

# Parallel Flow Heat Exchanger

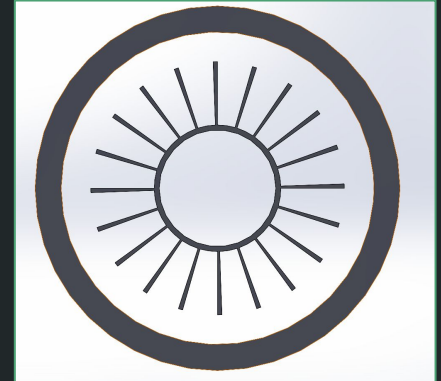
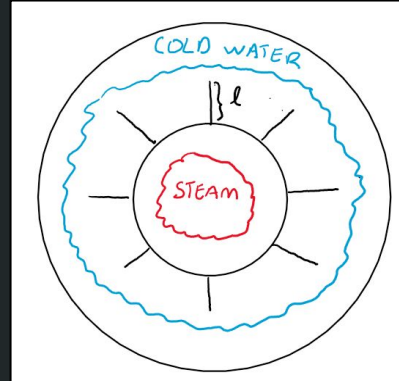
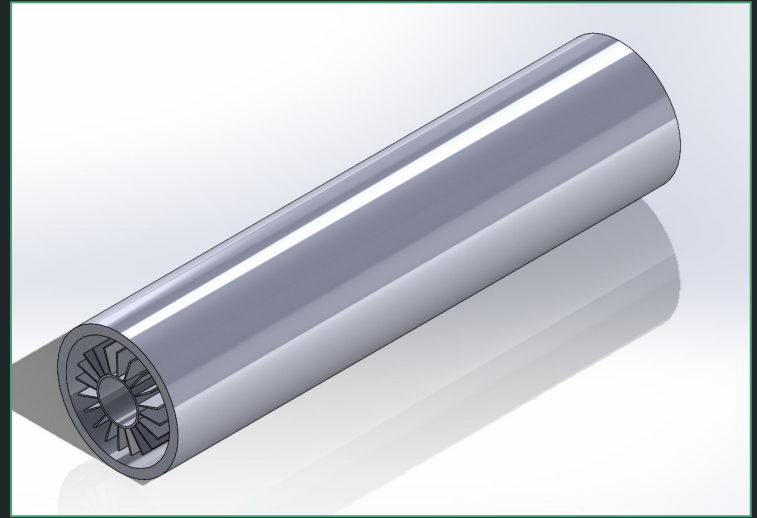
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Faraz Iqbal, Ashrafur Rahman, Ted Yee

# Current system

Problem Definition: Model the heat transfer from steam to cold water in a concentric pipe heat exchanger

- Concentric pipes
  - Inner pipe w/ fins
  - Adiabatic outer pipe
- Two fluids
  - Hot steam
  - Cold water



# Modeled Elements - Full Revolution and Wedge

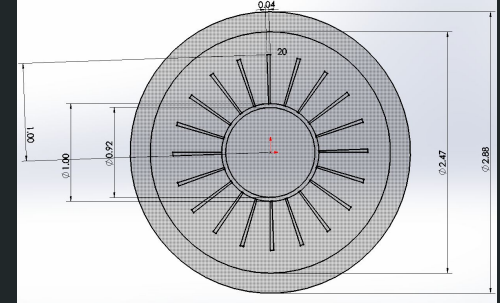
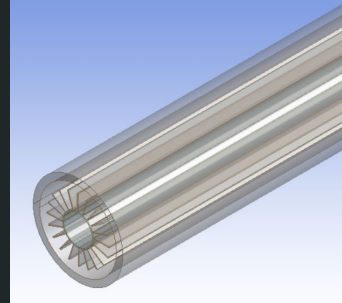
- Full Revolution

- Geometry:

- SolidWorks
    - 4 Bodies - Outer/Inner Pipe, Hot/Cold Fluid

- Variable:

- Flow Rate - cold water



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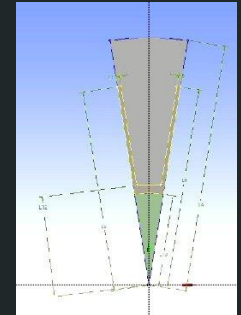
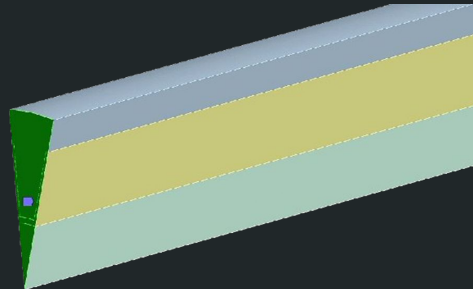
- Wedge - Space between fins

- Geometry:

- Ansys DesignModeler
    - 3 Bodies - Inner Pipe, Hot/Cold Fluid

- Variable:

- Geometry - angle of fin / number of fins

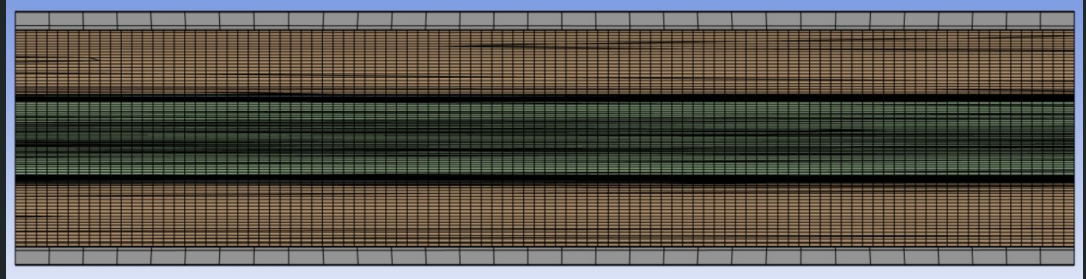


# Mesh Convergence Study - Full Revolution: Sweep

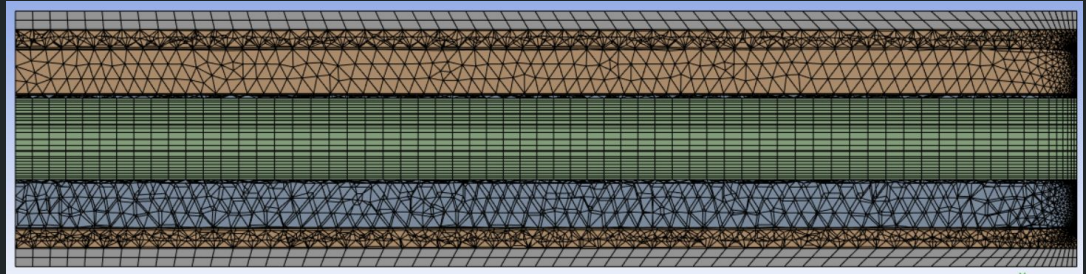
## Sweep Settings:

- Inner pipe, hot and cold fluid bodies
- 100 divisions of constant size across length of pipe

Mesh with Sweep:



Mesh without Sweep:

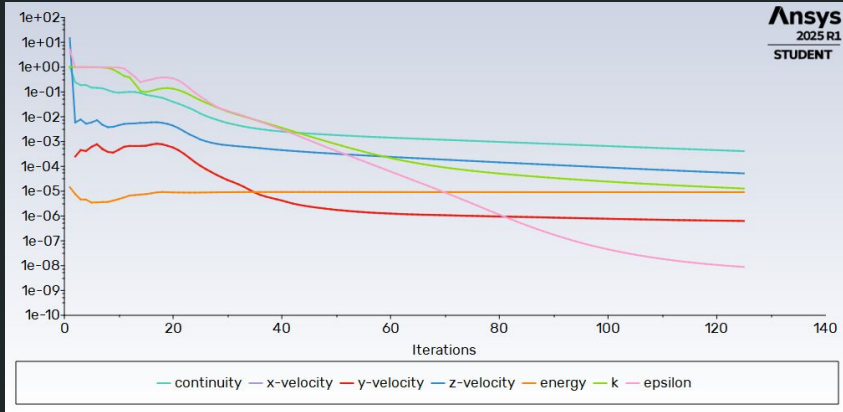


## Sweep Settings:

- N/A

# Mesh Convergence Study - Full Revolution: Residual Plot

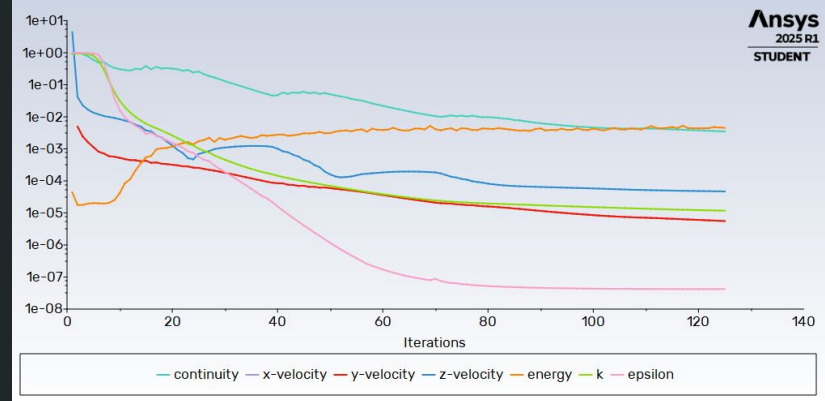
Mesh with Sweep:



