LAPORAN PRODUKSI PKS TERANTAM

Uraian	Satuan	Ju		
	Sutuun	Real	RKAP	
TBS Masuk				
Kb Terantam	Kg	13,060,100	11,572,000	
Kb Sei Kencana	Kg	2,048,520	1,926,000	
Kb Sei Lindai	Kg		-	
Kb Tamora	Kg	5,784,560	4,475,000	
Kb Inti/KKPA Sei Batu Langkah	Kg	519,140	5,177,000	
Kb Sei Berlian	Kg	292,260	-	
Total Inti	Kg	21,704,580	23,150,000	
Pihak Ketiga	Kg	2,705,800	3,639,533	
Total Pabrik	Kg	24,410,380	26,789,533	
TBS Olah	Kg			
Kb Terantam	Kg	13,397,440	11,572,000	
Kb Sei Kencana	Kg	2,048,520	1,926,000	
Kb Sei Lindai	Kg			
Kb Tamora	Kg	5,884,560	4,475,000	
Kb Inti/KKPA Sei Batu Langkah	Kg	519,140	5,177,000	
Kb Sei Berlian	Kg	292,260	-	
Total Inti	Kg	22,141,920	23,150,000	
Pihak Ketiga	Kg	2,879,460	3,639,533	
Total Pabrik	Kg	25,021,380	26,789,533	
Produksi CPO	Kg			
Kb Terantam	Kg	3,176,838	2,736,778	
Kb Sei Kencana	Kg	494,468	438,165	
Kb Sei Lindai	Kg	-	-	
Kb Tamora	Kg	1,418,428	1,071,763	
Kb Inti/KKPA Sei Batu Langkah	Kg	126,457	1,245,069	
Kb Sei Berlian	Kg	67,658	-	
Total Inti	Kg	5,283,849	5,491,774	
Pihak Ketiga	Kg	589,307	758,843	
Total Pabrik	Kg	5,873,156	6,250,617	
Produksi Kernel	Kg			
Kb Terantam	Kg	470,282	445,522	
Kb Sei Kencana	Kg	72,235	77,040	
Kb Sei Lindai	Kg	-		
Kb Tamora	Kg	208,732	179,000	
Kb Inti/KKPA Sei Batu Langkah	Kg	17,504	207,080	
Kb Sei Berlian	Kg	11,106		
Total Inti	Kg	779,859	908,642	
Pihak Ketiga	Kg	86,386	183,069	
Total Pabrik	Kg	866,245	1,091,711	
Rend CPO				
Kb Terantam	%	23.71	23.65	
Kb Sei Kencana	%	24.14	22.75	
Kb Sei Lindai	%		24.05	
Kb Tamora	%	24.10	23.95	
Kb Inti/KKPA Sei Batu Langkah	%	24.36	24.05	
Kb Inti/KKPA Sei Batu Langkah	% %	24.36 23.15	24.05	
			24.05	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian	%	23.15		
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti Pihak Ketiga	% %	23.15 23.86 20.47	23.72 20.85	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti	% % %	23.15 23.86	23.72	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik	% % %	23.15 23.86 20.47	23.72 20.85	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kernel	% % % %	23.15 23.86 20.47 23.47	23.72 20.85 23.33	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti Pilhak Ketiga Total Pabrik Rend Kernel Kb Terantam Kb Sei Kencana	% % % % % %	23.15 23.86 20.47 23.47	23.72 20.85 23.33 3.85 4.00	
Kb Inti/KKPA Sei Batu Langkah kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kernel Kb Terantam Kb Sei Kencana	% % % % % % %	23.15 23.86 20.47 23.47 3.51 3.53	23.72 20.85 23.33 3.85 4.00 4.00	
