# Implementation of CLM Below-Ground Biogeochemistry in PFLOTRAN

July 31, 2013

#### Abstract

## 1 CLM-CN

## 1.1 Reactions

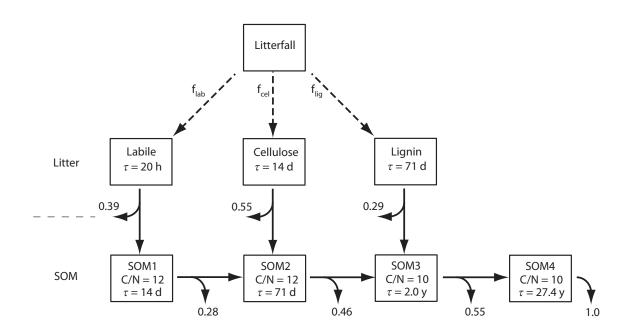


Figure 1: CLM-CN litter and soil organic pools and C and N flows Bonan et al. [2012]

### 1.1.1 General Reaction

The general decomposition reaction is

$$CN_u = (1 - f)CN_d + fCO_2 + nN_{\text{mineral}}$$
(1)

```
CN_u
               upstream pool [mol/m<sup>3</sup>]
CN_d
               downstream pool [mol/m<sup>3</sup>]
          =
CO_2
               [\text{mol/m}^3]
               mineral nitrogen [mol/m<sup>3</sup>]
N_{mineral}
          =
               molecular weight ratio of C and N divided by upstream pool C/N [-]
               molecular weight ratio of C and N divided by downstream pool C/N [-]
d
f
               respiration fraction [-]
n
               [u - (1 - f)d]
```

### 1.1.2 Soil Organic Matter Pools

The C/N ratio is fixed in soil organic matter pools. The reactions are

Table 1: Reactions for the soil organic matter pools

#### 1.1.3 Litter Pools

The C/N ratio is dependent on the input from plant function groups. As the C/N ratio is generally greater in the litter pools than in the soil organic pools Adair et al. [2008], mineral N is needed to decompose the litter pools. Namely, litter decomposition involves N immobilization through microbial mass synthesis. For example, one observation indicates a C/N ratio of 31.19 for yellow birch Adair et al. [2008]. The reactions are

Table 2: Reactions for the litter pools

### 1.1.4 Summary

$$\begin{aligned} \text{Lit1C} + u_1 \text{Lit1N} &= (1 - f_1) \, \text{SOM1} + f_1 \text{CO}_2 + n_1 \text{N}_{\text{mineral}} \\ \text{Lit2C} + u_2 \text{Lit2N} &= (1 - f_2) \, \text{SOM2} + f_2 \text{CO}_2 + n_2 \text{N}_{\text{mineral}} \\ \text{Lit3C} + u_3 \text{Lit3N} &= (1 - f_3) \, \text{SOM3} + f_3 \text{CO}_2 + n_3 \text{N}_{\text{mineral}} \\ \text{SOM1} &= (1 - f_4) \, \text{SOM2} + f_4 \text{CO}_2 + n_4 \text{N}_{\text{mineral}} \\ \text{SOM2} &= (1 - f_5) \, \text{SOM3} + f_5 \text{CO}_2 + n_5 \text{N}_{\text{mineral}} \\ \text{SOM3} &= (1 - f_6) \, \text{SOM4} + f_6 \text{CO}_2 + n_6 \text{N}_{\text{mineral}} \\ \text{SOM4} &= f_7 \text{CO}_2 + n_7 \text{N}_{\text{mineral}} \end{aligned}$$

$$u_i = \text{LitiN/LitiC}$$

### 1.2 Rate

### 1.2.1 General

$$R = f_T f_{\Psi} f_{\mathcal{N}} k \mathcal{C} \mathcal{N}_u \tag{2}$$

$$R = \text{rate } [\text{mol/(m}^3 \text{s})]$$

$$f_T = \exp \left[ 308.56 \left( \frac{1}{71.02} - \frac{1}{T - 227.13} \right) \right]$$

$$f_{\Psi} = \frac{\log (\Psi_{\text{min}}/\Psi)}{\log (\Psi_{\text{min}}/\Psi_{\text{max}})}$$

$$f_{\text{N}} = \frac{N_{\text{mineral}}}{N_{\text{mineral}} + k_{N_{\text{mineral}}}} (\text{if } u < 0)$$