## Results:

- Better continuity and turbulence
- Energy residual is smoother
- Energy residual decreasing at end of iteration
- Negative slopes throughout

Mesh without Sweep:

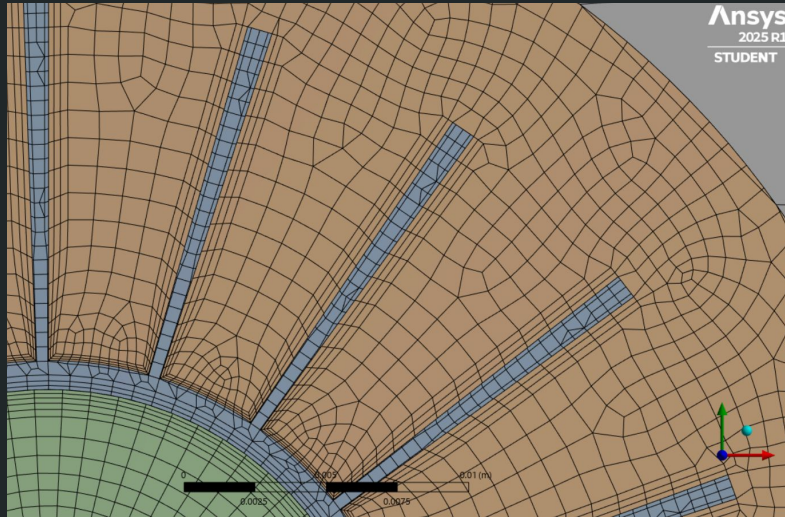


## Results:

- Energy residual rising over iterations
- Energy residual oscillations
- Early fluctuations in the z velocity residuals
- Still rising energy residual values at end of iteration

# Mesh Convergence Study - Full Revolution: Inflation

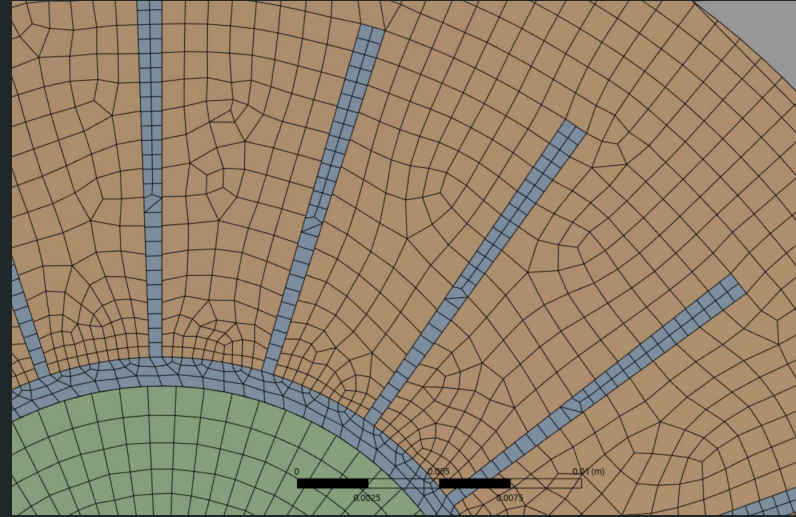
Mesh with Inflation:



Inflation Settings:

- 3 layers around fins and base of inner pipe
- 1 layer on inside of each fin
- 5 layers on steam face
- 3 layers on inner surface of inner pipe

Mesh without Inflation:



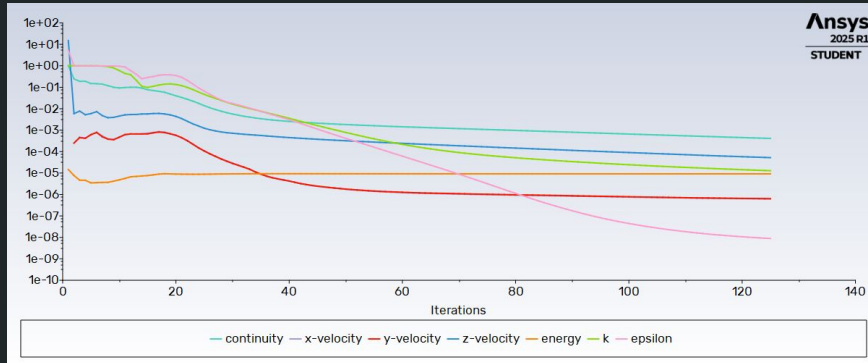
Inflation Settings:

- N/A



# Mesh Convergence Study - Full Revolution: Residual Plot

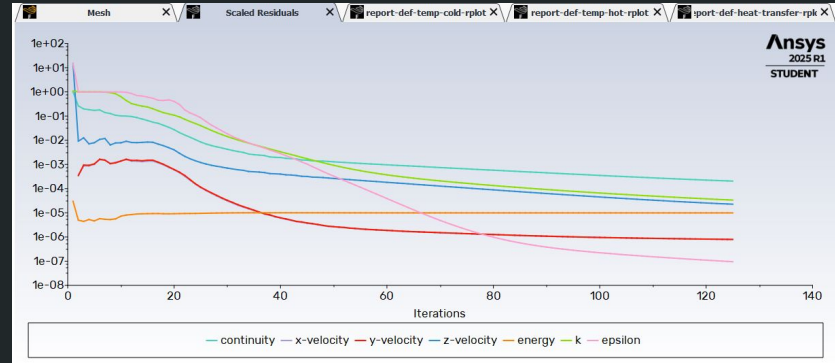
Mesh with Inflation:



Results:

- Better continuity and turbulence
- Energy residual is smooth

Mesh without Inflation:

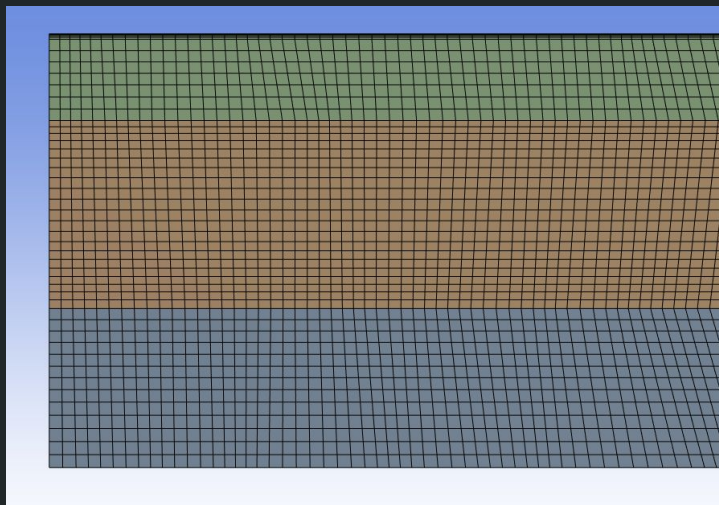


Results:

- Ends at higher residual magnitudes
- Energy residual curve is rough towards beginning

# Mesh Convergence Study - Wedge: Mesh (Body Sizing)

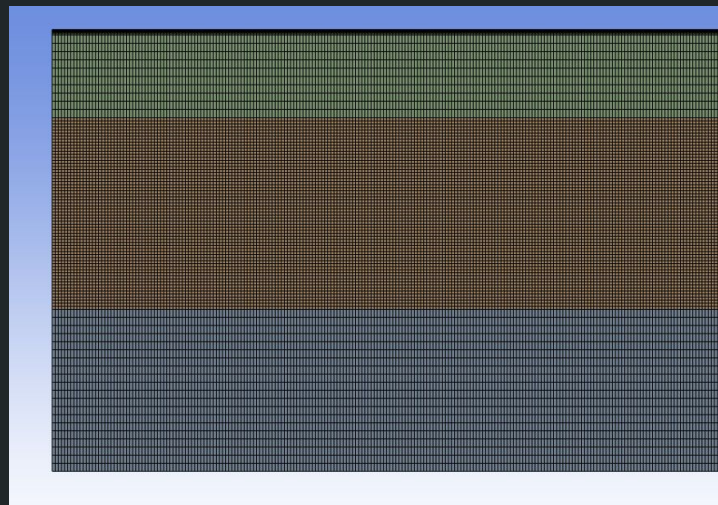
Standard Mesh (Default Growth):



