



**CE-580**

**COMPUTATIONAL TECHNIQUES**

**FOR**

**FLUID DYNAMICS**

**HOMEWORK #8**

**Finite Volume Solution to Turbulent Pipe Flow Using  
Wall Functions**

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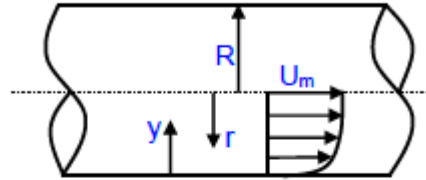
**1881978**

## CE 580 COMPUTATIONAL TECHNIQUES FOR FLUID DYNAMICS

### Homework 8

#### Finite Volume Solution to Turbulent Pipe Flow Using Wall Functions

Develop a computer program to obtain velocity distribution from an implicit FV solution to steady, uniform, turbulent flow in a circular pipe.



1. Use mixing length theory as the turbulence model.
2. Apply the boundary conditions

$$u = 0 \text{ at } y = 0 \quad \text{and} \quad u = U_m \text{ at } y = R.$$

3. Obtain initial data for velocity from the power law:  $u(y) = U_m (y/R)^{1/7}$
4. Consider the steady momentum equation. Obtain a finite volume discretization for variable mesh size. Generate the computational grid using constant ratio method. Describe an implicit solution to the discretized FV equations.
5. Obtain the wall shear stress from the logarithmic law of the wall. Describe the percent change in shear velocity in two consecutive iterations as computational error and terminate iterations when this change is negligible.
6. Determine the Reynolds number and the friction factor ( $f_m$ ) from the experimental formula. Compute the friction factor ( $f_c$ ) using the computed average velocity and the wall shear stress in the Darcy's equation. Compute the percent error between the experimental and computed friction factors.
7. Run your program for the data given below:

$U_m = 4 \text{ m/s}$	$R = 0.1 \text{ m}$	$N = 20$
$\nu = 1 \times 10^{-6} \text{ m}^2/\text{s}$	$\rho = 1000 \text{ kg/m}^3$	$\epsilon_{\max} = 1 \times 10^{-5}$
Grid ratio (G) = 1, 0.95, 0.90 and 0.86		

8. Make logarithmic plots of the velocity profiles ( $u^+ \sim y^+$ ) on the same page.
9. Prepare a table of results, presenting G,  $y_1^+$ ,  $f_c$ ,  $100 \cdot |f_c - f_m| / f_m$ , and number of iterations.
10. Write a discussion on the results you obtained.

### Assumptions

Using central differences for control points

$$r_{i+1}(v_e)_{i+1} \frac{u_{i+1} - u_i}{(\Delta_m)_{i+1}} - r_i(v_e)_i \frac{u_i - u_{i-1}}{(\Delta_m)_i} = \Delta_i(r_m)_i C_p$$

Defining new parameters for constants

$$a_i = \frac{r_i}{(\Delta_m)_i}, \quad d_i = \Delta_i(r_m)_i, \quad \Delta_i = y_{i+1} - y_i, \quad (\Delta_m)_i = \frac{(\Delta_i - \Delta_{i-1})}{2}$$

The tridiagonal form is

$$-A_i u_{i+1} + B_i u_i - C_i u_{i-1} = D_i$$

And coefficients A, B, C, D are

$$A_i = a_{i+1} v_{e_{i+1}}; \quad C_i = a_i v_{e_i}; \quad B_i = A_i + C_i; \quad D_i = -d_i C_p$$

Effective viscosity and Turbulent viscosity are calculated using mixing-length theory.

$$v_e = \nu + \nu_t$$

$$\mu_t = \rho \nu_t = \rho l_m^2 \frac{du}{dy}$$

Where

$$l_m = H \left[ 0.14 - 0.08 \left( 1 - \frac{y}{H} \right)^2 - 0.06 \left( 1 - \frac{y}{H} \right)^4 \right] f_\mu$$

$$f_\mu = 1 - \exp \left( -\frac{y^+}{A^+} \right) \quad A^+ = 26$$

$$y^+ = \frac{y u_*}{\nu} \quad u_* = \sqrt{\frac{\tau_w}{\rho}}$$

Instead of calculating wall shear,  $u_*$  is calculated at the first control point that is outside of the viscous sublayer using wall functions. Then wall shear is calculated using above relation.

