

Instructor: Dr. B.-C. Wang

February 12, 2010

Duration: 100 min

- (a) You are permitted to use the course textbook and a calculator.
- (b) Ask for clarification if a problem statement is not clear.
- (c) Use linear interpolation in the property tables as necessary.
- (d) **Show your work** (or, **the complete solution steps**) in a clear and logical manner. Solutions that require unreasonable effort (in the opinion of the instructor) for the marker to decipher will not be credited.

I. (15 marks)

As shown in the figure, two cylinders (A and B) are filled with water and connected using a very thin pipeline with a closed valve in the middle. In cylinder A, a piston is floating on the surface of the water. The piston mass is $m_p = 500$ kg, and the friction between the piston and cylinder A can be ignored. The density of water is $\rho = 1000$ kg/m³. The local acceleration of gravity is $g = 9.81$ m/s². The local atmospheric pressure is $P_0 = 1$ bar. The initial mass of water contained in cylinder A and cylinder B is: $m_{A1} = 200$ kg and $m_{B1} = 800$ kg, respectively. The internal cross sectional areas of cylinder A and cylinder B are $A_A = 0.4$ m² and $A_B = 0.2$ m², respectively. The height $h_0 = 0.75$ m.

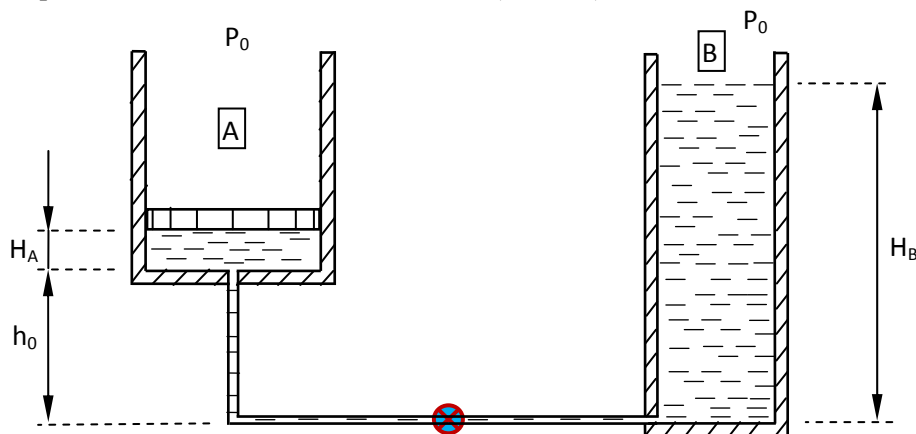
Questions:

At the initial state, the valve is closed,

- (a) Find the initial volumes of the water contained in cylinder A and cylinder B, i.e. V_{A1} and V_{B1} . (1 marks)
- (b) Find the initial heights of the water contained in cylinder A and cylinder B, i.e. H_{A1} and H_{B1} . (1 mark)
- (c) Find the initial pressure on *each side* of the valve, i.e. $P_{val, left}$ and $P_{val, right}$. (4 marks)
- (d) If the valve is opened, will the piston move up or down? Explain. (2 mark)

The valve is fully opened and water flows to an equilibrium. At the final state:

- (e) Find the final heights of the water contained in cylinder A and cylinder B, i.e. H_{A2} and H_{B2} . (5 marks)
- (f) Find the final pressure at the valve location, i.e. P_{val} . (2 marks)

Note that:

- (1) in the above problem statement, subscripts "1" and "2" are used to indicate the initial and the final states, respectively; and
- (2) the volume of the thin pipeline can be ignored.

2. (8 marks)

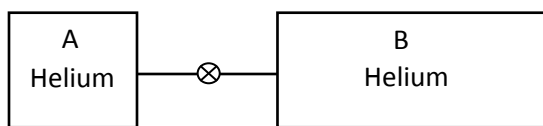
Two rigid tanks (A and B) are filled with helium and connected by a very thin pipeline. Helium contained in both tanks can be treated as an ideal gas. The thin pipeline goes through a valve which controls the flow rate between these two tanks. Initially, the valve is closed. The volume for these two rigid tanks is $V_A = 1 \text{ m}^3$ for tank A, and $V_B = 2 \text{ m}^3$ for tank B, respectively. The initial pressure and temperature of helium are $P_{A1} = 100 \text{ kPa}$ and $T_{A1} = 100^\circ\text{C}$ in tank A, and $P_{B1} = 300 \text{ kPa}$ and $T_{B1} = 500^\circ\text{C}$ in tank B, respectively. At the final state, the valve is opened and the helium gas in these two tanks reaches an equilibrium state, with a final temperature $T_2 = 300^\circ\text{C}$.