Kb Inti/KKPA Sei Batu Langkah Kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kemel Kb Terantam Kb Sei Kencana Kb Sei Lindai Kb Tamora	% % % % % % %	23.15 23.86 20.47 23.47 3.51 3.53	23.72 20.85 23.33 3.85 4.00 4.00	
Kb Inti/KKPA Sei Batu Langkah kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kernel Kb Terantam Kb Sei Kencana Kb Sei Lindai Kb Tamora	% % % % % % %	23.15 23.86 20.47 23.47 3.51 3.53 - 3.55 3.55	23.72 20.85 23.33 3.85 4.00 4.00	
Kb Intl/KKPA Sel Batu Langkah Kb Sel Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kemel Kb Terantam Kb Sel Kencana Kb Sel Lindal Kb Tamora Kb IntlikRPA Sel Batu Langkah Kb Sel Berlian	% % % % % % % % % % % % % %	23.15 23.86 20.47 23.47 3.51 3.53 - 3.55 3.37 3.80	23.72 20.85 23.33 3.85 4.00 4.00 4.00	
Kb Inti/KKPA Sei Batu Langkah kb Sei Berlian Total Inti Pihak Ketiga Total Pabrik Rend Kernel Kb Terantam Kb Sei Kencana Kb Sei Lindai Kb Tamora	% % % % % % %	23.15 23.86 20.47 23.47 3.51 3.53 - 3.55 3.55	23.72 20.85 23.33 3.85 4.00 4.00	

URAI	Satuan	Juni			
TBS Sisa Awal Mengolah		Kg	1,251,000		
TBS Diterima		Kg	24,410,380		
TBS Tersedia		Kg	25,661,380		
TBS Diolah	Realisasi	Kg	25,021,380		
TBS Diolah	RKAP	Kg	26,789,533		
TBS Sisa akhir giling	Kg	640,000			
Pabrik Mengolah (Jam Scr	ew Pres).				
Mengolah Efektife		Jam	674		
Stagnasi Pabrik		Jam	29.5		
Jam Bruto Pengolahan		Jam	703.5		
Hari Olah		Hari	30		
Kapasitas Pabrik Ton/TBS/Jar	<u>n</u>				
Efektif		Kg	37,124		
Bruto		Kg	35,567		
Kapasitas Screw Press	Unit				
Jam Jalan Efektip		Jam	2,696		
Stagnasi Pabrik		Jam	29.5		
Jam Bruto		Jam	2,726		
Kapasitas rata rata/Unit/Jam		Kg	9,281		
Kapasitas rata rata/Unit/Jam	/Bruto	Kg	8,892		
Hasil Pengolahan		16.	5 070 450		
Minyak Sawit	R K A P	Kg Kg	5,873,156 6,250,616		
Minyak Sawit		Kg %	23.47		
Rend.M.Sawit Rend.M.Sawit	R K A P	%	23.47		
Inti Sawit	Realisasi	Kg	866,245		
.Inti Sawit	RKAP	Kg	1,091,711		
Rend.Inti Sawit	Realisasi	% %	3.46		
Rend.Inti Sawit	RKAP	%	4.08		
Trendanti Odwit	N.KAI	~	1.00		
Mutu Produksi					
Minyak Sawit	- A L B	%	3.86		
	- Air	%	0.15		
	- Kotoran	%	0.015		
Inti Sawit	-ALB	%	0.98		
	- Air	%	6.73		
	- Kotoran	%	6.08		
Harga Pokok Pengolahan	Realisasi	Rp/Kg	490,51		
Harga Pokok Pengolahan	RKAP	Rp/Kg	451,52		

I. MUTU PRODUKSI MINYAK SAWIT				Nor	ma		
1. Kadar ALB		URAIAN		Satuan			Juni
1. Kadar ALB							
2. Kadar Air		MINYAK SAWIT				2 50	0.00
3. Kadar Kotoran							