Body Sizing Settings

- Element Size: **Default (1.5328e-2)**
- Growth Rate: **Default (1.2)**

Uniform Mesh Size:



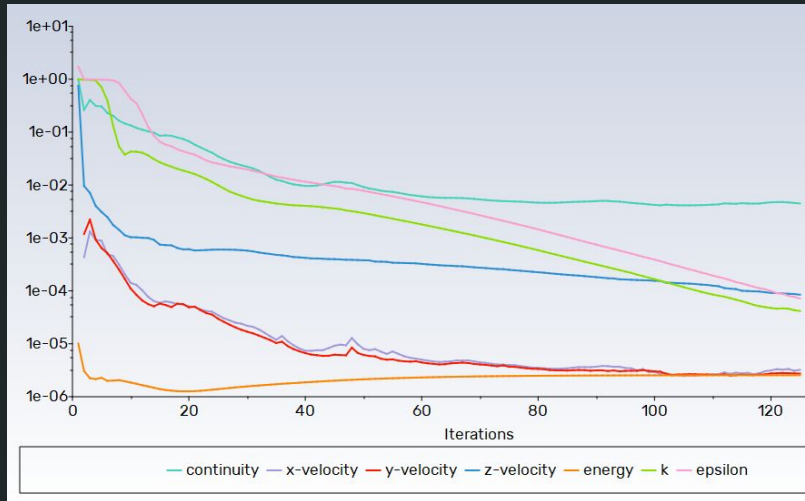
Body Sizing Settings

- Element Size: **1e-3**
- Growth Rate: **1.0**



# Mesh Convergence Study - Wedge: Residual Plot (Body Sizing)

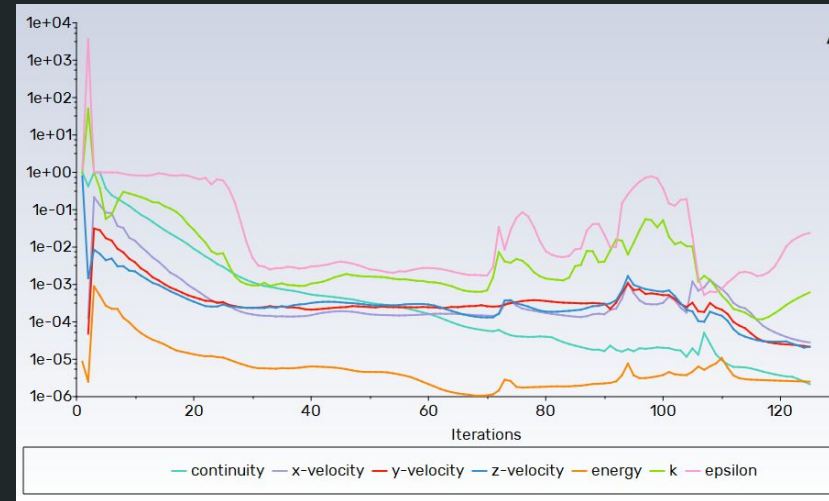
Standard Mesh (Default Growth):



Results:

- Most residuals decrease
- Energy residual slightly increases

Uniform Mesh Size:

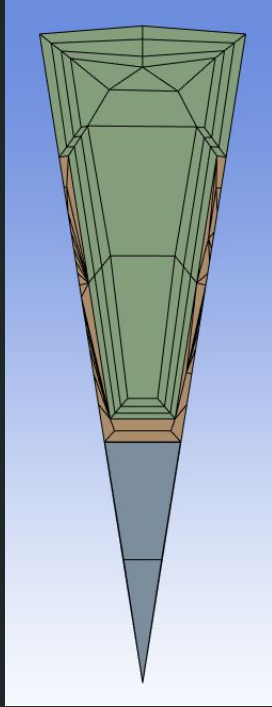


Results:

- Same range of values
- Fluctuations in energy and turbulence

# Mesh Convergence Study - Wedge: Mesh (Face Sizing)

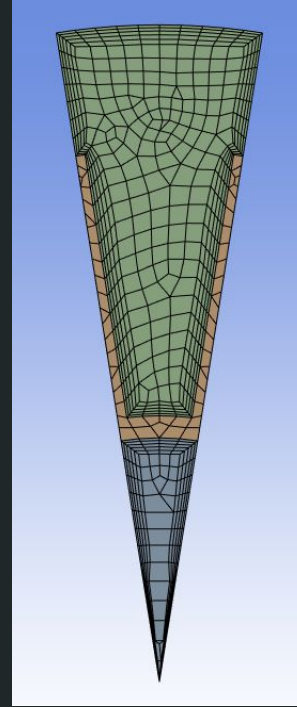
Standard Mesh (Less Inflation):



Face Sizing

- Maximum Layers: **3**
- Element Size: **0.01**

Mesh with Increased Inflation:

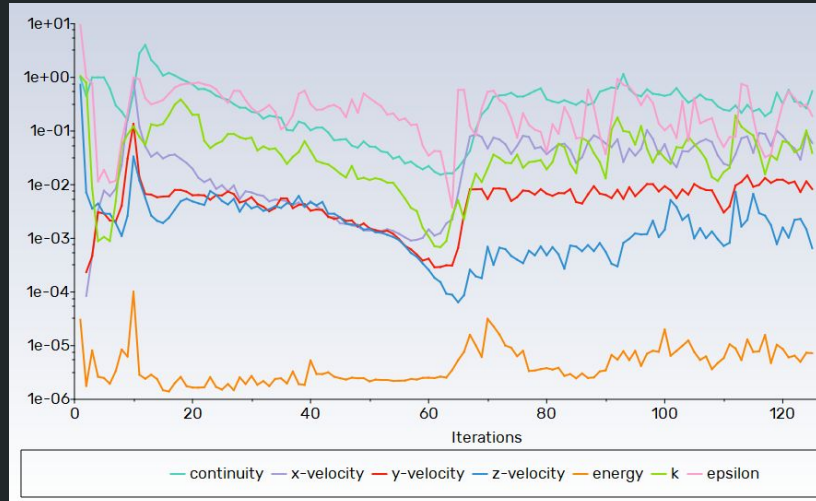


Face Sizing

- Maximum Layers: **5**
- Element Size: **0.001**

# Mesh Convergence Study - Wedge: Residual Plot (Face Sizing)

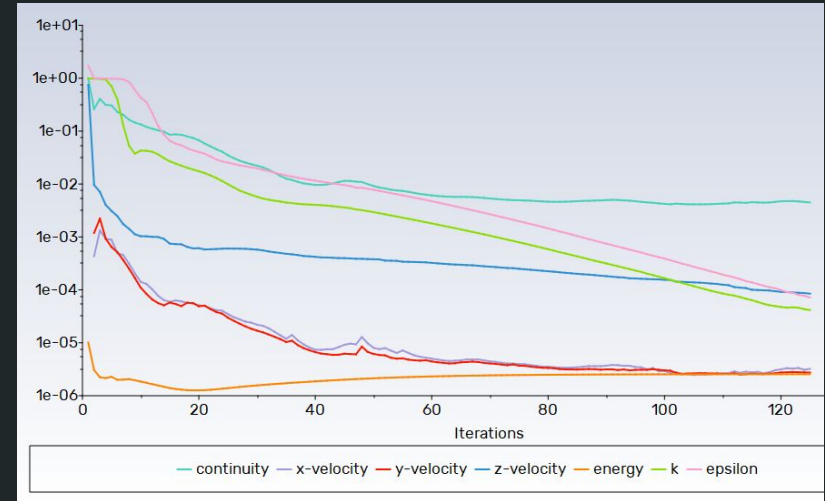
Standard Mesh (Less Inflation):



Results:

- High fluctuations in residuals
- No noticeable decrease

Mesh with Increased Inflation:



Results:

- Same range of values, but smooth residuals and decrease

# Final Mesh Settings - Both Simulations

## ➤ Full Revolution

### Inflation Settings:

- 3 layers around fins and base of inner pipe
- 1 layer on inside of each fin
- 5 layers on steam face
- 3 layers on inner surface of inner pipe

### Edge Sizing

- Divisions along edges of fins, base, and interfaces between fluids and pipes

### Sweep

- 100 divisions across pipe axis (both fluids + inner pipe)

## ➤ Wedge

### Body Sizing

- Element Size: Default (1.5328e-2)
- Growth Rate: Default (1.2)