Questions:

- Determine the initial mass of helium contained in tank A and tank B, i.e. m_{A1} and m_{B1} . (4 marks)
- Determine the final pressure, i.e. P_2 . (4 marks)

Note that:

- in the above problem statement, subscripts “1” and “2” are used to indicate the initial and the final states, respectively; and
- the volume of the thin pipeline can be ignored.

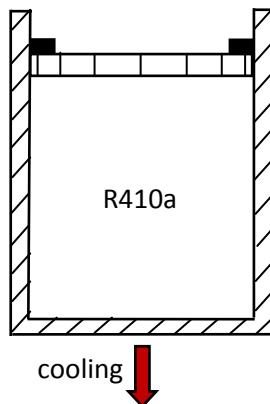


3. (17 marks)

A frictionless piston-cylinder assembly containing R410a undergoes a cooling process. The mass of R410a is $m = 100 \text{ kg}$. At the initial state (state 1), the piston pushes against a set of stops. The initial pressure and temperature of R410a are $P_1 = 550 \text{ kPa}$ and $T_1 = 260^\circ\text{C}$, respectively. It is observed that at the *exact moment* when the piston just begins to drop (state 2), the pressure of R410a is $P_2 = 150 \text{ kPa}$. After the piston leaves the stops, the system continues to dissipate heat to the environment until the final state (state 3) is reached, with the final temperature $T_3 = -55^\circ\text{C}$.

Questions:

- Determine the initial specific volume (v_1). (3 marks)
- Determine the specific volume (v_2) and temperature (T_2) of state 2. (5 marks)
- Determine the mass of the liquid (m_{f2}) and the mass of the vapour (m_{g2}) of state 2. (3 marks)
- Estimate the specific volume (v_3) of state 3. (2 marks)
- Illustrate all the state points (1, 2, 3) and the entire process (1→2→3) in both P-v and T-v diagrams. (4 marks)



Problem 1

step (a)

$$V_{A1} = m_{A1} / \rho = 200 / 1000 = 0.2 \text{ (m}^3\text{)}$$

$$V_{A2} = m_{A2} / \rho = 800 / 1000 = 0.8 \text{ (m}^3\text{)}$$

step (b)

$$H_{A1} = V_{A1} / A_A = 0.2 / 0.4 = 0.5 \text{ (m)}$$

$$H_{B1} = V_{B1} / A_B = 0.8 / 0.2 = 4 \text{ (m)}$$

step (c)

$$\begin{aligned} P_{Val}^{Left} &= P_0 + \frac{m_L g}{A_A} + \rho g (H_{A1} + h_0) \\ &= 10^5 + \frac{500 \times 9.81}{0.4} + 10^3 \times 9.81 \times (0.5 + 0.75) \\ &= 124525 \text{ (Pa)} \end{aligned}$$

or, 124.525 kPa

$$\begin{aligned} P_{Val}^{Right} &= P_0 + \rho g H_{B1} \\ &= 10^5 + 10^3 \times 9.81 \times 4 \\ &= 139240 \text{ (Pa)} \end{aligned}$$

or, 139.24 kPa

step (d)

Because $P_{Val}^{Left} < P_{Val}^{Right}$,

water will flow from B to A, and piston will move up.

step (e)

From the principle of mass conservation

$$m_{total} = m_{A1} + m_{B1} = m_{A2} + m_{B2}$$

$$\therefore 200 + 800 = \rho (A_A H_{A2} + A_B H_{B2})$$

$$\therefore 1000 = 10^3 (0.4 H_{A2} + 0.2 H_{B2})$$

$$\therefore 5 = 2 H_{A2} + H_{B2} \quad \text{————— (1)}$$

From the principle of force/pressure balance

$$p_{\text{Val},2}^{\text{Left}} = p_{\text{Val},2}^{\text{Right}}$$

$$P_0 + \frac{m_p g}{A_A} + \rho g (H_{A2} + h_0) = P_0 + \rho g H_{B2}$$

$$\therefore \frac{m_p}{A_A} + \rho (H_{A2} + h_0) = \rho H_{B2}$$

$$\therefore \frac{500}{0.4} + 1000 (H_{A2} + 0.75) = 1000 H_{B2}$$

$$2 + H_{A2} = H_{B2} \quad \text{————— (2)}$$

$$\text{From (1) \& (2) } \begin{cases} 5 = 2 H_{A2} + H_{B2} \\ 2 = -H_{A2} + H_{B2} \end{cases}$$

$$\Rightarrow \begin{cases} H_{A2} = 1 \text{ (m)} \\ H_{B2} = 3 \text{ (m)} \end{cases}$$

Step (f)

