{aligned}$$



Jacopo Francesco
Riccati (1676 - 1754)

- In a polyhedral region around the origin the MPC control law is equivalent to the constrained LQR controller with weights Q, R

MPC = constrained LQR

(Chmielewski, Manousiouthakis, 1996)

(Scokaert and Rawlings, 1998)

- The larger the horizon, the larger the region where MPC=LQR

Double Integrator Example

- System: $y(t) = \frac{1}{s^2}u(t)$ \rightarrow sampling + ZOH $T_s=1\text{ s}$
- $x(t+1) = \begin{bmatrix} 1 & 1 \\ 0 & 1 \end{bmatrix}x(t) + \begin{bmatrix} 0 \\ 1 \end{bmatrix}u(t)$
- $y(t) = \begin{bmatrix} 1 & 0 \end{bmatrix}x(t)$

- Constraints: $-1 \leq u(t) \leq 1$

- Control objective: min

$$\sum_{t=0}^{\infty} y^2(t) + \frac{1}{100}u^2(t)$$

$$u(k) = K_{LQ}x(k), \forall k \geq N = 2$$

$$\rightarrow \left(\sum_{k=0}^1 y^2(k) + \frac{1}{100}u^2(k) \right) + x'(2) \begin{bmatrix} 2.1429 & 1.2246 \\ 1.2246 & 1.3996 \end{bmatrix} x(2)$$

solution of algebraic Riccati equation

- Optimization problem

$$H = \begin{bmatrix} 0.8365 & 0.3603 \\ 0.3603 & 0.2059 \end{bmatrix}, F = \begin{bmatrix} 0.4624 & 1.2852 \\ 0.1682 & 0.5285 \end{bmatrix}$$

(cost function was normalized by
 $\max \text{svd}(H)$)

$$G = \begin{bmatrix} 1 & 0 \\ -1 & 0 \\ 0 & 1 \\ 0 & -1 \end{bmatrix}, W = \begin{bmatrix} 1 \\ 1 \\ 1 \\ 1 \end{bmatrix}, S = \begin{bmatrix} 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \end{bmatrix}$$

Example: AFTI-16

- Linearized model:

$$\left\{ \begin{array}{l} \dot{x} = \begin{bmatrix} -.0151 & -60.5651 & 0 & -32.174 \\ -.0001 & -1.3411 & .9929 & 0 \\ .00018 & 43.2541 & -.86939 & 0 \\ 0 & 0 & 1 & 0 \end{bmatrix} x + \begin{bmatrix} -2.516 & -13.136 \\ -.1689 & -.2514 \\ -17.251 & -1.5766 \\ 0 & 0 \end{bmatrix} u \\ y = \begin{bmatrix} 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix} x, \end{array} \right.$$



- Inputs: elevator and flaperon angle
- Outputs: attack and pitch angle
- Sampling time: $T_s = .05$ s (+ zero-order hold)
- Constraints: max 25° on both angles
- Open-loop response: unstable
(open-loop poles: $-7.6636, -0.0075 \pm 0.0556j, 5.4530$)

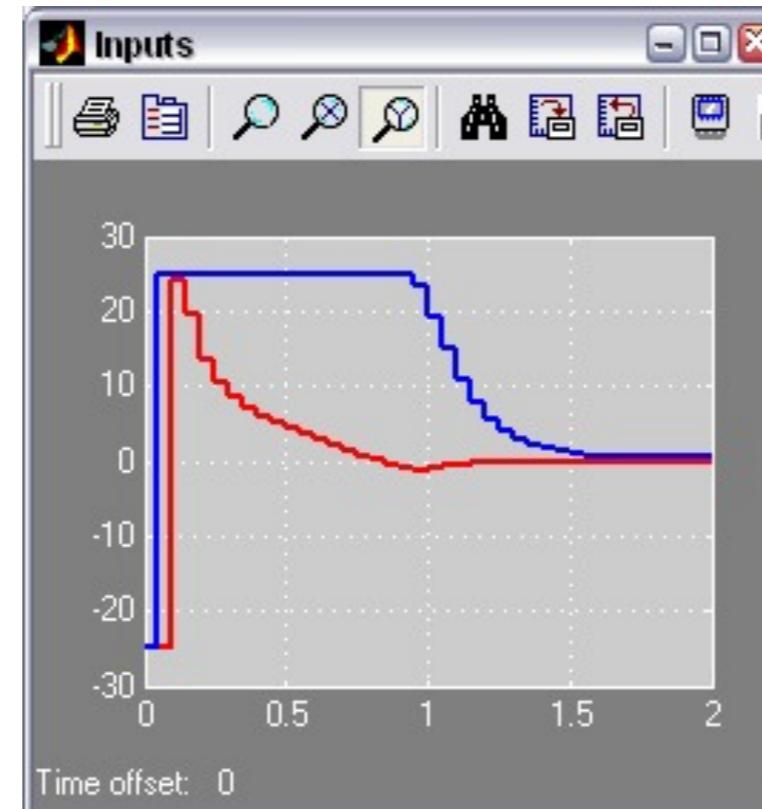
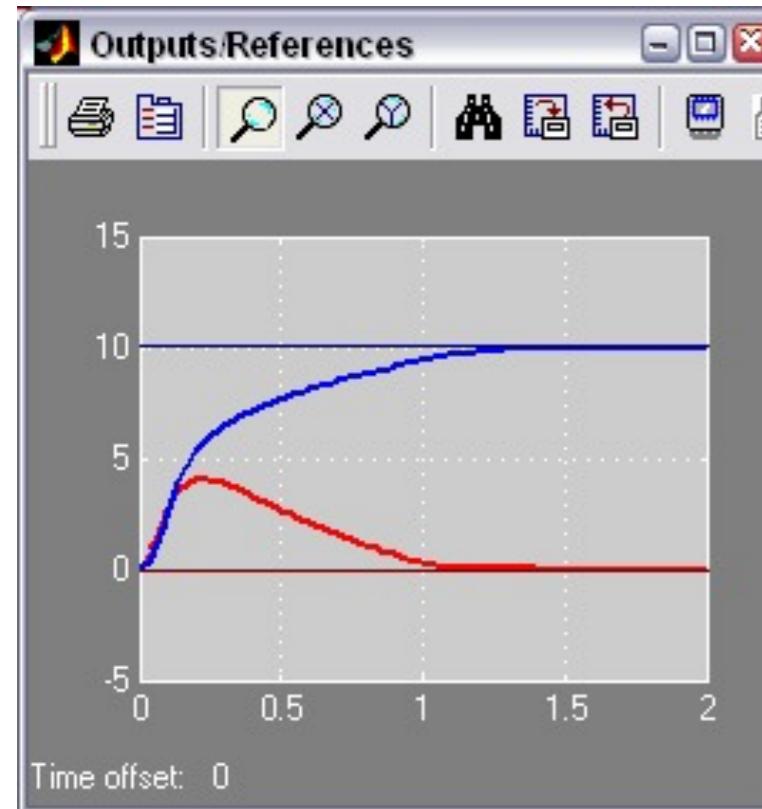
go to demo /demos/linear/afti16.m

(Hyb-Tbx)

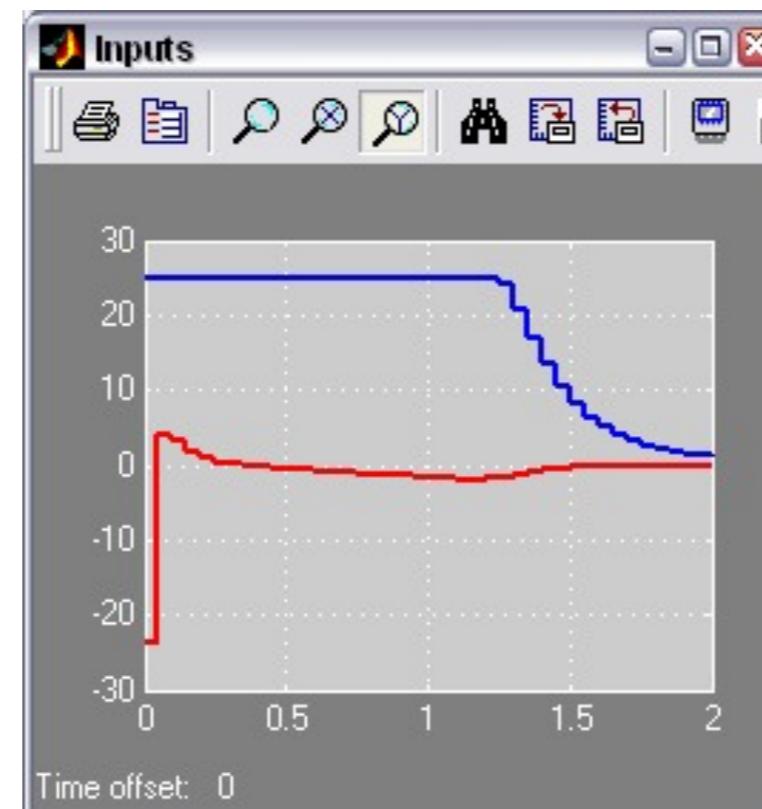
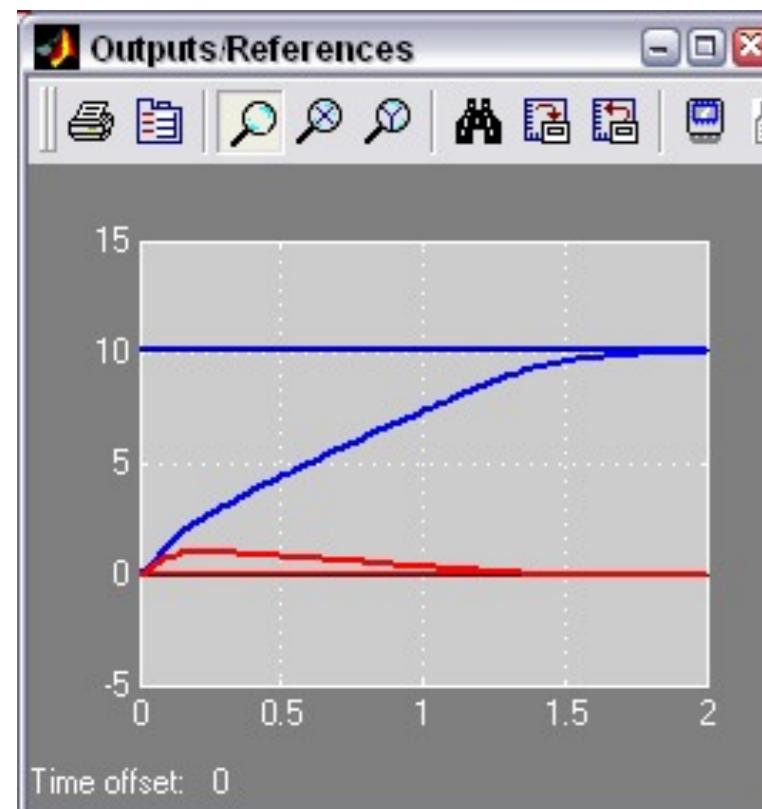
afti16.m