### Face Sizing

- Maximum Layers: 5
- Element Size: 0.001

# Model setup - Both Simulations

## Boundary Conditions

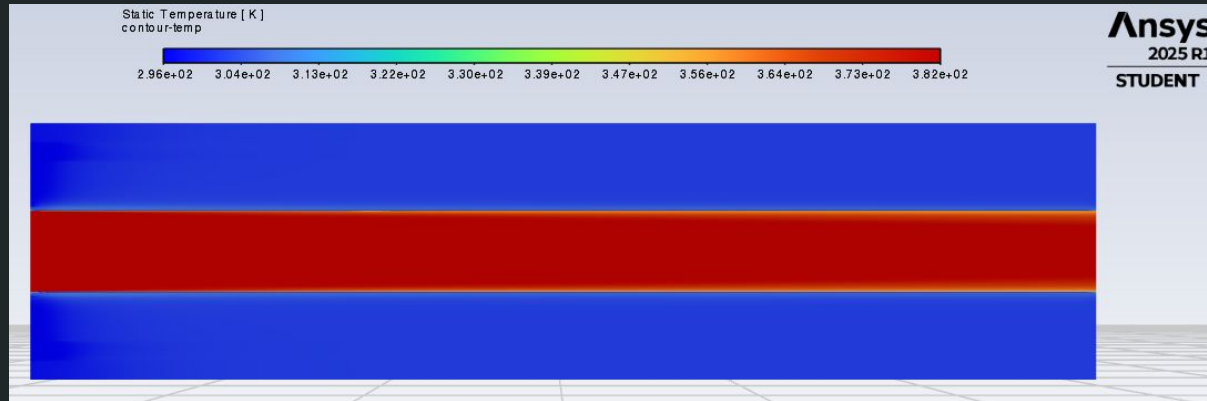
- Heat flux = 0 across outer pipe (adiabatic wall condition)
- Inlet
  - Steam = 5 psi (pressure inlet type)
  - Cold water = 1.324 kg/s (mass flow inlet type)

## Model

- Turbulent (k-epsilon)
- Steady state



# Results - Full Revolution Configuration



Simulation over 1 foot → 303.175 K to 303.320 K

Difference of 0.145 K

Inlet: 295.87 K +  $(0.145 * 41)$  = **301.82 K final temperature of outlet of cold water** (linear extrapolation)

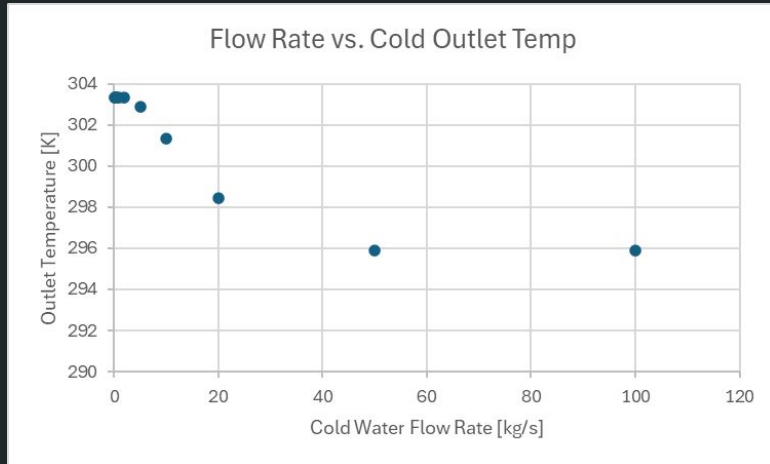
**Lab data = 310.483 K final temperature of outlet of cold water**

# Results - Full Revolution Configuration Parameter Sweep

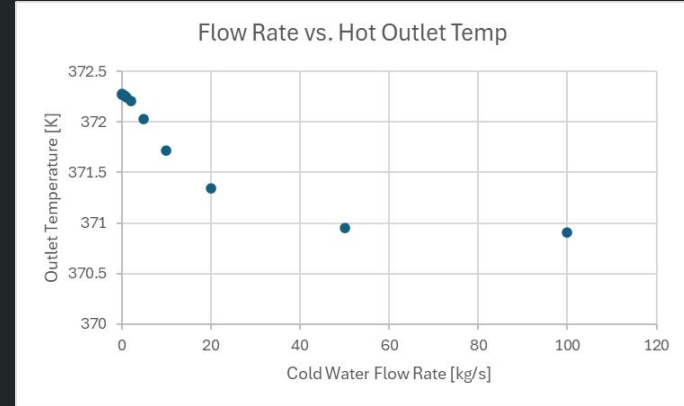
Swept Cold Water Flow Rate

1. Flow Rate vs. Cold Outlet Temp
2. Flow Rate vs. Hot Outlet Temp
3. Flow Rate vs. Heat Transfer Rate

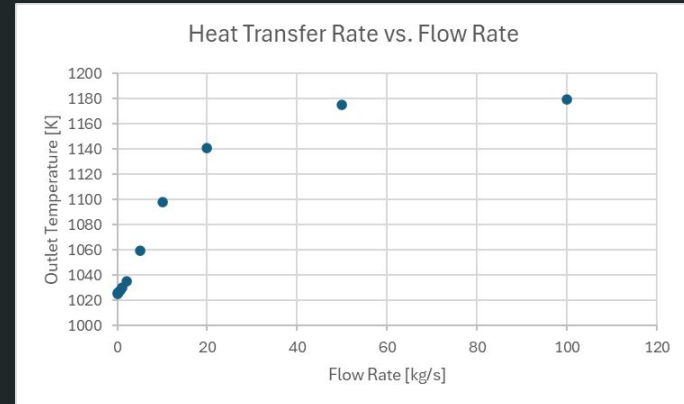
1.



2.

