

1. CONVECTIVE HEAT TRANSFER

As conveniently expressed by **Newton's law of cooling**, the rate of convection heat transfer is observed to be **proportional** to the **temperature difference**. Newton's law states that:

The rate of heat loss of a body is directly proportional to the difference in the temperatures between the body and its surroundings provided the temperature difference is small and the nature of radiating surface remains same.

$$\dot{Q}_{\text{conv}} = \frac{T_s - T_\infty}{R_{\text{conv}}} \text{ [W]}$$

$$R_{\text{conv}} = \frac{1}{h \cdot A_s}$$

$$\dot{Q} = h \cdot A_s \cdot \Delta T$$

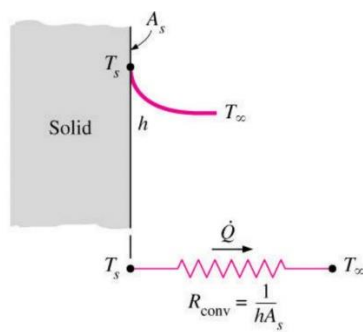
where

q is the local heat flux density [$\text{W} \cdot \text{m}^{-2}$]

h is the heat transfer coefficient [$\text{W} \cdot \text{m}^{-2} \cdot \text{K}$]

ΔT is the temperature difference [K]

Note that, ΔT is given by the surface or **wall temperature**, T_{wall} and the **bulk temperature**, T_∞ , which is the temperature of the fluid sufficiently far from the surface.



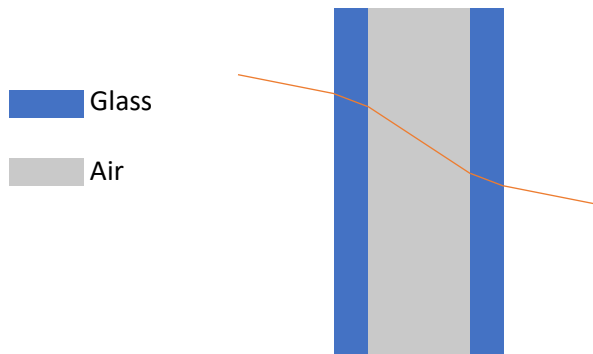
Electrical Analogy

$$R_{\text{total}} = R_{\text{conv1}} + R_{\text{wall}} + R_{\text{conv2}} = \frac{1}{h_i \cdot A} + \frac{1}{K \cdot A} + \frac{1}{h_o \cdot A} \quad [^\circ\text{C/W}]$$

According to this relation, it's possible to say that the temperature drop through a surface is proportional to its thermal resistance.

2.

2. Solve the same problem as that of double pane window with the air-gap thickness of 13 mm and glass thickness of 6 mm, comment on your results and explain why we have an optimal range for the air-gap's distance. Consider a 0.8-m-high and 1.5-m-wide double-pane window consisting of two 4-mm-thick layers of glass ($k=0.78 \text{ W/m} \cdot ^\circ\text{C}$) separated by a 10-mm-wide stagnant air space ($k=0.026 \text{ W/m} \cdot ^\circ\text{C}$).



$$R_{\text{conv1}} = \frac{1}{h \cdot A} = \frac{1}{10 \frac{\text{W}}{\text{m}^2 \cdot ^\circ\text{C}} \cdot 1,2 \text{ m}^2} = 0,0833^\circ\text{C/W}$$

$$R_{\text{glass 1,2}} = \frac{l}{k \cdot A} = \frac{0,006}{0,78 \frac{\text{W}}{\text{m} \cdot ^\circ\text{C}} \cdot 1,2 \text{ m}^2} = 0,0064^\circ\text{C/W}$$

$$R_{\text{air1,2}} = \frac{l}{k \cdot A} = \frac{0,013}{0,026 \frac{\text{W}}{\text{m} \cdot ^\circ\text{C}} \cdot 1,2 \text{ m}^2} = 0,416^\circ\text{C/W}$$

$$R_{\text{conv2}} = \frac{1}{h \cdot A} = \frac{1}{40 \frac{\text{W}}{\text{m}^2 \cdot ^\circ\text{C}} \cdot 1,2 \text{ m}^2} = 0,0208^\circ\text{C/W}$$

$$R_{\text{total}} = R_{\text{conv1}} + R_{\text{glass1}} + R_{\text{air}} + R_{\text{glass2}} + R_{\text{conv2}} = 0.5265^\circ\text{C/W}$$

Determine the steady rate of heat transfer through this double-pane window and the temperature of its inner surface.

$$\dot{Q}_{\text{conv}} = \frac{T_s - T_x}{R_{\text{conv}}} = \frac{20^\circ\text{C} - (-10)}{0,5265^\circ\text{C/W}} = 56,98 \text{ W}$$

$$\dot{Q}_{\text{conv}} = \frac{T_s - T_x}{R_{\text{conv}}} = \frac{20^\circ\text{C} - T_i}{0,0833^\circ\text{C/W}};$$

$$56,98 \text{ W} = \frac{20^\circ\text{C} - T_i}{0,0833^\circ\text{C/W}};$$

$$56,98 \text{ W} * 0,0833 \text{ }^{\circ}\text{C/ W} = 20^{\circ}\text{C} - T_1$$

$$T_1 = (20 - 4.74) \text{ }^{\circ}\text{C}$$

$$T_1 = 15.25 \text{ }^{\circ}\text{C}$$

$$\dot{Q}_{\text{glass1}} = \frac{T_s - T_x}{R_{\text{conv}}} = \frac{15.25^{\circ}\text{C} - T_{\text{,,}}}{0,0064^{\circ}\text{C/W}};$$

$$56,98 \text{ W} = \frac{15.25^{\circ}\text{C} - T_{\text{,}}}{0,0064^{\circ}\text{C/W}};$$

$$56,98 \text{ W} * 0,0064 \text{ }^{\circ}\text{C/ W} = 15,25^{\circ}\text{C} - T_1$$

$$T_1 = (15,25 - 0,364) \text{ }^{\circ}\text{C}$$

$$T_1 = 14.89 \text{ }^{\circ}\text{C}$$

$$\dot{Q}_{\text{wall}} = \frac{T_s - T_x}{R_{\text{conv}}} = \frac{14,89^{\circ}\text{C} - T_{\text{,,,}}}{0,416^{\circ}\text{C/W}};$$

$$56,98 \text{ W} = \frac{14,89^{\circ}\text{C} - T_{\text{,}}}{0,416^{\circ}\text{C/W}};$$

$$56,98 \text{ W} * 0,416 \text{ }^{\circ}\text{C/ W} = 14,89^{\circ}\text{C} - T_1$$

$$T_1 = (14,89 - 23,70) \text{ }^{\circ}\text{C}$$

$$T_1 = -8.81 \text{ }^{\circ}\text{C}$$

$$\dot{Q}_{\text{glass2}} = \frac{T_s - T_x}{R_{\text{conv}}} = \frac{-8.81^{\circ}\text{C} - T_{\text{,,,,}}}{0,0064^{\circ}\text{C/W}};$$

$$56,98 \text{ W} = \frac{-8,81^{\circ}\text{C} - T_{\text{,}}}{0,0064^{\circ}\text{C/W}};$$

$$56,98 \text{ W} * 0,0064 \text{ }^{\circ}\text{C/ W} = -8,81^{\circ}\text{C} - T_1$$

$$T_1 = (-8,81 - 0,364) \text{ }^{\circ}\text{C}$$

$$T_1 = -9.17 \text{ }^{\circ}\text{C}$$