

PLACE 2016

EXPLORING
NEW FRONTIERS

April 11-13 2016
FORT WORTH TEXAS

Learning from Shear and Extensional Rheology of a few Extrusion Coating Polyethylenes



CLOEREN
INCORPORATED

Presented by:
Olivier Catherine
Cloeren Incorporated

TAPPI
people resources solutions®

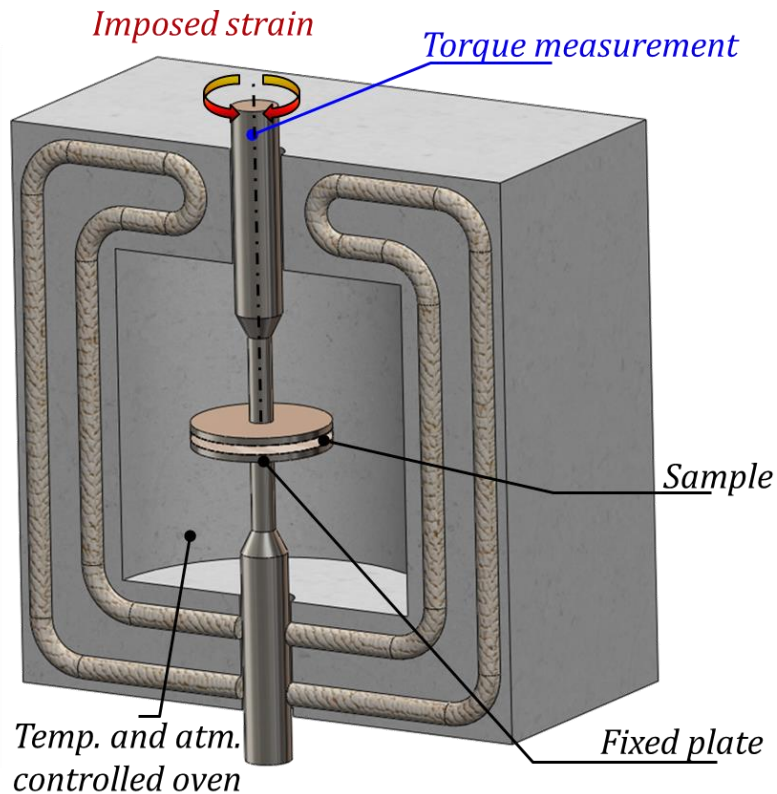


Introduction

- This presentation is the start of on-going work to determine the relationship between **polymer molecular structure & polydispersity / rheology / process-ability / final properties**
- Rheometry is a powerful tool to investigate the macromolecular structure of polymer melts and recent tools have been used to characterize a few extrusion coating grade resins
- Ultimate goal: to be able to **model** or **predict** through correlations between rheology and processing data:
 - Neck-in
 - Process Stability

Shear rheology: dynamic measurements

- Rotational Rheometer

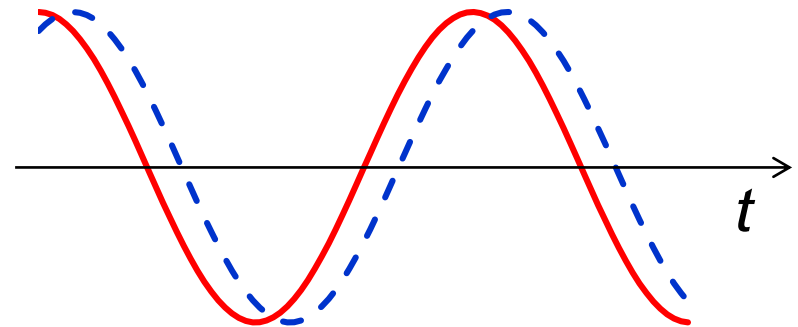


Dynamic strain is imposed:

$$\gamma^* = \gamma_0 \exp(i\omega t)$$

Delayed Shear stress response :

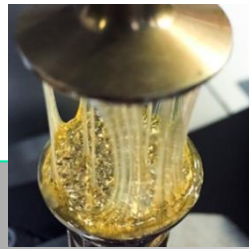
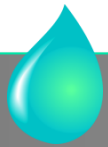
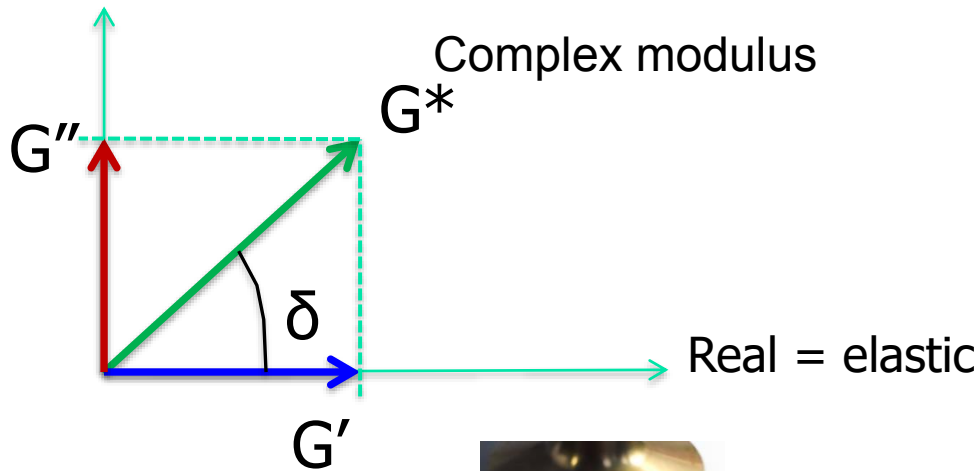
$$\tau^* = \tau_0 \exp i(\omega t + \delta)$$



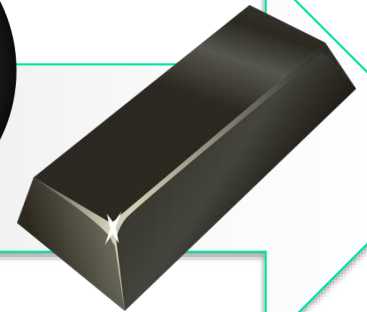
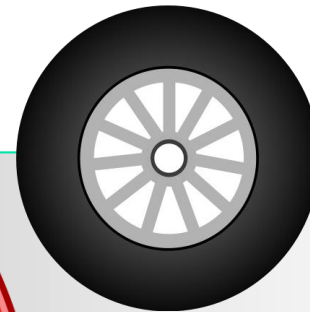


Shear rheology: dynamic measurements

Imaginary = Viscous



Polymer melts



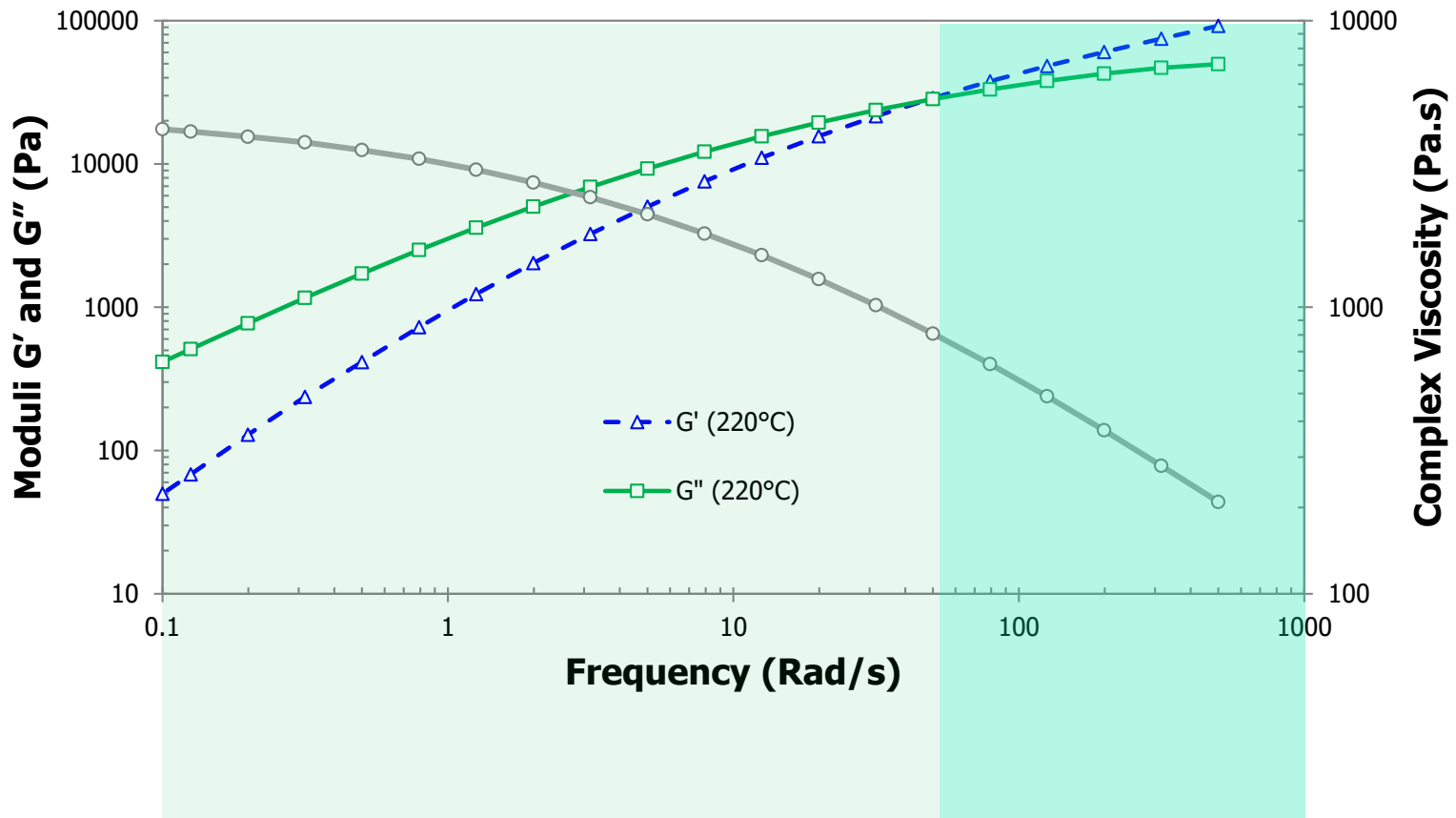
Ideally viscous

Ideally elastic



Shear rheology: dynamic measurements

Frequency sweep in linear viscoelastic region (LVR)

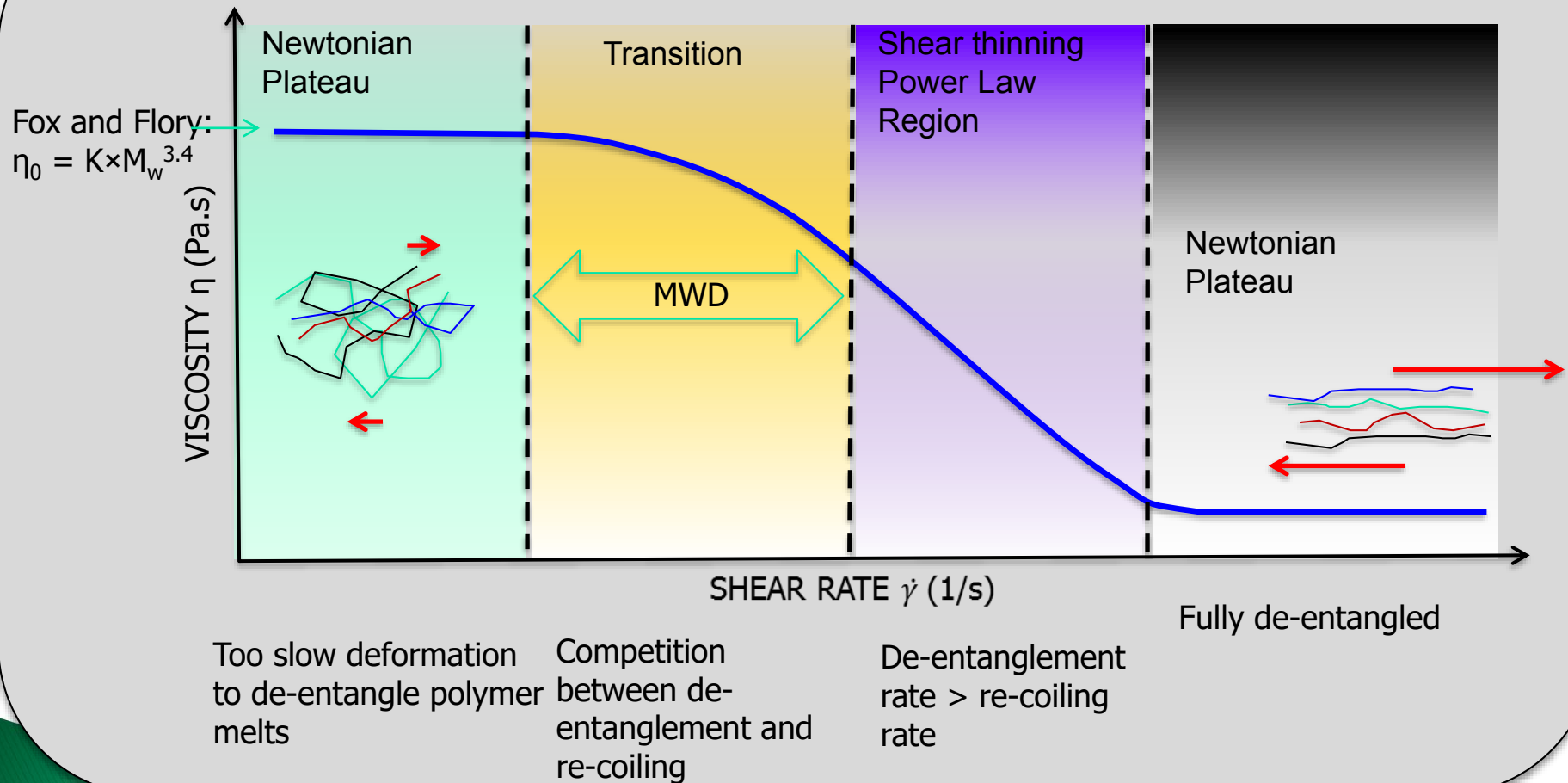


Low frequency: $G'' > G'$
(viscous dominant)