$$\frac{u}{u_*} = \frac{1}{\kappa} \ln(y^+) + \beta$$

$$\kappa = 0.41, \quad \beta = 5.3$$

After calculating wall shear,  $C_p$  can be determined using the relation

$$C_p = \frac{\partial p}{\partial x} = -2 \frac{\tau_w}{\text{Radius} \times \rho}$$

Grid is generated with constant ratio method Ratio between any two neighboring meshes is constant

$$\Delta Y_i = G \Delta_{i+1}$$

Distance between the last two mesh point can be calculated as

$$\Delta Y_N = \frac{H}{\sum_{i=0}^{N-2} G^i}$$

Mesh distribution can be completed marching down from N to 1

### **Boundary Conditions**

At (i=1) wall the momentum equation is

$$a_2(v_e)_2(u_2 - u_1) - R\tau_w = d_1C_p$$

After finding wall shear stress as described above, Define a relation for wall shear

$$C_w = \frac{\tau_w}{u_1}$$

Then the momentum balance for the first cell is

$$a_2(v_e)_2(u_2 - u_1) - RC_w u_1 = d_1C_p$$

In tridiagonal form coefficients A, B, C, D will be

$$-A_1 u_2 + B_1 u_1 - C_1 u_0 = D_1$$

$$A_1 = a_2(v_e)_2, \quad C_1 = 0, \quad B_1 = A_1 + C_w R, \quad D_1 = -d_1 C_p$$

Note that  $u_0$  is not defined, For no slip boundary condition on the wall:

$$u_w = E_0 u_1 + F_0 = 0, \quad E_0 = 0; F_0 = 0$$

At the centerline (i=N) momentum balance is

$$a_{N+1}(v_e)_{N+1}(u_{N+1} - u_N) - a_N(v_e)_N(u_N - u_{N-1}) = d_N C_p$$

In tridiagonal form

$$-A_N u_{N+1} + B_N u_N - C_N u_{N-1} = D_N$$

Where coefficients A, B, C, D are

$$A_N = 0 \text{ (At symmetry line } u_{N+1} = u_N)$$

$$C_N = a_N(v_e)_N, \quad B_N = C_N, \quad D_N = -d_N C_p$$

### **Initial condition**

An initial velocity distribution to start the solution procedure is get from the power law.

$$u(y) = U_{max} \left( \frac{y}{R} \right)^{\frac{1}{7}}$$

### **Error Calculation**

Error is defined as relative change in shear velocity, such as

$$Error = \frac{|u_{*old} - u_*|}{u_{*old}}$$

## Outputs

Required outputs can be calculated once the solution is converged

### Discharge

$$Q = \int u \times dA$$

Above integral can be taken numerically as such

$$Q = 2\pi \sum_{i=2}^N \frac{r_i + r_{i-1}}{2} \times \frac{(u_i + u_{i-1})}{2} \times \Delta_i$$

### Average velocity

$$V_{ave} = \frac{Q}{A}$$

### Reynolds Number

$$Re = \frac{V_{ave} \times D}{\nu}$$

### Friction factors

From experimental data, using Swamee-Jain formula

$$f_m = \frac{0.25}{\left[ \log \left( \frac{k_s}{3.7D} + \frac{5.74}{Re^{0.9}} \right) \right]^2}$$

Since we assumed smooth pipe we can drop  $k_s$  term and equation becomes

$$f_m = \frac{0.25}{\left[ \log \left( \frac{5.74}{Re^{0.9}} \right) \right]^2}$$