(MPC-Tbx)

Example: AFTI-16

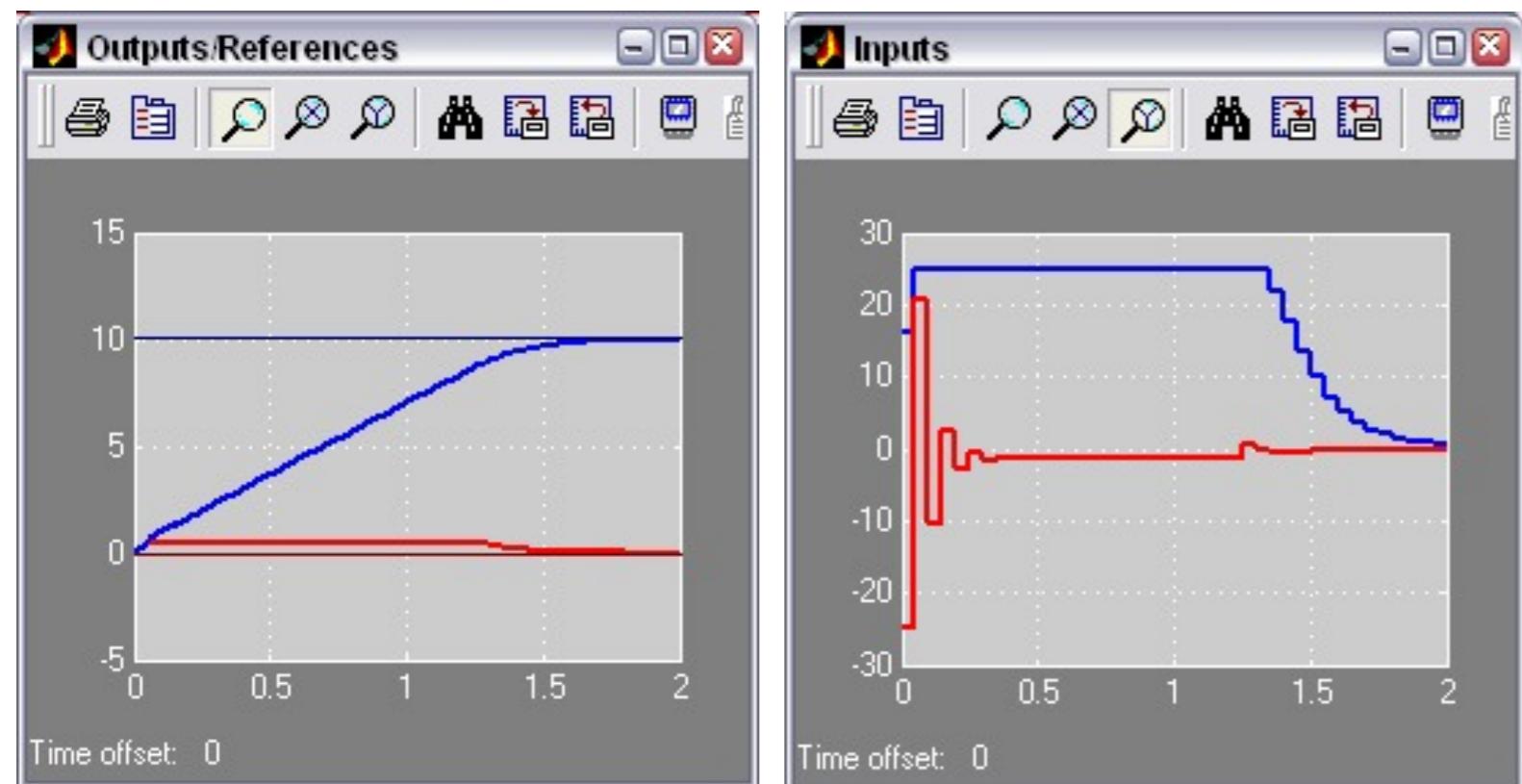


$N_y = 10, N_u = 3,$
 $w_y = \{10, 10\}, w_{\delta u} = \{.01, .01\},$
 $u_{\min} = -25^\circ, u_{\max} = 25^\circ$



$N_y = 10, N_u = 3,$
 $w_y = \{100, 10\}, w_{\delta u} = \{.01, .01\},$
 $u_{\min} = -25^\circ, u_{\max} = 25^\circ$

Example: AFTI-16



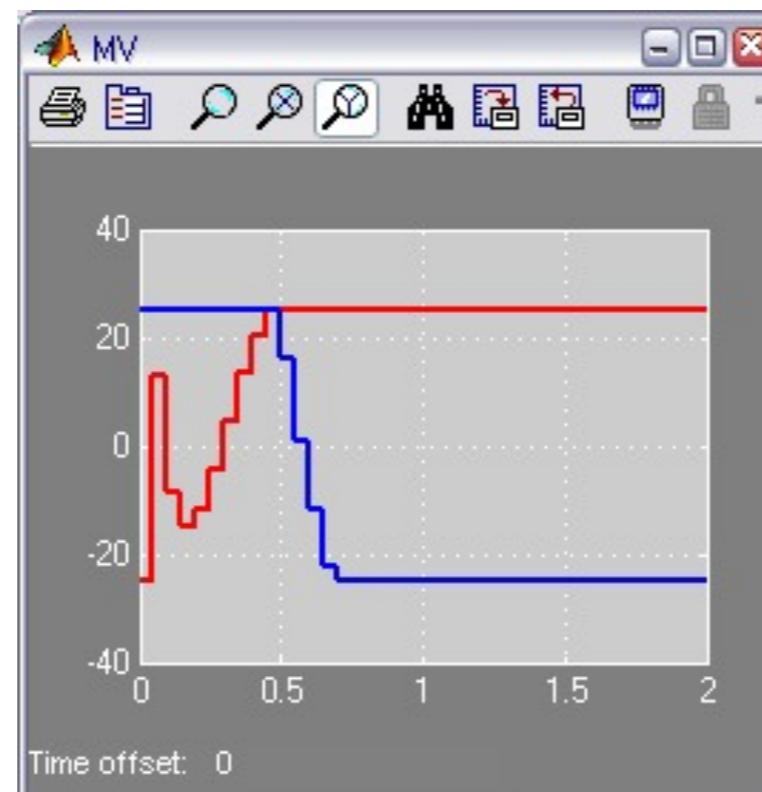
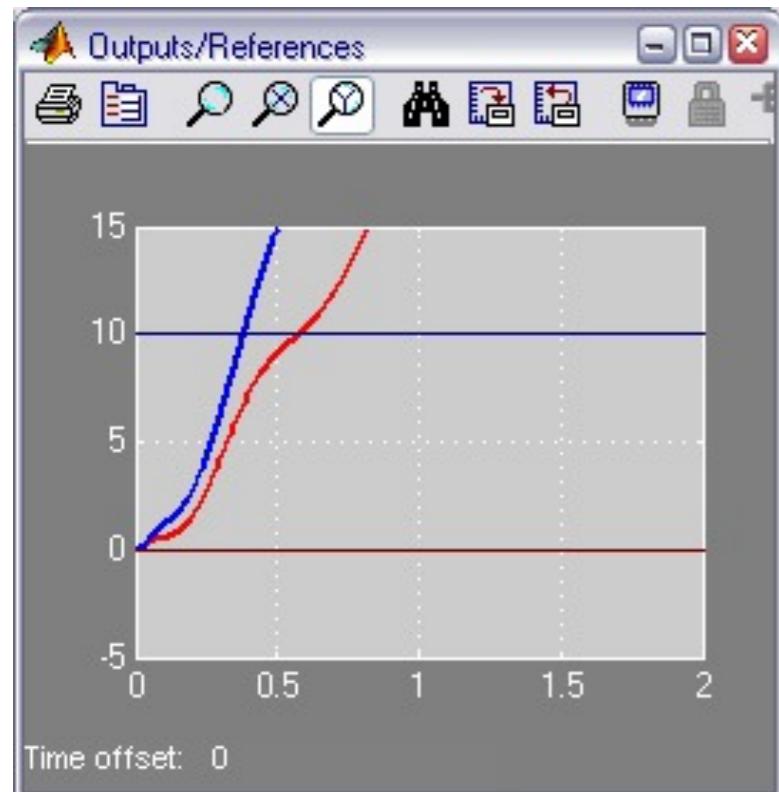
$N_y = 10, N_u = 3,$
 $w_y = \{10, 10\}, w_{\delta u} = \{.01, .01\},$
 $u_{\min} = -25^\circ, u_{\max} = 25^\circ,$
 $y_{1,\min} = -0.5^\circ, y_{1,\max} = 0.5^\circ$

Example: AFTI-16

Unconstrained MPC

(=linear controller, \approx LQR)

+ actuator saturation $\pm 25^\circ$



$$N_y = 10, N_u = 3,$$
$$w_y = \{10, 10\}, w_{\delta u} = \{.01, .01\},$$

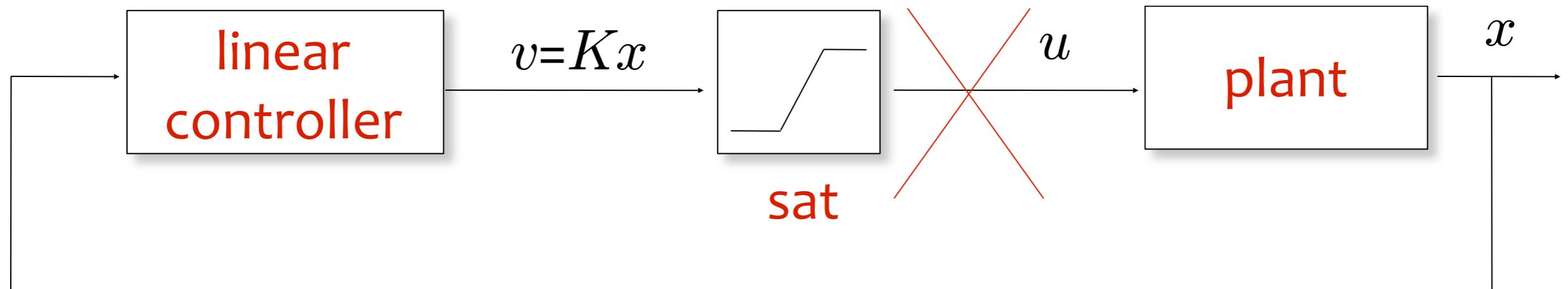


UNSTABLE !!!