High frequency: $G' > G''$
(elastic dominant)



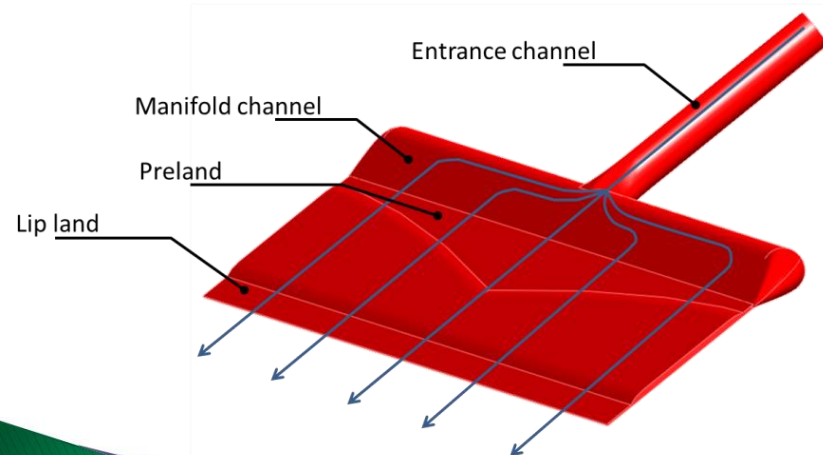
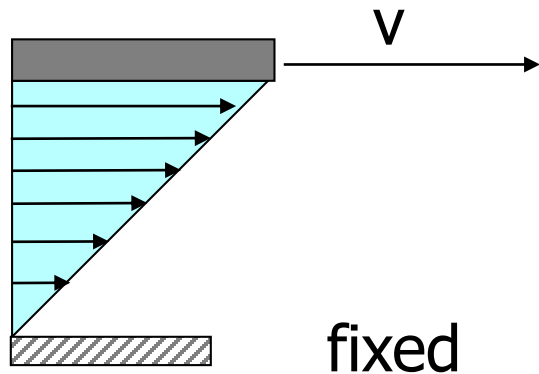
Shear rheology: dynamic measurements



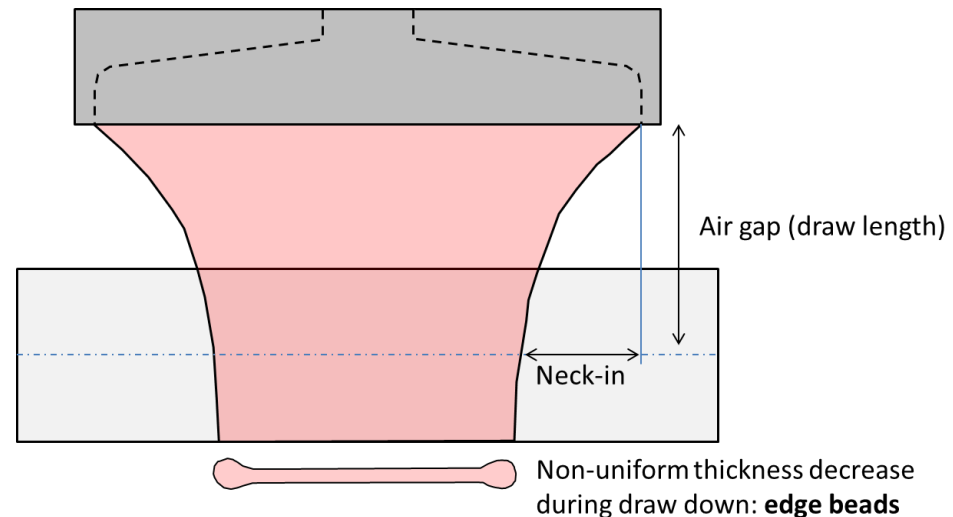
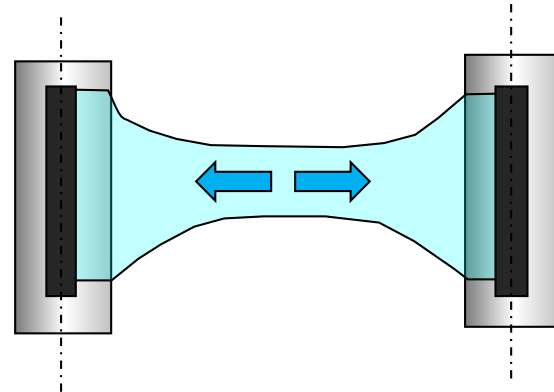


Elongational Viscosity – Neck in behavior

■ Shear flow



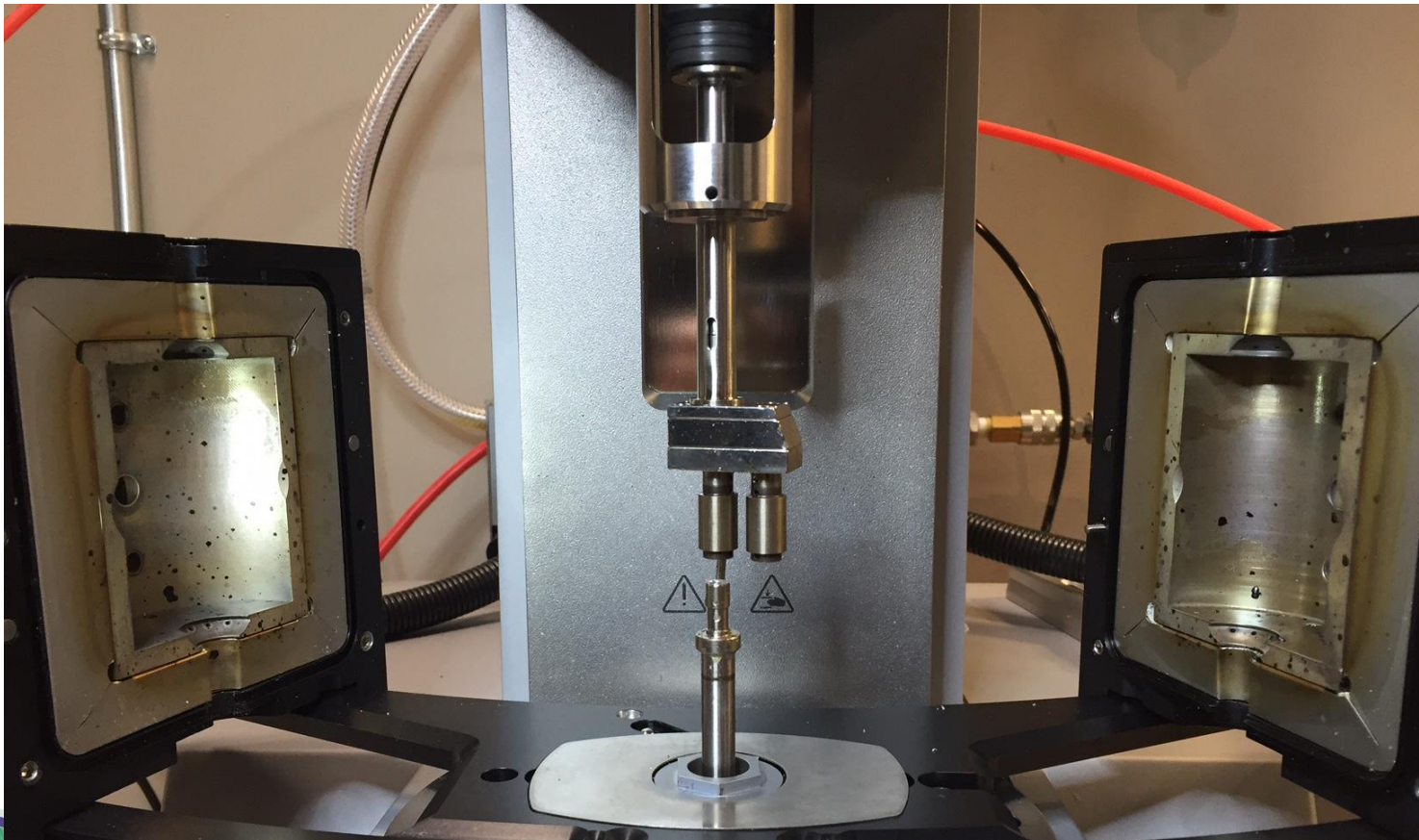
■ Extensional flow





Elongational Viscosity measurement

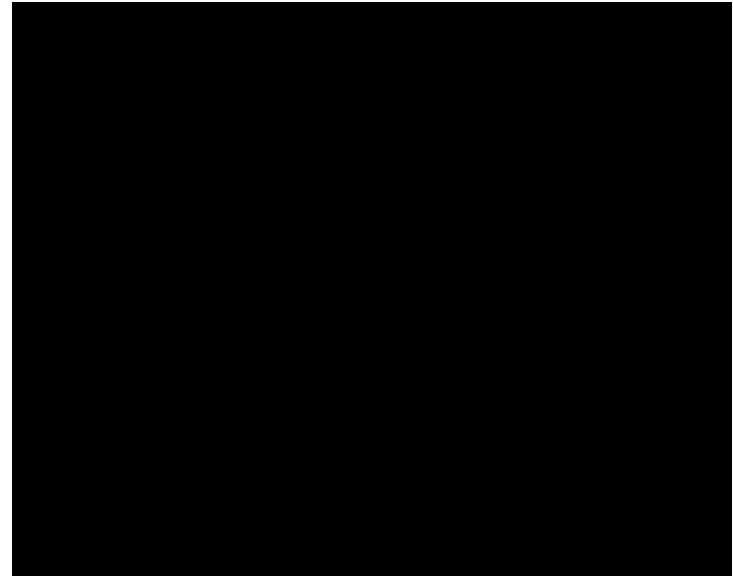
■ Sentmanat Extensional Rheometer (SER)





Elongational Viscosity measurement

■ Sentmanat Extensional Rheometer (SER)





Polymers

■ Tested materials:

Name	Commercial name	Type	Density (g/cm ³)	MFI (g/10 min)	Comment
LD1	Chevron Phillips Marflex 1017	Autoclave LDPE	0.917	7.0	Reference material
LD2	Westlake Chemical EC808AA	Autoclave LDPE	0.917	7.0	Similar to reference
m-PE	ExxonMobil Exceed 0019XC	m-PE	0.918	19	Molecular structure and molecular weight
LD3	Chevron Phillips Marflex 1019	Autoclave LDPE	0.917	16	Similar molecular weight as 0019XC?