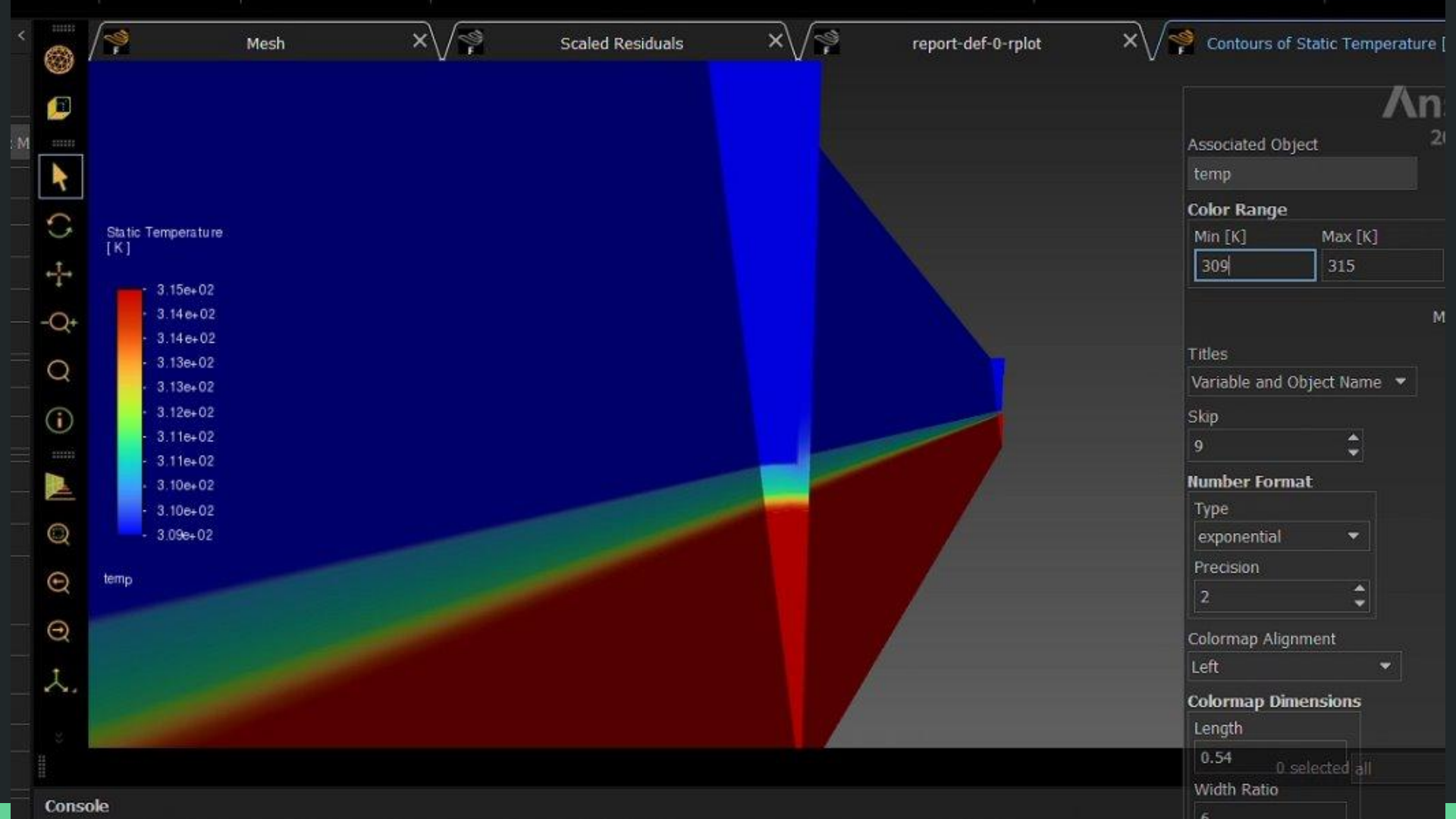


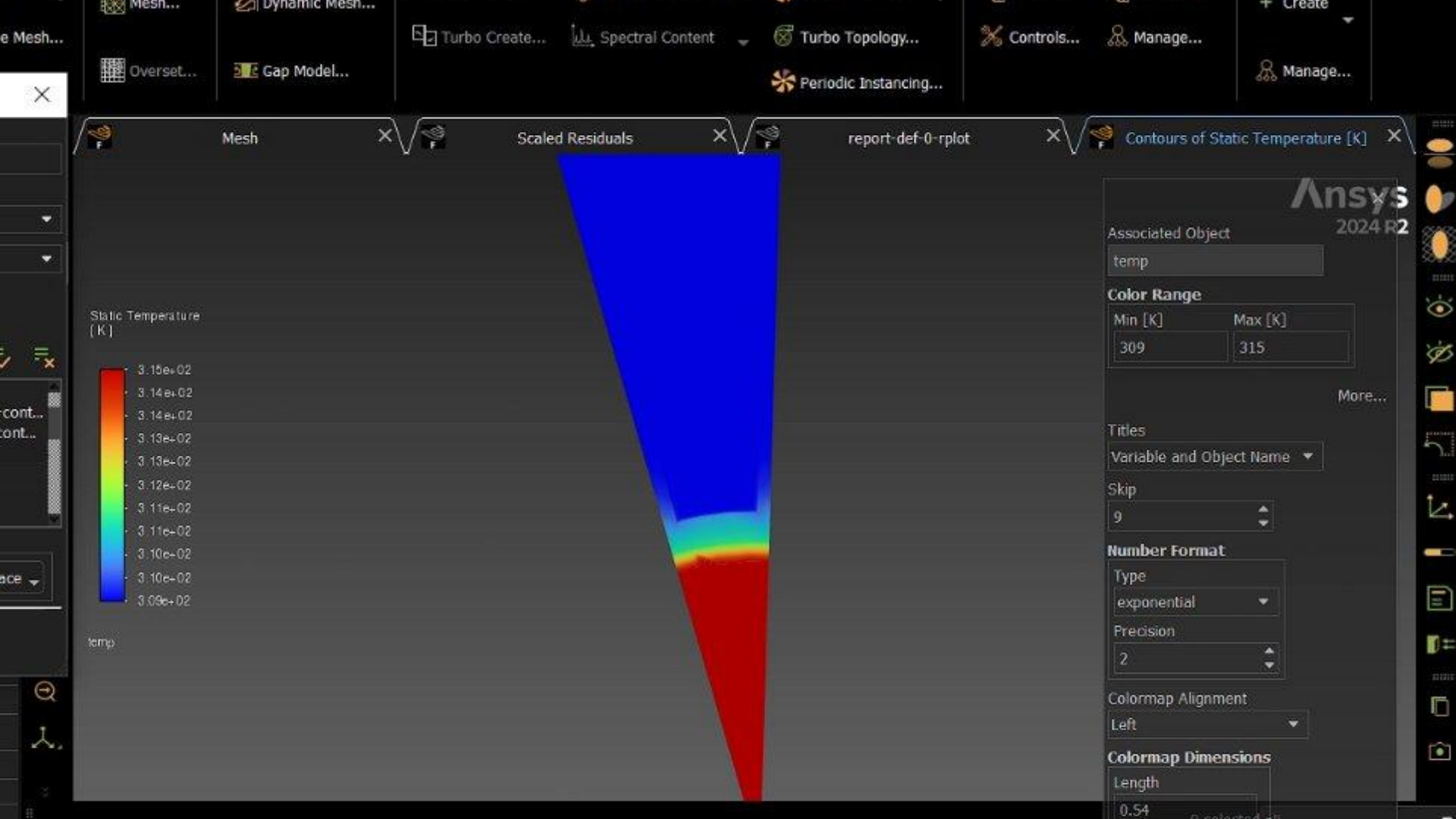
3.



# Results - Wedge Configuration

Number of Fins	Angle	Outlet Temp
40	9	300.03
20	18	301.07
8	22.5	300.43
4	45	300.36
3	60	301.21

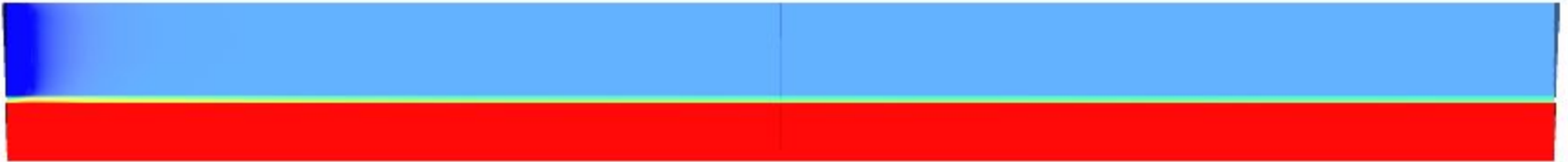
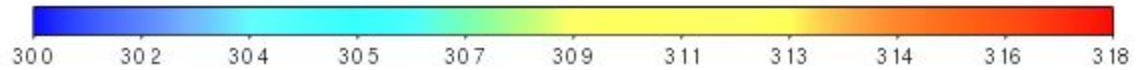






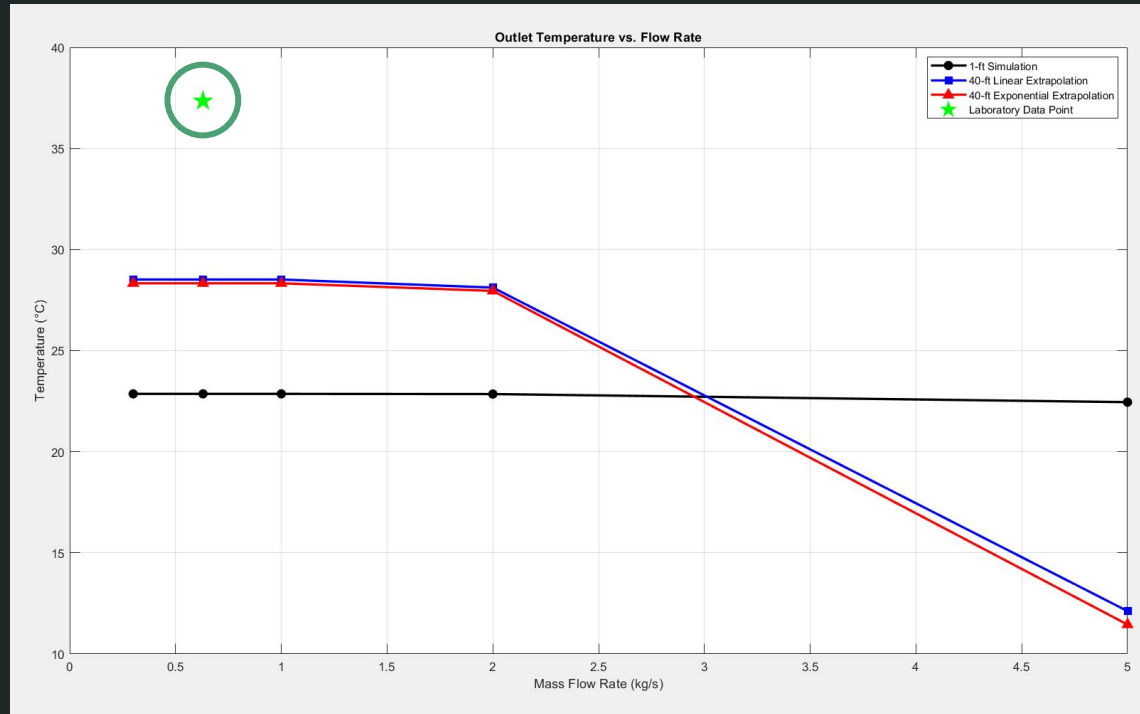
# Results - Wedge Configuration

Static Temperature  
[ K ]