From the converged solution, using Darcy's friction factor

$$f_d = \frac{8\tau_w}{\rho V_{ave}^2}$$

## Input Data

$$U_{max} = 4 \frac{m}{s} , \quad R = 0.1 \, m , \quad N = 20$$

$$\nu = 1 \times 10^{-6} \frac{m^2}{s} , \quad \rho = 1000 \frac{kg}{m^3} , \quad \epsilon_{max} = 1 \times 10^{-5}$$

$$Grid \, Raito = G = 1; 0.95; 0.90; 0.86$$

## Results and Discussion

Using wall functions saves us from grid refinement on solid boundaries. However, there is still a restriction on  $y_+$  value at the first grid point. It should be between 30 and 300, in other words, first grid point should be at fully turbulent region of the boundary layer. The reason is that wall function that is used (log law) is valid at turbulent region. If  $y_+$  value is in the valid range, wall shear can be estimated and using wall shear pressure drop can be calculated.

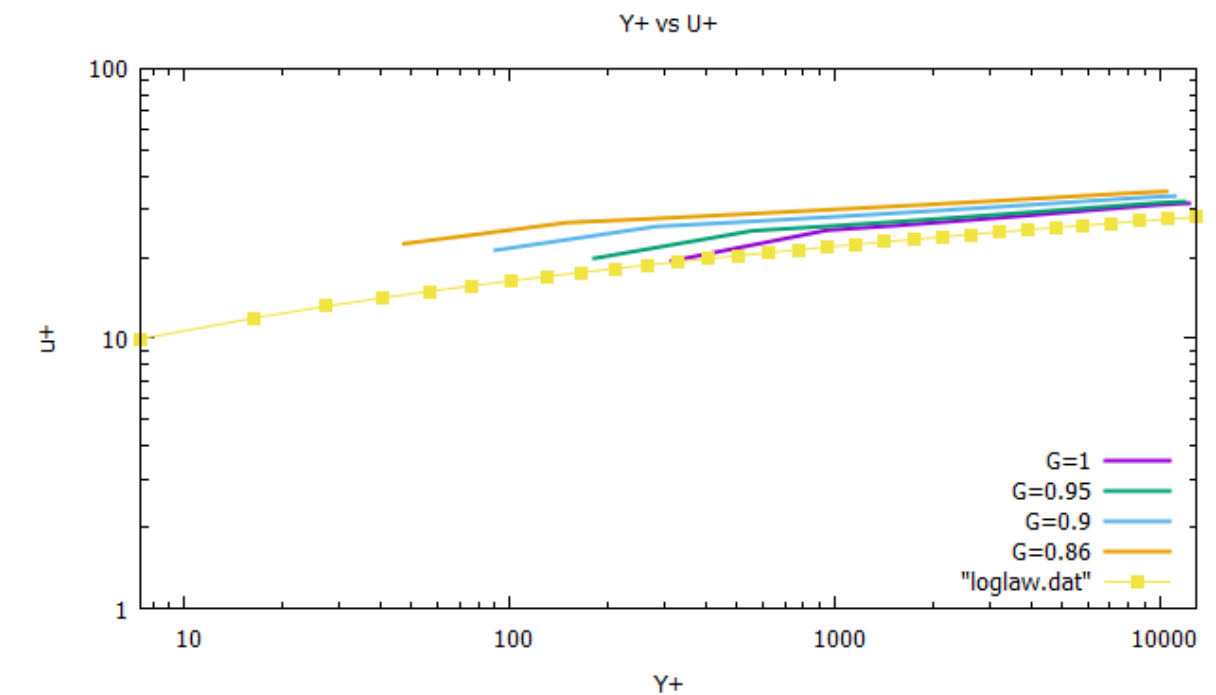


Figure 2:  $y_+$  vs  $u_+$  variation along grid points

Figure 2 shows the variation of  $u_+$  with respect to  $y_+$ . As grid refinement applied towards to the wall the solution stray away from log law behavior. This may be caused by interaction with buffer layer and turbulent layer at the first grid point, since first grid is very close to the wall. On the other hand, without grid refinement the solution matches with log law, meaning that first grid point is well placed to approximate wall shear.