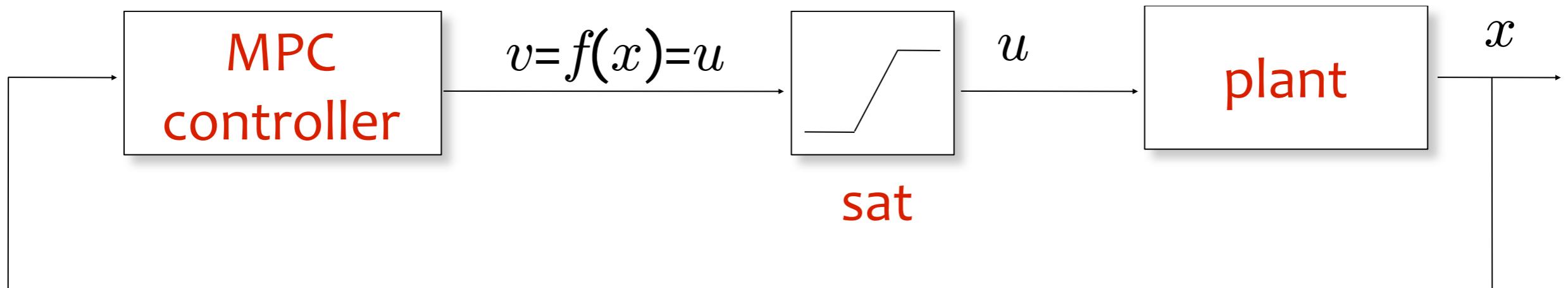
Saturation needs to be considered in the control design !

Saturation

- Saturation needs to be considered in the control design



- MPC takes it into account automatically (and optimally)



Tuning Guidelines

$$\min_{\Delta U} \quad \sum_{k=0}^{N-1} \|W^y(y(t+k+1|t) - r(t))\|^2 + \|W^{\Delta u}\Delta u(t)\|^2$$

subj. to $u_{\min} \leq u(t+k) \leq u_{\max}, \quad k = 0, \dots, N-1$
 $\Delta u_{\min} \leq \Delta u(t+k) \leq \Delta u_{\max}, \quad k = 0, \dots, N_u-1$
 $y_{\min} \leq y(t+k|t) \leq y_{\max}, \quad k = 1, \dots, N$
 $\Delta u(t+k) = 0, \quad k = N_u, \dots, N-1$

- **Weights:** the larger the ratio $W^y \ll W^{\Delta u}$ the more aggressive the controller
- **Input horizon:** the larger N_u , the more “optimal” but the more complex the controller
- **Output horizon:** the smaller N , the more aggressive the controller
- **Limits:** controller less aggressive if $\Delta u_{\min}, \Delta u_{\max}$ are small

Always try to set N_u as small as possible !

Scaling

- Humans think infinite precision ...
- Computers do not !
- Numerical difficulties may arise if variables assume very small or very large values

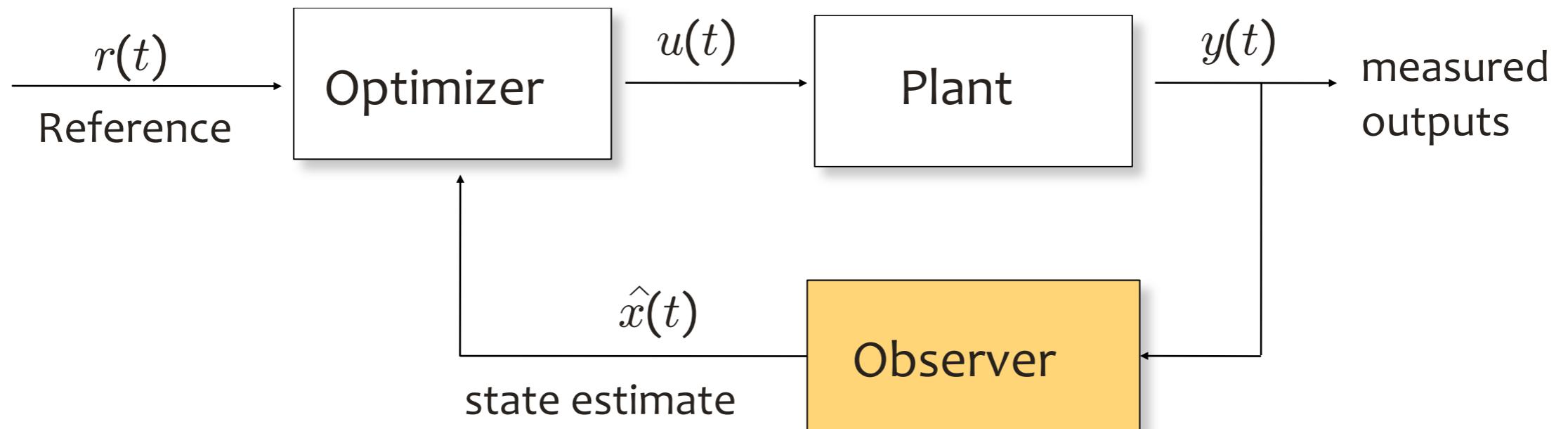
Example: $y_1 \in [-1e-4, 1e-4]$ (V)
 $y_2 \in [-1e4, 1e4]$ (Pa)

use instead: $y_1 \in [-0.1, 0.1]$ (mV)
 $y_2 \in [-10, 10]$ (kPa)

- Ideally all variables should range in $[-1, 1]$. For example, one can replace y with y/y_{\max}

Observer Design in MPC

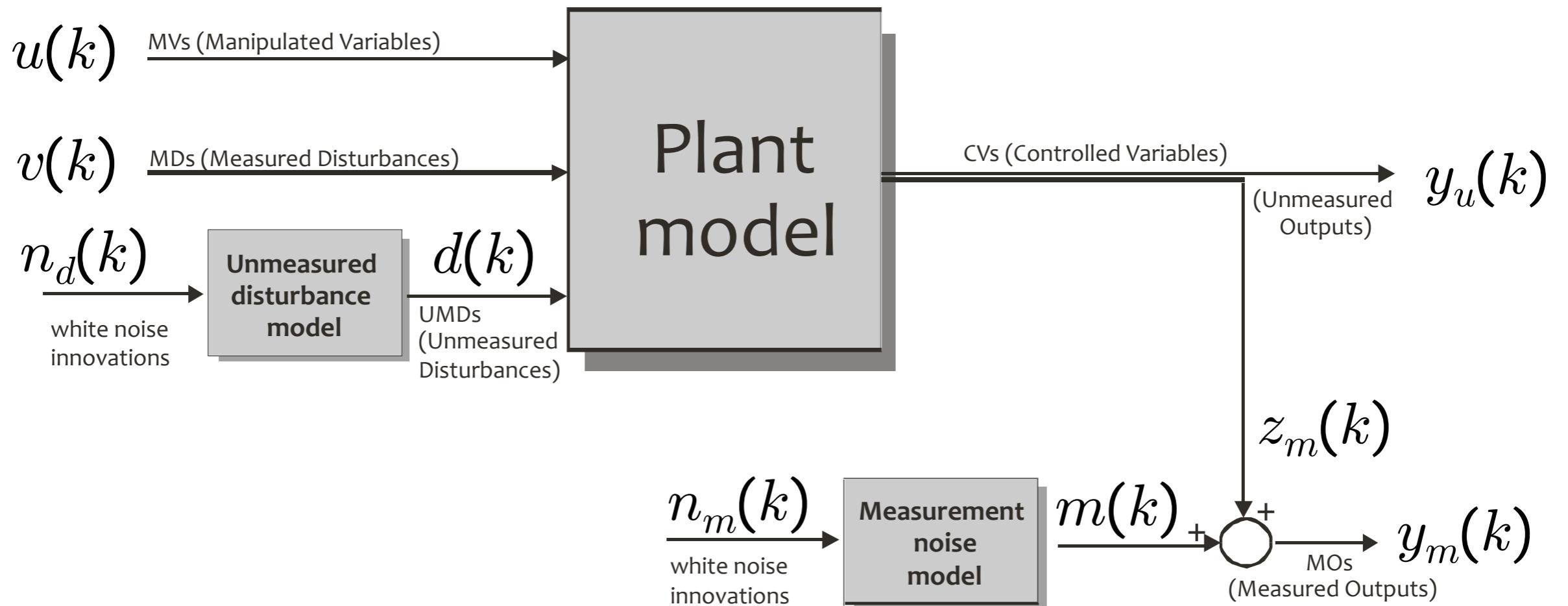
Observer Design for MPC



- Full state $x(t)$ may not be available
- Even if available, noise should be filtered out
- State of prediction model may be different from plant model $x(t)$ (e.g.: model reduction, identification)

we need to use a state observer

Model for Observer Design



unmeasured disturbance model

$$\begin{cases} x_d(k+1) = \bar{A}x_d(k) + \bar{B}n_d(k) \\ d(k) = \bar{C}x_d(k) + \bar{D}n_d(k) \end{cases}$$

measurement noise model

$$\begin{cases} x_m(k+1) = \tilde{A}x_m(k) + \tilde{B}n_m(k) \\ m(k) = \tilde{C}x_m(k) + \tilde{D}n_m(k) \end{cases}$$

- Note: meas. noise model not needed for optimization !