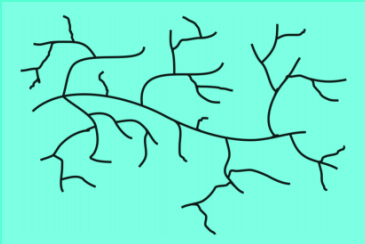


Molecular structure

■ Extrusion Coating resins tested:

■ LDPE:

- Broad molecular weight distribution
- Long and short chain present
- High degree of long chain branching (LCB)
- Branch spacing is irregular
- Some short chain branching



■ m-PE:

- narrow molecular weight distribution
- Chain branching could be anything – but usually short chain branching from co-monomer butane, hexane, octane -LLDPE structure
- Branch spacing is very regular

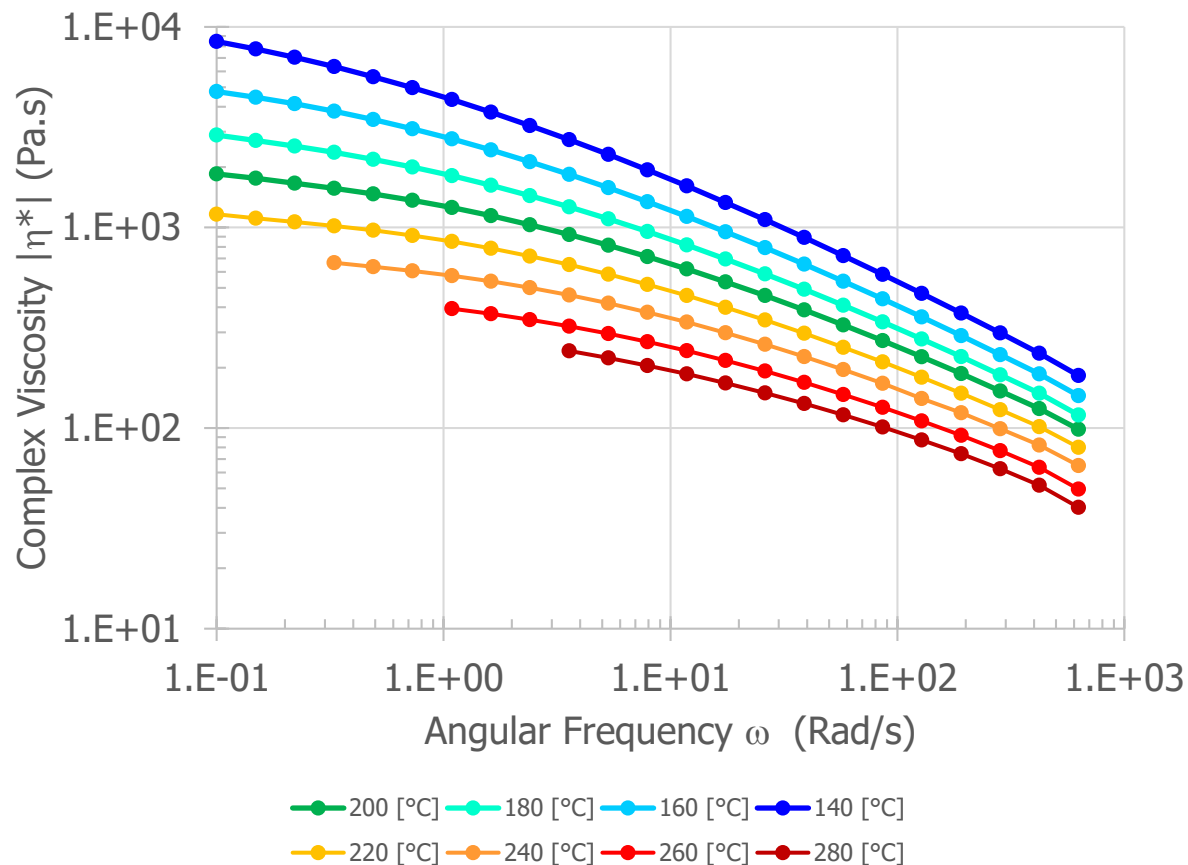




Results

■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm^3 , MFI = 7 g/10 min



Complex viscosity at several different temperatures: excellent data

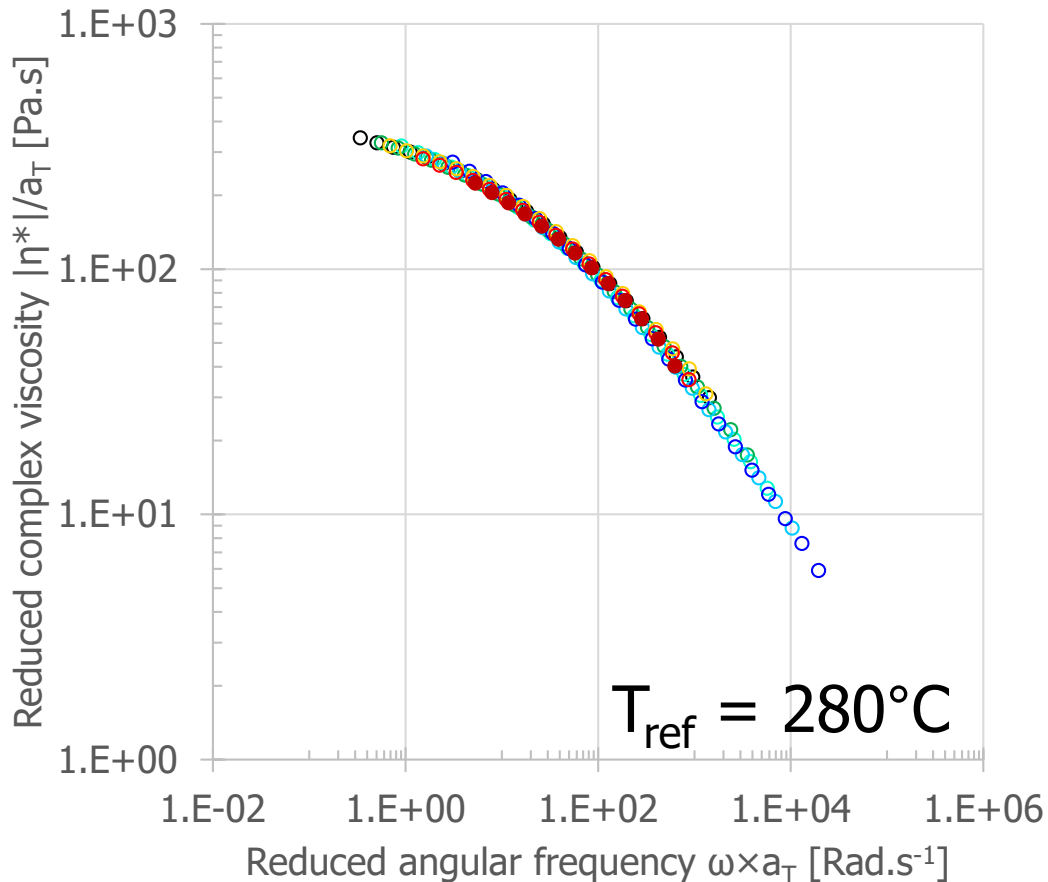
Difficult measurements at temperatures $> 240^\circ\text{C}$ at low frequencies due to degradation (despite N_2 atmosphere) resulting in increase of viscosity at low frequency



Results

■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm³ , MFI = 7 g/10 min



Viscosity master curve at 280°C

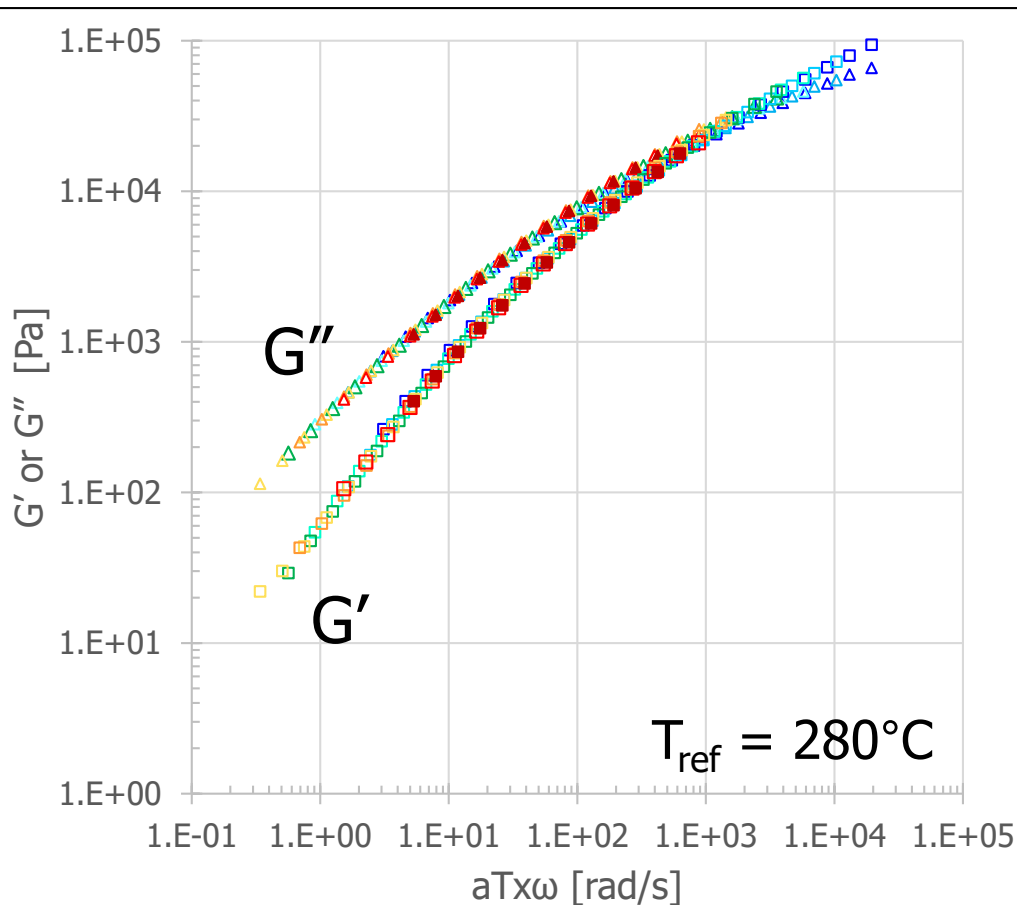
- time-temperature superposition (TTS): excellent superposition quality
- Zero-shear viscosity is not fully determined (Newtonian Plateau not reached)
 - ⇒ LCB
 - ⇒ Broad molecular weight distribution
- Strong shear thinning
 - Large entanglement density



Results

■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm^3 , MFI = 7 g/10 min



G' and G'' master curves at 280°C , after applying time-temperature superposition: excellent superposition quality

The melt is truly a viscoelastic material

$G'' > G'$ on majority of the frequency range: at this temperature the melt is viscous dominant

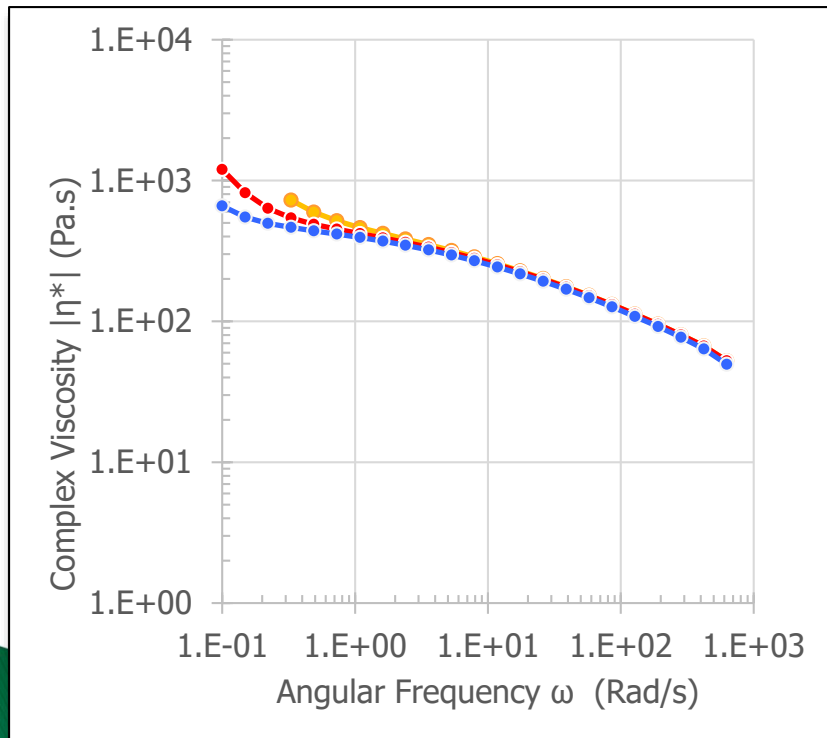
Cross over point at about 1,000 rad/s

Results

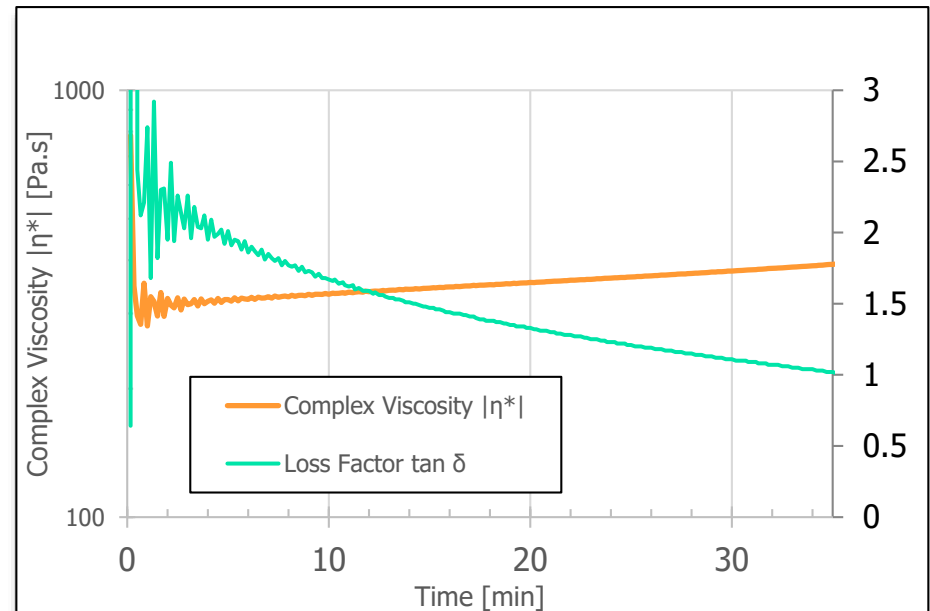
■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm^3 , MFI = 7 g/10 min
- Thermal stability under N_2 atmosphere