B/C the pressure from the left & right sides of the valve are balanced, we can optionally use the right side to calculate the pressure at the valve location

$$\begin{aligned} P_{\text{Val},2} &= P_0 + \rho g H_{B2} \\ &= 10^5 + 10^3 \times 9.81 \times 3 \\ &= 129430 \text{ (Pa)} \end{aligned}$$

$$\text{or, } 129.43 \text{ KPa}$$

Problem 2

step (a)

From Table A.5

$$R = 2.0771 \text{ kJ/kg}\cdot\text{K} \text{ for Helium}$$

For an ideal gas: $PV = mRT$

$$\therefore m_{A1} = \frac{P_{A1} V_A}{R T_{A1}} = \frac{100 \times 1}{2.0771 \times (273.15 + 100)} = 0.1290 \text{ kg}$$

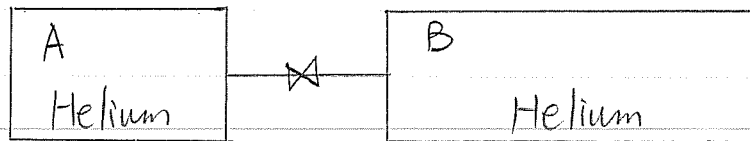
$$m_{B1} = \frac{P_{B1} V_B}{R T_{B1}} = \frac{300 \times 2}{2.0771 \times (273.15 + 500)} = 0.3736 \text{ (kg)}$$

step (b)

$$V = V_A + V_B = 1 + 2 = 3 \text{ (m}^3\text{)}$$

$$m = m_{A1} + m_{B1} = 0.1290 + 0.3736 = 0.5026 \text{ (kg)}$$

$$P = \frac{m R T_2}{V} = \frac{0.5026 \times 2.0771 \times (273.15 + 300)}{3} = 199.447 \text{ (kPa)}$$



Problem 3

Step (a) From Table B.4.1,

$T [^{\circ}\text{C}]$	$P [\text{kPa}]$
-15	480.4
$T_{\text{sat}} = ?$	550
-10	573.1

$$T_{\text{sat}} = -15 + \frac{550 - 480.4}{573.1 - 480.4} (-10 + 15)$$

$$= -11.26 (^{\circ}\text{C})$$

$$T = 260^{\circ}\text{C} > T_{\text{sat}}$$

\therefore Superheated Vapour at state 1.

From Table B.4.2, at $T_1 = 260^{\circ}\text{C}$

$P [\text{kPa}]$	$V [\text{m}^3/\text{kg}]$
500	0.12129
550	$V_1 = ?$
600	0.10093

Interpolation

$$V_1 = 0.12129 + \frac{550 - 500}{600 - 500} (0.10093 - 0.12129)$$

$$= 0.11111 (\text{m}^3/\text{kg})$$

Step (b)

Constant- v -process from state 1 to state 2

$$\therefore V_2 = V_1 = 0.11111 \text{ m}^3/\text{kg}$$

From Table B.4.1 (sat. Table)

$P [\text{kPa}]$	$T [^{\circ}\text{C}]$	$V_f [\text{m}^3/\text{kg}]$	$V_g [\text{m}^3/\text{kg}]$
138.8	-45	0.000752	0.17804
150	$T_2 = ?$	$V_{f2} = ?$	$V_{g2} = ?$
175.0	-40	0.000762	0.14291

$$V_{f2} = 0.000752 + \frac{150 - 138.8}{175 - 138.8} (0.000762 - 0.000752) = 0.00075509 (\text{m}^3/\text{kg})$$

$$V_{g2} = 0.17804 + \frac{150 - 138.8}{175 - 138.8} (0.14291 - 0.17804) = 0.16717 (\text{m}^3/\text{kg})$$

$$\text{B/c } V_{f2} < V_2 < V_{g2}$$

\therefore Saturated mixture (state 2)

$$T_2 = -45 + \frac{150 - 138.8}{175 - 138.8} (-40 + 45) = -43.45 (^{\circ}\text{C})$$

step (c)

$$\text{Quality: } X_2 = \frac{V_2 - V_f}{V_g - V_f} = \frac{0.11111 - 0.00075509}{0.16717 - 0.00075509} = 0.66313$$

$$m_{g2} = m \cdot X_2 = 100 \times 0.66313 = 66.313 \text{ (kg)}$$

$$m_{f2} = m - m_{g2} = 33.687 \text{ (kg)}$$

step (d)

constant-P-process from state 2 to state 3

$$\therefore P_3 = P_2 = 150 \text{ kPa}$$

From step (b) / Table B.4.1

$$T_{\text{sat}} = -43.45^\circ\text{C}$$

$$T < T_{\text{sat}}$$

\therefore Compressed liquid at state 3.

use the method of approximation:

$$V_3 \approx V_f|_{-55^\circ\text{C}} = 0.000735 \text{ (m}^3/\text{kg)}$$

step (e)