Observer Design

- Measurement update

$$\begin{bmatrix} \hat{x}(k|k) \\ \hat{x}_d(k|k) \\ \hat{x}_m(k|k) \end{bmatrix} = \begin{bmatrix} \hat{x}(k|k-1) \\ \hat{x}_d(k|k-1) \\ \hat{x}_m(k|k-1) \end{bmatrix} + M [y_m(k) - \hat{y}_m(k)]$$

- Time update

$$\begin{aligned} \hat{x}(k+1|k) &= A\hat{x}(k|k) + B_u u(k) + B_v v(k) + B_d \bar{C} \hat{x}_d(k|k) \\ \hat{x}_d(k+1|k) &= \bar{A} \hat{x}_d(k|k) \\ \hat{x}_m(k+1|k) &= \tilde{A} \hat{x}(k|k) \\ \hat{y}_m(k) &= C_m \hat{x}(k|k-1) + D_{vm} v(k) + \\ &\quad D_{dm} \bar{C} \hat{x}_d(k|k-1) + \tilde{C} \hat{x}_m(k|k-1) \end{aligned}$$

- NOTE: **separation principle** holds ! (under certain assumptions)

(Muske, Meadows, Rawlings, ACC94)

Kalman Filter Design



- Full model for designing observer gain M

$$\begin{bmatrix} x(k+1) \\ x_d(k+1) \\ x_m(k+1) \end{bmatrix} = \begin{bmatrix} A & B_d\bar{C} & 0 \\ 0 & \bar{A} & 0 \\ 0 & 0 & \tilde{A} \end{bmatrix} \begin{bmatrix} x(k) \\ x_d(k) \\ x_m(k) \end{bmatrix} + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} u(k) + \begin{bmatrix} B_v \\ 0 \\ 0 \end{bmatrix} v(k) +$$
$$\begin{bmatrix} B_d\bar{D} \\ \bar{B} \\ 0 \end{bmatrix} n_d(k) + \begin{bmatrix} 0 \\ 0 \\ \tilde{B} \end{bmatrix} n_m(k) + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} n_u(k)$$
$$y_m(k) = [C_m \ D_{dm}\bar{C} \ \tilde{C}] \begin{bmatrix} x(k) \\ x_d(k) \\ x_m(k) \end{bmatrix} + D_{vm}v(k) + \bar{D}_m n_d(k) + \tilde{D}_m n_m(k)$$

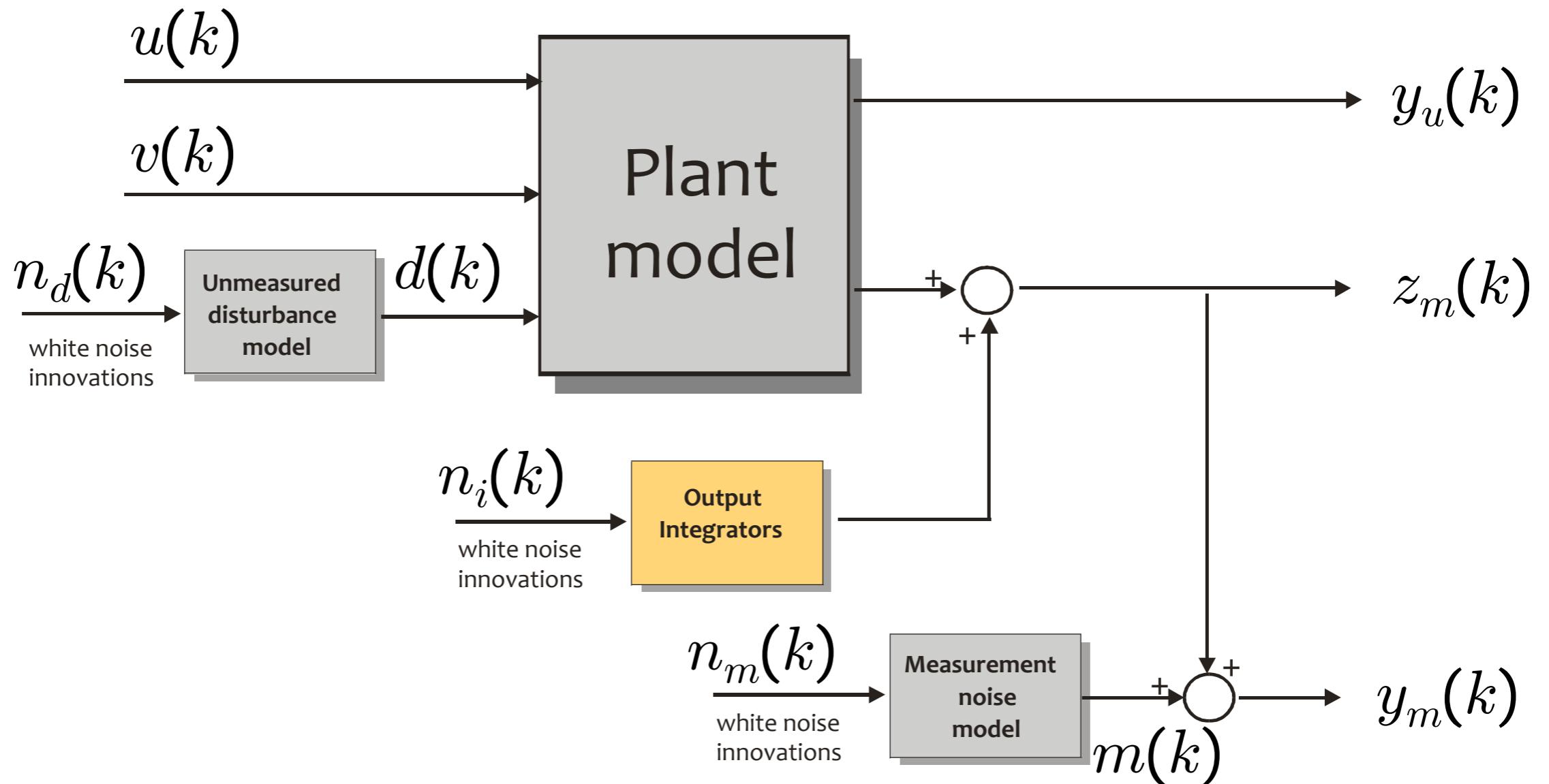
Rudolf Emil
Kalman
(1930 -)

- $n_d(k)$: represents source for modeling errors
- $n_m(k)$: represents source for measurement noise
- $n_u(k)$: white noise on all inputs u added for solvability of the Riccati equation

Integral Action in MPC

(and not only in MPC)

Output Integrators

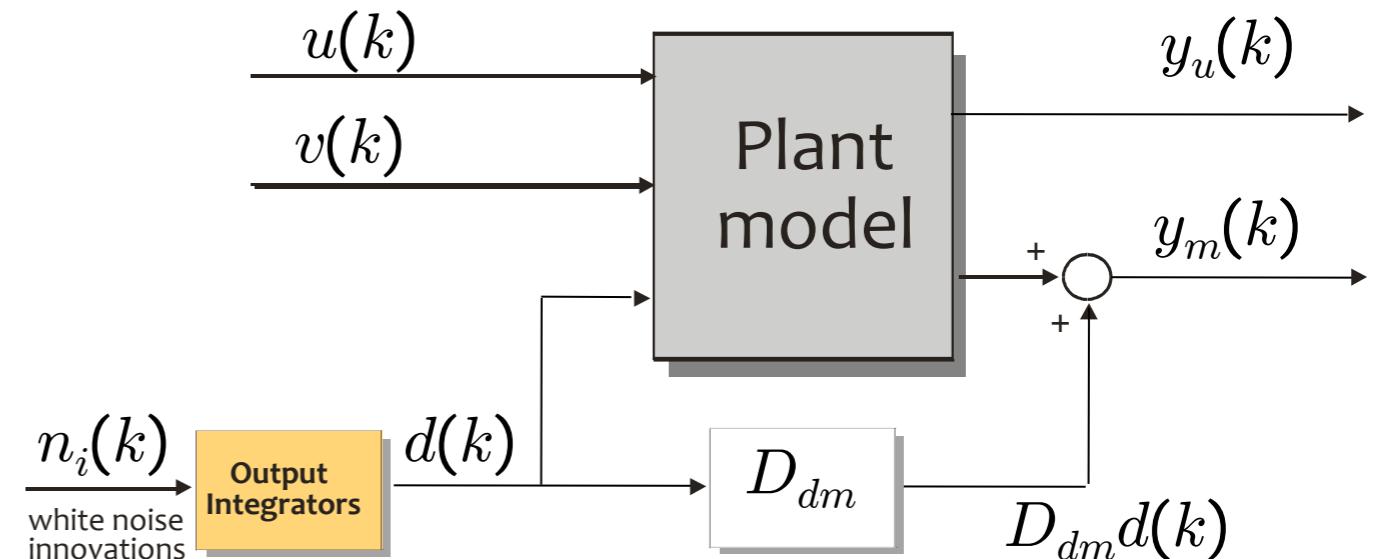


- Introduce **output integrators** as additional disturbance models
- Under certain conditions, observer + controller provide **zero offset** in steady-state