4. ALB BUAR Rebus				,-			
IL MUTU NITI SAWIT							
LABAR ALB				%		0.40	0.38
2. Kadar Air		Т					-
3. Kadar Kotoran							
S. Inti Berubah Warna							
S. Intil Berlubah Warna							
III. KEHLIANGAN MINYAK SAWIT		rna		%			15.01
1.Air Rebusan				%		45.00	44.97
Air Rebusan		NYAK SAWIT					-
2. Tandan Kosong		(N==)		%		3.40	
Tandan Kosong (NOS)		(NOS)		9/		2.50	
3. Buah Ikut Tankos (sample) %							
K. Minyak dalam buah ikut tankos (sample)		S		%			
S. Am pa s							0.18
Am pa s	4. Biji						
Semple S							
Draf Akhir 1,005	Ampas						
7. Solid Decanter (sample) % 2.50 2.22				76			
Solid Decarter				%			
Rendement Minyak Sawit (CPO) Effesiensi Pengutipan Minyak N. KEHILANGAN INT SAWIT 1. Ampas /serabut 2. LT.D.S I (sample) % 2.00 3.00 LT.D.S II (sample) % 2.00 3.00 LT.D.S II (sample) % 3.00 LT.D.S II (sample) % 3.00 LT.D.S II (sample) % 5.00 LT.D.S II (sa				%		12.00	15.75
Effesiensi Pengutipan Milnyak % 93.00 93.30 N. KEHLANGAN INTI SAWIT				%		1.65	
IV. KEHILANGAN INTIS ANIT	Rendement Minyak	Sawit (CPO)					
1. Ampas / Serabut (sample) % 2.00 3.00				%		93.00	93.33
2. LT.D.S (sample) % 2.00 3.00		IISAWII	(cample)	96		2.00	1 89
LT.D.S.II							
Clay Bath	L.T.D.S II						-
A Intidalam Duah ikut tankos (sample) % 0.20 0.40 Total Kehlingan Inti % 0.60 0.58 Rendement Inti Sawit (Kernel)	3. Hydrocyclone		(sample)	%		5.00	3.58
Total kehlangan Inti Rendement Inti Sawit (Kernel)							-
Rendement Inti Savit (Kernel)			(sample)				
Effisiensi pengutipan Initi % 92.00 85.41 V. PENILIKAN PABRIK				%		0.60	
V. PENILKAN PABRIK				%		92.00	
1. Komposis Crude Oil Tank	V. PENILIKAN PABR	IK					
- Kadar Air % 40,00 50,00 40,00 50	1. Komposisi Crude						-
NO S % 7,00 15,0	- Kadar Minyak						
Effisiense Ripple Mill							
2. Kadar Minyak dalam sludge Tank % 7.00 15.00 6.00 3. Kadar Air dalam Oil Tank % 0.40 0.60 0.47 4. Kadar Air dalam Oil Tank % 0.30 0.50 5. Kadar Kotoran Oil Tank % 0.20 0.30 0.27 6. Kadar Kotoran Oil Tank % 0.013 0.02 7. Kadar Air dalam Bij % 10.00 16.00 12.68 VITEMPERATUR DAN TEKANAN							
3. Kadar Air dalam Oli Tank							
A. Kadar Alor Oil Purifier 9% 0.30 0.50 0							
5. Kadar Kotoran Oll Tank % 0.20 0.30 0.27 6. Kadar Kotoran Oll Purifler % 0.013 0.02 - 7. Kadar Air dalam Biji % 10.00 16.00 12.68 VI TEMFERATUR DAN TEKANAN -Temp. *C 130.0 135.0 135.00 1. Rebusan -Tek. Kg/cm2 2.8 3.0 2.80 2. Digester -Temp. *C 100.0 95.0 90.0 3. Press -Tek. Kg/cm2 4.0 50.0 45.00 4. Crude Oll Tank -Temp. *C 90.0 95.0 90.0 5. CST -Temp. *C 90.0 95.0 90.0 5. CST -Temp. *C 90.0 95.0 90.0 5. CST -Temp. *C 90.0 95.0 90.0 7. Oil Tank -Temp. *C 90.0 95.0 90.0 8. Sludge Tank -Temp. *C 90.0 95.0 90.0 <t< td=""><td></td><td></td><td></td><td></td><td></td><td>0.50</td><td>-</td></t<>						0.50	-