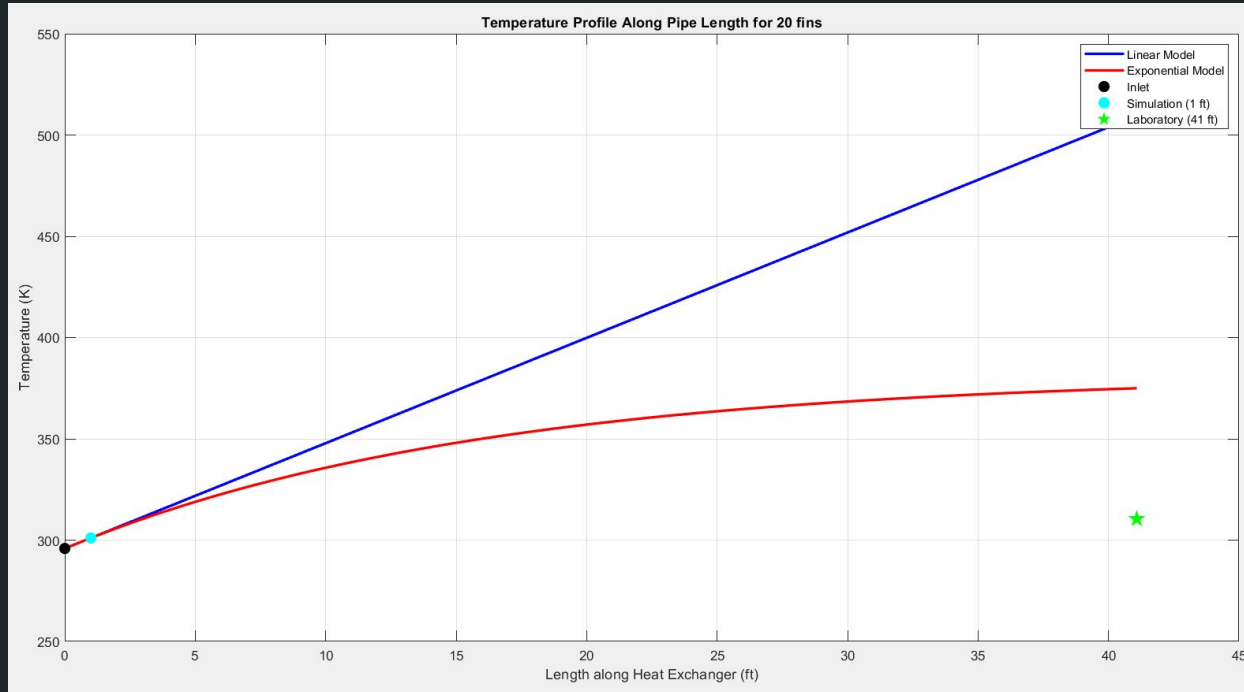
# Ansys Simulation vs. Lab Data - Full Revolution

Extrapolating the 1 foot simulation data to match the 40 feet set up in the ChemE lab



# Ansys Simulation vs. Lab Data

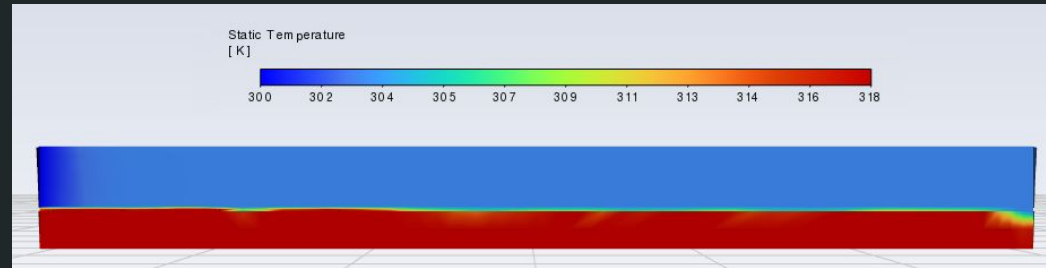
Extrapolating the 1 foot simulation data to match the 40 feet set up in the ChemE lab



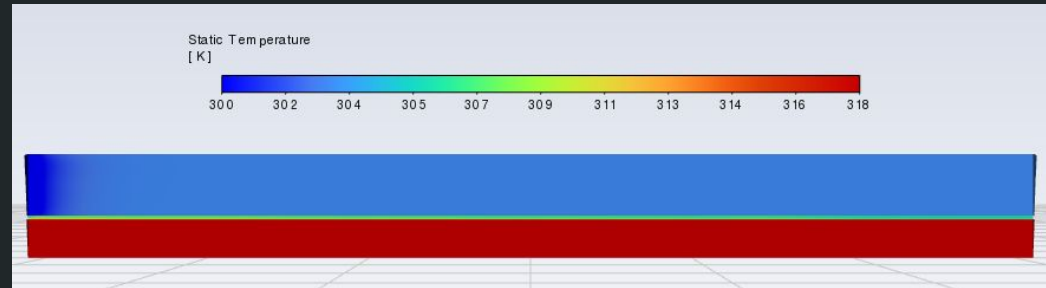
End

# Mesh Contours - Wedge

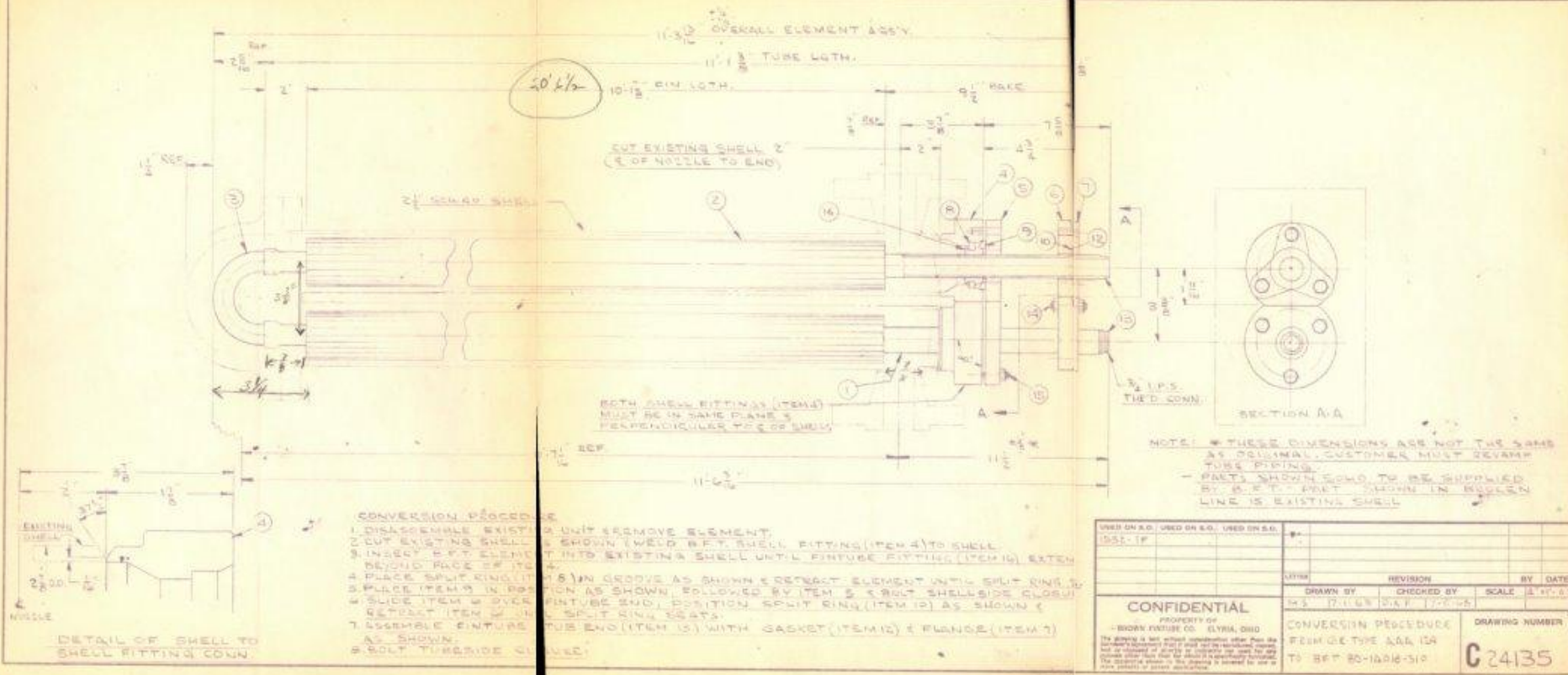
Standard Mesh (Less Inflation):



Uniform Mesh Size:





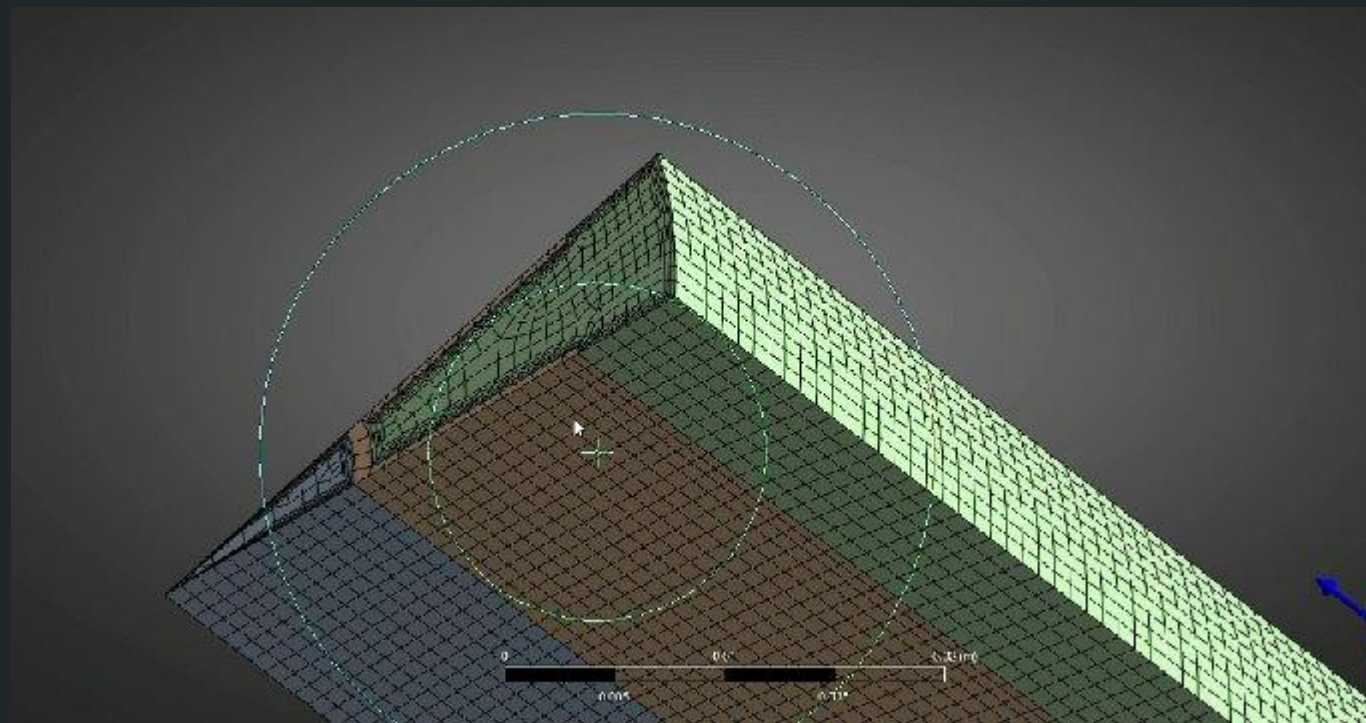


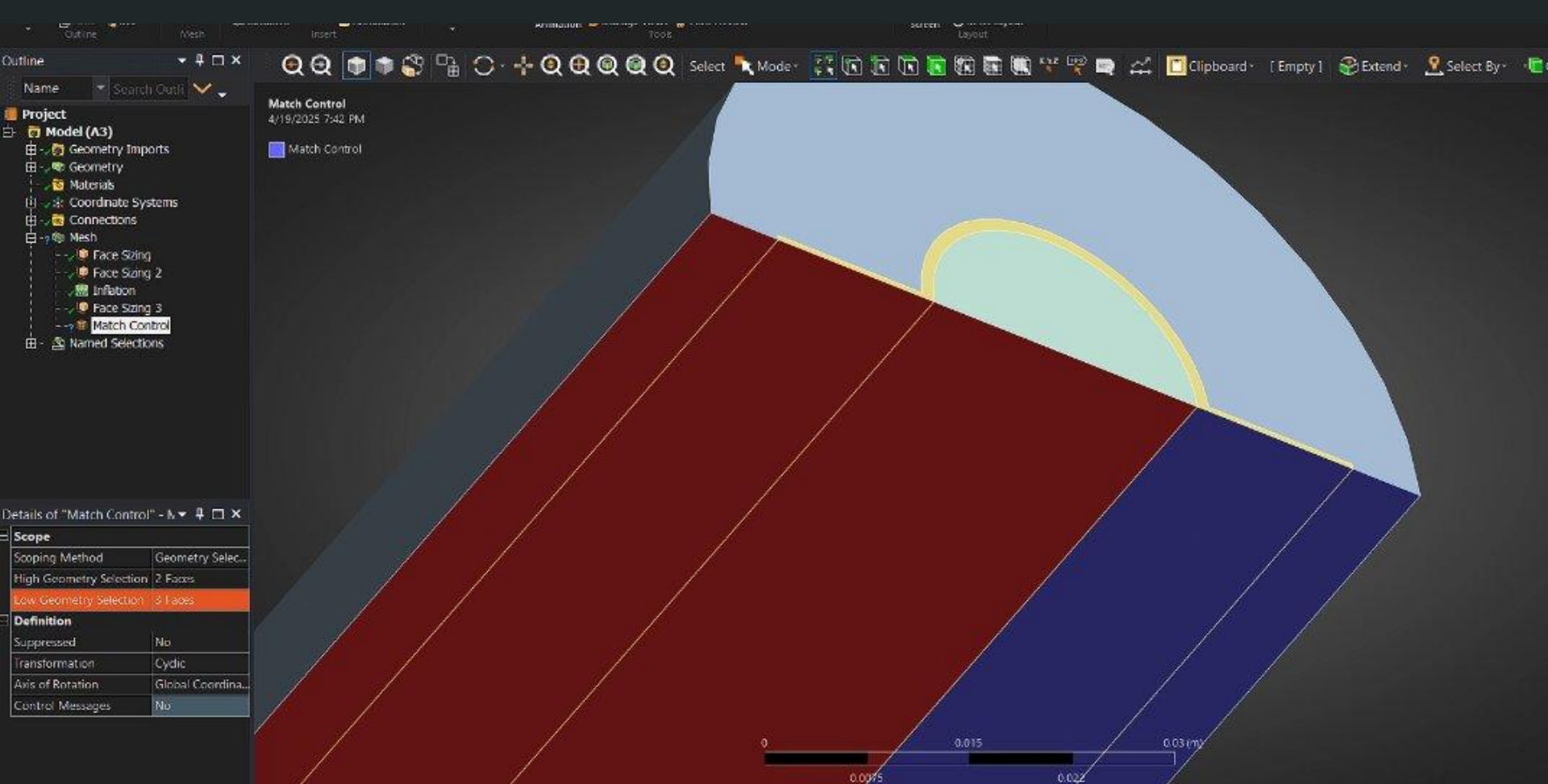
THE DRAWING IS NOT WITHOUT CONSIDERING OTHER THAN THE INTELLECTUAL AGREEMENT THAT IT SHALL NOT BE REPRODUCED, COPIED, OR IN ANY MANNER BEING USED FOR ANY PURPOSE OTHER THAN THAT FOR WHICH IT IS SPECIFICALLY SUBMITTED. THE ATTACHING SIGNATURE IN THE DRAWING IS COVERED BY ONE OR MORE PATENTS OR PENDING APPLICATIONS.

Technical drawing of a double pipe heat exchanger. The top part shows a cross-section of the U-tube bundle with dimensions: Overall Length  $1' 10"$ , Tube Length  $1' 1"$ , and Fin Length  $9 \frac{1}{2}"$ . The bottom part shows a side view of the bundle with dimensions:  $1 \frac{1}{8}"$  for the tube diameter,  $11 \frac{1}{32}"$  for the bundle height, and  $3 \frac{3}{8}"$  for the spacing between tubes. A small detail of a tube and fin is shown in the bottom right corner.