Integrators and Steady-State Offsets

- More generally, add integrators on states + outputs:

$$\begin{cases} x(k+1) = Ax(k) + B_u u(k) + \\ \quad B_v v(k) + B_d d(k) \\ d(k+1) = d(k) \\ y_m(k) = C_m x(k) + D_{vm} v(k) + \\ \quad D_{dm} d(k) \end{cases}$$



$$u \in \mathbb{R}^m, \quad y_m \in \mathbb{R}^p, \quad x \in \mathbb{R}^n$$

- Use the above model + meas.noise model to design an observer (e.g. Kalman filter)
 - Main idea: observer makes
MPC makes
 \Rightarrow the combination makes
 - Explanation: $D_{dm}\hat{d}$ compensates model mismatch in steady-state
- $y_m - (C_m\hat{x} + D_{dm}\hat{d}) \rightarrow 0$ (estimation error)
 $C_m\hat{x} + D_{dm}\hat{d} \rightarrow r$ (predicted tracking error)
 $y_m \rightarrow r$ (actual tracking error)

Error feedback

- Idea: add integrals of measured outputs as additional states (similar to linear state-feedback case) (Kwakernaak, 1972)

- Extended prediction model:

$$\begin{bmatrix} x(k+1) \\ q(k+1) \\ r(k+1) \end{bmatrix} = \begin{bmatrix} A & 0 & 0 \\ C & I & -I \\ 0 & 0 & I \end{bmatrix} \begin{bmatrix} x(k) \\ q(k) \\ r(k) \end{bmatrix} + \begin{bmatrix} B \\ 0 \\ 0 \end{bmatrix} u(k)$$
$$y(k) = [C \ 0 \ 0] \begin{bmatrix} x(k) \\ q(k) \\ r(k) \end{bmatrix}$$

- Implementation:

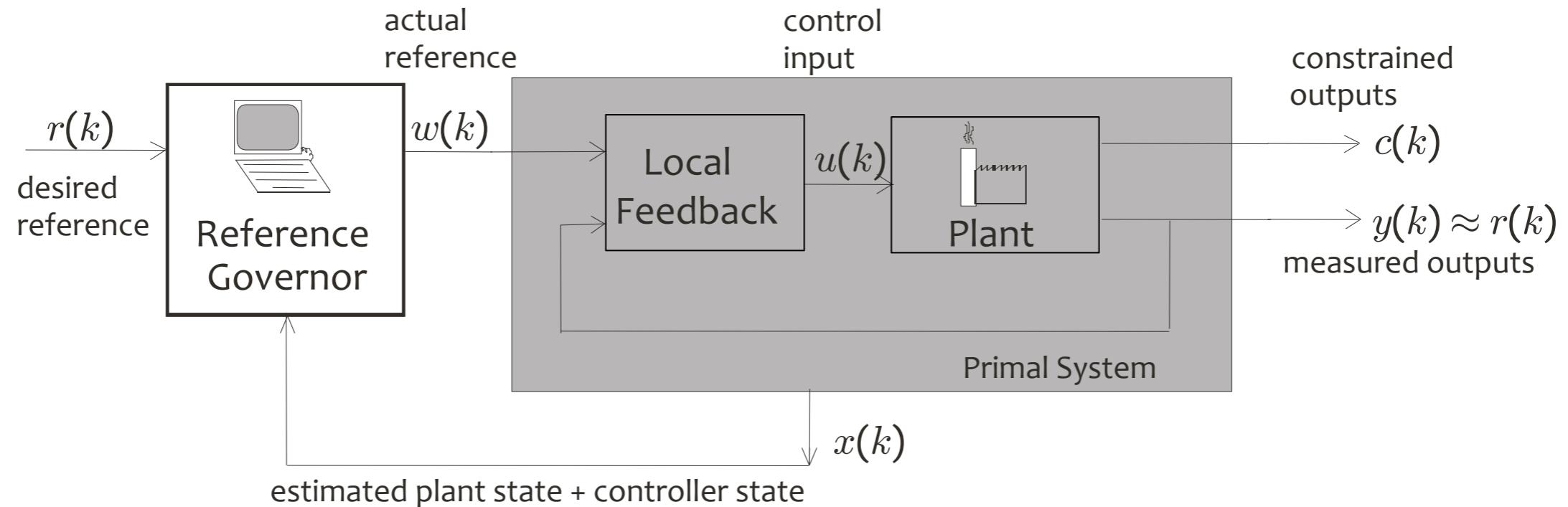
$$q(k+1) = q(k) + [y(k) - r(k)]$$

$$u(k) = f_{\text{MPC}} \left(\begin{bmatrix} x(k) \\ q(k) \\ r(k) \end{bmatrix} \right)$$

- Explanation: if closed-loop asymptotically stable $\Rightarrow q(k) \rightarrow \text{cost.}$ and hence $y(k) \rightarrow r(k)$

Reference Governor

- Idea: Apply MPC as the set-point generator to linear feedback loops (e.g.: PID) (Bemporad, 1997)



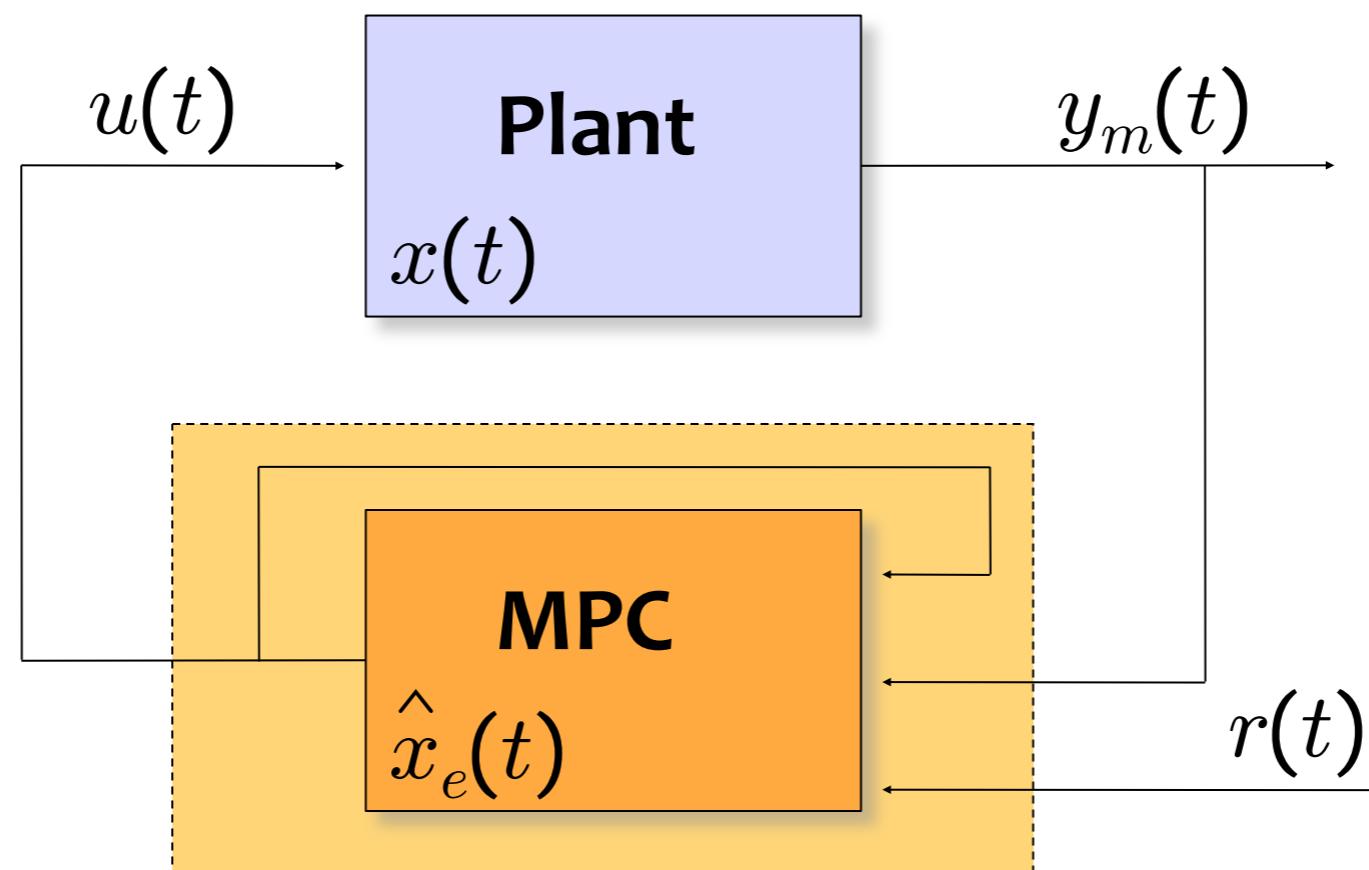
- Separation of problems:
 - Local feedback designed for stability, disturbance attenuation, good tracking, *without taking care of constraints*
 - Actual reference $w(t)$ generated on-line by an MPC algorithm *to take care of constraints*

Objective:

$$\begin{aligned} & \min_w \quad \|w - r\| \\ \text{s.t.} \quad & \text{constraints} + \text{closed-loop dynamics} \end{aligned}$$

MPC frequency analysis (inactive constraints)

- Unconstrained MPC gain + linear observer = linear dynamical system (= 2 d.o.f. dynamic controller)
- Closed-loop MPC analysis can be performed using standard frequency-domain tools (e.g. Bode plots for sensitivity analysis)



In MPC Tbx: `ss (mpc)` or `tf (mpc)` return the LTI discrete-time form of the linearized (=no constraints) MPC object

Controller matching problem

(Di Cairano, Bemporad,

ECC'09)

- Given the controller $u=Kx$, **find weights** Q, R, P for the MPC problem such that

$$-\begin{bmatrix} I & 0 & \dots & 0 \end{bmatrix} H^{-1} F = K_{fv}$$

that is, the **MPC controller coincides with K_{fv}** when the constraints are **not active**

