Lecture 9 - Lime-soda ash softening, Part 2

For waters with non-carbonate hardness, single-stage softening is insufficient. Leftover hardness is removed by addition of soda ash (Na2CO3)

8. $Ca^{2+} + SO_4^{2-} + Na_2CO_3 \rightarrow CaCO_3 + 2Na^+ + SO_4^{2-}$

9. $Ca^{2+} + 2CI^{-} + Na_2CO_3 \rightarrow CaCO_3V + 2Na^{+} + 2CI^{-}$

Practical limits of lime-soda ash softening are dictated by solubility of precipitates: CaCOz & Mg(OH)2

Ca: 30 mg/L as CaCOz

Mg: 10 mg/L as CaCOz

Total hardness: 40 mg/L as CaCOz

In practice, residual hardness = 50 to 80 mg/L

This water has high pH and needs to be recarbonated

"two-stage softening" also called "excess-lime treatment" and "split recarbonation treatment"

See Lecture 8, page 10

Split treatment is similar, except only part of water is treated with lime. Other part by-passes lime treatment and gets soda-ash treatment along with lime-treated water

The CO2 in untreated water neutralizes high pH in lime-treated water and recarb is not needed

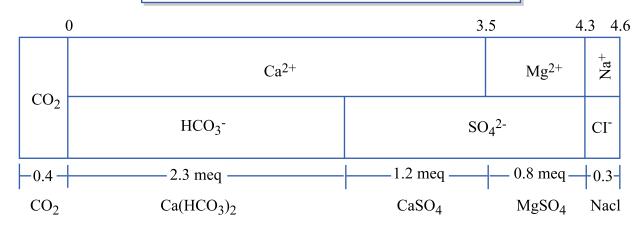
Water split is computed such that enough Mg is removed in lime-treated water to meet target Mg level in combined finished water

Computing chemical doses for lime soda ash softening - Example 11.4 from Viessman and Hammer, pg. 445 - pg 3 and 4 CO2 = 8.8 mg/L as CO2 AIK = 115 mg/L as CaCOz Ca++ = 70 mg/L 502- = 96 mg/L Mg++ = 9.7 mg/L Nat = 6,9 mg/L C1 = 10.6 mg/L Easiest method is to construct a table that converts all concentrations to equivalent concentrations, and then to equivalents of CaCOz Also use chart from VH Fig. 11.8, pg 446 mg/L MW equiv eq wt (gm/mole) (eq/molescule) (gm/mole-eq) as CaCOz (mg/L) 44.0 22.0 0.4 20.0 Ca2+ 20.0 3.5 175. 70 40.0 2 24.4 12.2 0.80 39.8 6,9 23.0 23.0 6.30 15.0 100 50.0 115.0 AIK 115 48.0 50,2 96 2.0 96.0 100,0 35.5 35.5 0.30 14.9 4.6 175 + 39.8 = 214.8 mg/L Total hardness as CaCO3 carbonate hardness = [AIK] = 115 mg/L as CaCO3

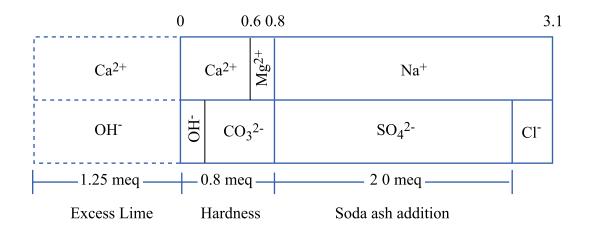
Mg noncarbonate hardness = 39.8 mg/l as CaCO3

Noncarbonate hardness = TH - CH = 99.8 mg/L as CaCO3

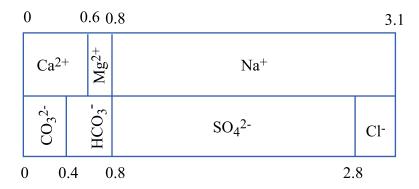
Milliequivalent Bar Graph for Example 11.4



(A) Bar graph & hypothetical chemical combinations in the raw water

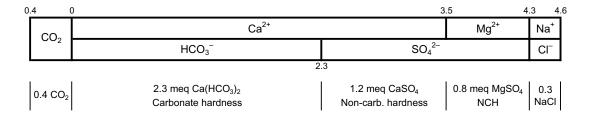


(B) Bar graph of the water after lime & soda ash additions & settling but before recarbonation.