Grid Ratio	$Y_+(1)$	$f_c$	$100 *  f_c - f_m  / f_m$	Iterations
0.86	47.28	$8.8 \cdot 10^{-3}$	28.96	50
0.9	90.43	$9.57 \cdot 10^{-3}$	22.79	51
0.95	181.81	$1.05 \cdot 10^{-2}$	14.68	51
1	314.23	$1.09 \cdot 10^{-2}$	11.81	50
<b>Table 1: Output Values</b>				

Table 1 shows the output values, after change in shear velocity in consequent iterations is small enough. Since the solution is implicit convergence achieved rapidly, and due to the algorithm to find shear velocity all three cases converged at 50 iterations.

Although all  $y_+$  values are in range of 30 and 300. The best result is achieved with the grid ratio of 1. As first grid moves closer to the wall, percent difference between Darcy's friction factor and experimental formula becomes larger. Again the reason for that may be the interaction with buffer layer and turbulent layer.



## Code Listing

```
program PipeFlow
c Taha Yaşar Demir / 1881978
c CE-580 HomeWrok #8
  parameter(mx=100)
  common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
  common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
  common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
  common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
  common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count

  call Init
  call Prior
  open(11,file="yplus.dat")
  open(12,file="output.dat")
  err = 1.
  count= 0.
  do while(err.gt.Tol)
c    do k=1,100
      call Solution
      count = count +1
      call Update
      print*, 'iteration number', count , 'Error' , err
      call Output
    enddo
  close(11)
  close(12)

  stop
end

c-----
subroutine Init
  parameter(mx=100)
  common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
  common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
  common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
  common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
  common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count

  Um = 4. ! m/s
  vis = 1e-6 ! m^2/s
  G = 1. ! Grid Ratio 1 - 0.95 - 0.9 - 0.86
  Rad = 0.1 ! m
  rho = 1000. ! kg/m^3
  N = 20 ! Grid points
  Tol = 1e-5 ! Error criteria
  Ap = 26.
  Pi = 22./7.
  rkp = 0.41
  beta= 5.3
```

```
call MakeGrid
call Analytic
```

```
return
end
```

C-----

```
subroutine MakeGrid
parameter(mx=100)
common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
real sum
```

```
sum = 0.0
do i=0,N-1
    sum = sum + G**i
enddo
dy(N+1) = Rad/sum
y(N+1) = Rad
```

```
do i=N+1,2,-1
    y(i-1) = y(i)-dy(i)
    dy(i-1) = G*dy(i)
    yc(i-1) = (y(i)+y(i-1))/2.
    r(i) = Rad - y(i)
    rc(i-1) = Rad - yc(i-1)
    print*, 'grid', y(i-1),dy(i-1),yc(i-1),r(i),rc(i-1)
```

C

```
enddo
do i=2,N
    dm(i) = (dy(i)+dy(i-1))/2
enddo
r(1) = Rad
y(1) = 0.

return
end
```

C-----

```
subroutine Analytic
parameter(mx=100)
common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
```

```
do i=1,N
    u(i) = Um*(yc(i)/Rad)**(1./7.)
enddo
```

```
return
end
```

C-----

```
subroutine Prior
parameter(mx=100)
```

```

common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count

```

```

Disc = 0.
do i=1,N
  Disc = Disc + 2.*pi*rc(i)*u(i)*dy(i)
enddo
V_ave = Disc/(pi*Rad**2)
V_ave = 0.85*Um
Re = 2.*V_ave*Rad/vis
fm = 0.25/((log10(5.74/(Re**0.9)))**2)
fd = fm
tau_w = (rho*fd*V_ave**2)/8.
us = sqrt(tau_w/rho)
do i=1,N
  yp(i) = yc(i)*us/vis
  fu(i) = 1-exp(-yp(i)/Ap)
  fml(i) = Rad*(0.14-0.08*(1-(yc(i)/Rad))**2
    & -0.06*(1-(yc(i)/Rad))**4)*fu(i)
enddo
do i=2,N
  vist(i) = (fml(i)**2)*abs((u(i)-u(i-1))/dm(i))
  vise(i) = (vis + vist(i))
enddo

return
end