$$k = \text{kinetic rate constant}[\text{s}^{-1}]$$

$$T = \text{temperature } [\text{K}]$$

$$\Psi = \text{soil water potential}[\text{Pa}]$$

$$CN_u = \text{upstream carbon pool } [\text{mol/m}^3]$$

$$N_{\text{mineral}} = \text{nitrogen concentration } [\text{mol/m}^3]$$

$$k_{\text{N}} = \text{Mineral N half saturation constant } [\text{mol/m}^3]$$

For the general reaction 1,

$$\begin{split} \frac{\partial \text{CN}_u}{\partial t} &= -R \\ \frac{\partial \text{CN}_d}{\partial t} &= (1 - f) \, R \\ \frac{\partial \text{CO}_2}{\partial t} &= f R \\ \frac{\partial \text{N}_{\text{mineral}}}{\partial t} &= n R \end{split}$$

### 1.2.2 Rates

$$R_{1} = f_{T}f_{\theta}f_{N}k_{1}\text{Lit1C}$$

$$R_{2} = f_{T}f_{\theta}f_{N}k_{2}\text{Lit2C}$$

$$R_{3} = f_{T}f_{\theta}f_{N}k_{3}\text{Lit3C}$$

$$R_{4} = f_{T}f_{\theta}f_{N}k_{4}\text{SOM1}$$

$$R_{5} = f_{T}f_{\theta}f_{N}k_{5}\text{SOM2}$$

$$R_{6} = f_{T}f_{\theta}f_{N}k_{6}\text{SOM3}$$

$$R_{7} = f_{T}f_{\theta}f_{N}k_{7}\text{SOM4}$$

### 1.2.3 Mass Conservation

$$\frac{\partial}{\partial t} \text{ (Lit1C)} = -R_1$$

$$\frac{\partial}{\partial t} \text{ (Lit1N)} = -u_1 R_1$$

$$\frac{\partial}{\partial t} \text{ (Lit2C)} = -R_2$$

$$\frac{\partial}{\partial t} \text{ (Lit3N)} = -u_2 R_2$$

$$\frac{\partial}{\partial t} \text{ (Lit3C)} = -R_3$$

$$\frac{\partial}{\partial t} \text{ (Lit3N)} = -u_3 R_3$$

$$\frac{\partial}{\partial t} \text{ (SOM1)} = (1 - f_1) R_1 - R_4$$

$$\frac{\partial}{\partial t} \text{ (SOM2)} = (1 - f_2) R_2 + (1 - f_4) R_4 - R_5$$

$$\frac{\partial}{\partial t} \text{ (SOM3)} = (1 - f_3) R_3 + (1 - f_5) R_5 - R_6$$

$$\frac{\partial}{\partial t} \text{ (SOM4)} = (1 - f_6) R_6 - R_7$$

$$\frac{\partial}{\partial t} \text{ (CO2)} = f_1 R_1 + f_2 R_2 + f_3 R_3 + f_4 R_4 + f_5 R_5 + f_6 R_6 + f_7 R_7$$

$$\frac{\partial}{\partial t} \text{ (N_{mineral})} = n_1 R_1 + n_2 R_2 + n_3 R_3 + n_4 R_4 + n_5 R_5 + n_6 R_6 + n_7 R_7$$

## 1.3 Implementation in PFLOTRAN

#### 1.3.1 Numerical Methods

Applying finite-volume spatial discretization:

$$\int \frac{\partial x}{\partial t} dV = \int -\sum R_j dV \tag{3}$$

$$\frac{\partial x}{\partial t} \Delta V = -\sum_{j} R_{j} \Delta V \tag{4}$$

Implicit time discretization:

$$\frac{\Delta V}{\Delta t} \left( x^{k+1} - x^k \right) = -\sum_{j} R_j^{k+1} \Delta V \tag{5}$$

Residual:

$$\mathcal{R} = \frac{\Delta V}{\Delta t} \left( x^{k+1} - x^k \right) + \sum_{i} R_i^{k+1} \Delta V \tag{6}$$

Jacobian:

$$\mathcal{J} = \frac{\partial \mathcal{R}}{\partial x} \tag{7}$$

Newton-Raphson Method:

$$\mathcal{J}\delta x = -\mathcal{R} \tag{8}$$

$$x^{k+1,i+1} = x^{k+1,i} + \delta x \tag{9}$$

Table 3: Units for residuals and Jacobian

	aqueous species	immobile species	mixed
$\boldsymbol{x}$	$\mathrm{mol/L}$	$\mathrm{mol/m^3}$	
$\Delta V$	m L	$\mathrm{m}^3$	${ m L}$
R	mol/Ls	$\rm mol/m^3 s$	mol/Ls
${\cal R}$	mol/s	mol/s	mol/s
${\cal J}$	L/s	$\mathrm{m}^3/\mathrm{s}$	

