Finite Difference Solution for 2D Flow with Temperature-Dependent Viscosity

1 Governing Equations

We consider the laminar flow of a viscous fluid where momentum inertia is neglected, and velocity is primarily in the *x*-direction. The governing equations are:

1.1 Momentum Equation (Stokes Flow)

The *x*-momentum equation simplifies to:

$$0 = -\frac{\partial p}{\partial x} + \frac{\partial}{\partial y} \left(\eta \frac{\partial u}{\partial y} \right). \tag{1}$$

where $\eta = \eta(T)$ is the temperature-dependent viscosity.

1.2 Energy Equation

The energy equation includes convection, diffusion, and viscous dissipation:

$$\rho C_p \left(\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} \right) = k \frac{\partial^2 T}{\partial y^2} + \Phi, \tag{2}$$

where the viscous dissipation function is given by:

$$\Phi = \eta \left(\frac{\partial u}{\partial y}\right)^2. \tag{3}$$

2 Finite Difference Discretization

We discretize the equations using a finite difference approach.

2.1 Velocity Computation

Using a simple centered difference scheme, we approximate the velocity profile:

$$u_{j} = \left(\frac{\frac{\partial p}{\partial x}}{\eta}\right) \frac{\Delta y^{2}}{2} j(N_{y} - j). \tag{4}$$

2.2 Temperature Evolution

Using an explicit finite difference scheme, the temperature update equation is:

$$T_{i}^{j} = T_{i}^{j} + \Delta t \left[\alpha \left(\frac{T_{i+1,j} - 2T_{i,j} + T_{i-1,j}}{\Delta x^{2}} + \frac{T_{i,j+1} - 2T_{i,j} + T_{i,j-1}}{\Delta y^{2}} \right) - u_{j} \frac{T_{i,j} - T_{i-1,j}}{\Delta x} + \frac{\Phi}{\rho C_{p}} \right].$$
(5)

3 Python Implementation

The following Python code implements the finite difference solution:

```
import numpy as np
  import matplotlib.pyplot as plt
4 # Grid parameters
_{5} Nx = 50 # Number of x points
  Ny = 50 # Number of y points
  Lx = 1.0 \# Length in x direction
8 Ly = 1.0 # Length in y direction
  dx = Lx / (Nx - 1)

dy = Ly / (Ny - 1)
12 # Physical parameters
p0 = 1.0 # Pressure at x0
p1 = 0.0 # Pressure at x1

p1 = 300.0 # Boundary temperature at y0 and y1
16 rho = 1.0 # Density
17 Cp = 1.0 # Specific heat
18 k = 1.0 # Thermal conductivity
19 eta0 = 1.0 # Reference viscosity
  b = 0.01 # Viscosity temperature dependence coefficient
22 # Initialize grids
27 dpdx = (p1 - p0) / Lx
28
29
  for j in range(1, Ny - 1):
      eta_avg = (eta0 * np.exp(-b * Tb)) # Approximate viscosity
31
      u[j] = (dpdx / eta_avg) * (dy**2 / 2) * (j * (Ny - j)) # Parabolic
35 T_new = np.copy(T)
  dt = 0.01 # Time step for stability
37
  alpha = k / (rho * Cp) # Thermal diffusivity
  for it in range(1000): # Time stepping
39
      T_new[:, 0] = Tb # Boundary condition at y0
      T_new[:, -1] = Tb # Boundary condition at y1
41
```

```
for i in range(1, Nx - 1):
43
            for j in range(1, Ny - 1):
    # Compute viscosity at this location
44
45
                eta = eta0 * np.exp(-b * T[i, j])
47
48
                Phi = eta * ( (u[j+1] - u[j]) / dy )**2
50
51
                T_{new[i, j]} = T[i, j] + dt * (
52
                     alpha * (
53
                         (T[i+1, j] - 2*T[i, j] + T[i-1, j]) / dx**2 +
54
                     (T[i, j+1] - 2*T[i, j] + T[i, j-1]) / dy**2
) - (u[j] * (T[i, j] - T[i-1, j]) / dx) + Phi / (rho *
55
56
       Cp)
57
58
59
       if np.linalg.norm(T_new - T) < 1e-6:</pre>
           break
61
       T = np.copy(T_new)
63
64
65 # Plot results
plt.figure(figsize=(8, 6))
67 plt.contourf(np.linspace(0, Lx, Nx), np.linspace(0, Ly, Ny), T.T, 50,
       cmap='hot')
plt.colorbar(label='Temperature (K)')
69 plt.xlabel('x')
plt.ylabel('y')
71 plt.title('Temperature Field')
72 plt.show()
```