- QP matrices: $H = (\mathcal{R} + \mathcal{S}' \mathcal{Q} \mathcal{S}), \quad F = \mathcal{T}' \mathcal{Q} \mathcal{S}$

$$\begin{array}{ll} \min_U & \frac{1}{2} U' H U + x'(t) F' U + \frac{1}{2} x(t) Y x(t) \\ \text{subj. to} & G U \leq W + S x(t), \end{array}$$

$$\mathcal{S} = \begin{bmatrix} B & 0 & \dots & 0 \\ AB & B & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ A^{N-1}B & A^{N-2}B & \dots & B \end{bmatrix} \quad \mathcal{Q} = \begin{bmatrix} Q & 0 & 0 & \dots & 0 \\ 0 & Q & 0 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots & \vdots \\ 0 & 0 & \dots & Q & 0 \\ 0 & 0 & \dots & 0 & P \end{bmatrix}$$
$$\mathcal{T} = \begin{bmatrix} A \\ A^2 \\ \vdots \\ A^N \end{bmatrix} \quad \mathcal{R} = \begin{bmatrix} R & 0 & \dots & 0 \\ 0 & R & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & R \end{bmatrix}$$

Controller matching problem - Example

- Open-loop process:

$$y(k) = 1.8y(k-1) + 1.2y(k-2) + u(k-1)$$

- Constraints: $-24 \leq u(k) \leq 24$

- Desired controller (**PID**): $K_I = 0.248, K_P = 0.752, K_D = 2.237$

$$u(k) = -\left(K_I \mathcal{I}(k) + K_P y(k) + \frac{K_D}{T_s} (y(k) - y(k-1)) \right)$$
$$\mathcal{I}(k) = \mathcal{I}(k-1) + T_s y(k)$$

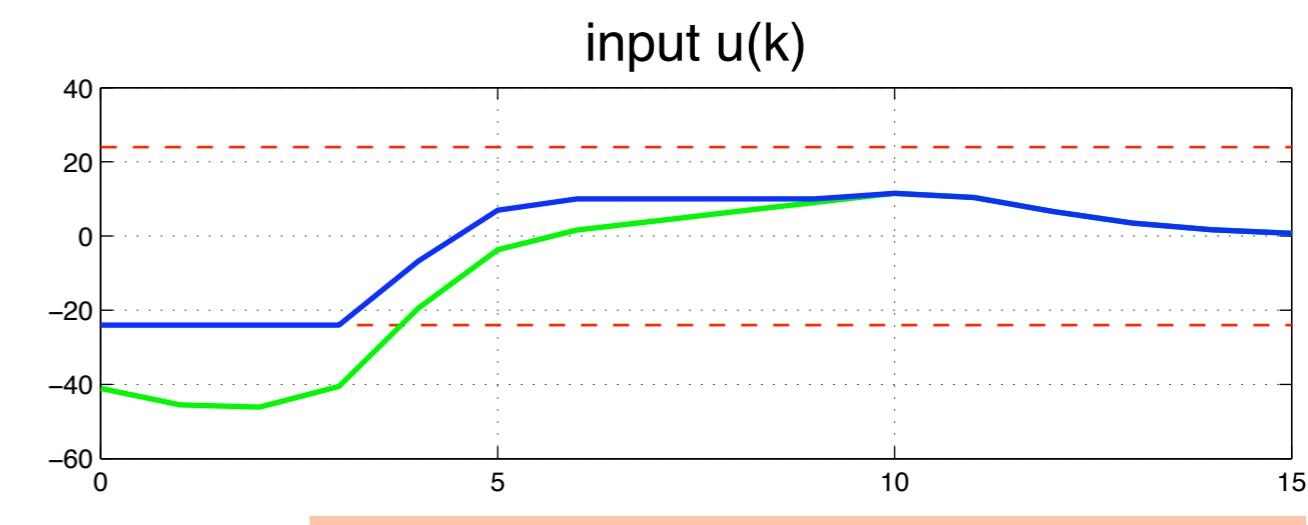
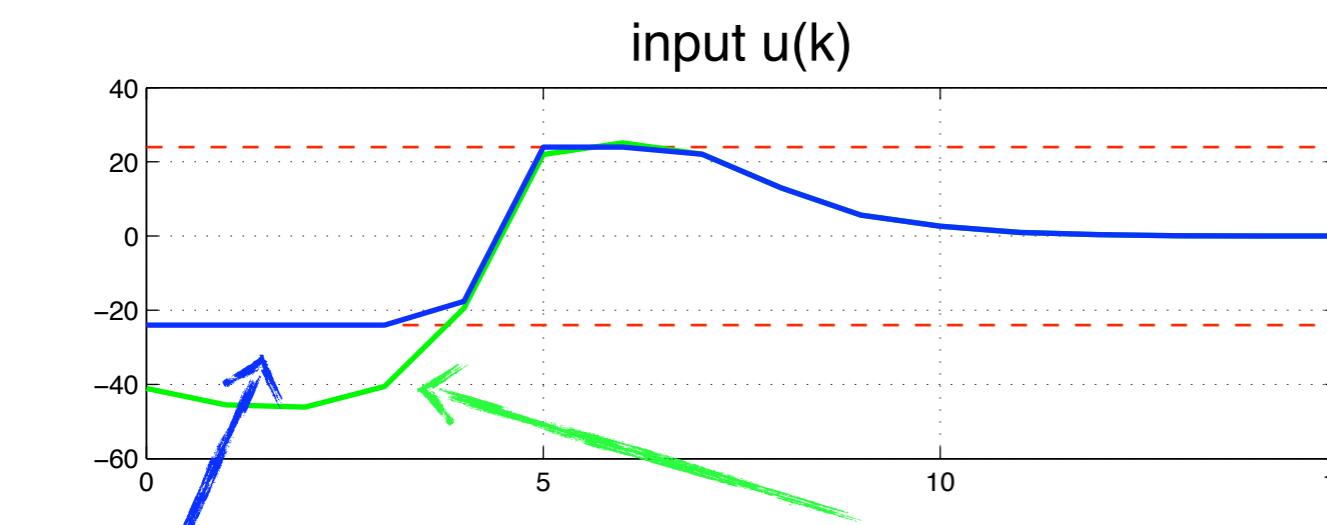
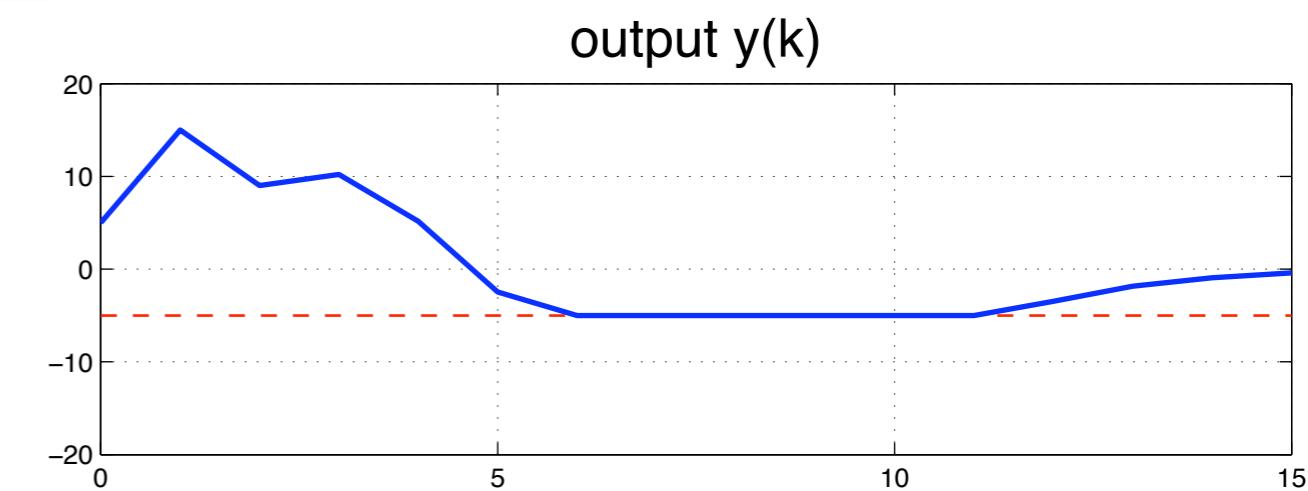
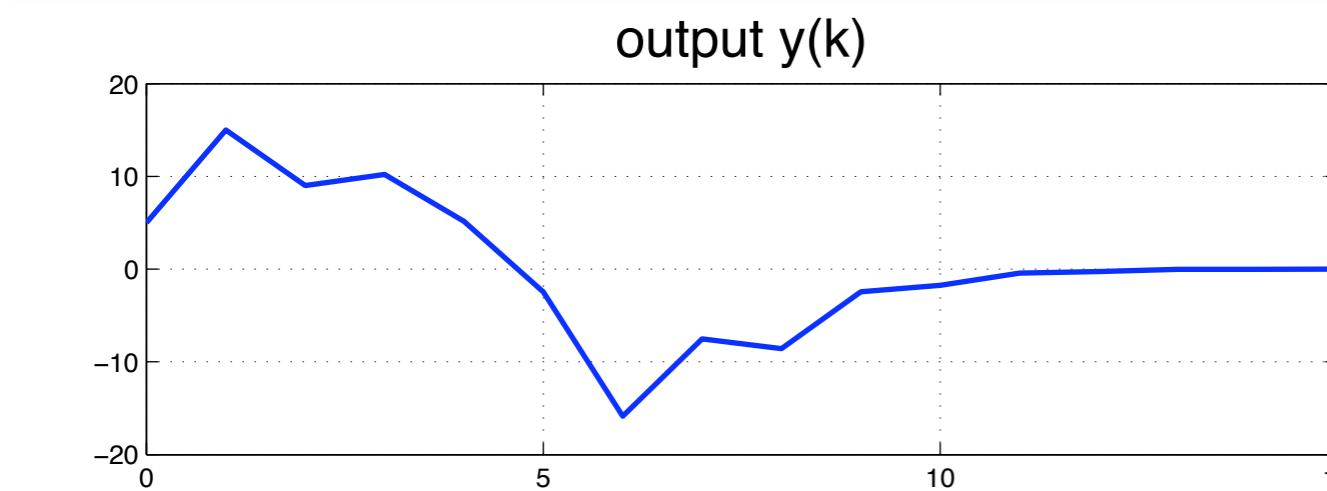
- State-space form:

$$x(k) = \begin{bmatrix} y(k-1) \\ y(k-2) \\ \mathcal{I}(k-1) \\ u(k-1) \end{bmatrix}$$

controller
matching
based on
inverse LQR

$$Q^* = \begin{bmatrix} 6.401 & 0.064 & -0.001 & 0.020 \\ 0.064 & 6.605 & 0.006 & 0.080 \\ -0.001 & 0.006 & 6.647 & -0.020 \\ 0.019 & 0.080 & -0.020 & 6.378 \end{bmatrix}$$
$$R^* = 1$$
$$P^* = \begin{bmatrix} 422.7 & 241.7 & 50.39 & 201.4 \\ 241.7 & 151.0 & 32.13 & 120.4 \\ 50.39 & 32.13 & 19.85 & 26.75 \\ 201.4 & 120.4 & 26.75 & 106.6 \end{bmatrix}$$