### 1.3.2 Implementation

The source code reaction\_sandbox\_clm\_cn.F90 implements CLM-CN with input file like the following:

#### CHEMISTRY

```
IMMOBILE_SPECIES
  N
  С
  SOM1
  SOM2
  SOM3
  SOM4
  LabileC
  CelluloseC
  LigninC
  LabileN
  CelluloseN
  LigninN
/
REACTION_SANDBOX
  \mathtt{CLM-CN}
    POOLS
             ! CN ratio
      SOM1
            12.d0
      SOM2 12.d0
      SOM3 10.d0
      SOM4 10.d0
      Labile
```

```
Cellulose
  Lignin
REACTION
  UPSTREAM_POOL Labile
  DOWNSTREAM_POOL SOM1
  TURNOVER_TIME 20. h
  RESPIRATION_FRACTION 0.39d0
  N_INHIBITION 1.d-10
REACTION
  UPSTREAM_POOL Cellulose
  DOWNSTREAM_POOL SOM2
  TURNOVER_TIME 14. d
  RESPIRATION_FRACTION 0.55
  N_INHIBITION 1.d-10
REACTION
  UPSTREAM_POOL Lignin
  DOWNSTREAM_POOL SOM3
  TURNOVER_TIME 71. d
  RESPIRATION_FRACTION 0.29d0
  N_INHIBITION 1.d-10
REACTION
  UPSTREAM_POOL SOM1
  DOWNSTREAM_POOL SOM2
  TURNOVER_TIME 14. d
  RESPIRATION_FRACTION 0.28d0
  N_INHIBITION 1.d-10
REACTION
  UPSTREAM_POOL SOM2
  DOWNSTREAM_POOL SOM3
  TURNOVER_TIME 71. d
  RESPIRATION_FRACTION 0.46d0
  N_INHIBITION 1.d-10
REACTION
  UPSTREAM_POOL SOM3
  DOWNSTREAM_POOL SOM4
  TURNOVER_TIME 2. y
  RESPIRATION_FRACTION 0.55d0
  N_INHIBITION 1.d-10
REACTION
```

```
UPSTREAM_POOL SOM4
TURNOVER_TIME 27.4 y
RESPIRATION_FRACTION 1.d0
N_INHIBITION 1.d-10
/
```

In the source code, the key is to specify the residual and Jacobian. The residuals are:

$$\mathcal{R}_{\text{Lit1C}} = \frac{\Delta V}{\Delta t} \left( \text{Lit1C}^{k+1} - \text{Lit1C}^{k} \right) + R_{1}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{Lit1N}} = \frac{\Delta V}{\Delta t} \left( \text{Lit1N}^{k+1} - \text{Lit1N}^{k} \right) + u_{1} R_{1}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{Lit2C}} = \frac{\Delta V}{\Delta t} \left( \text{Lit2C}^{k+1} - \text{Lit2C}^{k} \right) + R_{2}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{Lit2N}} = \frac{\Delta V}{\Delta t} \left( \text{Lit2N}^{k+1} - \text{Lit2N}^{k} \right) + u_{2} R_{2}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{Lit3C}} = \frac{\Delta V}{\Delta t} \left( \text{Lit3C}^{k+1} - \text{Lit3C}^{k} \right) + R_{3}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{Lit3N}} = \frac{\Delta V}{\Delta t} \left( \text{Lit3N}^{k+1} - \text{Lit3N}^{k} \right) + u_{3} R_{3}^{k+1} \Delta V$$

$$\mathcal{R}_{\text{SOM1}} = \frac{\Delta V}{\Delta t} \left( \text{SOM1}^{k+1} - \text{SOM1}^{k} \right) - \left[ (1 - f_{1}) R_{1}^{k+1} - R_{4}^{k+1} \right] \Delta V$$

$$\mathcal{R}_{\text{SOM2}} = \frac{\Delta V}{\Delta t} \left( \text{SOM2}^{k+1} - \text{SOM2}^{k} \right) - \left[ (1 - f_{2}) R_{2}^{k+1} + (1 - f_{4}) R_{4}^{k+1} - R_{5}^{k+1} \right] \Delta V$$