Measurement repeats at 260°C



Time sweep at 1 rad/s and 280°C



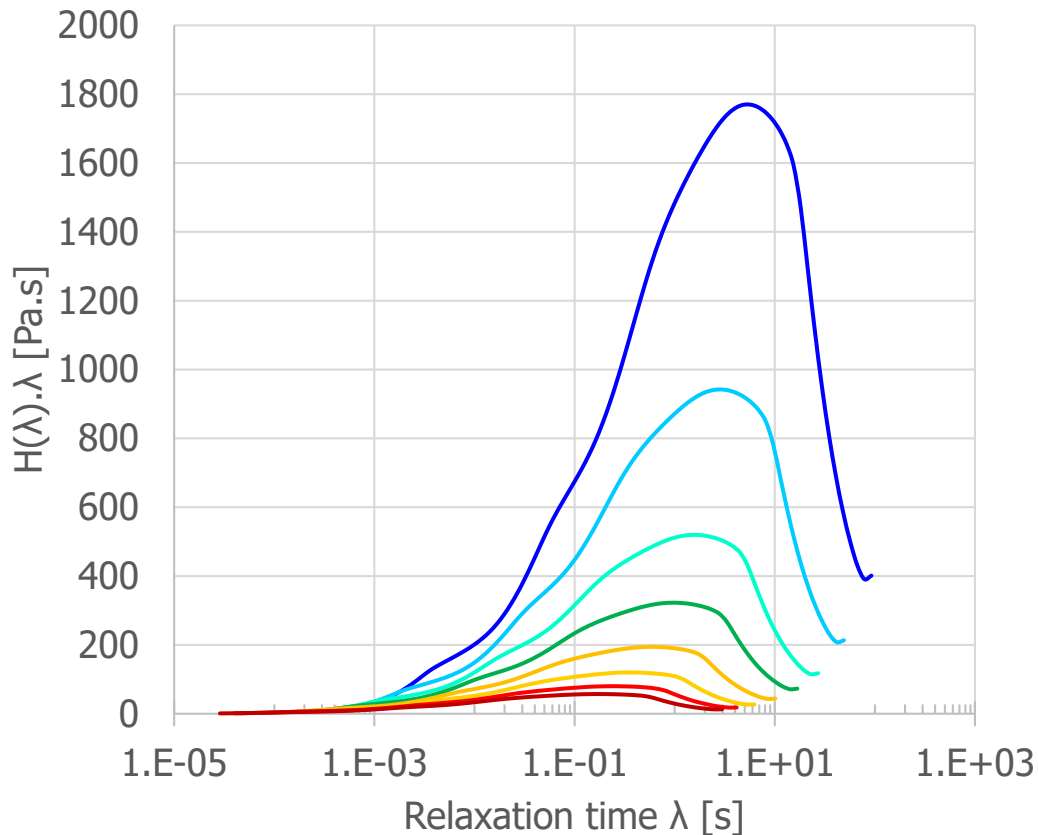
Over time: increase of complex viscosity and melt elasticity near processing temperature



Results

■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm^3 , MFI = 7 g/10 min



Relaxation time distribution:

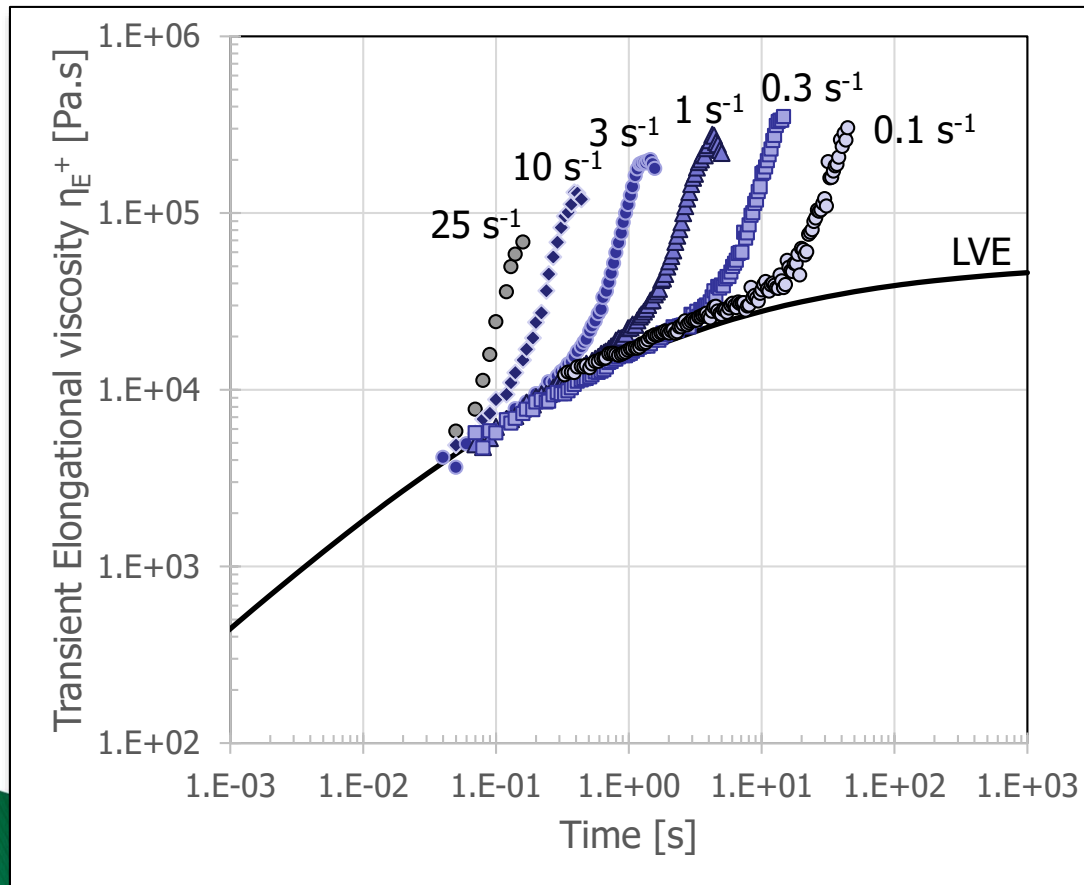
- melt rheology equivalent of the molecular weight distribution.
- Calculated from the G' and G'' master curves with the so-called Regularization method
- very broad distribution with asymmetrical shape biased towards longer relaxation times.
- The calculation does not directly show the high molecular weight shoulder seen with GPC



Results

■ Reference: **LD1**

- Autoclave LDPE - density = 0.917 g/cm^3 , MFI = 7 g/10 min



Transient elongational viscosity measurements at 140°C with the SER-3

- $\text{LVE} = 3 \times \eta^*$ (Carreau-Yasuda model)
- Strong strain hardening (deviation from LVE) characteristic of high density of long chain branching LCB



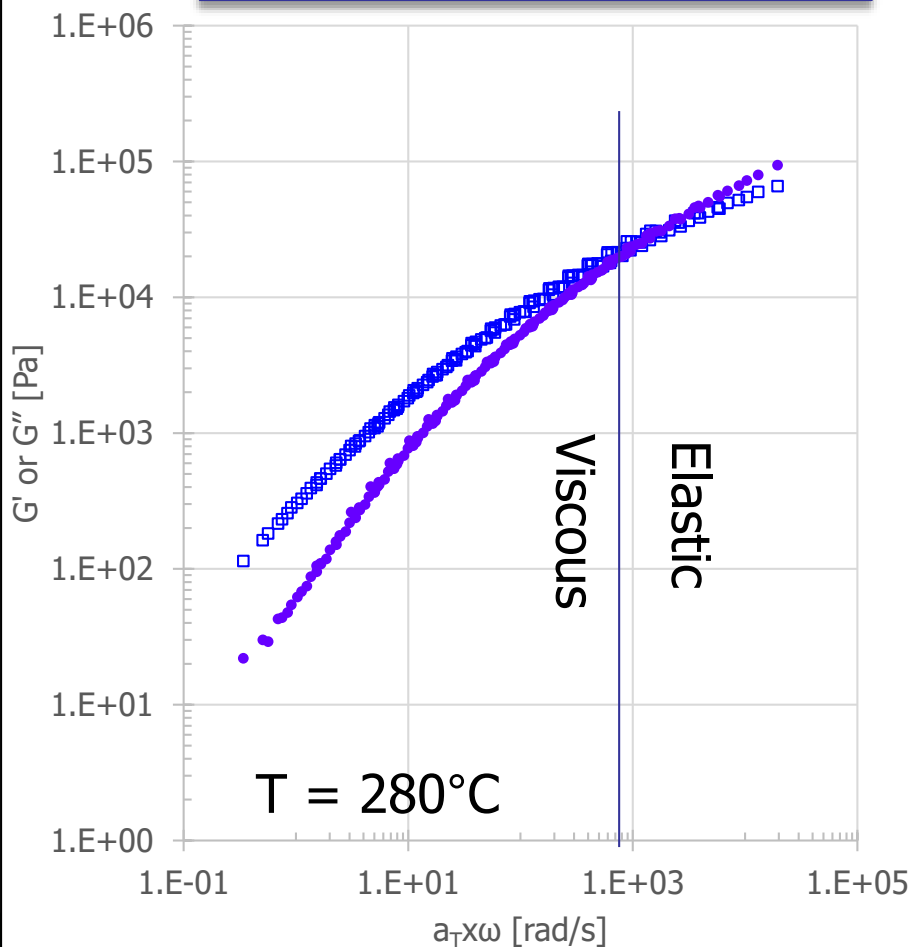
Comparisons

- Comparison of G'/G''
- Comparison of complex viscosity master curves
- Comparison of relaxation time distributions
- Comparison of transient extensional viscosity

