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Total number of pages: [2]

Total number of questions: 06

**B.Tech. || ME || 6<sup>th</sup> Sem**

**Heat Transfer**

**Subject Code: BTME-602 (RP)**

**Paper ID: M118**

(2011-2014 batch)

Time allowed: 3 Hrs

Max Marks: 60

**Important Instructions:**

- All questions are compulsory
- Assume any missing data

**PART A (2×10)**

All COs

Q. 1. Short-Answer Questions:

- Distinguish between free and forced convection.
- Define fin efficiency and effectiveness.
- State Fourier's law of heat conduction.
- Define NTU of a heat exchanger.
- A person claims that heat cannot be transferred in a vacuum. How do you respond to this claim?
- What do you mean by critical radius of insulation?
- State the difference between filmwise and dropwise condensation.
- Give a few specific examples of use of fins.
- What is the importance of conduction shape factor?
- Define emissive power and Intensity of radiation.

**PART B (8×5)**

- Q. 2. (a) Name and explain briefly the various modes of heat transfer. CO<sub>1</sub>, CO<sub>2</sub>
- (b) The composite wall of an oven consists of three materials, two of them are of known thermal conductivity,  $k_A = 20 \text{ W/m K}$  and  $k_C = 50 \text{ W/m K}$  and known thickness  $L_A = 0.3 \text{ m}$  and  $L_C = 0.15 \text{ m}$ . The third material B, which is sandwiched between material A and C is of known thickness,  $L_B = 0.15 \text{ m}$ , but of unknown thermal conductivity  $k_B$ .

Under steady state operating conditions, the measurement reveals an outer surface temperature of material C is  $20^\circ\text{C}$  and inner surface of A is  $600^\circ\text{C}$  and oven air temperature is  $800^\circ\text{C}$ . The inside convection coefficient is  $25 \text{ W/m}^2 \text{ K}$ . What is the value of  $k_B$ ?

OR

- (a) Drive an expression for temperature distribution during steady state heat conduction in a solid sphere with internal heat generation and exposed to convection environment. CO<sub>1</sub>, CO<sub>2</sub>
- (b) In a long nuclear reactor, 5 cm diameter cylindrical uranium rod cooled by water

from outside, serves as the fuel. Heat is generated uniformly in the rod ( $k = 29.5 \text{ W / m K}$ ) at a rate of  $7 \times 10^7 \text{ W/m}^3$ . If the outer surface temperature of the rod is  $150^\circ\text{C}$ . Calculate the temperature at the centre.

- Q. 3. Explain the criteria of selection of fins. Drive an expression for heat flow in a straight triangular fin. CO<sub>3</sub>

OR

A very long rod, 25 mm in diameter, has one end maintained at  $100^\circ\text{C}$ . The surface of the rod is exposed to ambient air at  $25^\circ\text{C}$  with convection coefficient of  $10 \text{ W/m}^2 \text{ K}$ . CO<sub>3</sub>

(a) What are the heat losses from the rods, constructed of pure copper ( $k = 398 \text{ W/m K}$ ) and stainless steel ( $k = 14 \text{ W/m K}$ )?

(b) Estimate how long the rods must be to be considered infinite.

- Q. 4. (a) What do you understand by Laminar, Turbulent and Thermal Boundary layers? CO<sub>5</sub>  
(b) Define effectiveness of heat exchanger. How maximum heat transfer rate is obtained?

OR

A heat exchanger is required to cool  $55,000 \text{ kg/h}$  of alcohol from  $66^\circ\text{C}$  to  $40^\circ\text{C}$  using  $40,000 \text{ kg/h}$  of water entering at  $5^\circ\text{C}$ . Calculate (i) exit temperature of water, (ii) heat transfer rate, (iii) surface area required for (a) parallel flow type, (b) counter flow type of heat exchanger. CO<sub>5</sub>

- Q. 5. (a) Discuss the conditions under which the dropwise condensation can take place. Why the rate of heat transfer in dropwise condensation is many time that of film condensation? CO<sub>4</sub>  
(b) Explain pool boiling.

OR

Drive an expression for Nusselt number for laminar film condensation on a vertical surface. Also state the assumption made in driving expression. CO<sub>4</sub>

- Q. 6. (a) State and prove the Kirchhoffs law of thermal radiation. CO<sub>6</sub>  
(b) A hot water radiator of overall dimensions  $2 \times 1 \times 0.2 \text{ m}$  is used to heat the room at  $18^\circ\text{C}$ . The surface temperature of radiator is  $60^\circ\text{C}$  and its surface is black. The actual surface of the radiator is 2.5 times the area of its envelope for convection for which the convection coefficient is given by  $h_c = 1.3(\Delta T)^{1/3} \text{ W/m}^2 \cdot \text{K}$ . Calculate the rate of heat loss from the radiator by convection and radiation.