$$\mathcal{R}_{\text{SOM3}} = \frac{\Delta V}{\Delta t} \left( \text{SOM3}^{k+1} - \text{SOM3}^{k} \right) - \left[ (1 - f_{3}) R_{3}^{k+1} + (1 - f_{5}) R_{5}^{k+1} - R_{6}^{k+1} \right] \Delta V$$

$$\mathcal{R}_{\text{SOM4}} = \frac{\Delta V}{\Delta t} \left( \text{SOM4}^{k+1} - \text{SOM4}^{k} \right) - \left[ (1 - f_{6}) R_{6}^{k+1} - R_{7}^{k+1} \right] \Delta V$$

$$\mathcal{R}_{\text{CO2}} = \frac{\Delta V}{\Delta t} \left( \text{CO}_{2}^{k+1} - \text{CO}_{2}^{k} \right)$$

$$- \left[ f_{1} R_{1}^{k+1} + f_{2} R_{2}^{k+1} + f_{3} R_{3}^{k+1} + f_{4} R_{4}^{k+1} + f_{5} R_{5}^{k+1} + f_{6} R_{6}^{k+1} + R_{7}^{k+1} \right] \Delta V$$

$$\mathcal{R}_{\text{N}_{\text{mineral}}} = \frac{\Delta V}{\Delta t} \left( \text{N}_{\text{mineral}}^{k+1} - \text{N}_{\text{mineral}}^{k} \right)$$

$$- \left[ n_{1} R_{1}^{k+1} + n_{2} R_{2}^{k+1} + n_{3} R_{3}^{k+1} + n_{4} R_{4}^{k+1} + n_{5} R_{5}^{k+1} + n_{6} R_{6}^{k+1} + R_{7}^{k+1} \right] \Delta V$$

For Lit1 decomposition, the rate is

$$R_1 = f_T f_{\Psi} f_{N} k_1 \text{Lit1C} \tag{10}$$

the derivatives are:

$$\frac{\partial R_1}{\partial \text{Lit1C}} = f_T f_{\Psi} f_{\text{N}} k_1 = R'_{1,\text{Lit1C}}$$
(11)

$$\frac{\partial R_1}{\partial \mathcal{N}_{\text{mineral}}} = f_T f_{\Psi} k_1 \text{Lit1C} \frac{k_N}{(k_N + \mathcal{N}_{\text{mineral}})^2} = R'_{1,N}$$
(12)

$$\begin{array}{lll} \frac{\partial R_{\rm Lit1N}}{\partial {\rm Lit1C}} & = \frac{\partial (u_1R_1)}{\partial {\rm Lit1C}} & = R_1 \frac{\partial u_1}{\partial {\rm Lit1C}} + u_1R_{1,{\rm Lit1C}} & = -R_1 \frac{{\rm Lit1N}}{{\rm Lit1C}^2} + u_1R'_{1,{\rm Lit1C}} \\ \frac{\partial R_{\rm Lit1N}}{\partial {\rm Lit1N}} & = \frac{\partial (u_1R_1)}{\partial {\rm Lit1N}} & = R_1 \frac{\partial u_1}{\partial {\rm Lit1N}} & = R_1 \frac{1}{{\rm Lit1C}} \\ \frac{\partial R_{\rm Lit1N}}{\partial {\rm Nmineral}} & = \frac{\partial (u_1R_1)}{\partial {\rm Nmineral}} & = R_1 \frac{\partial u_1}{\partial {\rm Nmineral}} + u_1R'_{1,{\rm N}} & = u_1R'_{1,{\rm N}} \\ \frac{\partial R_{\rm Nmineral}}{\partial {\rm Lit1C}} & = -\frac{\partial (n_1R_1)}{\partial {\rm Lit1C}} & = -R_1 \frac{\partial n_1}{\partial {\rm Lit1N}} & = -R_1 \frac{1}{{\rm Lit1C}} \\ \frac{\partial R_{\rm Nmineral}}{\partial {\rm Lit1N}} & = -\frac{\partial (n_1R_1)}{\partial {\rm Lit1N}} & = -R_1 \frac{\partial n_1}{\partial {\rm Lit1N}} & = -R_1 \frac{1}{{\rm Lit1C}} \\ \frac{\partial R_{\rm Nmineral}}{\partial {\rm Nmineral}} & = -\frac{\partial (n_1R_1)}{\partial {\rm Lit1N}} & = -R_1 \frac{\partial n_1}{\partial {\rm Nmineral}} & = -R_1 \frac{1}{{\rm Lit1C}} \\ & = -R_1 \frac{\partial n_1}{\partial {\rm Nmineral}} & = -R_1 \frac{\partial n_1}{\partial {\rm Nmineral}} & = -R_1 \frac{\partial n_1}{\partial {\rm Nmineral}} \\ \end{array}$$