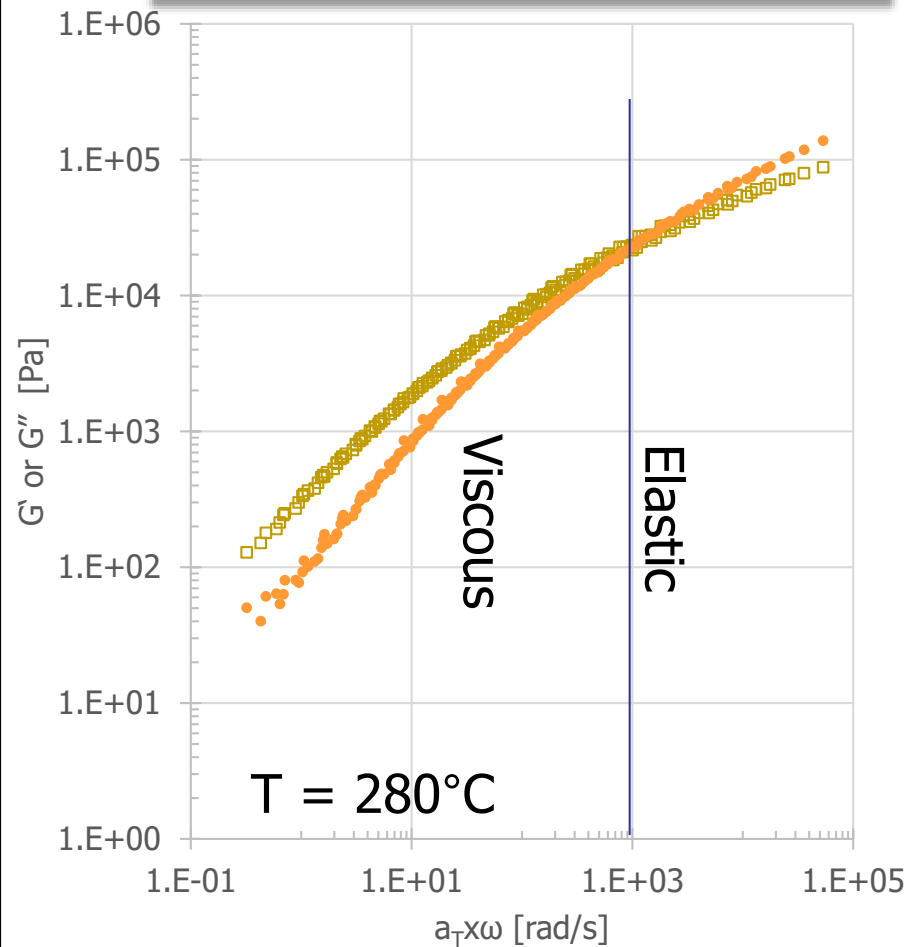


Comparison – G' and G''

LD1– 7MI .917 LDPE



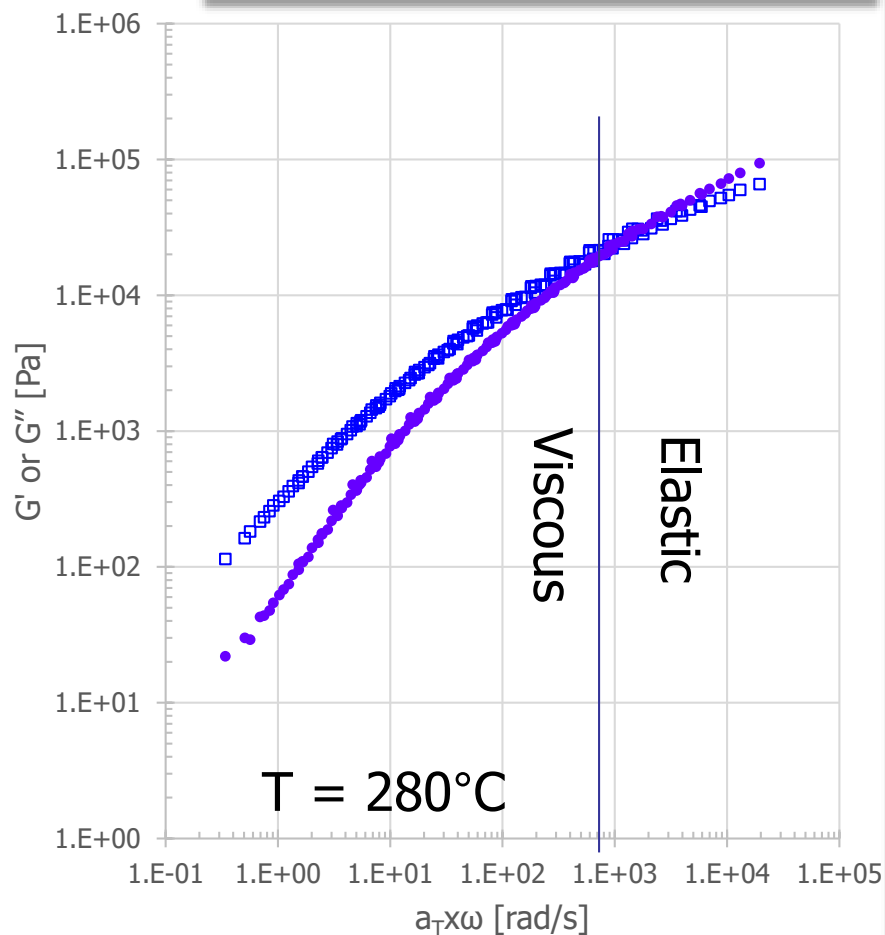
LD2– 7MI .917 LDPE



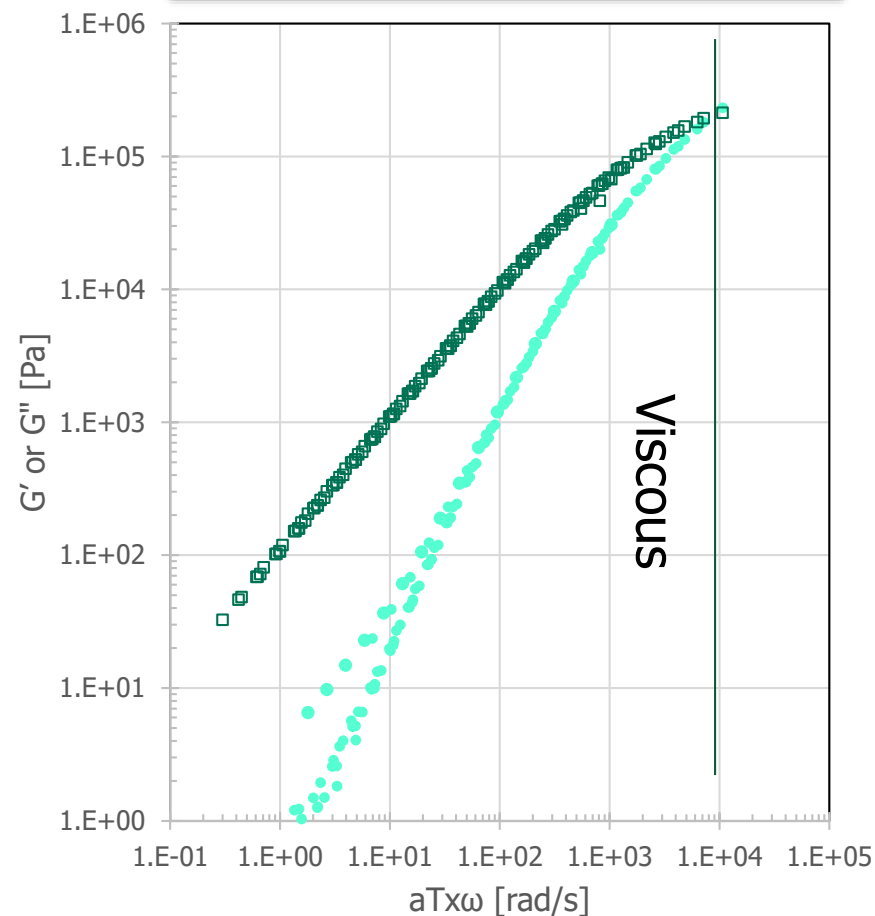


Comparison – G' and G''

LD1– 7MI .917 LDPE



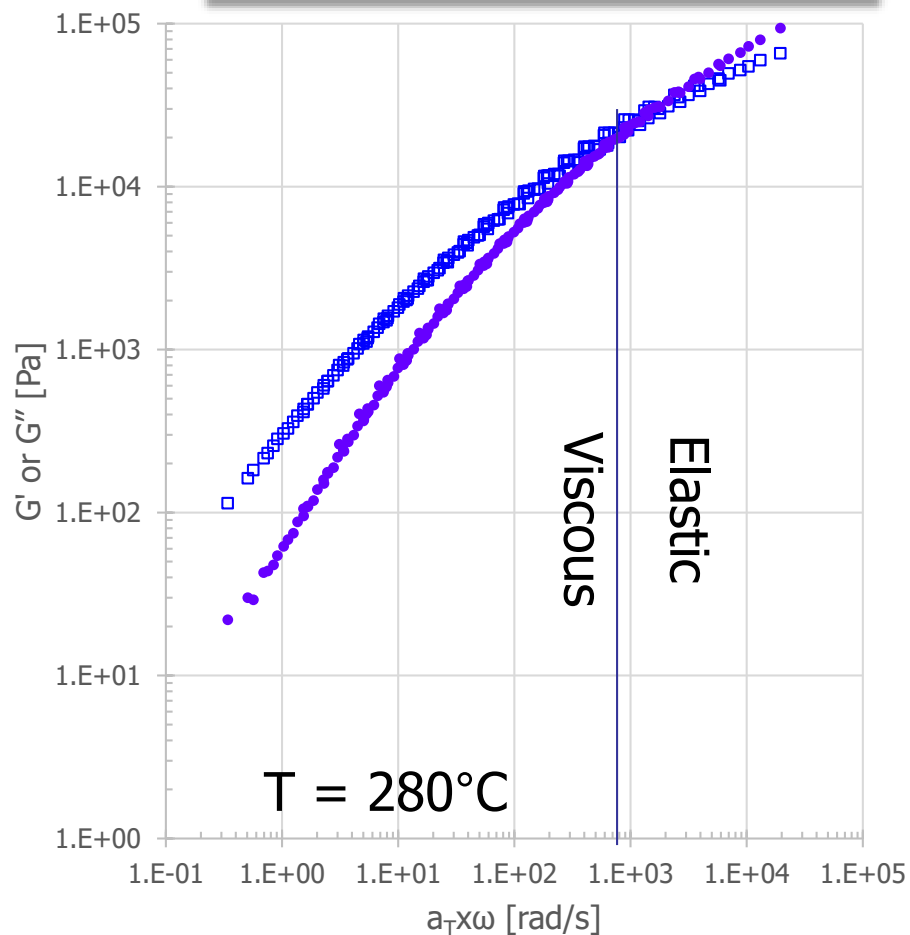
m-PE – 19MI .918 m-PE



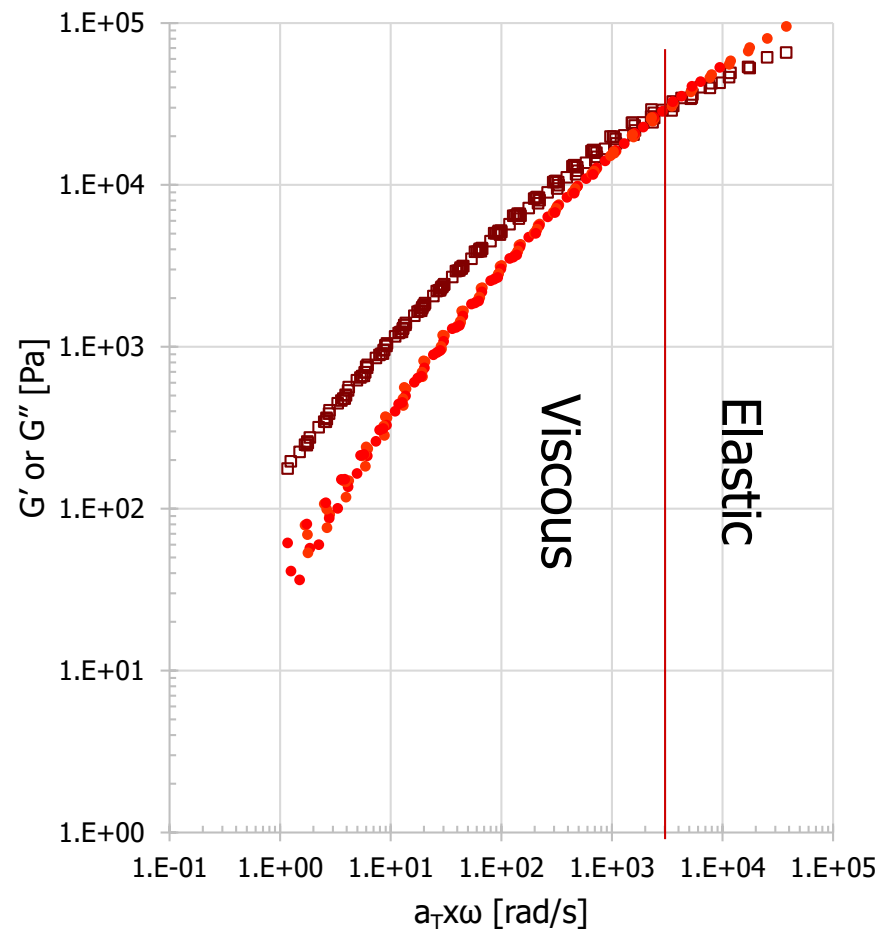


Comparison – G' and G''