[illegible]

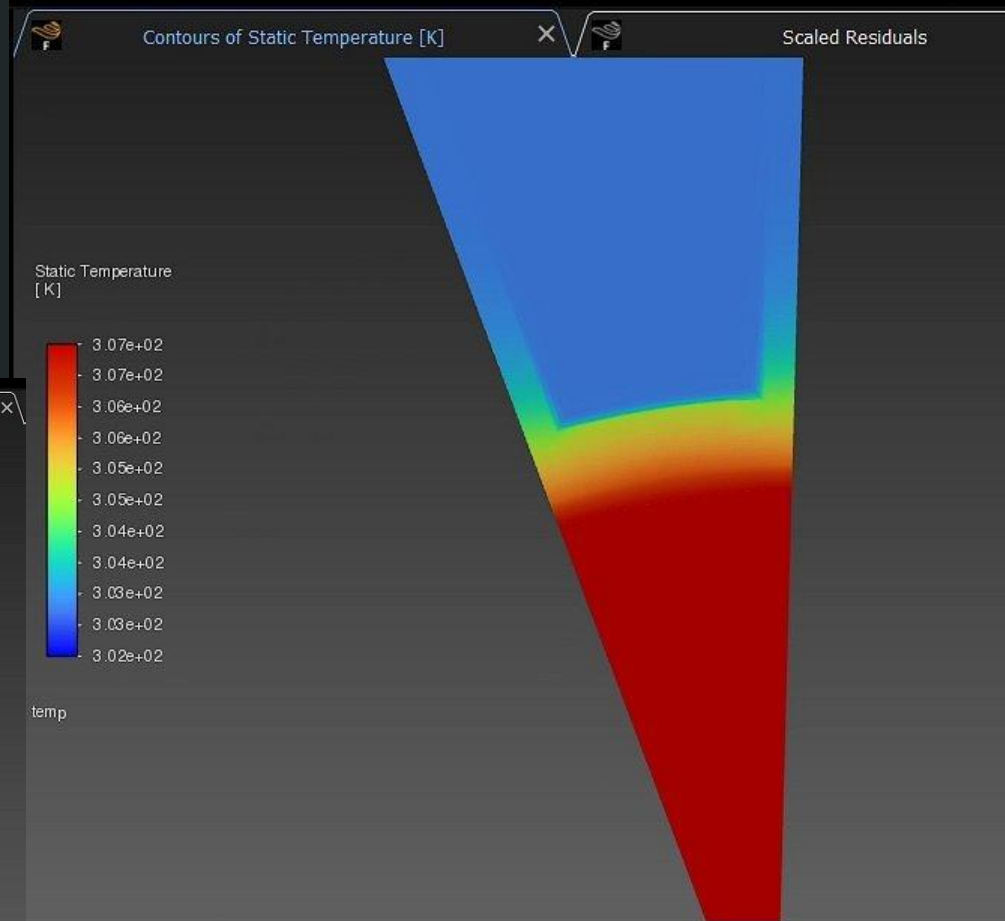
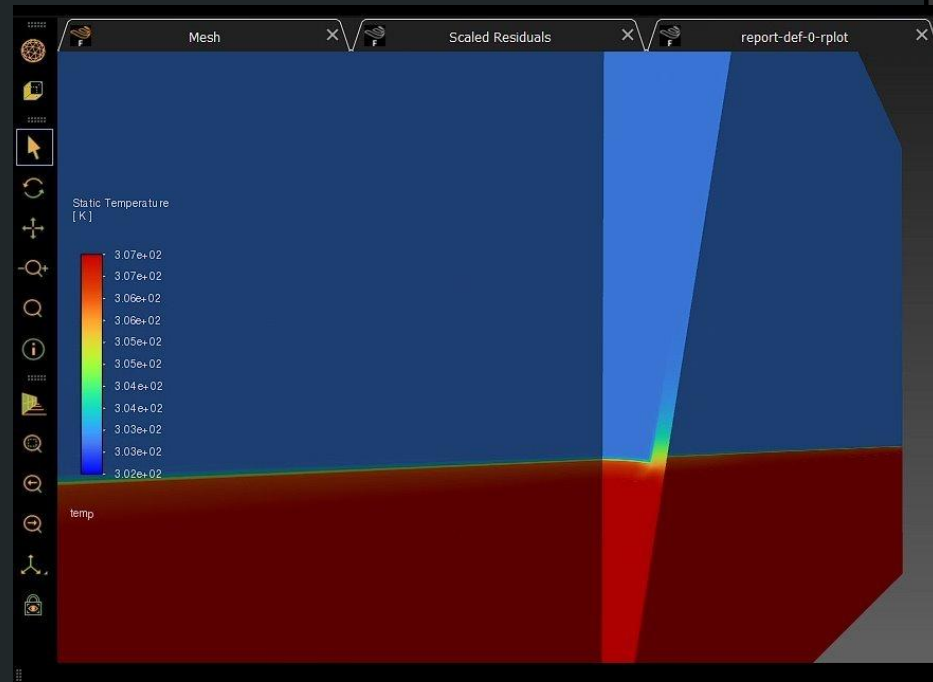
- Mesh
  - Face Spring
  - Face Spring 2
  - Inflation**
  - Face Spring 3
  - March Control
- Named Sections
  - cool\_fluid
  - hot\_fluid
  - plac
  - hot\_inlet
  - cool\_inlet
  - adiabatic wall
  - cool\_outlet
  - hot\_outlet
  - periodic\_steam\_right
  - periodic\_steam\_left
  - periodic\_in\_right
  - periodic\_in\_left
  - periodic\_under\_inlet
  - periodic\_water\_left



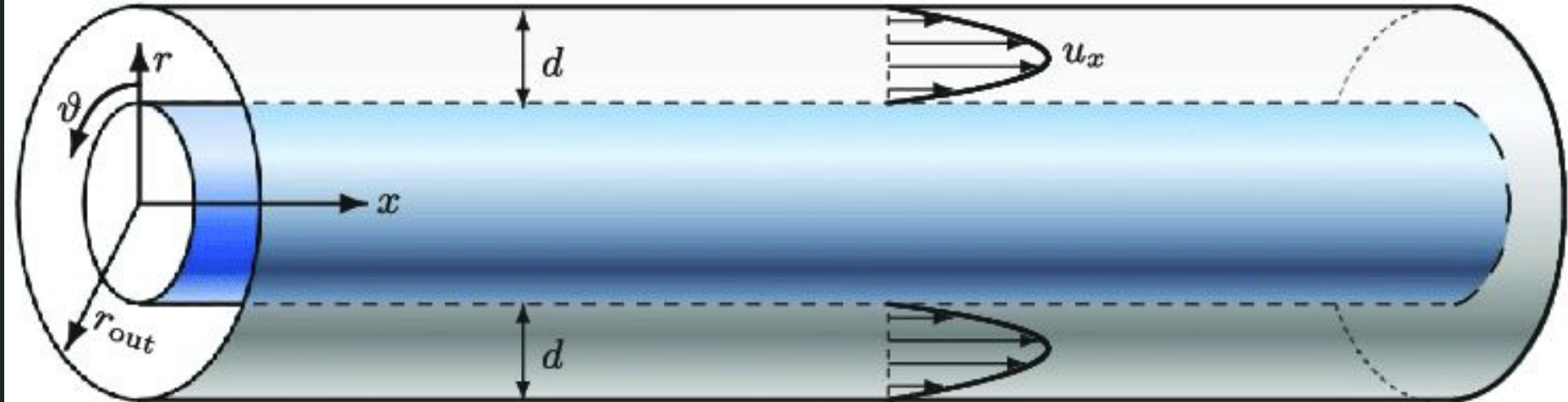




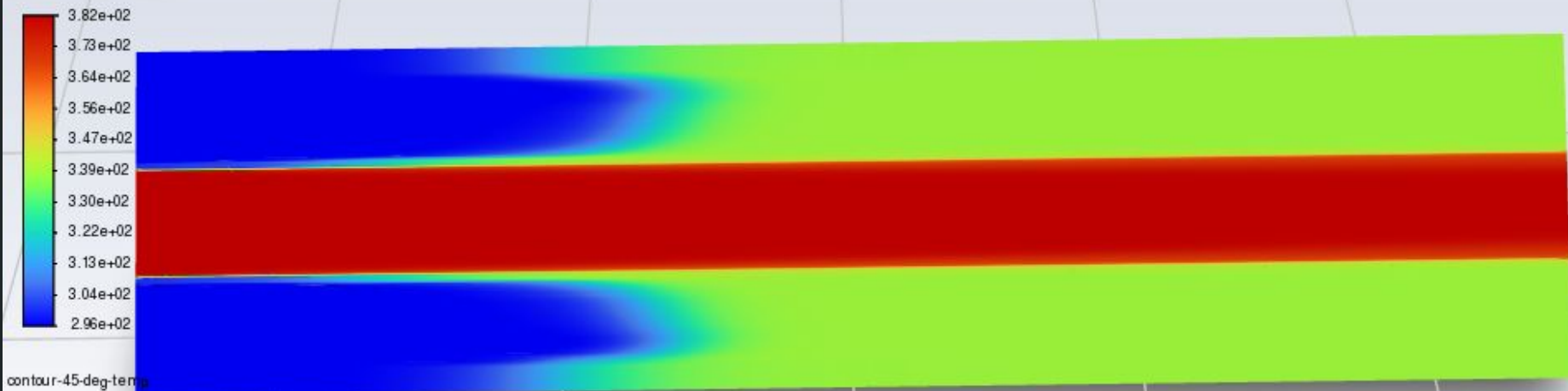
These were with the wrong dimensions but they're images of a slice midway through 1ft with 20fins







Static Temperature  
[ K ]



Outlet Temperature vs. Number of fins