Table 4: Jacobian for Litter Pools SOMi LitiN  $CO_2$  $N_{mine\underline{ral}}$  $\frac{R'_{i,\text{LitiC}}}{-R_i \frac{\text{LitiN}}{\text{LitiC}^2} + u_i R'_{i,\text{LitiC}}} - (1 - f_i) R'_{i,\text{LitiC}}}$  $R'_{i,N}$ LitiC  $u_i R'_{i,N}$  $R_i \frac{1}{\text{LitiC}}$ LitiN 0 0  $-(1 - f_i)R'_{i,N}$   $-f_iR'_{i,N}$   $-n_iR'_{i,N}$ SOMi0 0  $-f_i R'_{i,\text{LitiC}}$   $R_i \frac{\text{LitiN}}{\text{LitiC}^2} - n_i R'_{i,\text{LitiC}}$  $\mathrm{CO}_2$ 0 0 0  $N_{mineral}$ 

Table 5: Jacobian for SOM Pools							
	SOM1	SOM2	SOM3	SOM4	$CO_2$	$N_{\mathrm{mineral}}$	
SOM1	$R_4'$	0	0	0	0	0	
SOM2	$-(1-f_4)R_4'$	$R_5'$	0	0	0	0	
SOM3	0	$-(1-f_5)R_5'$	$R_6'$	0	0	0	
SOM4	0	0	$-(1-f_6)R_6'$	$R_7'$	0	0	
$CO_2$	$-f_4R_4'$	$-f_5R'_5$	$-f_6R'_6$	$-R_7'$	0	0	
$N_{\mathrm{mineral}}$	$-n_4R_4'$	$-n_5R_5'$	$-n_6R_6'$	$-n_7R_7'$	0	0	

## 1.4 Applications

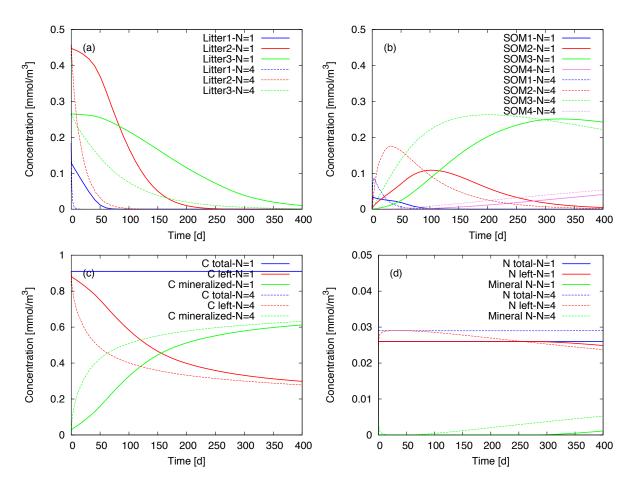


Figure 2: Demonstrating N limiting on C decomposition (initial mineral N=1 and 4  $\mu$  mol/m<sup>3</sup>)

## 2 CLM4.5 CH<sub>4</sub> Oxidation

### 2.1 Reaction

$$CH_4 + 2O_2 = CO_2 + 2H_2O$$
 (13)

### 2.2 Rate

$$R = k \frac{\text{CH}_4}{k_{\text{CH}4} + \text{CH}_4} \frac{\text{O}_2}{k_{\text{O}2} + \text{O}_2} f_T f_{\Psi}$$
 (14)

### 2.3 Residuals

$$\mathcal{R}_{\text{CH4}} = \frac{\Delta V}{\Delta t} \left( \text{CH}_4^{k+1} - \text{CH}_4^k \right) + R^{k+1} \Delta V$$

$$\mathcal{R}_{\text{O2}} = \frac{\Delta V}{\Delta t} \left( \text{O}_2^{k+1} - \text{O}_2^k \right) + 2R^{k+1} \Delta V$$

$$\mathcal{R}_{\text{CO2}} = \frac{\Delta V}{\Delta t} \left( \text{CO}_2^{k+1} - \text{CO}_2^k \right) - R^{k+1} \Delta V$$