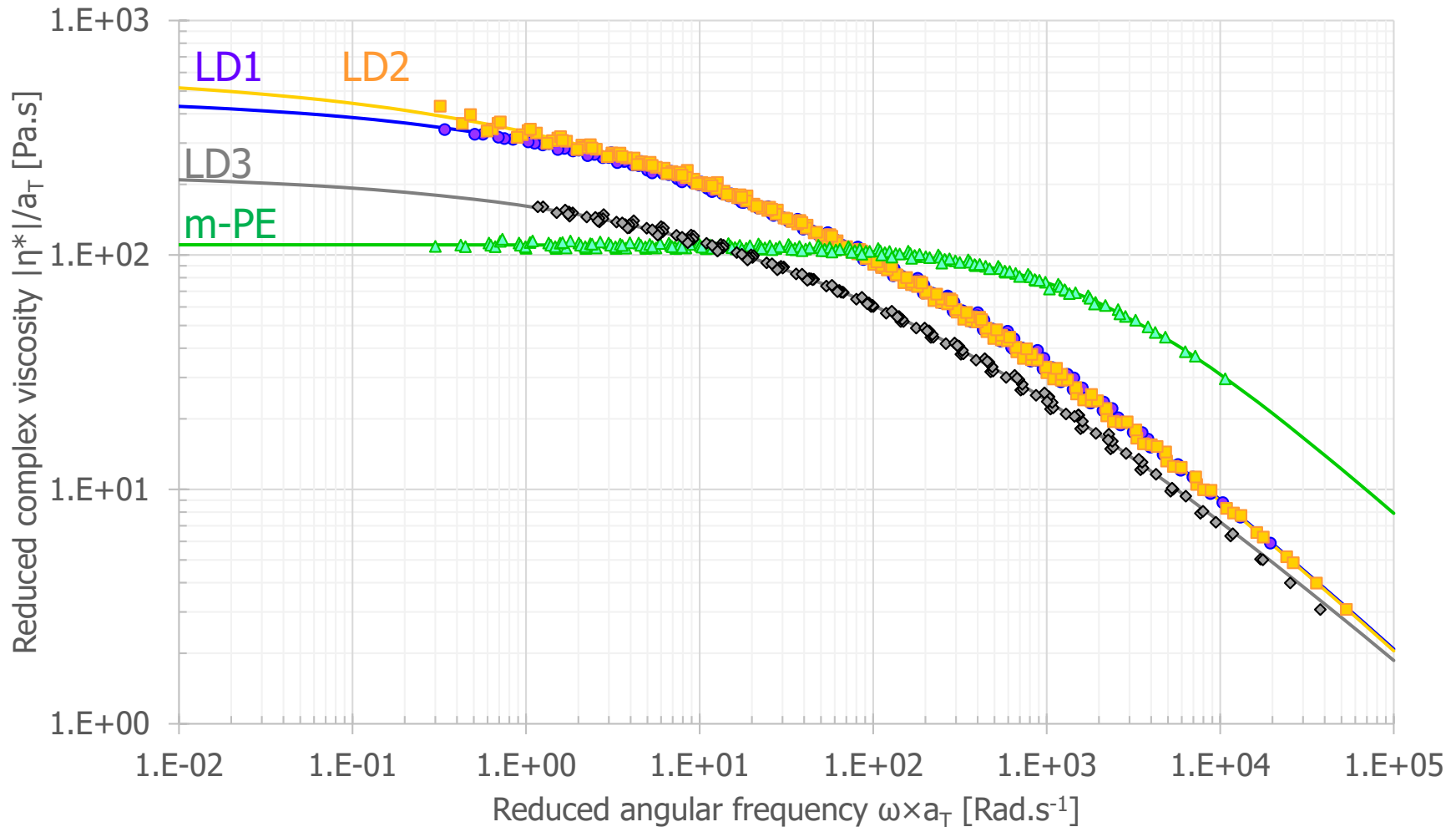
LD1– 7MI .917 LDPE



LD3– 16 MI .917



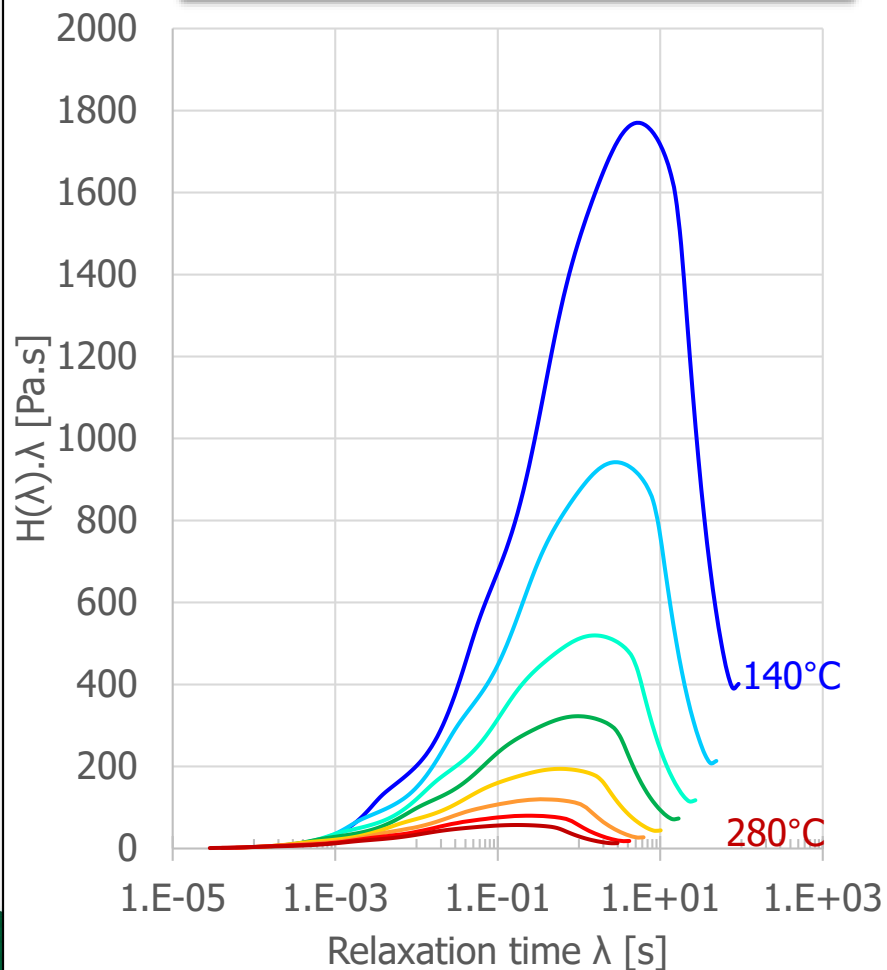
Comparison – Complex viscosity



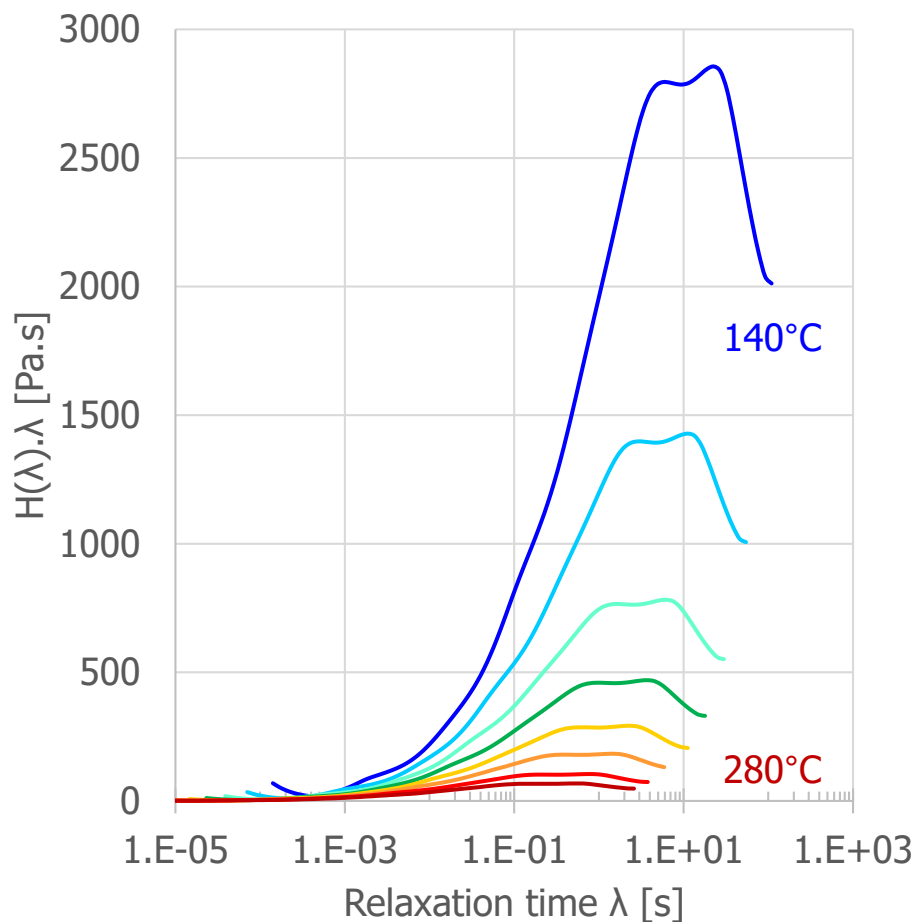


Comparison relaxation time

LD1- 7MI .917 LDPE

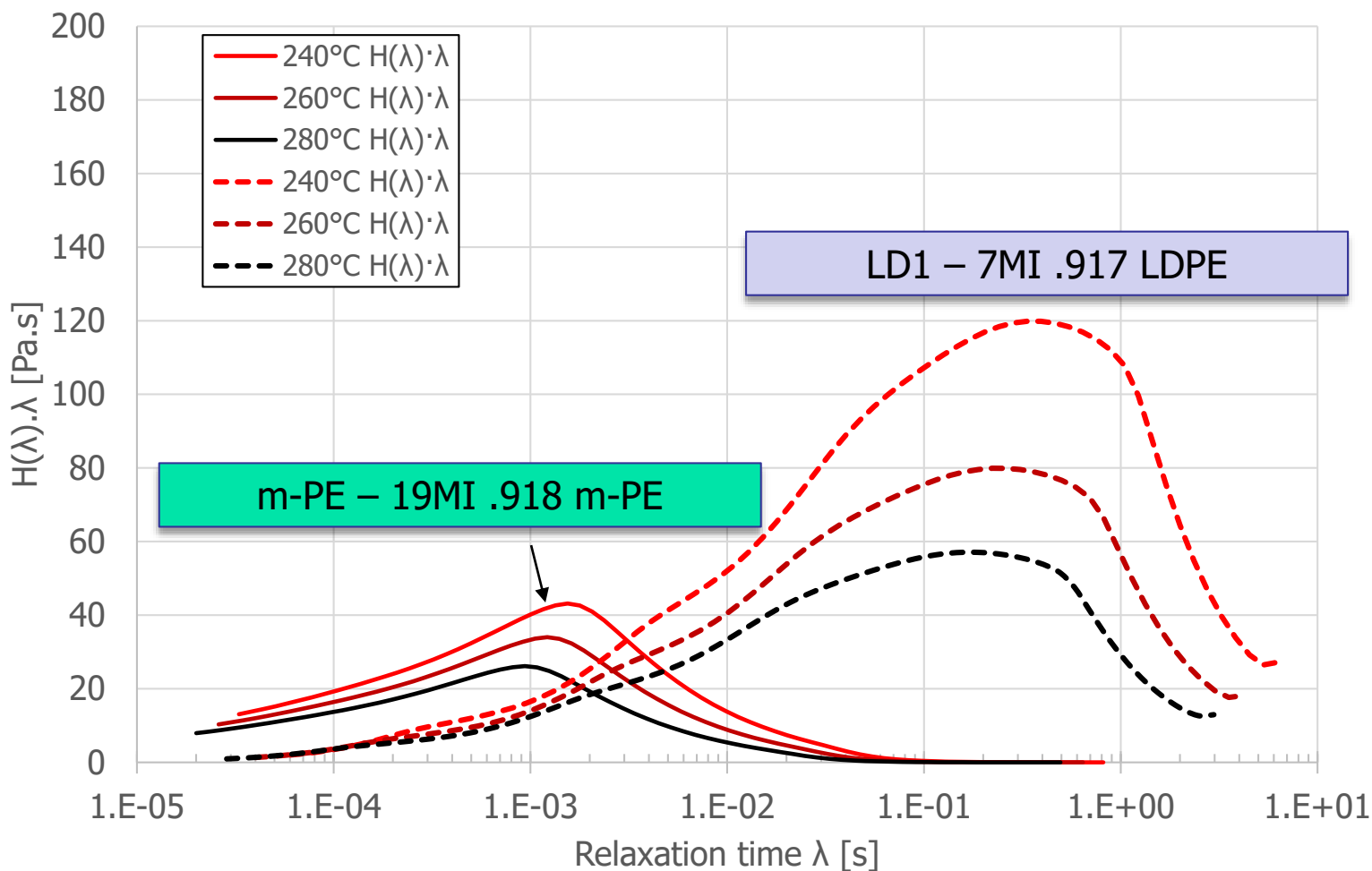


LD2- 7MI .917 LDPE



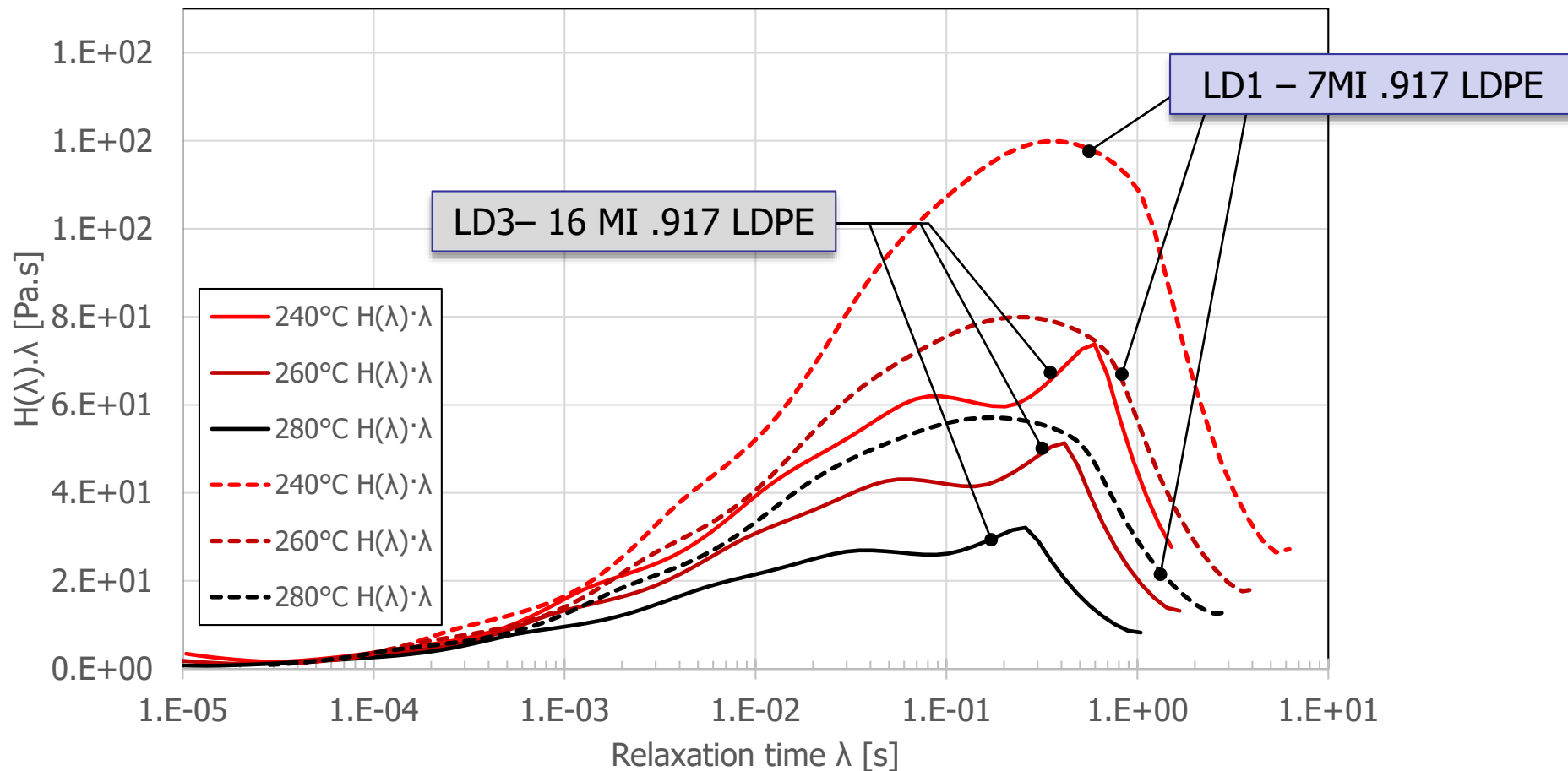


Comparison relaxation time





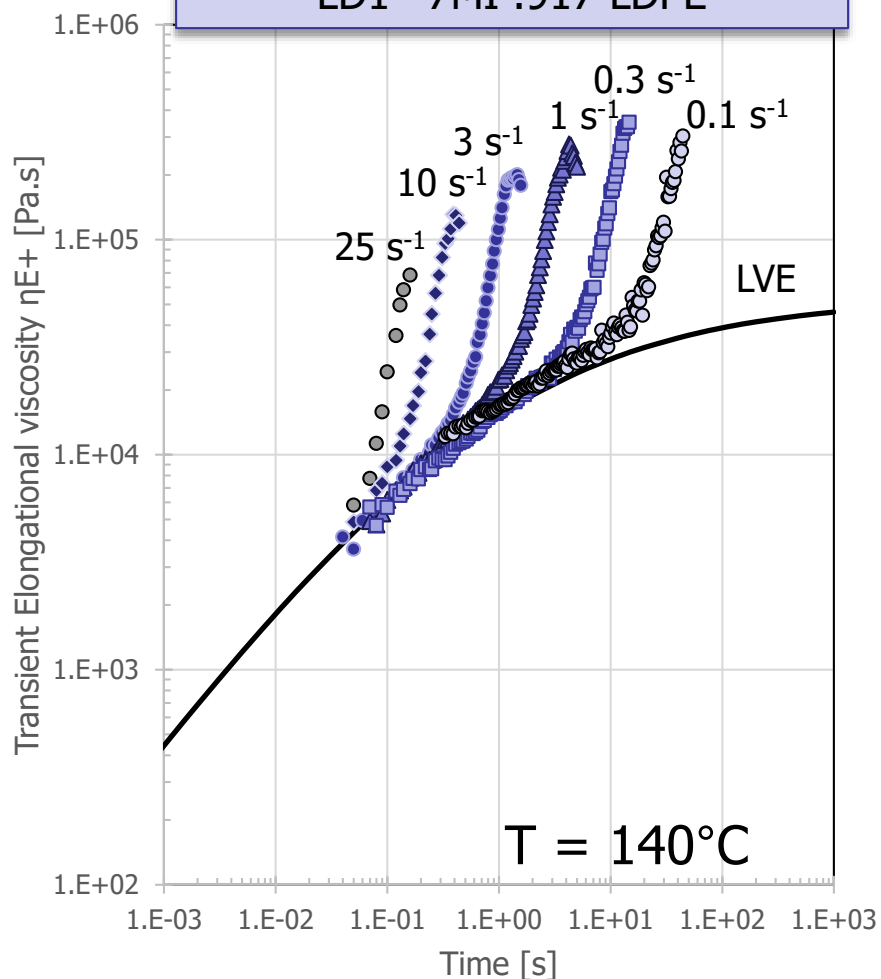
Comparison relaxation time



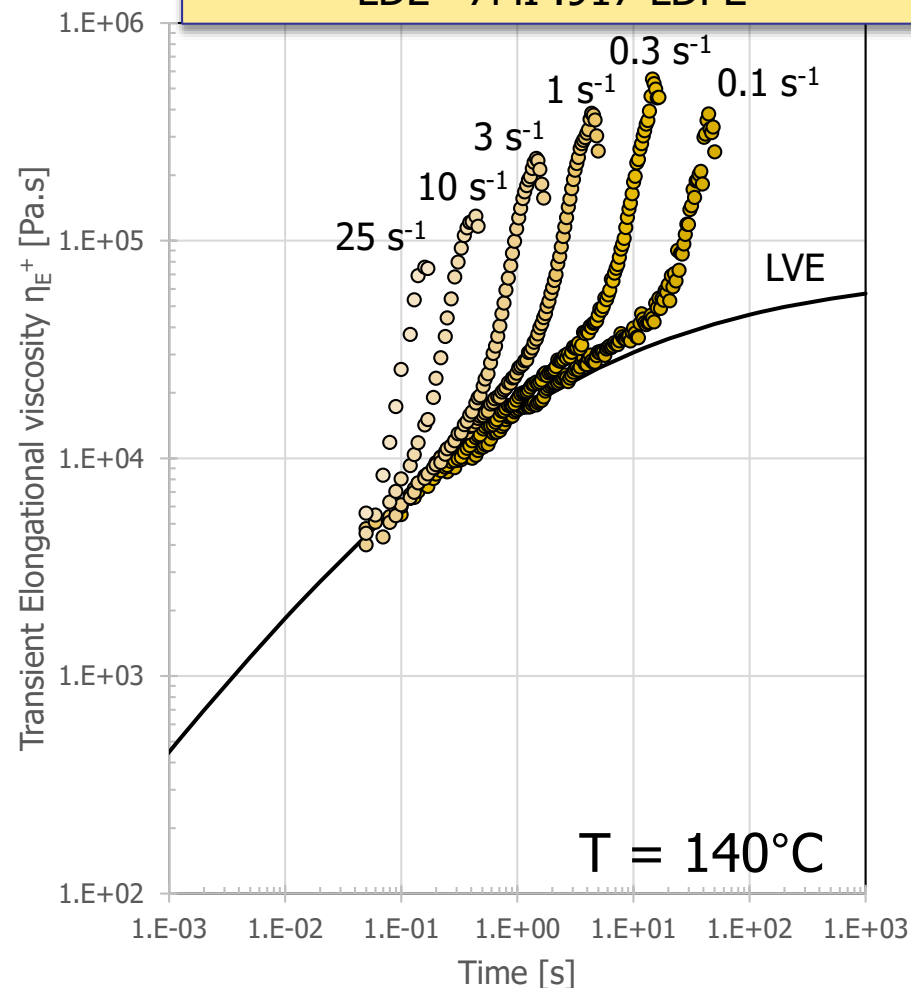


Comparison – Elongational Viscosity

LD1– 7MI .917 LDPE

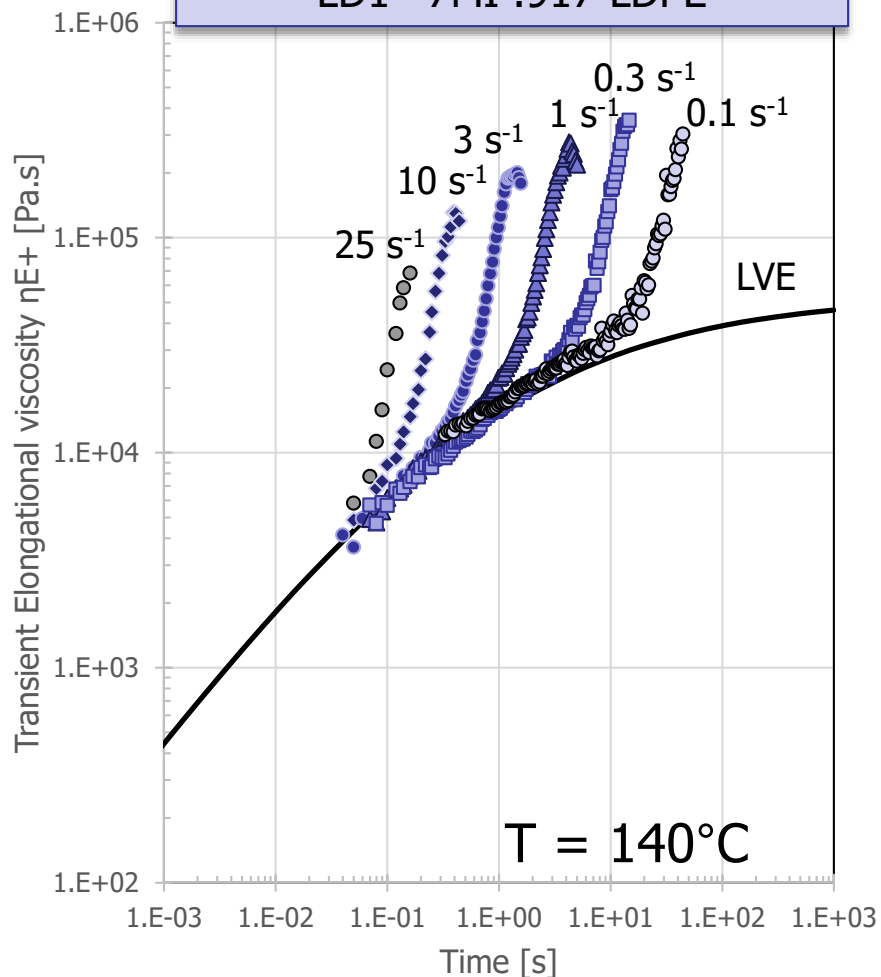


LD2– 7MI .917 LDPE

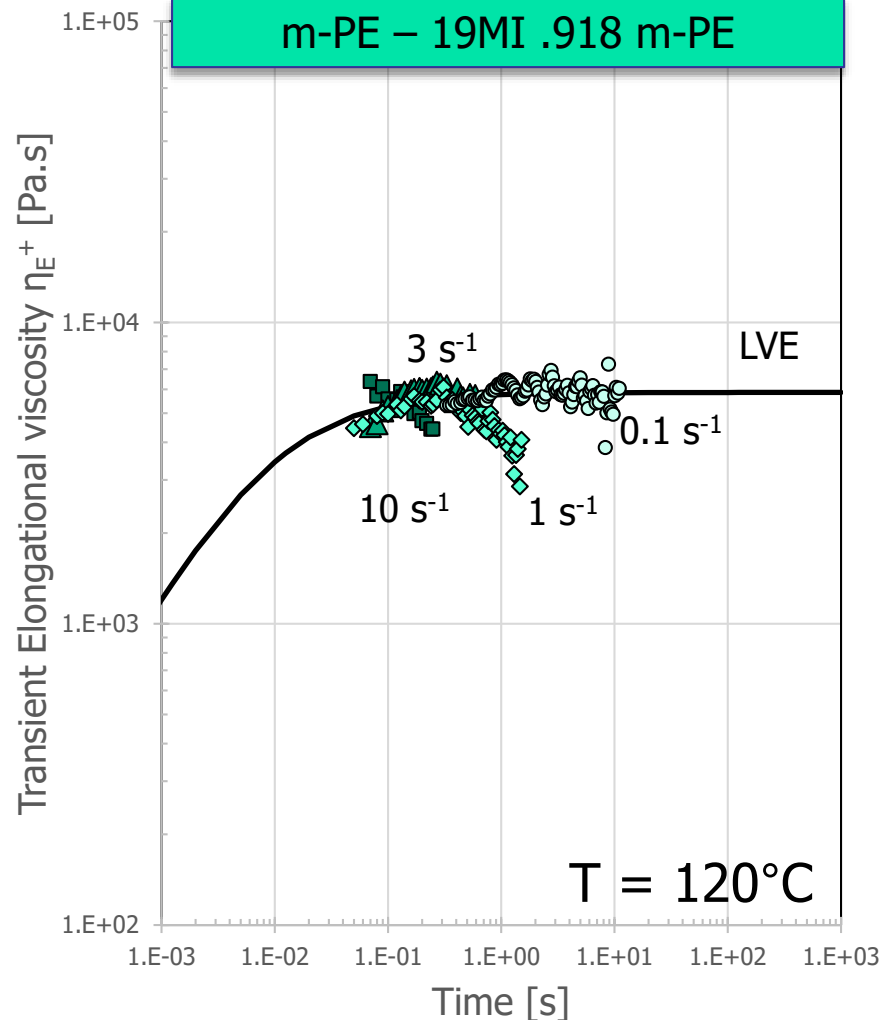


Comparison – Elongational Viscosity

LD1– 7MI .917 LDPE



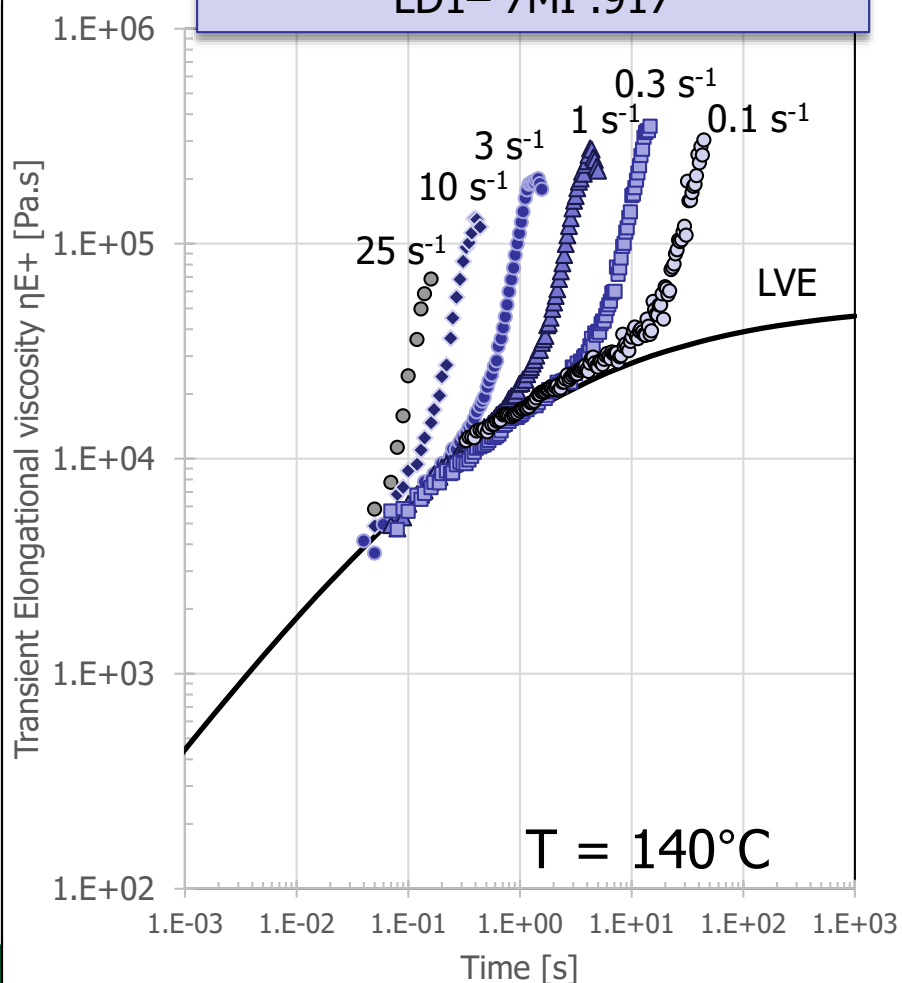
m-PE – 19MI .918 m-PE



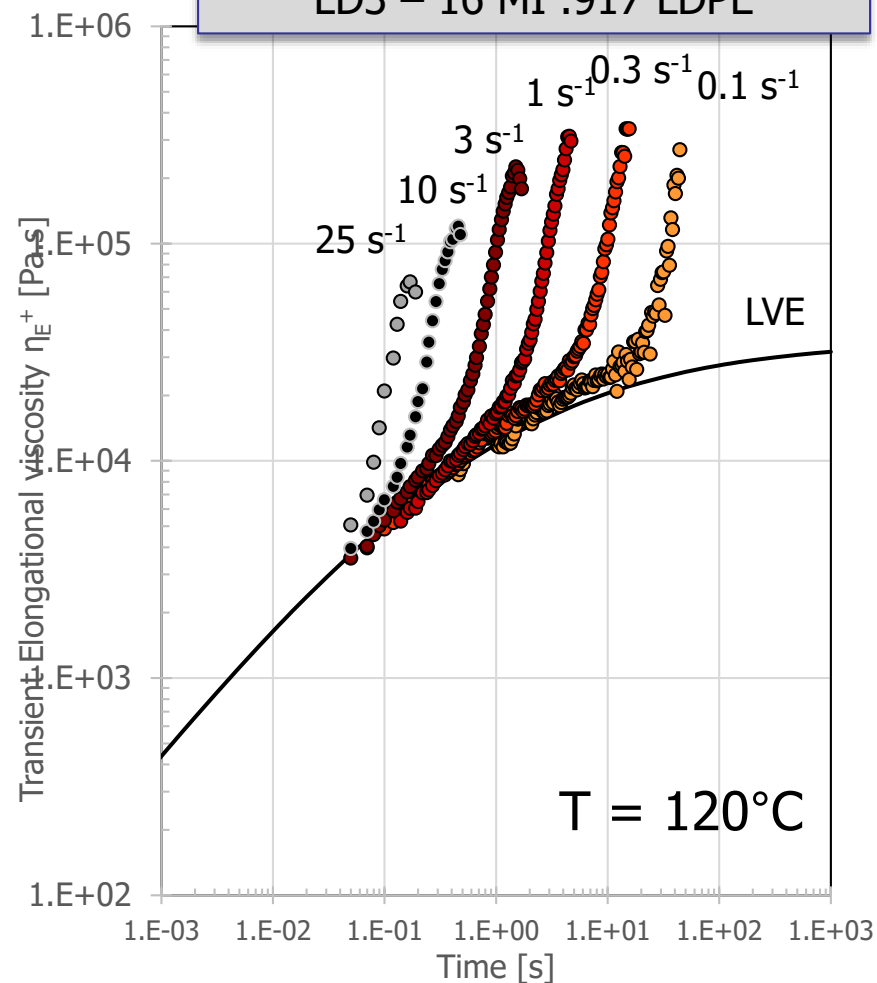


Comparison – Elongational Viscosity

LD1– 7MI .917



LD3 – 16 MI .917 LDPE





Key Rheological parameters