Controller matching problem - Example



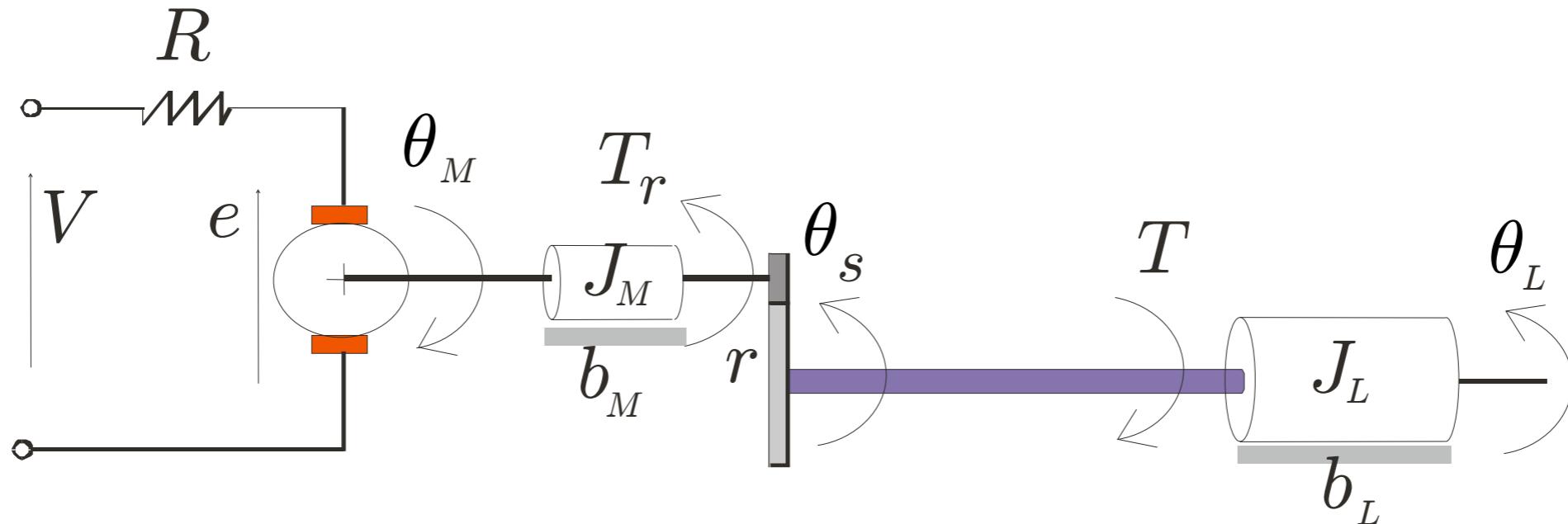
what PID would apply

matched MPC

add output constraint $y(k) \geq -5$

Note: it's not trivially a saturation of PID controller. In this case $\text{sat}(\text{PID})$ leads to instability

Example: MPC of a DC Servomotor



Symbol	Value (MKS)	Meaning
L_S	1.0	shaft length
d_S	0.02	shaft diameter
J_S	negligible	shaft inertia
J_M	0.5	motor inertia
β_M	0.1	motor viscous friction coefficient
R	20	resistance of armature
K_T	10	motor constant
ρ	20	gear ratio
k_θ	1280.2	torsional rigidity
\hat{J}_L	$20J_M$	nominal load inertia
β_L	25	load viscous friction coefficient

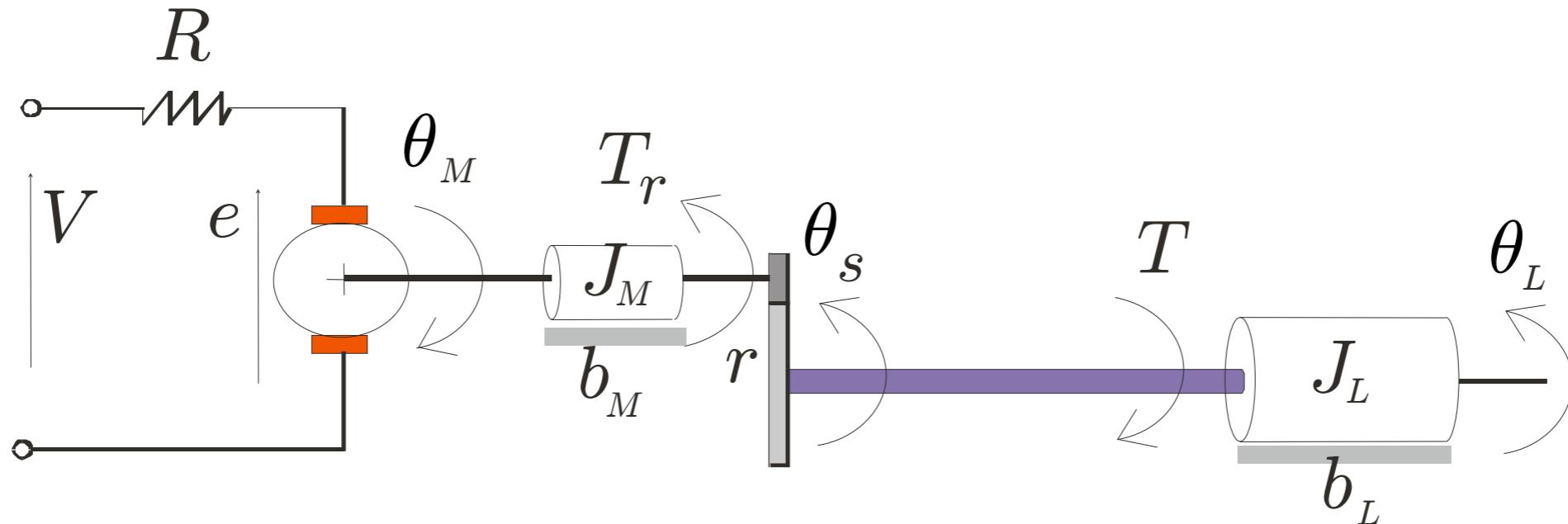
go to demo **/demos/linear/dcmotor.m**

(Hyb-Tbx)

mpcmotor.m

(MPC-Tbx)