## 2.4 Jacobian

$$\frac{\partial R}{\partial \text{CH}_4} = k \frac{k_{\text{CH}4}}{(k_{\text{CH}4} + \text{CH}_4)^2} \frac{\text{O}_2}{k_{\text{O}2} + \text{O}_2} f_T f_{\Psi} = R'_{\text{CH}4}$$
$$\frac{\partial R}{\partial \text{O}_2} = k \frac{\text{CH}_4}{k_{\text{CH}4} + \text{CH}_4} \frac{k_{\text{O}2}}{(k_{\text{O}4} + \text{O}_2)^2} f_T f_{\Psi} = R'_{\text{O}2}$$

Table 6: Jacobian for methane oxidation

	$\mathrm{CH}_4$	$O_2$	$CO_2$
$\mathrm{CH}_4$	$R'_{ m CH4}$	$R'_{\rm O2}$	0
$O_2$	$2R'_{\mathrm{CH4}}$	$2R'_{\rm O2}$	0
$CO_2$	$-R'_{\rm CH4}$	$-R'_{\rm O2}$	0

## 2.5 Application

Input file

CHEMISTRY
PRIMARY\_SPECIES
02(aq)
Methane(aq)
C02(aq)

```
REDOX_SPECIES
   CO2(aq)
   Methane(aq)
    02(aq)
 REACTION_SANDBOX
   CH40
      RATE_CONSTANT 1.25d-10 ! mol/m3 s
     HALFSATURATIONCH4 5.0d-6
     HALFSATURATIONO2 2.0d-5
 DATABASE ../../pflotran-clm4me/database/hanford.dati
CONSTRAINT initial
 CONCENTRATIONS
    02(aq)
           0.001 T
   Methane(aq) 0.001 T
   CO2(aq) 1.0d-10 T
END
  Code
subroutine CH4OReact(this, Residual, Jacobian, compute_derivative, &
                         rt_auxvar,global_auxvar,porosity,volume,reaction, &
                         option)
 word = "Methane(aq)"
  is_ch4 = GetPrimarySpeciesIDFromName(word,reaction,option)
 word = "CO2(aq)"
  is_co2 = GetPrimarySpeciesIDFromName(word,reaction,option)
 word = "02(aq)"
  is_o2 = GetPrimarySpeciesIDFromName(word,reaction,option)
 temp_K = global_auxvar%temp(1) + 273.15d0
 F_t = \exp(308.56d0*(one\_over\_71\_02 - 1.d0/(temp_K - 227.13d0)))
 F_theta = log(theta_min/global_auxvar%sat(1)) * one_over_log_theta_min
 L_water = porosity*global_auxvar%sat(iphase)*volume*1.d3
 c_ch4 = rt_auxvar%total(is_ch4,iphase)
 c_o2 = rt_auxvar%total(is_o2,iphase)
 rate = this%rate_constant * L_water * & ! mole/(L sec)
```

```
c_ch4/(this\%kmch4 + c_ch4) * c_o2/(this\%kmo2 + c_o2) * F_t * F_theta
Residual(is_ch4) = Residual(is_ch4) + rate
Residual(is_o2) = Residual(is_o2) + 2.0 * rate
Residual(is_co2) = Residual(is_co2) - rate
if (compute_derivative) then
  ! always add contribution to Jacobian
  ! units = (mol/sec)*(kg water/mol) = kg water/sec
  \frac{1}{2} dx/(k+x) = k/(k+x)^2
  drate_dch4 = rate * this%kmch4 / c_ch4 / (this%kmch4 + c_ch4)
  drate_do2 = rate * this%kmo2 / c_o2 / (this%kmo2 + c_o2)
  Jacobian(is_ch4,is_ch4) = Jacobian(is_ch4,is_ch4) - drate_dch4
  Jacobian(is_ch4,is_o2) = Jacobian(is_ch4,is_o2) - drate_do2
  Jacobian(is_o2,is_ch4) = Jacobian(is_o2,is_ch4) - 2.0 * drate_dch4
  Jacobian(is_o2,is_o2) = Jacobian(is_o2,is_o2) - 2.0 * drate_do2
  Jacobian(is_co2,is_ch4) = Jacobian(is_co2,is_ch4) + drate_dch4
  Jacobian(is_co2,is_o2) = Jacobian(is_co2,is_o2) + drate_do2
```

#### endif

end subroutine CH40React

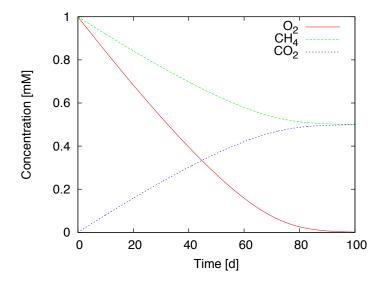


Figure 3: Example calculation for methane oxidation)