```

```

c-----
subroutine Solution
parameter(mx=100)
common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count

Cp = -2.*(tau_w/Rad)/rho
Cw = tau_w/u(1)
do i=1,N
  cd(i) = dy(i)*rc(i)
enddo
do i=2,N
  ca(i) = r(i)/dm(i)
enddo

rtau(N+1) = 0.
do i=N,2,-1
  rtau(i) = rtau(i+1) - dy(i)*rc(i)*Cp
enddo

```

```

c      u(N) = 4.
      do i=N,3,-1
          u(i-1)= u(i) - (rtau(i)*dm(i))/(r(i)*vise(i))
      enddo
      u(1) = u(2) - (rtau(2)*dm(2))/(r(2)*vise(2))/r(2) - tau_w/rho
      print*, 'u1', u(1) , 'tau_w', tau_w, 'Cp', Cp, 'uN', u(N)

      return
      end

```

```

C-----
      subroutine Update
      parameter(mx=100)
      common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
      common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
      common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
      common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
      common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count
      real law, us_old

      us_old = us
      call ustar
      tau_w = (us**2)*rho
      err = abs(us_old-us)/us_old
      print*, 'error',err,us
      do i=1,N
          yp(i) = yc(i)*us/vis
          fu(i) = 1-exp(-yp(i)/Ap)
          fml(i) = Rad*(0.14-0.08*(1-(yc(i)/Rad))**2
&          -0.06*(1-(yc(i)/Rad))**4)*fu(i)
      enddo
      do i=2,N
          ! Take average of two consequent viscous stress to eliminate oscilation
          vist(i)=(vist(i)+((fml(i)**2)*abs((u(i)-u(i-1))/dm(i))))/2.
c      vist(i)=(((fml(i)**2)*abs((u(i)-u(i-1))/dm(i))))
          vise(i) = vis + vist(i)
      enddo

      return
      end

```

```

C-----
      subroutine ustar
      parameter(mx=100)
      common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
      common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
      common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
      common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
      common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count
      real test, yplus
      yplus = us*yc(1)/vis
      test = us*(1/rkp)*log(yplus) + us*beta
      if(test.lt.u(1)) then

```

```

        us = us+ 0.005*us/(10*count)

    else

        us = (0.995*us+us)/2

    endif

    return
end

```

c-----

```

subroutine Output
parameter(mx=100)
common/grid/ Rad,r(mx),rc(mx),y(mx),yc(mx),dy(mx),dm(mx),N,G
common/var/ tau_w,u(mx),vis,vist(mx),vise(mx),rho,Um,rtau(mx)
common/const/Cp,rkp,beta,Cw,ca(mx),cd(mx),a(mx),b(mx),c(mx),d(mx)
common/turb/ fml(mx),fu(mx),yp(mx),Ap,us,up(mx)
common/out/ fm,fd,V_ave,Disc,Re,Pi,err,Tol,count
real loglaw,relative
do i=1,N
    Disc = Disc + 2.*pi*rc(i)*u(i)*dy(i)
enddo
V_ave = Disc/(pi*Rad**2)
c V_ave = 0.85*Um
Re = 2.*V_ave*Rad/vis
fm = 0.25/((log10(5.74/(Re**0.9)))**2)
fd = (8*tau_w)/(rho*(V_ave**2))
if(err.lt.Tol) then
do i=1,N
    yp(i) = us*yc(i)/vis
    up = u(i)/us
    loglaw= (1./rkp)*log(yp(i))+beta
    write(11,*) yp(i),up(i),loglaw
enddo
else
relative = 100*abs(fd-fm)/fm
write(12,*) G,yp(1),fd,relative,count
print*,'Ratio',' yp1',' fc',' difference',' Iteration'
print*, G,yp(1),fd,relative,count
endif
return

```

Fortran Code Used for Calculations