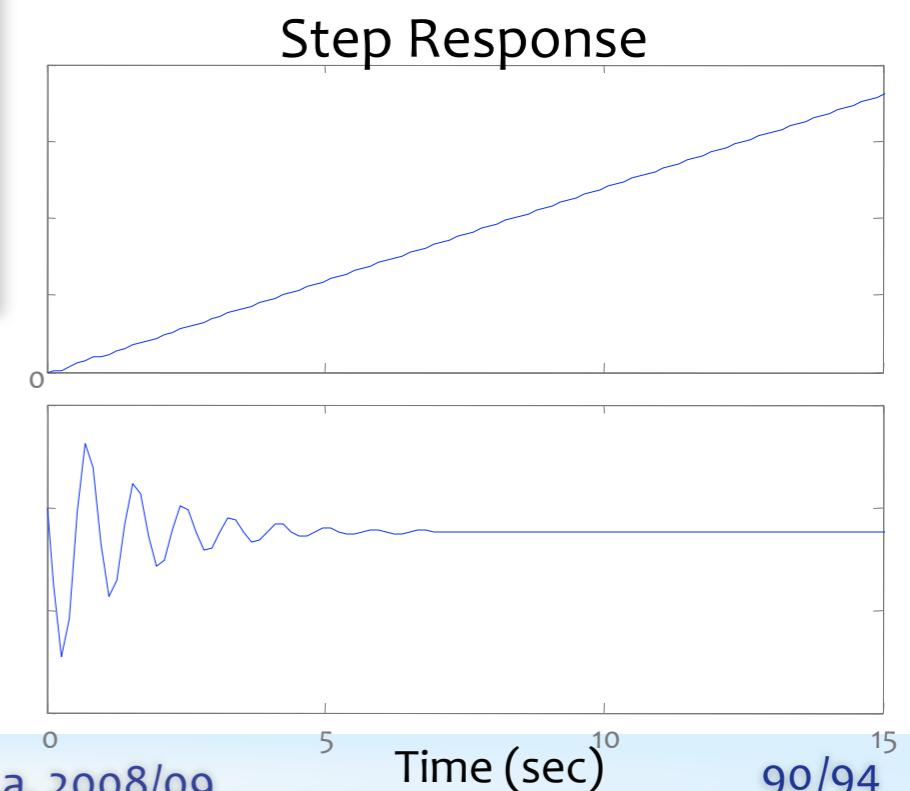
DC Servomotor - Model



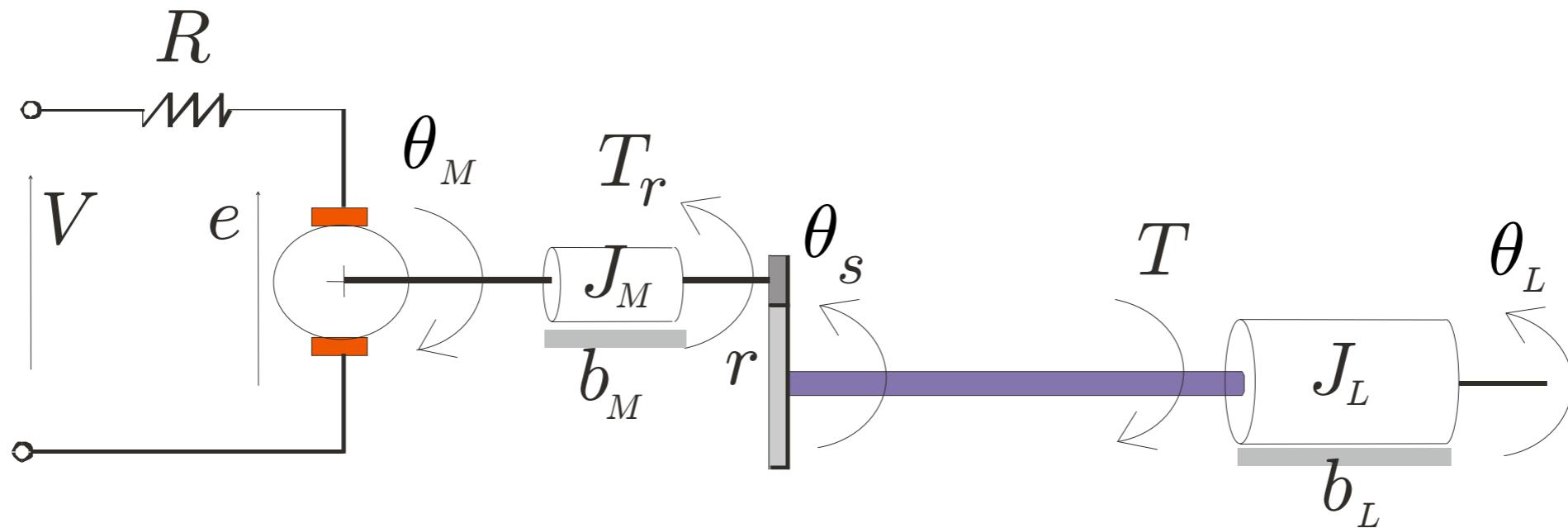
$$\dot{x} = \begin{bmatrix} 0 & 1 & 0 & 0 \\ -\frac{k_\theta}{J_L} & -\frac{\beta_L}{J_L} & \frac{k_\theta}{\rho J_L} & 0 \\ 0 & 0 & 0 & 1 \\ \frac{k_\theta}{\rho J_M} & 0 & -\frac{k_\theta}{\rho^2 J_M} & -\frac{\beta_M + k_T^2/R}{J_M} \end{bmatrix} x + \begin{bmatrix} 0 \\ 0 \\ 0 \\ \frac{k_T}{R J_M} \end{bmatrix} V$$

$$\theta_L = [1 \ 0 \ 0 \ 0] x$$

$$T = [k_\theta \ 0 \ -\frac{k_\theta}{\rho} \ 0] x$$



DC Servomotor: Specs



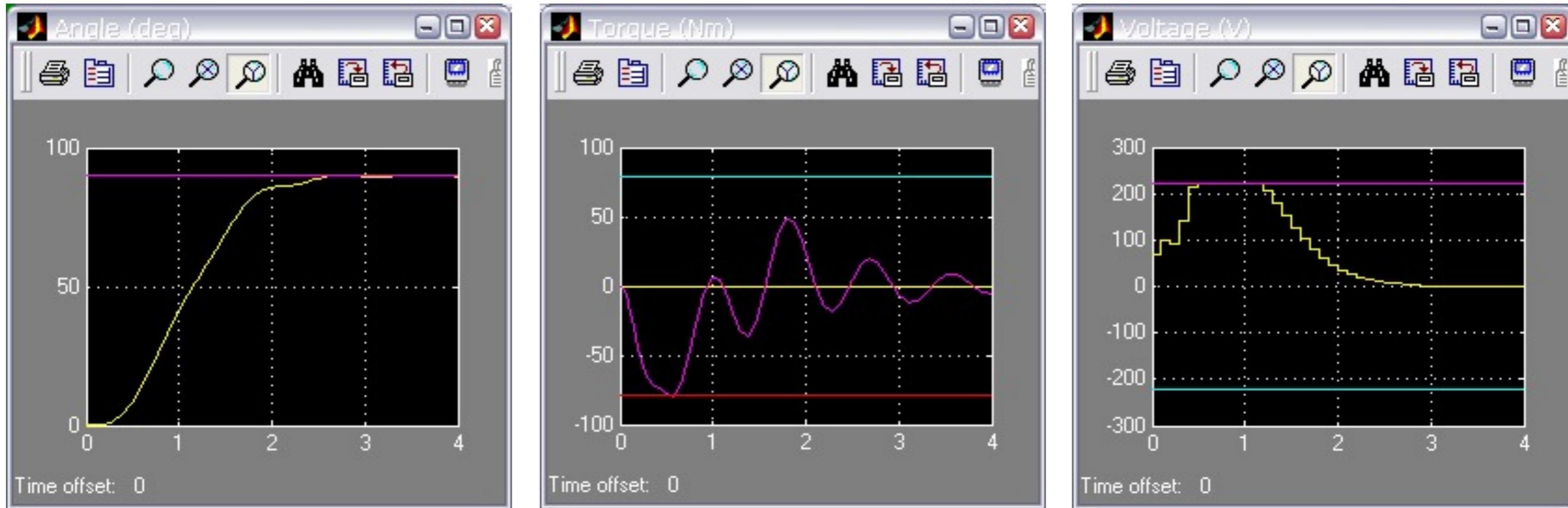
- Finite shear strength of steel shaft ($\tau_{adm} = 50 \text{ N/mm}^2$)
 $\Rightarrow |T| \leq 78.5398 \text{ Nm}$
- DC voltage limits $|V| \leq 220 \text{ V}$
- Sampling time: $T_s = .1 \text{ s}$ (+ zero-order hold)

DC Servomotor: Exercise

Design a model predictive controller for tracking an angle reference step signal r . Assume that only the position θ_L is measured.

- Try unconstrained MPC (no voltage and torque constraints) for tracking $r = \frac{\pi}{2}$ rad. Tune the controller to fulfill voltage and torque constraints. What happens if you change the reference signal to $r = \pi$ rad ?
- Tune a constrained MPC for $r = \frac{\pi}{2}$ rad. What happens if you change the reference signal to $r = \pi$ rad ? And $r(t) = 2\pi \sin(0.4t)$ rad ?
- Try different numbers of control moves M and prediction horizons P . What happens for increasing M ? For increasing P ? What happens if P/M are too small ? Look for the smallest M which provides a reasonably good performance.

DC Servomotor: MPC



$$r(t) \equiv 90 \text{ deg}$$

$$\begin{array}{ll} N & = 10 \\ w_y & = \{10, 0\} \end{array}$$

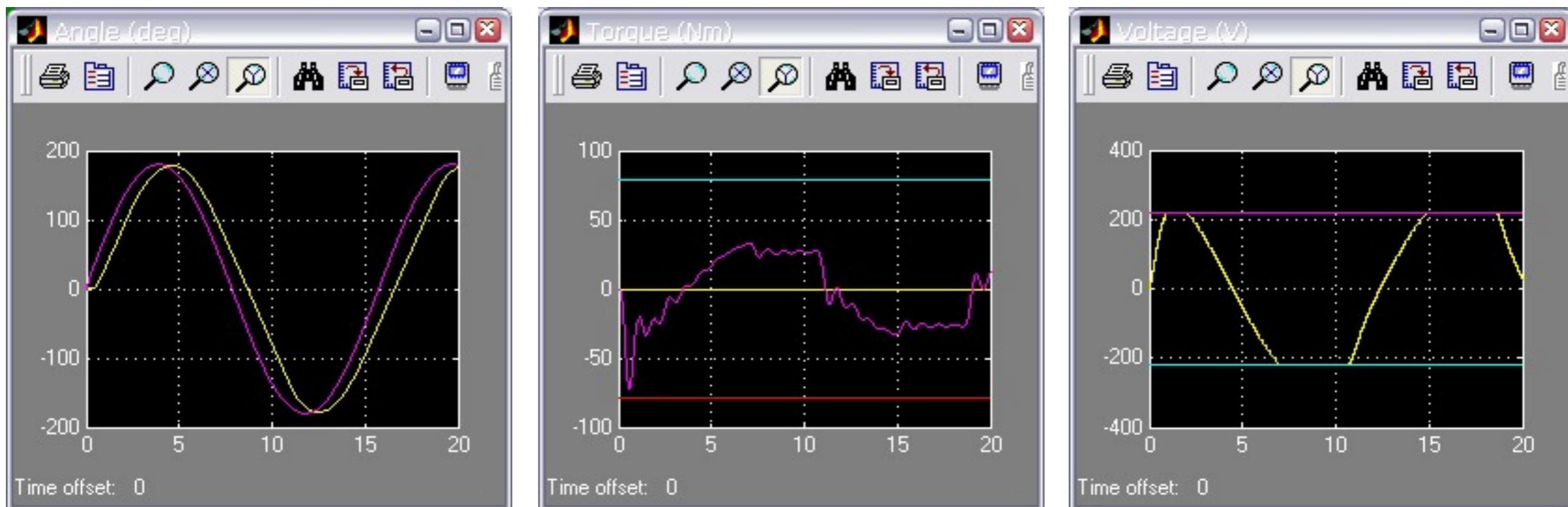
$$u_{\min} = -220 \text{ V}$$

$$y_{\min} = \{-\infty, -78.5398\} \text{ Nm} \quad y_{\max} = \{\infty, 78.5398\} \text{ Nm}$$

$$\begin{array}{ll} N_u & = 3 \\ w_{\delta u} & = .05 \\ w_u & = 0 \end{array}$$

$$u_{\max} = 220 \text{ V}$$

DC Servomotor: MPC



$$r(t) = 180 \sin(0.4t) \text{ deg}$$

$$N = 10$$

$$w_y = \{10, 0\}$$

$$u_{\min} = -220 \text{ V}$$

$$y_{\min} = \{-\infty, -78.5398\} \text{ Nm} \quad y_{\max} = \{\infty, 78.5398\} \text{ Nm}$$

$$N_u = 3$$

$$w_{\delta u} = .05$$

$$u_{\max} = 220 \text{ V}$$

$$w_u = 0$$