(C) Bar Graph of the water after two-stage recarbonation & final filtration

Before treatment:



After treatment with lime $Ca(OH)_2$ and intermediate reaction to remove carbonate hardness:

(chemical equations 1, 2, & 3)

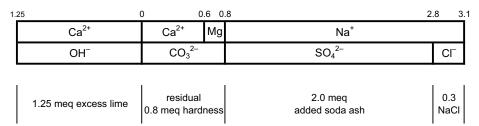
1.25		0 1.	2 2	2.0 2.3	
	Ca ²⁺	Ca ²⁺	Mg ²⁺	Na⁺	
	OH ⁻	SO ₄ ²⁻		Cl ⁻	
1.25 meq excess lime		2.0 meq NC	Н	0.3 NaCl	

After treatment with lime and intermediate reaction to remove noncarbonate Mg hardness: (chemical equations 4 & 5)

1.2	5	0 1.8	2.	.0 2
	Ca ²⁺	Ca ²⁺	Лg	Na⁺
	OH ⁻	SO ₄ ²⁻		CI ⁻
	1.25 meq excess lime	2.0 meq NCH		0.3 NaCl

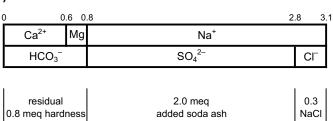
After treatment with soda ash Na₂CO₃:

(chemical equations 8 & 9)



After recarbonation:

(chemical equations 6 & 7)

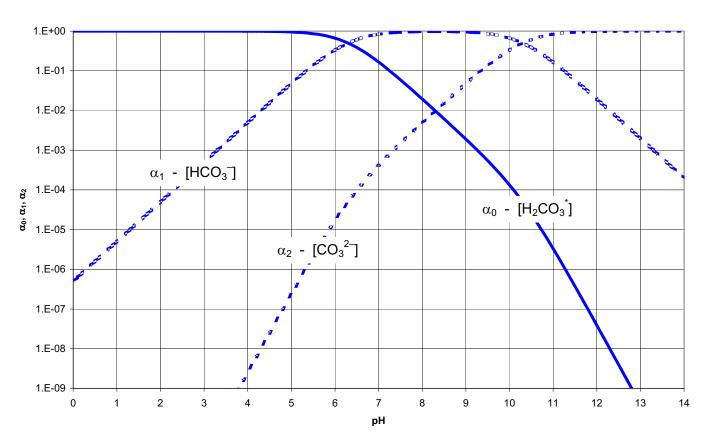


Lime required - 20.0 mg/L as CaCO2 For CO₂ For carbonate hardness - 115.0 For Mg non carbonate hardness -174.8 mall as Cacoz (3.5 meg) convert from Cacoz to Cao CaCO3 174.8 mg/L as CaCOz = 97.9 mg/L as CaO Include excess lime of 35 mg/L Regid lime = 133 mg/L Soda Ash for noncarbonate hardness (2.0 meg) NCH = 99.8 mg/L as CaCO3 (recall that Mg NCH was treated with lime but simply swaps ca for Mg, so still nceds treatment with goda ash) Regd Soda Ash - 99.8 mg/l as CaCOz Convert to Na2CO3: Na₂CO₃ = 2×25+12+2×16 Ca CO₃ = 40+12+3×16 2×23+12+3×16

Note that pg 14 shows HCO3 but will actually be an equilibrium between CO_2 , HCO3, CO_3^2 depending on pH per pg 6

Regd soda ash = 1.06 × 99.8 = 106 mg/L

Carbonate system equilibrium



Summary of chemical dosage calculations required for lime & lime-soda ash softening* REQUIRED CHEMICAL DOSAGE CALCULATIONS **PROCESS** Lime addition for softening: Single-Stage Lime: CaO = {carbonic acid concentration} + { calcium carbonate hardness} For waters with high calcium, low magnesium, Soda ash addition for softening: & carbonate hardness $Na_2CO_3 = none$ Carbon dioxide for pH adjustment after softening: source water estimated carbonate source water calcium alkalinity of softened alkalinity estimated residual calcium hardness of softened water Lime addition for softening: **Excess Lime:** For waters with high $\left\{\begin{array}{l} \text{magnesium} \\ \text{hardness} \end{array}\right\} + \left\{\begin{array}{l} \text{excess lime} \\ \text{dose} \end{array}\right\}$ $CaO = \begin{cases} carbonic acid \\ concentration \end{cases}$ + {total alkalinity } + calcium, high magnesium, and carbonate hardness; process may be one or Soda ash addition for softening: two stages $Na_2CO_3 = none$ Carbon dioxide for pH adjustment after softening: estimated residual source water source water excess lime calcium hardness total hardness (of softened water estimated residual magnesium hardness of softened water Lime addition for softening: Single-Stage Lime Soda CaO = {carbonic acid concentration} + { calcium carbonate hardness} Ash: For water with high Soda ash addition for softening: calcium, low magnesium, Na₂CO₃ = {calcium noncarbonate hardness} and /or {magnesium noncarbonate hardness} & carbonate and Carbon dioxide for pH adjustment after softening: noncarbonte hardness (source water) estimated residual soda ash source water calcium calcium hardness alkalinity dose hardness of softened water Lime addition for softening: Excess Lime - Soda (magnesium Ash: carbonic acid calcium carbonate For waters with high carbonate concentration concentration hardness calcium, high magnesium, and carbonate and excess lime noncarbonate hardness; requirement process may be one or two Soda ash addition for softening: stages calcium magnesium noncarbonate noncarbonate Carbon dioxide for pH adjustment after softening: (estimated residual (estimated hydroxide) alkalinity of softened magnesium hardness of softened water estimated hydroxide alkalinity of softened = CO2, second stage = alkalinity estimated residual hardness of softened * All quantities are expressed as mg/L as CaCO3

Figure by MIT OCW.