Material	Zero shear viscosity η_0 at 280°C† [Pa.s]	Pseudoplastic (shear thinning) index† [-]	Storage modulus G' at $G'' = 500$ Pa at 180°C‡ [Pa]	Peak relaxation time at 280°C [s]	Width half maximum of relaxation time [decades]
LD1	471.92	0.3389	129.4	0.159	≈ 2.19
LD2	602.06	0.2735	150.8	0.544	≈ 2.65
LD3	223.34	0.2948	130.3	0.259	≈ 2.14
m-PE	110.50	0.3404	4.8	$9.37 \cdot 10^{-4}$	≈ 1.55
Physical meaning	Molecular weight	De-entanglement rate to recoil rate	Melt elasticity	Melt elasticity	Polydispersity

† Carreau-Yasuda curve fit

‡P.A. Clevenhag, C. Oveby – TAPPI PLACE 2004



Key Rheological parameters

Material	Ultimate Trouton Ratio at 25 s ⁻¹	Ultimate Trouton Ratio at 1 s ⁻¹
LD1	27.2	36.1
LD2	29.4	45.9
LD3	31.3	53.2
m-PE	1.3 for $\dot{\epsilon} = 10 \text{ s}^{-1}$	1.8
Physical meaning	Melt strength at high stretch rate	Melt strength at medium stretch rate



Conclusions

- Melt rheology is a powerful tool for the investigation of the molecular structure and the polydispersity of a given polymer