## 3 Acetoclastic Methanogenesis

## 3.1 Reaction

$$Ac^{-} + H_2O = CH_4 + HCO_3^{-}$$
 (15)

$$(1 + y/2)Ac^{-} + 0.5yH^{+} + H_{2}O = CH_{4} + HCO_{3}^{-} + yC_{bio}$$
(16)

### 3.2 Rate

$$R = k C_{\text{bio}} \frac{Ac^{-}}{k_{\Lambda c} + Ac^{-}} f_{T} f_{\Psi}$$

$$\tag{17}$$

### 3.3 Mass Conservation

$$\frac{\partial Ac^{-}}{\partial t} = -(1 + \frac{y}{2})R$$

$$\frac{\partial H^{+}}{\partial t} = -\frac{y}{2}R$$

$$\frac{\partial CH_{4}}{\partial t} = R$$

$$\frac{\partial HCO_{3}^{-}}{\partial t} = R$$

$$\frac{\partial C_{\text{bio}}}{\partial t} = 1000\theta yR$$

Note: for the last equation, PFLOTRAN accounts for the  $1000\theta$  internally.

### 3.4 Residuals

$$\mathcal{R}_{Ac-} = \frac{\Delta V}{\Delta t} \left( Ac^{-k+1} - Ac^{-k} \right) + (1 + y/2)R^{k+1}\Delta V$$

$$\mathcal{R}_{CH4} = \frac{\Delta V}{\Delta t} \left( CH_4^{k+1} - CH_4^k \right) - R^{k+1}\Delta V$$

$$\mathcal{R}_{Cbio} = \frac{\Delta V}{\Delta t} \left( C_{bio}^{k+1} - C_{bio}^k \right) - yR^{k+1}\Delta V$$

$$\mathcal{R}_{HCO3-} = \frac{\Delta V}{\Delta t} \left( HCO_3^{-k+1} - HCO_3^{-k} \right) - R^{k+1}\Delta V$$

$$\mathcal{R}_{H+} = \frac{\Delta V}{\Delta t} \left( H^{+k+1} - H^{+k} \right) + y/2R^{k+1}\Delta V$$

## 3.5 Jacobian

$$\frac{\partial R}{\partial Ac} = kC_{\text{bio}} \frac{k_{\text{Ac}}}{(k_{\text{Ac}} + Ac^{-})^{2}} f_{T} f_{\Psi} = R'_{a}$$

$$\frac{\partial R}{\partial C_{\text{bio}}} = k \frac{Ac^{-}}{k_{\text{Ac}} + Ac^{-}} f_{T} f_{\Psi} = R'_{b}$$

Table 7: Jacobian for methane oxidation					
	$Ac^-$	$\mathrm{CH}_4$	$C_{ m bio}$	$HCO_3^-$	$\mathrm{H}^{+}$
$Ac^-$	$(1+y/2)R_a'$	0	$(1+y/2)R_b'$	0	0
$\mathrm{CH}_4$	$-R'_a$	0	$-R_b'$	0	0
$C_{\mathrm{bio}}$	$-yR'_a$	0	$-yR_b'$	0	0
$HCO_3^-$	$-R'_a$	0	$-R_b'$	0	0
$\mathrm{H}^{+}$	$0.5yR'_a$	0	$0.5yR_b'$	0	0