7. Kadar Air dalam Bij				%	0.20	0.30	0.27
VITEMPERATUR DAN TEKANAN - 1 -							-
1. Rebusan				%	10.00	16.00	12.68
1-fek		AN IEKANAN	- Temp	°C	130.0	135.0	135.00
2. Digester -1 emp, 'C 90.0 95.0 90.00 3. Press -1 rek, Kg/cm2 40.0 50.0 45.00 4. Crude Oli Tank -1 emp, 'C 90.0 95.0 90.00 5. CST -1 emp, 'C 90.0 95.0 90.00 5. CST -1 emp, 'C 90.0 95.0 90.00 7. Oli Tank -1 emp, 'C 90.0 95.0 90.00 7. Oli Tank -1 emp, 'C 90.0 95.0 90.00 8. Sludge Tank -1 emp, 'C 90.0 95.0 90.00 9. Hot Water Tank -1 emp, 'C 90.0 95.0 90.00 9. Hot Water Tank -1 emp, 'C 90.0 95.0 90.00 10. Vacum Dryer -1 rek, mm Hg 600.0 700.0 690.00 11. Storage Tank -1 emp, 'C 40.0 45.0 45.00 12. Silo Biji -1 emp, 'C 50.0 70.0 50.00 13. Silo Inti 8 ag, Atas -1 emp, 'C 60.0 70.0 70.00 8ag, Atas -1 emp, 'C 60.0 70.0 60.00 8ag Atas -1 emp, 'C 50.0 70.0 60.00 14. Boller -1 rek, Kg/cm2 17.0 20.0 39.00 14. Boller -1 rek, Kg/cm2 17.0 20.0 39.00 15.00 17 ck, Kg/cm2 17.0 20.0 39.00 16. Silo Inti 8 ag, Atas -1 emp, 'C 50.0 70.0 50.00 17. Ke, Kg/cm2 17.0 20.0 39.00 18. Boller -1 rek, Kg/cm2 17.0 20.0 30.00 18. Boller -1 rek, Kg/cm2 17.0 20.0	1. Nebusan						
3. Press	2. Digester			°C	90.0	95.0	90.00
5. CST - Temp. *C 90.0 95.0 90.0 7. Oil Tank - Temp. *C 90.0 95.0 90.00 7. Oil Tank - Temp. *C 90.0 95.0 90.00 8. Sludge Tank - Temp. *C 90.0 95.0 90.00 9. Hot Water Tank - Temp. *C 90.0 95.0 95.0 10. Vacum Dryer - Tek. mm Hg 600.0 700.0 690.0 11. Slorage Tank - Temp. *C 50.0 70.0 50.0 12. Slio Biji - Temp. *C 50.0 70.0 50.0 13. Slio Intil Bag, Etas - Temp. *C 60.0 70.0 60.0 Bag Atas - Temp. *C 60.0 70.0 60.0 14. Boller - Tek. Kg/cm2 17.0 20.0 50.0	3. Press		- Tek.	Kg/cm2			
6. Buffer Tank			- Temp.				
7. Oil Tank							
8. Sludge Tank			- Temp.				
9. Hot Water Tank 10. Vacum Dryer 1. Temp. 1. Te							
11. Storage Tank							
12. Slio Biji	10. Vacum Dryer						
13.Silo Intit Bag.Atas -Temp. °C 60.0 70.0 70.00	11. Storage Tank						
Bag_Tengah - Temp.		D 44					
Bag.Atas -Temp. °C 50.0 60.0 50.00 14. Boiler -Tek. Kg/cm2 17.0 20.0 19.00	13. SIIO INTI						
14. Boiler -Tek. Kg/cm2 17.0 20.0 19.00				°C			
	14. Boiler						
	15. BPV		- Tek.	Kg/cm2		3.2	2.90