- Looking at shear rheology only is too limited when comparing the behavior of different polymer families related to extrusion coating process
- Elongational viscosity provides valuable information regarding melt strength
- Future work will be carried on:
 - With more polymers to be investigated within the LDPE (Autoclave and Tubular), m-PE, PP, EVA, PLA, biopolymers, PET etc...
 - Processing evaluation work will be carried out (measurement of edge bead profile, neck-in, determination of stable process window etc)
 - A correlation between processing characteristics and shear and elongational viscosity will be evaluated
 - Possibly, a process model will be built using a viscoelastic constitutive equation which takes into account the elongational and shear viscosity data



Thank you

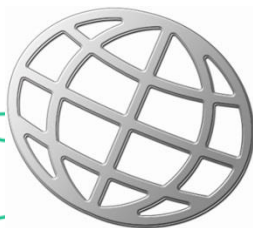
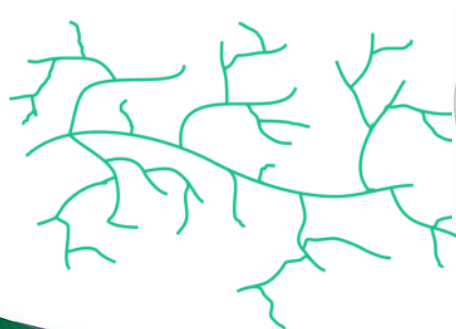
PRESENTED BY

Olivier Catherine

Title

Cloeren Incorporated

ocatherine@cloeren.com



CLOEREN
INCORPORATED