## 3.6 Application

```
Input
CHEMISTRY
 PRIMARY_SPECIES
    Acetate-
   Methane(aq)
   HCO3-
 SECONDARY_SPECIES
    OH-
   CO3--
   CO2(aq)
    Acetic_acid(aq)
 REDOX_SPECIES
    Acetate-
   Methane(aq)
  IMMOBILE_SPECIES
    Acemeg
 REACTION_SANDBOX
     AceMeg
      RATE_CONSTANT
                         1.0d-6
      HALFSATURATIONAC
                         1.0d-5
```

```
YIELDCOEFFICIENT 0.02
 DATABASE ../../pflotran-clm4me/database/hanford.dat
/end{verbatim}
\noindent Code
\begin{verbatim}
 L_water = porosity*global_auxvar%sat(iphase)*volume*1.d3
 c_ac = rt_auxvar%pri_molal(this%is_ac)
 c_bio = rt_auxvar%immobile(this%ispec_id_cbio)
 rate = this%rate_constant * L_water * &
   c_bio * c_ac/(this\%kmac + c_ac) * F_t * F_theta
 ! alway subtract contribution from residual (mole/sec)
 Residual(this%is_ac) = Residual(this%is_ac) + (1.0 + 0.5 * this%yield) * rate
 Residual(this%is_ch4) = Residual(this%is_ch4) - rate
 Residual(this%is_cbio) = Residual(this%is_cbio) - this%yield * rate
 Residual(this%is_hco3) = Residual(this%is_hco3) - rate
 Residual(this%is_h) = Residual(this%is_h) + 0.5 * this%yield * rate
 if (compute_derivative) then
! 11. If using an analytical Jacobian, add code for Jacobian evaluation
    ! always add contribution to Jacobian
    ! units = (mol/sec)*(kg water/mol) = kg water/sec
   drate_dac = rate * this%kmac / c_ac / (this%kmac + c_ac)
   drate_dcb = rate / c_bio
    Jacobian(this%is_ac, this%is_ac)
                                        = Jacobian(this%is_ac,this%is_ac)
                                        - (1.0 + 0.5 * this\%yield) * drate_dac
    Jacobian(this%is_ch4, this%is_ac)
                                        = Jacobian(this%is_ch4,this%is_ac)
                                        + drate_dac
                                        = Jacobian(this%is_cbio,this%is_ac) &
    Jacobian(this%is_cbio,this%is_ac)
                                        + this%yield * drate_dac
    Jacobian(this%is_hco3,this%is_ac)
                                        = Jacobian(this%is_hco3,this%is_ac) &
                                        + 0.5 * this%yield * drate_dac
    Jacobian(this%is_ac, this%is_cbio) = Jacobian(this%is_ac,this%is_cbio) &
                                        - (1.0 + 0.5 * this\%yield) * drate_dcb
    Jacobian(this%is_ch4, this%is_cbio) = Jacobian(this%is_ch4,this%is_cbio) &
                                        + drate_dcb
    Jacobian(this%is_cbio,this%is_cbio) = Jacobian(this%is_cbio,this%is_cbio) &
                                        + this%yield * drate_dcb
```

endif

For  $k_{Ac} = 0$ ,

$$\begin{split} \frac{\partial \mathbf{A} \mathbf{c}}{\partial t} &= -(1+0.5y)k\mathbf{C}_{\mathrm{bio}} \\ \frac{\partial \mathbf{C}_{\mathrm{bio}}}{\partial t} &= 1000\theta y k\mathbf{C}_{\mathrm{bio}} \end{split}$$

$$\begin{aligned} \mathbf{C}_{\mathrm{bio}} &= \mathbf{C}_{\mathrm{bio},0} \mathrm{EXP}(1000\theta y k t) \\ \mathrm{Ac} &= \mathrm{Ac}_0 - \frac{1 + 0.5 y}{1000\theta y} \mathbf{C}_{\mathrm{bio},0} \mathrm{EXP}(1000\theta y k t) \end{aligned}$$

This analytical solution is used in the following figure to check the numerical solution. Note  $C_{\rm bio}$  is supposed to stop increasing when acetate is exhausted.

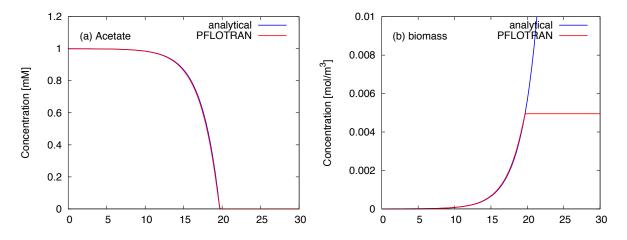


Figure 4: Example calculation for acetoclastic methanogenesis:

## References

- E. Carol Adair, William J. Parton, Steven J. del Grosso, Whendee L. Silver, Mark E. Harmon, Sonia A. Hall, Ingrid C. Burke, and Stephen C. Hart. Simple three-pool model accurately describes patterns of long-term litter decomposition in diverse climates. *Global Change Biology*, 14(11):2636–2660, 2008. ISSN 1365-2486. doi: 10.1111/j.1365-2486.2008.01674.x. URL http://dx.doi.org/10.1111/j.1365-2486.2008.01674.x.
- Gordon B. Bonan, Melannie D. Hartman, William J. Parton, and William R. Wieder. Evaluating litter decomposition in earth system models with long-term litterbag experiments: an example using the community land model version 4 (clm4). *Global Change Biology*, pages n/a-n/a, 2012. ISSN 1365-2486. doi: 10.1111/gcb.12031. URL http://dx.doi.org/10.1111/gcb.12031.